DOCUMENT INFO

DocID:

00000226

Filename:

58603-1999-02-18-COR-01 (Proposed Conditions for Approval of Aboveground

Temporary Storage Tank - Gorman).pdf

Fire Protection Consultants Building & Fire Code Specialists 115-14 Beach Channel Drive, Rockaway Park, N.Y. 11694 Phone: 718-474-3400 Fax No. 718-945-5931

The City of New York - Fire Department Bureau of Fire Prevention 9 MetroTech Brooklyn, NY 11201-3857 Feb. 18, 1999

Attn: Mr. James Hansen, P.E.

Director of Engineering and
Technical Management Standards



Re: MOTTVA Enterprises, LLC (Shell oil Co.)
25 Paidge Ave. Brooklyn, NY
B.S. # 980089
F.P. Index # 9805103A
Response To F.D. Letter of January 26, 1999

Dear Mr. Hansen

Following phone conversation and conference calls from Mr. Anthony Sigona, P.E. of Department of Environmental Conservation and Douglas Lessing of Handex with your office, we respectfully request reconsideration for approval of a 275 gallons aboveground tank for temporary storage of recovered hydrocarbons at the referenced bulk oil terminal with the following conditions:

- 1- The proposed tank shall be installed in a concrete curb in addition to 110% secondary containment provided with the tank
- 2- The tank shall be provided with a high level alarm which would shut down the pumps supplying recovered product into the tank as shown on DWG. 4 of 6
- 3- The proposed high level alarm shall be monitored at the dispatch office which is manned 24 hours a day, seven (7) days a week
- 4- A 20 lb. Dry chemical extinguisher shall be installed in the vicinity of the tank. This is in addition to the existing foam monitor and yard hydrants located within 50 feet of the tank.

Walter T. Gorman, P.E., P.C.

Consulting Engineers

Fire Protection Consultants Building & Fire Code Specialists

Phone: 718-474-3400

115-14 Beach Channel Drive, Rockaway Park, N.Y. 11694 Fax No.718-945-5931

> Feb. 18, 1999 Page 2 of 2

We appreciate reconsidering the denial for the installation of the proposed tank. Should you have any question, please feel free to call my office.



cc: Mr. Anthony Sigona, P.E. - DEC

Mr. Mario D'Antonio, Mgr. - Motiva

Mr. Doug Lessing - Handex

Mr. Abbas Family, P.E., Dir.- WTG PE PC

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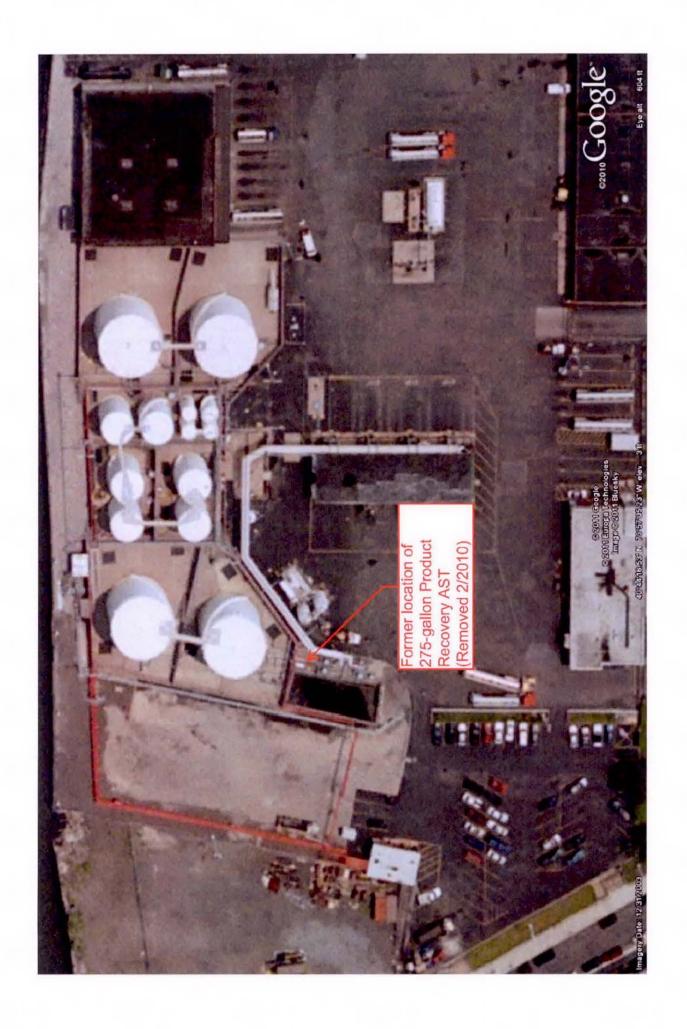
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58603-2011-11-15-FIG-01 (Former AST

Location - SCI).pdf



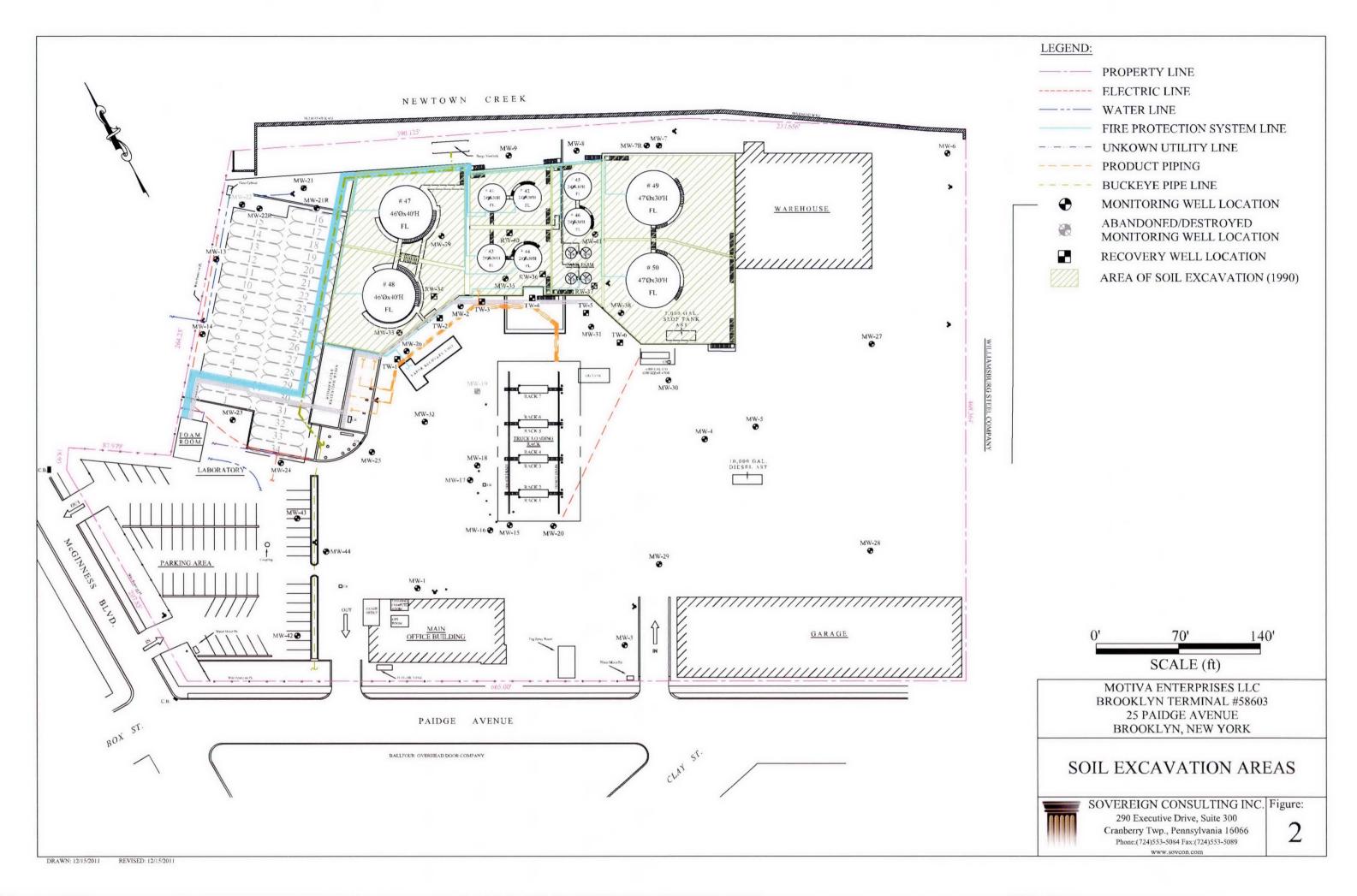
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58603-2011-11-15-FIG-01 (Former Product Recovery AST - SCI).pdf



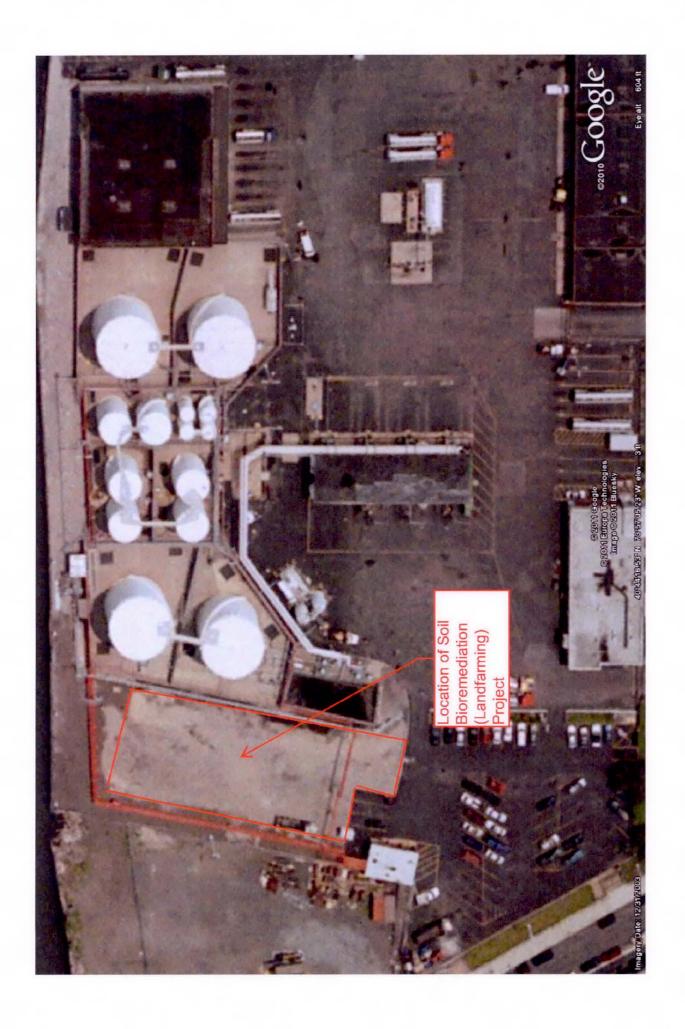
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58603-2011-11-15-FIG-01 (Landfarming

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Filename:

58603-2009-07-20-PER-01 (SPDES Permit

Renewal Application - Motiva).pdf



July 20, 2009

New York State Department of Environmental Conservation **Division of Environmental Permits** Bureau of Environmental Analysis 625 Broadway Albany, NY 12233-1750

SUBJECT: SPDES RENEWAL APPLICATION MOTIVA ENTERPRISES LLC -**BROOKLYN TERMINAL** DEC NO. 2-6101-00105/00019 **SPDES NO. NY0006131**

Dear Madam or Sir:

Enclosed is State Pollutant Discharge Elimination System (SPDES) Renewal Application for the Motiva Enterprises LLC Brooklyn Terminal located at 25 Paidge Avenue, Brooklyn, New York 11222.

Please contact Ms. Jennifer Bothwell at (860) 749-2839 or me at (856)810-7720 if you have any questions about the information included in the enclosed application.

Sincerely:

David L. Bier

Field Environmental Coordinator

lavid 1 Bier

Enclosure

CC: NYSDEC Region 2 – John Cryan - Regional Permit Administrator J. Lintz/F. Signareillo - Motiva - Brooklyn, NY

NEW YORK STATE DEPARTMENT OF ENVIRONMENTAL CONSERVATION State Pollutant Discharge Elimination System (SPDES) NOTICE / RENEWAL APPLICATION / PERMIT



Please read ALL instructions on the back before completing this application form. Please TYPE or PRINT clearly in ink.

PART 1 - NOTICE

04/15/2009

Permittee Contact Name, Title, Address

Facility and SPDES Permit Information

MOTIVA ENTERPRISES LLC MARIO D'ANTONIO, JAMES W. LINTZ

25 PAIDGE AVE

BROOKLYN

NY 11122-1281

Name: MOTIVA MARKETING TERMINAL

Ind. Code: 5171 County: KINGS

DEC No.: 2-6101-00105/00019

SPDES No.: NY 000 6131
Expiration Date: 02/01/2010
Application Due By: 08/05/2009

Are these name(s) & address(es) correct? if not, please write corrections above.

The State Pollutant Discharge Elimination System Permit for the facility referenced above expires on the date indicated. You are required by law to file a complete renewal application at least 180 days prior to expiration of your current permit. Note the "Application Due By" date above.

CAUTION: This short application form and attached questionnaire are the only forms acceptable for permit renewal. Sign Part 2 below and mail only this form and the completed questionnaire using the enclosed envelope. *Effective April 1, 1994 the Department no longer assesses SPDES application fees.*

-if there are changes to your discharge, or to operations affecting the discharge, then in addition to this renewal application, you must also submit a <u>separate</u> permit modification application to the Regional Permit Administrator for the DEC region in which the facility is located, as required by your current permit. See the reverse side of this page for instructions on filing a modification request.

PART 2 - RENE	WAL APPLI	CATION	
CERTIFICATION: I hereby affirm that under penalty of perjury that the inf the best of my knowledge and belief. False statements made herein are pun			
JAMES W. LINTZ	TE	ERMINAL COMPLEX	MANAGEA
Name of person signing application (see instructions on back)	Title	1/20/09	
Signature	Date		
PART 3 - PERMIT (Below	v this line -	Official Use Only)	
Effective Date:	 Address:	NYSDEC - Division of Environmental Ar	
Permit Administrator		625 Broadway, Albany, NY	12233-1750
Signature	Date		
This permit together with the previous valid permit for together with the previous valid permit for together authorization to discharge wastewater in accord previously issued valid permit, modifications thereof or issued attached hereto. Nothing in this permit shall be deemed to permit on the grounds specified in 6NYCRR §621.14, 6NYC issued or which arise thereafter.	ance with a as part of thi waive the D	all terms, conditions and limitalistics permit, including any special epartment's authority to initiate	ations specified in the I or general conditions a a modification of this
Attachments: General Conditions dated/_			



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Please enter the	DEC Number:	į
numbers from your		
current permit:	SPDES Number: NY	

SPDES RENEWAL APPLICATION QUESTIONNAIRE

THIS PAGE MUST BE COMPLETED AND RETURNED WITH YOUR COMPLETED APPLICATION

Pleasé	TYPE or PF	RINT neatly using a	dequate pressure to ma	ake ALL	copies legible.	Keep a c	opy for yo	our records.	
1.	Has the SF	PDES permit for yo	ur facility been modified	in the p	ast 5 years		YES	M NO	.•
2.	Best Mana minimizes material str	gement Practices (the potential for rel orage areas; plants	icture, store, handle or o BMP) plan requirement ease of pollutants to rec site runoff, in-plant trans aste disposal areas.	s for to	dic or hazardous vaters from suct	substan ancillary	ces. A BN industrial	MP plan prev Lactivities, in	ents or . cluding
	Does your current per		illary activities as descri	bed abo	ve, which are no		by BMP r YES	equirements NO	in your
Please	indicate wh	ich of the following	best describes the situ	ation at	your facility:	•			•
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			"Self Evaluation List" h implete modification ap					s facility nee	ds to be
	need to be "Request F Modification The items	e Modified. I have For SPDES Application application. See on the "Self Evalua	"Self Evaluation List" he requested the appropriation Forms" (included in a The "Request For SPI ation List" have left me following general conce	riate for this rene DES App unable t	ms by phone O wal package) to lication Forms" o conclude whe	R I have allow me page for	complete to submit a toll free	ed and attac apermittee- 800 numbe	hed the initiated
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Shell/Motiva 0008144

<u>ATTACHMENT</u>

SPDES RENEWAL APPLICATION SUPPLEMENTAL FACILITY INFORMATION:

FACILITY: Motiva Enterprises LLC

Brooklyn Terminal 25 Paidge Avenue

Brooklyn, NY 011222-1281

SPDES NO. NY0006131

DEC NO. 2-6101-00105/00019

<u>Background</u>: The Motiva Brooklyn Terminal has an Action Level Monitoring requirement for benzene, ethylbenzene, toluene & xylene(s) (BTEX) in the current permit. Based on a review of BTEX Action Level Monitoring Data, the NYSDEC Region 2 Office requested that facility improvements be made to address BTEX concentrations in the discharge. After evaluating the facility operations, Motiva will be making the following improvements to eliminate BTEX in Outfall No. 001:

2009 Improvements (4th Quarter):

- The terminal gasoline truck loading rack canopy will be extended to cover the entire loading area, eliminating stormwater entering the area and eliminating potential product impact to rainwater flowing to Outfall 001.
 - The stormwater collection strip-drains at the perimeter of the loading area will be eliminated and a roll-over containment berm will be installed around the loading area to provide containment and prevent surface runoff of rainwater from entering the loading containment area.
 - Drainage from the containment area will be disconnected from the oil/water separator that flow to Outfall 001 and will be connected to an underground (vaulted) containment tank. The 6,000 gallon containment tank will contain the volume of the largest truck product compartment for SPCC Plan purposes.
 - Non-contact stormwater diverted from the loading area will continue to flow to Outfall 001 in the same quantities as before.

Note: These improvements will eliminate stormwater entering the truck loading area and prevent BTEX impacted water from entering the terminal drainage system that flow to Outfall 001.

Proposed 2010 Improvements:

 An engineering evaluation is underway for the proposed replacement of the terminal's main oil/water separator. This work is being done to update an existing oil/water separator, which is still in good operating condition. The replacement is part of normal facility operational maintenance. There will be no significant change of the separator size since the terminal operations remain the same and water discharge volume remain the same.

Request for Removal of MTBE Limit - The terminal has not received, stored or loaded gasoline containing MTBE since 2003. Based on this, Motiva requests the Department consider removing the MTBE parameter/limit from the permit.

BEST MANAGEMENT PRACTICES & STORMWATER POLLUTION PREVENTION PLAN

MOTIVA ENTERPRISES LLC

BROOKLYN TERMINAL

Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222

Tel. (718) 383-4066

FACILITY INFORMATION PAGE

Facility Information:

• Facilities Addressed in this Plan:

Owner/Operator – Motiva Enterprises LLC

Brooklyn Terminal

Name & Address of Owner:

Motiva Enterprises LLC 910 Louisiana Street Houston, TX 77002

 Designated person accountable for the implementation of this Plan at the facility sated above: James W. Lintz – Terminal Manager Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222

Tel. (718) 383-4066

STORMWATER POLLUTION PREVENTION PLAN

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STORMWATER POLLUTION PREVENTION PLAN

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STORMWATER POLLUTION PREVENTION PLAN

REVISION RECORD

Note: It is the responsibility of the holder of this plan to insure that all changes and updates are made. The holder should:

- Remove and discard obsolete pages.
- Replace obsolete pages with updated pages.
- Record each revision on this form.

	Affected Pages	Description of Change(s)						
Change Date	Numbers		Name					
July 2000	Entire Plan	Update per SPDES Permit	D. Bier					
Oct. 26, 2004	Entire Plan	Review of Terminal & Operational changes – None needed at this time.						
July 2009	Cover, ii, v,	Update	D. Bier					
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	EXAMPLE							
01/01/99	1-1 thru 1-4, 5-2	Update						

Motiva Enterprises LLC Brooklyn Terminal

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BMP/SWPPP 2009 Update

1.1 PURPOSE

This document was prepared in accordance with the requirements set forth in the Brooklyn Terminal SPDES Permit No. NY 0006131, Special Conditions – Best Management Practices. The Best Management Practices (BMP) Plan discusses best management practices, inspections and evaluations to be utilized to prevent pollution of stormwater runoff. The plan also discusses response actions that will be taken in the event of a chemical or oil discharge and the key personnel involved in cleanup. This BMP Plan is formatted to also serve as Stormwater Pollution Prevention Plan (SWPPP).

1.2 PLAN REVIEW AND UPDATE PROCEDURES

Facility Management will coordinate review and update procedures. The following changes will require revisions and updates to the BMP Plan:

- Commission or decommission of tanks.
- Replacement, reconstruction or movement of tanks.
- Construction or demolition that might alter secondary containment structures and or drainage systems.
- Revisions of standard operating or maintenance procedures at the Facility.
- A change in ownership.

The Facility shall amend the plan as necessary to address any sources or potential sources of pollution identified as a result of a Comprehensive Site Compliance Evaluation conducted according to Section 5.2 of this plan. The amended plan and all actions required by the plan shall be completed within 60 days of the date the Facility becomes aware or should have become aware that any of the conditions listed above has occurred.

1.3 PLAN DISTRIBUTION

Copies of the Plan shall be maintained at the Brooklyn Terminal. A copy will be available to the New York State Department of Environmental Conservation (NYSDEC) upon request.

2.0 GENERAL INFORMATION

2.1 TYPE OF FACILITY

The facility is an onshore storage terminal that receives and distributes gasoline, ethanol and gasoline additives. Specific facility information is provided in the terminal's Integrated Contingency Plan (ICP).

2.2 POLLUTION PREVENTION TEAM

The Terminal Manager assumes the responsibility for implementation, maintenance and revision of the BMP/SWPP Plan. The Terminal Manager and Terminal Superintendent/Supervisor serve as members of the BMP/Stormwater Pollution Prevention Team. Additional terminal and environmental personnel as designated by the Terminal Manager will assist in the development and implementation of the BMP/SWPP Plan as necessary. Emergency Contacts for the Terminal are provided in the ICP. Roles and responsibilities of the company responders are also detailed in the ICP.

2.3 EXTERNAL CONTACTS

The Facility will ensure that required notifications are made to federal, state and local agencies when appropriate. Internal and External Reporting requirements are outlined in the ICP.

2.4 SURFACE WATER PROXIMITY

The Facility is positioned adjacent to the Newtown Creek. The Newtown Creek empties into the East River. Maps and charts of the surface water bodies are incorporated in to the ICP.

2.5 SURFACE DRAINAGE

The facility is located on a relatively flat area. Drainage from the contained areas is addressed below. The Terminal Spill Prevention Control and Countermeasure (SPCC) Plan (the SPCC Plan is part of the ICP) also addresses the rate and direction of flow from potential spill areas. Rainfall onto the soil surfaces outside of the Terminal's operational area infiltrates into the soil or flows toward the Terminal's operational areas. All operational areas of the Terminal drain to the oil/water separator for treatment prior to discharge from the SPDES Discharge No. 001. Effluent monitoring is conducted for the following parameters:

- Flow
- Oil & Grease
- pH
- Benzene, Toluene, Ethylbenzene, Xylene(s) and MTBE

Drainage from Diked Areas

 The drainage from the diked storage areas is controlled by individual manual valves that are kept closed except when draining stormwater to the oil/water separator. The diked containment basins are isolated from the adjacent basins by dikes and the

Motiva Enterprises LLC Brooklyn Terminal

2-1

BMP/SWPPP 2009 Update manual valves. Water, which is drained from these areas, is directed to the oil/water separator system and eventually discharged at Outfall No. 001 under the Facility's SPDES Permit. All water to be discharged is visually inspected for presence of oil/sheen prior to the opening any valves. Any presence of oil/sheen is immediately reported to the Terminal Manager or the Terminal Supervisor.

- The dike walls and containment floors are constructed of reinforced concrete and the drainage system is constructed of a combination of catch basins and drainage piping.
 Drainage is restricted by valves as necessary to isolate the stormwater in the area which it accumulates.
- The terminal is fenced and areas are lighted to provide security and unauthorized tampering with equipment.

Drainage From the Undiked Areas

- Drainage from the truck loading rack flows to a primary oil/water separator that then discharges to the terminal's main oil/water separator.
- Rainwater accumulation on soil and grassy areas is allowed to percolate or evaporate.
 All areas within the terminal where stormwater can be potentially impacted drain to controlled operational areas or containment areas.
- Rainwater accumulation from the paved yard area collects in catchbasins and then drains
 to the main oil/water separator. The oil/water separator system provides treatment prior
 to discharge through the SPDES Outfall No. 1.

Areas that may reasonably be expected to affect stormwater quality at the site and drainage routes from these areas, are shown in the SPCC Plan and the FRP. The plans also include prevention measures that minimize the potential for surface water contamination by terminal operations.

3.0 POTENTIAL POLLUTANT SOURCES

3.1 IDENTIFICATION OF POTENTIAL POLLUTANT SOURCES & BEST MANAGEMENT CONTROLS

There is limited potential for the materials stored or processed on site to impact surface waters since most of the materials are contained within closed systems, such as tanks, pipes and other equipment. The significant materials that are handled and/or stored at the Terminal include: gasoline, ethanol and gasoline additives. In addition to these materials, small amounts of maintenance related materials are stored and used. These materials are stored inside buildings to prevent any contact with stormwater. Diesel fuel is not stored at the Terminal, but is contained in fuel tanks of the trucks that load at the Terminal. Figure 3.1 below is a narrative description of the materials, how the materials are handled and the Materials Management Practices (BMPs) empolyed to reduce the potential of these sources to contribute pollutants to stormwater discharges.

3.2 SPILLS & LEAKS

There have been no spills of toxic or hazardous substances by Motiva Enterprises at the Terminal. Spills that occur are reported and are to be documented as prescribed in the ICP. Please see the ICP for a listing of any potential spills or leaks.

3.3 MONITORING PROGRAM

Stormwater is monitored in accordance with the Terminal's SPDES Permit (No. NY0006131). Sampling data is reported in the monthly Discharge Monitoring Reports (DMRs) with copies of the reports and data kept in the Terminal's files. The monitoring parameters are noted in Section 2.5 of this plan.

FIGURE 3.1

POLLUTANT SOURCE IDENTIFICATION AND MATERIALS MANAGEMENT PRACTICES

Material	Method/Location of Storage or Disposal	Materials (Management Practices	Stormwater Diversion Control Measures	Stormwäter Freatment
Gasoline and No. 2 Diesel Fuel	Gasoline: Pipeline, Dock lines and terminal transfer lines and hoses. Diesel Fuel: transfer lines, dispenser and hoses.	Corrosion protection, annual pressure testing, regular inspections as per SPCC Plan and lines equipped with gate valves/check valves	Lines Within contained area which flows to oil/water separator	Yes. Except lines outside terminal containment and operational area
Gasoline, No. 2 Diesel Fuel and Gasoline Additives	(19) Aboveground Storage Tanks located throughout Facility	Corrosion protection, liquid level monitoring devices, high level alarms, regular inspections	Secondary containment berms	Yes, oil/water separator
Gasoline and Gasoline Additives	Truck Loading rack	Loading/unloading policy, warning signs, air brake interlock system, roof. See SPCC Plan for additional details	Depressed area surrounded by curbing drains to oil/water separator	Yes, oil/water separator
Fire Fighting Foam	Storage Tank and containers at foam room	Regular inspections and covered storage	Sealed containers	No
Drums (new material)	Stored at warehouse	Visual inspections	Stored indoors	No
Gasoline, No. 2 Diesel Fuel and No. 2 Fuel Oil (Heating Oil	Dock (dock connection containment)	Hose testing, unloading procedures, USCG Dock Ops Manual, Best Management Practices (BMP's)	Collection trays/Containment basins	Yes, water to oil/water separator
Maintenance Materials (Lubricants. Detergents, Etc.)	Stored in small containers	Stored inside buildings	Materials covered and/or sealed	No
Waste Materials	In waste storage area and temporary satellite areas	Weekly inspection, suitable containers	Materials covered and/or sealed	No

4.1 GOOD HOUSEKEEPING

Facility personnel maintain the Facility in a neat and orderly condition:

- Good housekeeping: Procedures include, but are not limited to, remediating oil stained soil, maintaining the integrity of secondary containment areas, and minimizing/eliminating trash accumulation in storage areas.
- Vehicle Maintenance: The terminal has a vehicle maintenance bay. The vehicle maintenance bay is inside a building preventing potential contact with stormwater.
- Vehicle or Equipment Washing: The terminal maintains a vehicle wash bay.
 Drainage from the wash bay is treated by an oil/water separator and then discharges to the New York City sewer for treatment by the Public Owned Treatment Works (POTW).
- Roof Areas: There are no process activities at the Facility so roof areas are not subject to contamination from exhaust or vents.
- Sediment and Erosion Control: Areas surrounding outfalls are periodically inspected for sediment / erosion problems. Earthen dikes are regularly inspected as described in the SPCC plan.
- Preventive Maintenance: Regular inspections and preventive maintenance of pollution control measures is scheduled by Facility management (See Section 5.0 of this plan). The inspections noted insure preventive maintenance is performed and that potential deficiencies are noted and corrected.

4.2 SPILL PREVENTION AND RESPONSE PROCEDURES

Motiva has established procedures for responding to spills that occur at the Facility. These procedures include initial response actions, internal notifications and external notifications, implementation of the Incident Command System, disposal, and follow-up procedures. These procedures are outlined in the terminal FRP. Oil Spill Removal Organizations (OSROs) are under contract and will be activated if necessary. The OSROs are listed in the FRP.

The areas with the highest potential for spills are the tank farm, the truck loading rack, and the dock. Drainage for these areas is described in the SPCC Plan and the FRP. As noted previously, the tank farm and the truck loading rack are contained to prevent a potential release of products or potentially contaminated stormwater. Transfers of materials at the dock are performed using portable drip collection trays/basins. Several have the potential for contaminating stormwater have also been identified. These areas are discussed as follows:

- All storage tanks are within containment areas that have the capacity to hold the contents of the largest volume tank plus normal precipitation.
- All other products and chemicals and their containers are stored under a roof which minimizes potential stormwater contact.
- Hazardous and non-hazardous waste containers are kept closed and are stored under a roof
- All dumpsters that are used to store waste materials are supplied with attached covers to minimize potential contact with stormwater.

Motiva Enterprises, LLC Brooklyn Terminal

BMP Plan July 2000

4.3 EMPLOYEE TRAINING

Operators and other site personnel are instructed on their respective job responsibilities and duties.

- Site personnel are trained in the safe handling of materials and spill response procedures during safety meetings and annual safety training classes.
- Training classes include: HAZWOPER (OSHA 1910.120), HAZWOPER refresher training, hazard communications, first responder awareness, and hazardous waste training.
- Additional training is also discussed in the FRP and SPCC plans.

4.4 NON-STORMWATER DISCHARGES

All non-stormwater discharges are closely monitored for contaminants. A list of areas that have the potential to generate such discharges is shown in Figure 4.1. Facility management has taken every reasonable measure to ensure that potentially contaminated discharges do not leave the Facility.

4.5 MANAGEMENT OF RUNOFF

The use of appropriate pollution control measures are implemented when determined to be reasonable and appropriate. Appropriate pollution control measures at the Facility include dikes, sumps, oil/water separators, controlled drainage, corrosion protection (when applicable), roofs/covers, inspections, and training. Facility Management ensures that these pollution prevention measures are implemented and maintained at all times.

In addition to the measures implemented under the SPDES Permit, the Facility complies with applicable municipal stormwater programs developed under NPDES permits issued for the discharge of the municipal separate storm sewer that receives the facility's discharge (Note that no discharge of stormwater from the terminal to municipal stormwater drains presently occurs). These measures will be implemented during future expansion projects and areas of concern will be addressed prior to construction:

- Oil and sediment control structures or other devices will be used within the drainage system for all construction which occurs at this facility on or after the effective date of this general permit and/or may impact the drainage system.
- Removal of total suspended solids from new potential stormwater discharges will be incorporated in the design and installation of permanent stormwater management devices.
- Where possible, stormwater will be segregated from new operations to minimize potential impact.

FIGURE 4.1

EVALUATION OF NON-STORMWATER DISCHARGES

The terminal has the following non-stormwater discharges:

- 1. Tank bottom water
- 2. Truck loading rack wash down water
- 3. Tank hydrostatic test water

The tank bottom water is treated off-site at a permitted facility and the other water described above is treated by an oil/water separator prior to discharged in accordance with the terminal SPDES Permit No. NY0006131.

Review of other terminal water discharges:

- 1. Building roofs and the disposition of the associated runoff are listed below. Stormwater from the terminal roofs is not impacted by any processes or materials.
 - Warehouse roof stormwater to ground via gutters
 - Office roof and employee building roof stormwater to ground via gutters
 - Loading rack canopy to stormwater drainage system via piping

The above runoff would either percolate into surrounding soil or enter the stormwater drainage system through direct piping or flowing to a surface drain that flows to the stormwater drainage system, which then flows to the terminal's oil/water separator.

- 2. Sanitary sewage from restroom toilets, floor drains and sinks flows to the City of New York wastewater treatment system.
- 3. The warehouse and storage building areas do not have any floor drains.
- 4. Vehicle wash bay flows to an oil/water separator and to the City of New York wastewater treatment system.

Motiva Enterprises, LLC Brooklyn Terminal

BMP Plan July 2000

5.0 INSPECTIONS

5.1 REGULARLY SCHEDULED INSPECTIONS

Regularly scheduled inspections of storage tanks, secondary containment berms, and response equipment are conducted as part of the regular SPCC procedures. A description of the inspections and inspection documentation are included in the SPCC Plan and the FRP.

5.2 COMPREHENSIVE SITE COMPLIANCE EVAULATION

Qualified personnel conduct site compliance evaluations at least once per year in addition to regularly scheduled inspections. Such evaluations include inspections of material handling areas and other potential sources of pollution identified in this plan, structural pollution prevention measures, and inspection of spill response equipment. These records will be retained as part of the BMP Plan for at least three years. A sample inspection form is located at the end of the Plan (BMP Form 1).

Motiva Enterprises, LLC Brooklyn Terminal

BMP Form 1

SITE COMPLIANCE EVALUATION REPORT

No Indicates Unsatisfactory			
Gondition	Yes	No	Gomments & Action Taken
Bermed Areas			
Waste Storage Area	<u> </u>		
Hazardous and Non-Hazardous		}	·
Review of Housekeeping Efforts		 	
(trash storage, chemical handling	•		
procedures, etc.)			
Survey Grounds for evidence of			
contamination (i.e, ditches,			
concrete areas, grass areas and			
gravel areas) Spill Response Equipment	 		
Opin Response Equipment		!	
Foam Storage Area			
Drum Storage Area			
Pipelines			
Maintenance			
Docks		<u> </u>	
Docks			
Tanks		·	
Process Equipment			
Inspected By:	<u> </u>		Date:
Facility Manager			Date:
COMMENTS:		······································	
· .			
	•		
	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	, <u>.</u>	

NOTE: Based upon the results of this evaluation, any changes in the potential pollutant sources at the terminal shall be incorporated in the SWPPP within 2 weeks of this evaluation. Any changes in the SWPPP pollution prevention measures shall be implemented within 12 weeks after this evaluation is completed.

Motiva Enterprises, LLC Brooklyn Terminal

FORM 1

SWPPP/BMP July 2000

New York State Department of Environmental Conservation <u>Major Oil Storage Facility - Site Inspection Report</u>

08/7/06

NYSDEC MOSF#	MOSF License Expiration Date						
MOSF Inspection #	CBS#	Air Permit#		SPDES #	SPDES #		
Facility Name		Facility Owner					
Facility Address		Facility Owner Addres	ss				
Telephone Number		Telephone Number					
Facility Representative / Title		NYSDEC Representat	ive / Title		·		
Tanks Inspected : Tank#	· · · · · · · · · · · · · · · · · · ·						
RECORDS INSPECTION (1) Does the facility have a Spill Prevention, Control and Countermeasures (SPCC) plan? (40 CFR 112.3 and 6NYCRR 610.4.a.(4)			Yes	No	X NOT APPLIC ABLE		
(2) Date of SPCC plan (40 CFR 112.5(b)) 6NYCRR 610.4.a.(4)							
(3) Is the SPCC plan signed by a NYS licensed and registered Professional Engineer? 6NYCRR 610.4.a.(4) (DER 11 Appendix B Attachment 3(d)3.a.)			r? Yes	No	X		
(4) Is the SPCC plan approved by	facility management? 40 CFR 112.3-7) 6NYCRR 61	.0.4.z.(4)	Yes	No	X		
(5) Does the facility have a Facility	Response Plan (FRP)? 10 CFR 112.20) 6NYCRR 610.	4.a.(4)	Yes	No	X		
(6) Does the facility have a U.S. Co (33 CF)	ast Guard Operations Manua R ,154,156) 6NYCRR 610.4.a.(Yes	No	X		
(7) Are records of monthly ground	water inspections available.?		Yes	No	х		
(8) Is the license information curre (Article 12, Section 174)	nt and correct		specify deficie	encies			
(9) Has the facility met the requirements of its general and special license conditions? (DER-11, Appendix B, Attachments 3b,3c,3d)			specify deficion	encies			
(10) Date of last five year in-depth inspection.	secondary containment system	n integrity					
(Der-11,Appendix B, Attac	chment 3(b), Special License (Condition # 3j)			· · · · · · · · · · · · · · · · · · ·		

				·····	1
Aboveground Storage Tanks (ASTs) RECORDS INSPECTION	Yes		No		X
(11) Are monthly inspections performed for ASTs?			: 		
(6 NYCRR 613.6 (a))					
Do the reports include:	Yes		No		х
(12a) Inspection of exterior surfaces of tanks, pipes, valves or other equipment for leaks?					
(6 NYCRR 613.6 (a)(1))					
(12 b) Identify areas of the facility that need maintenance?	Yes	<u> </u>	No		X
(6 NYCRR 613.6 (a)(2))					
					_
(12 c) Inspection and monitoring of leak detection systems, cathodic protection	Yes		No		X
monitoring equipment and other warning systems in place?				·	_
(6 NYCRR 613.6 (a)(3))					
(12 d) Are the monthly inspection reports signed by the tank inspector?	Yes	·	No		X
(6 NYCRR 613.6 (c)(2)(vii))					
(13 a) Are ten year inspections performed for ASTs?	Yes		No		X
(6 NYCRR 613.6 (b))				ļ	_
(13 b) Are the ten year inspection reports signed by the inspector?	Yes	-1	No	···	X
(6 NYCRR 613.6 (c)(vii))					
(13 c) Do the inspections follow standard practices and procedures (API or STI as applicable)?	Yes		No	<u> </u>	X
(6 NYCRR 613.6 (b)(3)(iii))					
				1	_

(13 d) Was the NYSDEC notified prior to any major tank repairs or modifications?	Yes			No			X
(General License Condition # 5)							
(13 e) Were the major tank modifications designed by a NYS licensed and registered Professional Engineer?	Yes			No			X
(14) If motor fuel tank has pressurized piping, is it equipped with a shear valve?	Yes			No		_	X
(6 NYCRR 613.3 (e)(1))			_	· · · · · · · · · · · · · · · · · · ·			
<u>Underground Storage Tanks (USTs)</u> <u>RECORDS</u> INSPECTION	Yes			No			X
(15) Is UST leak monitoring being performed (double wall tank - interstice is checked)? 1 (inoperative system) -		tank #					
2 (monitoring records not maintained) - 3 (inappropriate method) (6 NYCRR 613.5(b)(3) - 614.5)		viola tion					
 (16) Is eathodic protection for steel UST and piping systems monitored annually? 1 (no monitoring on tank)- 2 (no monitoring on line) - 	Yes			No			X
3 (records not maintained) - 4 (system not maintained to achieve protection) - 5 (inadequate method) (6 NYCRR 613.5 (b)(2))		tank #					
		viola tion					
 (17) Has tightness testing been conducted on the tank and piping system? Check for both tank and piping. 1 (entire tank not tested) - 2 (piping system not tested) 	Yes			No			X
(6 NYCRR 613.5 (a))		-		·			
(18) Are annual cathodic protection reports available?	Yes		<u> </u>	No			X
(6 NYCRR 613.5 (b)(4))							
(19) Does the inspection report indicate that cathodic protection is operating properly?	Yes			No	<u> </u>		Х
(ECL Art. 17, Title 10, Section 1007.1) (6 NYCRR 613.5 (b)(3))							
	<u> </u>		<u></u>	<u> </u>			

(20) Inventory records for metered USTs: 1 (no records) -		No			X
2 (poor equipment) - 3 (no reconciliation) - 4 (reconciliation performed other than 10 days) -		tank #			
5 (no investigation of discrepancy) (6 NYCRR 613.4 (a)(1), 613.4 (c), 613.4 (d))		viola tion			
Aboveground Storage Tanks (ASTs) OUTDOOR	ta	nk#			
INSPECTION (21) Is there a gauge, high level alarm or other equivalent device for AST?					
N (no) -					
1 (inoperative) -	Aları	on.			
2 (gauge) - 3 (high level alarm) or					
4 (other equivalent device; indicate) (6 NYCRR 613.3 (c)(3)(i) & (iii))					
(NYCRR 613.3 (c)(3)(i) & (iii)) (22) Is the design/working capacity and identification number marked on AST and at gauge?	Yes		No		X
(6 NYCRR 613.3 (c)(3)(ii))					
(23) Is solenoid or equivalent valve in place for gravity fed motor fuels	Yes		No	<u> </u>	X
dispensers?		 		<u> </u>	1 1
(6 NYCRR 613.3 (c)(2))					4
(24) Were any unreported spills observed during the inspection?		<u></u>			•
(6 NYCRR 613.8)					
(25) Are check valves in place for pump filled tanks with remote fills?	Yes		No		X
(6 NYCRR 613.3 (c)(4))					
	-	 			
(26) Are operating valve in place on every line with gravity head?	Yes		No		X
(6 NYCRR 613.3 (e)(5))					_
(27) If the tank is in service or temporarily out-o- service, is there a need for maintenance?	Yes		No		X
					~
(6 NYCRR 613.9 (a)(2))					-

(28) Are the cathodic protection monitoring ports connected and reports available to indicate that the system is working properly?		No	Yes					X
(6 NYCRR 614.3 (e)(5))						·		
(29) Are dike drain valves locked in closed positio	n?						, <u> </u>	
(6 NYCRR 613.3 (c)(6)	(iii))				·			
(30). Tank installed after 12/86, tank system meets standards. If no, missing items? Y/N/X ASTs must (1) be welded steel		Yes	No				X	
(2) have surface coating (paint),	•							
(3) if on ground have cathodic protection and				,				
(4) If on ground have an impermeable barrier un ability to monitor for leaks between tank bottom:								i
(6 NYCRR 614.9-11)	and parties.							
(
(31) Type of Secondary Containment (ASTs) - Secondary containment constructed of:		tank#						
	5- (asphalt)				1			1
	i- (asphalt with sealant) '- (geomembrane-liner							
· · · · · · · · · · · · · · · · · · ·	- (geomemorane mier 8- (clay with ballast)	construction						
)- (other; indicate)	const	ruction	}				
(6 NYCRR 613.3 (c)(6))								
					<u> </u>	<u> </u>	<u> </u>	
(32) Are permanently out-of-service tanks closed properly? (6 NYCRR 613.9 (b))		Yes			No			X
]
	,							
(33) Does transfer area/ loading rack area have secondary containment?		Yes	No				<u> </u>	X
(49CFR 112 .7(c))					ļ			
(34) Does transfer area/ loading rack area second (6NYCRR 613.3.	- ·		<u> </u>	!			<u> </u>	
		<u> L</u>						

							
Underground Storage Tanks (USTs) OUTDOOR INSPECTION	Yes			No			X
(35) If tanks were installed after 12/86, does the tank system meet standards. If							
no, missing items?							
1 (corrosion resistant) -							
2 (secondary containment) -						,	
3 (leak monitoring) -		_					
4 (overfill prevention (auto shut off valve, high level alarm or ball float valve)) - 5						·	
(corrosion resistant piping) with -			İ				
6 (leak monitoring (Line leak detector for pressurized piping)) or							1 1
7 (having only one check valve under pump in suction piping system) -							
8 (tank label) -							ł
9 (as-built plans or drawings)							
(6 NYCRR 614.3 - 614.5)] [[[
(0.11 CAR 014-3)			L	L		<u> </u>	
	Yes			No			X
(36) Do unmetered tanks have annual standpipe test, tank test or other leak				 			
detection method?							1 1
(6 NYCRR 613.4 (a)(2))					ļ ļ		
(0.1.2.0.2.2.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7.7			 		-		
·			1]]
			l	<u> </u>	<u> </u>		
(37) Is the fillport color coded to identify product in the tank?	Yes			No			X
		****************	T	T .			1 (
(6 NYCRR 613.3 (b))							
· · · · · · · · · · · · · · · · · · ·				<u> </u>			1 1
			1	<u> </u>	<u> </u>	<u> </u>	
	Yes			No			X
(38) Have tank top, dispenser sumps and fill port catch basins been properly			,			·	4 1
maintained?							
,					1		յ ն
(6 NYCRR 613.3 (d))			İ] [
			ì	1			
					·		
(40) Remarks / Comments (refer to item number)							
(40) Account me / Commence (10101 to 10012 manager)							
1							

(40) Remarks / Comments (Continued)		
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58603-2009-03-31-COR-01 (SPDES Action 38

Plan - Motiva).pdf



March 31, 2009

VIA FAX AND US MAIL

New York State Department of Environmental Conservation Division of Water, Region 2 Attention: Vichit Aramsombatdee 47-40 21st Street Long Island City, NY 11101-5407

SUBJECT: NYSDEC INSPECTION/NOTICE OF VIOLATION

MOTIVA ENTERPRISES LLC - BROOKLYN TERMINAL

FEBRUARY 11, 2009 INSPECTION SPDES PERMIT NO. NY0006131

Dear Mr. Aramsombatdee:

This is in response to your February 12, 2009 letter regarding the subject SPDES Inspection. Based on your inspection, you noted three items requiring corrective action. An action plan or response for each item is included below:

- The Department requests a Comprehensive Action Plan to prevent the discharge of Benzene, Toluene, Ethylbenzene and Xylene(s) (BTEX) at levels higher than the Action Levels of 0.1 mg/l.
 - As an interim measure, the terminal will continue routine inspections of the oil/water separators and clean the separators as necessary to minimize the potential for product contacting stormwater prior discharge.
 - o As a long-term solution, Motiva Enterprises LLC (Motiva) proposes to evaluate the existing truck loading rack stormwater collection and treatment system. Based on the evaluation, treatment system improvements will be designed and installed. Initial conceptual improvements for the system include the installation of granular activated carbon to treat potential BTEX concentrations. The proposed schedule for the work is as follows:

PO Box 736

Mariton, NJ 08053

Phone: (856) 810-7720

Fax: (856) 810-7721

- Evaluation of the existing system and identification and design of appropriate improvements will take approximately 2 – 3 months (Estimated Completion June 30, 2009)
- Review and approval by the City of New York (6 9 months)
- Construction of system improvements 3 months (Depending on timely approvals being received by the City of New York, Motiva proposes to complete construction by March 31, 2010 or earlier. However, any delay in approvals required by the City of New York will delay completion accordingly).
- Use of unapproved method to analyze Benzene, Toluene, Ethylbenzene and Xylenes I am not quite clear what the Department is requesting with regard to the October 16, 2006 analysis. Motiva understands that the method SW 846 8260 was inadvertently used to analyze the sample in question. Motiva has made note of this and informed our contract laboratory that such future samples should be analyzed using only EPA Method 624. Unfortunately, due to the time that has elapsed, the 2006 sample cannot be reanalyzed. It should be noted that Method 8260, although not the specified method, is similar in that it is a GC/MS method with similar detection limits. The results did demonstrate that the levels of all potential contaminants were below levels that could pose substantial environmental harm.
- The facility Best Management Practices Plan needs to be updated the plan will be updated by April 30, 2009.

Please call me at (856) 810-7720 if have any questions regarding this response or the proposal for addressing BTEX at the Brooklyn Terminal.

Sincerely:

David L. Bier

Field Environmental Coordinator

and I see

cc: J. W. Lintz/F. Signoriello - Motiva - Brooklyn, NY



TO: VICHIT ARAMSOMBATDEE, PE NYSDEC
FAX NO. 718-482-6516
TEL. NO. 718-482-4933
FROM:
MOTIVA ENTERPRISES LLC ATTN: DAVID L. BIER PO BOX 736 MARLTON, NJ 08054
TEL. (856) 810 - 7720
FAX NO. (856) 810 – 7721
MESSAGE: DEAR MR. ARAMSOMBATDEE -
ATTACHED IS IN RESPONSE TO YOUR
INSPECTION OF THE MOTIVA BROOKLYN
TERMINAL ON FEB. 11, 2009. PLEASE
CALL ME IF YOU WOULD LIKE
TO DISCUSS. THANK YOU,
Dave Bres

PO Box 736

Mariton, NJ 08053

Phone: (856) 810-7720

Fax: (856) 810-7721

New York State Department of Environmental Conservation

Division of Water, Region 2

47-40 21ST Street, Long Island City, NY 11101-5407 Phone: (718) 482-4933 • FAX: (718) 482-6516

Website: www.dec.ny.gov



CERTIFIED MAIL NO. 7005 0390 0004 3765 4375 WITH RETURN RECEIPT REQUESTED

February 12, 2009

Mr. Frank Signoriello, Terminal Supervisor Motiva Enterprises LLC 25 Paidge Avenue Brooklyn, NY 11222

RE:

NOTICE OF VIOLATION SPDES Permit No. NY 0006131 Annual Compliance Inspection

Dear Mr. Signoriello:

On February 11, 2009 the referenced facility was inspected for the purpose of evaluating its compliance with the requirements of its permit issued under the State Pollution Discharge Elimination System (SPDES) and Article 17 of the Environmental Conservation Law.

The following items were noted during the inspection:

A review of the facility's discharge monitoring reports for Benzene, Toluene, Ethylbenzene, and Xylenes from the period January 2007 to December 2008 indicated the following:

Outfall	Parameter	Reported Value	Action Level	Period
001 Ethylbenzene Toluene		0.17 mg/l	0.1 mg/l	2/07 to 4/07
		1.1 mg/l	0.1 mg/l	2/07 to 4/07
	Xylenes	0,92 mg/l	0.1 mg/i	2/07 to 4/07
001 Benzene Ethylbenzene		1.0 mg/i (6/28/07); 0.19 mg/i (7/18/07)	0.1 mg/l	5/07 to 7/07
		0.44 mg/l (6/28/07); 0.29 mg/l (6/27/07); 0.23 mg/l (7/18/07)	0.1 mg/l	5/07 to 7/07
	Toluene	6.7 mg/l (6/28/07); 0.76 mg/l (6/27/07); 2.1 mg/l (7/18/07)	0.1 mg/l	5/07 to 7/07
	Xylenes	3.7 mg/l (6/28/07); 0.66 mg/l (6/27/07); 1.18 mg/l (7/18/07)	0.1 mg/l	5/07 to 7/07

Outfall	Parameter	Reported Value	Action Level	Period
001	Toluene	0.56 mg/l (11/6/07); 0.12 mg/l (11/20/07)	0.1 mg/l	11/07 to 1/08
	Xylenes	0.35 mg/l (11/6/07)	0.1 mg/l	11/07 to 1/08
001	Toluene	0.33 mg/l (6/5/08)	0.1 mg/l	5/08 to 7/08
THE PROPERTY AND ADDRESS AND A	Xylenes	0.36 mg/l (6/5/08)	0.1 mg/l	5/08 to 7/08

The facility's SPDES permit page 3 of 9 states "If levels higher than the actions levels are confirmed the results shall constitute an application for permit modification and the permit may be reopened for consideration of revised action levels or effluent limits."

Based on the results shown above, the Benzene, Toluene, Ethylbenzene, Xylenes levels higher than the action levels of 0.1 mg/l are confirmed. The Department shall proceed with the facility permit modification. In the interim, in order to prevent the discharge of Benzene, Toluene, Ethylbenzene, Xylenes levels higher than the action levels of 0.1 mg/l which may cause or contribute to a violation of water quality standards, the Department requests that a Comprehensive Corrective Action Plan be submitted to this office for review and approval by March 31, 2009. The plan must include a proposed schedule for implementation of the recommended corrective action.

- The facility still has not rectified the problem of using the unapproved method to analyze Benzene, Toluene, Ethylbenzene, and Xylenes (BTEX). The BTEX hydrostatic test samples collected on October 16, 2006 were analyzed by the method SW 846 8260. NYSDEC had already informed the facility twice in the compliance inspection reports (first notification: September 12, 2005 (Mr. Mario A. D' Antonio); second notification: June 6, 2006 (Mr. E.D. Bernhard Jr.)) that the method SW 846 8260 is unapproved method and it is not authorized under the 40 Code of Federal Regulations (CFR) Part 136. Please inform the laboratory that the approved method for BTEX analysis under 40 CFR Part 136 is EPA method number 624.
- The facility Best Management Practices (BMP) Plan needs to be updated to reflect the recent changes at the facility.

The Department reserves its right to initiate an enforcement actions for the items noted in this Notice of Violation.

If you have any further questions, please contact me at (718) 482 4946.

Very truly yours

Vichit Aramsombatdee, PE Environmental Engineer 2

Region 2, Division of Water

cc: Robert Elburn, PE, Regional Water Engineer;

Selvin Southwell, PE, Deputy Regional Water Engineer

DOCUMENT INFO

DocID:

00000316

Filename:

58603-2009-04-01-OTH-01 (Emissions

Inventory 2008 - Trinity).pdf



This 2008 Emission Statement package was sent to you because the New York State Department of Environmental Conservation (Department) has identified that your facility is required to obtain a Title V permit pursuant to Title 6 of the New York Codes, Rules and Regulations (6 NYCRR) Subpart 201-6.

The federal Clean Air Act (§182(a)(3)(B), §502(b)(3)), State Environmental Conservation Law (§72-0303) and 6 NYCRR 202-2, "Emission Statements," requires your facility to report emissions annually and pay a permit fee based on the actual total tonnage of emissions. The information on this form allows the Department to calculate the emissions from your facility and report these emissions in the required format to the United States Environmental Protection Agency and the Great Lakes Commission.

Your 2009 permit fee will be based on your reported 2008 actual emissions as confirmed by the Department. This statutory fee is redetermined annually and published as a rule by the Department.

If you do not respond to this survey, you will be in violation of the Environmental Conservation Law, enforcement action will be initiated and your fee will be based on your maximum permitted emissions. Fees based on your maximum permitted emissions may be much higher than fees based on your actual emissions. The Department will send an invoice for fees at a later date.

The Department developed the 2008 emission statements from information contained in the Air Facility System (AFS). AFS contains your facility's permit data from information provided to the Regional NYSDEC Offices through permitting applications and modifications.

If there are any questions regarding this form, please call Ronald Stannard or members of his staff at 518-402-8396.

You may request that information submitted in emission statements be designated as a trade secret in accordance with Public Officers Law §87(2)(d) and 6 NYCRR Part 616. Data elements not considered trade secrets include: facility emissions, estimated emissions method, and Source Classification Code (SCC). The Department will evaluate claims of confidentiality in accordance with Part 616.



COMPLETED EMISSION STATEMENTS MUST BE SUBMITTED TO THE DEPARTMENT AND POSTMARKED ON OR BEFORE APRIL 15, 2009 TO THE ATTENTION OF:

Ronald W. Stannard, P.E. New York State Department of Environmental Conservation Division of Air Resources 625 Broadway Albany, NY 12233-3251

Section 1 - Certification

Emission statements must include certification by a representative of your facility. The certification must include the full name, original signature, date of signature and telephone number of the representative.

Emission statements must also include facility level information consisting of:

- verification of facility owner
- · verification of full name of facility
- verification of street address (physical location) of facility
- verification of the four digit SIC for the facility
- verification of DEC ID.

Make necessary changes directly on the emission statement by crossing out the incorrect information and writing in the correct information. For blank emission statements, please complete all of the above information. If either the fuel/combustion and incineration or industrial process section is not applicable to your facility, sign the certification and indicate that this section is not applicable to your facility.

You are required to report <u>all</u> emissions at your facility <u>except</u> emissions from the following activities:

- a. On-road internal combustion engines (cars, buses, trucks).
- b. Non-road internal combustion engines (lawn and garden equipment, light mobile commercial welders, forklifts).
- c. Surface cleaning/degreasing for janitorial purposes other than of industrial

Page 2 of 10



machines.

- d. Architectural surfacing coatings (building/house paint).
- e. Asphalt paving.
- f. Commercial/consumer solvent use (household products, toiletries, aerosol products, polishes, pesticides, nonindustrial adhesives and space deodorants).

Section 2 - 2008 Facility Fuel Use Reporting Form

Section 2.1 - Facility Fuel Use (Combustion and Incineration)

Report all of your facility's fuel consumption by fuel type. This should include fuel consumed from exempt and non-exempt sources. Report the corresponding sulfur content and heat value of each fuel burned in 2008. If necessary, contact your fuel supplier to obtain heat value and sulfur content information. Be certain to report the correct quantity of fuel with the appropriate units. Reported fuel in Section 2.1 should equal the sum of all fuel reported in Section 2.3 and Section 4.

Section 2.2 - Combustion and Incineration Process Emissions Summary (OPTIONAL)

Section 2.2 is OPTIONAL. Report the 2008 emissions total of each contaminant from your facility for combustion and incineration processes. The emissions total for each contaminant reported here should equal the sum of actual emissions reported in Section 2.3. Blank spaces are provided for corrections or additions to the list of contaminants.

Use Table 2 (Chemical Family Code) to determine the criteria group to which each contaminant belongs. This will enable you to determine how each contaminant contributes to your facility's emissions totals. To calculate your facility's total emissions for 2008 subject to emission fees, add actual totals for all the contaminants except those with chemical family codes of 5 and 6.

<u>Please note:</u> Chemical families 1, 7, 8, and 11 will be billed as Particulates and chemical families 4 and 9 will be billed as Volatile Organic Compounds.



Section 2.3. - Combustion and Incineration Process Emissions

Report <u>all</u> emissions (stack and fugitive) from combustion and incineration activities for all emission units and processes. Information from permits for most or all emission processes has been provided with descriptions of the process, including Source Classification Codes (SCCs).

In order to streamline the emission statement, the Department has included a number of exempt sources in the section of the statement that pertains to that source. Only those processes that have been entered into AFS as exempt will have an exempt identifier. Other exempt processes may not contain the exempt identifier and will appear in the statement with all remaining sources at the facility. The emissions from all other exempt sources not identified in the statement must be reported in Section 4 "Periodic Inventory Blank Reporting Forms."

Please note, reporting of emissions data for exempt processes is required this year. If you believe that a process listed in your emission statement, which is not marked as exempt, is now exempt pursuant to 6 NYCRR 201-3.2, report the emissions from that activity where it is listed in the emission statement. Clearly indicate in both the total emissions section and at the emission unit that it may be exempt. The Department will review the information provided, determine whether the process is exempt and notify your facility.

If your facility has other fuel combustion and incineration emission processes that are not listed in Section 2.3, use the Blank Form provided at the end of this section for submitting emissions. The Blank Form may also be used to report emissions in cases where you would need to correct or rewrite information.

Report and/or verify the following information for each emission unit:

- Emission unit number and total heat input for the emission unit. The Emission unit assigned by the Department corresponds to either the emission point number on your current state facility permit or to the Emission Unit number assigned under your Draft or Issued Title V permit. Total heat input is the sum of the maximum heat input (million Btu per hour) for all processes at the Emission Unit.
- The ID number, size and a description of the unit. This is your ID, maximum rated capacity (e.g., MMBtu/hr, brake horsepower-hour), and usually the manufacturer's name.
- Control equipment description and overall control efficiency of the equipment for that process. The description refers to the type of equipment (e.g., baghouse, scrubber, flue gas desulfurization). Efficiency for each criteria pollutant considers the equipment's actual control including downtime and maintenance degradation.

Page 4 of 10



- Fuel burned. This information corresponds to a Source Classification Code (SCC) that describes the process and the fuel. The Department will assign an SCC based on information provided. An emission unit may have several SCCs (usually one for each type of fuel).
- Operational data for each SCC.

Annual Average

- On average, the hours per day and days per week the equipment at this emission process operated on this fuel.
- The number of weeks in 2008 the equipment at this emission process operated on this fuel.

Percent fuel use by season

• The percentage of total fuel burned in 2008 for this SCC for the three month periods (the sum of the percentages must equal 100%):

December 2008, January and February 2008

March - May 2008

June - August 2008

September - November 2008

Jun. - Aug. and Jan. Feb. & Dec. of 2008

- On average, the hours per day and days per week the equipment at this emission process operated on this fuel.
- The number of days during this period the sources at this emission process operated on this fuel.
- Reporting the emissions corresponding to the fuel burned at each SCC is OPTIONAL. If this section is not completed, the Department will use federal emission factors to calculate emissions. If you choose to report emissions for a specific SCC, report emissions by criteria pollutant in pounds per year and list under <u>HD</u> (How Determined) the method code from Table 1 below. If published emission factors were used, state the emission factor and its source (i.e., AP-42, FIRE, TANKS, etc.).



TABLE 1

HD - How Determined (Estimated Emissions Method Code)

- 1 Stack test of emissions
- 2 Material balance calculations or fuel analysis
- 3 Published emission factors
- 4 Best engineering judgement
- 5 Stack test of emissions from identical emission source
- 6 Stack test of emissions from geometrically similar emission source
- 7 Continuous stack monitoring
- 8 Modeling/Estimation Software (TANKS, LAEEM, etc.) please specify
- 9 Manufacturer's guarantee

Section 3 - Industrial Process Facility Emissions Forms

If your emission statement includes general emission categories such as Unspeciated VOC or Unspeciated Particulates (these have replaced all generic VOC and particulate CAS Codes used in the past) instead of specific contaminants, you need only report the emissions of these general categories and not attempt to identify each specific contaminant individually by CAS Code (Please note that this does not apply to HAPs and to HAPs that are also VOCs or particulates, HAPs must be reported by CAS Code). This does not relieve you of the responsibility of reporting all non-exempt emissions at your facility and the individual contaminants shown on the emission statement.

Section 3.1 - Industrial Emissions Summary

Report <u>all</u> 2008 emissions (stack and fugitive) of each contaminant from your facility for industrial processes. The emissions total for each contaminant reported here should equal the <u>sum of actual emissions reported in Section 3.2.</u> Do not include emissions from exempt activities. Blank spaces are provided for corrections or additions to the list of contaminants.

Use Table 2 below (Chemical Family Code) to determine the criteria group to which each contaminant belongs. This will enable you to determine how each contaminant contributes to your facility's emissions totals. To calculate your facility's total emissions for 2008 subject to emission fees, add actual totals for all the contaminants except those with chemical family codes of 5 and 6. Report all of your facility's actual emissions by CAS Code. Blank spaces are provided for corrections or additions to the list of contaminants.



TABLE 2

Chemical Family Code

- 1 Particulates (PART)
- 2 Sulfur Dioxide (SO₂)
- 3 Nitrogen Oxides (NO_x)
- 4 Volatile Organic Compounds (VOC)
- 5 Carbon Monoxide (CO)
- 6 Other
- 7 PM-10
 - 8 PART and Hazardous Air Pollutant (HAP)
 - 9 VOC and HAP
 - 10 HAP Only
- 11 PM 2.5

<u>Please note:</u> Chemical families 1, 7, 8, and 11 will be billed as Particulates and chemical families 4 and 9 will be billed as Volatile Organic Compounds.

Section 3.2. Industrial Process Emissions

Report <u>all</u> emissions (stack and fugitive) from industrial activities for all emission units and processes. Information from permits for most or all emission processes has been provided with descriptions of the process, including Source Classification Codes (SCCs).

In order to streamline the emission statement, the Department has included a number of exempt sources in the section of the statement that pertains to that source. Only those processes that have been entered into AFS as exempt will have an exempt identifier. Other exempt processes may not contain the exempt identifier and will appear in the statement with all remaining sources at the facility. The emissions from all other exempt sources not identified in the statement must be reported in Section 4 "Periodic Inventory Blank Reporting Forms."

Please note, reporting of emissions data for exempt processes is required this year. If you believe that a process listed in your emission statement, which is not marked as exempt, is now exempt pursuant to 6 NYCRR 201-3.2, report the emissions from that activity where it is listed in the emission statement. Clearly indicate in both the total emissions section and at the emission unit that it may be exempt. The Department will review the information provided, determine whether the process is exempt and notify your facility.



If your facility has other industrial emission processes that are not listed in Section 3.2, use the Blank Form provided at the end of this section for submitting emissions. The Blank Form may also be used to report emissions in cases where you would need to correct or rewrite information.

Report and/or verify the following information for each emission unit:

- Emission unit number. The Emission unit number corresponds to either the emission point number assigned by the Department on your current state facility permit or to the Emission unit number assigned under your Draft or Issued Title V permit.
- Verify the SCC Code by ensuring the SCC Description matches the process at that
 emission unit. Make any necessary corrections. The Department will assign an SCC
 based on your description.
- Annual throughput should be reported in the units shown under throughput units. If you wish to use alternative throughput units, clearly indicate this directly on the form.
- The Unit Description identifies the equipment used in the process at that emission unit. Make any necessary corrections to this information.
- Control equipment description and the overall control efficiency of the equipment for that emission process. The description refers to the type of equipment (e.g., catalytic oxidizer, flare, scrubber). Efficiency for each criteria pollutant considers the equipment's actual control including downtime and maintenance degradation.
- Operational Data.

Annual Average

- On average, the hours per day and days per week the equipment at this
 emission process operated.
- The number of weeks in 2008 the units at this emission process operated.

Percent operation by season

• The percentage of total process rates in 2008 for this SCC for the three month periods (the sum of the percentages must equal 100%):

December 2008, January and February 2008
March - May 2008
June - August 2008
September - November 2008

Page 8 of 10



Jun. - Aug. and Jan. Feb. & Dec. of 2008

- On average, the hours per day and days per week the equipment at this
 emission process operated.
- The number of days during this period the units at this emission process operated.
- Actual Emissions by CAS Code for SCC. The actual emissions for each contaminant at the process must be reported in pounds per year. If your emission statement includes general emission categories such as Unspeciated VOC or Unspeciated Particulates (these have replaced all generic VOC and particulate CAS Codes used in the past) instead of specific contaminants, you need only report the emissions of these general categories and not attempt to identify each specific contaminant individually by CAS Code (Please note that this does not apply to HAPs and to HAPs that are also VOCs or particulates, HAPs must be reported by CAS Code). Report the method used to determine your emissions by using the appropriate HD code found in Table 1.

<u>Section 4 - Periodic Inventory Blank Reporting Forms</u> (This section is for inventory purposes only. Emissions from these categories will not be used for billing.)

Report NOx, VOC, and CO emissions from your facility's exempt activities. Exempt activities are identified in 6 NYCRR Part 201, "Permits and Certificates," Section 201-3.2. Emissions from these sources should be estimated and provided for each process indicated as exempt in your emission statement. Emissions from all other exempt sources must be reported on the blank forms located in Section 4. Care should be taken to ensure that each activity is reported and identified by the exemption category that best describes the activity. Emissions may be aggregated for activities that fall under the same exemption category.

Please note, if you feel an Emission Unit or activity that is identified in your emission statement is now exempt pursuant to 6 NYCRR Part 201, report the emissions from that activity where it is listed in the emission statement. Clearly indicate in both the total emission section and at the emission unit that it may be exempt. The Department will review the information provided and determine whether the process is exempt and review the results with your facility.

Quantify your actual emissions in pounds per year for NOx, VOC and CO and indicate the method in which emissions were determined by listing the appropriate <u>HD</u> number found in Table 1 on page 6. Because of the number of units that can be covered by one exemption description, control equipment information is not asked for. Actual emissions reported should



take into account any removal efficiency provided by a control device.

The following information should be provided in Section 4 to satisfy your periodic inventory requirements:

- An estimation of the Process Rate or Fuel quantity should be provided. This should be done in the appropriate units for the activity described. This is the total annual process rate for the activity described. If you cannot provide the Process Rate in the Process Units requested, you must report the information in Process Units acceptable to you and clearly indicate those units.
- Estimation of Actual Emissions for NOx, VOC, and CO. The emissions for each contaminant at the process must be reported in pounds per year. Indicate the method in which emissions were determined by listing under <u>HD</u> the appropriate method code found in Table 1 on page 6.
- Operational Data.

Annual Average

- ► On average, the hours per day and days per week the units at this emission point operated.
- ► The number of weeks in 2005 the units at this emission point operated.

2008 Emissions Inventory Motiva Enterprises, LLC • Brooklyn Terminal

Prepared by:

TRINITY CONSULTANTS 100 Davidson Avenue Suite 200 Somerset, NJ 08873 (732) 356-9121

April 2009

Project 093101.0009



EXECUTIVE SUMMARY

APPENDIX A
EMISSIONS INVENTORY CALCULATIONS

APPENDIX B
TANKS OUTPUT

APPENDIX C
THE STATE OF NEW YORK 2008 EMISSION STATEMENT

Motiva Enterprises LLC (Motiva) operates a bulk gasoline terminal in Brooklyn, New York. The air emission sources at the Brooklyn Terminal include eighteen storage tanks, loading racks, a vapor recovery unit (VRU), fugitive emissions from components such as pump seals, valves, and connectors and two combustion-heating units. This report contains the completed 2008 emissions inventory for Motiva's Brooklyn Terminal.

TABLE 1-1. PETROLEUM UNIT EMISSIONS INVENTORY SUMMARY

	·VC	VOCs		HAPs HAP Speciation									
***************************************	VOC Ozone	VOC Annual	VOC Annual	Annust	Benzene Annual	Ethylbenzene Annual	Hexana Annual	Isoociane Annyal	MTBE Annual	Toluena Annual	Xylenes Azmuai	Naphthalene Annual	1,2,4- Trimethy benzene Annual
Source	(lb/day)	(tpv)	(lb/vr)	(tpv)	(tpy)	(tpy)	(фу)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)	(tpy)
Loading Rack								:			.,	·	
VRU Emissions	13.29	2.51	5,016.74	0,064	0.002	0.002	0.013	0.021	0.005	0.006	0.014	1.5E-07	0.000
Rack Fugitives	85.52	16.14	32,281,69	0.267	0.050	0.004	0.089	0.00	0.029	0.070	0.023	3.2E-05	0.002
Process Fugitives	6.11	1.11	2,229.90	0.019	0.003	0.0003	0.006	0.00	0.002	0.005	0.002	2.2E-06	0.000
Storage Tanks	30.68	6.74	13,473.59	0.112	0.022	0.002	0.036	0.00	0.011	0.030	0.011	1.3E-05	0.001
Heater	0.02	0.00	7.46										
Totals	135,6	26.5	53,009.38	0.462	0.078	0.009	0.144	0.021	0.047	0.111	0.050	0.0000	0.60
Totale (lb/pt)	12,477.011	53,009,382		924.271	156.10	18.81	288.12	41.40	93.85	221.49	99.17	0.09	5,2

VOC emissions are calculated on a lb/day basis for the peak ozone season – June 1st through August 31st,

TABLE 1-2. COMBUSTION UNIT EMISSIONS INVENTORY SUMMARY

Pollutant	(lb/yr)
Particulate Matter	10.306
Sulfur Dioxide	0.814
Nitrogen Oxides	135.611
Carbon Monoxide	113.913
VOC	7.459

The Brooklyn Terminal 2008 emissions from the petroleum emission units totaled 26.5 tons of volatile organic compounds (VOCs) and 0.46 tons of hazardous air pollutants (HAPs). In addition, the Brooklyn Terminal emitted 135.6 pounds per day of VOCs during the peak ozone season. The inventory emissions are broken down into three emission source categories: loading rack emissions, process fugitive emissions, and storage tank emissions. The loading rack emissions are further broken down into VRU and fugitive rack emissions and are based on a VRU rating of 1.93 mg/L (10/18/07 performance test). The storage tank and loading rack emissions are also broken down by petroleum product. HAP speciation based upon "reformulated" gasoline speciation profiles are provided. Combustion unit emissions are based on 1.36 MMSCF of natural gas combusted during 2008. Note that the individual emission source categories may not add up to the total emission amounts due to significant digit rounding.

Motiva Enterprises, LLC

The detailed emissions inventory calculation spreadsheets are included in Appendix A. These spreadsheets provide all necessary information regarding theories, methodologies, references, assumptions, and estimations employed in estimating 2008 emissions from the Brooklyn Terminal. The spreadsheets included are:

- 2008 Throughput and Turnover Calculations
- 2008 HAP Speciation Data
- 2008 Annual Emissions Loading Racks
- 2008 Ozone Season Emissions Loading Racks
- 2008 Annual Emissions Fugitives
- 2008 Ozone Season Emissions Fugitives
- 2008 Annual Emissions Storage Tanks
- 2008 Ozone Season Emissions Storage Tanks
- 2008 Combustion Emissions Garage Heater

The TANKS 4 output sheets are included in Appendix B. The State of New York 2008 Emission Statement forms are included in Appendix C.

Motiva Enterprises, LLC

APP	ENDIX	A

EMISSIONS INVENTORY CALCULATIONS

Motiva Enterprises, LLC

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL SUMMARY OF EMISSIONS - 2008

	vo	Cs		HAPs				HAP Sp	eciation				1,2,4-
Source	VOC Ozone (lb/day)	VOC Annual (tpy)	VOC Annual (lb/yr)	Annual (tpy)	Benzene Annual (tpy)	Ethylbenzene Annual (tpy)	Hexane Annual (tpy)	Isooctane Annual (tpy)	MTBE Annual (tpy)	Toluene Annual (tpy)	Xylenes Annual (tpy)	Naphthalene Annual (tpy)	Trimethyl benzene Annual (tpy)
Loading Rack VRU Emissions Rack Fugitives	13.29 85,52	2.51 16.14	5,016.74 32,281.69	0.064 0.267	0.002 0.050	0.002 0.004	0.013 0.089	0.021 0.00	0.005 0.029	0.006 0.070	0.014 0.023	1.5E-07 3.2E-05	
Process Fugitives	6.11	1.11	2,229.90	0.019	0.003	0.0003	0.006	0.00	0.002	0.005	0.002	2.2E-06	0.000
Storage Tanks	30.68	6.74	13,473.59	0.112	0.022	0.002	0.036	0.00	0.011	0.030	0.011	1.3E-05	0.001
Heater	0.02	0.00	7.46							• •			
Totals	135.6	26.5	53,009.38	0,462	0.078	0.009	0.144	0.021	0.047	0.111	0.050	0.0000	0.003
Totals (lb/yr)	12,477.071	53,009.382		924.271	156.10	18.81	288.12	41,40	93.85	221.49	99.17	0.09	5,23

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL 2008 COMBUSTION UNIT EMISSIONS

Natural gas used for terminal comfort heaters in 2008

13,561.000 Therms

1,356,105,424 BTUs 1,356.105 MMBTU 1,356 MMSCF

Assume equal distribution across months (ozone and CO season emissions = 25% of annual)

Fuel Combustion Unit: Fuel Fired: Garage Heater Natural Gas

Boller & Fuel Information:

Source Type (utility, and com, res)	Commercial	Control!Efficiency	
Firing Configuration (normal or tange)	«Normal	Particulate Matter (percent)	0%
		 Sulfur Dioxide (percent) 	0%
Average Gring Rate (MMBtu/hour)		Nitrogen Oxides (percent)	0%
Maximum Firing Rate (MMBtu/hour)		Maximum Operation: (hr/day).	24
Rated Maximum Firing Rate (MMBtu/hour)		(day/wk)	7
		(wk/yr)	52
Fuel Type (grade)	Natural Gas	Average Operation (fir/day)	1.36
Average Fuel Heat Content (Btu/SCF)	1,000	(day/wk)	7
Weight % of Sulfur in Oil (percent)	Negligible	(WE/VE)	52

Calculated Operational Data:

Average Fuel Usage (MMSCF/hour)		Average Operating Rate (hr/yr)	495
Maximum Fuel Usage (MMSCF/pr) Average Fuel Usage (MMSCF/yr) Maximum Fuel Usage (MMSCF/yr)		Maximum Operating Rate (hr/yr)	495
Average Fuel Usage (MMSCF/yr)	1.36		
Maximum Fuel Usage (MMSCF/уг)			

Emission Factors:

Source: AP-42, 5th Edition, Table 1.4-1, -2.

Pollutant	Factor	SUnits)	Rating
Particulate Matter	7.6	Ib/MMSCF	D
Sulfur Dioxide	0.6	lb/MMSCE	A
Nitrogen Oxides:	100	16/MMSCE	В
Carbon:Monoxide	84	Ib/MMSCF	В
Volatile Organic Material	5.5	1b/MMSCR	с

Calculated Emissions:

	Annual
Pollutant	(Lb/Hr) (Lb/Yr)
Particulate Matter	0.001
Sulfur Dioxide	0.000
Nitrogen Oxides	0.015 135.6 1
Carbon Monoxide	0.013
Volatile Organic Material	0.001 7.46

Brooklyn08_Draft_041009.xls

4/10/2009

BROOKLYN NY TERMINAL

2008 Monthly Rack Throughput Volumes in Gallons

	REGULAR GASOLINE	SUPER GASOLINE	TOTAL GASOLINE	TOTAL ADDITIVE	TOTAL ETHANOL	TOTAL OC DIESEL
Jan	19,338,061	6,963,432	26,301,493	6,831	2,929,789	2,381
Feb	18,423,812	6,695,462	25,119,274	6,655	2,797,667	2,615
Mar	19,887,479	7,103,519	26,990,998	6,792	3,002,990	2,946
Apr	18,428,196	6,293,015	24,721,211	6,107	2,746,140	2,281
May	14,841,265	4,697,525	19,538,790	4,902	2,170,944	198
Jun	18,557,814	5,735,225	24,293,039	6,165	2,695,607	-
Jul	17,425,867	5,480,160	22,906,027	5,823	2,540,959	-
Aug	15,938,397	5,186,807	21,125,204	5,406	2,345,975	-
Sep	16,068,700	5,252,185	21,320,885	5,270	2,369,902	-
Oct	17,601,260	5,629,900	23,231,160	5,458	2,586,304	
Nov	15,909,161	5,522,887	21,432,048	4,886	2,388,302	-
Dec	17,241,918	6,101,231	23,343,149	5,318	2,601,183	-
TOTAL	209,661,930	70,661,348	280,323,278	69,613	31,175,762	10,421
	O DATE TOTALS					
Regular	209,661,930	74.79%				
Super	70.661.348	25.21%				
EtOH .	81,175,762					
OC	10.421					
Total Wa	8.050			:		····

The throughput information was sent by Dave via email on April 6, 09

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL 2008 THROUGHPUTS

THEOLIGHDIT DIVENTORY AND THENOVER CALCULATIONS

						TF	<u>IROUGHP</u>	JI INVENTORY A	<u>ND TURNO</u>	VER CALCULATI	IONS						
	Tank 9	Tunk (0.	Tank 41	Tank 42	Tank 43	Timk 44	Tank 45	Tani 46	12nk 47	Jant 48	Tank 49	Tank 10	Tank 51	Tank 57	Tank 53	Tank 56	Tank 55
	Throughput	Throughpur	Throughput	Throughput.	Throughput	Throughput	Throughput	Throughput	Throughout	Throughput	Throughput	Throughput	Throughput	Throwshout	Throughput	2 Throughput	Throughput
	(gal)	(gal)	(8al)	69	(gal)	(gal)	(gal)	(3¢1)	(gal)	(cd) 12	(gal)	gall	(gal)	e e (gal)	(gal)	(ga) 5	(gal)
- January	2,316	2316	732,447.3	132 447.3	1,740,425.5	1,740,425.5	732,447.3	732,447.3	7,928,605.0	9,928,605.0	3,481,716.0	3.481,716.0	0.0	1,042.0	670.8	1,1578	2,381.0
Pebnuary	2,256	2,256	699,416.8	699,416 8	1,658,143.1	1,658,133.1	699,416.8	699,-16.8	7,553,762.9	7,553,762,9	3,347,731.0	3347,731.0	0.0	1,0152	670.8	1 (28.0	2,615.0
March	2,302	CI 102	750,747.5	750,747.5	1,789,873.1	1,789,873 1	750,747.5	750,747,5	8,153,866.4	8,153,866.4	3,551,759.5	3,551,759.5	0.6	10361	670.8	3 1 10 12 3 2 3	2,946.0
5-4970+	2,070	2,070	686,535.0	686,535.0	1,658,537.6	1,658,530,6	686,535.0	686,535.0	7,555,560.4	7,555,560 4	3,146,507.5	3) 46,507.5	0.0	19316	670.8	10850	2,281.0
ha)	1,662	1,662	542,735.0	542,736.0	1,335,713.9	1,335,713.9	542,736.0	542,136,0	6,084,918.7	6,084,918-7,-	2,348,762.5	2,348,762-5	0.0	747.8	670.8	830 8	198.0
June	2,090	2,090	673,901.8	673,901.8	1,670,203.3	1,670,203.3	673,901.8	673.901.8	7,608,703.7	7,608,703.7	2,867,612.5	2367,612.5	0.0	9404	670.8	1 044 9 2	0.0
i. Tub	1,974	1974	635,239.8	46. 635,239.8	1,568,328.0	1,568,328.0	635,239.8	635, 39.8	7,144,605.5	g144,605.5°	2,740,080.0	2,740,080.0	0.0	888 3	670.8	5-9869e 101	0.0
August 2 1	1,833	27,813 PO-10	586,493.8	586,493.8 %	1,434,455.7	1 434 455 2	586,493.8	586 493 8	6,534,742.8	3-76-534742-8	2,593,403.5	2,593,403.5	0.0	824.0	670.8	369 9169	0.0
September	1,786	1,786	592,475.5	592,475.5	1,446,183.0	61,446,183.0	592,475.5	592475/5	6,588,167.0	6,588 167.0	2,626,092.5	2,626,092.5	0.0	2039	670.8	893,23	0.0
GCober	₹,850	J 850	646,576.0	646,576.0	1,584,113.4	1.384313.4	646,576.0	646,376.0	7,216,516.6	37,216516.6	2,814,950.0	2314.950.0	0.0	832.6	670.8	9251	0.0
November	1,656	1,656	597,075.5	597,075,5	1,431,824.5	1 431 824 5	597,075.5	197.0753	6,522,756.0	6,522,756.0	2,761,443.5	2,761,441,5%	0.0	F 27450	670.8	2001	0.0
December	1,803	1,803	650,295.8	550,795.8	1,551,772.6	1551,772.6	650,295.8	650,295 8	7,069,186.4	7,069,186.4	3,050,615.5	3,050,605,55	6.0	3112	670.8	9014	0.0
Total Co.	23,598	23,598	7,793,941	7,793,941	18,869,574	18,869,574	7,793,941	7,793,941.	85,961,391	\$5,961,391	35,330,674	330 678	0	0.619	8,050	11.799	10,421
Tank volume *	8,400	8,400	79,800	79,800	79,800	79,800	79,800	79,100	373,800	373,800	429,000	124 200	5,040	3780-4	4,200	4,200	10,466
					m		02.2		. 210.6		24.1				1.9		1.0
- Innover	2.8	2.8 3.73	97.7	977	236.5	e 2000	97.7	7//	230,0	230.0	84.1	832	0.0		1.9		1.0

co	NTENTS O	CATALOG BY MONT	H ²						
nk45	Tank 46	Tank 47	Tank 48	Tank 49	Tank 50	Tank 51	Tank 52	Tank 53	Ta
hand!	Ethanol Ethanol	Rep Clas Rep Clas	Reg Gas Reg Gas	Prem Gree Prom Gree	Prem Gas Prem Gas	Additive Additive	Additive Additive	Waste Water Waste Water	A.
hakol hakol	Ethanol Ethanol	Reg Gas Reg Gas	Reg Gas Reg Gas	Prem Gas Prem Gas	Prem Gas Prem Gas	Additive Additive	Additive Additive	Waste Water Waste Water	A

	January	Additive	Additive	Sthanol	Ethanol	Reg Gas	Reg Gas	Ethapol	Filtunal	Rep Clas	Reg Gas	Prem Gree	Prem Gas	Atlative	Additive	Weste Water	Additive	Distillate
	February	Additive	Additive	Ethanol	Ethanol	Reg Gas	Reg Gas	Ethanol	Ethinol	Reg Gas	Reg Gas	Prem Gas	Prem Gas	Additive	Additive	Waste Water	Additive	Distillate
	March	Additive	Additive	Etharni -	Ethanol	Reg Gas	Reg Gas	Ethalol	Ethinol	Reg Gas	Reg Gas	Prom Gas	Prem Gas	Additive	Additive	Waste Waler	Additive	Profiliate
	April	Addmyd	Additive	Ethanol	Ethanol	Reg Gas	Reg Gas	Ethatol	Ethanol	Reg Gu	Reg Gas	Prem Gas	Prem Gas	Additive	Additive	Waste Water	Additive	Distrible
	May	Additive	Additive	Ethanol	Ethenol	Reg Gas	Reg Gas	Ethanol.	Ethanol	Reg Gas	Reg Gas	Press Gas	Prem Gas	Additive	Additive	Waste Water	Additive	Distillate
	June	Addutve	Additive	(Ethanol	Ethenol	Reg Gas	Reg Gas	Echoaol	Ethanol	Peg Giu	Reg Gas	Prom Ges	Prem Gas	Addative	Additive	Waste Water	Additive	Distilate.
	July	Additive	Additive	Ethanol	Ethanol	Reg Gas	Reg Gas	- Etharol	Ethunol	Reg Gas	Reg Gas	Prem Gas	Prem Gas	Adany	Additive	Waste Water	Additive	Distilate.
	August	Additive	Additive	Ethanol	Ethanol	Reg Gas	Reg Gas	Ettarolt	Ethanol	Reg Gas	Reg Gas	Prem Gas	Prem Ges	Address	Additive	Waste Water	Additive	Distillate
	September	Additive	Additive	Ethanol 2	Ethanol	Reg Gas	Reg Gas	E(hano)	Ethanal	Peg Gas	Reg Gas	Prem Car	Prem Gas	Arlaime	Additive	Waste Water	Additive	hetilate
	October	Additive	Additive	Ethanol	Ethanol	Reg Gas	Reg Gas	Bilanol	Ethanol	Reg Gas	Reg Gas	Prem Ges	Prem Gas	Additive	Additive	Waste Water	Additive	Distillate
	November	Additive	Additive	Etherol	Ethanol	Rey Gas	Reg Gas	Ethanol	Ethanol	Reg Gas	Reg Gas	Prem Gas	Prem Gas	o'Additive	Additive	Waste Water	Additive	Distillate
:	December	Additive	Additive	gr Ethanol	Ethanol	Reg Gas	Reg Gas	Ethanol	Ethanol	Reg Gas	Reg Gas	Prem Gas	Prem Gas	Additive	Additive	Waste Water	Additive	Distillate (A.V.)

							SI	EASONAL USE CAL	CULATIO	IS BY TANK								_
	Tank 9	Tank 10	Tank 41	Tani 42	Tank 43	Tank 44	Tank 45	Tank 46	Tank 47	Tani 48	Tank 49	Tank 50	Tank 51	Tank 32	Tank 53	Tank 54	Tank 55	
Jan-March	29.1%	20.1%	28.0%	28.0%	27.5%	27.5%	28.0%	28.0%	27.5%	275%	29.4%	20406	0.0%	20.1%	25.0%	29.19	76.2% 23.8%	1
April June July Sep	24.7%	73.79	24.4%	244% 233%	24.7% 23.6%	23.09	24.4% 23.3%	233%	24.7% 23.6%	23.5%	23.7% 22.5%	22.5%	0.0%	23.7%	25.0% 25.0%	2.7%	0.0% 0.0%	
Oct - Dec	22,5%		24.3%	/43%	24.2%	4.0	24.3%	4	24.2%		24.4%	44	0.0%		25.0%	4.3	100%	

TOTAL THROUGHPUTS

RVP SCHEDULE³ 15.0 15.0 15.0 13.5 83 83 83 83 10.9 13.5 15.0

OZONE SEASON THROUGHPUTS

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MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL TANK EMISSIONS - 2008 ANNUAL EMISSIONS

Total VOC Emissions from Tauks

Tank ID	Туре	ontents	Total losses (lb/yr)	Trital insses: (top/yr)
1K-9 "	Vertical Fixed Roof	Additives	89.00	0.04
TK-10	Vertical Fixed Roof	Additive	89.00 🖁	0.04
TK-41	Internal Floating Roof	Ethanol	278.42	0.14
IK-42	Internal Floating Roof	Ethanol	276.99	0.14
TK 48	Internal Floating Roof	Gasolme	1,440.59	0.72
TK-44	Internal Floating Roof	Gasoline	1,396.44	9.70
TK-45	Internal Floating Roof	Ethanol	276.99	014
TK-46	Internal Floating Roof	Ethanol :	255.99	043
TK-47	Internal Floating Roof	Gasoline	2,223.53	171
TK 48 2	Internal Floating Roof	Gasoline:	2,223.53	1911
IK-49	Internal Floating Roof	Gasoline	2,421.41	4 × 4 × 420
IK 50	Internal Floating Roof	Gasoline	2,421.41	1/21
IK-SI	Horizontal Fixed Roof	Additive	- 1	
TK-52	Horizontal Fixed Roof	Additive	34.58	0.02
IK:53:	Horizontal Fixed Roof	Contact Water	- 8	
JK-54	Herizontal Fixed Roof	Additive	44.27	0.02
TK-55	Horizontal Fixed Roof	Diese	1.44	0.00
100 mg/s		Total	13473.59	6.74

Total HAP Emissions from Tanks

Tank ID		P. Santi	Hexane MTBE	Toluene Xylénes	Naphthalene 3½24-Trimethylbeitzene	Total pollutant
Tank ID	1 ype	Benzene Bthylbenzene (ton/yr) (ton/yr)	(lon/yr) (lon/yr)	(ton/yr) (ton/yr)	(ton/yr) (ton/yr)	(ton/yr)
K-9 Add	Vertical Fixed Roof	0.001	0.000 0.000	0.001 0.000	0.000 0.000	0.00
TK-10 Add	Vertical:Fixed Roof	0.001 0.000	0.000	0.0010.000	0.000	0.00
K-41 ETDy	Internal Floating Roof	0.000	0.000	0.000	0.000	0.00
K-42 ETOK	Internal Fibating Roof.	0.000	0.000 0.000	0.000	0.000 6.000	0.00
K-43 G-	Internal Floating Roof	0.002 0.000	0.004	0.003 0.001	0.000	0.01
K-44 &	Internal Floating Roof	0.002	0.004 0.001	0.003	0.000 0.000	0.01
K-45 € 1°64	Internal Floating Roof	0.000 0.000	0.000	0.000	0.000 0.000	0.00
K-46 & FOIT	Internal Floating Roof	0.000 6 000	0.000	0.000 0.000	0.000	0.00
K-47 <i>G</i> -	Internal Floating Roof	0.003	0.006 0.002	. 0.005 0.002	0.000	0.02
K-48 · &	Internal Floating Roof	0.003 0.000	0.006 0.002	0.005	0.000	0.02
K-49 &	Internal Floating Roof	0.004 0.000	0.007 0.002	0.005	0.000	0.02
K-50 &	Internal Ploating Rivor	0.004 0.000	0.007 0.002	0.005	0.000	0.02
TK-51 AN	Horizontal Fixed Roof	0.000	0.000	0.000	0.000	0.00
rk-52 Add	Horizonta Fixed Roof	0.000	0.000 0.000	0.000	0.000	0.00
TK-53 Walter	(Inrigental Fixed Roof 2011	0.000	0.000	0.000	0.000	0.00
K-54 Add	Horizontal Fixed Roof	0.000 0.000	0.000	0.000 0.000	0.000	. 0.00
rK-55 Diesel	Horizontal Fixed Roof:	0.000 0.000	0.000 0:000	0.000	0.000 0.000	0.00
	200					
	Totals (ton/yr)	0.02 2.3(£-03)	0.04	0.03	1.3E-05 0.001	
						0.11
				Total emissions		0.11
				(ton/yr)		

	VOC (lb/yr)	Benzene	Ethylbenzene	Hexme	MTBE	Toluene	Xylones	Naphthalene	1,2,4-Trimethylbenzene	Total
Fixed Roof Tanks	258.2900	4.09	1.15	0.88	0.00	3.88	2.58	8.7E-04	0.00	12.60
Floating Roof Tanks	13215.3000	40.19	3.48	70.15	22.08	55.42	18,49	0.02	1.38	211.21

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL TANK EMISSIONS - 2008 ANNUAL EMISSIONS

Total Standing Loss VOC Emissions from Gasoline Tanks

Tenk ID	Турс	Contents	Standing (Ib 97)
TK-41 Inter	nal Floating Roof	Ethanol	203 12
TK-45° Inter	nal Floating Roof	Etharol	201.69
IK-43 Inter	nal Floating Roof	Gasoline	1516472
TK-44 Inter	nal Floating Roof	Gasoline	1-258-05
IK-45 Inte	nal Floating Roof	Ethanol	201.69
TK 46 Inter	nal Floating Roof	Ethanol	217.46
TK-47 Inter	nal Floating Roof	Crasoline	190091
IK-48 Inter	nal Floating Roof	Gasoline	1,900.91
TK-49 Inte	nal Floating Roof	Gasoline	2,291.69
TK-50 Inter	nai Floating Roof	Gasoline	2,291.69
		r Tetal	* 11831.93

Total Standing Loss HAP Emissions from Gasoline Tanks

			•		•	
Tank ID	Туре	Benzene Ethylbenzene	Hexane MIBI	Toluene Xylenes	Naphthalene 1,2,4-Trimethylbenzene	Total pollutant
		(lb/yr) (lb/yr)	(lb/yr) (lb/yr)	(lb/yr)(lb/yr)	(lb/yr) (lb/yr).	(lb/yr)
TK-41	Internal Floating Roof	0.428 .0.022	0.411 0.000	0.342 0.119	0.000 0000	1.32
TK-42	Internal Floating-Roof	0.425 0.022	0.408 0.600	0.340 0.118	0.000 6 0.000	1.31
TK-43	Internal Floating Roof	4.265 0.378	7.647 2:484	6.031 2.009	0.003 0.156	22.97
TK-44	Internal Floating Roof	3.931 0,348	7.049 2.290	5.559 1.852	0.003	21.18
TK-45	Internal Floating Roof	0.425 0.022	0.408 0.000	0.340	0.000 0.000	1.31
TK-46	Internal Floating Roofs 6.5	0.458 0.024	0.440 0.000	0.366 0.127	0.000 0.000	1.42
TK-47	Internal Floating Roofs	5.940 0.527	10.651 3.461	8.400 2.798	0.004 5 0.217.	32.00
TK-48	Internal Elbating-Roof - 1	5,940 0.527	10.651 3/361	8.400	0.004 0.217	32.00
TK-49	Internal Floating Roof	7.162 0.635	/ 12.840 4.172	10.127	0.005	38.57
TK-50	Internal Floating Roof	7.162 0.635	12.840 4:172	10.127	0.005 0.261	38.57
i	- 100 miles					
	Totals (lb/yz)	36.14	63.34 20.04	50.03 16.69	0.02	
1						
				Total emissions		190.66
1				(16/yr) _j		

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL TANK EMISSIONS - 2008 ANNUAL EMISSIONS

Total Withdrawal Loss VOC Emissions from Gasoline Tanks

Tank ID	Туре	Contents	Wallidgawal (Ib/yt)
TK-41 Internal	Floating Roof	Biganol	353
TK-42 Internal	Floating Roof	Financi	75.3
TK 43 Internal	Floating Roof	Gasoline.	75:87
TK-44 Internal	Floating Roof	Gasoline	138 38
IK45 Internal	Floating Roof	Ethanole	Establish 1
LK-46 Internal	Floating Roof	Ethanelt	38.54
TK-47 Internal	Floating Roof	Gasoline	302.62
IK-48 Internal	Floating Roof	Gasoline	32262
Tik 49 Internal	Floating Roof	Gasoline	12972
TK-50 Internal	Floating Roof	Gasoline	129.72
		. ↓ Total	11283.40

Total Withdrawal Loss HAP Emissions from Gasoline Tanks

	A CONTRACTOR OF THE PARTY OF TH		Procedurate Southern Stand		NEWSCOOK OF THE STREET		September 1997 - 1997		Acceptance of the second	
Tank ID	Type	Benzene	Pthylbenzene	Hexane	MTBE	Toluene	Xylenes	Naphthalene	1.2.4 Trimethylbenzene	Total pollutant
		(lb/yr)	le (lb/yr)	(lb/yr)	e(lb/yr)	(lb/yr)	(lb/yt)	(lb/yr)	(lbyr).	(lb/yı)
TK-41	Internal Floating Roof	0.159	0.008	0.152	0.000	0.127	0.044	0.000	0.000	0.49
TK-42	Internal Floating Roof	0.159	.0.008	0.152	0.000	0.127	0.044	. 0.000	0.000	0.49
T K-4 3	Internal Floating Roof	0.237	0.021	0.425	0.138	0.335	0.112	0.000	0.009	1.28
TK-44	Internal Floating Roof	0.432	0.038	0.775	0.252	0.612	0.204	0.000	0.016	2.33
TK-45	Internal Floating Roof	0.159	0.0083	0.152	0.000	0.127	0.044	0.000	0.000	0.49
TK-46	Internal Floating Roof	0.081	0.004	0.078	0.000	0.065	0.023	0.000	0.000	0.2
TK-47	Internal Floating Roof.	1.008	0.089	1.808	0.58	1.426	0.475	0.001	0.037	5.43
TK-48	Internal Floating Roof	1.008	0.089	1.808	0.587	1.426	0475	0.001	0,037	5.43
TK-49	Internal Floating Roof 9	0.405	0.036	0.727	0.236	0.573	+ 0491	0.000	0.015	2.18
TK-50	Internal Floating Roof	0.405	0.036	0.727	0.236	0.573	0.191	0.000	0.015	2.18
	200					•				
	Totals (lb/yr)	4.05	0.34	6.80	2 04	5.39	1.80	0.002	0.13	
							Tetal emissions			20.56
							(Tb/yz)			•

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL TANK EMISSIONS - 2008 PEAK OZONE SEASON EMISSIONS

Total VOC Emissions from Tanks

Tank ID		Contents		Total losses
			digital control of	(lb/season)
TK-9		Additive	990	25.59
TK-10	y devailed a state of	Additive		25.59
TK-41	Bugging his constant	Ethanol		80.77
T K-42	A salaha peraka	Ethanol		80.33
TK-43	The properties the Decar	Gasoline		285.83
ГК -4 4	and a first transfer for the second	Gasoline		284.4
TK-45	According to the second	Ethanol		80.3
TK-46	Ground and the Control	Ethanol		76.2
TK-47	strain discount to the	Gasoline	4.36	451.8
TK-48	file and also forestees	Gasoline	190	451.8
ſK-49	more differences which	Gasoline		478.5
FK-50	in careful to the conflict	Gasoline		478.5
ΓK-51	Committee Commit	Additive		
ΓK-52	SOCIETY OF STREET	Additive	10	9.8
ΓK-53	Planton of the college server	Contact Water		
ΓK-54		Additive	16 W	12.7
TK-55	Herry and Color Stage	Diesel		0.5
		TOTAL	0.00	2822.9

Total HAP Emissions from Tanks

	Туре		Ethylbenzene		MTBE		Xylenes		1,2,4-Trimethylbenzene	
			(lb/day)	- Date V	(lb/day)		(lb/day)		(lb/day)	
0.0	Vertical Fixed Roof		0.001		0.000		0.003	0.000	0.000	
TO (0)	Vertical Fixed Roof		0.001		0.000		0.003	600	0.000	
THE STATE OF	Internal Floating Roof		0.000		0.000		0.001		0.000	
100	Internal Floating Roof		0.000		0.000		0.001		0.000	
II.	Internal Floating Roof		0.001		0.006		0.005	1,100	0.000	
112-14	Internal Floating Roof		0.001		0.006		0.005		0.000	0.00
inca.	Internal Floating Roof		0.000		0.000		0.001	100	0.000	
m.	Internal Floating Roof	709	0.000	100	0.000		0.000		0.000	0.00
	Internal Floating Roof		0.001		0.009		0.007		0.001	
Te.	Internal Floating Roof		0.001		0.009		0.007		0.001	
316	Internal Floating Roof		0.001		0.009		0.008	A 100	0.001	
	Internal Floating Roof		0.001		0.009	1.0	800.0	200	0.001	
10.5	Horizontal Fixed Roof		0.000	2 0.00	0.000	0.00	0.000		0.000	
Trees.	Horizontal Fixed Roof	1-0	0.000		0.000		0.001		0.000	
	Horizontal Fixed Roof	5.0	0.000		0.000		0.000	7.5	0.000	
103.	Horizontal Fixed Roof		0.001		0.000		0.001		0.000	
100	Horizontal Fixed Roof		0.000		0.000		-0.000	- 0.000	0.000	
	Total (lb/day)		0.01		0.05		0.05		0.00	
							Total tank			11.
	<u> </u>						emissions (lb/day)			

HAP Speciation Profiles Used

All gas considered "Worst Case Gasoline"				
wt fraction 1				
Велгене	0.003125			
ethylbenzene:	0.0003			
nexane	0.0056			
VIBE (RFG)	0.001821			
oluene	0.0044			
rylenes	0.0015			
Naphthalene	0.000002			
1,2,4-Tramethylbenzene	0.000114			

Distillate used for fugitives and VRU for other facilities				
	wt fraction 1			
Benzene	0.002			
Ethylbenzene	0.003			
Hexane	0.0005			
VITBE	0.00			
Foluene	0.025			
Xylenes	0.012			
Vaphthalene	0.0006			
1,2,4-Trimethylbenzene	0.0032			

All additives considered as a "worst-case" additive: Star Jet Kerosene		
	wt fraction 1	
Benzene	0.01593	
ethylbenzene	0.00448	
hexane	0.00343	
MTBE	0.00	
toluene	0.01498	
xylenes	0.00997	
Naphthalene	0.00	
1,2,4-Trimethylbenzene	0.00	

Denatured Ethanol Speciation					
wt fraction ¹					
Benzene.	0.00211				
Ethylbenzene	0.00011				
-Hexane	0.00202				
MTBE	0.00				
Toluene	0.00168				
Gylene Gylene	0.00059				
Naphthalene	0.0000003				

¹ The revised Shell HAPs speciation for gasoline, additive, distillate and ethanol was provided by Dave Bier of Motiva on 5/23/07. Dave confirmed to use the same speciation as NJ terminals for NY terminals per 4/7/08 email.

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL

:			Stream Properties		и	JADING K
	Variable	Units	Gas Andrews	Distillato	Additive	Ethanol
	Saturation Factor, S		1.0	1.0	1.0	1.0
	Vapor Molecular Weight, MW	lb/lbmol	6:1	130	120	46.07
	Trije Yapor Pressure, P	psia	9.59 40 5.631	0.0054	U.35	1.86
	Lithud Temperature, T	Deg F	53.2	53.2	53.2	53.2
	isiquid Temperature, R	Deg R	515.2	513.2	513.2	513.2
	Throughput	1000 gal/yr	280,323	10	70	31.176

Vapor Recovery Unit (VRU) Specifications

,		
Variable	Units	Value
Capture Efficiency (MACT)	-,	98.7
VRU Rating	mg/liter	1.93
	R/1000 gal	0.016

Loading Rack Emission Rate - Gas

Variable	Equation	Results	Units
Conding Loss Factor, L ₁	12.46 * (S * P * MW)/T	8.63	lb/1000 gal
Foading Loss	L _L (lb/1000 gal) * Throughput	1,209	tpy
VRU:Imput	Loss (lb/yr) * Capture Efficiency/100	1,193	tpy
/RU Emissions (Cutput)	Throughput * VRU Rating	2:26	toy
lack Figitive Emissions	Loss (lb/yr) * (1 - Capture Efficiency/100)	15.72	tpy
otal Emissions	VRU Emissions + Rack Fugitives	17.98	tpy
VRU Control Efficiency	(Input - Output) / Exput	99.81	%

Loading Ruck Emission Rate - Distillate

Variable	Equation.	Results	Units
Loading Loss Factor, L	12.46 * (S * P * MW)/T	0.02	lb/1000 gal
Loading Loss	L _L (lb/1000 gal) * Throughput	0.18	lb/yr
VRU-Emissions	Loss * Capture Efficiency/100 *(1 - VRU Control Efficiency/100)	0.00	lb/yr
Rack Fogitive Emissions	Loss (lb/yr) * (1 - Capture Efficiency/100)	0.00	lb/yr
Total	VRU Emissions + Rack Fugitives	0.00	lb/vr

Loading Rack Emission Rate - Additive

Variable	Equation	Results	Units
Loading Loss Factor, L	12.46 * (S * P * MW)/T	1.05	lb/1000 gal
Loading Loss	L _L (lb/1000 gal) * Throughput	73.01	lb/yr
VRU Emissions	Less * Capture Efficiency/100 *(1 - VRU Control Efficiency/100)	0.14	1b/yr
Rack Fugitive Emissions	Loss (lb/yr) * (1 - Capture Efficiency/100)	0.95	lb/yr
Total	VRU Emissions + Rack Fugitives	1.09	lb/yr

Loading Rack Emission Rate - Ethanol

Variable	Equation	Results	Units
Loading Loss Factor, L	12.46*(S * P* MW)/T	2.08	lb/1000 gal
Loading Loss	LL (lb/1000 gal) * Throughput	32.43	фу
VRU Input.	Loss (tpy) * Capture Efficiency/100	32:01	tpy
/RU Emissions (Output)	Throughput * VRU Rating	0.25	tpy
Rack Fugitive Emissions	Loss (tpy) * (1 - Capture Efficiency/100)	0.42	tpy
RU Control Efficiency	(Input - Output) / Joput	50 €99,22	%
Total Emissions	VRU Emissions + Rack Fugitives	0.67	tpy

MOTIVA ENTERPRISES, LLA DINCORDA IN LESSIONS LOADING RACK EMISSIONS - 2008 ANNUAL EMISSIONS From Leading Rack

2505000000000000000	VOC Emissions (ton/yr)	VOC Emissions (ton/yr)	Total
Foei	VRU Emissions	Rack Figitives	(lon/yr)
Gas		2.26 15.72	17.98
Distillate		0.00	0.00
Additive		0.00	0.00
Ethanol		0.25 0.42	0.67
Total		2.51	18.65

Hazardous Air Pollutant Speciation Data

Hazardon Air Pollutant	CAS#	Emission Factor (mg/L) Gas	Vapor Weight % Dist] ste ²	Vapor Weight % Additive ²	Vapor Weight % Ethanol
Benzene	71-43-2	0.001610	3.00	0.14	0.21
Ethy@enzene	100-41-4	0.002010	0.25	0.44	0.01
Hexane	110-54-3	0.011000	1.00	0.28	0.20
SOOCTAINE MTBE	540-84-1	0.017700	-	New Address of the Control of the Co	-
MTBE	1634-04-4	0.00374	-		0.17
Tolucte	108-88-3	0.005390	1.65	1.37	0.06
Xylenes	1330-20-7	0.012200	0.87	0.90	0,00
Naphthalene			0.04	0.11	0.00003

- Generalize emission figure data obtained from Table S.A of the Horsesbore Air Pollutzet Emissions from Generalize Decoding Operations at Bulk Generalize Terminals, Optober 1998

Loading Rack Fugitives Harardous Air Pollutant Speciation Data

Hazardou Air Polhtan [‡]	CAS#	Emission Factor Vapor wt % Gas	Vapor Weight % Distillate ²	Vapor Weight % Additive ²	Vaper Weight % Ethanol
Benzene	71-43-2	0.3125	3.00	0.14	0.21
Ethylbenzene	100-41-4	0.0277	0.25	0.44	10.0
Hexane	110-54-3	0.5603	1.00	0.28	0.20
Isooctage	540-84-1	\$\$\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	_		
MTBE	1634-04-4	0.182	-		0.17
Toluege	108-88-3	0.442	1.65	1.37	0.06
Kyjenes	1330-20-7	0.147	0.87	0.90	0.00
Naphthalene I ,2,4-Trimethylbenzene		0,0002 0.011	0.04	0.11	0.00

- 1. Reformalised Crygorosted gospline with MTRE speciation data provided by Dave Bier of Markon Paterpoises on \$15077 for N1 Terminate

Hazardous Air Pollutant Emissions by Emission Source - Loading Rack Fugitives

	•					
Hazardous Air Pollutant	CAS#	Emissions (lb/yr)	Emissions (lb/yr) Distillate	Emissions (lb/yr) Additive	Emissions (lb/yr) Ethanol	Total (lb/yr)
Benzene	71-43-2	98.24	0.00	0.00	1.78	100.02
Ethylbenzene	100-41-4	871	0.00		0.09	8.80
Hexane	110-54-3	176.14	0.00	0.00	1.71	177.85
sooctane	540-84-1	\$40 P. A. A. B.	-		-	-
MTBE	1634-04-4	57.23	-		1.42	58.65
l'oluene	108-88-3	138.92	0.00	10.01	0.49	139.43
Cylenes	1330-20-7	46.28	0.00	0.01	0.00	46.28
Vapathalene		0.06	0.00	0.00	0.00	0.06
,2,4-Trimethylbenzene		3.58			-	3.58
Total		520 17	0.00	0.03	5.49	534.69

Hazardeus Air Poliutant Emissions by Emission Source - VRU

Hazardous Air Pollutant	CAS#	Emissions (lb/yr) Gas	Emissions (lb/yr) Distillate	Emissions ('b/yr) Additive	Emissions (lb/yr) Ethanol	Tota! (lb/yr)
Benzene	71-43-2	3.72	0.00	0.00	1.06	4.82
thylbenzene :	100-41-4	4.70	0.00	0.00	0.06	4.76
lexane.	110-54-3	25.73	0.00	0.00	1.02	26.75
ooctane	540-84-1	41.40				41.40
ITBE	1634-04-4	8.22			0.85	9.06
oluene	108-88-3	12.61	0.00	0.00	0.29	12.90
ylenes .	1330-26-7	28.54	0.00	0.00	0.00	28.54
aphthalene		MARKET REPORTS	0.00	0.00	0.00	0.00
2,4-Trimethylbenzene					•	-
Total		124.96	0.00	0.00	3.27	128.24

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MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL LOADING RACK EMISSIONS - 2008 PEAK OZONE SEASON EMISSIONS

Stream Properti

Variable	Units	Gas Gas	Distillate	Additive	Ethanel
Saturation Factor, S	-	\$10	1.0	1.0	. 1.0
Yapor Molecular Weight, MW	lb/lbmol	631	130	120	46.07
True Vapor Pressure, P	psia	5.631	0.0054	0.36	1.86
Liquid Temperature, T	Deg F	53.2	53.2	53.2	53.2
Liquid Temperature, R	Deg R	513.2	513.2	513.2	513.2
Throughput	1000 gal/yr	68 324	0	17	7,583

Vapar Recovery Unit (VRU) Specifications

Variable	Units	 Value
Capture Efficiency (MACT)	-	98.7
VRU Rating	mg/liter	1.93
	Ib/1000 gal	0.016

Loading Rack Emission Rate - Gas

Variable	Equation	Results	Units
Loading Loss Factor, L.	12.46 * (S * P * MW) / T	8.63	lb/1000 gal
Loading Loss	L _L (lb/1000 gal) * Throughput	589,415	lb/season
VRO Imput	Loss (lb/yr) * Capture Efficiency/100	581,753	lb/season
VRU(Einlistions (Output)	Throughput * VRU Rating	1,100	Ib/season
Rack/Fuguive Emissions	Loss (lh/yr) * (1 - Capture Efficiency/100)	7,662	lb/season
Total Emissions	VRU Emissions + Rack Fugitives	8,763	lb/season
VRU Control Efficiency	(Input - Output) / Input	99.81	%

Loading Rack Emission Rate - Distillate

Vanable	Equation	Results	Units
Loading Loss Factor, L	12.46 * (S * P * MW)/T	0.02	1b/1000 gal
Eoading Loss	L _L (lb/1000 gal) * Throughput	0.00	lb/season
VRU Emissions	Loss * Cupture Efficiency/100 *(1 - VRU Control Efficiency/100)	0.00	lb/season
Rack Fugitive Emissions	Loss (lb/yt) * (1 - Capture Efficiency/100)	0.00	lb/season
Total	VRU Emissions + Rack Fugitives	0.00	lb/season

Loading Rack Emission Rate - Additive

Variable	Equation	Results	Units
Loading Loss Factor, L	12.46 * (S * P * MW)/T	1.05	lb/1000 gal
Loading Loss	L _L (lb/1000 gal) * Throughput	18.24	lb/season
/RU Emissions	Loss * Capture Efficiency/100 *(1 - VRU Control Efficiency/100)	0.03	lb/season
Rack Fugitive Emissions	Loss (lb/yr) * (1 - Capture Efficiency/100)	0.24	lb/season
Total	VRU Emissions + Rack Fugitives	0.27	lb/season

Loading Rack Emission Rate - Ethanol

Variable	Equation	Results	Units
Eoading Loss Factor, L	12.46 * (S * P * MW) / T	2.08	1b/1000 gal
Loading Loss	L. (lb/1000 gal) * Throughput	15,775.29	lb/season
VRU Input	Loss (tpy) * Capture Efficiency/100	15,570.21	lb/season
RUEmissions (Output)	Throughput * VRU Rating	-122.11	lb/season
Rack Fugitive Emissions	Loss (tpy) * (1 - Capture Efficiency/100)	205.08	lb/season
ZRTI Control Efficiency	(Japut - Output) / Japut	39.22	%
Total Emissions	VRU Emissions + Rack Fugitives	327.19	lb/season

Total VOC Emissions from Loading Rack

Fuel	VOC Emissions (ton/season) VRU Emissions	VOC Emissions (ton/scason) Rack Fuguiyes	Total (ton/season)
Gas	0.	55 3.83	4.38
Distillate	-		-
Additive	0.000	0.00012	0.00014
Ethanel	0.	06 0.10	0.16
Total	0.	61 3.93	4.55

Hazardous Air Pollutant Speciation Data

Hazardous Air Polluran ²	CAS#	Emission Factor (mg/L)	Vapor Weiglu % Distilate ²	Yapor Weight %	Vapor Weight% Ethanol
Benzene	71-43-2	0.001610	3.00	0.14	0.21
Ethylbenzene	100-41-4	0.002010	0.25	0.44	0.01
Hexane	110-54-3	0.011000	1.00	0.28	0.20
Isoociane	540-84-1	0.017700			-
MTBE	1634-04-4	0.00374			0.17
Toluene	108-88-3	0.005390	1.65	137	0.06
Xylenes	1330-20-7	0.012200	0.87	0.90	0.00
Naphtialene			0.04	0.11	0.00003

- Gardine emission factor data obtained from Table 5-3 of the Hazardous Air Pollutant Emissions from Gasoline Unloading Operations at Bulk Gasoline Terrainals, October 199
- 2 Secretize data derived from information contained in the Countitation of Att Tenissian Express for Developm Distribution and Parall Machanian Explicite Sectionals 1005

Loading Rack Fugitives Hazardous Air Pollutant Speciation Data

Hazardous Air Pollutan ²	CAS#	Emission Factor Vapor wt % Gas	Vapor Weight % Distillate ²	Vapor Weight % Additive ²	Vapor Weight % Ethanol
Benzene	71-43-2	0.3125	3.0	0.14	0.21
Ethyllonzone	100-41-4	0,0277	0.2	0.44	0.01
Hexare	110-54-3	0.5603	1.0	0.28	0.20
Isooctane	540-84-1		-		-
MTBE	1634-04-4	0.182	-	\$455 materials	0.17
Tolueze	108-88-3	0.442	1.6	1.37	0.06
Xylenes	1330-20-7	0.147	0.8	7 0.90	0.00
Naphthalene		0.0002	0.0		0.00
1,2,4-1 nmethylbenzene		0.011		PERSONAL REP	

- Reformulated/Oxygenated gesoline with NTBE speciation data provided by Dave Bir: of Motiva Enterprises on 5/16/07 for NJ Terminals.
- 2. Speciation data derived from information contained in the Compilation of Air Entission Factors for Petroleum Distribution and Retail Marketing Facilities, September 1995.

Hazardons Air Pollutant Emissions by Emission Source - Loading Rack Fugitives

Hazardous Air Pollutant	CAS#	Emissions (Ih/season) Gas	Emissions (lb/season) Distillare	Emissions (lb/season) Additive	Emissions (lb/season) Ethanol	Total (lb/season)
Scozene .	71-43-2	23.94	-	0.00033	0.43	24.38
thylbenzene	100-41-4	2.12	-	0.00104	0.02	2.15
lexane .	110-54-3	42.93		0.00066	0.41	43.35
ooctane)	540-84-1		-			
CTDB:	1634-04-4	13.95	-	表写,影影、图像感	0.35	14.29
oluene	108-88-3	33.86	-	0.00325	0.12	33.98
lylenes	1330-20-7	11.28	-	0.00213	0.00	11.28
laphinalene		0.02		0.00026	0.00	0.02
2,4 Trimethylbenzene	,	0.87		- 技術科学		0.87
Total		128.98	-	0.00768	1.33	130.32

Hazardous Air Pollutant Emissions by Emission Source - VRU

Hazardous Air Pollutant	CAS#	Emissions (lb/season) Gas	Emissions (lb/season) Distillate	Emissions (lb/season) Additive	Emissions (lb/sesson) Ethanol	Total (lb/season)
Benzene	71-43-2	0.92	-	0.000048	0.26	1.18
Ethylbenzene	100-41-4	1,15	-	0.000150	0.01	1.16
Hexane	110-54-3	6.27	-	0.000095	0.25	6.52
Isoociane	540-84-1	10.09	-			10.09
MTDE	1634-04-4	2,00	-		0.21	2.21
Toluene	108-88-3	3.07		0.000467	0.07	3.14
Xylenes	1330-20-7	6.56	_	0.000307	0.00	6.96
Naph halene		2000	-	0.000037	0.00	0.00
1,2,4-Trimethylbenzene			-			-
Total		30.46		0.001103	0.79	31,25

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MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL FUGITIVE EMISSIONS - 2008 ANNUAL EMISSIONS

Total Volatile Organic Compound (VOC) Emissions by Component Type

Component Type	Service	Average Emission Factor (lb/hr)/source	Quantity	VOC Emissions (lb/hr)	VOC Emissions (ton/yr)
Valves	Vapor	0.00002866	10	0.00	0.00
	Light Liquid	0.00009480	926	0.09	0.38
Pump Seals	Vapor	0.00014330	-	•	- j
	Light Liquid	0.00419000	31	0.04	0.16
Others ²	Vapor	0.00026500	-	•	-]
	Light Liquid	0:00028700	90	- 0.03	0.11
Fittings ³	Vapor	0.00009259	64	0.01	0.03
	Light Liquid	0:00001764	5,542	0.10	0.43
	•		Total	0:25	1.11

^{1.} These factors are for real organic compound emission rates (including non-VOC's such as methane and ethane). Emission factors extracted from the U.S. EPA Proceed for Equipment Leak Emission Estimates

Publication No. EPA-4579, 05.017 Table 2.3. Marketing Terminal Average Projection Partors

Total Volatile Organic Compound (VOC) Emissions by Service

Service	VOC Emissions (lb/hr)	VOC Emissions (ton/yr)
Mapor	0.01	0.03
Light Liquid	0.25	1.09
Total	0.25	1.11

Hazardous Air Pollutant Speciation Data

HAP	CAS#	Vapor wt% ⁴
Benzene	71-43-2	0.3125
Ethylbenzene	100-41-4	0.0277
Hexane	110-54-3	0.5603
Isooctane	540-84-1	· ·
MTBE	1634-0 4-4	0.18205
Toluene	108-88-3	0.4419
Xylenes	1330-20-7	0.1472
Naphthalene		0.0002
1,2,4-Trimethylbenzene		0.0114

Reformulated/Oxygenated gasoline with MTBE speciation data provided by Dave Bier of Motiva Enterprises on 5/16/07 for NJ Terminals.

Assumes worst case according for security of passenger of casoline.

Total Hazardous Air Pollutant Emissions from Process Fugitive Emissions

HAP	CAS#	Emissions (lb/yr)
Benzene	71-43-2	6.97
Ethylbenzene	100-41-4	0.62
Hexane	110-54-3	12.49
Isooctane	540-84-1	
MTBE	1634-04-4	4,06
Toluene	108-88-3	9.85
Xylenes	1330-20-7	3.28
Naphthalene		0.00
1,2,4-Trimethylbenzene		0.25
Total		37.53

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^{2.} The "other" equipment type should be applied for any equipment type other than fittings, pumps, or valves.

^{1. &}quot;Fittings" were not identified as flanges or non-flanged connectors; therefore, the fitting emissions were estimated by averaging the estimates from the connector and the flange correlation equations

MOTIVA ENTERPRISES, LLC BROOKLYN TERMINAL FUGITIVE EMISSIONS - 2008 PEAK OZONE SEASON EMISSIONS

Total Volatile Organic Compound (VOC) Emissions by Component Type

Component Type	Service	Average Emission Factor (lb/hr)/source	Quantity	VOC Emissions (lb/day)	VOC Emissions (Ib/season)
Valves Vapo	r	0;00002866	10	0.01	0.66
Light	Liquid	0.00009480	926	2.11	193.74
Pump Seals Vapo	г	0:00014330	-		-
Light	Liquid	0:00119000	31	0.89	81.98
Others ² Vapo	r	0.00026500	-		-
	Liquid	0.00028700	. 90	0.62	56.84
Fittings ³ Vapo	r	0.00009259	64	0.14	13.02
Light	Liquid	0.00001764	5,542	2.35	215.82
			Total	6.11	562.06

¹⁻ These factors are for total organic compound emission rates (including non-VOC's such as methane and ethane). Emission factors extracted from the U.S. EPA Protocal for Equipment Leak Emission Estimates Publication No. EPA-453/R-95-017, Table 2-3, Marketing Terminal Average Emission Ractors.

Total Volatile Organic Compound (VOC) Emissions by Service

Service	VOC Emissions (lb/day)	VOC Emissions (lb/season)
Vapor	0.15	13.68
Light Liquid	5.96	548.38
Total	6.11	562.06

Hazardous Air Pollutant Speciation Data

HAP	CAS#	-Vapor wt% ⁴
Benzene	71-43-2	.0.3125
Ethylbenzene	100-41-4	0.0277
Hexane	110-54-3	.0,5603
isooctane	540-84-1	
MTBE	1634-04-4	0.18205
Toluene	108 - 88-3	0.4419
Xylenes	1330-20-7	0.1472
Naphthalene		0.0002
1,2,4-Trimethylbenzene		0.0114

^{*}Normal gaseline speciation data chaland from the Compilation of Air Emission Factors for Petroleum Distribution and Retail Marketing Facilities, September 1995.
Assumes word case scenario of year-round transport of gaseline.

Total Hazardous Air Pollutant Emissions from Process Fugitive Emissions

HAP	CAS#	Emissions (lb/season)
Benzene	71-43-2	1.76
Ethylbenzene	100-41-4	0.16
Hexane	110-54-3	3.15
Isooctane	540-84-1	
MTBE	1634-04-4	1.02
Tohiene	108-88-3	2.48
Xylenes	1330-20-7	0.83
Naphthalene		0.00
1,2,4-Trimethylbenzene	•	0.06
Total		9.46

² The "other" equipment type should be applied for any equipment type other than fittings, pumps, or valves.

^{3. &}quot;Fittings" were not identified as flanges or non-langed connectors; therefore, the fitting emissions were estimated by averaging the estimates from the connector and the flange correlation equations.

APPENDIX B

TANKS 4 OUTPUT

Motiva Enterprises, LLC

TANKS ...9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

		ca		

User Identification: BK009
City: Bracklyn
State: NY

Company: SHELL OIL COMPANY - BROOKLYN

Type of Tank: Vertical Fixed Roof Tank

Description:

Tank Dimensions

Shell Height (ft): 16.00 11.00 Diameter (ft): Liquid Height (ft) : 14.00 Avg. Liquid Height (ft): 5.50 8,400.00 Volume (gallons): 2.81 Tumovers: Net Throughput(gal/yr): 23,598.00 Is Tank Heated (v/n): Ν

Paint Characteristics

Shell Color/Shade: White/White
Shell Condition Good
Roof Color/Shade: While/White
Roof Condition: Good

Roof Characteristics

 Type:
 Cone

 Height (ft)
 0.34

 Slope (ft/ft) (Cone Roof)
 0.06

Breather Vent Settings

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK009 - Vertical Fixed Roof Tank Brooklyn, NY

			Daily Liquid Surf mperature (deg		Liquid Bulk Temp	Va.	por Pressure (p	sia)	Vapor Mol.	Liquid Mass	Vapor Mass	Moi.	Basis for Vapor Pressure
dure/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight	Fract.	Fract.	Weight	Calculations
neric Addžive	Jan	44.31	41,43	47.20	53,22	0.3600	0.3600	0,3600	120.0000		······································	1,410.00	Option 1: VP40 = .36 VP50 = .36
neric Additive	Feb	45.17	41.85	48.49	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36
neric Additive	Mar	48.86	45.12	52.60	53.22	0.3800	0.3800	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36
neric Additive	Apr	53.89	49.28	58.51	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP50 = .36 VP60 = .36
nenc Additive	May	58.34	53.45	63.23	53.22	0.3600	0.3600	0,3600	120.0000			1,410.00	Option 1: VPS0 = .36 VP60 = .36
neric Addilive	Jun	62.56	57.55	67.57	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP50 = .36 VP70 = .36
neric Additive	Jul	65.18	60,26	70.09	53.22	0.3600	0.3500	0,3600	120.0000			1,410.00	Option 1: VP80 = .36 VP70 = .38
neric Additive.	Aug	64.49	59.83	69.14	53.22	0.3600	.0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
neric Additive	Sep	61.09	56.69	65.49	53.22	0.3600	0.3500	0,3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
neric Additive	Oct	56.03	52.02	60.04	53,22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP50 = .36 VP60 = .36
neric Additive	Nov	51.02	47.86	54.17	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP50 = .36 VP60 = .36
neric Additive	Dec	46.12	43.39	48.86	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1; VP40 = .36 VP50 = .36

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK009 - Vertical Fixed Roof Tank Brooklyn, NY

							***********		······································			
Month:	January	February	March	April	May	June	July	August	September	October	November	December ————
Standing Losses (lb):	3.8856	4.1462	5.1985	6.2635	6.7870	6.6270	6.6337	6.2602	5.7655	5.4671	4.0701	3,6185
Vapor Space Volume (cu ft):	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,003.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008,7138
Vapor Density (lb/ou ft):	0.0080	0.0089	0.0079	0.0078	0.0078	0.0077	0.0077	0,0077	0.0077	0.0078	0.0079	0.0080
Vepor Space Expansion Factor:	0.0187	0.0221	0.0253	0.0318	0.0336	0.0342	0.0333	0.0313	0.0298	0.0269	0.0205	0.0175
Vented Vapor Saturation Factor:	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.5316	0.8316	0.8316	0.8316	0.8316	0.8316
Tank Vapor Space Volume:												
Vapor Space Volume (cu ft):	1,008,7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1,008.7138	1.008.7138	1,008.7138
Tank Diameter (fl):	11.0000	11.0000	11,0000	11.0000	11.0000	11.0000	11,0000	11,0000	11.0000	11.0900	11.0000	11.0000
Vapor Space Outage (fl):	10.6143	10.6143	10.6143	10.6143	10.6143	10.6143	10.6143	10.6143	10.6143	10.6143	10.6143	10.6143
Tank Shell Height (ft):	18.0000	16.0000	16,0000	16.0000	16,0000	16,0000	16,0000	16,0000	16.0000	16,0000	16,0000	16.0000
Average Liquid Height (ft):	5.5000	5.5000	5.5000	5.5000	5.5000	5,5000	5.5000	5.5000	5.5000	5.5000	5.5000	5.5000
Roof Outage (fi):	0.1143	0.1143	0.1143	0.1143	0,1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143
Roof Outage (Cone Roof)	2440	0.440	04440	2442	0.4440	0.4440	84440	04440	0.4410	2442	04447	0.4442
Roof Dutage (fi):	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143 0.3430
Roof Height (ft):	0.3430	0.3430	0.3430	0.3430	0.3430	0.3430	0.3430	0.3430	0.3430	0.3430	0.3430	0.3430
Roof Slope (ft/ft):	0.0624	0.0624	0.0624 5.5000	0.0624	0.0824	0.0624	0.0624	0.0624	0.0624 5.5000	0.0624 5.5000	0.0624 5.5000	5,5000
Shell Radius (fi):	5.5000	5.5000	5,5000	5,5000	5.5000	5.5000	5,5000	5.5000	5.5000	5.5000	5.5000	5.5000
Vepor Density	4 2400	0.000	g.co.**	D 0075	0.0070	2.0077	0.0077	0.0077	0.0077	0.0070	0.0079	0.0080
Vapor Density (lb/cu fl):	0.0080	0.0080	0.0079	0.0078	0.0078	0,0077				0.0078		
Vapor Molecular Weight (lb/lb-mole):	120,0000	120.0000	120.0000	120.0000	120.0000	120.0000	120,0000	120,0000	120,0000	120.0000	120,0000	120,0000
Vapor Pressure at Daily Average Liquid		0.0000	2.000	0.0000	0.0000	A 8500	0.0000	0.0000		0.000	0.3600	0.3600
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	. 0.3600	510.6856	505,7950
Daily Avg, Liquid Surface Temp, (deg, R):	603.9812	504.8409	508.5307	513.5620 50,3000	518.0109	522.2313	524,8471	524,1592	520,7602	515.6984	46.4000	35,7000
Daily Average Ambient Temp. (deg. F); Idea! Gas Constant R	31,3000	32,5000	39,9000	50,3000	59.7000	68.9500	74,9500	74.0000	67,2000	56.7000	40.4000	30.7000
{ psia cult / (lb-mol-deg R)}:	10,731	10.731	10.731	10.731	10.731	10,731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	512.8900	512,8900	512.8900	512.8900	512,8900	512,8900	512.8900	512,8900	512.8900	512.8900	512.8900	512.8900
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1760	0.1700	0.1700	0.1700	0.1700	0.1700	0,1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof);	0.1700	0.1700	0,1700	0.1700	0.1700	0,1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation	0.1100	011100	0.1700	V.(100	0.11.00	0.1100	0.7100	0.1700	0.1700	0.7700	0.1100	000
Factor (Blu/sqfl day):	548.0000	795.0000	1,118.0000	1,457.0000	1,690.0000	1,802,0000	1,784.0000	1,583.0000	1,280.0000	951,0000	593.0000	457.0000
Vapor Space Expansion Factor			•									
Vapor Space Expansion Factor:	0,0187	0.0221	0.9253	0.0318	0.0336	0.0342	0.0333	0.0313	0.0296	0.0259	0.0205	0.0175
Daily Vapor Temperature Renge (deg. R):	11,5385	13.2882	14.9697	18.4553	19.5644	20.0255	19.6518	18.6231	17.6128	16.0468	12.6147	10.9593
Daily Vanor Pressure Range (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.C000	0.0000	0.0000	0.0000
Breather Vent Press, Selfing Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0800	0.0600	0.0600
Vapor Pressure at Dally Average Liquid								•				
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0,3600
Vapor Pressure at Daily Minimum Liquid												
Surface Temperature (psta):	0.3600	0.3600	0.3800	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600
Vapor Pressure at Daily Maximum Liquid												
Surface Temperature (psla):	0.3800	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	9.3600	0.3600	0.3690	0.3600
Daily Avg. Liquid Surface Temp. (deg R):	503.9812	504.8409	508.5307	513.5620	518.0109	522,2313	524,8471	524.1592	520.7602	515.6984	610.6858	505.7950
Daily Min. Liquid Surface Temp. (deg R):	501,0970	501.5188	504.7883	508,9481	513.1198	517.2249	519.9342	519.5034	518.3570	511.6867	507.5319	503.0551
Daily Max. Liquid Surface Temp. (deg R):	506.8653	508.1629	512.2731	518.1758	522,9020	527.2377	529.7601	528.8149	525.1634	519.7101	513.8393	508.5348
Daily Ambient Temp. Range (deg. R):	12.4000	13.2000	13.4000	16,0000	16.0000	15.9000	15.5000	15,4000	16,0000	16.0000	13.6000	12.2090
Vented Vapor Saturation Factor							•					
Vented Vapor Saturation Factor:	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8318	0.8316	0.8316	0.8316	0.8316	0.8316
Vapor Pressure at Daily Average Liquid:												
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3800	0.3600	0.3600	0.3600	0.3600
Vapor Space Outage (ff):	10,6143	10.6143	10.6143	10.6143	10.8143	10.6143	10.8143	10.6143	10.6143	10.6143	10.6143	10.6143
Working Losses (lb):	2.3822	2.3205	2.3678	2.1291	1.7095	2.1497	2.0304	1,8854	1.8370	1.9029	1,7033	1,8545
Vapor Molecular Weight (foilb-mole);	120,0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0300	120.0000	120.0000	120.0000
Vapor Pressure at Daily Average Liquid						*.						

ANKS 4.0 Report	egen egeneratione											
Surface Temperature (psia): Net Throughput (gal/mo.): Annual Tumovers: Tumover Factor. Maximum Liquid Volume (gal): Maximum Liquid Helight (fi): Tank Diamater (fi): Working Loss Product Factor.	0.3600 2,316.0000 2,8093 1,0000 8,400.0000 14,0000 11,0000	9.3800 2,256.0000 2.8093 1.0000 8,400.0000 14.0000 11.0000	0.3500 2,302,0000 2,8093 1,0000 8,400,000 14,0000 11,0000	0.3600 2,070.0000 2.8093 1.0000 8,400.0000 14.0000 11.0000	0.3600 1,662,0000 2.8093 1.0000 8,400,0000 14,0000 11,0000	0.3600 2,090.0000 2,8993 1,0000 8,400.0000 14,0000 11,0000	0.3600 1,974,0000 2,8093 1,0000 8,400,0000 14,0000 11,0000	0.3600 1,833.0000 2.8093 1.0000 8,400.0000 14,0000 11,0000	0.3600 1,786.0000 2.8093 1.0000 6,400.0000 14.0000 11.0000	0,3800 1,850,0000 2,8093 1,0000 8,400,000 14,0000 11,0000	0.3500 1,658.0000 2.8093 1.0000 8,400.0000 14,0000 11,0000	0.3603 1,803.0003 2.8993 1,0003 6,400.0003 14,0003 11,0003
• • • •				•						•	•	
Total Losses (lb):	6.2678	6.4667	7.5663	0.3926	8.4965	B.7768	8.6641	8.1456	7.602\$	7.3700	5.7734	5.4730
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TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK009 - Vertical Fixed Roof Tank Brooklyn, NY

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Generic Additive	24.27	64.72	89.00

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Id	on	fi	fica	afi	'nп

User Identification: BK010
City: Brooklyn
State: New York

Company: SHELL OIL COMPANY - BROOKLYN

Type of Tank: Vertical Fixed Roof Tank

Description:

Tank Dimensions

Shell Height (ft): 16.00 Diameter (ft): 11.00 Liquid Height (ft): 14.00 Avg. Liquid Height (ft): 5.50 8.400.00 Volume (gallons): 2.81 Tumovers: 23,598.00 Net Throughput(gal/yr): Is Tank Heated (v/n): N

Paint Characteristics

Shell Cotor/Shade: White/White
Shell Condition Good
Roof Cotor/Shade: White/White
Roof Condition: Good

Roof Characteristics

 Type:
 Cone

 ... Helght (ft)
 0.00

 Slope (ft/ft) (Cone Roof)
 0.06

Breather Vent Settings

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Intl Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK010 - Vertical Fixed Roof Tank Brooklyn, New York

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este a la companya di sensiti di sensiti di sensiti di sensiti di sensiti di sensiti di sensiti di sensiti di s			Daily Liquid Surf emperature (deg		Liquid Bulk Temp	Ve	por Pressure (p	aia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Weight	Calculations
Seneric Additive	Jan	44.31	41.43	47.20	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36
Generic Additive	Feb	45.17	41.85	48.49	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .38 VP50 = .36
Generic Additive	Mar	48.86	45,12	52.60	53.22	0.3600	0.3600	0.3600	120.0000		•	1,410.00	Option 1: VP40 = ,36 VP50 = .36
Seneric Additive	Арг	53.89	49.28	58.51	53.22	0.3600	9.3600	0.3600	120,0000			1,410.00	Option 1: VP50 = .36 VP60 = .36
Generic Additive	May	58.34	53.45	63,23	63.22	0.3600	0.3800	0.3600	120,0000			1,410.00	Option 1; VP50 = ,36 VP60 = .36
Seneric Additive	ർശ	62.56	57.55	67.57	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
Seneric Additive	ht	65.18	80.26	70.09	53.22	0.3600	0.3600	0.3600	120,0000			1,410.00	Option 1; VP60 = .36 VP70 = .36
Generic Additive	Aug	64.49	59.83	69.14	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
Semenic Additive	Sep	61.09	56.69	65.4 9	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
Generic Additive	Oct	56.03	52.02	60.04	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP50 = .36 VP60 = .36
Seneric Additive	Nov	51.02	47.86	54.17	53.22	0.3608	0.3600	0.3600	120.0000			1,410.00	Option 1; VP50 = .36 VP60 = .36
Seneric Additive	Dec	46.12	43.39	48,86	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36

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TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK010 - Vertical Fixed Roof Tank Brooklyn, New York

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Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (/b):	3.8857	4.1463	5.1986	6.2636	6.7871	6.6272	6.6338	6.2604	5.7656	5.4673	4,0702	3.6186
Vapor Space Volume (cu ft):	1,008,7376	1,008.7376	1,008,7376	1,008.7376	1,008.7376	1,008,7376	1,008.7376	1,008,7376	1,008,7376	1,008.7376	1,008.7378	1,008.7376
Vapor Density (lb/cu ft):	0,0080	0.0080	0.0079	0.0078	0.0078	0.0077	0,0077	0.0077	0.0077	6.0078	0.0079	0.0080
Vapor Space Expansion Factor:	0.0187	0.0221	0.0253	0.0318	0.0336	0.0342	0.0333	0.0313	8,0296	0.0269	8.0205	0.0175
Venied Vapor Saturation Factor:	0.8316	0.8316	0.8316	0.8316	D.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316
Tank Vapor Space Volume;												
Vapor Space Volume (cu ft):	1,008.7376	1,008.7376	1,008.7376	1,008,7376	1,008,7376	1,008.7376	1,008.7376	1,008. 7 376	1,008.7376	1,008,7376	1,008.7376	1,008.7378
Tank Diameter (ft):	11.0000	11.0000	11,0000	11,0000	11,0000	11.0000	11.0000	11.0000	11.0000	11.0020	11.0000	11.0000
Vapor Space Outage (ft):	10.6146	10.6148	10.6146	10.6146	10.6146	10.6146	10.6146	10,6146	10.6146	10.6146	10.6146	10.6146
Tank Shell Height (ft):	16,0000	16.0000	16.0000	16.0000	16.0000	16.0000	16.0000	16,0000	16.0000	16.0000	16.0000	16,0000
Average Liquid Height (ft):	5.5000	5.5000	5.5000	5.5000	5.5009	5.5000	6.5000	5.5000	5.5000	5.5000	5.5000	5.5000
Roof Outage (ff):	0.1148	0.1146	0.1146	0.1146	D.1146	0.1146	0.1146	0.1146	0.1146	0.1146	0.1146	0.1146
Roof Outage (Cona Roof)												•
Roof Outage (ft):	0.1146	0.1146	0.1146	0.1146	0.1146	0.1148	0.1146	0.1146	0.1146	0.1146	0.1146	0.1146
Roof Helght (ft):	0.0000	8.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Roof Slope (ft/ft):	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0625	0.0626	0.0625
Shell Radius (#):	5.5000	5.5000	5.5000	5.5000	5.5000	5.5000	5.5000	5.5000	5.5000	5,5000	5,5000	5.5000
Vapor Density												
Vapor Density (lb/cu ft):	0.800.0	0.0080	0.0079	0.0078	0.0078	0.0077	0.0077	0.0077	0.0077	0.0078	0.0079	0,000,0
Vapor Molecular Weight (lb/lb-mole):	120,0000	120.0000	120.0000	120.0000	120,0000	120.0000	120.0000	120,0000	120,0000	120.0000	120,0000	120.0000
Vapor Pressure at Daily Average Liquid												
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3609	0.3600	0.3600	0.3800	0.3600	0.3690	0.3800	0.3600
Daily Avg. Liquid Surface Temp. (deg. R):	503.9812	504.8409	508,5307	513,5620	518,0109	522.2313	524.8471	524.1592	520.7602	515.6984	51 D.6858	505.7950
Daily Average Amblent Temp. (deg. F):	31,3000	32.5000	39,9000	50.3000	59.7000	68.9500	74.9500	74.0000	67,2000	56,7000	46.4000	35.7000
Ideal Gas Constant R												
(psla cuft / (lb-mol-deg R)):	10,731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731
Liquid Bulk Temperature (deg. R):	512.8900	512.8900	512,8900	512.8900	512.890D	512.8900	512,8900	512.8900	512.8900	512.8900	512.8900	512.8900
Tank Paint Solar Absorptance (Shell):	.0.1700	0.1700	0,1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Tank Paint Solar Absorptance (Roof):	0.1700	0.1700	0.1700	0,1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700
Daily Total Solar Insulation						•						
Fector (Btu/sqft day):	548.0000	795,0000	1,118.0000	1,457.0000	1,690.0000	1,802.0000	1,784.0000	1,583.0000	1,280.0000	951,0000	593.0000	457.0000
Vepor Space Expansion Fector												0.4175
Vapor Space Expansion Factor:	0.0187	0.9221	0.0253	0.0318	0.0336	0.0342	0.0333	0.0313	0.0296	0.0269	0.0205	0.0176
Daily Vapor Temperature Range (deg. R):	11.5365	13.2882	14.9897	18,4553	19.5644	20.0255	19.6618	18.6231	17.6128	16.0468	12.6147	10.9593
Daily Vapor Pressure Range (osia):	0,000,0	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0009
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.080.0	0.0600	0.0600	0.0600	0.0600	0.0600	0.0800	0.0600	0.0600	0.0600
Vapor Pressure at Daily Average Liquid			0.0000	0.0000		2.000	0.0000					
Surface Temperature (psia):	0,3600	0,3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600
Vapor Pressure at Daily Minimum Liquid	****	0.0000	0.0000	0.0000	0.0000	4 5466	0.0000	0.0000		0.0000	0.0020	D 0000
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600
Vapor Pressure at Daily Maximum Liquid	0.4000	0.0000	p.0000	0.000	0.000	0.0000	0.0000	0.000	8 0000	0.0000	0.0000	0.0000
Surface Temperature (paia):	0.3600	0.3600	0.3600	0.3808	0.3600	0.3600	0.3600	0.3600	0.3800	0.3600	0.3600	0.3600
Daily Avg. Liquid Surface Temp. (deg R):	503.9812	504.8409	508.5307	513,5620	518.0109	522,2313	524.8471	524.1592	520,7602	515,6984	510.6858	505,7950
Daily Min. Liquid Surface Temp. (deg R):	501.0970	501.5188	504.7883	508,9481	513.1198	517.2249	519.9342	519.5034 528.8149	516,3570 525,1634	511.6867 519.7101	507.5319	503,0551 508,5348
Daily Max. Liquid Surface Temp. (deg R):	505,8653	508.1629	512.2731	518.1758	522,9020	527.2377	529.7601				513,8393	
Daily Ambient Temp, Range (deg. R):	12.4000	13,2000	13.4000	16.0000	16.0000	15.9000	15.5000	15.4000	16,0000	16,0000	13.6000	12.2000
Vented Vener Saluration Factor	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316	0.8316
Vented Vapor Saturation Factor:	0.8310	010010	0.0310	V.0310	0.0310	0.0310	V 02 10	0.0310	0.6310	U.03 19	0.0310	บ.ของเซ
Vapor Pressure at Daily Average Liquid:	0.000	n nêne	0.3600	0.3600	0.0000	0.0000	u saus .	0.0000	2020	0.000	0.0000	0.0000
Surface Temperature (psla):	0.3600	0.3600			0.3800	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600
Vapor Space Cutage (it):	10.6146	10.6146	10.6146	10.6146	10.6146	10.6146	10.6146	10.6146	10.6146	10.6146	10.6148	10.6146
Working Losses (lb):	2.3822	2,3205	2,3678	2,1291	1.7095	2.1497	2.0304	1.8854	1.8370	1.9029	1.7033	1.8545
Vapor Molecular Weight (Ib/Ib-mole):	120,9000	120,0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.0000	120.00CD	120.0000	120.0000
Vapor Prossure at Daily Average Liquid		•					•		-	•		•

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ANKS 4.0 Report Surface Temperature (psia): Net Throughput (gel/mo.):	0.3600 2,316,0000	0.3600 2,255,0000	.0.3600 2,302,000 2,5093	0,3600 2,070,0000	0.3500 1,662.0000	0.3600 2,090.0000	0.3600 1,974.0000	0.3600 1,833.0000	0.3600 1,786.0000	0.3600 1,850.0000	0.3600 1,658.0000	0.3600 1,803.0000
Annual Tumovers: Tumover Factor: Maximum Liquid Volume (gal); Maximum Liquid Height (fi): Tank Diameter (ft): Working Loss Product Factor:	2.8093 1.0000 8.400.0000 14.0000 11.0000	: 2,8093 1,0000 8,400,0000 14,0000 11,0000	2.6093 1.0000 8,400.0000 14,0000 11,0000	2,8093 1,0000 8,400,0000 14,0000 11,0000	.: 2.8093 .1.0000 8,400.0000 14,0000 11,0000	· · 2,8093 1,0000 8,400,0000 14,0000 11,0000 1,0000	2.8093 1.0000 8,400.0000 14.0000 11.0000	2,5093 1,0000 8,400,0000 14,0000 11,0000 1,0000	2.8093 1.0000 8.400.0000 14.0000 11.0000	2.8093 1.0000 8,400.0000 14.0000 11.0000	2.8093 1.0000 8,400.0000 14.0000 11.0000	2,8093 1,0000 8,400,0000 14,0000 11,0000
Total Losses (lb):	6.2679	6.4667	7,5664	8.3927	8.4966	8.7769	8,6842	8.1457	7.6027	7.3701	5.7735	5.4731
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TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK010 - Vertical Fixed Roof Tank Brooklyn, New York

1.11

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Generic Additive	24.27	64.72	89.00

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

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User Identification:

BK041

City: State: BROOKLYN

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft): Volume (gallons): 24.00 79.800.00

Turnovers:

Self Supp, Roof? (y/n):

97.67

No. of Columns: Eff. Col. Diam. (ff): 1.00 1.00

Paint Characteristics

Internal Shell Condition: Shell Color/Shade: Light Rust White/White

Shell Condition
Roof Color/Shade:

Good White/White Good

Roof Condition:

Rim-Seal System
Primary Seal:
Secondary Seal

Mechanical Shoe Rim-mounted

Deck Characteristics

Deck Fitting Category: Deck Type: Detail Welded

Deck Fitting/Status

Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed Automatic Gauge Float Well/Bolled Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Welf (24-in. Diam.)/Pipe Col.-Flex. Fabric Sleeve Seal Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask. Roof Leg or Hanger Well/Adjustable Quantity

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK041 - Internal Floating Roof Tank BROOKLYN, NY

en en en en en en en en en en en en en e			Daily Liquid Surl Imperature (deg		Liquid Bulk Temp	Vaj	oor Pressure (pa	sia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure
ixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Мак.	Weight	Fract.	Fract.	Welght	Calculations
enatured ethanol	Jan	44.31	41.43	47.20	53.22	1.1228	N/A	N/A	46.0700			48.07	Option 4: RVP=3.5, ASTM Slope=3
enatured ethanol	Feb	45.17	41.85	48.49	53.22	1.1457	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASYM Slope=3
enatured ethanol	Mar	48.86	45.12	52.60	53.22	1_2491	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
enatured ethanol	Арг	53,89	49.28	58.51	53.22	1.4024	N/A	N/A	46.0700			46.07	Option 4: RVP=3,5, ASTM Slope=3
lonerie berulans	May	58.34	53.45	63.23	53.22	1.5508	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
enatured ethanol	Jun	62.56	57.55	67.57	53.22	1.7033	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
enatured ethanol	Jul	65.18	60.26	70.09	53.22	1.8039	N/A	N/A	46.0700			46,07	Option 4: RVP=3.5, ASTM Slope=3
enatured ethanol	Aug	64.49	59.83	69.14	53.22	1,7770	N/A	N∕A	48.0700			46.07	Option 4: RVP=3.5, ASTM Stope=3
enatured elhanol	Sep	61.09	56.69	65.49	53.22	1.6488	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Stope=3
snatured ethanol	Oct	56.03	52.02	60.04	53.22	1.4721	N/A	N/A	46.0700			48.07	Option 4: RVP=3.5, ASTM Stope=3
enatured ethanol	Nov	51.02	47.86	54.17	53.22	1.3129	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Stope=3
enatured ethanol	Dec	46.12	43.39	48.86	53.22	1,1717	N/A	N/A	46.0700			45.07	Option 4: RVP=3.5, ASTM Stope=3

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TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK041 - Internal Floating Roof Tank BROOKLYN, NY

Mon#x	January	February	March	April	May	June	July	August	September	Ociober	November	Decembe
Rim Seal Losses (ib):	1.0978	1.1213	1.2271	1.3855	1.5404	1,7015	1,8088	1.7800	1.6437	1.4581	1.2929	1.1478
Seal Factor A (Ib-molé/II-yr):	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0,6090	0.6000	0.6000
Seal Factor B (lb-mole/fl-yr (mph)*n):	0.4000	0.4000	0.4000	0.4900	0.4000	0.4000	0.4000	0.4000	0.4900	0.4000	0.4000	0.400
Value of Vapor Pressure Function: Vapor Pressure at Daily Average Liquid	0.0199	0.0203	0.0222	0.0251	0.0279	0.0308	0.0327	0.0322	0.0297	0.0264	0.0234	0.020
Surface Temperature (osia):	1,1226	1,1457	1,2491	1,4024	1.5508	4 7000	1,8039	4 7770	4.0400	4 4704	4.0400	1.1717
Tank Diameter (ff):	24.0000	24.0000	24.0000	24,0000	24,0000	1.7033 24.0000	24,8000	1.7770 24.0000	1.6488 24.0000	1,4721 24,0000	1,3129 24,0000	24,0000
Vapor Molecular Weight (Ib/Ib-mole):	46.0700	46,0700	46,0700	46,0700	46.0700	46,0700	46,0700	46.0700	46,0700	46.0700	46.0700	46,070
Product Factor.	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000	1.0000	1.0000	1,0000
Mihdrawai Losses (ib):	7.0770	6.7579	7.2538	6.6334	5.2440	6.5113	6.1378	5.6668	5,7246	6,2473	5,7690	6.283
Number of Columns:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.000
Effective Column Diameter (fi):	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0003	1.0000	1.0000	1.000
Net Throughput (gal/mo.):	732,447.3000	699,416.8000	750,747,5000	686,535.0000	542,736.0000	673,901.8000	635,239.8000	586,493.8000	592,475,5000	646,576.0000	597,075.5000	650,295,800
Shell Clingage Factor (bbl/1000 sqff):	0.0016	0.0015	0.0015	0.0016	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0019
Average Organic Liquid Density (Ib/gal):	6.6100	6,6100	6.6100	6.6100	6.6100	6.6100	6.6100	6.6100	6.6100	6.6100	6.6100	6.6100
Tank Diameter (fi):	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24,0000	24.0000
Deck Fitting Losses (ib):	11.8626	12.1161	13.2592	14.9711	16.6453	18.3860	19.5452	19.2341	17,7616	15.7554	13.9700	12.4030
Value of Vapor Pressure Function:	0.0199	0.0203	0.0222	0.0251	0.0279	0.0308	0.0327	0.0322	0,0297	0.0264	0.0234	0.0208
Vapor Molecular Weight (lb/lb-mole):	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.6000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Filling Loss Fact.(lb-mole/yr):	155.6000	155.6000	155,6000	155,6000	155.6000	155.6000	155,6000	155,6000	155.6000	155.6000	155.6000	155,6000
Deck Seam Losses (b):	0.0000	0.0000	0.0000	0.0008	0.0000	9.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.9890
Deck Seam Length (ft):	0.0000	0.0000	0.0000	0.0008	0,0000	9.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0900
Deck Seam Loss per Unit Length												
Factor (fb-mole/ff-yr);	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0,0000	0.0000	0.0000	8.0000
Deck Seam Length Factor(fl/sqft):	0.9000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (ft):	24.9000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Vapor Molecular Weight (lb/lb-mole):	48.0700	46.0700	46.0700 1.0000	46.0700 1.0000	46.0700	46.0700	46.0700	46,0700	46.0700	46.0700	46.0700	46.0700
Product Factor:	1.0000	1.0000	1.0000	1.6960	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (fb):	20.0374	19.9952	21.7401	22.9900	23.4297	26.5988	27.4918	26.6809	25.1299	23.4608	21.0318	19.8341
					-		Roof Fitting Loss Fac					
Roof Fitting/Status			•	Quantit	1	KFa(lb-mole/yr)	KFb(lb-mole/(y	raph'n))		m	Losses(fb)	
Ladder Well (36-in, Diam./Sikling Cover, Gasketed				,		56.00		0.00	0.	00	68,9913	
Automatic Gauge Float Well/Bolted Cover, Gasketed					ĺ	2.80		0.00	ŭ. 0.		3,3496	
Automatic Gauge Float Well/Unboiled Cover, Gasketed						4.30		17.00	Ö.		5.1440	
Column Well (24-in, Diam.)/Pipe ColFlex, Febric Sleeve Seal						10,00		0.00	Ö.		11.9527	
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.						43.00		0.00	Õ.		51.4397	
Roof Leg or Hanger Well/Adjustable					;	7.90		0.00	0.		47,2528	

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK041 - Internal Floating Roof Tank BROOKLYN, NY

[4:1] (A)			Losses(lbs)		
Components	Rim Seal Loss		Deck Fitting Loss	Deck Seam Loss	Total Emissions
denatured ethanol	17.21	75.31	185.91	0.00	278.42

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

mti		

User Identification:

BK042

Citv: State: BROOKLYN

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft): Volume (gallons):

24.00 79 800.00

Turnovers:

97.67

Self Supp. Roof? (v/n):

No. of Columns:

1.00

Eff. Col. Diam. (ft):

1.00

Paint Characteristics

Internal Shell Condition: Shell Color/Shade:

Light Rust White/White

Shell Condition Roof Color/Shade:

Good White/White

N

Roof Condition:

Good

Rim-Seal System

Primary Seal: Secondary Seal Mechanical Shoe Rim-mounted

Deck Characteristics

Deck Fitting Category: Deck Type:

Detail Welded

Deck Fitting/Status

Deck Fitting/Status		Quantity
Ladder Well (36-in. Diam.)/Silding Cover, Gasketed Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Well (24-in. Diam.)/Pipe ColFlex. Fabric Sleeve Seal Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Silding Cover, Gask. Roof Leg or Hanger Well/Adjustable		1 1 1 1 1 1 5

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK042 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surf. emperature (deg		Liquid Bulk Temp	Vej	por Pressure (p	sía)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vepor Pressure	
xture/Component () (500)	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Weight	Calculations	•
natured ethanol	Jan	44.31	41.43	47.20	53.22	1.1226	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	Feb	45.17	41.65	48.49	53.22	1.1457	N/A	ŃΑ	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	Mar	48.86	45.12	52.60	53,22	1,2491	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	Apr	53.89	49.28	58.51	53.22	1.4024	N/A	N/A	46.0700		•	46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	May	58.34	53.45	63.23	53.22	1.5508	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	•
natured ethanol	Jun	62.56	57.55	67.57	53.22	1.7033	N/A	N/A	48.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	Jud	65.18	60.26	70.09	53.22	1.8039	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	Aug	64.49	59.83	59.14	53,22	1,7770	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	Sep	61.09	56.69	85.49	53.22	1.6488	N/A	N/A	46.0700	•		46.07	Option 4: RVP=3.5, ASTM Slope=3	· ·
natured ethanol	Oct	56.03	52.02	60.04	53.22	1.4721	N/A	N∕A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanol	Nov	51.02	47.68	54.17	53.22	1.3129	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	
natured ethanoi	Dec	46.12	43.39	48.86	53.22	1,1717	N/A	N/A .	46.0700			46.07	Option 4: RVP+3.5, ASTM Slope=3	

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TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK042 - Internal Floating Roof Tank BROOKLYN, NY

Film Seal Losses (B): 1.0578 1.1219 1.2271 1.3855 1.5404 1.7015 1.8988 1.700 1.6437 1.4381 1.2212 Seal Factor (A) Chemolity (Film) 0.0800 0.6000	Month:	January	February	March	April	May	June	July	August	September	October	November	Decemb
Seal Factor 8 (St-makeN-15 (mps)/m):						1.5404	1.7015		1.7800	1.6437	1,4581	1.2929	1.14
Value of Vapor Pressum Función: 0.0199 0.0203 0.0222 0.0251 0.0279 0.0308 0.0327 0.0322 0.0237 0.0254 0.0237 Vapor Pressum Función: 0.0234 Vapor Valor Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Melcadar Veight (léth-inde): 0.0234 Vapor Valor Veight (léth-inde): 0.0234 Valor Valor Veight (léth-inde): 0.0234 Valor Valor Veight (léth-inde): 0.0234 Valor V						00000	0.6000		0.6000	0.6000	0.6000	0,6000	0.600
Vapor Pressure at Daily Nerrope Liquid 1,126													0.400
Tank Diameter (II):	Vapor Pressure at Daily Average Liquid	0.0199	0.0203	0.0222	0.0251	0.0279	0.0308	0.0327	0.0322	0.0297	0.0264	0.0234	0.020
Vapor Moleculari Weight (bilb-mole): 46,0770 46,07						1,5508	1.7033		1.7770	1.6488	1.4721	1.3129	1.171
Product Factor 1,0000 1,												24.0000	24.000
Militriarwal Losses (b): 7.0770 6.7579 7.233 8.6334 5.2440 6.5115 6.1378 5.6968 5.7248 6.2473 5.7690						46,0700	46.0700		46,0700	46.0700	48.0700	46.0700	46.070
Number of Columns 1,0000	Product Factor:	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0006	1.0000	1.0000	1.0000	1,0000	1.000
Effective Column Diameter (ft):													6.283
Net Throughput (galfma,): 732,447,3000 699,416,8000 750,747,5000 686,635,0000 686,635,0000 686,635,0000 686,635,0000 686,635,0000 686,000 68100 6													1.000
Shell Clingage Factor (his/1000 sqrt); 0.0015 0.001													1.000
Average Organic Liquid Density (ib/gal): 6.6100 6.6													650,295,800
Tank Diameter (ft): 24,0000													0.001
Deck Filting Losses (ib): 11,7711 12,0227 13,1570 14,8556 16,5169 18,2442 18,3945 19,0858 17,5246 15,6339 13,8622 Value of Vapor Pressure Function: 0,0199 0,0283 0,0222 0,0251 0,0279 0,0308 0,0327 0,0322 0,0297 0,0264 0,0234 Vapor Molecular Weight (b/fb-mole): 46,0700 46,0700 46,0700 46,0700 46,0700 46,0700 46,0700 46,0700 46,0700 1,00													6.610
Value of Vepor Pressure Function: 0.0199 0.0203 0.0222 0.0251 0.0279 0.0308 0.0327 0.0322 0.0297 0.0284 0.0234 Vapor Molecular Welght (Milb-mole): 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 1.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 <td>Tenk Diameter (R):</td> <td>24,0000</td> <td>24,0000</td> <td>24.0000</td> <td>24.0000</td> <td>24.0000</td> <td>24.0000</td> <td>24.0000</td> <td>24,9000</td> <td>24.0000</td> <td>24.0000</td> <td>24.0000</td> <td>24,000</td>	Tenk Diameter (R):	24,0000	24,0000	24.0000	24.0000	24.0000	24.0000	24.0000	24,9000	24.0000	24.0000	24.0000	24,000
Vapor Molecular Weight (IzMs-mole): 46,0700 45,0700 46,070													12.307
Product Factor: 1,0000 1													0.020
Tot. Roof Fitting Loss Fact (lb-molelyty): 154,4000 154,4													46.070
Deck Seam Lossas (b): 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0													1.000
Deck Seam Length (ft): 0.0000 0.0	Tot. Roof Fitting Loss Fact.(lb-mole/yr):	154,4000	154.4000	154.4000	154.4980	154.4000	154,4000	154.4000	154.4000	154.4000	154,4000	154,4000	154.400
Dack Seam Loss per Unit Length													0.000
Factor (fo-mole/fil-yr): 0,0000		0000.0	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000			0.0000	0.0000	9,000
Deck Seam Length Factor(ff/sqrt): 0.0000 0.00		0.0900	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000			0.0000	0.0000	0.000
Tank Diameter (ff): 24,0000 24													0,000
Vegor Molecular Weight (Ib/Ib-mole): 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700 46.0700													24,000
			46.0700	46,0700									46.070
			1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.000
olal Losses (b): 19.9459 19.9018 21.6379 22.8745 23.3014 25.4570 27.3410 26.5326 24.9929 23.3392 20.9241	olai Losses (Ib):	19.9459	19,9018	21.6379	22.8745	23.3014	26.4570	27,3410	26.5326	24.9929	23.3392	20.9241	19.738

Roof Filing/Status	Quantity KF.		ing Loss Factors b(ib-mole/(yr mph^n))	· · · m	Losses(lb)
Ledder Well (36-in. Diam.)/Sliding Cover, Gasketed Access Hatch (24-in. Diam.)/Slidled Cover, Gasketed Automatic Gauge Float Well/Linbolled Cover, Gasketed Column Welf (24-in. Diam.)/Fige ColFlox. Fabric Steeve Seal Sample Pipe or Well (24-in. Diam.)/Slotled Pipe-Sliding Cover, Gask. Roof Leg or Hanger Welf/Adjustable	1 1 1 1 1	\$8.00 1.60 4.30 10.00 43.00 7.90	0.00 0.00 17.00 0.00 0.00	0.00 0.00 0.38 0.00 0.00	66.9913 1.9140 5.1440 11.8627 51.4397 47.2528

TANKS 4.0 Report

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK042 - Internal Floating Roof Tank BROOKLYN, NY

,			Losses(lbs)		
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
denatured ethanol	17.21	75.31	184.48	0.00	276.99

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification:

BK043 BROOKLYN

City: State:

NY

Company:

SHELL OIL COMPANY - BROOKLYN

internal Floating Roof Tank

Type of Tank: Description:

Tank Dimensions

Diameter (ft):

43,00

Volume (gallons):

79,800.00

Turnovers:

236.46

Self Supp. Roof? (y/n):

No. of Columns:

1.00

Eff. Col. Diam. (ft):

1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Ν

Shell Color/Shade:

White/White

Shell Condition

Good

Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal. Secondary Seal Mechanical Shoe

Rim-mounted

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Quantity

Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed Access Hatch (24-in, Diam.)/Bolted Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Well (24-in. Diam.)/Pipe Col.-Flex. Fabric Sleeve Seal Sample Pipe or Well (24-in, Diam.)/Slotted Pipe-Stiding Cover, Gask. Roof Leg or Hanger Well/Adjustable

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK043 - Internal Floating Roof Tank BROOKLYN, NY

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emerago e e .				Delly Liquid Surf		Liquid Bulk Temp	V	por Pressure (psi	-1	Væpor Mol.	Uquid Mass	Vapor Mass	Mal.	Basis for Vacor Pressure
Mixture/Component		Month	Avg,	Min.	Max.	(deg F)	Avg.	Miv. Miv	Max.	Weight.	Fract.	Fract.	Weight	Calculations
STAR - RFG 2.0 (15)		Jan	44.31	41.43	47.20	53.22	6.0619	N/A	N/A	62,0000			62,00	Option 4: RVP=15, ASTM Slope=3
TAR - RFG 2.0 (15)	*	Feb	45.17	41.85	48.49	53.22	6.1639	N/A	N/A	62,0000			62.00	Option 4: RVP=15, ASTM Stope=3
TAR - RFG 2.0 (15)		Mar	48.86	45,12	52.60	53.22	8.6173	N/A	N/A	62,0008			62.00	Option 4: RVP=15, ASTM Stope=3
ter - RFG 2.0 (13.5)		Apr	53.89	49.28	58.51	53.22	5,4598	N/A	N/A	62.0000	•		62.00	Option 4: RVP=13.5, ASTM Slope=3
tar Gasoline (RVP 8.1)		May	58.34	53,45	63.23	53.22	3.9662	N/A	N/A	66,0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
tar Gasoline (RVP 8.1)	•	Jun	62.56	57.55	67.57	53.22	4.3143	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Stope=3
tar Gasoline (RVP 8.1)		Jul	65.18	60.26	70.09	53.22	4.5422	NA	N/A	66.0000			66,00	Option 4: RVP=8.1, ASTM Stope=3
atar Gasoline (RVP B.1)		Aug	64.49 :	59.83	69.14	53.22	4.4814	N/A	N/A	68.0000			68.00	Option 4: RVP=8.1, ASTM Stope=3
Star Gasoline (RVP 8.1)		Sep	61.09	56.69	65.49	53.22	4.1903	NA	N/A	66.0000			68.00	Option 4: RVP=8.1, ASTM Slope=3
Star - RFG 2.0 (13.5)		Oct	56.03	52.02	60.04	53.22	6.7266	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Slope=3
TAR - RFG 2.0 (15)		Nev	51.02	47.65	54.17	53.22	6.8941	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Slope=3
STAR - RFG 2.0 (15)		Dec	46.12	43.39	48.86	53.22	6.2787	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Stope=3

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TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK043 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	March	April	May	June	July	August	September	October	November	Decembe
Rim Seal Lesses (lb):	17.6143	18.0030	19.7851	19.1559	11.1322	12,2939	13.0746	12.8645	11.8758	20.2285	20.9191	18.445
Seal Factor A (lb-mole/ff-yr):	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000
Seal Factor B (lb-mole/ft-yr (mph)^n):	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.408
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0.1437	0.0785	0.0856	0.0921	0.0907	0.0837	0.1518	0.1569	0.1384
Vapor Pressure at Daily Average Liquid												
Surface Temperature (psia):	6.0619	6,1639	6.6173	6,4598	3,9662	4.3143	4,5422	4,4814	4,1903	6.7266	6,8941	6.278
. Tank Diameter (ft):	43.000D	43.0000	43.0000	43.0000	43.0000	43.0000	43.0000	43.0000	43.0000	43.0000	43,0000	43,000
Vapor Molecular Weight (lb/lb-mole):	62,0008	62.0000	62.0000	62,0000	66,0000	66.0000	66.0000	66.0000	66.0000	62.0000	62.0000	62,000
Product Factor:	1.0009	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000
Wilhdrawai Losses (lb):	6.9979	5,6671	7.1967	6.6687	5.3707	6.7156	6.3059	5.7677	5.8148	6.3694	5.7571	6.2394
Humber of Columns:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.9000	1.0000	1.0000	1.0000	1.9000
Effective Column Diameter (fl):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	1,740,425.5000	1,658,143.1000	1,789,873,1000	1,658,537.6000	1,335,713,9000	1,670,203.3000	1,568,328.0000	1,434,455,7000	1,446,183.0000	1,584,113.4000	1,431,824.5000	1,551,772,6000
Shell Clingage Factor (bbl/1000 sqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	8.0015	0.0015	0.0016
Average Organic Liquid Density (th/gal):	5,0170	5.0170	5.0170	5.0170	5.0170	5.0170	5,0170	5,0170	5.0170	5.0170	5.0170	5.0170
Tank Diameter (ft):	43,0000	43.0000	43.0000	43,0000	43.0000	43,0000	43.0000	43.0000	43.0000	43.0000	43.00 00	43.0000
Deck Fitting Losses (lb):	105.4126	107.7392	118.4039	114,6383	66.6207	73,5727	78.2447	78.9875	71.0705	121.0574	125.1905	110.3886
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0.1437	0.0785	0.0866	0.0921	0.0907	0.0837	0.1518	0.1569	0.1384
Vapor Molecular Weight (Ib/Ib-mole):	62,0000	62,0000	62.0000	62,0000	66.0000	66.0000	66,0000	66.0D00	66.0000	62.0000	62,0000	62.0000
Product Factor:	1.0000	1.0000	1.0000	1,0000	1.0000	1,0090	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fiting Loss Fact.(lb-mole/yr):	154.4000	154,4000	154,4000	154.4000	154.4000	154,4000	154.4000	154,40G0	154,4000	154,4000	154.4000	154.4000
Deck Seam Losses ([h); 🍛	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	8.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length (ft):	0.0000	0.000.0	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length												
Factor (lb-mole/ft-yr):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length Factor(ft/sqft):	0.0000	0.0000	0.0090	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	00000	0.0000	0,0000
Tank Diameter (ft):	43,0000	43.0000	43.0000	43,0000	43,0000	43,0000	43,0000	43,0000	43.0000	43,0000	43.0000	43.0000
Vapor Molecular Weight (Ib/Ib-mole):	62,0000	62.0000	62,0090	62,0000	66.0000	66,0000	66,0000	66,0000	66,6000	62.00C0	62.0000	62.0000
Product Factor.	1,0000	1.0000	1.0000	1,0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (ib):	130.0248	132,4093	145,3858	140,4629	83.1235	92.5821	97.6253	95.6198	88.7611	147.6553	151.8668	135.0737
,	······································						Roof Fitting Loss Fa	clors				
Roof Fitting/Status				Quanti	ty	KFa(lb-mole/yr)	KFb(fb-mole/(/r mph^л))		m	Losses(b)	
Ledder Weil (36-in, Diam, Visilding Cover, Gasketed					•	56.00		0.00		.00	423,8031	
Access Hatch (24-in, Diam.)/Bolted Cover, Gasketed					1	1.60		0.00		.00	12.1087	
Access natch (24-in, Diani, Morted Cover, Gasketed Automatic Gauga Float Well/Unbolled Cover, Gasketed					4	4.30		17.00		.38	32,5420	
Automatic Gauge Float Well onboiled Cover, Gasketed Column Well (24-in, Diam,)Pipe ColFlex, Fabric Sleeve Seal					1	4.30 10.00		0.00		.00	75.6791	
Column Weil (244th, Diam, Mipe Column). Paoric Steeve Sea Sample Pipe or Weil (244th, Diam, MS) otted Pipe-Sliding Cover, Gask.					i	43.00		. 0,00		.00	326.4202	
Roof Len or Hanner Well/Adjustable					<u>:</u>	7.90		0.00		.00	298.9325	

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK048 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	March	Aprîl	May	June	July	August	September	October	November	Decembe
Rim Seal Losses (fb):	50.2485	51.3575	56,4412	54.6482	31.7570	35.0709	37.2980	36.6987	33,6782	57.7061	59,8763	52.620
Seal Factor A (fo-mole/ft-yr);	1.6000	1.6000	1.6000	1,6900	1.6000	1.6000	1.6000	1.6000	1,6000	1.6000	1.6000	1,6000
Seal Factor B (lb-mole/ft-yr (mph)*n);	0.3000	0.3000	0.3000	0.3000	0.3090	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000
Vakue of Vapor Pressure Function: Vapor Pressure at Dally Average Liquid	0.1321	0.1351	0.1484	0.1437	0.0785	0.0668	0.0921	0.0907	0.0837	0.1618	0.1569	0.1384
Surface Temperature (psia):	6,0619	6.1639	6.6173	6.4598	3.9652	4,3143	4,5422	4.4814	4.1903	6.7266	6.8941	6,2787
Tank Diameter (fl):	46.0000	46,0000	46.0009	46.0000	48,0000	46.0000	46.0000	46.0000	46,0000	46.0000	46.0000	46.0000
Vapor Molecular Weight (fb/lb-mole):	62.0000	62,0000	62.0000	62,0000	66.0000	66.0000	66,0000	66,0000	66,0000	62.0000	62.0000	62.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000
Withdrawal Losses (ib):	29.7561	28.3494	30.6016	28.3561	22.8368	28.5556	26.8138	24.5250	24.7255	27.0837	24.4800	26.5307
Number of Columns:	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0003	1.0000	1.0000
Effective Column Diameter (ff):	1.0000	1,0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	7,928,605.0000	7,553,762.9000	8,153,866,4000	7,555,560,4800	6,084,918.7000	7,608,703.7000	7,144,605.5000	6,534,742.8000	6,588,167.0000	7,216,516,6000	6,522,756,0000	7,069,186.4000
Shell Clingage Factor (bbl/1000 sqft):	0.0016	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	8.0015	0.0015
Average Organic Liquid Density (lb/gal):	5.0170	5,0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170
Tank Diameter (fl):	46.0000	46.0000	46.0000	46,0000	46.0000	46.0000	46.0000	46.0000	45.0000	46.0000	46.0000	46.0000
Dack Fitting Losses (lb):	121.1153	123.7884	135,0418	131.7153	76.5447	84.5323	89.9004	88.4558	81.6575	139,0906	143,8394	126.8325
Value of Vapor Pressure Function;	0.1321	0.1351	0.1484	0.1437	0.0785	0.0866	0.0921	0.0907	0.0837	0.1518	0.1569	0.1384
Vapor Molecular Weight (Ib/Ib-mole):	62,0000	62.0000	62.0000	62,0000	66.0000	66.0000	66,0000	66,0000	66.0000	62,0000	62,0000	82,0000
Product Factor	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000	1.0000	1,0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	177.4000	177.4000	177.4000	177,4000	177,4000	177.4000	177,4000	177,4000	177.4000	177.4000	177.4000	177.4000
Deck Seam Losses (lb):	0.0000	0.0000	0,000	0000.0	0.0000	. 0.0000	0.0000	0.0000	0.0000	0.0008	0.0000	0.0000
Deck Seam Length (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length				**	•							
Factor (lb-mole/fl-yr):	0.0000	0.0000	0.0000	0.0000 .	0.0000	0.0000	0.0000	0000.0	0.0000	. 0,000	0.0000	0.0000
Deck Seam Length Factor(ft/sqft):	0.0000	0.0000	0.000	0.0000	0.0000	0.0000	0,0000	0.0000	0.000.0	0.0000	0.0000	0.0000
Tank Diameter (ft):	46.0000	46.0000	46,0000	46.0000	46.0000	46.0000	46.0000	46.0000	46,0008	45.0000	45,0000	46,0000
Vapor Molecular Weight (lb/lb-mole):	62.0000°	62,0000	62.0000	62.0000	66.0000	66.0000	66.0000	66.0003	66,0000.	62.0000	62,0000	62.0000
Product Factor:	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.8000
Total Losses (lb):	201,1200	203,4953	223.0846	214,7176	131.1385	148.1588	154.0122	149.6795	140,2611	223,8804	227,9957	205,9837

Roof Fitting/Status	Quantily	KFa(lb-mole/yr)	Roof Fitting Loss Factors KFb(to-mole/(yr mph*n))		m	Losses(lb)
D		700		-,		
Roof Leg or Hanger Well/Adjustable	. 5	7.90	0.00		0.00	298.9325
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Stiding Cover, Ungask.	1	43.00	0.00		0.00 *	325,4202
Column Well (24-in. Diam.)/Buill-Up ColSliding Cover, Gask.	1.	33.00	00.0		0.00	249.7411
Automatic Gauge Float Well/Linbolled Cover, Gaskeled	1	4.30	17.00		0.38	32.5420
Access Hatch (24-in, Diam.)/Bulted Cover, Gasketed	1	1.60	0.00		0.00	12.1087
Ladder Well (36-in. Diam.)/Stiding Cover, Gasketed	1	56.00	0.00		0.00	423.8031

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TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK048 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surf. Temperature (deg F)		Bulk Temp		Vapor Pressure (psia)		Vapor Mal.	Liquid Mass	Vapor Mess	Mal.	Basis for Vapor Pressure	
lixture/Component \(\gamma g^{\alpha} \)	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight	Fract.	Fract.	Weight	Calculations	
TAR - RFG 2.0 (15)	Jan	44.31	41.43	47.20	53.22	6,0619	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Stope=3	
TAR - RFG 2.0 (15)	Feb	45.17	41.85	48.49	53.22	6.1639	N/A	N/A	62.0000	•		62.00	Option 4: RVP=15, ASTM Stope=3	
TAR - RFG 2.0 (15)	Mar	48.86	45.12	52.60	53.22	6.6173	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Stope=3	
lar - RFG 2.0 (13.5)	Apr	53,89	49.28	58.51	53.22	6.4598	N/A	N/A	62,0000			62.00	Option 4: RVP=13.5, ASTM Slops=3	
tar Gasoline (RVP 8.1)	May	58.34	53.45	63.23	63.22	3.9662	N/A	N/A	66.0000		. •	66,00	Option 4: RVP=8.1, ASTM Slope=3	
ter Gasoline (RVP 8.1)	Jun	62,56	57.55	67.57	53.22	4.3143	N/A	N/A	68.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3	
lar Gasoline (RVP 8.1)	Jul	65.18	60.26	70,09	53.22	4.5422	N/A	N/A .	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3	
lar Gasoline (RVP 8.1)	Aug	64.49	59.83	69.14	53.22	4,4814	N/A	N/A	66.0000			68.00	Option 4: RVP=8.1, ASYM Stope=3	
lar Gasoline (RVP 8.1)	Sep	61,09	56.69	65.49	63.22	4.1903	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Stope=3	
lar - RFG 2.0 (13.5)	Oct	56.03	52.02	60.04	53.22	6.7266	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Slope=3	
TAR - RFG 2.0 (15)	Nov	51.02	47,86	54.17	53.22	6.8941	N/A	N/A	62.0000			. 62.90	Option 4: RVP=15. ASTM Slope=3	
TAR - RFG 2.0 (15)	Dec	46.12	43.39	48.86	53.22	6.2787	N/A	N/A	62,0000			62.00	Option 4: RVP=15, ASTM Slope=3	

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification:

BK048

City: State: BROOKLYN NY

N.

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank: Description: Internal Floating Roof Tank

Tank Dimensions

Diameter (ft):

46.00

Volume (gallons):

373,800.00

Turnovars:

229.97

Self Supp. Roof? (v/n):

No. of Columns:

1.00

Eff. Col. Diam. (ft):

1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Shell Color/Shade:

White/White

Shell Condition

Good

Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal:

Liquid-mounted

Secondary Seal

None

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Quantity

Roof Leg or Hanger Well/Adjustable
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Ungask.
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.
Automatic Gauge Float Well/Anhobited Cover, Gasketed
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psla)

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK047 - Internal Floating Roof Tank BROOKLYN, NY

1. 1.1.1.1.1	Losses(lbs)										
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions						
STAR - RFG 2.0 (15)	270.34	139.72	651.62	0.00	1,061.68						
Star - RFG 2.0 (13.5)	112.35	55.44	270.81	0.00	438.60						
Star Gasoline (RVP 8.1)	174.70	127.46	421.09	0.00	723.25.						

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK047 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	March	Aprit	May	June	July	August	Seplember	October	November	Decembe
Rim Seal Losses (lb):	50.2485	51.3575	56.4412	54.6462	31.7570	35.0709	37,2980	36.6987	33.8782	57.7081	59.6763	52.6205
Seal Factor A (fo-mole/ft-yr):	1.6000	1.6000	1.6000	1.6000	1,6000	1.6000	1.6000	1.6000	1.6800	1.6000	1.6000	1.600
Seal Factor B (lb-mole/lt-yr (mph) n):	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.300
Value of Vapor Pressure Function: Vapor Pressure at Daily Average Liquid	0.1321	0.1351	0.1484	0.1437	0.0785	0.0866	0.0921	0.0907	0.0837	0.1518	0.1569	0,1384
Surface Temperature (psia):	6.0619	6,1639	6.6173	6.4598	3.9662	4.3143	4.5422	4,4814	4.1903	6.7256	6.8941	6.278
Tank Diameter (ft):	46.0000	46.0000	46,0000	46,0000	46,0000	46.0000	46.0000	46.0000	46,0000	46.0000	46.0000	46.000
Vapor Molecular Weight (lb/lb-mole):	62,0000	62.0000	62,0000	62,0000	66.0000	66.0000	66.0008	66.0000	66,0000	62.0000	62,0000	62.000
Product Factor:	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.000
Wilhdrawel Losses (b):	29.7581	28.3494	30.6016	28,3581	22.8368	28.5556	26,8138	24.5250	24.7255	27.0837	24.4800	26,530
Number of Columns:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.000
Effective Column Diameter (ff):	1.0000 7,928,605.0000	1,0000 7,553,762,9000	1,0000	1.0000 7,555,560.4000	1.0000 6.084,918,7000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.000
Net Throughput (gal/mo.): Shell Clingage Factor (bbl/1000 sqfl);	7,928,605.0000	0.0015	8,153,866,4000 0.0015	0.0015	0.0015	7,608,703,7000 0,0015	7,144,605.5000	6,534,742.8000	6,588,167,0000	7,216,516.6000	6,522,756.0000	7,069,186.4000
Average Organic Liquid Density (b/gal):	5.0170		5.0170	0.0015 5.0170			0.0016	0.0015	0.0015	0.0815	0.0015	0.0015
Average Organic ciquid Density (iosgan): Tank Diameter (ft);	46,0000	5,8170 46,0000	46.0000	46.0000	5.0170 46.0000	5.0170	5.0170	5,0170	5.0170	5.0170	5.0170	5.0170
Tank Despeter (it).	46.0000	46.0000	40.000	40.0000	46.0003	46.0000	46.0000	46,0000	46.0000	46.0000	46,0000	46.9000
Deck Fitting Losses (lb):	121.1153	123.7884	136.0418	131.7153	76.5447	84.5323	89.9004	88.4558	81.6575	139.0906	143.8394	128.8325
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0.1437	0.0785	0.0866	0.0921	0.0907	0.0837	0.1518	0.1569	0.1384
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62,0000	62.0000	66.0000	66,0000	66,0000	66.0000	66.0000	62.0000	62.0000	62.0000
Product Factor:	1.0000	1.0000 177.4000	1.0000 177.4000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000
Tot. Roof Fitting Loss Fact-(lb-mole/yr):	177.4000	177.4000	177.4000	177.4000	177.4000	177,4000	177.4000	177.4000	177.4000	177.4000	177.4000	177.4000
Deck Seam Losses (b):	0.0000	0.0000	0.0060	. 0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length (ft);	0.000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length	0.0000	0.000										
Factor (tb-mote/ft-yr): Deck Seam Length Factor(ft/soft);	0.0000	0.0000 0.0000	0.0000 0.0000	0.0000 0.0000	0,0000 0000.0	0.0000	0,000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (ft):	46,0000	46,0000	46,0000	46.0000	46,0000	0.0000 46.0000	0.0000 46.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (Ib/Ib-mole):	62.0000	62,0000	62,0000	62.0000	68.0000	68,0000		48.0000	46.0000	46.0000	46.0000	46.0000
Product Factor:	1.0000	1.0000	1.0000	1,0000	1,0000	1.0000	66.0000 1.00 0 0	66.0000	66.0000	62.0000	62.0000	62,0000
Flound Falaut.	1.0000	1.000	1,000	1.0000	1,0000	1.0000	1.0008	1.0000	1.0000	1.0000	1.0000	1,0000
Total Losses (ib):	201.1200	203.4953	223.0846	214.7176	131.1385	148.1588	154.0122	149,6795	140.2611	223.8804	227.9957	205.9837
Para Citica Market		***************************************					Roof Filting Loss Fa					
Roof Filling/Status				Quanti	ty	KFa(tb-mole/yr)	KFb(lb-mole/()	rmph^n))		m	Losses(lb)	
Roof Leg or Hanger Well/Adjustable				,	5	7.90		0.00		.00	298.9325	
Sample Pipe or Well (24-In. Diam.)/Slotted Pipe-Sliding Cover, Ungask.					1	43.00		0.00		1.00	285.9325 325.4202	
Automatic Gauge Float Well/Unboked Cover, Gasketed					1.	4.30		17.00		1.38	32.5420	
Access Hatch (24-in, Diam,)/Bolled Cover, Gasketed					1	1.60		0.00		1.00	12.1087	
Ladder Well (36-in. Diam.)/Śliding Cover, Gaskeled					1	56.00		0.00		1.00	423.8031.	
Column Welf (24-in, Diam.)/Built-Up CofSliding Cover, Gask.					1	33.00		0.00		1.00	249.7411	

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TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK047 - Internal Floating Roof Tank BROOKLYN, NY

in de la Profesionation de la Profesional Profesionation de la Profesionation de la Profesion			Daily Liquid Surf mperature (deg		Liquid Bulk Temp	Vaj	por Pressure (ps	ia)	Vapor Mol.	Liquid . Mass	Vapor Mass	Moi.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract	Fract.	Weight	Calculations
STAR - RFG 2.0 (15)	Jan	44.31	41.43	47.20	53.22	6,0619	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Slope=3
STAR • RFG 2.0 (15)	Feb	45.17	41.85	48.49	53.22	6.1639	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Stope=3
STAR - RFG 2.0 (15)	Mar	48.86	45.12	52.60	53.22	6.6173	N/A	N/A	62.0000			52.00	Option 4: RVP=15, ASTM Stope=3
Star - RFG 2.0 (13.5)	Apr	53.89	49.28	58.51	53.22	6.4598	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Slope=3
Star Gasoline (RVP 8.1)	May	58.34	53.45	63.23	53.22	3.9662	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Jun	62.56	57.55	67,57	53.22	4.3143	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Stope=3
Star Gasoline (RVP 8.1)	Jul	65.1B	60.26	70.09	53.22	4.5422	N/A	N/A	66,0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gescline (RVP 8.1)	Aug	64.49	59.83	69.14	63.22	4.4814	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Sep	61.09	56.69	65.49	53.22	4.1903	N/A	N/A	66,0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star - RFG 2.0 (13.5)	Oct	56.03	52.02	60.04	53.22	6.7266	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Slope=3
STAR - RFG 2.0 (15)	Nov	51.02	47.86	54.17	63.22	6.8941	N/A	N/A	62.0000			62.00 -	Option 4: RVP=15, ASTM Stope=3
STAR - RFG 2.0 (15)	Dec .	46.12	43.39	48.86	53.22	6,2787	N/A	N/A	62.0D06 · ·			62.00	Option 4: RVP=15, ASTM Slope=3

John William Controlled Control

A SERVICE REPORT

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Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification:

BK047 BROOKLYN

City: State:

NY

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft):

46.00

Volume (gallons):

373,800.00

Turnovers:

229.97

Self Supp. Roof? (y/n):

No. of Columns:

1.00

Eff. Col. Diam. (ft):

1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Shell Color/Shade: Shell Condition White/White

Shell Condition Roof Color/Shade: Good White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal:

Liquid-mounted

Secondary Seal

None

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Quantity

Roof Leg or Hanger Well/Adjustable
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Ungask.
Automatic Gauge Float Well/Unbolted Cover, Gasketed
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed
Column Well (24-in. Diam.)/Built-Up Col.-Sliding Cover, Gask.

Meterological Data used in Emissions Calculations: JFK Intl Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

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TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK046 - Internal Floating Roof Tank BROOKLYN, NY

	Losses(lbs)										
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions						
denatured ethanol	32.98	38.54	184.48	0.00	255.99						

BK046 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	Fabruary	March	April	May	June	July	August	September	October	November	Decembe
Rim Seal Losses (b):	2.1042	2.1491	2.3519	2,6555	2.9525	3.2613	3,4689	3.4117	3,1505	2.7947	2.4780	2.2000
Seal Factor A (lb-mote/ft-yr):	0000.0	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000
Seal Factor B (Ib-mole/fi-yr (mph)^n):	0.4000	0.4900	0.4000	0.4000 0.0251	0.4000	0.4000	0.4000	0.4000	0.4000	9.4000	0.4000	0.4000
Value of Vapor Pressure Function: Vapor Pressure at Daily Average Liquid	0.0199	0.0203	0.0222	0,0251	0.0279	0.0308	0.0327	0.0322	0.0297	0.0264	0.0234	0.0208
Surface Temperature (psia):	1.1226	1.1457	1,2491	1.4024	1.5508	1,7033	1.8039	1,7770	1.6488	1,4721	1,3129	1.1717
Tank Diameter (fi):	45.0000	45,0000	46.0000	46,0000	46.0000	46.0000	46.0000	46.0000	46.0000	46,0000	46.0000	48.0000
Vapor Malacular Welahi (IMb-male):	46.0700	46.0700	46,0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700
Product Factor:	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.8000	1.0000	1.0000
Withdrawal Losses (b):	3.6217	3.4584	3,7122	3.3947	2.6837	3.3322	3.1411	2.9000	2.9298	3.1971	2.9523	3.2165
Number of Columns:	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1,0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000
Net Throughput (gal/mo.): Shell Clingage Factor (bbl/1000 soft);	732,447.3800 0.0015	699,416.8090 0.0015	750,747.5000 0.0015	686,535,0000 0,0015	542,738,0000 0.0015	673,901,8000 0.0015	635,239,8000 0.0015	586,493.8000	592,475.5000	646,576.0000	597,075.5000	650,295,8000
Average Organic Liquid Density (bb/gal);	6,6100	6,6100	6.6100	6,6100	6.6100	6.6100	6,6100	0.0015 6.6100	0.0015 6.6100	0.0015 6.6100	0.0015 6.6100	0.0015 6,6100
Tank Diameter (ft):	46.0000	48.0000	48.0000	48.0000	46.0000	46.0000	46,0000	46.0000	46.0000	46.0000	46.0000	46.0000
Deck Fitting Losses (Ib):	11.7711	12.0227	13.1570	14,8556	16.5169	18.2442	19.3945	19.0858	17.6246	15,6339	13.8622	12,3074
Value of Vapor Pressure Function:	0.0199	0.0203	0.0222	0.0251	0.0279	0.0308	0.0327	0.0322	0.0297	0.0264	0.0234	0.0208
Vapor Molecular Weight (lb/lb-mole):	46.0700	46.0700	48.0700	46,0700	46.0700	46.0700	46.0700	46.0700	46.0700	46.0700	48,0700	46,0700
Product Factor:	1.6000	1.0000	1.0000	1.0000	1.0000	1,0000	1,9008	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact (lb-mole/yr):	154,4000	154.4000	154.4000	154.4090	154.4000	154.4000	154.4000	154.4000	154.4000	154.4000	154.4000	154.4000
Deck Seam Losses (lb):	0.0000	0.0000	0.0000	0,0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0800	0.0000
Deck Seam Length (fi):	0.0000	0.0000	0.0800	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length Factor (tb-mole/ft-yr);	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	. 0,0000	B 0000	0.0000
Deck Seam Length Factor(fl/sqft):	0.0000	0.000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.000	0.0000 0.0000	0.0000 0.0000
Tank Diameter (fi):	46,0000	46,0000	46,0000	46,0000	46,0000	46,0000	46,0000	46.0000	46,0000	48,0000	46.0000	46,0000
Vapor Molecular Welcht (fb/fb-mole):	46.0700	46.0700	46.0700	46.0700	48.0700	46.0700	46,0700	46.0700	46,0700	48.0700		46.0700
Product Factor:	1.0000	- 1.0000	1.0000	1.0000	1.0030	1.0000	1,0000	1.0000	1.0000	1.0000	1,0000	1.0000
Tolat Losses (fb):	17,4970	17.6302	19.2211	20.9059	22.1531	24.8377	26,0024	25.3975	23.7047	21.6256	19.2925	17.7229
					· · · · · · · · · · · · · · · · · · ·		Roof Fitting Loss Fac	tors			 	
Roof Fitting/Status				Quantity	•	KFa(ib-mole/yr)	KFb(fb-mole/(y	r mph^n))		m	Losses(b)	
Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed						56.00	* s:,	0,00 '		00	66.9913	
Access Hatch (24-in, Diam.)/Bolted Cover, Gasketed				1		1.69		0.00		00	1,9140	
Automatic Gauge Float Well/United Cover, Gasketed				i		4.30		17.00		38	5.1440	
Column Well (24-in. Diam.)/Pipe ColFlex. Fabric Sleeve Seal				1		10.00		0.00		00	11.9627	
Sample Pipe or Well (24-In. Diam.)/Stotled Pipe-Slicting Cover, Gask.				1		43.00		0,00	0.		51,4397.	
Roof Leg or Hanger Well/Adjustable				. 5		7.90		0.00		00	47.2528	

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TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK046 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surf emperature (deg		Liquid Bulk Temp	Va	por Pressure (p	sla)	Vaper Mel.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure	•	
/ixkure/Component (2) (50%)	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Weight	Calculations		
enatured ethenol	Jan	44.31	41.43	47.20	53.22	1.1226	N/A	n/A	46,0700			46.07	Option 4: RVP=3.5, ASTM Slope=3		
lenatured ethanol	Feb	45.17	41.85	48.49	53.22	1.1457	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	*	
fenatured ethanol	Mar	48.86	45.12	62.60	53.22	1,2491	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3		
senatured ethanol	Apr	53.89	49.28	58.51	53.22	1.4024	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3		
lenatured ethanol	May	58.34	53.45	63.23	53.22	1.6508	N/A	N/A	46.0703			46.07	Option 4; RVP=3.6, ASTM Slope=3		٠.
lanatured ethanol	Jun	62.56	57.55	67.57	53.22	1.7033	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3		• • • • • • • • • • • • • • • • • • • •
enatured ethanoi	Jul	65.18	60.26	70.09	53.22	1.8039	· N/A	N∕A	46.0700			48.07	Option 4; RVP=3.5, ASTM Slope=3		
lanatured ethanol	Aug	64.49	59.83	69.14	53.22	1.7770	N/A	N/A	48.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3		•
lenatured ethanol	Sep	61.09	56.69	85.49	53.22	1.6488	N/A	N/A	46,0700			46.07	Option 4; RVP=3.5, ASTM Slope=3		
Innatured ethanol	Oct	56.03	52.02	60.04	53.22	1,4721	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Stops=3		:
lenatured ethanol	Nov	51.02	47.86	54.17	53.22	1.3129	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Stope=3		
lonatured ethanol	Dec	46.12	43.39	48.86	53.22	1.1717	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3		

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: City:

BK046 BROOKLYN

State:

Company:

NY SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft): Volume (gallons): 46 00

79.800.00 97.67

Turnovers: Self Supp. Roof? (v/n):

1.00

No. of Columns: Eff. Col. Diam. (ft):

1,00

Paint Characteristics

Internal Shell Condition: Shell Color/Shade: Shell:Condition

Light Rust White/White Good

Roof Color/Shade: Roof Condition:

White/White Good

Rim-Sea! System

Primary Seal: Secondary Seal Mechanical Shoe Rim-mounted

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Ladder Well (36-in, Diam.)/Sliding Cover, Gasketed Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Well (24-in. Diam.)/Pipe Col.-Flex. Fabric Sleeve Seal Sample Pipe or Well (24-in, Diam.)/Slotted Pipe-Sliding Cover, Gask. Roof Leg or Hanger Well/Adjustable

Quantity

Meterological Data used in Emissions Calculations: JFK Intt Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

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Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK045 - Internal Floating Roof Tank BROOKLYN, NY

(a.) (46)	77-11-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1-1	and the comment of the second	Losses(Ibs)	(1) (1) (1) (1) (1) (1) (1) (1) (1) (1)	
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
denatured ethanol	17.21	75.31	184.48	0.00	276.99

Description of the property of th

BK045 - Internal Floating Roof Tank BROOKLYN, NY

Rim Seal Losses (b);	April May	y June	July	August	September	October	November	Decemb
Seal Factor B (ib-molett-fyr (mph)-n);	1.3855 1.5404	4 1,7015	1.8088	1.7800	1,6437	1,4581	1.2929	1,147
Value of Vapor Pressure Function: Vapor Pressure at Daily Average Liquid Surface Temperatum (cps): 1.1.1226 1.1.457 1.2491 1.3 Surface Temperatum (cps): 1.3 Line 1.1.226 1.1.457 1.2491 1.3 Surface Temperatum (cps): 1.3 Line 1.1.226 1.3 Line 1.3 L	0.6000 0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.600
Vapor Pressure at Daily Average Liquid Surface Temperature (psia); 1.1226 1.1457 1.2491 Tank Diameter (II); 24,0000 24,0	0.4000 0.4000	0.4000	0.4000	0.4600	0.4000	0.4000	0.4000	0,400
Surface Temperatum (poia):	0.0251 0.0279	9 0.0308	0.0327	0.0322	0.0297	0.0264	0.0234	0.020
Tank Diameter (ft):	1,4024 1,5503	1,7033	1,6039	1,7770	1,6488	1.4721	1.3129	1.171
Value Very	24.0000 24.0000		24.0000	24,0000	24.0000	24.0000	24,3000	24.000
Product Factor. 1.0000 1.0000 1.0000 1.0000 1.0000 1.0000 1.0000 1.0000 1.0000 1.0000	46.0700 46.0700		46.0700	46,0700	46,0700	46.0700	46.0700	46.070
Number of Columns 1,0000	1.0000 1.0000		1.0000	1.0000	1.0000	1.0000	1,0000	1.000
Effective Column Diameter (ft):	8.6334 5.2440	0 6,5113	6.1378	5.6668	5.7248	6,2473	6.7690	6.283
Net Throughput (gal/mo.): 732,447,3000 689,416,8000 750,747,5000 58 58 58 58 58 58 58	1.0000 1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1,000
Shell Clingage Factor (bb/1000 eqfl);	1.0000 1.0000		1.0000	1,0000	1.0000	1.0000	1.0000	1.000
Average Örganic Liquid Density (Ibigal): Tank Diameter (II): 24.0000 24.	86,535.0000 542,735.0000	673,901.8000	635,239.8000	586,493.8000	592,475.5000	646,576,0000	597,075,5000	650,295,800
Tank Diameter (ft): 24.0000 24.0000 24.0000 24.0000 Deck Fitting Losses (fb): 11,7711 12,0227 13.1570 Value of Vapor Pressure Function: 0,0199 0,0203 0,0222 Vapor Molecular Weight (fisht-mole): 46,0700 45,0700 48.0700 Product Factor: 1,0000 1,0000 1,0000 Tot. Roof Fitting Loss Fact (fb-mole/yr): 154,4000 154,4000 154,4000 Deck Seam Losses (fb): 0,0000 0,0000 0,0000 Deck Seam Length (ft): 9,0000 0,0000 0,0000 De	0.0015 0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.001
Deck Fitting Losses (b):	6,6100 6,6100	6.6100	6.6100	6.6100	6,6100	6.6100	6.6100	6.6100
Value of Vapor Pressure Function: 0.0199 0.0203 0.0222 Vapor Molecular Weight (Bilb-mole): 46.0700 45.0700 48.0700 Product Factor: 1.0000 1.0000 1.0000 Tot. Roof Fitting Loss Fact, (ib-mole/yr): 154.4000 154.4000 Deck Seam Losses (b): 0.0000 0.0000 0.0000 Deck Seam Length (gi): 0.0000 0.0000 0.0000 Deck Seam Length (Pur Length 0.0000 0.0000 0.0000 Peactor (Ib-molerityr): 0.0000 0.0000 0.0000 Deck Seam Length (Factor(Rissqft): 0.0000 0.0000 0.0000 Vapor Molecular Weight (Rissqft): 0.0000 0.0000 0.0000 Vapor Molecular Weight (Rissqft): 46.0700 46.0700 46.0700 Vapor Molecular Weight (Rissqft): 1.0000 1.0000	24.0000 24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Vapor Molecular Weighk (Infih-mole):	14.8556 16.5169		19.3945	19.0858	17.6246	15.6339	13.8622	12.3074
Product Factor;	0.0251 0.0279		0.0327	0.0322	0.0297	0.0264	0.0234	0.0208
Tot. Ronf Fitting Loss Fact.(ib-motelyr): 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 154.4000 156.4000 156.6000 156	46.0700 46.0700		46.0700	46.0700	46.0700	46.0700	46,0700	46.0700
Deck Seam Losses (b):	1.0000 1.0000		1.0000	1,0000	1.0000	1.0000	1.0000	1.0090
Deck Seam Length (ft):	154,4000 154,4000	154.4000	154.4000	154.4000	154.4000	154.4000	154.4000	154.4000
Deck Seam Loss per Unit Length	0.0000 0.0000		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Factor (fb-molefil-yr); 0.0000 0.0000 0.0000 0.0000 Deck Seam Length Factor (flx-file); 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.0000 0	0.0000 0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length Factori(Risqft):								
Tank Diameter (iii)	0.000,0		0000.0	0.0000	0.0000	0.0000	0.0000	0.0000
Vapor Molecular Weight (Ibith-mole): 46,0700 46,0700 46,0700 46,0700 1,0000 <	0.0000 0.0000		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Product Factor; 1,0000	24.0000 24.0000		24.0000	24.0800	24.0000	24.0000	24.0000	24.0000
Fotal Losses (b): 19.9459 19.9018 21,6379 Roof Fitting/Status Ladder Well (36-in, Diam.)/Stiding Cover, Gasketed Access Hatch (24-in. Diam.)/Stiding Cover, Gasketed Automatic Sauge Float Well/Unbolied Cover, Gasketed	46.0700 46.0700		46.0700	46.0700	46.0700	46.0700	46.0700	46.0700
Roof Filling/Status Ladder Well (36-in, £lzm.)/Silding Cover, Gasketed Access Hatch (24-in. D/am.)/Bolled Cover, Gasketed Automatic Sauge Float Well/Unbolled Cover, Gasketed	1.0000 1.0000	1.0000	1.0060	1.0000	1.0000	1,0000	1.0000	1.8000
Ladder Well (36-In, Dłam.)/Silding Cover, Gaskeled Access Hatch (24-In, Dłam.)/Sildled Cover, Gaskeled Automatic Gauge Float Well/Unbolled Cover, Gasketed	22.8745 23.3014	26.4570	27.3410	26.5326	24.9929	23.3392	20.9241	19.7385
Ladder Well (36-In, Đizm.)/Sliding Cover, Gaskeled Access Hatch (24-In, Diam.)/Bidled Cover, Gaskeled Automatic Gauge Float Well/Unbolled Cover, Gasketed			Roof Fitting Loss Faci	kors				
Access Hatch (24-in. Diam.)/Botlled Cover, Gasketed Automatic Gauge Float Well/Unbolled Cover, Gasketed	Quantity	KFa(lb-mole/yr)	KFb(lb-mole.(yr	raph^n)}		m	Losses(lb)	
Access Hatch (24-in. Diam.)/Botlled Cover, Gasketed Automatic Gauge Float Well/Unbolled Cover, Gasketed	1	56,00		0.00	0.	m ·	66.9913	
Automatic Gauge Float Welf/Unbolled Cover, Gasketed	i	1.60		0.00	0.		1,9140	
	i	4.30		17.00	0.		5.1440	
	1.	10.60		0.00	0.			•
Roof Leg or Hanger Well/Adjustable	5 .	7.90		0.00	U. Q.		11.9 627 47.2528.	
Sample Pips or Well (24-in, Diam.)/Stotled Pipe-Skiding Cover, Gask.	1	43.00		0.00		00	51.4397	

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK045 - Internal Floating Roof Tank BROOKLYN, NY

e na ome e la comitana e en Ana e espíricos e la comi			Daily Liquid Suri Emperature (deg		Liquid Bulk Temp	Var	or Pressure (ps	ia)	Vapor Mol.	Liquid Mass	Vapor Mess	Mal.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Mex.	(deg F)	Avg.	Min.	Max.	WeighL	Fract.	Frect.	Weight	Calculations
denatured ethanol	Jan -	44.31	41.43	47.20	53.22	1,1226	N/A	N/A	46,0700			46.07	Ontion 4: RVP=3.5. ASTM Slope=3
denatured etherical	Feb	45.17	41.85	48.49	53.22	1,1457	N/A	N/A	46,0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
denatured ethanol	Mar	48.86	45.12	52.60	53.22	1,2491	N/A	N/A	46,0700			46.07	Option 4: RVP=3.5, ASTM Stope=3
denatured ethanol	Apr	53.89	49.28	58.51	53.22	1.4024	N/A	N/A	46,0700			46.07	Option 4: RVP=3.5, ASTM Stope=3
denatured ethanol	May	58.34	53.45	63.23	53.22	1.5508	NA	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Stope=3
denatured efnanol	Jun	62.56	57.55	67.57	53.22	1.7033	N/A	N/A	48.07BD			46.07	Option 4: RVP=3.5, ASTM Slope=3
denakred sihanol	Jul .	65.18	60.26	70.09	53.22	1.8039	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
denatured efinanol	Aug :	64.49	59.83	69.14	53.22	1.7770	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
denatured ethanol	Sep	61.09	56.69	65.49	53.22	1.6488	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3.
denatured effianol .	Oct	56.03	52.02	60.04	53.22	1.4721	N/A	N/A	46.0700			46.07	Option 4: RVP=3.6, ASTM Stope=3
denatured ethanol	Nov	51.02	47.86	54.17	53.22	1.3129	N/A	N/A	46.0700			46,07	Option 4: RVP=3.5, ASTM Slope=3
denatured ethanof	Dec	46.12	43.39	48.86	53.22	1.1717	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification:

BK045

City: State: BROOKLYN NY

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft): Volume (gallons): 24.00

Turnovers:

79.800.00

Self Supp. Roof? (y/n):

97.67

No. of Columns: Eff. Col. Diam. (ft): 1.00 1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Shell Color/Shade: Shell Condition

White/White Good

Roof Color/Shade: Roof Condition:

White/White

Good

Rim-Seal System

Primary Seal: Secondary Seal Mechanical Shoe

Rim-mounted

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Quantity

Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed Access Hatch (24-In, Diam,)/Bolted Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Well (24-in, Diam.)/Pipe Col.-Flex, Fabric Sleeve Seal Roof Leg or Hanger Well/Adjustable Sample Pipe or Well (24-in, Diam.)/Slotted Pipe-Sliding Cover, Gask.

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK044 - Internal Floating Roof Tank BROOKLYN, NY

Losses(lbs)								
Components		RIm Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions		
STAR - RFG 2.0 (15)		41.22	49.43	. 441.94	0.00	532.59		
Star - RFG 2.0 (13.5)		31.92	34.28	342.29	0.00	408.50		
Star Gasoline (RVP 8.1)	-	34.18	54.67	· 366.50	0.00	455:35.		

BK044 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	March	April	May	June	July	August	September	October	November	Decembe
Film Seal Losses (ib):	9,8312	10.0482	11.0429	10.6917	6.2133	6.8617	7.2974	7.1802	6.6283	11.2903	9,9419	10.2953
Seal Factor A (lb-mole/ft-yr):	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000	0.6000
Seaf Factor B (lb-mole/ft-yr (mph)*n):	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0.4000	0,4000	0.4004
Value of Vepor Pressure Function: Vapor Pressure at Daily Average Liquid	0.1321	0.1351	0.1484	0.1437	0.0785	0.0866	0.0921	0.0907	0.0837	0.1518	0.1336	0.138
Surface Temperature (psia):	6.0619	6.1639	6.6173	6.4598	3,9662	4.3143	4.5422	4.4814	4.1903	6.7266	6.1141	6.2787
Tank Diameler (fl):	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24,0000	24.0000	24,0000
Vapor Molecular Weight (lb/lb-mole):	62.0000	62.0000	62,9000	62,0000	66.0000	66.0000	66.0000	66.0000	66,0000	62.0000	62,0000	62,000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000	1.0000	1,0000	1.0000	1.0000	1.0000	1,0000
Withdrawal Losses (lb):	12.7635	12.1601	13.1262	12.1630	9.7955	12.2485	11.5014	10.5197	10.6057	11.6172	10.5004	11.3800
Number of Columns:	1.0000	1.0000	1.0000	1.0030	1.0000	1,0000	1.0000	1.0000	1.0008	1.0000	1.0000	1.0000
Effective Column Diameter (#);	1.0000	1,0000	-1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Net Throughput (gal/mo.):	1,740,425.6000	1,658,143.1000	1,789,873.1000	1,658,537,6000	1,335,713.9000	1,670,203.3000	1,568,328.0000	1,434,455.7000	1,446,183.0000	1,584,113.4000	1,431,824.5000	1,551,772.6000
Shell Clingage Factor (bbl/1000 sqff):	0.0015	0.0015	0.0015	0.0016	0.0015	0.0015	0.0016	0.0016	0.0015	0.0015	0.0015	0.0016
'Average Organic Liquid Density (lb/gal):	5.0170	5.0170	5.0170	5,0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170
Tank Diameter (#):	24.0000	24.0000	24.0000	24,0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000	24.0000
Deck Fitting Losses (Ib);	105.4126	107.7392	118.4039	114.6383	66.6207	73.5727	78.2447	76.9875	71.0705	121.0574	106.5988	110.3886
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0.1437	0.0785	0.0856	0,0921	0.0907	0.0837	0.1518	0.1336	0.1384
Vapor Molecular Weight (IMb-mole):	62.0000	62,0000	62.0000	62.0000	66.0000	68.0000	66,0000	66,0000	66,0000	62,0000	62.0000	62,0000
Product Factor:	1.0000	1.0000	1,0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Tot. Roof Fitting Loss Fact.(b-mcle/yr):	154.4000	154.4000	. 154,4000	154.4000	154,4000	154,4000	154.4000	154.4000	154,4000	. 154.4000	154.4000	154,4000
Deck Seam Losses (lb):	0.0006	0.0000	0.0000	0.0000	0.0000	0.000.0	0,000	0.0000	0.0000	0.0000	0.0800	0.0000
Deck Seam Length (ft):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0090
Deck Seam Loss per Unit Length		•		•					•			
Factor (b-mote/fi-yr);	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length Factor(ft/sqft):	0000.0	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (fl):	24,0000	24.0000	24.0000	24.0000	24.0000	24.0000	24,0000	24.0000	24.0000	24.0000	24.0000	24.0000
Vapor Molecular Weight (lb/lb-mole):	62.0000	62,0000	62.0000	62.0000	66.0000	66,0000	66,0000	66.0000	65.0000	62.0000	62,0000	62.0000
Product Factor:	1.0000	1.0000	1,0000	1,0000	1.0000	1,0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000
Cotal Losses (ib);	128,0074	129.9475	142,5729	137.4930	82.629 6	92.6829	97,0436	94.6873	89.3046	143.9649	127.0410	132.0639

Roof Fitting/Status	Quantity		illing Loss Factors KFb(ib-mole/(уг mph*n))	m	Losses(lb)
Ladder Well (36-in. Diam.)/Skding Cover, Gasketed Access Hatch (24-in. Diam.)/Skding Cover, Gasketed Automatic Gauge Float Well/Unbolled Cover, Gasketed Cokumn Well (24-in. Diam.)/Pipe Cover, Flex. Fabric Steeve Seal Sample Pipe or Well (24-in. Diam.)/Stotted Pipe-Stding Cover, Gask. Roof Leg or Hanger Well/Adjustable	1 1 1 1 1 5	56.00 1.60 4.30 10.00 43.00 7.90	0.00 0.00 17.00 - · · · · · · · · · · · · · · · · · ·	0.00 0.00 0.38 0.00 0.00 0.00	417.1523 11.9186 32.0313 74.4915 320.3134. 294.2414

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK044 - Internal Floating Roof Tank BROOKLYN, NY

• •			Dally Liquid Surf. emperature (deg		Uquid Butk Temp	Vaş	oor Pressure (ps	ia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure	
Vibriure/Component http://	Month:	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract	Fract.	Weight	Calculations	
STAR - RFG 2.0 (15)	Jan	44.31	41.43	47.20	53,22	6.0619	N/A	N/A	62.0008			62.00	Option 4: RVP=15, ASTM Slope=3	
STAR - RFG 2.0 (15)	Feb	45.17	41.85	48.49	53.22	6.1639	N/A	NA	62.0000			62.00	Option 4: RVP=15, ASTM Slope=3	• "
STAR - RFG 2.0 (15)	Mar	48.86	45.12	52.60	53.22	6.6173	N/A	N/A	82.0000			62,00	Option 4: RVP=15, ASTM Stope=3	
Star - RFG 2.0 (13.5)	Арг	53,89	49.28	58.51	53.22	6.4598	N/A	N/A	62,0880			62,00	Option 4: RVP=13.5, ASTM Slope=3	
Star Gasoline (RVP 8.1)	May	58.34	53.45	63.23	53.22	3,9662	N/A	N/A	69.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3	
lar Gasoline (RVP 8.1)	Jun	62.56	57.55	67.57	53.22	4,3143	NIA	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3	• •
ter Gasoline (RVP 8.1)	Jul	65.18	60.26	70.09	53.22	4,5422	N/A	N/A:	66,0000			66,00	Option 4: RVP=8.1, ASTM Slope=3	
star Gasoline (RVP 8.1)	Aug	64.49	59,83	69.14	53.22	4.4814	N/A	N/A	66,0000			66,00	Option 4: RVP=8.1, ASTM Stope=3	
tar Gasoline (RVP 8.1)	Sep	61.09	56.69	65.49	53.22	4.1903	N/A	N/A	68.0000	. •	٠٠.	66.00	Option 4: RVP=8.1, ASTM Slope=3	***
Star - RFG 2.0 (13.5)	Oct	56.03	52.02	60.04	53.22	6.7266	N/A	N/A	62.0000		F1:	62.00	Option 4: RVP=13.5, ASTM Slope=3	
tar - RFG 2.0 (13.5)	Nov	51.02	.47.86	54.17	53.22	6.1141	N/A	N/A	62.0000		٠.	62.00	Option 4: RVP=13.5, ASTM Slope=3	
TAR - RFG 2.0 (15)	Dec	46.12	43.39	48.86	53.22	6.2787	N/A	N/A	62.0000	-	·. :	62,00	Option 4: RVP=15, ASTM Slope=3	

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification:

BK044 BROOKLYN

City: State:

NY

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft); Volume (gallons); 24.00

79.800.00

Turnovers:

9,800.00

Self Supp. Roof? (v/n):

N

No. of Columns:

1.00

Eff. Col. Diam. (fl);

1.00

Paint Characteristics Internal Shell Condition:

Light Rust

Shell Color/Shade:

White/White

Shell Condition

Good

Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal:

Mechanical Shoe

Secondary Seal

Rim-mounted

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Ladder Welt (36-in. Diam.)/Sliding Cover, Gasketed
Access Hatch (24-in. Diam.)/Bofted Cover, Gasketed
Automatic Gauge Float Well/Unbolted Cover, Gasketed
Column Well (24-in. Diam.)/Pipe Cot.-Flex. Fabric Sleeve Seal
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.
Roof Leg or Hanger Well/Adjustable

Quantity

Meterological Data used in Emissions Calculations: JFK Intl Alrport, New York (Avg Atmospheric Pressure = 14.7 psla)

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK043 - Internal Floating Roof Tank BROOKLYN, NY

Life		Losses(lbs)								
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions					
STAR - RFG 2.0 (15)	94.77	32.86	567.13	0.00	694.76					
Star - RFG 2.0 (13.5)	39.38	13.04	235.70	0.00	288.12					
Star Gasoline (RVP 8.1)	61.24	29.97	366.50	0.00	457.71					

TANKS 4,0 Report

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK048 - Internal Floating Roof Tank BROOKLYN, NY

		Losses(lbs)										
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions							
STAR - RFG 2.0 (15)	270.34	139.72	651.62	0.00	1,061.68							
Star - RFG 2.0 (13.5)	112.35	55.44	270.81	0.00	438.60							
Star Gasoline (RVP 8.1)	174.70	127.46	421.09	0.00	723.25							

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

ماندا	-4:6	 tion

User Identification:

BK049

City: State: BROOKLYN

Company: Type of Tank: SHELL OIL COMPANY - BROOKLYN Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft): Volume (gallons): 47.00

Volume (gailons Turnovers: 420,000.00

Self Supp. Roof? (v/n):

84.12

No. of Columns: Eff. Col. Diam. (ft): 1.00 1.00

Paint Characteristics

Internal Shell Condition: Shell Color/Shade: Light Rust White/White

N

Shell Color/Shade: Shell Condition Roof Color/Shade:

Good White/White Good

Roof Condition:

Rim-Seal System

Primary Seal: Secondary Seal Liquid-mounted None

.

Deck Characteristics

Deck Fitting Category: Deck Type: Detail Welded

Deck Fitting/Status

Quantity

Roof Leg or Hanger Well/Adjustable Column Well (24-in. Dlam.)/Pipe Col.-Flex. Fabric Sleeve Seal Automatic Gauge Float Well/Unbolled Cover, Ungasketed Access Hatch (24-in. Diam.)/Bolled Cover, Gasketed Ladder Well (36-in. Diam.)/Siding Cover, Ungasketed Slotted Guide-Pole/Sample Well/Gask. Stiding Cover, w. Float

Meterological Data used in Emissions Calculations: JFK Intil Airport, New York (Avg Atmospheric Pressure = 14.7 psla)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK049 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surl		Liquid Bulk Temp	Vap	oor Pressure (ps	ia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Weighl	Calculations
STAR - RFG 2.0 (15)	Jan	44.31	41.43	47.20	53.22	6.0619	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Stope=3
STAR - RFG 2.0 (15)	Feb	45.17	41,85	48.49	53.22	6.1639	N/A	N/A	62,0000			62.00	Option 4: RVP=15, ASTM Stope=3
STAR - RFG 2.0 (15)	Mar	48.86	45.12	5260	53.22	6.6173	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Slope=3
Star - RFG 2.0 (13.5)	Арг	53.89	49.28	58.51	53.22	6.4598	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Stope=3
Star Gasoline (RVP 8.1)	May	58.34	53.45	63.23	53.22	3.9662	N/A	N/A	00000.88			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Jun	62.56	57.55	67.57	53.22	4.3143	N/A	N/A	66,0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Juli	65.18	60,26	70.09	53.22	4.5422	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Aug	64.49	59.83	69.14	53.22	4,4814	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Sep	61.09	56.69	65.49	63.22	4.1903	N/A	N/A	66,0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star - RFG 2.0 (13.5)	Oct	56.03	52.02	60.04	53.22	6.7266	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Slope=3
STAR - RFG 2.0 (15)	Nov	51.02	47.86	54.17	53.22	6.8941	N/A	N/A	62.0000		•	62.00	Option 4: RVP=15, ASTM Slope=3
STAR - RFG 2.0 (15)	Dec	46.12	43.39	48.86	63.22	8.2787	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Stope=3

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BK049 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	March	April	Way	June	July	August	September	October	November	Decembe
Rim Seal Losses (fb):	51.3409	52,4740	57.6682	55.8342	32,4474	35,8333	38.1088	37.4965	34.6147	68.9606	60.9736	53.764
Seal Factor A (lb-mole/ft/yr):	1.6000	1.6000	1.6000	1.6000	1,6000	1.6000	1,6000	1.6000	1,6000	1.5000	1.6000	1.600
Seal Factor B (lb-mole/fl-yr (mph)*n):	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	9.3000	0.3000	0.3000	0.3000	0.300
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0.1437	0.0785	0.0866	0.0921	0.0907	0.0837	0.1518	0.1569	0,138
Vapor Pressure at Daily Average Liquid				•								
Surface Temperature (psia):	6.0619	6.1639	6.6173	6.4598	3,9662	4,3143	4.5422	4.4514	4.1903	6.7266	6.8941	6.278
.Tank Diameter (ft):	47.0000	47.0000	47.9000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.000
Vapor Molecutar Weight (lb/lb-mole):	62,0000	62.0000	62,0000	62.0000	66.0000	66,0000	66.0000	66,0000	66,0000	62,0000	62.0000	62.000
Product Factor:	1,0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1,0000	1,0000	1.0000	1.0000	1.000
Mühdrawal Losses (lb):	12.7831	12.2912	13.0403	11.5524	8.6235	10.5284	10.0602	9.5217	9,6417	10.3351	10.1386	11.2000
Number of Columns:	1.0000	1,0000	1,0000	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000	1.0000	1.0000	1.0000
Effective Column Diameter (ft):	1.0000	1.0000	1.0000	1.0000	1.0000	1.0080	1.0000	1.0000	1,0000	1.0000	1,0000	1.000
Net Throughput (gal/mo.):	3,481,716.0000	3,347,731.0000	3,551,759,5000	3,146,507.5000	2,348,762,5000	2,867,612.5000	2,740,080.0000	2,593,403.5000	2,626,092,5000	2,814,950.0000	2,761,443.5000	3,050,615,500
Shell Clingage Factor (bbl/1000 sqfl):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0D15	0.0015	0,0015	0.0015	0.0019
Average Organic Liquid Density (lb/gal):	5.0170	5.0170	5.0170	5,0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170
Tank Diameter (N):	47,0000	47.0000	47.0000	47,0000	47.0000	47.0000	47.0000	47.0000	47,0000	47.0000	47.0900	47.0000
Deck Fitting Losses (lb):	155.2515	158.6780	174.3851	168,8391	98.1188	108.3577	115.2387	113.3870	104.6725	178.2931	184.3803	162.5801
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0,1437	0.0785	0.0866	0.0921	0.0907	0.0837	0.1518	0.1569	0.1384
Vapor Molecular Weight (Ib/lò-mole):	62.0000	62.0000	62.0000	62,0000	0000.00	0000,88	66,0000	66.0000	66,0000	62,0000	62,0000	62,0000
Product Factor.	1,0000	1.0000	1,0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000
Tot. Roof Fitting Loss Fact.(lb-mole/yr):	227.4000	227.4000	227.4000	227.4000	227.4000	227.4000	227.4000	227.4000	227,4000	227.4000	227.4000	227.4000
Deck Seam Losses (Ib):	0,000,0	0.0000	0000.0	0000,0	0.0003	0.0000	0.0000	0.0000	0.0900	0.00CB	0.0000	0.0000
Deck Seam Length (ft):	0000,0	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0068	0.0000	0.0000
Deck Seam Loss per Unit Length												
Factor (to-mole/ft-yr):	0.0000	0.0000	0.0000	0,0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length Factor(ft/sqft):	0.0000	0.0000	D.0900	0.000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (ft):	47,0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47,0000	47.0000	47.0000	47,0000	47.0000
Vapor Molecular Weight (lb/lb-mole):	62,0000	62,0000	62.0000	62,0000	68.0000	66.0006	66.0000	66.0000	66,0000	62,0000	62.0000	62.0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Total Losses (lb):	219,3755	223.4432	245.0938	236.2257	139.1897	154,7194	163,4077	160.4052	148.9289	247.5858	255,4926	227.5448
	**************************************						Roof Fitting Loss Fa	clors				
Roof Fitting/Status				Quant	ity	KFa(ib-mole/yr)	KFb(lb-mole/(m	Losses(ib)	
Roof Leg or Hanger Well/Adjustable					12	7.90		0.00	(0.00	717.4380	
Column Well (24-in, Diam.)/Pipe ColFlex, Fabric Sleave Seal					1	10.00		0.00		0.00	75.6791	
Automatic Gauge Float Well/Unbolted Cover, Ungasketed					1	14.00		5.40		1.10	105.9508	
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed					1	1.60		0.00		0.00	12.1087	
Ladder Well (364n, Diam, VSIding Cover, Ungasketed					i	76.00		0.00		0.00	575.1613	
Stotled Guide-Pole/Sample Well/Gask, Sliding Cover, w. Float					i	31,00		36.00		2.00	234.6053	

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TANKS 4.0.9d

Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK049 - Internal Floating Roof Tank BROOKLYN, NY

146	Losses(lbs)												
Components	Rim Seal Loss	Withdrawl Loss	Deck Filting Loss	Deck Seam Loss	Total Emissions								
STAR - RFG 2.0 (15)	276.22	59.45	835.28	0.00	1,170.95								
Star - RFG 2.0 (13.5)	114.79	21.89	347.13	0.00	483.81								
Star Gasoline (RVP 8.1)	178.50	48.38	539.77	0.00	766.65								

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

14	lan	tifi	ca	41	an

User Identification: City: BK050 BROOKLYN

State: Company: NY SHELL OIL COMPANY - BROOKLYN Internal Floating Roof Tank

Type of Tank; Description:

.

Tank Dimensions

 Diameter (ft):
 47.00

 Volume (gations):
 424,200.00

 Turnovers:
 83.29

 Self Supp. Roof? (y/n):
 N

 No. of Columns:
 1.00

 Eff. Col. Diam. (ft):
 1.00

A may green and the proof of the expect of a given

Paint Characteristics

Internal Shell Condition:

Shell Color/Shade:

White/White
Shell Condition

Good
Roof Color/Shade:

White/White
Roof Condition:

Good

Rim-Seal System

Primary Seal: Secondary Seal Liquid-mounted None

Deck Characteristics

Deck Fitting Category: Deck Type: Detail Welded

Deck Fitting/Status

Roof Leg or Hanger Well/Adjustable
Column Well (24-in. Dlam.)/Pipe Col.-Flex. Fabric Sieeve Seal
Automatic Gauge Float Well/Unbolled Cover, Ungasketed
Access Hatch (24-in. Dlam.)/Bolled Cover, Gasketed
Slotted Guide-Pole/Sample Well/Gask. Sliding Cover, w. Float
Cadder Well (36-in. Diam.)/Sliding Cover, Ungasketed

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

Quantity

file:///Cl/Program

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK050 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surf emperature (deg		Liquid Buik Temp	Va	oor Pressure (p:	sla)	Vapor Mol.	Liquid Mass	Vapor Mass	¹Mol.	Basis for Vapor Pressure
xture/Component	Month	Avg.	Min.	Мах.	(deg F)	Avg.	Min,	Max.	Weight.	Fract.	Fract.	Weight	Calculations
AR - RFG 2.0 (15)	Jan	44.31	41,43	47.20	53.22	6.0619	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Slope=3
TAR - RFG 2.0 (15)	Feb	45.17	41.85	48.49	53.22	6.1639	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Slope=3
TAR - RFG 2.0 (15)	Mar	48.86	45.12	52.60	53.22	6.6173	N/A	N/A	62.8000			62.00	Option 4: RVP=15, ASTM Slope=3
ar - RFG 2.0 (13.5)	Apr	53.89	49.28	58.51	53.22	6.4598	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Slope=3
ar Gasoline (RVP 8.1)	May	55.34	53.45	63.23	53.22	3.9662	N/A	N/A	0000.88			66.00	Option 4: RVP=8.1, ASTM Slope=3
ar Gasoline (RVP 8.1)	Jun	62.56	57.55	67.57	53.22	4.3143	N/A	N/A	66,0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
ar Gasoline (RVP 8.1)	Jul	65.18	60.26	70.09	53.22	4.5422	:N/A	N/A	66,0000	•		66,90	Option 4: RVP=8.1, ASTM Slope=3
ar Gasoline (RVP 8.1)	Aug	64.49	59.83	69.14	53.22	4.4814	N/A	N/A	86.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
ar Gasoline (RVP 8.1)	Sep	61.09	56.69	65.49	53.22	4.1903	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
ar - RFG 2.0 (13.5)	Oct	56.03	52.02	60.04	53.22	6.7268	N/A	N/A	62.0000			62.00	Option 4: RVP=13.5, ASTM Slope=3
AR - RFG 2.0 (15)	Nov	51.02	47.86	54.17	53.22	6,5941	N/A	N/A	62.0000			62.00	Option 4: RVP=15, ASTM Slope=3
TAR - RFG 2.0 (15)	Dec	48.12	43,39	48.86	53.22	6.2787	N/A	N/A	62,0000			62.00	Option 4: RVF=15, ASTM Slope=3

BK050 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	March	lingA	May	June	July	August	September	October	November	December
Firm Seal Losses (Ib):	51.3409	52,4740	57.6682	55.8342	32.4474	35.8333	38.1088	37,4965	34.6147	58.9606	60.9736	53.7644
Seal Factor A (fb-mole/ft-yr):	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1.6000	1,6000	1.6000	1.6000
Seal Factor B (to-mole/ft-yr (mph)/n):	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000	0.3000
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0.1437	0.0785	0.9866	0.0921	0,0907	0.0837	0.1518	0.1569	0.1384
Vapor Pressure at Daily Average Liquid												
Surface Temperature (psia):	6,0619	6.1639	6.6173	6.4598	3.9662	4.3143	4.5422	4.4814	4.1903	6.7266	6.8941	6.2787
Tank Diameter (fl):	47,0000	47.0000	47.0000	47.0DC0	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000
Vapor Molecular Weight (lb/lb-mole):	62,0000	62.0000	62,0000	62.0000	86.000C	66,0000	66.0000	66.0000	66,0000	62,0000	62.0000	62.0000
Product Factor.	1,0000	1.0000	1.0900	1.0000	1,0000	1.0000	1.0000	1,0000	1,0000	1.0000	1.0000	1,0000
Withdrawal Losses (ib):	12.7831	12.2912	13.0403	11.5524	8.6235	10.5284	10,0602	9.5217	9.6417	10.3351	10.1386	11.2003
Number of Columns:	1,0008	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000
Effective Column Diameter (ff):	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000
Net Throughput (galfmo.):	3,481,716.0000	3,347,731.0000	3,551,759.5000	3,146,507.5000	2,348,762.5000	2,867,612.5000	2,740,080.0000	2,593,403.5000	2,626,092.5000	2,814,950.0000	2,761,443,5000	3,050,616.5000
Shell Clingage Factor (bbl/1000 aqft):	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0615
Average Organic Liquid Density (lb/gal):	5.0170	5.0170	5.0170	5.0170	5.0170	5.0170	5.8170	6.0170	5.0170	5.0170	5.0170	5.0170
Tank Diameter (ft):	47.0000	47.0000	47.0000	47.0000	47,0000	47,0000	47.0000	47.0000	47,0000	47.0000	47.0000	47.0000
eck Fitting Losses (lb):	155.2515	158.6780	174.3851	168.8391	98.1188	108.3577	115.2387	113.3870	104.8725	178.2931	184.3803	162.5801
Value of Vapor Pressure Function:	0.1321	0.1351	0.1484	0.1437	0.0785	0.0866	0.0921	0,0907	0.0837	D.1518	0,1569	0.1384
Vapor Molecular Weight (Ib/Ib-mole);	62.0000	62.0000	62,0000	62.0000	66,0000	66.0000	66,9000	66,9000	66,0000	62.0000	62.0000	62,0000
Product Factor:	1.0000	1.0000	1.0000	1.0000	1.00CD	1.0000	1.0090	1.0000	1.0000	. 1.0000	1.0000	1,0000
ToL Roof Fitting Loss Fact.(lb-mole/yr):	227.4000	227,4900	227.4000	227.4000	227.4000	227,4000	227.4000	227,4000	227,4000	227.4000	227.4000	227.4000
eck Seam Losses ((b):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Length (R):	D.60C0	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Deck Seam Loss per Unit Length									•	•		
Factor (lb-mole/it-yr):	0.000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	. 0.0000	0.0000
Deck Seam Length Factor(fVsqfl):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Tank Diameter (ft):	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47.0000	47,0000	47.0000
Vapor Molacular Weight (Ib/Ib-mole):	62.0060	82.0000	62,0000	62.0000	66.0000	66.0000	66.0000	68.0000	66.0000	62,0000	62,0000	62.0000
Product Factor:	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000
Total Losses (Ib):	219.3755	223.4432	245.0936	236.2257	139.1897	154.7194	163.4077	180.4052	148,9289	247,5888	255.4928	227,5448
Roof Fitting/Status				Quanti	ity	KFa(fb-mole/yr)	Roof Fitting Loss Fa KFb(lb-mole/(m	Losses(lb)	
			····	· · · · · · · · · · · · · · · · · · ·								
Roof Leg or Hanger Well/Adjustable					12	7.90		0.00		0.00	717.4380	

Roof Fitting/Status	Quantity	KFa(fo-mole/yr)	Roof Filling Loss Factors KFb(b-mole/(yr mph/n))	· m	Losses(b)
Roof Leg or Hanger Well/Adjustable	12	7.90	0.00	0.00	717.4380
Column Well (24-in, Diam.)/Pipe ColFlex, Fabric Sleeve Seal	1	10.00	9.00	0.00	75.6791
Automatic Gauge Float Well/Unbolted Cover, Ungasketed	1	14.00	5.40	1.10	105.9508
Access Hatch (24-in, Diam.)/Solled Cover, Gasketed	1	1,60	00.0	0.00	12.1087
Stotted Guide-Pole/Sample Well/Gask. Silding Cover, w. Float	1	31.00	36,00	2.00	234.6053
Ladder Weij (36-in, Diam,)/Sikiing Cover, Ungaskefed	. 1	76.00	0.00	0.00	575.1613

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK050 - Internal Floating Roof Tank BROOKLYN, NY

		Losses(lbs)												
Components	Rim Seal Loss	Withdrawi Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions									
STAR - RFG 2.0 (15)	276.22	59.45	835.28	0.00	1,170.95									
Star - RFG 2.0 (13.5)	114.79	21.89	347.13	0.00	483.81									
Star Gasoline (RVP 8.1)	178.50	48.38	539.77	0.00	766.65									

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: City: State:

Company:

Type of Tank: Description: BK052 Brooklyn

NY SHELL OIL COMPANY - BROOKLYN

Horizontal Tank

Tank Dimensions

 Shell Length (ft):
 18.00

 Diameter (ft):
 6.00

 Volume (gallons):
 3,780.00

 Turnovers:
 2.81

 Net Throughput(gallyr):
 10,649.00

 Is Tank Heated (v/n):
 N

Is Tank Heated (y/n):

Is Tank Underground (y/n):

N

Paint Characteristics

Shell Color/Shade: White/White Shell Condition Good

Breather Vent Settings

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK052 - Horizontal Tank Brooklyn, NY

			Daily Liquid Surf emperature (deg		Liquid Bulk Temp	Va	por Pressure (p	sia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol,	Basis for Vapor Pressure
lxture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max,	Weight.	Fract.	Fract.	Weight	Calculations
eneric Additive	Jan	44.31	41.43	47.20	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36
eneric Additive	Feb	45.17	41.85	48.49	53,22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36
eneric Additive	Mar	48.86	45.12	52.60	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36
eneric Additive	Арг	53.89	49.28	58.51	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP50 = .36 VP60 = .36
eneric Additive	May	58,34	53.45	63.23	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP60 = .36
eneric Additive	Jun	62.56	57.55	67.57	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
eneric Additive	, Jul	65.18	60.26	70,09	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1; VP60 = .36 VP70 = .36
eneric Additive	Aug	64.49	59.83	69.14	53.22	0.3600	0.3600	0.3600	120,0000			1,410.00	Option 1: VP60 = .38 VP70 = .38
eneric Additive	Sep	61.09	56.69	65.49	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
eneric Additiva	Oct	56.03	52.02	60.04	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP60 = .36
eneric Additive	Nov	61.02	47.88	54.17	53.22	0.3600	0.3600	0.3600	120.0000			1,418.00	Option 1: VP50 = .36 VP60 = .36
eneric Additive	Dec	46,12	43,39	48.86	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36

BK052 - Horizontal Tank Brooklyn, NY

			-									
lenth:	January	February	March	April	May	June	July	August	Seplember	October	November	Dacem
landing Losses (lb):	1.4293	1.5155	1.9002	2,2895	2.4808	2.4223	2.4248	2.2883	2.1074	1,9984	1.4877	1.32
Vapor Space Volume (cir il):	324.1643	324.1643	324.1643	324.1643	324.1643	324.1643	324.1643	324.1643	324.1643	324.1643	324.1643	324.16
Vapor Density (lb/cu ft);	0.0080	0.0080	0.0079	0.0078	0.0078	0,0077	0.0077	. 0.0077	0.0077	0.0078	0.0079	0,00
Vapor Space Expansion Factor:	0.0187	0.0221	0.0253	0.0318	0.0336	0.0342	0.0333	0.0313	0.0298	0.0269	0.0205	0.01
Vented Vapor Saturation Factor:	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.94
ank Vapor Space Volume:	324,1643	324.1643	324.1643	504 4040	201.4048	324.1643	774 4540	324,1643	324.1643	324.1643	324,1643	324,16
Vapor Space Volume (cu ft):				324.1643	324.1643		324.1643					-6.00
Tank Diameter (ff):	6.0000	6.0000 11.7294	6.0000 11,7294	6.0000 11,7294	6.0000	6.0000 11,7294	6.0000 11.7294	6.0000 11.7294	6.0000 11.7294	6.0000 11.7294	6.0000 11,7294	11.7
Effective Diameter (fi):	11,7294 3,0000	3.0000	3,0000	3.0000	11.7294 3.0000	3,9000	3.0000	3.0000	3.0000	3.0000	3.0000	3.00
Vapor Space Outage (ft): Tank Shelf Length (ft):	18.0000	18.0000	18.0000	18.0000	18.0000	18.0000	18.0000	18.0000	18.0000	18.0000	18.0000	18.0
abor Density						•						
Vapor Density (lb/cu fl):	0.0080	0.0080	0.0079	0.0078	0.0078	0.0077	0.0077	0.0377	8.0077	0.0078	0.0079	0.00
Vapor Molecular Weight (Ib/Ib-mole): Vapor Pressure et Daily Average Liquid	120.0000	120,0000	120,0000	120.0000	120.0000	120.0000	120.0008	120,0000	120.0000	120.0000	120.0000	120.0
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0,3600	0.3600	0.3600	0.3600	0.3600	0.3
Daily Avg. Liquid Surface Temp. (deg. R):	503,9812	504.8409	508.5307	513.5620	518.0109	522.2313	524.8471	624.1592	520.7602	515.6984	510.6856	505.79
Daily Average Ambient Temp. (deg. F): Ideat Gas Constant R	31.3000	32,5000	39.9000	50.3000	59.7000	68.9500	74.9500	74.0000	67.2000	56.7000	46.4000	35.7
(psia cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.
Liquid Bulk Temperature (deg. R):	512,8900	512.8900	512.8900	512,8900	512,8900	512.8900	612.8900	612.8900	512,8900	512,8900	512.8900	512,6
Tank Paint Solar Absorptance (Shell):	0.1700	0,1700	0.1790	0.1700	0.1700	0.1700	0.1700	0,1700	0.1700	0.1700	0.1700	0.1
Daily Total Solar Insulation Factor (Btu/agti day):	548,0000	795,0000	1,118.0000	1,457.0000	1,690,0000	1,802.0000	1.784.0000	1,583,0000	1,280,0000	951,0000	593,0000	457.0
• •			,	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	,,,,,,,,,,,,	.,			,		,	
apor Space Expansion Factor Vapor Space Expansion Factor:	0.0187	0.0221	0.0253	0.0318	0.0336	0.0342	0.0333	0.0313	0.0296	0.0269	0.0205	0.0
Daily Vapor Temperature Range (deg. R):	11.5365	13.2882	14.9597	18.4553	19.5644	20.0255	19.6518	18.6231	17.6128	16.0468	12.6147	10.9
ally Vapor Pressure Renge (psia);	0.0000	0.0000	0.0000	0.0000	8,0000	0.0000	0.0000	00000	0.0000	0.0000	0.0000	0.0
Breather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0,0600	0.9600	0.0600	0.0
Vapor Pressure at Dally Average Liquid												
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0,3
/apor Pressure at Daily Minimum Liquid	0.000	0.0000	0.2000	0.2000	0.9500	0.9600	0,3600	44600	A 2000	0.0000	0.3600	0.3
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0,3600	0.3600	0.3000	0.3600	0.3600	0,3600	0,3000	U.
/apor Pressure at Dally Maximum Liquid	0.3600	0.3600	0,3600	8,3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3
Surface Temperature (psia):	503.9812	504.8409	508,5307	513.5620	518.0109	522,2313	524.8471	524.1592	520.7602	515.6984	510.6856	505.7
Dally Avg. Liquid Surface Temp. (deg R); Daily Min. Liquid Surface Temp. (deg R);	501.0970	501,5188	504,7883	508,9481	513.1198	517.2249	519.9342	519.5034	516.3570	511.6867	607.5319	503.
Dally Max, Liquid Surface Temp. (deg R);	506,8663	508,1629	512,2731	518.1758	522,9020	527.2377	529,7601	528.8149	525,1634	519,7101	513,8393	508.5
Daily Ambient Temp. Range (deg. R):	12.4000	13.2000	13.4000	16,0000	16.0000	15.9000	15,5000	15.4000	16.0000	16.0000	13.6000	12.
nted Vapor Saturation Factor												
/ented Vapor Saturation Factor:	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.9459	0.5
/epor Pressure at Daily Average Liquid:												
Surface Temperature (psia):	0,3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600 -	0.3600	0.3603	0.3600	0.3
(apor Space Outage (ft):	3.0000	3.0000	3.8000	3.0000	3.0000	3,0000	3.0000	3.0000	3.0000	3.0000	3.0000	3.0
	1.0718	1.0442	1.0657	0.9582	0.7692	0.9673	0.9137	0.8482	0.8269	0.8584	0.7666	8.0
orking Losses (lb); Zapor Molecular Welght (lb/lb-mole);	120,0000	120,0000	120,0000	120.0000	120,0000	120.0000	120.0000	120,0000	120.0000	120.0000	120,0000	120.0
/apor Motecular weight (loxio-mote); /apor Pressure at Daily Average Lilouid	120,0000	Vederal	120,0000	120,000	120,000	140.0000	120.0000	IEVAUGU	120.0000	120.0000	120,0000	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3
surrace remperature (para): let Throughput (galimo.):	1,042.0000	1,015.2000	1,036.1000	931,6000	747,8000	940,4000	888.3000	824.6000	803,9000	832,6000	745.3000	811.3
er maugrapus (gasmos). nauai Turnovers:	2.8093	2.8093	2.8093	2.8093	2.8093	2.8093	2,8083	2.8093	2.8093	2.8093	2.8093	2.
umover Factor	1.0000	1,0000	1.0000	1.0000	1.0000	1.0800	1.0000	1.0000	1.0000	1,0000	1,0000	1,1
Carnover raccor; Carok Diameler (ft);	6.0000	6.0000	6.0000	6.0000	6.0000	6.0000	6.0000	6.0000	6.0000	6.0000	6.0000	6.0
Yorking Loss Product Factor:	1.0000	1.0000	1.0000	1,0000	1.0000	1,0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0
TOTARIO LUSO FIGUROL FORMA.	1.0000	1.0000	1.0000	1.4000	1.0000	1.0000	1.0000	12000	1.0000	1.0000	1.0000	1.0

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Talal Losses (lb):	2.4921	2.5597	2.9659	3.2477	3,2500	3.3896	3.3385	3.1364	2,9343	2.8548	2.2543	2.1570
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TANKS 4.0 Repor:

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK052 - Horizontal Tank Brooklyn, NY

	Losses(lbs)								
Components	Working Loss	Breathing Loss	Total Emissions						
Generic Additive	10.92	23,66	34.58						

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: City:

BK053 Brooklyn

State: Company:

SHELL OIL COMPANY - BROOKLYN Horizontal Tenk

Type of Tank:

Description:

Tank Dimensions

Shell Length (ft): 16.00 Diameter (ft): 8.00 4,200.00 Volume (gallons): 1.92 Turnovers: 8,050.00 Net Throughput(gal/yr):

N

Is Tank Healed (y/n): Is Tank Underground (y/n):

Paint Characteristics

Shell Color/Shade: White/White Shell Condition Good

Breather Vent Settings

-0.03 Vacuum Settings (psig): 0.03 Pressure Settings (psig)

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Almospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK053 - Horizontal Tank Brooklyn, NY

			Delly Liquid Surf. Temperature (deg F)		Liquid Bulk Temp	Vapor Pressure (psia)		sia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mol,	Basis for Vapor Pressure
Mixture/Component Month Avg. Min.	Max.	(deg F)	Avg.	Min. Max.		Weight.	FracL	Fraci.	Weight	Calculations			
ontaci Waler	Jan	44.31	41.43	47.20	53.22				66.0000			66.00	
ontact Water	Feb	45.17	41.85	48.49	53.22				68.0003			66.00	
ontact Water	Mar	48.86	45.12	52.60	53.22				66.0000			66.00	
ontact Water	Apr	53.89	49.28	58.51	53.22				66.0003			66.00	
intact Water	May	58.34	53.45	63.23	53.22				66.0000			66.00	
entact Water	Jun	62.56	57.55	67.57	53.22				66.0000			66.00	
ontact Water	· Jul -	65.18	60.28	70.09	53.22				66.0000			66.00	
ontact Water	Aug	64,49	59.83	69.14	53.22				66.0000			66.00	
ontact Water	Sep	61.09	56.69	65.49	53.22				66,0000			66.00	
ontact Water	Oct	56.03	52.02	60.04	53.22				66.0003			66.00	
ontact Water	Nov	51.02	47.86	54.17	53.22				0000.88			66.00	
ontact Water	Dec	46.12	43.39	48.86	53.22				66.0000			66.00	

BK053 - Horizontal Tank Brooklyn, NY

									·					
Month:	January	February	March	April	Мау	June	July	August	September	October	November	December		
Standing Losses (lb):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000		
Vapor Space Volume (cu ft):	512.2597	512.2597	512.2597	512.2697	512.25 9 7	512,2597	512.2597	512,2597	512,2597	512,2597	512.2597	512.2597		
Vapor Density (lb/cu fl):	0.0000	0,0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000		
Vapor Space Expansion Factor:	0.0168	0.0222	0.0254	0.0319	0.0337	0.0343	0.0334	0.0314	0.0297	0.0270	0.0206	0.0176		
Vented Vapor Saturation Factor:	1.0000	1.0000	1.0000	1 .00 00	1.0000	1.0000	1,0000	1,0000	1.6000	1.0000	1.0000	1,0000		
Tank Vapor Space Volume:	512.2597	512,2597	512.2597	512.2597	512.2597	512.2597	512.2597	512.2697	512.2597	512,2597	512,2597	512,2597		
Vepor Space Volume (cu fl): Tank Diameter (fl):	8,0000	8,0000	8.0000	512.2091 8.0000	8.0000	8.0000	8.0000	8.0090	8.0000	8.0000	8,0000	8,0000		
Effective Diameter (fi):	12,7694	12,7694	12.7694	12,7694	12.7694	12.7694	12,7694	12.7694	12,7694	12.7694	12.7694	12.7694		
Vapor Space Outeoe (fil):	4.0000	4.0000	4.0000	4.0000	4.0000	4,0000	4.0000	4.0000	4.0000	4.0000	4,0000	4.0000		
Tank Shell Length (ft):	16.0000	16,0000	16.0900	16.0000	16.0000	16.0000	18.0000	16.0000	16.0000	16.0009	16.0000	16,0000		
Vapor Density														
Vapor Density (lb/cu ft):	0.000	0.000	0.0000	0.0000	0,0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.000	0.0000		
Vapor Molecular Weight (Ib/Ib-mole):	66.0000	66.0000	66,0000	66.0000	66,0000	66,0000	66.0000	66,0000	66.0000	66.0000	0000.33	€6.0000		
Vapor Pressure at Dally Average Liquid				* * * * * * * * * * * * * * * * * * * *								0.0000		
Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	9.0000	0.0000	0.0000	0.0000	0.0000		
Daily Avg, Liquid Surface Temp, (deg. R):	503.9812	504.8409	508.5307	513.5620	518.0109	522.2313 68.9500	524.8471 74.9500	524.1592 74.0000	520.7602	515,6984 56,7000	510.6856 46.4000	505.7950 35.7000		
Daily Average Ambient Temp. (deg, F): Ideal Gas Constant R	31,3000	32.5000	39,9000	50,3000	59.7000	08.9500	74.9000	74,0000	67.2000	55.7000	40.4000	33.7000		
(psla cuft / (lb-mol-deg R)):	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731	10.731		
Liquid Bulk Temperature (deg. R):	512,8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900		
Tank Paint Solar Absorptance (Shell):	0.1700	0.1700	0.1700	0.1790	0.170D	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700		
Daily Total Soler Insulation	040.000	705 0000	d ddn aban'	/ t== anno	4 555 5555	4 444 2444	4 704 0000	4 500 5050	4 000 0000	004.004	500 0000	157 6665		
Factor (Btu/sqft day):	548.0000	795.0000	1,118.0000	1,457.0000	1,690.0000	1,802.0000	1,784.0000	1,593.0000	1,280.0000	951.0000	593.0000	457.0000		
/apor Space Expansion Factor														
Vapor Space Expansion Factor:	0.0198	0.0222	0.0254	0.0319	0.0337	0.0343	0.0334	0.0314	0.0297	0.0270	0.0206	0.0176		
Daily Vapor Temperature Range (deg. R):	11,5365 8,0000	13,2882 0,0090	14.9697 0.0000	18.45\$3 0.8800	19.5644 0.0000	20.0255	19.6518 0.0000	18.6231	17.6128	16.0468	12.6147 0.0000	10.9593		
Daily Vapor Pressure Range (psia): Breather Vent Press, Setting Range(psia):	8,0600	0.0600	0.0800	0.0600	0.0000	0.0600	0.0000	0,000,0 0,000,0	0.0000 0.0600	0.0000 0.0600	0.0600	0.0800		
Vapor Pressure at Daily Average Liquid	0.4000	0.0000	0.0000	0.000	0.0000	0.5050	0.0000	0.0000	0.0000	0.0000	0.000	0.000		
Surface Temperature (osla):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000		
Vapor Pressure at Daily Winimum Liquid								*****						
Surface Temperature (psia):	0.000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000		
Vapor Pressure at Daily Maximum Liquid														
Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0,0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000		
Daily Avg. Liquid Surface Temp. (deg R):	503.9812	504.8409	508.5307	513.5620	518.0109	522.2313	524.8471	524.1592	520.7602	515,6984	510.6856	505.7950		
Daily Min. Liquid Surface Temp. (deg R):	501.0970	501.5188	504.7883	508.9481 518.1758	513.1198	517.2249	519.9342 529.7601	519.5034 628.8149	516.3570	511.6887 519.7101	507.5319 513.8383	503.0551 508.5348		
Daily Max, Liquid Surface Temp. (deg R): Daily Ambient Temp. Range (deg, R):	506.8653 12.4000	508.1629 13.2000	512.2731 13.4000	16.0000	522,9020 16,0000	527.2377 15,9000	15.5000	15.4000	525.1634 16.0000	15.0000	13,6000	12,2000		
Dary America Temp. reside (ded. v.)	12.4000	13.2000	10,4000	10.0000	10.0000	13,3000	13.3000	10.4000	10.000	10.0000	13.0000	UUQAAI		
/ented Vapor Saluration Factor	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1,9000	1.0000	1.0000	1,0000	1.0000	1,0000		
Vented Vapor Saturation Factor: Vapor Pressure at Daily Average Liquid:	1.0500	1.0000	1.000	1.0000	LUGQU	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000		
Surface Temperature (psis):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0,000	0,000	0.0000	0.0000		
Vapor Space Outage (#):	4.0000	4.0000	4,0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000		
and the state of t		******	******											
Vorking Losses (lb):	0.0000	0.0000	0,000	0.0000	0,0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0,0000		
Vapor Molecular Weight (IL/Ib-mole):	66.0000	66.0000	66.0000	68.0000	66.0000	66.0000	66.0000	0000.38	66.0000	66.0000	66.0000	88.0000		
Vapor Pressure at Daily Average Liquid														
Surface Temperature (psia):	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000		
Net Throughput (gal/mo.):	670.8333	670.8333	670.8333	670.8333	670.8333	870.8333	670.8333	670.8333	670,8333	670.8333	670.8333	670.8333		
Annual Turnovers:	1.9167	1,9167	1.9167	1.9167	1,9167	1.9167	1.9167	1.9167	1.9167	1.9167	1.9167	1.9167		
Turnover Factor:	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1,0900	1.0000	1.0000	1.0000	1.0000		
Tank Diameter (ft):	8,0000	8.0000	8.0000	9.0000	9.0000	8.0000	8.0000	8.0000	8.0000	8.0000	8,0000	8.0000		
Working Loss Product Factor:	1.0000	1.0000	1.0000	1.0000	1,0000	1,0000	1,0000	1.0000	1.0000	1,0000	1.0000	1,0000		

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK053 - Horizontal Tank Brooklyn, NY

	The second secon	Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Contact Water	0.00	0.00	0.00

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: City:

BK054 Brooklyn NY

State: Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Horizontal Tank

Description:

Tank Dimensions

14.00 Shell Length (ft): 8.00 Diameter (ft): 4,200.00 Volume (gallons): 2.81 Turnovers: Net Throughput(gal/yr): 11.799.00

Ñ

Is Tank Heated (y/n): Is Tank Underground (y/n):

Paint Characteristics

Shell Color/Shade: Shell Condition

White/White Good

Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig)

-0.03 0.03

Meterological Data used in Emissions Calculations: JFK Intl Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK054 - Horizontal Tank Brooklyn, NY

				aily Liquid Surf. nperature (deg F)		Va	or Pressure (p	sia)	Vapor Mol.	Liquid Mass	Vapor Mass	Mal.	Basis for Vapor Pressure
xdure/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Welght	Celculations
eneric Additive	Jan	44.31	41.43	47.20	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1; VP40 = .38 VP50 = .36
meric Additive	Feb	45.17	41.85	48.49	53.22	0.3600	0.3600	0,3600	120.0000			1,410.00	Option 1: VP40 = .36 VP60 = .36
eneric Additive	Mar	48.86	45.12	52,60	53.22	0.3500	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .38 VP50 = .38
neric Additive	Apr	63.89	49.28	58.51	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VPS0 = .36 VP60 = .36
eneric Additive	May	58.34	53.45	63.23	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP50 = .36 VP60 = .36
meric Additive	Jun	62.56	57.55	67.57	53.22	0.3800	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP78 = .36
eneric Additive	Jul	65.18	60.26	70.09	53.22	0.3600	0.3600	0.3500	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
eneric Additive	Aug	64.49	59.83	69.14	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
eneric Additive	Sep	61.09	56,69	65.49	53.22	0.3500	0.3600	0.3500	120,0000			1,410.00	Option 1: VP60 = .36 VP70 = .36
neric Additive	Oct	56.03	52.02	60.04	53.22	0.3600	0.3600	0.3500	120.0000	•		1,410.00	Option 1: VP50 = .36 VP60 = .36
eneric Additive	Nov	51.02	47.86	54.17	53.22	0.3800	0.3600	0.3600	120.0000			1,410.00	Option 1; VP50 = .36 VP60 = .36
nenc Additive	Dec	46.12	43.39	48.86	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP40 = .36 VP50 = .36

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK054 - Horizontal Tank Brooklyn, NY

				·								
Month:	January	February	March	April	May	June	July	August	September	October	Movember	December
Standing Losses (lb):	1,9290	2.0584	2.5808	3.1095	3,3694	3.2900	3,2933	3.1079	2.8623	2.7142	2.0206	1.7964
Vapor Space Volume (cu fi):	448.2272	448.2272	448.2272	448.2272	448.2272	448.2272	448.2272	448.2272	448.2272	448.2272	448.2272	448.2272
Vapor Density (lb/cu ft):	0.0080	0.0080	0.0079	8.0078	0.0078	0.0077	0.0077	0.0077	0.0077	0.0078	0.0079	0.0080
Vepor Space Expansion Factor:	0.0187	0.0221	0.0253	0.0318	0.0336	0.0342	0.0333	0.0313	0.0296	0.0269	0.0205	0.0175
Vented Vapor Saturation Factor:	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291
Tank Vapor Space Volume:												
Vapor Space Volume (cu fi):	448,2272	448,2272	448.2272	448.2272	448,2272	448.2272	448,2272	448.2272	448.2272	448.2272	448.2272	448,2272
Tank Diameter (ft):	8,0000	8.0000	8.0000	8,0000	8.0000	8.0000	8.0000	8.0000	8,0000	6.0000	9,0000	.8,0000
Effective Diameter (ft):	11.9447	11,9447	11.9447	11.9447	11.9447	11,9447	11,9447	11.9447	11.9447	11.9447	11,9447	11.9447
Vapor Space Outage (ff):	4,0090	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4,0000	4.0009	4.0000	4,0000	4.0000
Tank Shell Length (tt):	14.0000	14.0000	14.0000	14.0000	14.0000	14.0000	14.0000	14.0000	14.0000	14.0000	14.0000	14.0000
/apor Density												
Vapor Density (lb/cu ft):	0.0080	0,0080	0.0079	0.0078	0.0078	0.0077	0.0077	0.0077	0.0077	0.0078	0.0079	0808.0
Vapor Molecular Weight (Ib/lb-mole):	120,0000	120.0000	120.0000	120,0000	120.0000	120.0000	120.0000	120,0000	120.0000	120,0000	120.0000	120,0000
Vapor Pressure at Dally Average Liquid		•										
Suriace Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600
Daily Avg. Liquid Surface Temp. (deg. R):	503,9812	504,8409	508.5307	513,5620	518.0109	522,2313	524.8471	524.1592	520.7602	515.6984	510.6956	505.7950
Daily Average Ambient Temp. (deg. F):	31,3000	32,5000	39.9000	50,3000	59,7000	68.9500	74,9500	74,0000	67.2000	56,7000	46,4000	35.7000
Ideal Gas Constant R												
(psia cuft/ (lb-mol-deg R));	10,731	10,731	10.731	10,731	10.731	10,731	10,731	10.731	10.731	10,731	10.731	10.731
Liquid Bulk Temperature (deg. R):	\$12,8900	512.8900	512.8900	512,8900	512.8900	512,8900	512.8900	512,8900	512.8900	512,8900	512.8900	512,8900
Tank Paint Solar Absorptiones (Shell):	0,1700	0.1700	0.1700	0,1700	0,1700	0.1700	0,1700	0.1700	0.1700	0,1700	0.1700	0.1700
Daily Total Solar Insulation	8,1700	4,1140	4.1700	V.1100	0.1700	4.1700	,	0.1100	4.1104	011100	0.1100	V.1.7.00
Factor (Blu/sqfi day):	548,0000	795.0DC0	1,118,0000	1,457.0000	1,890.0000	1,802.0000	1,784.0000	1,583.0000	1,280.0000	951.0000	593,0000	457.0000
Vapor Space Expansion Factor												
Vapor Space Expension Factor:	0,0187	0.0221	8.0253	0.0318	0.0336	0,0342	0.0333	0.0313	0.0296	0.6269	0.0205	0.0175
Daily Vapor Temperature Range (deg. R):	11,5365	13,2882	14.9697	18.4653	19.6644	20.0255	19.6518	18.6231	17.6128	16.0468	12.6147	10.9593
Daily Vapor Pressure Range (psia):	0.0000	0.0008	0.0000	0.0000	0.0000	0.0000	0.0000	0,000	0.0000	0.0000	0.0000	0.0000
Breather Vant Press: Setting Range(psia);	0.0300	0.0600	0.0600	0,000,0	0.0500	0.0800	0.0600	0.0000	0.0600	0.0000	0.0600	0.0600
Vapor Pressure at Daily Average Liquid	0.0000	0.0000	0.5000	0,0000	0.000	0.0000	010000	0.0000	0.000	0.000	0.000	0.0000
Surface Temperature (csia):	0.3600	0.3600	0,3600	9,3600	0.3600	0,3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600
Vapor Pressure at Daily Minimum Liquid	0,3000	0.0000	0.0000	0.0000	0.0000	0,0000	0.0000	0.0000	0.000	0.0000	4.0504	515555
Surface Temperature (psia):	0.3800	0,3600	0.3600	0.3600	0.3600	0.3500	0,3690	0.3600	0.3600	0.3600	0.3600	0.3600
	0,3000	0.3000	0.0000	0.000	0.3000	0.5000	0,3000	U.SGDO	0.0000	0.000	0.5000	0.5050
Vapor Pressure al Daily Maximum Liquid	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	9.3690	0:3800	0.3600	0.3690	0.3600
Surface Temperature (psia):	503,9812	504:8409	508.5307	513.5620	518.0109	522.2313	524,8471	524.1592	520.7 6 02	515.6984	510,6856	505.7950
Dally Avg. Liquid Surface Temp. (deg R):	503,9812 501,0970	504.5409 501.5188	504.7883	508.9481	513.1198	517.2249	519.9342	519,5034	516,3570	511.6867	507.5319	503.0551
Daily Min. Liquid Surface Temp. (deg R):			512.2731	518.1758	522,9020	527.237 7	529.7601	528.8149	525.1 6 34	519,7101	513.8393	508,5348
Daily Max. Liquid Surface Temp. (deg R);	596.8653	508.1629 13.2000	13,4000	16,0000	16.0000	15,9000	15.5000	15,4000	16.0000	16.0000	13.6000	12,2000
Daily Ambient Temp, Range (deg. R):	12,4000	13,2000	13,4000	16,0000	10,000	10.8000	10.0080	19/4000	10.0000	10.0000	13.0000	12,2000
/ented Vepor Saturation Factor	0.0001	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291	0.9291
Vented Vapor Saturation Factor.	0.9291	0.9291	0.9281	0.9291	0.9291	0.929 (0.8291	0.9291	0.8291	0.3231	0,029;	0.0281
Vapor Pressure at Daily Average Liquid:			0.000	0.0000	0.0400	0.3600	0.3600	0,3600	0.3600	0.3600	0.3600	0,3600
Surface Temperature (psla):	0,3600	0.3800	0.3600	0.3600	0.3600		4.0000	4.0000	4.0000	4.0000	4.0000	4.0000
Vapor Space Outege (fi):	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000
n. Hardana ma	4 4000	4 4000	4 4014	1 0047	0.0545	1.0749	1.0151	0.9425	0.9187	0.9515	0.8518	0.9272
Norking Losses (Ib):	1.1909	1.1602	1,1841	1.0647	0.8545		1.0151			120,0000	120.0000	120,0000
Vapor Molecular Weight (lb/tb-mole):	120.0000	120.0000	120.0000	120.0000	120,0000	120.0000	120,0000	120.0000	120.0000	120.0000	120.0000	120,0000
Vapor Pressure at Daily Average Liquid		0.0000	0.0000	0.0000	0.000	0.0000	0.000	0.000	0.0000	0.0000	0.000	6.0000
Surface Temperature (psia):	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600	0.3600
Net Throughput (gal/mo.):	1,157.8000	1,128,0000	1,151.2000	1,035.1000	830,8000	1,044.9000	986,9000	918.300D	893.2000	925.1000	828.1000	931.4000
Annual Turnovers:	2.8093	2.8093	2.8093	2.8093	2.8093	2.8093	2.8093	2.8093	2.8093	2,8093	2.8093	2.8093
Turnover Factor:	1.0000	1.0000	1.0000	1,0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0003	1.0000
		E 0000	8.0000	8.0000	0.0000	8.0000	8.0000	8,0000	8,0000	9.0000	0.000	8,0000
Tank Diameter (ft):	8.0000 1.0000	8.0000 1.0000	1,0000	1,0000	8.0000 1.0000	1,6000	1.0000	1.0000	1,0000	1.0000	8.0000 1.0000	1.0000

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Total Losses (lb):	3.1199	3.2186	3.7649	4.1742	4.2240	4.3648	4.3084	4.0504	3.7811	2.6657	2.8724	2.7236
	1.0						4.3084		 " .			
Marine Carlos (Marine) (1995) 1987 - Marine Marine (1995) 1987 - Marine (1995)						ŕ	• • • •		, '		* * .	
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TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK054 - Horizontal Tank Brooklyn, NY

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Generic Additive	12.14	32.13	44.27

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: Çîty:

State:

Company: SHELL OIL COMPANY - BROOKLYN Horizontal Tank

BK055

Brooklyn

New York

Type of Tank:

Description:

Tank Dimensions

Shell Length (ft): 27.83 Diameter (ft): 8.00 Volume (gallons): 10,466.00 Turnovers: 1.00 Net Throughput(gal/yr): 10.421.00 Is Tank Heated (v/n): И

is Tank Underground (v/n): N

Paint Characteristics

Shell Color/Shade: White/White Shell Condition Good

Breather Vent Settings

Vacuum Settings (psig): -0.03 Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Almospheric Pressure = 14.7 psla)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK055 - Horizontal Tank Brooklyn, New York

			Daily Liquid Surf Imperature (deg		Liquid Bulk Temp	Va	por Pressure (p	sia}	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure
fixture/Component	Month	Avg.	Min	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Weight	Calculations
Vistillate fuel oil no. 2	Jan	44.31	41.43	47.20	53.22	0.0037	0.0033	0.0041	130.0000			188.00	Option 1: VP40 = ,0031 VP50 = .0045
distillate fuel oil no. 2	Feb	45.17	41.85	48.49	53.22	0.0038	0.0034	0.0043	130.0000			188,00	Option 1: VP40 = .0031 VP50 = .0045
Nstillate fuel oil no. 2	Mar	48.86	45.12	52.60	53.22	0.0043	0.0038	0.0053	130,0000			188.00	Option 1: VP40 = .0031 VP50 = .0045
istitate fuel oil no. 2	Apr	53.89	49.28	58.51	53.22	0.0056	0.0044	0.0070	130.0000			188,00	Option 1: VP50 = .0045 VP60 = .0074
istilate fuel oil no. 2	May	58.34	53.45	63.23	53.22	0.0069	0.0055	0.0079	130,0000			188.00	Option 1: VP50 = .9045 VP69 = .9074
istillate fuel oil no. 2	Jun	62.56	57.55	67.57	53.22	0.0078	0.0067	0.0086	130.0000			188.00	Option 1; VP60 = ,0074 VP70 = .009
istillate fuel oil no. 2	Jul	65.18	60.26	. 70.09	53.22	0.0082	0.0074	0.0090	130.0000			188.00	Option 1; VP60 = .0074 VP70 = .009
ristillate fuel oil no. 2	Aug	64.49	59.83	69.14	53.22	0.0081	0.0074	0.0089	130.0000			188.00	Option 1: VP60 = .0074 VP70 = .009
istilale fuel oil no. 2	Sep	61.09	56,69	65.49	63.22	0.0076	0.0964	0.0083	130.0000			188.00	Option 1: VP60 = .0074 VP70 = .009
istilitate fuel oil no. 2	Oct	56.03	52.02	60.04	53.22	0.0062	0.0051	0.0074	130.0000			188.00	Option 1: VP60 = .0045 VP60 = .0074
itstillate fuel oil no. 2	Nov	51.02	47.86	54.17	53.22	0.0048	0.0042	0.0057	130.0000			188.00	Option 1: VP50 = .0045 VP60 = .0074
istillate fuel oil no. 2	Dec	46.12	43,39	48.86	53.22	0.0040	0.0036	0.0043	130.0000			188.00	Option 1: VP40 = .0031 VP50 = .0045

Jan Grand Garage (1987)

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK055 - Horizontal Tank Brooklyn, New York

												
ndh:	January	February	March	April	May	June	July	August	September	October	November	Decen
nding Losses (ib):	0.0463	0.0510	0.0726	0.1135	0.1511	9.1663	0.1753	0.1632	0.1404	0.1101	0.0629	0.0
apor Space Volume (cu fl):	891,0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891,0117	891.0
apor Density (lb/cu fi):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0
apor Space Expansion Factor:	0,0189	0.0223	0.0255	0.0320	0.0338	0.0344	0.0335	0.0315	0.0299	0.0272	0.0207	0.0
ented Vapor Saturation Factor:	0.9992	0.9992	0.9991	0.9958	0.9985	0.9983	0.9983	0.9983	0.9984	0.9987	0.9990	9.0
nk Vapor Space Volume:	004 84 AM	004 0447	904 0449	004 0447	004.0447	*****	504 5447	404 0447	****	po.1 e.4 e	001.011.0	891.0
apor Space Volume (cu ft):	891,0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	891.0117	
ank Diameter (R):	8.0000	8.0000	0000.8	8,0000	8.0000	8,0000	8.0000	8.0000	8.0000	8.0000	8.0000	8.
flective Diameter (fl):	16.8410	16.8410 4.0000	16.8410 4.0000	16.8410	16.8410	16.8410	16.8410	16.8410	16.8410	16.8410	16.8410 4.0000	16. 4.
apor Space Oulage (ft):	4.0000 27.8300	4.0000 27.8300	4.0000 27.8300	4.0000 27.8300	4.0000 27.8300	4.0000 27.8300	4.0000 27.8300	4.0000 27.6300	4.0000 27.8300	4.0000 27.8300	4.0000 27.8309	4. 27.
ank Shell Length (ft):	27.0000	21,0300	27.0300	27.0300	21,2300	21.0386	27.0300	21.0300	27.0300	27.0300	27.0300	21.
oor Density apor Density (#b/cu ft):	0.0001	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0002	0.0001	8,0001	0.
apor Molecular Weight (IbAb-mole):	130,0000	130.0000	130,0000	130,0000	130,0000	130,0000	130.0000	130,0000	130.0000	130,0000	130,0000	130.
apor Pressure at Daily Average Liquid								***************************************				
Surface Temperature (osta):	0.0037	0.0038	0.0643	8.0056	0.0069	0.0078	0.0082	0.0081	0.0076	0.0062	0.8048	Ò
ally Avg. Liquid Surface Temp. (deg. R):	503.9812	504.8409	508.5307	513,5620	518.0109	522.2313	524.8471	524.1592	520,7602	515,6984	510.6856	505.
aily Average Amblent Temp. (deg. F): eal Gas Constant R	31.3000	32.5000	39.9000	50,3000	59.7000	68.9500	74.9500	74.0000	67.2000	56.7000	46.4000	35
(psia cuft / (lb-mol-deg R)):	10.731	10.731·	10.731	10.731	10.731	10,731	10.731	10.731	10.731	10.731	10,731	1
quid Bulk Temperature (deg. R):	512.8900	512,8900	512,8900	512,8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900	512.8900	512
ank Paint Solar Absorptance (Shell);	8.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0.1700	0
illy Total Solar Insulation Factor (Btu/soft day):	548.0000	795.0000	1,118,0000	1,457.0000	1,690.00D0	1,802,0000	1,784,0000	1,583,0000	1,280,0000	951.0000	593,0000	457
or Space Expansion Factor						,	,					
on Space Expansion Factor.	0.0189	0.0223	0.0255	0.0320	0.0338	0.0344	0.0335	0.0315	0,0299	0.0272	0.0207	0
ajur Space Expansion Pacies. ally Vapor Temperature Range (deg. R):	11,5365	13.2882	14.9697	18.4553	19,5644	20.0255	19.6518	18.6231	17.6128	16.0488	12.6147	10
ny vapor remperature range (ceg. rk): nily Vapor Pressure Range (csia):	0.0008	0.0009	0.0014	0.0026	0.0024	0.0019	0.0016	0.0015	0.0018	0.0023	0.0015	
any vapor Pressore Range (psia): eather Vent Press. Setting Range(psia):	0.0600	0.0600	0.0600	0.0600	0.0600	0.0600	0.0800	0.0600	0.0600	0.0600	0.0500	Ċ
eamer vent Press. Sesing Kangelpsia). ipor Pressure at Dally Average Liquid	0,000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.000	0.0000	0.0000	0.0000	,
Surface Temperatura (paía):	0.0037	0.0038	0.0043	0.0056	0.0069	0.0078	0.0082	0.0081	0.0076	0.0062	0.0048	0
orace remperature (pass). por Pressure et Dally Minimum Liquid	0.003)	0.0030	0.0043	0.0000	0.0008	0.0010	0.0002	0.0001	0.0076	0.0002	0.0040	U
por Pressure en Dany Winnimum Liquid Surface Temperature (osia):	0.0833	8.0034	0.0038	0.0044	0.0056	0.0067	0.0074	0.0074	0.0084	0.0051	0.0042	
surrace remperature (psia): apor Pressure at Daily Maximum Liquid	0.0000	0,0034	0.0030	0.0044	0.0000	0.0007	0,0014	0.0014	0.0004	1 600,0	0.0042	
	0.0041	0.0043	0.0053	0.0070	0.0079	0.0086	0.0090	0.0089	0.0083	0.0074	0.0057	C
Surface Temperature (psia); ilv Avg. Liguid Surface Temp. (deg R);	503.9812	504.8409	508.5307	513,5620	518.0109	522,2313	524.8471	524.1592	520.7602	515.6984	510.6856	505
	501.0970	501.5188	504,7883	508.9481	513.1198	517.2249	519.9342	519.5034	518.3570	511.6867	507.5319	503
aily Min. Liquid Surface Temp. (deg R); ally Max. Liquid Surface Temp. (deg R);	506,8653	508.1629	512,2731	518.1758	522,9020	527.2377	529,7601	528,8149	525,1634	519.7101	513,8393	508
aly Max. Exquite Surface Ferrip. (deg. R): ally Ambient Temp. Range (deg. R):	12.4000	13.2000	13,4000	16.0000	16.0000	15.9000	15,5000	15,4000	16,0000	16.0000	13.6000	12
ed Vapor Salvration Factor												
nted Vapor Saturation Factor: por Pressure at Daily Average Liquid;	0,9992	0.9992	0.9991	0.9988	0.9985	0.9983	0.9983	0.9983	0.9984	0.9987	0.9990	ı
Surface Temperature (psia):	0.0037	0.0038	0.0043	0.0056	0.0069	0.0078	0.0082	0.0081	0.0076	0,0062	0.0048	0
por Space Culage (ft):	4.0000	4.0000	4.0000	4.0000	4.0000	4.0000	4,0000	4.0000	4.0000	4.0000	4.0090	4
• •				•								
ring Losses (lb);	0.0273	0.0310	0.0396	0.0397	0.0042	0.0003	0.0000	0.0090	0.0000	0.0000	0.0000	0
por Molecular Weight (Ib/Ib-mole):	130,0000	130,0000	130.0000	130,0000	130.0000	130.0000	130.0000	130.0000	130.0000	130,0000	130.0000	130
por Pressure at Daily Average Liquid												
Surface Temperature (psia):	0.0037	0.0038	0.0043	0.0056	0.0069	0.0078	0.0082	0.0081	0.0076	0.0062	0.0048	C
t Throughput (gal/rao.):	2,351.0000	2,615.0000	2,946.0000	2,281.0000	198.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	٥
nual Tumovers:	0.9957	0.9957	0.9957	0.9957	0.9957	0.9957	0.9967	0.9957	0.9957	0.9957	0.9957	6
mover Factor:	1.0000	1.0000	1.0000	1.0000	1.0000	1,0000	1.0000	1.0000	1.0000	1.0000	1.0000	1
	8,0000	8.0000	8.0000	8,0000	8,0000	8,0006	8.0000	8,0000	8.0000	8.0090	8.0000	8.
ink Dlameter (ft):	0,000	0.0000	0,000	0,0000	0,0000	0,000	0.0000	0.0000	0.0000	8.0000	0.0000	

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TANKS 4,0 Report

Total Losses (lb):

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

BK055 - Horizontal Tank Brooklyn, New York

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Distilate fuel oil no. 2	0.14	1.30	1.44

TANKS 4.0.9d Emissions Report - Detail Format Total Emissions Summaries - All Tanks in Report

Emissions Report for: January, February, March, April, May, June, July, August, September, October, November, December

ank Identification				Losses (lbs)
K009	SHELL OIL COMPANY - BROOKLYN	Vertical Fixed Roof Tank	Brooklyπ, NY	89.00
K010	SHELL OIL COMPANY - BROOKLYN	Vertical Fixed Roof Tank	Brooklyn, New York	89.00
K041	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	278.42
K042	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	276.99
K043	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	1,440.59
K044	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	1,396.44
K045	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	276.99
K046	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	255.99
K047	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	2,223.53
K048	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	2,223.53
K049	\$HELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	2,421.41
K050	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	2,421.41
K052	SHELL OIL COMPANY - BROOKLYN	Horizonial Tank	Brooklyn, NY	34.58
K053	SHELL OIL COMPANY - BROOKLYN	Horizontal Tank	Brooklyn, NY	0.00
K054	SHELL OIL COMPANY - BROOKLYN	Horizontal Tank	Brooklyn, NY	44.27
K055	SHELL OIL COMPANY - BROOKLYN	Horizontal Tank	Brooklyn, New York	1.44
otal Emissions for all Tanks:				13,473.58

TANKS 4 .9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: City:

State: NY

Company: Type of Tank: SHELL OIL COMPANY - BROOKLYN Vertical Fixed Roof Tank

BK009

Brooklyn

Description:

Tank Dimensions

Shell Height (ft): 16.00 Diameter (ft): 11.00 Liquid Height (ft): 14.00 Ava. Liquid Height (ft): 5.50 Volume (gallons): 8.400.00 Tumovers: 2.81 Net Throughput(gal/yr): 23.598.00

N

Is Tank Heated (v/n):

Paint Characteristics

Shell Color/Shade: White/White Shell Condition Good Roof Color/Shade: White/White Roof Condition: Good

Roof Characteristics

Cone

Type: Height (ft) 0.34 Slope (fl/fl) (Cone Roof) 0.06

Breather Vent Settings

Vacuum Settings (psig): -0.03 Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK009 - Vertical Fixed Roof Tank Brooklyn, NY

Mixture/Component	Month	Avg.	Daily Liquid Surf Temperature (deg Min.		Liquid Bulk Temp (deg F)	Va Avg.	por Pressure (p Min.	osla) Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. W ei ght	Basis for Vapor Pressure Calculations	:	÷.
Generic Additive	Jun	62.56	57.55	67.57	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36		
Generic Additive	Jul	65.18	60.26	70.09	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .36		
Generic Additive	Aug	64.49	59.83	89.14	53.22	0.3600	0.3600	0.3600	120.0000			1,410.00	Option 1: VP60 = .36 VP70 = .38		

Higher.

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK009 - Vertical Fixed Roof Tank Brooklyn, NY

Month:	January	February	March	April	May	June	July	August	September	October	November	Decen
Slanding Losses (lb):						6.6270	6.6337	6.2602				
Vapor Space Volume (cu fl):						1,008.7138	1,008,7138	1,008.7138				
Vapor Density (Ib/cu ft):						0.0077	0.0077	0.0077				
Vapor Space Expansion Factor:						0.0342	0.0333	0.0313				
Vented Vapor Saturation Factor:						0.8316	0.8316	0.8316				
nk Vapor Space Volume:												
unk vapor space volume: Vapor Space Volume (cu ff):						1,008.7138	1,008,7138	1,008.7138				
Tank Diameler (ft):						11.0000	11.0000	11.0000				
/apor Space Outage (ft):						10.6143	10.6143	10.6143				
ank Shell Height (it):						16.0000	16.0000	16,0000				
Average Liquid Height (ft):						5.500D	5,5000	5.5000				
Roof Oulage (fl):						0.1143	0.1143	0.1143				
oof Outage (Cone Roof)												
Roof Oulage (fi):			•			0.1143	0.1143	0.1143				
Roof Height (ft):						0.3430	0.3430	0.3430				
Roof Stope (ft/ff):						0.0624	0.0624	0.0624				
Shell Redius (fi):						5.5000	5,5000	5.5000				
apor Density												
Vapor Density (lb/cu fl):						0.0077	0.0077	0.0077				
Vapor Molecular Weight (Ib/Ib-mole):			•			120,0000	120.0000	120,0000				
Vapor Pressure at Daily Average Liquid												
Surface Temperature (pala):						0.3600	0.3600	0.3800				
Daily Avg. Liquid Surface Temp. (deg. R):						522,2313	524.8471	524.1592				
Daily Average Amblent Temp. (deg. F):						68.9500	74.9500	74.0000				
Ideal Gas Constant R												
(psis cuft / (fb-mof-deg R));						10.731	10.731	10.731				
Liquid Bulk Temperature (deg. R):						512.8900	512.8900	512.8900				
Tank Paint Solar Absorptance (Shelf):						0.1700	0.1700	0.1700				
Tank Paint Solar Absorptance (Roof):						0.1700	0.1700	0.1700				
Daily Total Solar Insulation												
Factor (Blu/sqft day):						1,802.0000	1,784.0000	1,583.0000				
apor Space Expansion Factor					•							
Vapor Space Expansion Factor:						0.0342	0.0333	0.0313				
Daily Vepor Temperature Range (deg. R):						20.0255	19.6518	18.6231				
Daily Vapor Pressure Range (psla):						0.0000	0.0000	0.0000				
Breather Vent Press. Setting Range(psia):						0.0600	0.0600	0.0600.				
Vapor Pressure at Deily Average Liquid						0.0000	0.0000	0.0000				
Surface Temperature (psia):						0.3600	0.3600	0.3600				
Vapor Pressure at Daily Minimum Liquid						0.3600	0.3600	0.2000				
Surface Temperature (pela):						0.3000	0.3000	0.3600				
Vapor Pressure at Daily Maximum Liquid						0.3800	0,3600	0.3800				
Surface Temperature (psia):						622.2313	524.8471	524.1592				
Daily Avg. Liquid Surface Temp. (deg R):						517,2249	519.9342	519.5034				
Daily Min, Liquid Surface Temp. (deg R):						527.2377	529.7601	528.8149				
Daily Max. Liquid Súrface Temp. (deg R): Daily Amblent Temp. Range (deg. R):						15.9000	15,5000	15,4000				
							•					
ented Vapor Saturation Factor Vented Vapor Saturation Factor:						0.8316	0.8316	0.8316				
Vecor Pressure at Dally Average Liquid:												
Surface Temperature (pala);						0.3600	0.3600	0.3600				
Vapor Space Outage (fl):						10.6143	10.6143	10.6143				
arking Losses (Ib):						2.1497	2.0304	1.8854				
Vapor Molecular Weight (lb/lb-mole):						120,0000	120.0000	120,0000				

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Surface Temperature (psia): Net Throughput (gatimo.): Annual Tumovers: Tumover Factor: Maximum Liquid Volume (gal): Maximum Liquid Height (fi): Tank Diameter (fi): Working Loss Product Factor:			·	. •	g gir	0.3600 2,090,0000 2,8093 1,0000 8,400,0000 14,0000 11,0000	0:3600 1,974,0000 2,8093 1,0000 8,400,0000 14,0000 11,0000	0.3600 1,833,0000 2,8093 1,0000 8,400,0000 14,0000 11,0000
Total Losses (lb):						8.7768	8.8641	8.1458
	. •						•	4

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TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK009 - Vertical Fixed Roof Tank Brooklyn, NY

	- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1	Losses(lbs)	AND MANAGEMENT CONTRACTOR OF THE PROPERTY OF T
Components	Working Loss	Breathing Loss	Total Emissions
Generic Additive	6.07	19.52	25.59

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

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Ida	ntifi	 ión

User Identification: BK010
City: Brooklyn
State: New York

Company: SHELL OIL COMPANY - BROOKLYN

Type of Tank: Vertical Fixed Roof Tank

Description:

Tank Dimensions

16.00 Shell Height (ft): Diameter (ft): 11.00 14.00 Liquid Height (ft): Avg. Liquid Height (ft): 5.50 8.400.00 Volume (gallons): 2.81 Turnovers: Net Throughput(gal/yr): 23.598.00 Is Tank Healed (v/n): Ν

Paint Characteristics

Shell Color/Shade: White/White
Shell Condition Good
Roof Color/Shade: White/White
Roof Condition: Good

Roof Characteristics

Type: Cone

Height (ft) 0.00

Slope (ft/ft) (Cone Roof) 0.06

Breather Vent Settings

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

Arriga teace in

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Shell/Motiva 0008299

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK010 - Vertical Fixed Roof Tank Brooklyn, New York

Matura/Component	Month	Avg.	Daily Liquid Surf. Temperature (deg F Min.		Liquid Sulk Temp (deg F)	V. Avg.	apor Pressure (p Min	sia) Max.	Vapor Mol. Weight.	Liquid Mass Fract	Vapor Mass Fract.	Mal. Weight	Basis for Vapor Pressure Calculations	
Generic Additive Generic Additive Generic Additive	jun jul Aug	62.56 65.18 64.49	57.55 60.26 59.83	67.57 70.09 69.14	53.22 53.22 53.22	0.3600 0.3600 0.360D	0.3600 0.3600 0.3600	0.3600 0.3600 0.3600	120.0000 120.0000 120.0000	A		1,410.00 1,410.00 1,410.00	Option 1: VP60 = .96 VP70 = .96 Option 1: VP60 = .36 VP70 = .36 Option 1: VP60 = .36 VP70 = .36	

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TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK010 - Vertical Fixed Roof Tank Brooklyn, New York

onth:	January	February	March	April	May	June	July	August	Seplember	October	November	Dece
- All Annual Control of the Control						0.007	C 0000	å non s		***************************************		
ding Losses (lb):						6.6272	6.6338	6.2604				
oor Space Volume (cu ff):						1,008.7376	1,009.7376	1,008.7378				
por Density (Ib/ou ft):						0.0077	8.0077	0.0077				
por Space Expansion Factor:						0.0342	0.0333	0,0313				
nted Vapor Saturation Factor.						0.8316	0.8316	0.8316				
Vapor Space Volume:									•			
oor Space Volume (cu ft):						1,008.7376	1,008.7376	1,008.7376				
nk Diameter (f1):					-	11.0000	11.0000	11.0000				
or Space Outage (fi):						10.6146	10.6146	10.6146				
ık Shell Height (ft):						16.0000	16,0000	16.0000				
erage Liquid Height (ft):						5.5090	5.5000	5.5000				
of Outage (ft):						0,1146	0.1146	0.1146				
f Outage (Cone Roof)												
oof Outage (ff):						0.1146	0.1145	0.1146				
of Height (fl):						0.0000	0.0000	0.0000				
of Slope (fl/ft);						0.0625	0.0625	0.0625				
eli Radius (ft):						5,5000	5.5000	5.5000				
or Density												
por Density (lb/cu ft):						0.0077	0.0077	0.0077				
nor Molecular Weight (Ib/Ib-mole):	•					120.0000	120,0000	120.0000				
or Pressure at Daily Average Liquid												
Surface Temperature (pola):						0.3600	0.3600	0.3600				
ly Avg. Liquid Surface Temp. (deg. R):						522.2313	524.8471	524.1592				
ly Average Ambient Temp. (deg. F):						58.9500	74.9500	74.0000				
al Gas Constant R												
(psia cult / (lb-mol-deg RV):						10.731	10.731	10.731				
juld Bulk Temperature (dag. R);						512.8900	512.8900	512,8900				
nk Paint Solar Absorptance (Shell):						0.1700	0.1700	0.1700				
nk Paint Solar Absorptance (Roof):						0.1700	0.1700	0.1700				
ily Total Solar Insulation						5.1100	4.1104	011.00				
Factor (Btu/sqft day):						1,802.0000	1,784.0000	1,583.0000				
x Space Expansion Factor												
por Space Expansion Factor:						0.0342	0.0333	0.0313				
ly Vapor Temperature Range (deg. R):						20.0255	19.6518	18.6231				
ly Vapor Pressure Range (psia):						0.0000	0.000.0	0.0000				
y vapor Pressus Range (psia): pilher Vent Press, Sotting Range(psia):						0.0600	0.0600	0.0000				
por Pressure at Datly Average Liquid						0.0000	0.0000	0.0000				
						0.3800	0.3600	0.3600				
Surface Temperature (psia):						0.3000	0.3000	0.3000				
or Pressure at Daily Minimum Liquid						0.0000	0.3600	0.3600				
Surface Temperature (psia):						0.3600	0.3600	0.3000				
or Pressure at Dally Maximum Liquid							0.0000	0.0000				
iurface Temperature (psia):						0.3690	0.3600	0.3600				
fy Avg. Liquid Surface Temp. (deg R):						522.2313	524.8471	524.1592			·	
y Min, Liquid Surface Temp. (deg R):						517.2249	519.9342	519.5034				
y Max. Liquid Surface Temp. (deg R):	4					527,2377	529.7601	528.8149				
ly Amblent Temp. Range (deg. R):						15,9000	15.5000	15.4000				
d Vapor Saturation Factor				•								
nled Vapor Saturation Factor:						0.8316	0.8316	0.8316				
or Pressure at Daily Average Liquid:						•		_				
Surface Temperature (psia);						0.3600	0.3600	0.3600				
or Space Outage (ft):		•				10.6146	10.8146	10.8146				
ing Losses (b):						2.1497	2.0304	1.8854				
or Molecular Weight (lh/lb-mole):						120.0000	120,0000	120.0000				
KO MICHOLOGIA TROUTA (MAICHINIO)						1201000	,					

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Surface Temperature (psia): Net Throughpul (gelfmo.): Annuet Tumovers: Tumover Factor: Maximum Liquid Volume (gelf): Maximum Liquid Velght (ft): Tank Diameter (ft): Working Loss Product Factor:	erre de experiención y en grante de	ega sa			0,3600 2,690,0000 - 2,8093 1,0000 8,400,0000 14,0000 11,0000 1,0000	0.3800 1,974.0000 2.8093 1.9000 8,400.0000 14.0000 11.0000	0.3600 1,833,0000 2.8093 1.0000 8,400,0000 14,0000 11,0000
Total Losses (lb):					8.7769	8,6642	8.1457
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TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK010 - Vertical Fixed Roof Tank Brooklyn, New York

	The second secon		
Components	Working Loss	Breathing Loss	Total Emissions
Generic Additive	6.07	19.52	25.59

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Steel Arthur Line

Identification

User Identification:

BK041

City:

BROOKLYN

State

N

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank: Description:

Internal Floating Roof Tank

Tank Dimensions

Diameter (ft):

24.00

Volume (gallons):

79.800.00

Tignovers:

97.67

Self Supp. Roof? (y/n):

No. of Columns:

1.00

Eff. Col. Diam. (ft):

1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Shell Color/Shade:

White/White

Shell Condition

Good

Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal." Secondary Seal Mechanical Shoe

Rim-mounted

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Quantity

Ladder Well (36-in, Diam.)/Sliding Cover, Gasketed Automatic Gauge Float Well/Bolted Cover, Gasketed Automatic Gauge Float Well/Unbolled Cover, Gaskeled Column Well (24-in, Diam.)/Pipe Col.-Flex: Fabric Sleeve Seal Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask. Roof Leg or Hanger Well/Adjustable

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK041 - Internal Floating Roof Tank BROOKLYN, NY

Mixture/Component	Month		Deity Liquid Surf. emperature (deg l Min.		Liquid Bulk Temp (deg F)	Vaj Avg.	oor Pressure (p Min.	sia) Max.	Vapor Mol. Weight	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
denatured ethanol denatured ethanol denatured ethanol	 Jul Jul Jun	62.56 65.18 64.49	57.56 60.26 59,83	67.57 70.09 69.14	53.22 53.22 53.22	1.7033 1.8039 1.7770	n/a n/a n/a	n/a n/a n/a	46.67C0 46.07C0 46.07C0			46.07 46.07 46.07	Option 4: RVP=3.5, ASTM Slope=3 Option 4: RVP=3.5, ASTM Slope=3 Option 4: RVP=3.5, ASTM Slope=3

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK041 - Internal Floating Roof Tank BROOKLYN, NY

Monte	January	February	March	April	May	June	July	August	September	October	November	Decen
Rim Seal Losses (lb);						1.7015	1.8088	1.7800				
Seal Factor A (lb-mole/fi-yr):						0.6000	0.6000	0.6000				
Seel Factor B (lb-mole/ff-yr (mph)*n):						0,4000	0.4000	0.4000			•	
Value of Vapor Pressure Function:						0.0308	0.0327	0.0322				
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):						1.7033	1.8039	1.7770				
Tank Diameter (ft):						24.0000	24,0000	24,0000				
Vapor Molecular Weight (Ib/Ib-mole):						46.0700	46.070D	46.0700				
Product Factor:	*					1.0000	1.0000	1.0000				
Rhdrawal Losses (lh);						6.5113	6.1378	5.6668				
Number of Columns:						1.0000	1,0000	1.0000				
Effective Column Diameter (ft):						1.0000	1,0000	1.0000				
Net Throughput (gal/mo.):					673	3,901.8000	635,239.8000	586,493.8000				
Shell Clingage Factor (bb/1000 soft):						0.0015	0.0015	8,0015				
Average Organic Liquid Density (b/gall):						6.6100	6.6100	6,6100				
Tank Diameler (fl):						24.0000	24.0000	24.0000				
ck Filling Losses (ib):						18.3860	19.5452	19.2341				
afue of Vapor Pressure Function:						0.0308	0.0327	0.0322				
Vapor Molecular Weight (Ib/Ib-mole):						46.0700	46.0700	46,0700				
Product Factor:						1.0000	1.0000	1.0000				
Tol. Roof Filling Loss Fact (ib-moletyr);						155,6000	155.6000	155.8000				
ock Seam Losses (b):						0.0000	0.0000	0.0000				
Deck Seam Length (ft): Deck Seam Loss per Unit Length						0.0000	0.0000	0.0000				
Factor (Ib-mole/fI-yr):						0.0000	0.0000	0.0000				
Deck Seam Length Factor((Vsqft):						0.0000	0.0000	0.0000				
Tank Diameter (#):						24.0000	24.0000	24.0000				
Vapor Molecular Weight (Ib/Ib-mole):						46.0700	46.0709	48.0700				
Product Factor:						1,0000	1.0000	1.0000				
ofal Losses (lb):						26.5988	27.4918	26.6809				
							Roof Filling Loss Faci	tors			······································	
nof Fitting/Status				Quantity	KFa(Ib-	-moleryr)	KFb(lb-mole/(yr		m		Losses(lb)	
edder Well (36-in. Dam.)/Sliding Cover, Gasketed				1		56.00		0.00	0.00		20.7506	
ulomatic Gauge Floet Wel/Bottled Cover, Gasketed				i		2.89		0.00	0.00		1:0375	
nomatic Gauge Float Well/Unbolted Cover, Gasketed				1		4.30		17.00	0.38		1.5934	
dumm Well (24-in. Diam.)/Pipe ColRex. Fabric Sleeve Seal				Ì		10.00		.0.00	0.00		3.7055	
ample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask				1		43.00		0.00	0.00		15.9335	
of Leg or Hanger Well/Adjustable				5		7.90		0.00	0.00		14.5366	

Service of the

Line Higgs year .

Shell/Motiva 0008308

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK041 - Internal Floating Roof Tank BROOKLYN, NY

h(file.)		7 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	Losses(lbs)		
Components	Rim Seal Loss	.Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
denatured ethanol	5.29	18.32	57.17	0.00	

TANKS 4.0.9d

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

Identification

User Identification: City:

BK042 BROOKLYN

NY

State: Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank: Description:

Internal Floating Roof Tank

Tank Dimensions

Diameter (ft): Volume (gallons): Turnovers: Self Supp. Roof? (y/n): No. of Columns:

24.00 79.800.00

97.67

Ν

1.00 1.00

Eff. Col. Diam. (ft): **Paint Characteristics**

> Internal Shell Condition: Shell Color/Shade: Shell Condition Roof Color/Shade:

Light Rust White/White Good

White/White

Good

Roof Condition: Rim-Seal System

Primary Seal: Secondary Seal Mechanical Shoe Rim-mounted

Deck Characteristics

Deck Fitting Category: Deck Type:

Detail Welded

Deck Fitting/Status

Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed Access Hatch (24-in, Diam, //Bolted Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Well (24-in. Diam.)/Pipe Col.-Flex. Fabric Sleeve Seal Sample Pipe or Well (24-in. Dlam.)/Slotted Pipe-Sliding Cover, Gask. Roof Leg or Hanger Well/Adjustable

Quantity

Meterological Data used in Emissions Calculations; JFK Int'l Airport, New York (Avg Almospheric Pressure = 14.7 psla)

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TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK042 - Internal Floating Roof Tank BROOKLYN, NY

Micture/Component (**/****)		Temp		Liquid Daily Liquid Surf. Bulk Temperature (deg F) Temp		Vapor Pressure (psia)			Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Besis for Vapor Pressuro	
• • •	Month	Avg.	Min.	Mex.	(deg F)	Avg.	Min.	Мах.	Weight.	Fract.	Fract.	Weight	Calculations	
denatured athanol	Jun	62.56	57.55	67.57	53,22	1.7033	N/A	N/A	46.0700			46.07 ·	Option 4: RVP=3.5, ASTM Slope=3	
denatured ethanol	Jul	65.18	60.26	70.09	53.22	1.8039	N/A	N/A	46.0700			46,07	Option 4: RVP=3.5, ASTM Slope=3	•
denatured ethenol	Aug	64.49	59,83	69,14	53.22	1.7770	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3	1

Survival and are

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK042 - Internal Floating Roof Tank BROOKLYN, NY

San Factor (Month:	January	February	March	April	May	June	July	August	September	October	November	Decemi
Seal Factor (i)	Rim Seal Losses (Ib):					·····							
Value of Vagor Princenson Functions:													
Vispon Freedom as Daily Averages Lacid Surface Temporary Lacid Surface Temporary Lacid Surface Temporary Lacid Surface Temporary Lacid L													
Surface Tempore Duming (mails) 1,7000							0,0308	0.0327	0.0322				
Vapor Medicalish Weight (Erb-mole): 46.0770 45.0700 69.0700 Frobust Factor 1.0000							1,7033	1.8039	1.7770				
Froduct Feder													
Wilhibrared Lasses (fb):													
Number of Columents 1,0000	Product Factor;						1,0000	1.0009	1.0000				
Effection Column Claimeter (T):	Withdrawal Losses (lb):												
Net Timusipant (galimo): 673,007,000 683,238,600 564,468,600 561,6													
Shell Crizgage Fador (pict/1000 sq)); 0.0015													
Average Organic Uquid Dessity (Bigsi):								635,239,8000				•	
Tank Diameler (19): Deck Filting Lasses (16): 18,2442 19,3845 19,8895 19,8895 Value of Vapor Pressure Function: 0,0398 0,0327 0,0327 Vapor Money Law Weight (Infline Incidence) 46,0700 46,0700 46,0700 Vapor Money Law Weight (Infline Incidence) 46,0700 46,0700 46,0700 Vapor Money Law Weight (Infline Incidence) 1,0000 1,0000 1,0000 Deck Saem Lasses (Ib): 0,0000 0,0000 0,0000 Deck Saem Lasses (Ib): 0,0000 Deck Saem Lasses (Ib)			•										
Value of Vapor Pressure Function: 0,0308 0,1327 0,1932 0,1832 0													
Value of Vapor Pressure Function: 0.0308 0.1327 0.1322 0.1322 Vapor Molecular Welight (high-male): 46.0700 46.0700 46.0700 46.0700 1.0000 1.0	Punk Citing I neepe Ah)						18 2442	19.3945	19 0858			•	
Vapor Molecular Weight (hith-mole):													
Tot. Roof Fitting Loss Fad.(b-mole/ry):							46.0700		46.0700	•			
Deck Seam Losses (fb):					•								
Deck Seam Length (fit)	Tot. Roof Fitting Loss Fact (b-mole/yr):						154 <i>A</i> 000	154,4000	154.4000				
Deck Seam Loss per Unit Length Factor (In-model*)-yr): 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.00000 0.00000 0.00000 0.0000 0.00000 0.00000 0.0000 0.0000 0.0000 0.0000	Deck Seam Losses (lb):						0.0000		0.0000				
Factor (1b-mole/fl-yr)							0.0000	0.0000	0.0000				
Deck Seam Length Factor (11/4 or 11/4						0.000	4 0000	0.000					
Tank Diameter (ft):													
Vapor Molecular (Veight (full-mole): Product Factor: 46.0700 1.0000 1.0000 1.0000 48.0700 1.0000 1.0000 Total Losses (fb): 26.4570 27.3410 26.5326 26.5326 Roof Fitting/Status Quentity KFa(b-mole/yr) KFa(b-mole/yr) KFa(b-mole/yr) (KFa(b-mole/yr) MFa(b-mole/yr) (KFa(b-mole/yr)) mm Losses(fb) Ladder Well (38-in. Diam./JSiting Cover, Gasketed 1 55.00 0.00 0.00 0.00 0.00 0.5929 Actomatic Gauge Float Well/Unbothed Cover, Gasketed 1 1.60 0.00 0.00 0.00 0.5929 Actomatic Gauge Float Well/Unbothed Cover, Gasketed 1 4.30 17.00 0.38 1.9924 Column/Pype ColFlex. Fabric Steeve Steel Coturn Well (24-in. Diam.//Pype ColFlex. Fabric Steeve Steel 1 0.00 0.00 0.00 0.00 0.00 3.7055			*								•		
Product Factor: 1,000 1													
Total Losses (fb): 26.4570 27.3410 26.5326	Product Factor.						1.0000	1.0000	1.0000				
Total Losses (iii)	No. 1	•					5			4.4			
Roof Fitting/Status Roof Fitting Loss Factors Roof F		•					26 4570	27 3/10	26 5326	124 - 2	:		
Roof Filting/Status Quantity KFa(lb-mole/yr) KFa(lb-mole/yrmph*n) m Losses(lb)	tora coases (m).				·					424	.: .		
Ladder Well (36-in, Diam, lyStiding Cover, Gasketed 1 55.00 0.00 0.00 20.7508 Access Hatch (24-in, Diam, lyStiding Cover, Gasketed 1 1.60 0.00 0.00 0.5929 Automatic George Float Well/Umbodied Cover, Gasketed 1 4.30 17.00 0.38 1.9894 Column Well (24-in, Diam, l/Fjoe ColFlox, Fabric Steeve Seal 1 10.00 0.00 0.00 3.7055	,	*			÷			Roof Fitting Loss Fac	tors				
Access Haich (24-In. Diam.)/Rolled Cover, Gasketed 1 1.60 0.00 0.00 0.5928 Automatic Gauge Float Wet/Unbodied Cover, Gasketed 1 4.30 17.00 0.38 1.5934 Column Wet [24-in. Diam.)/Pipe Col-Flex. Fabric Steeve Seal 1 10.00 0.00 0.00 3.7055	Roof Fitting/Status	. ,		:	Quantity	**	KFa(lb-mole/yr)	K/Fb(lb-mole/(y	rmph'n))	m		Losses(lb)	
Access Hatch (74-In. Diam.)/Boiled Cover, Gasketed 1 1.60 0.00 0.00 0.5928 Automatic Gauge Float Well/Unbolled Cover, Gasketed 1 4.30 17.00 0.38 1.5934 Column Well (24-In. Diam.)/Pipe ColFlex. Fabric Steeve Seal 1 10.00 0.00 0.00 3.7055	Ladder Wall (18. in Diam Visiting Cover Gaskeled		<u> </u>		1		58.00		0.00	0.00		20.7506	
Automatic Gauge Float Well/Unbolled Cover, Gasketed 1 4.30 17.00 0.38 1.5934 Column Well (24-in, Diam.) (Pipe ColFlex, Fabric Steeve Seal 1.000 0.00 0.00 3.7055					i		1.60		0.00	0.00		0.5929	
Octobil treat least a particular five over a particular and advant a con-	Automatic Gauge Float Well/Unbolled Cover, Gasketed				1		4.30						
Sample Pine or Well (24-In, Diam,)/Stolled Pine-Silding Cover, Gask. 1 43.00 0.00 0.00 15.9335	Column Well (24-in. Diam.)/Pipe ColFlex. Fabric Sleeve Seal				1								
Roof Leg or Hanger Well/Adjustable 5 7.90 0.00 0.00 14.6366					1								

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TANKS 4.0 Report

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK042 - Internal Floating Roof Tank BROOKLYN, NY

		The second secon	Losses(lbs)		
Components	Rim Seal Loss	Withdrawi Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
denatured ethanol	5.29	18.32	56.72	0.00	80.33

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification:

BK043

Citv: State: BROOKLYN

Company:

SHELL OIL COMPANY - BROOKLYN

Internal Floating Roof Tank

Type of Tank:

Description:

Tank Dimensions

Diameter (ft):

43.00

Volume (gallons):

79.800.00

Turnovers:

Self Supp. Roof? (v/n):

236.46

No. of Columns:

1.00

Eff. Col. Diam. (ff):

1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Shell Color/Shade:

White/White

Shell Condition

Good

Roof Color/Shade:

Roof Condition:

White/White Good

Rim-Seal System

Primary Seal: Secondary Seal Mechanical Shoe

Rim-mounted

Deck Characteristics

Deck Fitting Category:

Deck Type:

Detail Welded

Deck Fitting/Status

Quantity

Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed Access Hatch (24-in, Diam.)/Bulted Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Well (24-in, Diam,\/Pipe Col.-Flex, Fabric Sleeve Seal Sample Pipe or Well (24-in, Diam.)/Slotted Pipe-Stiding Cover, Gask. Roof Leg or Hanger Well/Adjustable

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK043 - Internal Floating Roof Tank BROOKLYN, NY

Mixture/Component	Month		Daily Liquid Surf. Temperature (deg l Min.		Liquid Bulk Temp (deg F)	Vaj Avg.	oor Pressure (p Min.	sia) Max.	Vøper Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Star Gasoline (RVP 8.1) Star Gasoline (RVP 8.1) Star Gasoline (RVP 8.1)	Jun Jul Aug	62.56 65.18 64.49	57.55 60.26 59.83	67.57 70.09 69.14	53.22 53.22 53.22	4.3143 4.5422 4.4814	nva nva nva	n/a n/a n/a	68.0000 68.0000 66.0000			66.00 66.00 66.00	Opion 4: RVP=8.1, ASTM Sbpe=3 Opion 4: RVP=8.1, ASTM Sbpe=3 Opion 4: RVP=8.1, ASTM Sbpe=3

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all endings of displaces the property of

And Control of the Section of the Se

BK043 - Internal Floating Roof Tank BROOKLYN, NY

Nonth:	January	February	March	April	May J	une July	August	September	October	November	Dece
im Seal Losses (lb):		·			12,2						
Seal Factor A (lb-mote/fi-yr):					0.0						
Seal Factor B (lb-mole/fl-yr (mph)^n):					0,4						
/alue of Vapor Pressure Function:					0.0	386 0.0921	0.0907				
/apor Pressure at Daily Average Liquid											
Surface Temperature (psia):					4.3						
Fank Diameter (ft):					43.0						
/apor Molecular Weight (Ib/Ib-mole):					66.0						
Product Factor:					1.0	000 1.0000	1.0000				
thdrawal (.osses (lb):					6.7						
lumber of Columns:					1.0						
ffective Column Diameler (fi):					1,0						
Net Throughput (gal/mo.):					1,670,203.3						
Shell Clingage Factor (bbl/1000 sqft);					0.0						
Average Organic Liquid Density (Ib/gal):					5.0						
Fank Diameter (ft):					43.0	000 43,0000	43.0000				
ck Fitting Losses (lb):					73.5		76.9875				
/elue of Vapor Pressure Function:					0.0		0.0907				
/aper Molecular Weight (lb/lb-mole):					66.0						
Product Factor:					1.0						
fot, Roof Fitting Loss Fact.(lb-mole/yr):					154.4	000 154.4000	154,4000				
ck Seam Losses (b): 11					0.0						
eck Seam Length (ft):					0.0	0.0000	0.0000				
eck Seam Loss per Unit Length											
Factor (lb-mole/ft-yr):					0.0		0000.0				
eck Seam Length Factor(ft/sqft);					0.0		0.0000				
ank Diameter (ft):					43.0		43,0000				
/apor Molecular Weight (lb/lb-mole):					66.0						
Product Factor.					1.0	1,000	1,0000				
alai Losses (lb):					92.5	21 97.6253	95.6196				
						Roof Fitting Loss	actors				
oof Filting/Status				Quantity	KFa(ib-mole/y) KFb(lb-mok	/(yrmph^n))	m		Losses(fb)	
dder We'il (36-in, Diam, J/Sikfing Cover, Gasketed			<u> </u>	1	58.0	0	0.00	0.00		83,7004	
cess Hatch (24-in, Diam.)/Bulled Cover, Gasketed				i	1.6		0.00	0.00		2.3914	
Iomatic Gauge Float Well/Unbolted Cover, Gasketed				i	4.3		17.00	0.38		6.4270	
lumn Well (24-in. Diam.)/Pipe ColFlex. Fabric Sleeve Sest				i	10.0		0.00	0.00		14.9465	
mple Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.		•		1	43.0		0.00	0.00		64.27CD	
of Lea or Hanger Well/Adjustable				Ė	7.9		0.00	0.00		59.0387	

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK043 - Internal Floating Roof Tank BROOKLYN, NY

Line Alleria

49%	Losses(lbs)									
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions					
Star Gasoline (RVP 8.1)	38.23	18.79	228.80	0.00	285.83					

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

Quantity

		4.5		45	
ıđ	en	TITI	ca	tion	ľ

User Identification: City: BK044 BROOKLYN

State:

Company: Type of Tank: Description: SHELL OIL COMPANY - BROOKLYN

Internal Floating Roof Tank

Tank Dimensions

Diameter (ft):
Votume (gallons):
Turnovers:
Set Supp. Roof? (v/n):

24.00 79.800.00

236.46

Self Supp. Roof? (y/n): No. of Columns:

1.00 1.00

Paint Characteristics

Eff. Col. Diam. (ft):

Internal Shell Condition: Shell Color/Shade: Shell Condition Roof Color/Shade: Light Rust White/White Good White/White Good

N

Rim-Seal System

Roof Condition:

Primary Seal: Secondary Seal Mechanical Shoe Rim-mounted

Deck Characteristics

Deck Fitting Category: Deck Type: Detail Welded

Deck Fitting/Status

Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed
Access Hatch (24-in. Diam.)/Bölted Cover, Gasketed
Automatic Gauge Float Well/Unbolted Cover, Gasketed
Column Well (24-in. Diam.)/Pipe Col.-Flex. Fabric Sleeve Seal
Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.
Roof Leg or Hanger Well/Adjustable

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK044 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surt emperature (deg		Liquid Bulk Temp	Vaj	por Pressure (ps	ia}	Vapor Mot.	Liquid Mass	Vapor Mass	Mol	Basis for Vapor Pressure
Mixture/Component (#15%);	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight	Fract.	Fract.	Welghi	Calculations
Star Gasoline (RVP 8.1)	lun	62,56	57.55	87.57	53.22	4.3143	N/A	N/A	66,0000	*		66.00	Option 4: RVP=8.1, ASTM Slope=3
Ster Gasoline (RVP 6.1)	Jun Jul	65,18	60.26	70.09	53.22	4.5422	N/A	N/A	66,0000			66.00	Option 4: RVP=8.1, ASTM Stope=3
Star Gasoline (RVP 8.1)	Aug	64.49	59.83	69.14	53.22	4.4814	N/A	N/A	68.0000			66.00	Option 4: RVP=8.1, ASTM Stope=3

PROSESSION OF THE PROSESSION FOR THE

BK044 - Internal Floating Roof Tank BROOKLYN, NY

onlin:	January	February	March	April	May	June	July	August	September	October	November	Decem
im Seal Losses (ib):						6.8617	7.2974	7,1802				
Seal Factor A (ib-mole/ft-yr):						0.6000	0.6000	0.6000				
Seal Factor 8 (lb-moterff-yr (mph)*n):						0.4000	0.4000	0.4000				
Value of Vapor Pressure Function: Vapor Pressure at Daily Average Liquid						0.0866	0,0921	0.0907				
Surface Temperature (osial):						4.3143	4,5422	4,4814				
Tank Diameter (ft):						24.0000	24,0000	24.0000				
Vapor Molecular Weight (Itv/ib-mole);						66.0000	66.0000	68.0000				
Product Factor:						1.0000	1,0000	1.0000				
findrawal Losses (ib):						12.2485	11.5014	10.5197				
Number of Columns:						1.0000	1,0000	1.0000				
Effective Column Diameter (#);						1,0000	1.0000	1.0000				
Net Throughput (gal/mo.):						1,670,203.3000	1,568,328,0000	1,434,455.7000				
Shell Clingage Factor (bbY1000 sqft): Average Organic Liquid Density (lb/gal);						0.0015 5.0170	0.0015 5.0170	0.0015 5.0170				
Average Organic Exquid Desisity (lovgae); Tank Diameter (ft):						24.0000	24.0000	24,0000				
ck Fitting Losses (lb):						73.5727	78.2447	76.9875				
falue of Vapor Pressure Function:						0.0866	0.0921	0.0907				
/apor Molecular Weight (lb/lb-mole): Product Factor:						66.0000 1.0000	66.0000	66.0000 1.0000				
roduct Factor: Fot. Roof Filling Loss Fact.(Ib-mole/yr):						154,4000	1,0000 . 154,4000	.154.4000				
*												
ck Seam Losses (lb):						0.0000	0.0000	0.0000				
Deck Seam Length (#):						0.0000	0.0000	0.0000				
Deck Seam Loss per Unit Length Factor (Ib-mole/fi-yr):						0.0000	0.0000	0.000.0				
Pack Seam Length Factor(ft/soft):						0.0000	0.0000	0.000.0				
Tank Diameter (it):						24.0000	24.0000	24.0000				
Vapor Molecular Weight (lb/lb-mole);						66.0000	66,0000	0000.66				
Product Factor:						1.0000	1.0000	1.0000				
•		•			4.5				• .			
otal Losses (lb):	·.	•				92,6829	97.0436	94.6873			·.	
			····									
oof Fitting/Status				Quantity	٠.	KFa(ib-mole/yr)	Roof Fitting Loss Fac KFb(lb-mole/(y	iors raiph^n))		m	Losses(lb)	
				·					· · · · ·			
sdder Well (36-in. Diam.)/Sliding Cover, Gasketed				1		56,00		0.00	0.0		83.7004	
coss Halch (24-in. Diam.)/Bolled Cover, Gasketed				1		1.60 4.30		0.00 17.00	0.0		2.3914 6.4270	
utomatic Gauge Float Well/Unbolted Cover, Gasketed olumn Well (24-in. Diam.)/Pipe ColFlex. Fabric Steeve Seat				1		10.00	• •	17.00 0.00	· · 0.0		6.4270 14.9465	
olumn well (24-in. Diam.)/Pipe CotPiex. Fabric Steeve Sea: ample Pipe or Well (24-in. Diam.)/Stoffed Pipe-Stidling Cover, Gask.				1		43.00		0.00	0.0 0.0		14.9465 64.2700	
emple ripe or vieu (24-in. biain.ys.oned ripe-skoing cover, sask. oof Leg or Hanger Well/Adjustable						40.00		2,00	0.0		59.0387	

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK044 - Internal Floating Roof Tank BROOKLYN, NY

	Losses(lbs)											
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions							
Star Gasoline (RVP 8.1)	21.34	34.27	228.80	0.00	284.41							

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification:

BK045

City: State: Brooklyn Ny

Company: Type of Tank: SHELL OIL COMPANY - BROOKLYN
Internal Floating Roof Tank

of Tank:

Description:

Tank Dimensions

Diameter (ft): Volume (gallons): 24.00 79.800.00

Turnovers:

97.67

Self Supp. Roof? (y/n):

\$1.01

No. of Columns: Eff. Col. Diam. (ft): 1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Shell Color/Shade: Shell Condition White/White Good

Roof Color/Shade:

White/White

Roof Condition:

Good

N

Rim-Seal System

Primary Seal: Secondary Seal

Mechanical Shoe

Rim-mounted

Deck Characteristics

Deck Fitting Category:

Deck Type:

Detail Welded

Deck Fitting/Status

1 1 1 1

Quantity

Ladder Well (36-in. Diam.)/Silding Cover, Gasketed Access Hatch (24-in. Diam.)/Boiled Cover, Gasketed

Automatic Gauge Float Well/Unbolled Cover, Gasketed Column Well (24-in. Diam.)/Pipe Col.-Flex: Fabric Sleeve Seal

Roof Leg or Hanger Well/Adjustable

Sample Pipe or Well (24-in. Diam.)/Stotted Pipe-Stiding Cover, Gask.

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Almospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK045 - Internal Floating Roof Tank BROOKLYN, NY

		Te	Daily Liquid Surf emperature (deg	: F)	Liquid Bulk Temp	Vay	por Pressure (p	sla)	Vapor Mol.	Liquid Mass	Vepor Mass	Mas.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract	Weight	Calculations
denatured estanos	Jun	62.56	57.55	67.57	53.22	1,7033	N/A	N/A	46,0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
denatured efnano!	juž	65,18	69.26	70.09	53.22	1.8039	N/A	N/A	46.0700			46,07	Option 4: RVP=3.5, ASTM Slope=3
denatured ethanol	Aug	64.49	59.83	69.14	53.22	1.7770	N/A	N/A	48.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3

BK045 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	Merch	April	May	enul	. July	August	September	Oclober	November	Decen
Rim Seal Losses (ib):			· · · · · · · · · · · · · · · · · · ·			1.7015	1.8088	1.7800				
Seal Factor A (Ib-mole/fl-yr):						0.6000	0,5000	0.6000				
Seal Factor B (lb-mote/fl-yr (mph)*n):						0.40 90 0.0308	0.4000 0.0327	0.4000 0.0322				
Value of Vapor Pressure Function:						0,0308	0.0327	0.0322				
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):						1,7033	1.6039	1,7770				
Sungos remperature (para): Fank Diameter (ft):						24,0000	24.0009	24.0000				
/apor Molecular Weight (Ib/Ib-mole):						46,0700	46.0700	46.0700				
Product Factor:						1,0000	1.0000	1.0000				
Uktrawal Losses (b);						6.5113	6.1378	5,6668				
Number of Columns:						1.0000	1,0000	1.0000				
Effective Column Diameter (ft):						1.0000	1,0000	1.0000				
Vel Throughpul (gal/mo.);					673	3,901.8000	635,239.8000	586,493.8000				
Shell Clingage Factor (bbV1000 sqft):						0.0015	6.0015	0.0015				
Average Organic Liquid Density (In/gal):						8.6100	6,6100 24,0000	6.6100				
Tank Diameter (ff):						24.0000	24,0000	24.0000				
ck Fitting Losses (lb):						18.2442	19.3945	19.0658				
alue of Vapor Pressure Function:						0.0398	0.0327	0.0322				
/apor Molecular Weight (Ib/Ib-mole):						46.0700	46.0700	46.0700				
Product Factor.						1,9000	1,0000	1.0000				
Tot. Roof Filting Loss Fact.(lb-mole/yr):						154,4000	154.4000	154,4000				
ck Seam Losses (lb):						0.0000	0.0008	0.0000				
Deck Seam Length (ft):						0.0000	0.0000	0.0000				
leck Seam Loss per Unit Length												
Factor (lb-mole/ft-yr):						0.0000 0.0000	0.0000	0.0000				
leck Seam Length Factor(ft/sqff):						24,0000	24.0000	24,0000		-		
'ank Diameter (ft): 'apor Molecular Weight (ib/lb-mole):						46,0760	46.0700	46.0700				
rapor woxacular vivagin (uno-more). Product Factor:						1.0900	1.0000	1.0000				
ioua racio.						1.0000	1.0000					
otal Losses (lb):	,					26.4570	27.3410	26,5326				
		<u></u>	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	······································			Roof Filling Loss Fact	ors				
oof Filling/Status				Quantity	KFa(lb-	-mote/yr)	KFb(lb-mole/(yr		m		Losses(lb)	
adder Well (36-in. Diam.)/Sliding Cover, Gasketed				1		56.00		0.00	0.00		20.7506	
cess Hatch (24-in, Diam.)/Bolted Cover, Gasketed		•		i		1.60		0.00	0.00		0.5929	
iomatic Gauge Float Well/Unboiled Cover, Gasketed				i		4.30		17.00	0.38		1.5934	
Numn Well (24-in, Diam.)/Pipe ColFlex. Fabric Steeve Seal				1		10.00		0.00	0.00		3.7055	
of Leg or Hanger Well/Adjustable				5		7.90		0.00	0.00		14.6366	
mole Pipe or Well (24-in. Diam.)/Slotted Pipe-Stiding Cover, Gask.				1		43.00		0.00	0.00		15,9335	

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK045 - Internal Floating Roof Tank BROOKLYN, NY

1830		The state of the s	Losses(lbs)		
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
denatured ethanol	5.29	18.32	56.72	0.00	80.33

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

		_		
7.4	enfi	-	-46	~ "

User Identification: City:

BK046 BROOKLYN

State: Company: NY

Type of Tank:

SHELL OIL COMPANY - BROOKLYN Internal Floating Roof Tank

Description:

Tank Dimensions

Diameter (ft): Volume (gallons):

46.00 79.800.00

Turnovers:

Self Supp. Roof? (v/n):

97.67

No. of Columns: Eff. Col. Diam. (ft): 1.00 1.00

Paint Characteristics Internal Shell Condition: Shell Color/Shade:

Light Rust White/White Good

N

Shell Condition Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal: Secondary Seal Mechanical Shoe Rim-mounted

Deck Characteristics

Deck Fitting Category: Deck Type:

Detail Welded

Deck Fitting/Status

Quantity

Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed Access Hatch (24-in, Diam, VBolted Cover, Gasketed Automatic Gauge Float Well/Unbolted Cover, Gasketed Column Well (24-in. Diam.)/Pipe Col.-Flex. Fabric Sleeve Seal Sample Pipe or Well (24-in, Diam.)/Slotted Pipe-Sliding Cover, Gask. Roof Leg or Hanger Well/Adjustable

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

12 m

Shell/Motiva 0008330

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK046 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surf		Liquid Bulk Temp	Vej	or Pressure (s	osia)	Vapor Mol	Liquid Mass	Vapor Mass	¹Mol.	Seels for Vapor Pressure
Mixture/Component () () ()	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract.	Y/eight	Calculations
denatured ethanol	Jun	62.56	57.55	67.57	53.22	1.7033	N/A	NA	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3
denatured ethanol	Jul	65.18	6D.26	70.09	53.22	1.8039	N/A	N/A	46.0700	•		46.07	Option 4: RVP=3.5, ASTM Slope=3
denatured ethanol	Aug	64.49	59.83	69.14	53.22	1,7770	N/A	N/A	46.0700			46.07	Option 4: RVP=3.5, ASTM Slope=3

BK046 - Internal Floating Roof Tank BROOKLYN, NY

vionth:	January	February	March	April	May	June	July	August	September	Oclober	November	Decemb
Rim Seal Losses (Ib):		,		· "-		3.2613	3.4669	3.4117				
Seal Factor A (th-mole/fl-yr):						0.6000	0,6000	0.6000				
Seal Factor B (lb-mole/fl-yr (mph)*n):						0.4900	0.4000	0.4000				
Value of Vapor Pressure Function: Vapor Pressure at Daily Average Liquid						0,0308	0.0327	0.0322				
Surface Temperature (psia):				•		1,7033	1.8039	1.7770				
Tank Diameter (ff):						46.0000	46.0000	46,0000				
Vapor Mojecular Weight (lb/lb-moje);						46.0700	46.0700	46.0700				
Product Factor:						1.0000	1.0000	1.0000				
filhdrawal Losses (lb);						3,3322	3.1411	2.9000				
Number of Columns:						1.0000	1,0000	1.0000				
Effective Column Diameter (ft):						1.0000	1,0000	1.0000				
Net Throughput (gal/mo.):						673,901.8000	635,239.8000	586,493.8000				
Sheli Clingage Factor (bbV1000 sqft):						0.0015	0.0015	0.0015				
Average Organic Liquid Density (Ib/gal);						5.6100	6.6100	6.6100				
Tank Diameter (ff):						46.0000	46.0000	46.0000				
eck Fitting Losses (lb):						18.2442	19,3945	19.0858				
Value of Vapor Pressure Function;						0.0308	0.0327	0.0322				
Vapor Molecular Weight (lb/lb-mole):						46.0700	46.0700	48.0700				
Product Factor: Tot, Roof Fitting Loss Fact.(lb-mole/yr):						1.0000 154.4000	1,0000 154,4000	1.0000 154.4000				
· , , , , , , , , , , , , , , , , , , ,								,				
eck Seam Losses (lb):						0.0000	0.0000	0.0000				
Deck Seam Length (ft):						0.0000	0.0000	0.0000				
Deck Seam Loss per Unit Length						0.0000	0.0000	0.0000				
Factor (lb-mole/fl-yr); Deck Seam Length Factor(fl/sqff);						0.0000 0.0000	0,0000	0000.0 0000.0				
Deck Seam Lengar Factor(10scpt). Tank Diameter (ff):						46,0000	46.0000	48,0000				
Vapor Molecular Weight (lb/lb-mole);						48.0700	46,0700	46.0700				
Product Factor:						1.0000	1.0000	1.0000				
110000							1.0000	110000				
iotal Losses (ib);						24.8377	26.0024	25,3975				
Tank Fifther of Charles				Quantily		KFa(lb-mole/yr)	Roof Fitting Loss Fac KFb(lb-mole/(yr				Losses(lb)	
Roof Fitting/Status	·			Quantity		Kra(ID-IIIUIG)	кгоцо-поведу	притијј		•	rosses(in)	
adder Well (36-In, Dlam.)/Sliding Cover, Gaskeled				1		56.00		0.00	0.00		20.7506	
ccess Hatch (24-in. Diam.)/Bolled Cover, Gasketed				1		1.60		0.00	0.00		0.5929	
utomatic Gauge Float Well/Unbolted Cover, Gasketed				1		4.30		17.00	. 0,38		1.5934	
column Well (24-in, Diam.)/Pipe ColFlex, Fabric Sleeve Seal				1		10.00		0.00	0.00		3.7055	
ample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Gask.				1		43.00		0.00	0.00		15.9335	
oof Leg or Hanger Well/Adjustable				5		7.90		0.00	0.00		14,6386	

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK046 - Internal Floating Roof Tank BROOKLYN, NY

			Losses(lbs)		
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
denatured ethanol	10.14	9,37	56.72	0.00	76.24

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

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Id	on	41	Fi	ca	fi	

User Identification:

BK047

City: State:

BROOKLYN NY

Company:

SHELL OIL COMPANY - BROOKLYN Internal Floating Roof Tank

Type of Tank:

Description:

Tank Dimensions

Diameter (ft):

46.00

Volume (gallons):

373.800.00

Turnovers:

229.97

Self Supp. Roof? (y/n):

No. of Columns:

1,00

Eff. Col. Diam. (ff):

1.00

Paint Characteristics

Internal Shell Condition: Shell Color/Shade:

Liaht Rust

Shell Condition

White/White

Good

Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal: Secondary Seal

Liquid-mounted

None

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Quantity

Roof Leg or Hanger Well/Adjustable Sample Pipe or Well (24-in. Diam.)/Slotted Pipe-Sliding Cover, Ungask. Automatic Gauge Float Well/Unbolted Cover, Gasketed Access Hatch (24-in, Diam.)/Bolted Cover, Gasketed Ladder Well (36-in. Diam.)/Stiding Cover, Gasketed Column Well (24-In. Diam.)/Built-Up Col.-Sliding Cover, Gask.

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK047 - Internal Floating Roof Tank BROOKLYN, NY

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The state of the s

Mbdure/Component	Month		Daily Llquid Surf, Temperature (deg F Min,		Liquid Bulk Temp (deg F)	Va Avg.	por Pressure (p Min.	sia) Max.	Yapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calcurations
Star Gascline (RVP 8.1) Star Gascline (RVP 8.1) Star Gascline (RVP 8.1)	Jun Jul Aug	62,56 65,18 64,49	57.55 60.26 59.83	67.57 70.09 69.14	53.22 53.22 53.22	4.3143 4.5422 4.4814	n/a n/a n/a	N/A N/A N/A	66.0000 66.0000 68.0000			66.00 66.00 66.00	Option 4: RVP=8.1, ASTM Slope=3 Option 4: RVP=8.1, ASTM Slope=3 Option 4: RVP=8.1, ASTM Slope=3

Proposition of the second of t

BK047 - Internal Floating Roof Tank BROOKLYN, NY

								·	-,	·····	
viorith:	January February	March	April	May	June	July	August	September	October	November	Decer
im Seal Losses (lb);					35.0709	37,2980	36.6987				
Seal Factor A (lb-mole/fi-yr):					1.6000	1.6000	1.6000				
Seal Factor B (lb-mole/ft-yr (mph)*n);					0.3000	0.3000	0,3000				
falue of Vapor Pressure Function:		* * * * * * * * * * * * * * * * * * *			0.0866	0.0921	0.0907				
/apor Pressure at Daily Average Liquid											
Surface Temperature (psia):	•				4.3143	4,5422	4.4814			*	
Fank Diemeter (il):					46,0000	46.0000	46.0000				
Vapor Motecutar Weight (It/Ib-mole):					66,0000	66.0000	66,0000				
Product Factor:					1.0000	1,0000	1,0800				
Indrawal Losses (lb):					28.5556	26.8138	24,5250				
vumber of Columns:		•			1.0000	1.0000	1.0000				
Effective Column Diameter (ff);					1.0000	1.0000	1,0000				
Net Throughpul (gal/mo.):					7,608,703.7000	7,144,605.5000	6,534,742.8000				
Shell Clingage Factor (bbl/1000 sqfl);					0.0015	0.0015	0.0015				
Average Organic Liquid Density (ib/gal):					5.0170	5.0170	5.0170				
Tank Diameter (ff):					46,0000	46.0000	46.0000				
ck Fiting Losses (lb):					84.5323	89.9004	88.4558	•			
/alue of Vapor Pressure Function:					0.0866	0.0921	0.0907				
/apor Molecular Weight (Ib/Ib-mole):					66,0000	66.0000	66.0000				
Product Fector:					1.0000	1.0000	1.0000				
ict. Roof Fäting Loss Fact.(ib-mole/yr):					177.4000	177.4000	177.4000				
ck Seam Losses (lb):					0.0000	0.0000	0.0000				
eck Seam Length (ft):					0.0000	0.0000	0.0000				
eck Seam Loss per Unil Length											
Factor (lb-mole/fit-yr):					0.0000	0.0000	0.0009				
eck Seam Length Factor(fl/sqff);					0.0000	0.0000	0.0000				
ank Diameter (ft):					46.0000	46.0000	48.0000				
/apor Molecular Weight (lb/fo-mole):					66.0000	66.0000	68.0000				
Product Fector:					1.0008	1.0000	1.0000				
otal Losses (Ib);					148.1588	154.0122	149.6795				
				•		Roof Fitting Loss Fa					
od Fiting/Status			Quantity		KFa(lb-mole/yr)	KFb(lb-mole/()		m	1	Losses(lb)	
nos Leg or Hanger Well/Adjustable			5		7.90		00.0	0.00)	59.0387	
mple Pipe or Well (24-in, Diam.)/Slotted Pipe-Sliding Cover, Ungask.			1		43.00		00.0	0.00		64:2700	
iomatic Gauge Float Well/Unbolted Cover, Gasketed			1		4.30		17.00	0.35		6.4270	
cess Hatch (24-in. Diam.)/Bolted Cover, Gasketed			1		1.60		00.0	0.00		2.3914	
dder Well (36-in. Diam.)/Silding Cover, Gasketed			1		56.00		0.00	0.00		83.7004	
olumn Well (24-in, Diam.)/Buill-Up ColSliding Cover, Gask.			4		33.00		00.0	0.00		49.3235	

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK047 - Internal Floating Roof Tank BROOKLYN, NY

etal to			Losses(ibs)		
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Star Gasoline (RVP 8.1)	109.07	79.89	262.89	0.00	451.85

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

ld	An	4i	fic	ati	on

User Identification: City: State:

BK048 BROOKLYN

NY

Company: Type of Tank: Description:

SHELL OIL COMPANY - BROOKLYN

Internal Floating Roof Tank

Tank Dimensions

Diameter (ft): Volume (gallons): Turnovers: Self Supp. Roof? (v/n): 46.00

373.800.00 229.97

N

1.00

No. of Columns: Eff. Col. Diam. (ft):

1.00

Paint Characteristics

Internal Shell Condition: Shell Color/Shade: Shell Condition Roof Color/Shade:

Light Rust White/White Good White/White

Roof Condition: Good

Rim-Seal System

Primary Seal: Secondary Seal Liquid-mounted None

Deck Characteristics

Deck Fitting Category:

Detail Welded

Deck Type:

Deck Fitting/Status

Roof Leg or Hanger Well/Adjustable Sample Pipe or Well (24-In. Diam.)/Slotted Pipe-Sliding Cover, Ungask. Column Well (24-in, Diam.)/Built-Up Col.-Sliding Cover, Gask. Automatic Gauge Float Well/Unbolled Cover, Gasketed Access Hatch (24-in, Diam.)/Bolted Cover, Gasketed Ladder Well (36-in. Diam.)/Sliding Cover, Gasketed

Quantity

Meterological Data used in Emissions Calculations: JFK intil Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK048 - Internal Floating Roof Tank BROOKLYN, NY

Mixture/Component ;	Month		Daily Liquid Sur emperature (deg Min.		Liquid Sulk Temp (deg F)	Vaj Avg.	per Pressure (p Min.	sla) Max.	Vapor Mol. Weight.	Liquid Mass Fract	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations	
Siar Gasoline (RVP 8.1)	Jun	62.56	57.55	67.57	53,22	4.3143	N/A	N/A	68.0000		7100	66.00	Option 4: RVP=8.1, ASTM Slope=3	· · · · · · · · · · · · · · · · · · ·
Star Gasoline (RVP 8.1) Star Gasoline (RVP 8.1)	Jul Aug	65.18 64.49	60.26 59.83	70.09 69.14	53.22 53,22	4,5422 4,4814	n/a n/a	N/A N/A	66.0000 ·	-	•	66.00 66.00	Option 4: RVP=8.1, ASTM Slope=3 Option 4: RVP=8.1, ASTM Slope=3	

BK048 - Internal Floating Roof Tank BROOKLYN, NY

Manth:	January	February	March	April	May	June	July	August	September	October	November	Dece
Film Seal Losses (lb):						35.0709	37.2960	36.6967				
Seal Factor A (Ib-mole/ft-yr):						1.6000	1.6000	1.6000				
Seal Factor B (lb-mole/ft-yr (mph)^n):						0.3000	0.3000	0.3000				
Value of Vapor Pressure Function:						0.0866	0.0921	0.0907				
Vapor Pressure at Daily Average Liquid						4.04.00	1 -100	4 404.4				
Surface Temperature (psia): Tank Diameler (ff):						4.3143 46.0000	4.5422 46.0000	4.4814 46.0000				
Vapor Molecular Weight (lb/lb-mole):						66,0000	66,0000	46.0000 68,0000				
Product Factor:						1.0000	1.0000	1,0000				
Product Factor:						1,0000	1.0000	1.0000				
Afithdrawal Losses (lb):						28.5556	26.8138	24,5250	•			
Number of Columns:						1.0000	1.0000	1.0000				
Effective Column Diameter (ft):						1.0000	1,0000	1.0000				
Net Throughput (gal/mo.):						7,608,703.7000	7,144,605.5000	6,634,742.8000				
Shell Clingage Factor (bbV1000 sqfl):						0.0015	0.0015	0.0015				
Average Organic Liquid Density (lb/gal):						5.0170	5.0170	5.0170				
Tank Diameter (ff):						46.0000	46.0000	46.0000				
Deck Filling Losses (lb):						84.5323	89.9004	88.4558				
Value of Vapor Pressure Function:						0.0866	0.0921	0.0907				
Vacor Molecular Weight (Ib/Ib-mole):						68,0000	66,0000	66,0000				
Product Factor:						1.0000	1.0000	1.0000				
Tot. Roof Filting Loss Fact.(lb-mole/yr):						177,4000	177.4000	177,4000				
Tot. Take I king 2003 I kecija motorjij.						17111000	,,,,,,,,,	1111100				
Deck Seam Losses (lb):						0.0000	0.0000	0.0000				
Deck Seam Length (ft):						0.0000	0.0000	0.0000				
Deck Seam Loss per Unit Length												
Factor (th-mole/ft-yr):						0.0000	0.0000	0.0000				
Deck Seam Length Factor(ft/sqft):						0.0000	0.0008	0.0000				
Tank Chameter (ft):						46.0000	46.000D	46,0000				
Vapor Molecular Weight (lb/lb-mole):						66.0000	66.0000	66.0000				
Product Factor:						1.0000	1.0000	1.0000				
• *									•	4.84		
Fotal Losses (lb):		,				148,1588	154.0122	149,6795				
							Roof Filting Loss Fac	- Lune				
Roof Fitting/Status				Quantity	. 1	KFa(8b-mole/yr)	KFb(lb-mole/(y	r mph*n))	-	m	Losses(b)	
							· · · · · · · · · · · · · · · · · · ·					
Roof Leg or Hanger Well/Adjustable				5		7.90		0.00		.00	59.0387	
Sample Pipe or Well (24 In. Dlam.)/Slotted Pipe-Sliding Cover, Ungask.				1		43.00		0.00	0	.00	64.2700	
Column Well (24-in, Diam.)/Buill-Up ColSilding Cover, Gask.				1		33.00		0.00		.00	49.3235	
Automatic Gauge Float Well/Unboiled Cover, Gaskeled				1		4.30		17.00		.38	6.4270	
Access Hatch (24-in. Diam.)/Bolled Cever, Gasketed]		1.60		0.00		.00	2,3914	
adder Well (36-In, Diam.)/Sliding Cover, Gasketed				1		56,00		0.00	Q.	.00	83.7004	

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK048 - Internal Floating Roof Tank BROOKLYN, NY

The state of the s			Losses(lbs)		
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions
Star Gasoline (RVP 8.1)	109.07	79.89	262,89	0.00	451.85

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

Quantity

Identification

User Identification:

BK049

City: State: BROOKLYN

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank:

Description:

Internal Floating Roof Tank

Tank Dimensions

Diameter (ft):

47.00

Volume (gallons):

420,000.00

Turnovers:

84.12

Self Supp. Roof? (y/n):

No. of Columns:

1.00

Eff. Col. Diam. (ft):

1.00

Paint Characteristics

Internal Shell Condition:

Light Rust

Shell Color/Shade:

White/White

Shell Condition

Good

Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seai System

Primary Seal: Secondary Seal Liquid-mounted

None

Deck Characteristics

Deck Fitting Category:

Detail

Deck Type:

Welded

Deck Fitting/Status

Roof Leg or Hanger Well/Adjustable Column Well (24-in, Diam.)/Pipe Col.-Flex, Fabric Sleeve Seal Automatic Gauge Float Well/Unbolted Cover, Ungasketed Access Hatch (24-in, Diam.)/Bolted Cover, Gasketed Ladder Well (36-in, Diam, VSliding Cover, Ungasketed Slotted Guide-Pole/Sample Well/Gask. Sliding Cover, w. Float

Meterological Data used in Emissions Calculations: JFK Intl Alrport, New York (Avg Atmospheric Pressure = 14.7 psla)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK049 - Internal Floating Roof Tank BROOKLYN, NY

Mixture/Companent	 Monito		Delly Liquid Surl emperature (deg Min.		Liquid Bulk Temp (deg F)	Va Avg.	por Pressure (p Mini	sia) Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Star Gasoline (RVP 8.1) Star Gasoline (RVP 8.1) Star Gasoline (RVP 8.1)	Jun Jul Aug	62.56 65.18 64.49	57.55 60.26 59.83	67.57 70.09 69.14	53.22 53.22 53.22	4.3143 4.5422 4.4814	n/a N/a N/a	n/a n/a n/a	66.0000 66.0000 66.0000			66.00 66.00	Option 4: RVP=8.1, ASTM Slope=3 Option 4: RVP=8.1, ASTM Slope=3 Option 4: RVP=8.1, ASTM Slope=3

BK049 - Internal Floating Roof Tank BROOKLYN, NY

Month:	January	February	March	April	May	June	July	August	September	Ociober	November	Decemb
Rim Seal Losses (lb):						35.8333	38.1088	37.4965				
Seal Factor A (fb-mote/ft-yr):						1.6000	1.6000	1.6000				
Seal Factor B (/b-mole/ft-yr (mph)*n):						0.3000	0.3000	0.3000				
Value of Vapor Pressure Function:						9380.0	0.0921	0.0907				
Vapor Pressure at Daily Averege Liquid												
Surface Temperature (psia):						4.3143	4.5422	4.4814				
Tank Diameter (ft):						47.0000	47.0000	47,0000				
Vapor Molecular Weight (lb/lb-mole):						68.0000	66.0000	66.0000				
Product Factor:						1.0000	1.0900	1.0000				
Nithdrawal Losses (lb):						10.5284	10.0802	9.5217				
Number of Columns:						1.0000	1.0000	1.0000				
Effective Column Diameter (ft):						1,0000	1.0000	1.0000				
Net Throughput (gal/mo.):						2,867,612,5000	2,740,080,0000	2,593,403.5000				
Shell Clingage Factor (bbl/1000 sqft):						0.0015	0.0015	0.0015				
Average Organic Liquid Density (lb/gal):						5.0170	5.0170	5.0170				
Tank Diameter (ft):						47.0000	47.0000	47.0000				
eck Fitting Losses (fb):						108.3577	115.2387	113.3870				
Value of Vapor Pressure Function:						0.0866	0.0921	0.0907				
Vapor Molecular Weight (Ib/Ib-mole):						66.0000	66.0000	66.0000				
Product Factor:						1.0000	1,0000	1.0000				
Tot. Roof Fitting Loss Fact.(lb-mole/yr):						227.4000	227.4000	227.4000				
Oeck Seam Losses (Ib):						0.0000	0.0000	0.0000				
Deck Seam Length (ft): Deck Seam Loss per Unit Length		•				0.0003	0.0000	0.0000				
Factor (Ib-mcle/Ti-yr):						0.0000	0.000.0	0.0000				
Deck Seam Length Factor(f/sqft):						0.0000	0.0000	0.0000				
Tank Diameter (ft):						47,9000	47.0000	47.0000				
Vapor Molecular Weight (ib/lb-mole):						66.0000	0000.66	66,000				
Product Factor:						1.0000	1,0000	1.000D				
Total Losses (lb);						154,7194	163.4077	160.4052	_			
-							Roof Filling Loss Factors					
Roof Fitting/Status				Quantily	К	Fa(lb-mole/yr)	KFb(lb-mole/(yr mph*n))		m		Losses(lb)	
Roof Leg or Henger Well/Adjustable				12		7.90		0.00	0.00		141.6929	
Column Well (24-in, Diam.)/Pipe ColFlex, Fabric Sleeve Seel				1		10,00		0.00	0.00		14.9465	
unomatic Gauge Float Well/Unbolted Cover, Ungasketed				i		14.00		5.40	1.10		20.9251	
coss Halch (24-in, Diam.)/Boiled Cover, Gasketed				1		1.60		0.00	0.00		23914	
adder Well (36-in, Diam.)/Sliding Cover, Ungasketed				ì		76,00		0.00	00.0		113.5935	
Hotted Guide-Pole/Samole Well/Gask, Sliding Cover, w. Float				1		31.00		36.00	2.00		48.3342	_

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK049 - Internal Floating Roof Tank BROOKLYN, NY

		Losses(lbs)											
Components	Rim Seal Loss	Withdrawi Loss	Deck Fitling Loss	Deck Seam Loss	Total Emissions								
Star Gasoline (RVP 8.1)	111.44	30.11	336.98	0.00	478.53								

TANKS 4.0.9d

Emissions Report - Detail Format

Tank Indentification and Physical Characteristics

en			

User Identification: BK050
City: BROOKLYN
State: NY

Company: SHELL OIL COMPANY - BROOKLYN

Type of Tank: Internal Floating Roof Tank

Description:

Tank Dimensions

 Diameter (ft):
 47.00

 Volume (gallons):
 424,200.00

 Turnovers:
 83.29

 Self Supp. Roof? (y/n):
 N

 No. of Columns:
 1.00

 Eff. Col. Diam. (ft):
 1.00

Paint Characteristics

Internal Shell Condition:

Shell Color/Shade:

Shell Condition

Good

Roof Color/Shade:

White/White

Roof Condition:

Good

Rim-Seal System

Primary Seal: Liquid-mounted Secondary Seal None

Deck Characteristics

Deck Fitting Category: Detail
Deck Type: Welded

Deck Fitting/Status

Roof Leg or Hanger Well/Adjustable
Column Well (24-in. Diam.)/Pipe Col.-Flex. Fabric Sleeve Seal
Automatic Gauge Float Weil/Unbolted Cover, Ungasketed
Access Hatch (24-in. Diam.)/Bolted Cover, Gasketed
Slotted Guide-Pole/Sample Well/Gask. Sliding Cover, w. Float
Ladder Well (36-in. Diam.)/Sliding Cover, Ungasketed

Quantity

Meterological Data used in Emissions Calculations: JFK Int7 Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

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TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK050 - Internal Floating Roof Tank BROOKLYN, NY

			Daily Liquid Surf		Liquid Bulk Temp	Va	por Pressure (p	sia)	Vapor Mol.	Liquid Mass	Vepor Mass	· Mol.	Básis for Vapor Pressure
Mixture/Component 1999	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Fract.	Fract	Weight	Calculations
Star Gasoline (RVP 8.1)	Jun	62.58	57.55	67.57	53.22	4.3143	N/A	N/A	66.0900			68,00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Jul	65.18	60.26	70.09	53.22	4.5422	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3
Star Gasoline (RVP 8.1)	Aug	64.49	59.83	69.14	53.22	4.4814	N/A	N/A	66.0000			66.00	Option 4: RVP=8.1, ASTM Slope=3

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK050 - Internal Floating Roof Tank BROOKLYN, NY

onth:	January	February	March	April	May	June	July	August	September	October	November	Decen
im Seal Losses (lb):						35,8333	38.1088	37.4985	***************************************			
Seal Factor A (lb-mole/it-yr):						1.6000	1.6000	1.6000				
Seal Factor B (lb-male/ft-yr (mph)^n):						0.3000	0.3000	0.3000				
Vakue of Vapor Pressure Function: Vapor Pressure at Daily Average Liquid						0.0866	0.0921	0.0907				
Surface Temperature (psia):						4.3143	4.5422	4.4814				
Fank Diameter (f1):						47.0000	47.0000	47.0000				
Vapor Molecular Weight (lb/lib-mole):						66,0000	66,0000	66.0000				
Product Factor:						1.0000	1.0000	1.0000			•	
thdrawal Losses (lb):	•					10.5284	10.0602	9.5217				
Number of Columns:						1.0000	1.0000	1.0000				
Effective Column Diameter (ff):						1,0000	1.0000	1.0000				
Net Throughput (gal/mo.): Shell Clingage Factor (bb//1000 soft):			*			2,867,612.5000 0.0015	2,740,080.0000 0.0015	2,593,403.5000				
onea Cangago macaor (obomoco sept): Averago Organic Liquid Donsily (Ib/gat);							5,0170	0.0015 5.0170				
Average Organic ciquid Density (birgar). Tank Diameter (ff):						5,0170 47,0000	47.0000	47.000D				
auk mambri (ii):						41,000	47.03.0	47.0000			*	
k Fitting Losses (Ib):						108,3577	115.2387	113.3870				
alue of Vapor Pressure Function:						0.0866	0.0921	0.0907				
/apor Molecular Weight (lb/lb-mole):						0000.33	66.0000	66.0000				
Product Factor:						1.0000	1.0000	1.0000				
ot. Roof Fitting Loss Fact.(lb-mole/yr):						227.4000	227.4000	227.4000				
ck Seam Losses (b):						0.0000	0.0000	0,0000				
Deck Seam Length (ft): Deck Seam Loss per Unit Length						0.000.0	0.000	0.0000				
· Factor (Ib-mole/fl-yr):						0.0000	0.0000	0,0000				
racior (ib-molentyr); Deck Seam Length Factor(ft/soff);						0.0000	0.0000	0.0000				
rank Diameter (ff):						47.0000	47.0000	47.0000				
apor Molecular Weight (Ib/Ib-mole):						66.0000	68.0000	68.0000				
Product Factor.						1.0000	1.0000	1.0000				
				•		1.0405			•			
tal Losses (lb):					-	154.7194	163.4077	160,4052				
							Roof Fitting Loss Far					
cof Fitting/Status				Quantity		KFa(lb-mole/yr)	KFb(:b-mole/(y	r mpin'n)}	ı,	l 	Losses(lb)	
of Leg or Hanger Well/Adjustable				12		7.90		0.00	0.00)	141.6929	
okumn Well (24-in, Diam.)/Pipe ColRex. Fabric Sleave Seal				1		10,00		0.00	0.00		14.9465	
tomatic Gauge Float Well/Unbolted Cover, Ungasketed				Í		14.00		5.40	1.10		20.9251	
cess Hatch (24-in, Diam.)/Bolled Cover, Gasketed				1		1.60		0.00	0.00		2.3914	
ottad Guide-Pole/Sample Well/Gask, Sliding Cover, w. Float				1		31.00		36.00	2.00		45.3342	
dder Well (36-in, Diam.)/Sliding Cover, Ungasketed				1		76.00		0.00	0.00		113.5935	

TANKS 4.0 Report

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK050 - Internal Floating Roof Tank BROOKLYN, NY

		Losses(lbs)											
Components	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions								
Star Gasoline (RVP 8.1)	111.44	30.11	336.98	0.00	478.53								

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: Cltv:

BK052 Brooklyn

State: NY

Company:

SHELL OIL COMPANY - BROOKLYN

Type of Tank: Description:

Horizonial Tank

Tank Dimensions

Shell Length (ft): Diameter (ft): Volume (gallons): Turnovers:

Net Throughput(gal/yr): Is Tank Heated (y/n):

3.780.00 2.81 10,619.00

18.00

6.00

Is Tank Underground (y/n):

Paint Characteristics

Shell Color/Shade: Shell Condition

White/White

Good

Breather Vent Settings

Vacuum Settings (psig):

-0.03

0.03

Pressure Settings (psig)

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK052 - Horizontal Tank Brooklyn, NY

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and the first property of the control of the

			Daily Liquid Surf. emperature (deg l	F)	Liquid Bulk Temp	Va	por Pressure (j	•	Vapor Mol.	Liquid Mass	Vapor Mass	Mol.	Basis for Vapor Pressure	
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max	Weight.	Fract	Fract.	Weight	Calculations	
Generic Additive	Jun	62.56	57,55	67.57	53.22	0,3600	0.3600	0.3600	120.0300			1,410.00	Option 1: VP60 = .36 VP70 = .36	
Generic Additive Generic Additive	Jul Aug	65.18 64.49	60.26 59.83	70.09 69.14	53.22 53.22	0.3600 0.3600	0.3600 0.3600	0.3600 0.3600	120.0000 120.0000		•	1,410.00 1,410.00	Option 1: VP60 = .36 VP70 = .36 Option 1: VP60 = .36 VP70 = .36	•

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK052 - Horizontal Tank Brooklyn, NY

Month:	January	February	March	April	May	June	July	August	September	October	November	December
Standing Losses (b):						2.4223	2.4248	2.2883				
Vapor Space Volume (cu fi);						324,1643	324,1643	324.1643				
Vapor Density (fb/cu ft):						0.0077	0.0077	0.0077				
Vapor Space Expansion Factor:						0.0342	0.0333	0.0313				
Vented Vacor Saturation Factor:						0.9459	0.9459	0.9459				
vented vapor saturation Factor:						0.9459	0.9459	0.9459				
Tank Vapor Space Volume:												
Vapor Space Volume (cu ft):						324.1843	324.1643	324.1643				
Tank Clameter (ft):						6,0000	6.0000	6,0000	•			
Effective Diameter (II):						11.7294	11.7294	11.7294				
Vapor Space Outage (fi):						3.0000	3.0000	3,0000				
Tank Shell Length (ft):						18,0000	18.0000	18.0000				
Vapor Density Vapor Density (ib/ou ft):				•		0.0077	0.0077	0.0077				
Vapor Molecular Weight (lb/lb-mole):						120,0000	120.0000	120.0000				
Vapor Pressure at Daily Average Liquid						120,0000	120.0000	120,0000		•		
Surface Temperature (osia);						0.3600	0.3600	0.3600				
Daily Avg. Liquid Surface Temp. (deg. R):						522.2313	524.8471	524:1592				
Daily Average Ambient Temp. (deg. F):						68.9500	74.9500	74.0000				
Ideal Gas Constant R												
: (psia cuft / (lb-mol-deg R)):						10.731	10.731	10,731				
Liquid Bulk Temperature (deg. R);						512,8900	512.8900	512.8900				
Tenk Peint Solar Absorptance (Shell):						0.1700	0.1700	0,1700				
Daily Total Solar Insulation												
Factor (Blu/sqft day):						1,802.0000	1,784.0000	1,583.0000				
Vapor Space Expansion Factor												
Vapor Space Expansion Factor:						0.0342	0.0333	9.0313				
Daily Vapor Temperature Range (deg. R):						20.0255	19.6518	18,6231				
Dally Vapor Pressure Range (pala):						0.0000	0.0000	0.0000				
Breather Vent Press. Setting Range(psia):						0.0600	0.0600	0.0600				
Vapor Pressure at Daily Average Liquid												
Surface Temperature (psia):						0.3500	0.3600	0.3600				
Vapor Pressure at Dally Minimum Liquid												
Surface Temperature (psia):						0.3600	0.3600	0.3600				
Vapor Pressure at Daily Maximum Liquid								-				
Surface Temperature (psia):						0.3609	0.3600	0.3600				
Daily Avg. Liquid Surface Temp. (deg R);						522.2313	524.8471	524,1592				
Daily Min, Liquid Surface Temp. (deg R):						517.2249	519.9342	519.5034				
Daily Max. Liquid Surface Temp. (deg R):						52 7 .2377	529.7601	528.8149				
Daily Ambient Temp. Range (deg. R):						15.9000	16.5000	15,4000				
Vented Vapor Saturation Factor Vented Vapor Saturation Factor;						0.9459	0.9459	0.9459				
Vapor Pressure at Daily Average Liquid:						0.0100	VIO 164	0.0100				
Surface Temperature (psia):						0.3500	0.3600	0.3600				
Vapor Space Outage (ft):						3.0000	3,0000	3.0000				
Working Losses (lb):						0.9673	0.9137	0.8482				
Vapor Molecular Weight (Ib/Ib-mole):						120.0000	120,0000	120,0000				
Vapor Pressure at Daily Average Liquid												
Surface Temperature (psia):						D.3600	0.3600	0.3600				
						94D.4000	888.3000	824.6000				
Net Throughput (gal/mo.):												
Annual Turnovers:						2.8093	2.8093	2.8093				
Tumover Factor:						1.0000	1.0000	1.0000				
Tank Diameter (fi):						6.0000	6.0000	6.0000				
Working Loss Product Factor:						1.0000	1.0000	1.0000				

TANKS 4.0 Report

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK052 - Horizontal Tank Brooklyn, NY

	Losses(lbs)											
Components	Working Loss	Breathing Loss	Total Emissions									
Generic Additive	2.73	7.14	9.86									

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Marini Marini

Identification

User Identification: BK053 City: Brooklyn State: NY

Company: SHELL OIL COMPANY - BROOKLYN

Type of Tank: Horizontal Tank

Description:

Tank Dimensions

 Shell Length (ft):
 16.00

 Diameter (ft):
 8.00

 Volume (gallons):
 4,200.00

 Turnovers:
 1.92

 Net Throughput(gal/yr):
 8,050.00

Is Tank Heated (y/n):

Is Tank Underground (y/n):

N

Paint Characteristics

Shell Color/Shade: White/White Shell Condition Good

Breather Vent Settings

Vacuum Settlings (psig): -0.03
Pressure Settlings (psig): 0.03

Meterological Data used in Emissions Calculations; JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK053 - Horizontal Tank Brooklyn, NY

e 10 85 775 ...

Möture/Component	Month		Daily Liquid Surf. emperature (deg Min.		Liquid Sulk Temp (deg F)	Vi Avg.	apor Pressure (p Min.	sia) Max.	Vapor Mol. Weight	Liquid Mass Frect	Vapor Mass Fred.	Mol. Weight	Basis for Vapor Pressure Calculations
Contact Water Contact Water Contact Water	Jun Jul Aug	62.56 65.18 64.49	57.55 60.26 59.83	67.57 70.09 69.14	53.22 53.22 53.22				66,0000 66,0000 66,0000			66.00 86.00 66.00	

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK053 - Horizontal Tank Brooklyn, NY

		,	······································									
confr:	January	February	March	April	May	June	July	August	September	October	November	Cecx
landing Losses (lb):						0.0000	0.0000	0.0000				
Vapor Space Volumié (cu ft):						512.2597	512.2597	612.2597				
Vapor Density (lb/cu fl):						0.0000	0.0000	0.0000				
						0,0343	0.0334	0.0300				
/apor Space Expansion Factor.												
ented Vapor Saturation Factor:						1.0000	1.0000	1:0900				
nk Vapor Space Volume:												
apor Space Volume (cu fl):						512.2597	512.2597	512.2597				
ank Diameler (ft):						8.0000	8.0000	8.0000				
factive Diameter (ft):						12,7694	12.7694	12.7694				
/apor Space Outage (ft):						4.0000	4.0000	4.0000				
ank Shell Length (ft):						16.0000	16.0000	16.0000				
por Density												
Vapor Density (lb/cu fl):						0.0000	0.0000	0.0000				
/apor Molecular Weight (lb/lb-mole):						66.0000	66,0000	66,0000				
apor Pressure at Daily Average Liquid												
Surface Temperature (psia):						0.0000	0.0000	0.0000				
						522.2313	524.8471	524,1592				
Daily Avg. Liquid Surface Temp. (deg. R):												
Paily Average Ambient Temp. (deg, F):						68.9500	74.9500	74,0000				
deal Gas Constant R												
(psia cuft / (fb-mol-deg R)):						10.731	10.731	10.731				
guld Bulk Temperature (deg. R):						512,8900	512.8900	512.8900				
ank Paint Solar Absorptance (Shelf):						0.1700	0.1700	0.1700				
ally Total Solar Insulation												
Factor (Btu/soft day):						1,802.0000	1,784.0000	1,583.0000				
or Space Expansion Factor												
apor Space Expansion Factor						0.0343	0.0334	0.0314				
ally Vapor Temperature Range (deg. R):						20.0255	19.6518	18.6231				
						0.0000	0.000.0	0.0000				
ally Vapor Pressure Range (psla):								0.0600				
reather Vent Press. Setting Range(osia):						0.0600	0.0600	0.0600				
apor Pressure at Dally Average Elquid												
Surface Temperature (psia):						0.0000	0.0008	0.0000				
apor Pressure at Dally Minimum Llouid												
Surface Temperature (psia):						0.0000	0.0000	0000.0				
/apor Pressure at Daily Maximum Liquid												
Surface Temperature (psia):						0.0000	0.0000	0.0000				
ally Avg. Liquid Surface Temp. (deg R);						522.2313	524.8471	524.1592				
tally Min. Liquid Surface Temp. (deg R):						517,2249	519.9342	619.6034				
aily Max, Liquid Surface Temp. (deg R):						527.2377	529,7601	528.6149				
aily Ambient Temp. Range (deg. R):						15.9000	15,5000	15,4000				
nted Vapor Saturation Factor /ented Vapor Saturation Factor:						1.0000	1.0000	1.0000				
/apor Pressure at Dally Average Liquid:						0.0000	0,0000	0.0000				
Surface Temperature (psia):							4.0000	4,0000				
epor Space Outage (fi):						4.0000	4.0000	4,0000				
						0,000	0.0000	0.0000				
king Losses (lb);												
spor Molecular Weight (Ib/Ib-mole):						66.0000	66,0000	66.0000				
apor Pressure at Daily Average Liquid												
Surface Temperature (psia):						0.0000	0.0000	0.0000				
et Throughput (gal/mo.):						670.8333	670.8333	670.8333				
nnual Tumovers:						1.9167	1.9167	1.9167				
						1,0000	1,0000	1.0000				
umover Factor:												
						8.0000	8,0000	8,0000				
ink Diameter (ft): orking Loss Product Factor:						1.0000	1,0000	1.0000				

0,0000

0.0000



TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK053 - Horizontal Tank Brooklyn, NY

	Losses(lbs)											
Components	Working Loss	Breathing Loss	Total Emissions									
Contact Water	0.00	0.00	0,00									

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: City: BK054 Brooklyn

State:

Company: SHELL OIL COMPANY - BROOKLYN

Type of Tank: Description: Herizontal Tank

Tank Dimensions

 Shell Length (ft):
 14.00

 Diameter (ft):
 8.00

 Volume (gallons):
 4,200.00

 Turnovers:
 2.81

 Net Throughput(gal/yr):
 11,799.00

Is Tank Healed (y/n):

Is Tank Underground (y/n):

N

Paint Characteristics

Shell Color/Shade: White/White Shell Condition Good

Breather Vent Settings

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Almospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK054 - Horizontal Tank Brooklyn, NY

Mixture/Component	Month		Daily Liquid Surf emperature (deg Min.		Liquid Bulk Temp (deg F)	Avg.	per Pressure (p Min.	Max.	Vepor Mol. Weight,	Liquid Mess Fract.	Vøpor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations	
Generic Additive Generic Additive Generic Additive	Jun Jul Aug	62.56 65.18 64.49	57.55 60.26 59.83	67.57 70.09 69.14	53.22 53.22 53.22	0.3600 0.3600 0.3600	0.3600 0.3600 0.3600	0.3600 0.3600 0.3600	120,0000 120,0000 120,0000			1,410.00 1,410.00 1,410.00	Option 1: VP60 = .36 VP70 = .36 Option 1: VP60 = .36 VP70 = .36 Option 1: VP60 = .36 VP70 = .36	

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK054 - Horizontal Tank Brooklyn, NY

fonth:	January	February	March	linqA	May	June	July	August	September	October	November	Dece
anding Losses (lb):						3.2900	3.2933	3.1079				
/apor Space Volume (cu ft);						448.2272	448.2272	448.2272				
Vapor Density (lb/cu ft):						0.0077	0.0077	0.0077				
Vapor Space Expansion Factor:						0.0342	0.0333	0.0313				
Vented Vapor Saturation Factor:						0.9291	0.9291	0,9291				
ank Vapor Space Volume:												
Vapor Space Volume (cu fl):						448 2272	448,2272	448.2272				
Tank Diameter (ft):						8.0000	8.0000	8.0000				
Effective Diameter (ft):						11.9447	11.9447	11.9447				
Vapor Space Outage (ft):						4.0000	4.0000	4.0000				
Tank Shall Length (ii):						14.0000	14.0000	14.0000				
apor Density		-										
Vapor Density (lb/cu ft):						0.0077	0.0077	0.0077				
Vapor Molecular Weight (lb/lb-mole):						120.0000	120.0000	120,0000				
Vapor Pressure at Daily Average Liquid												
Surface Temperature (psia):						0.3600	0.3600	0.3600				
Daily Avg, Liquid Surface Temp. (deg. R):						522.2313	524.8471	524.1592				
Daily Average Ambient Temp. (deg. F):						68.9500	74.9500	74,0000				
Ideal Gas Constant R						00.5000	(7.0000	742000				
						40 704	40 704	46 704				
(psla cuft / (lh-mol-deg R)):						10.731	10.731	10.731				
Liquid Bulk Temperature (deg. R):						512,8900	512.8900	512.8900				
Tank Paint Solar Absorptance (Shell):						0.1700	0.1709	0.1700				
Daily Total Solar Insulation												
Factor (Blu/sqft day):						1,802.0000	1,784.0000	1,583.0000				
apor Space Expansion Factor												
Vapor Space Expansion Factor:						0.0342	0.0333	0,0313				
Daily Vapor Temperature Range (deg. R):						20.0255	19.6518	18.6231				
Dally Vapor Pressure Range (psia):						0.0000	0.0000	0.0000				
Breather Vent Press. Setting Range(psia):						0.0600	0.0600	. 0.0600				
Vapor Pressure at Daily Average Liquid						0.5050		. 0.0000				
Surface Temperature (psia):						0.3600	0.3600	0.3600				
Vapor Pressure at Dally Minimum Liquid						02000	0.5000	0.0000				
						0.3600	0.3600	0,3600				
Surface Temperature (psia):						0.4800	0.3000	0,3000				
Vapor Pressure at Daily Maximum Liquid												
Surface Temperature (psia):						0.3600	0.3600	0.3600				
Daily Avg. Liquid Surface Temp. (deg R);						622.2313	524.8471	524.1592				
Dally Min. Liquid Surface Temp. (deg R):						517.2249	519.9342	619.5034				
Daily Max. Liquid Surface Temp. (deg R):						527 2377	529.7601	528.8149	•		•	
Daily Ambient Temp. Range (deg. R):						15.9000	15.5000	15.4000				
enled Vapor Saluration Factor	,											
Vented Vapor Saturation Factor:						0.9291	0.9291	0.9291				
Vapor Pressure at Daily Average Liquid:												
Surface Temperature (psia):						0.3600	0.3600	0.3600				
Vapor Space Outage (it);						4.0000	4.0000	4.0000	•			
forking Lossea (lb):						1.0748	1,0151	0.9426				
Vapor Molecular Weight (Ib/Ib-mole):						120.0000	120,0000	120.0000				
Vapor Pressure at Dally Average Liquid												
Surface Temperature (pale);						0.3600	0.3600	0.3600				
Vel Throughpul (gal/mo.):						1,044.9000	986,9000	916,3000				
							2.8093	2.8093				
Annual Turnovers:						2.8093						
Tumover Factor:						1.0000	1.0000	1.0000				
Tank Diameter (#):						8.0000	8.0000	8.0000				
Norking Loss Product Factor:						1.0000	1.0000	1.0000				

And the second section of

Total Losses (lb):		4.3648	4.3084	4.0504
produces				# A.
		. ::	:	
er taget		<i>:</i> .		
		211.1 1.10		
SAN CONTRACTOR			profitti	

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TANKS 4.0 Report

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK054 - Horizontal Tank Brooklyn, NY

A CONTRACTOR OF THE PROPERTY O		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Generic Additive	3.03	9.69	12.72

TANKS 4.0.9d

Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification

User Identification: BK055
City: Brooklyn
State: New York

Company: SHELL OIL COMPANY - BROOKLYN

Type of Tank: Horizontal Tank

Description:

Tank Dimensions

 Shell Length (ft):
 27.83

 Dlamefer (ft):
 8.00

 Volume (gallons):
 10,466.00

 Turnovers:
 1.00

 Net Throughput(gallyr):
 10,421.00

Is Tank Heated (y/n):
Is Tank Underground (y/n):

N

Paint Characteristics

Shell Color/Shade: White/White Shell Condition Good

Breather Vent Settings

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: JFK Int'l Airport, New York (Avg Atmospheric Pressure = 14.7 psia)

TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

BK055 - Horizontal Tank Brooklyn, New York

 Müxture/Component	Month		Daily Liquid Surf. emperature (degl Min.		Liquid Bulk Temp (deg F)	Va Avg.	por Pressure (p Min.	sia) Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract,	Mol. Welght	Basis for Vapor Pressure Celculations
Distilate fuel oil no. 2 Distilate fuel oil no. 2 Distilate fuel oil no. 2	Jan Jal Aug	62.56 65.18 64.49	57,55 60,26 59,83	67.57 70.09 69.14	53,22 53,22 53,22	0.0078 0.0082 0.0081	0.0067 0.0074 0.0074	0.0086 0.0090 0.0089	130,0000 130,0000 130,0000			188.00 188.00 188.00	Option 1: VP60 = .0074 VP70 = .009 Option 1: VP60 = .0074 VP70 = .009 Option 1: VP60 = .0074 VP70 = .009

TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

BK055 - Horizontal Tank Brooklyn, New York

fonth:	January	February	March	FinqA	May	June	July	August	September	Ociober	November	Decem
tending Losses (ib);				,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		0.1663	0.1753	0.1632				
Vapor Space Volume (cu ft):						891,0117	891,0117	891.0117				
Vapor Density (It/cu ft):						0.0002	0.0002	0.0002				
Vapor Space Expansion Factor:						0.0344	0.0335	0.0315				
Vented Vapor Saturation Factor:						0.9983	0.9983	0.9963				
ank Vapor Space Volume:												
Vepor Space Volume (cu ff):						691.0117	891.0117	891.0117				
Tank Diameter (ft):						8.0000	8.0000	8.0000				
Effective Diameter (ft):						18.8410	16.8410	16.8410				
Vapor Space Outage (ft):						4.0000	4,0000	4.0000				
Tank Shell Length (#):						27.8308	27.8300	27,6300				
epor Densily												
Vapor Density (lb/cu fl):						0.0002	0.0002	0.0002				
Vapor Molecular Weight (IMb-mole):						130,0000	130.0000	130.0000				
Vapor Pressure at Dally Average Liquid												
Surface Temperature (psia):						0.0078	0.0082	0.0081				
Daily Avg. Liquid Surface Temp, (deg. R):						522.2313	524,8471	524.1592				
						68.9500	74.9500	74.0000				
Daily Average Ambient Temp. (deg. F):						00.8300	74.9000	74,000				
Ideal Gas Constant R							40 ***4	40.704				
(psia cuft / (b-mol-deg R)):						10.731	10,731	10.731				
Liquid Bulk Temperature (deg. R):						512.8900	512.8900	512.8900				
Tank Paint Solar Absorptance (Shell):						0,1700	0.1700	0.1700				
Dally Total Solar Insulation												
Factor (Btw/sqft day):						1,802.0000	1,784.0000	1,583,0000				
apor Space Expansion Factor												
Vapor Space Expansion Factor:						0.0344	0.0335	0.0315				
Daily Vapor Temperature Range (deg. R):						20.0255	19.6518	18.8231				
Dally Vapor Pressure Range (psia);						0.0019	0.0016	0.0015				
Breather Vent Press, Setting Range(psia):						0,0600	0.080.0	0.0800				
Vapor Pressure at Dally Average Liquid												
Surface Temperature (pala):						0,0078	8.0082	0.0081				
Vapor Pressure at Daily Minimum Liquid						0,00.0	0.000	0.000				
Surface Temperature (psia);						0.0067	0.0074	0.0074				
Vapor Pressure at Daily Maximum Liquid						0.2221	2.0011					
Surface Temperature (psia):						0.0086	0.0090	0.0089				
Daily Avg, Liquid Surface Temp. (deg R):						522,2313	524.8471	524.1592				
						517 2249	519.9342	519.5034				
Daily Min. Liquid Surface Temp. (deg R):						627.2377	529.7601	528.8149				
Daily Max. Liquid Surface Temp. (deg R):												
Daily Ambient Temp. Range (deg. R):						15,9000	15,5000	15.40DO				
ented Vapor Saturation Factor						0.0000	ള ഹാരം	0.9983				
Vented Vapor Saturation Factor: Vapor Pressure at Daily Average Liquid;						0.9963	0.9983					
Surface Temperature (psia):						0.0078	0.0082	0.0081				
Vepor Space Outage (ft):						4.0000	4.0000	4,0000				
crking Losses (b):						0,0000	0.0000	0.0000				
Vapor Molecular Weight (fb/lb-mole):						130,0000	130,0000	130.0000				
Vapor Pressure at Daily Average Liquid												
Surface Temperature (psia):						0.0078	0.0082	0.0081				
Net Throughput (gal/mo.):						0.0000	0.0000	0.0003				
Annual Turnovers:						0.9957	0.9957	0.9957				
Tumover Factor:						1,0000	1.0000	1.0000				
Tank Diameter (fi):						8,0000	8.0000	8.0000				
rank Diameter (n): Working Less Product Factor:						1,0000	1.0000	1.0000				

TANKS 4.0 Report

TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

Emissions Report for: June, July, August

BK055 - Horizontal Tank Brooklyn, New York

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Distilate fuel oil no. 2	0.00	0.50	0.50

TANKS 4.0.9d Emissions Report - Detail Format Total Emissions Summaries - All Tanks in Report

Emissions Report for: June, July, August

Tank Identification				Losses (lbs)
. BK009	SHELL OIL COMPANY - BROOKLYN	Vertical Fixed Roof Tank	Brooklyn, NY	25.59
BK010	SHELL OIL COMPANY - BROOKLYN	Vertical Fixed Roof Tank	Brooklyn, New York	25.59
BK041	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	80.77
ВК042	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	80.33
BK043	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	285.83
ВК044	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	284.41
BK045	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	80.33
BK046	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	76.24
BK047	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	451.85
ВК048	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	451.85
BK049	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	478.53
BK050	SHELL OIL COMPANY - BROOKLYN	Internal Floating Roof Tank	BROOKLYN, NY	478.53
BK052	SHELL OIL COMPANY - BROOKLYN	Horizontal Tank	Brooklyл, NY	9.86
• вко53	SHELL OIL COMPANY - BROOKLYN	Horizonlal Tank	Brooklyn, NY	0.00
BK054	SHELL OIL COMPANY - BROOKLYN	Horizontal Tank	Brooklyn, NY	12.72
BK055	SHELL OIL COMPANY - BROOKLYN	Horizontal Tank	Brooklyn, New York	0.50
Total Emissions for all Tanks:				2,822.94

APP:	END	IX	C

THE STATE OF NEW YORK 2008 EMISSION STATEMENT

Motiva Enterprises, LLC

Trinity Consultants

New York State Department of Environmental Conservation 625 Broadway, Albany, New York 12233



February 11, 2009

MOTIVA ENTERPRISES LLC

DEC ID: 2610100105

25 PAIDGE AVE

BROOKLYN, NY 11222

Attn: Environmental Manager

Dear Sir or Madam:

The New York State Department of Environmental Conservation (NYSDEC) is collecting 2008 fuel consumption data and air emissions from combustion, incineration, and industrial processes at facilities across the State. NYSDEC is required by the 1990 federal Clean Air Act to collect this information annually.

NYSDEC records indicate that your facility is required to have a Title V permit pursuant to 6 NYCRR 201-6, and therefore must complete the enclosed **2008 Emission Statement** pursuant to 6 NYCRR Subpart 202-2.

NYSDEC uses permit records to provide an individualized emission statement for each facility. If your Title V permit, permit modification or permit renewal has not been issued you may not see updated information as provided in permit applications or previous emission statement submittals. Every attempt has been made to update emission statement information and have your form reflect current permit data. Despite these efforts, the duly authorized representative at the facility is required under 6 NYCRR 202-2.3(a)(1) to verify the truth, accuracy, and completeness of the emission statement.

Environmental Conservation Law (section 72-0303) requires operating permit fees to be based on the previous year's actual emissions, as demonstrated to the Department's satisfaction, and that the emission statement be used to demonstrate actual emissions.

Please return the completed statement by April 15, 2009 to:

Mr. Ronald W. Stannard, P.E.

NYS Department of Environmental Conservation Division of Air Resources 625 Broadway Albany, NY 12233-3251

Enforcement action will be initiated for all emission statements that are post marked after April 15, 2009. If you do not respond, your fee bill will based on maximum permitted emissions. Please note that this fee may be significantly higher than the fee associated with actual emissions. Do not pay your fee now. You will be billed at a later date.

Questions on the emission statement should be directed to Mr.Stannard or his staff at (518) 402-8396.

Sincerely,

David J. Shaw

Director

Division of Air Resources

New York State Department of Environmental Conservation Division of Air Resources 2008 Emission Statement Section 1 - Certification

or: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

Attn: MARIO A D'ANTO	JANO OF Environmental Manager					
hone:		Primary SIC:	5171	DECID: 261010010	5	
		•				
Table of Con	tents	e de la companya del companya de la companya de la companya del companya de la co	1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1			
				**************************************	• • • • • •	
Section 2	.1	Facility Fuel	Use (Combustion	and Incineration)	`.	1:
Section 2	2	Combustion	and Incineration E	imissions Summa	ry (Optional)	
Section 2	3	Combustion	and Incineration F	rocess Emissions	3	• '
Section 3	.1	Industrial Em	issions Summary	• .	•	
Section 3	2	Industrial Pro	cess Emissions			•
Section 4	#7;44 \$	Periodic Inve	ntory Blank Repo	rting Forms		•
•	· · · · · · · · · · · · · · · · · · ·				•	
	<u> </u>					<u>. </u>
	•					
4		Section 1 - Certificat	ion			
with the instruct	, is based upon the best in tions provided by the Depa s punishable as a Class A	nformation available, a artment.I (We) under	and is complet stand that any	e and accurate false statemen	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep s punishable as a Class A	nformation available, a artment.I (We) under	and is complet stand that any nt to Section 2	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep s punishable as a Class A	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep is punishable as a Class A Fuel/Combustic	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep s punishable as a Class A	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep is punishable as a Class A Fuel/Combustic	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep is punishable as a Class A Fuel/Combustic	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep is punishable as a Class A Fuel/Combustic	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep is punishable as a Class A Fuel/Combustic Print Fuil Name	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep is punishable as a Class A Fuel/Combustic Print Fuil Name	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Dep is punishable as a Class A Fuel/Combustic Print Fuil Name	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the Department	nformation available, a artment. I (We) under misdemeanor pursua	and is complet stand that any nt to Section 2 ocess Certifica Telephone #	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the Department	nformation available, artment. I (We) under misdemeanor pursua on and Incineration Pr	and is complet stand that any nt to Section 2 ocess Certifica Telephone #	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the Department	nformation available, artment. I (We) under misdemeanor pursua on and Incineration Pr	and is complet stand that any nt to Section 2 ocess Certifica Telephone #	e and accurate false statemen 110.45 of the Pe	nt contained	
y my signature with the instruct	, is based upon the best in ions provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the provided by the Department of the Department	nformation available, artment. I (We) under misdemeanor pursua on and Incineration Pr	and is complet stand that any nt to Section 2 ocess Certifica Telephone #	te and accurate false statement 10.45 of the Period	nt contained	
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Section 2.1 - Facility Fuel Use (Combustion and Incineration)

Owner: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543

HOUSTON, TX 77002

Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Section 2. - Total Fuel Consumption

Indicate which fuels this facility is capable of burning and provide actual quantity, sulfur content, ash content, and heat value for fuels used in 2008

Note - This survey is for stationary sources only. Do not include fuel used for mobile sources (e.g., fleet vehicles, forklifts, portable emergency generators, etc.)

Fuel Type	Quantity 2008	Units	Sulfur Avg (%)	Ash Avg (%)	Heat Value MMBTU/Unit
NUMBER 2 OIL	0	1000 gallons burned	NA	NA	. NA
NATURAL GAS	1.356	million cubic feet burned	, NA	NA	1020 Btulsicf

Sulfur, Ash, and Heat Value should be reported where N/A (not applicable) has not been preprinted. Otherwise, maximum default limits will be applied.

*- Specify Fuel

Section 2.2 - Combustion and Incineration Emissions Summary (Optional)

y: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Total Combustion and Incineration Process Emissions by Contaminant

Enter the 2008 emissions total of each contaminant from this facility for combustion and incineration processes (if known)

Chem Family	CAS No.	Contaminant Name	Actual Emissions (Lbs/yr)
5 .	000630-08-0	CARBON MONOXIDE	113.91
. 8	007439-92-1	LEAD	
2	007446-09-5	SULFUR DIOXIDE	0.81
. 7	0NY075-00-5	PM-10	10.31
11	0NY075-02-5	PM 2.5	10-31
· 1	0NY075-10-0	UNSPECIATED PARTICULATES (EMISSION STATEMENT USE ONLY)	10.31
7	0NY075-10-5	UNSPECIATED PM-10 (EMISSION STATEMENT USE ONLY)	10.31
· 3	0NY210-00-0	OXIDES OF NITROGEN	135.61
4	0NY998-10-0	UNSPECIATED VOC (EMISSION STATEMENT USE ONLY)	7.46
1000			
\ -			
	•		

Note: This section is optional

Section 2.3 - Combustion and Incineration Process Emissions

Owner: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07 DECID: 2610100105 Primary SIC: 5171 Process Data Emission Unit: U-FAC01 SCC: 1-03-005-01 INS/COM:DISTILLATE;GRADES1&2 Process ID: 011 (EXEMPT) SCC Desc: EXTERNAL COMBUSTION BOILERS - COMMERCIAL/INDUSTRIAL COMMERCIAL/INSTITUTIONAL BOILER - DISTILLATE OIL Grades 1 and 2 Oil Fuel Type: NUMBER 2 OIL **Annual Thruput:** O Thruput Units: 1000 gallons burned **Process Description:** Space Heating **Control Equipment Description:** Provide control efficiency below with emissions summary Operational Data: Annual Average Jan, Feb, & Dec of 2008 Percent Fuel Use by Season Jun - Aug Days/Wk Total Days Hrs/Day Days/Wk Total Days Days/Wk Dec-Feb Mar-May Jun-Aug Sep-Nov Hrs/Day **Process Contaminant Summary:** Providing fuel combustion emissions for the process listed above is OPTIONAL. REPORT EMISSIONS IF KNOWN. Otherwise, federal emission factors will be used to calculate your emissions. Control Efficiency Actual Chem Emission Family CAS No. (%) (Lbs/yr) Factor HD Source **Contaminant Name** 5 000630-08-0 **CARBON MONOXIDE** 2 007446-09-5 SULFUR DIOXIDE 7 0NY075-00-5 0NY075-10-0 UNSPECIATED PARTICULATES (EMISSION STATEMENT USE ONLY) 0NY210-00-0 OXIDES OF NITROGEN 0NY998-10-0 UNSPECIATED VOC (EMISSION STATEMENT USE ONLY)

Section 2.3 - Combustion and Incineration Process Emissions

ar: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SiC: 5171

DECID: 2610100105

sc	s Data				;	Emissi	on Unit:	U-FAC01					
	C: 1-05-001-0	6 SPACE HE	EATER: ND;	NATURAL	GAS		• •	Process I	D: E02	(EXEMP	T)	•	
SCC Des	sc: EXTERNAL INDUSTRIA Natural Gas	AL SPACE H		RS - SPACE	E HEATERS		•	•	٠			, .	
Fuel Typ	e: NATURAL	GAS		Annual T	hruput:	1.35	6	Thruput Units	s: milli	on cubic fee	t bume	ed	
Process	Description:			-		· · · · · · ·		•					
Hot water	er heating syste	m for garage	e area:	•						•			
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	Equipment De	•			•		•	• .					
Provi	de control effici	ency below v	with emissio	ns summar	У						,		
6.									,				•
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Onorot	ional Data:					-							,
	- Annual Aver		Por	roomt Eugl	Use by Seas			Jun - Aug		lo	n Esh	, & Dec of	2008
Hrs/D			Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	Hrs/Day	Days/Wk	otal D	ays Hrs/D	ay Da	ys/Wk To	tal Days
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	ting fuel comi nerwise, feder							REPORTEN	IISSIO	ias it kim	JVVN.		;
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Chem				. •		•	٠.			' Actual		Emission	ì
	CAS No.	Contamina					٠.			Actual (Lbs/yr)	HD	Emission Factor	Source
	CAS No. 000630-08-0	Contamina			· .				iciency (%)		HD 3		Source
Family						· · · · · · · · · · · · · · · · · · ·	• •		iciency (%)	(Lbs/yr)			Source
Family 5	000630-08-0	CARBON N	MONOXIDE		· · · · · ·		· .		iciency (%)	(Lbs/yr)			Source
Family 5 8	000630-08-0 007439-92-1	CARBON N LEAD SULFUR D	MONOXIDE			· · · · · · · · · · · · · · · · · · ·			iciency (%)	(Lbs/yr)	3		Source
Family 5 8	000630-08-0 007439-92-1 007446-09-5	CARBON N LEAD SULFUR D PM-10	MONOXIDE						iciency (%)	(Lbs/yr) 113.9) - 0.81	3		Source
5 8 2 7	000630-08-0 007439-92-1 007446-09-5 0NY075-00-5	CARBON M LEAD SULFUR D PM-10 PM 2.5	MONOXIDE	CULATES	(EMISSION	STATEME	NT USE C	Eff	iciency (%)	(Lbs/yr) 113.9) - 0.81 10-31	3		Source AP-4.
5 8 2 7	000630-08-0 007439-92-1 007446-09-5 0NY075-00-5 0NY075-02-5	CARBON M LEAD SULFUR D PM-10 PM 2.5 UNSPECIA	MONOXIDE MOXIDE	-				Eff	iciency (%)	(Lbs/yr) 113.9) - 0.81 10-31	3 3 3		Source AP-4.
5 8 2 7 11 1	000630-08-0 007439-92-1 007446-09-5 0NY075-00-5 0NY075-02-5 0NY075-10-0	CARBON M LEAD SULFUR D PM-10 PM 2.5 UNSPECIA UNSPECIA	MONOXIDE NIOXIDE NIED PARTI	(EMISSIO				Eff	(%)	(Lbslyr) 113.9) 0.81 10-31 10-31	3 3 3 3		Source AP-4.
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Section 2.3 - Combustion and Incineration Process Emissions Blank Form

Owner: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002

Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

BROOKLYN, NY 11222

			X.,		44	Primary Si	C: 5171	1 .	DECID	: 26101	00105		
roces	s Data					Emission	Unit:	NA					
sc			NA						ID: NA				
SCC Des		3									·,		
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Section 3.1 - Industrial Process Emissions Summary

910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Total Industrial Process Emissions by Contaminant

Enter the 2008 emissions total of each contaminant from this facility

Chem Family	CAS No.	Contaminant Name	Actual Emissions (Lbs/yr)
9	000071432	BENZENE	156.1
9	000091203	NAPHTHALENE	0.09
: 4	000095636	BENZENE, 1,2,4-TRIMETHYL-	5.23
. 9	000100414	ETHYLBENZENE	18.81
9 .	000108883	TOLUENE	221.49
9	000110543	HEXANE	288.12
9	000540841	PENTANE, 2,2,4-TRIMETHYL- (ISO-octane)	41-4
4	000560214	TRIMETHYL PENTANE, 2,2,3-	~A
9	001330207	XYLENE, M, O & P MIXT.	99-17
9	001634044	METHYL TERTBUTYL ETHER	93.85
7 🔻	008006619	GASOLINE	NA
4	0NY998100	UNSPECIATED VOC (EMISSION STATEMENT USE ONLY)	52,085.11

Section 3.2 - Industrial Process Emissions

Owner: MOTIVA ENTERPRISES LLC

910 LOUISIANA ST OSP 2543

HOUSTON, TX 77002

Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

Emission Unit: U-00VRU

DECID: 2610100105

Process Data

SCC: 4-04-002-50 MISCELL LEAKS: LOADING RACKS

Process ID: VRU

SCC Desc: BULK TERMINALS/PLANTS

BULK PLANTS Loading Racks

Annual Thruput:

Thruput Units: 1000 GALLONS TRANSFERRED

Process Description:

Process VRU in Emission Unit U-00VRU consists of the following:

Hydrocarbon vapor & air mixture is collected from truck.

Loading via tight connections made to the top of the trucks for both the product and vapor.

The vapor is carried in piping to the vapor condenser located on the Vapor Recovery Unit (Emission Source/Control 00010 & 0010C, respectively) skid. This Vapor Recovery Unit uses two carbon adsorption beds alternately (Emission Points 00001 & 00VRU) with a vacuum system employed to facilitate desorbtion.

4. Condensed liquid hydrocarbon collected at bottom of vapor condenser and returned to storage.

Control Equipment Description:

Provide control efficiency below with emissions summary

Emission Point Identifiers:

List all Emission Point(s) associated with the Emission Unit listed above

10000 00VRU

	•		
One	ration	ral D	ata:

A	nnual Averag	e	Percent Operation by Season				Jun - Aug			
Hrs/Day	Days/Wk	Wks/Yr	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	Hrs/Day	Days/Wk	Total Days	
24	7.	5ચ	25%	25%.	asiv.	as`/.	24	. 7	92	

Process Contaminant Summary:

Provide actual emissions for process listed above

Cher Fami	m ily CAS No.	Contaminant Name	Efficiency (%)	Actual (Lbs/yr)	HD	Emissión Factor s	Source
9	000071432	BENZENE		4.82	3		AP-42
9	. 000091203	NAPHTHALENE		3×10-4	3		<u> </u>
9	000100414	ETHYLBENZENE		4.76	3		
9	000108883	TOLUENE		12.9	3		
9	000110543	HEXANE		26.75	_3	<u> </u>	לי
9	000540841	PENTANE, 2,2,4TRIMETHYL- (ISO-Octane)		41.4	_3		
9	001330207	XYLENE, M, O & P MIXT.		28.54	3		
9	001634044	METHYL TERTBUTYL ETHER		9.06	<u>3</u>		
-							1

Section 3.2 - Industrial Process Emissions

)r: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

		ant Summary: ssions for process listed above		Control	:	,	•	
Chem Famil	y CAS No.	Contaminant Name	. •	Efficiency (%)	Actual (Lbs/yr)		Emission Factor	Source
4	0NY998100	UNSPECIATED VOC (EMISSION STATEMENT USE ONLY)		: 1	1888.5	. 3		AP-42
				2-15-75				
						•		
				<u> </u>				

Section 3.2 - Industrial Process Emissions

Owner: MOTIVA ENTERPRISES LLC-910 LOUISIANA ST OSP 2543

HOUSTON, TX 77002

Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Process Data

SCC: 4-07-999-97 MISCELLANEOUS

Emission Unit: U-ADTNK

Process ID: ADT

SCC Desc: ORGANIC CHEMICAL STORAGE.

ORGANIC CHEMICAL STORAGE - MISCELLANEOUS

Specify in Comments

Annual Thruput:

38.084.

Thruput Units: 1000 GALLONS STORAGE CAPACITY

Process Description:

Process ADT in Emission Unit U-ADTNK is for the additive storage tanks. Four of these additive tanks (Tanks #7, #8, #9 & #10) are vertical tanks with cone fixed roots. The other five tanks (Tanks # 51, # 52, # 54, # 55 & # 56) are horizontal tanks. Gasoline additive Tanks # 7, # 55, # 8, # 9, # 53, #51, #10, #52 and #54 correspond to Emission Points and Emission Source/Control 000XV, 00XX, 00XIV, 00XIV, 00XIV, 00XIV, 0XIII, 0XVII and XVIII respectively. The emissions from these additive tanks are insignificant. The facility is willing to accept a federally enforceable limit of 526,900,000 gallons/year of gasoline throughput.

Fixed Roof Tanks (Additive + Distillate Tanks)

Control Equipment Description:

Provide control efficiency below with emissions summary

Emission Point Identifiers:

List all Emission Point(s) associated with the Emission Unit listed above

IVX00 VX000 XVIII 000XX

Operational Data:

Annual Average			P	ercent Opera	tion by Seaso	Jun - Aug			
Hrs/Day	Days/Wk	Wks/Yr		Mar-May	Jun-Aug	Sep-Nov	Hrs/Day	Days/Wk	Total Days
24	7	52.	a5%	asy.	dsy.	asy.	· a4	7	92
	************								<u>-</u>

Process Contaminant Summary:

Provide actual emissions for process listed above Control Efficiency Chem Actual **Emission** (%) Family CAS No. **Contaminant Name** (Lbs/yr) HD Factor Source TANKS 4.09d + 000071432 4.09 Q BENZENE DISTILLATE & ADDITIVE HI 8 NAPHTHALENE 9 000091203 8.7x104 SPECIATION 4 000095636 BENZENE, 1,2,4-TRIMETHYL-0 Я ጷ 000100414 **ETHYLBENZENE** 1.15 9 000108883 TOLÜENE B 3-88 0.88 B g 000110543 **HEXANE** 9 000540841 PENTANE, 2,2,4-TRIMETHYL-O જ 2.58 8 9 XYLENE, M, O & P MIXT. 001330207 Š 9 001634044 METHYL TERTBUTYL ETHER 0

Section 3.2 - Industrial Process Emissions

r: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Prov	ide actual emis	sions for process listed above	Control	•	٠.		
Chem Family	CAS No.	Contaminant Name	Efficiency (%)	Actual (Lbs/yr)	HD	Emission Factor	Source
4	0NY998100	UNSPECIATED VOC (EMISSION STATEMENT USE ONLY)		245.69	8		TANKS 4.090
					\equiv		DISTILLATE &
							ADDITIVE HA

Section 3.2 - Industrial Process Emissions

Owner: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Process Data

Emission Unit: U-GTANK

SCC: 4-04-001-60 INT.FLOAT-PRI.SEAL;ST.LOSSES

Process ID: GDT

SCC Desc: BULK TERMINALS/PLANTS

BULK TERMINALS

INTERNAL FLOAT ROOF W/ PRIMARY SEAL-SPECIFY LIQUID:STANDING LOSS

Annual Thruput:

311, 499

Thruput Units: 1000 GALLONS STORAGE CAPACITY

Process Description:

Process GDT for gasoline/distillate in Emission unit U-GTANK consists of the following:

- 1. The control of vapor losses due to standing and working of storage tanks.
- 2. The internal floating roof tank compared with atmospheric pressure tanks achieves a high percent reduction of evaporation loss because the roof floats on the product and air space is almost completely eliminated.

There are ten (10) storage tanks of different volumes containing gasoline or petroleum distillates, Tanks # 41, # 42, # 43, # 44, # 45, # 46, # 47, # 48, # 49 and # 50. These gasoline or petroleum distillates storage tanks correspond to Emission Points and Emission Source/Control 0000V, 000II,

Control Equipment Description:

Provide control efficiency below with emissions summary

Tanks 41, 42, 45 & 46 Stored Ethanol in 2008

Tanks 43, 44, 47, 48, 49 & 50 stored Gasoline in 2008

Standing LOSSES of all Floating Roof Tanks

Emission Point Identifiers:

List all Emission Point(s) associated with the Emission Unit listed above

0000V 0000X 000II 00VI 000IX 000VI 000XI 00III 00VII 0VIII 0VIII

Operational Data:

A	nnual Average	·	Pe	rcent Opera	tion by Seaso	Jun - Aug			
Hrs/Day	Days/Wk	Wks/Yr	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	Hrs/Day	Days/Wk	Total Days
24	1.	52	25%	25%	as`/.	as./	24	7	92

Process Contaminant Summary:

Provide actual emissions for process listed above Control Chem Efficiency Actual Emission Family CAS No. Factor (Lbs/yr) **Contaminant Name** HD Source TANES 4.09d + 36.14 BENZENE 000071432 GASOLINE & 8 **NAPHTHALENE** 0.02 000091203 ETHANOL HAP 1.25 SPECIATION 000095636 BENZENE, 1,2,4-TRIMETHYL-9 **ETHYLBENZENE** 000100414 3.14 8 000108883 TOLUENE 50.03 g 000110543 **HEXANE** 63.34 g. 000540841 8 PENTANE, 2,2,4-TRIMETHYL-0 001330207 XYLENE, M, O & P MIXT. 16.69 B 001634044 METHYL TERTBUTYL ETHER 20.04

Section 3.2 - Industrial Process Emissions

r: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Proces	ss Contamin	ant Summary:	•							
Prov	ide actual emis	sions for process listed ab		Control				*1		
Chem Family	CAS No.	Contaminant Name			Efficiency (%)	Actual (Lbs/yr)	НD	Emission Factor	Source	
4	0NY998100	UNSPECIATED VOC (E	MISSION STATEMENT USE	ONLY)	.1	1,641.27	. <i>ĝ</i>		TANKS	4.09d ·
									GASOLI	f ,
•		F .								SOL HA
							<u> </u>		- SPC C I	ATION

Section 3.2 - Industrial Process Emissions Blank Form

Owner: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002

Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Emission Unit: U-G TANK

SCC: 4-04-001-18 BULK: INFLOAT: RUP 13/10/7 WD

Process ID: 604

SCC Desc: BULK TERMINALS I PLANTS :-

BULK TERMINALS

BULK TERM : INTERN FLOAT ROOF (PRISECISEAL) : GAS RUP 13/10/7: WITHDRAWAL

Annual Thruput:

Thruput Units: 1000 Gallons

Process Description:

working Losses from all Internal Floating Roof Tank's Tanks 41,42,45 &46 Stored Ethanol in 2008

Tanks 43,44, 47,48,49 & 50 Stored Rasoline in 2008

Control Equipment Description:

Provide control efficiency below with emissions summary

Emission Point Identifiers:

List all Emission Point(s) associated with the Emission Unit listed above

uper	atio	nai .	vata:	

A	nnual Average	**************	Percent Operation by Season				Jun - Aug			
Hrs/Day	Days/Wk	Wks/Yr	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	Hrs/Day	Days/Wk	Total Days	
24	7	52	257	25'/.	<u>as 7.</u>	32, V.	24	7_	92	

Process Contaminant Summary:

		sions for process listed above		Contro	N.			
Chem Family CAS No.		Contaminant Name			cy Actual (Lbs/yr)	HD	Emission Factor	Source
9	5000T1432	Benzene			4.05	Q.		TANKS 4.090+
a	000100414	Ethylbenzene			0.34	8		ETHANOL 4
9	000108883	Toluene			5.39	ጸ		<u>CPECI</u> MTION
9	000110543	Hexane			6.8	8		
q ć	00540841	Pentane, 224 Trimethyl			0	S		
ar 4	01330207	Xylene, morp mixt	·. ·		8.1	8		
9 6	01634044				2.04	Q		
4 (0018PPY4C			13	62-84	8		
9	91-20-3	Naphthalene	•	0	.002	Z	٠	
9	95-63-6	1,2,4 Trimethal boazens	•	•	.13	5		

Section 3.2 - Industrial Process Emissions Blank Form

Primary SIC: 5171 ·

MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

> DARID: 610000GT07 DECID: 2610100105

Process Data

SCC: 4-07-999-98 MISCELLANE OUS

Process ID: 603

SCC Desc: DRGANIC ENEMICAL STURAGE

ORGANIC CHEMICAL STURAGE - MISCELLANEOUS
Specify in Comments.

Annual Thruput:

Thruput Units: 1000 Gallons Transferred

Process Description:
Additive Storage Tanks, Pour of these (7,8,9210) are Vertical tanks with Core fixed roofs. The other Six tanks (51,52,53,54,55256) are Horizontal tanks. Emission Unit: U-ADTNK

Process ID: 603

Process ID: 603

Process ID: 603

**COMMENTAL CHEMICAL STURAGE - MISCELLANEOUS
Specify in Comments.

**Opening of the Comments of the Comm

Emissions have been reported under Process ID: ADT

Control Equipment Description:

Provide control efficiency below with emissions summary

List all Emission Point(s) associated with the Emission Unit listed above

Emission Point Identifiers:

Operational Data: - Annual Average Percent Operation by Season -Jun - Aug Days/Wk Days/Wk Hrs/Day Wks/Yr Dec-Feb Mar-May Jun-Aug Sep-Nov Hrs/Day Total Days Process Contaminant Summary: Provide actual emissions for process listed above Control Efficiency Actual Chem **Emission** Family CAS No. (Lbs/yr) Factor Contaminant Name HD Source

Section 3.2 - Industrial Process Emissions Blank Form

r: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002

95-63-6

1,2,4 Trimethylbenzene

Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Process Data Emission Unit: SCC: 4-04-001-SI MISC LOSSE'S . VALV. FLAG PUMP Process ID: E 05 SCC Desc: BULK TERMINALS ! PLANTS BUCK TERMINALS - VALVES, FLANGES, PUMPS 1000 Gallons 311,587 Thruput Units: **Annual Thruput: Process Description:** Process Fugitives **Control Equipment Description:** nivide control efficiency below with emissions summary **Emission Point Identifiers:** List all Emission Point(s) associated with the Emission Unit listed above **Operational Data: Annual Average** Percent Operation by Season Jun - Aug Days/Wk Days/Wk Wks/Yr Sep-Nov Hrs/Day Hrs/Day Dec-Feb Mar-May Jun-Aug 25% જેડ7. 24 **5**2 **45%** asY. 4 Process Contaminant Summary: Provide actual emissions for process listed above Control Efficiency Actual Chem **Emission** Family CAS No. (Lbs/yr) Factor **Contaminant Name** HD Source 000071432 6.97 AP-42 Benzene 000100414 Ethulbenzene 0.62 9.85 000108813 Toluene 3 3 Hexane 000110543 3 000540841 Pentane, 224 Thirnethyl 3.28 3 001330207 xylene mode P mixt 3 4.06. methyl Terra Butyl Ether 001634044 2192-37 0018PP740 unspeciated VOC 4.5 X10-3 91-20-3 Naphthalene (Emission statement only)

0.25

Section 3.2 - Industrial Process Emissions Blank Form

r: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

DARID: 610000GT07

Primary SIC: 5171

DECID: 2610100105

Process Data

Emission Unit:

in an in l

SCC: 4-04-001-54 TANK TRUCK VAPOR LEAKS

Process ID: EO

SCC Desc: BULK TERMINAL PLANTS

BULK TERMINALS TANK TRUCK LEAKS

Annual Thruput: 311,587

Thruput Units:

1000 Gallons

Process Description:

MACT LUADING LOSSES

LOADING RACK FUGITIVES

Control Equipment Description:

Provide control efficiency below with emissions summary

Emission Point Identifiers:

List all Emission Point(s) associated with the Emission Unit listed above

3001

Operational Data:

А	nnual Average	ė	Percent Operation by Season				Jun - Aug			
Hrs/Day	Days/Wk	Wks/Yr	Dec-Feb	Mar-May	Jun-Aug	Sep-Nov	Hrs/Day	Days/Wk	Total Days	
24	7	કર્	25%	₹2%	25%	&s'\ .	24	7	92	

Process Contaminant Summary:

F	rovide actual emis	sions for process listed above	Control			
Chem Family CAS No.		Contaminant Name	Efficiency Actual (%) (Lbs/yr)	НD	Emission Factor	Source
9	000071432	Benzene	100-023	· 3		AP-42
9	000100414	. Ethylborzene	8.8	3		· .
9	000108883	Toluene	139.43	3		
9	000110943	Hexane	177.85	. 3		
q	000540841	Pentane 224 minothyl	O'	3.	•	
9	001330207	xylene morp mixt.	46-28	3		1
~: વ\	01634044	methyl Tetra Bulyl Ether	58.65	3	•	. 2
4	0018ppY40	Unspecialted VOC (Emission statement use only)	31,747	3		
9	91-20-3	waphthalen e	0.06	3		
7	95-63-6	1,2,4 Trimethylbenseno.	₹ <i>∙58</i>	3	•	· ·

Section 4 - Periodic Inventory Blank Reporting Form

r: MOTIVA ENTERPRISES LLC 910 LOUISIANA ST OSP 2543 HOUSTON, TX 77002 Facility: MOTIVA ENTERPRISES LLC 25 PAIDGE AVE BROOKLYN, NY 11222

									DAND. 010000	0101			
		•		•		Prima	ry SIC: 517	1 ·	DECID: 261010	0105			
Process Data			NA							_			
scc:	- 1 se				٠		Ann	ual Thruput:	L NA				
SCC Desc:		-	NA				Th	ruput Units:	NA				
		• . • •	. 1411		. 7 - 3	· · · · / ;		•				- .	
				×, .1			·		•				
		,	•										
Operational Dat	<u>a:</u>						-						٠.
Annua Hrs/Day Da	al Average ays/Wk	Wks/Yr	Dec-Feb	ercent Ope Mar-May		by Season-Aug	Sep-Nov	Hrs/Day	Jun - Aug Days/Wk	Total Da	- iys		•
NA	NA	NA	NA	NA		r∨A .	<u>NA</u>	<u>~A</u>	NA	NA			
Process Contar	ninant S	ummary:			•								
Provide actual	emission	s for proce	ss listed ab	ove				. 0-		•			
Chem Family CAS No.	Con	taminant N	ame					Effic	ntrol ciency Actual (%) (Lbs/yr)		Emission Factor	Source	:
000630-0	3-0 CAR	BON MONO	DXIDE						i	•		•	_
3 0NY210-0	0-0 OXII	DES OF NIT	ROGEN						, NA				_
4 ONY998-1	0-0 UNS	PECIATED	VOC (EMIS	SION STAT	EMEN	T USE O	NLY)			·····			

	DOCUMENT INFO	17 31
		37
DocID:	00000313	38
Filename:	58603-2009-02-12-COR-01 (Notice of Violation SPDES - NYSDEC).pdf	

New York State Department of Environmental Conservation

Division of Water, Region 2

47-40 21^{\$7} Street, Long Island City, NY 11101-5407 Phone: (718) 482-4933 • FAX: (718) 482-6516

Website: www.dec.ny.gov



CERTIFIED MAIL NO. 7005 0390 0004 3765 4375 WITH RETURN RECEIPT REQUESTED

February 12, 2009

Mr. Frank Signoriello, Terminal Supervisor Motiva Enterprises LLC 25 Paidge Avenue Brooklyn, NY 11222

RE:

NOTICE OF VIOLATION SPDES Permit No. NY 0006131 Annual Compliance Inspection

Dear Mr. Signoriello:

On February 11, 2009 the referenced facility was inspected for the purpose of evaluating its compliance with the requirements of its permit issued under the State Pollution Discharge Elimination System (SPDES) and Article 17 of the Environmental Conservation Law.

The following items were noted during the inspection:

 A review of the facility's discharge monitoring reports for Benzene, Toluene, Ethylbenzene, and Xylenes from the period January 2007 to December 2008 indicated the following:

Outfall .	Parameter	Reported Value	Action Level	Period
001	Ethylbenzene	0.17 mg/l	0.1 mg/l	2/07 to 4/07
	Toluene	1.1 mg/l	0.1 mg/l	2/07 to 4/07
	Xylenes	0.92 mg/l	0.1 mg/l	2/07 to 4/07
001	Benzene	1.0 mg/l (6/28/07); 0.19 mg/l (7/18/07)	0.1 mg/l	5/07 to 7/07
	Ethylbenzene	0.44 mg/l (6/28/07); 0.29 mg/l (6/27/07); 0.23 mg/l (7/18/07)	0.1 mg/l	5/07 to 7/07
	Toluene	6.7 mg/l (6/28/07); 0.76 mg/l (6/27/07); 2.1 mg/l (7/18/07)	0.1 mg/l	5/07 to 7/07
	Xylenes	3.7 mg/l (6/28/07); 0.66 mg/l (6/27/07); 1.18 mg/l (7/18/07)	0.1 mg/l	5/07 to 7/07

Outfall	Parameter	Reported Value	Action Level	Period
001	Toluene	0.56 mg/l (11/6/07); 0.12 mg/l (11/20/07)	0.1 mg/l	11/07 to 1/08
	Xylenes	0.35 mg/l (11/6/07)	0.1 mg/l	11/07 to 1/08
001	Toluene	0.33 mg/l (6/5/08)	0.1 mg/l	5/08 to 7/08
	Xylenes	0.36 mg/l (6/5/08)	0.1 mg/l	5/08 to 7/08

The facility's SPDES permit page 3 of 9 states "If levels higher than the actions levels are confirmed the results shall constitute an application for permit modification and the permit may be reopened for consideration of revised action levels or effluent limits."

Based on the results shown above, the Benzene, Toluene, Ethylbenzene, Xylenes levels higher than the action levels of 0.1 mg/l are confirmed. The Department shall proceed with the facility permit modification. In the interim, in order to prevent the discharge of Benzene, Toluene, Ethylbenzene, Xylenes levels higher than the action levels of 0.1 mg/l which may cause or contribute to a violation of water quality standards, the Department requests that a Comprehensive Corrective Action Plan be submitted to this office for review and approval by March 31, 2009. The plan must include a proposed schedule for implementation of the recommended corrective action.

- The facility still has not rectified the problem of using the unapproved method to analyze Benzene, Toluene, Ethylbenzene, and Xylenes (BTEX). The BTEX hydrostatic test samples collected on October 16, 2006 were analyzed by the method SW 846 8260. NYSDEC had already informed the facility twice in the compliance inspection reports (first notification: September 12, 2005 (Mr. Mario A. D' Antonio); second notification: June 6, 2006 (Mr. E.D. Bernhard Jr.)) that the method SW 846 8260 is unapproved method and it is not authorized under the 40 Code of Federal Regulations (CFR) Part 136. Please inform the laboratory that the approved method for BTEX analysis under 40 CFR Part 136 is EPA method number
- The facility Best Management Practices (BMP) Plan needs to be updated to reflect the recent changes at the facility.

The Department reserves its right to initiate an enforcement actions for the items noted in this Notice of Violation.

If you have any further questions, please contact me at (718) 482 4946.

Very truly yours,

Vichit Aramsombatdee, PE Environmental Engineer 2

Region 2, Division of Water

Robert Elburn, PE, Regional Water Engineer;
Selvin Southwell, PE, Deputy Regional Water Engineer

DocID:

00000421

Filename:

58603-2010-08-30-OTH-01 (Truck Rack and Additive Tanks Containment Volume

Calculations - RPMS).pdf

MOTIVA ENTERPRISES LLC

BROOKLYN TERMINAL BROOKLYN, NEW YORK

TRUCK LOADING RACK AND ADDITIVE TANKS 51 & 54 CONTAINMENT AREAS

CONTAINMENT VOLUME CALCULATIONS

PREPARED BY:



CONSULTING ENGINEERS

1 ROSSMOOR DRIVE MONROE TWP., NEW JERSEY 08831

RPMS PROJECT NO. 4844

AUGUST 2010

ADDITIVE TANKS CONTAINMENT

TANK 54 - 3,000 Gal. Vertical Tank

Dimensions:

 $D_{54} := 8.00$ ft H := 13.33 ft

Tank Volume: $V_{54} := 3000$

Gal.

TANK 51 - 5,000 Gal. Horizontal Tank

Dimensions:

 $D_{51} := 8.00$ ft L := 14.50

Tank Volume:

 $V_{51} := 5000$

Gal.

Check Dike Containment For 110% of the Largest Tank Capacity

Containment Dike Dimensions

Dimensions:

$$B_{\text{\scriptsize C}}:=12.00~\text{ft}$$

$$L_c := 32.67$$
 ft

$$H_c := 5.33$$
 ft

Containment Capacity

Gross Area:

$$A_g := B_c \cdot L_c$$

$$A_g = 392.04$$

Area Displaced by Tank 54:
$$A_{54} := \frac{\pi \cdot D_{54}}{4}$$
 $A_{54} = 6.28$

$$A_{54} := \frac{\pi \cdot D_{54}}{4}$$

$$A_{54} = 6.28$$

Net Area:

$$A_{net} := A_g - A_{54}$$
 $A_{net} = 385.76$

$$A_{net} = 385.76$$

 $\mathfrak{f}\mathfrak{t}^2$

Total Dike Containment:

$$V_c := A_{net} \cdot H_c \cdot 7.48$$

$$V_c = 15379.51$$

Gal.

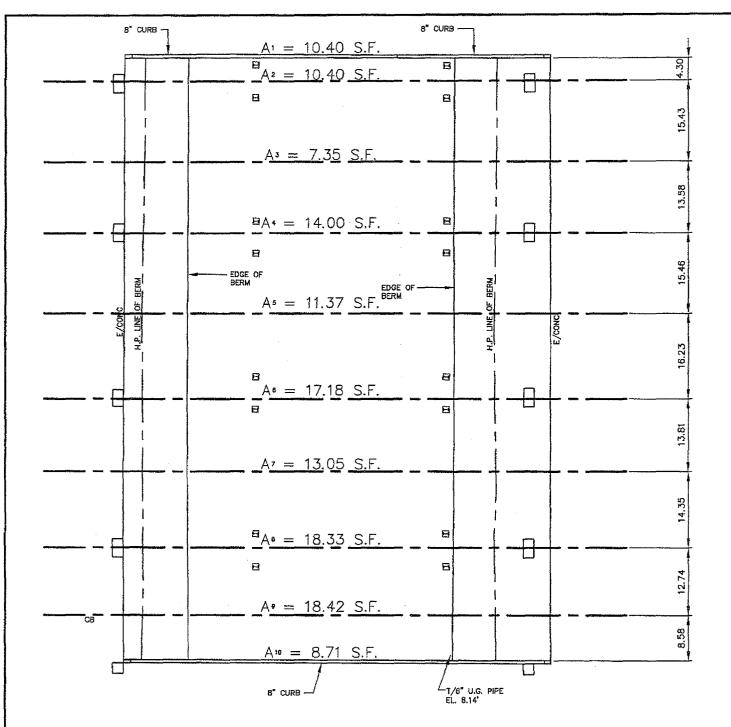
Containment Volume Required

$$V_R := 1.10 \cdot V_{51}$$

$$V_R := 1.10 \cdot V_{51}$$
 $V_R = 5500.00$ Gal.

$$V_C >> V_R => OK$$

Containment capacity exceeds by far the required capacity



TRUCK LOADING RACK

A = DENOTES AREA ACROSS PLANE WITH RESPECT TO CONTROL ELEVATION 10.00'

TOTAL CONTAINMENT VOLUME = 1,539 S.F. = 11,510 GAL.

Motiva Enterprises LLC Brooklyn Terminal Truck Rack Containment Calculation RPMS Project No. 4844

Plane	Area (ft²)	Dist. Between Planes (ft)	Volume (ft ³)
A_1	10.40		
A_2	10.40	4.30	44.72
		15.43	136.94
A ₃	7.35	13.58	144.97
A_4	14.00		
A ₅	11.37	15.46	196.11
		16.23	231.68
A_6	17.18	13.81	208.74
A ₇	13.05	, , , , ,	200.7
A_8	18.33	14.35	225.15
, ,,	10.00	12.74	234.10
A ₉	18.42	8.58	116.20
·A ₁₀	8.71	0.50	116.39

Total = 1,539 ft³ 11,510 Gal.

MOTIVA ENTERPRISES LLC. BROOKLYN, NY

TANK NO. 54 INNAGE TABLE

GAUGE HEIGHT 14"-5 3/4" LOCATED 1"-0" IN FROM TANK SHELL TO BEE OPPOSITE HINGE.

				, , , ,		44-77.00				
	FT.	GALLONS	FT.	GALLONS	FT.	GALLONS		WOH	CALLONS .	ļ
ē	Q	21	G	2,280	12		SAFE FILL) + SAFE FILL	0	21	В
0	Li	50		2,312	171	4,576	JANKE I MELL	1/8	2₹	5
Ţ	2 1	В1	1 2	2,343	2	4,607		1/4	25	Ė
ò	3)	112	3	2.574	3	4,638		3.6	32	i c
M	4	164	4	2,405	4	4,670		1/2	36,	M
	5	176	5.	2,437	5	4,701		F/E	59	í
Z	16	206	16	2,488	6	4,733		2/4		Ϋ́
				- 1144				il type	: 25 i	. "



Skell Additive alphany inc.

Tanks For All Purposes - General Steel Plate Construction

1850 STEINWAY ST. - LONG ISLAND CITY, N. Y. 11105

Phone: 718 274-3700

Tank #5/

NEW YORK CITY

5,000 GALLONS, 96" DIA. X 14'-6" LONG FUEL TANK

GAUGE MEASUREMENT CHART

INCHES	GALLONS	INCHES	GALLONS	INCHES	GALLONS
1	9	33	1,522	65	3,605
2	25	34	1,585	66	3,667
` 3	47	35	1,649	67	3,727
4	72	36	1,713	68	3,788
5	100	37	1,778	69	3,848
6	130	38	1,842	70	3,907
7	163	39	1,907	71	3,966
8	199	40	1,973	72	4,024
9	237	41	2,038	73	4,081
10	277	42	2,104	74	4,137
11.	318	43	2,170	75	4,192
12	381	44	2,236	76	4,247
13	405	45	2,302	77	4.300
14	451	46	2,368	78	4,352
15	499	47	2,435	79	4,404
16	548	48	2,501	80 //	4.454
17	598	49	2,567	81-6-9	4.502 SAFETIL
18	649	50	2,633	82	4,550
19	701	51	, 2,700	83	4,596
20	755	52	2,761	84	4,641
21	810	53	2,832	85	4.684
22	864	54	2,898	86	4,725
23	921	5 5	2,963	87	4,765
24	978	56	3,029	88	4,802
25	1,035	57	3,094	89	4,838
26	1,094	58	3,160	90	4,871
27	1,153	59	3,224	91	4,902
28	1,213	60	3,288	92	4,930
29	1.274	61	3,352	93	4,955
30	1,335	62	3,416	94	4,977
31	1,397	63	3,480	95	4,993
32	1,460	64	3,542	96	5,002

MOTIVA ENTERPRISES LLC. BROOKLYN, NY

TANK NO. 54 INNAGE TABLE

GAUGE HEIGHT 14'-5 3/4" LOCATED 1'-0" IN FROM TANK SHELL TO RIM OPPOSITE HINGE.

	FT.	GALLONS FT.	GALLONS	FY.	GALLONS		INCH GALLONS
В	IN.	IN. 21 6	2,250	1N.	4,544 /	SAFE FILL SAFE FILL	0 21 8
7	1	50 1	2,512	12 1 2	4.676	JATE TALL	1/8 7,5
r	3	81 2 112 3	2,343 2,274	3	4,607 4,638		1/4 26 7
D dA	4	144 4	2,40€	4	4.570		1/2 36 3
z	5 6	176 5 206 6	2,437 2,468	6	4,701 4,733		5/8 39 3/4 43 T
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^{1.} TANK SHELL MEIGHT: 13'-4"

THIS TABLE SUPERSEDES ALL TABLES ISSUED PRIOR TO 09/02

CHART IS CERTIFIED FOR THIS TANK ONLY. COMPUTED BY: JF 09/26/02 STRAPPED BY: JPY & 9K 09/25/02

SAYBOLT LP

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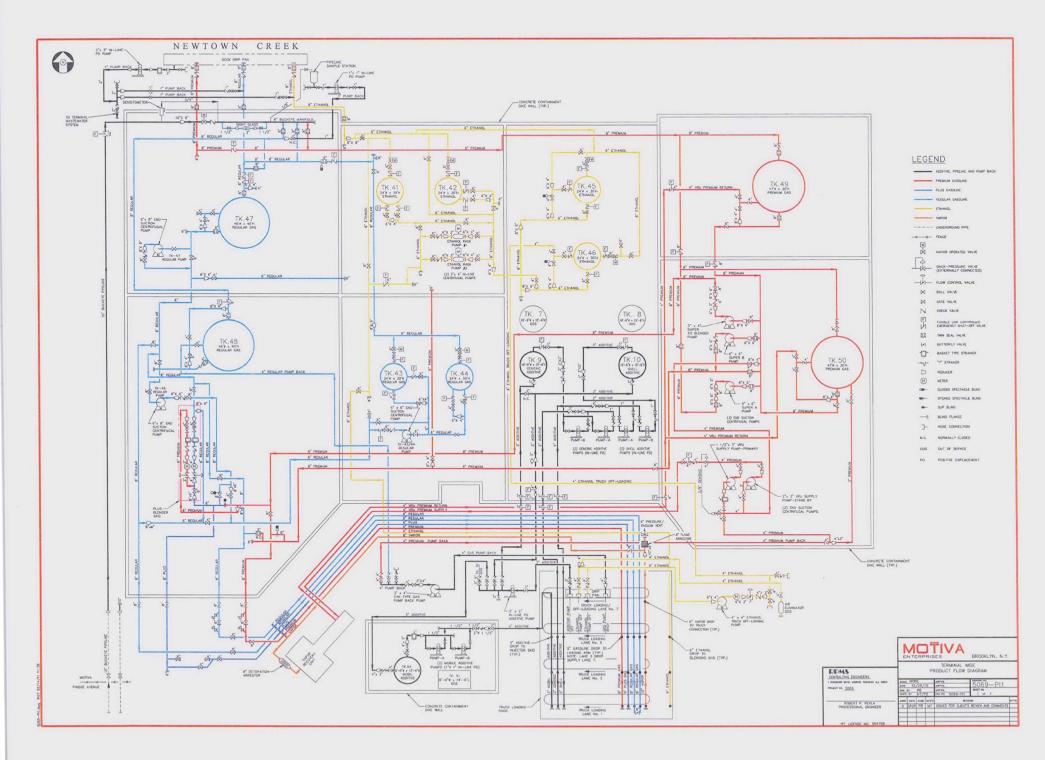
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B. TANK SHELL COMPUTED AT 60" F.

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B. FRACTIONS NOT APPLICABLE BELOW 0'-1"
5. SAFEFILL: 12'-0"

Product Flow Diagram



ms DS's

MATERIAL SAFETY DATA SHEET

Review Date: 01/04/2006

SECTION 1

PRODUCT AND COMPANY IDENTIFICATION

PRODUCT: Denatured Ethanol

MSDS NUMBER: 5708MU - 2 **PRODUCT CODE(S):** 02704, 05482

MANUFACTURER

TELEPHONE NUMBERS

Motiva Enterprises LLC

Spill Information: (877) 242-7400

P.O. Box 4540

Health Information: (877) 504-9351

Houston, TX. 77210-4540

MSDS Assistance Number: (877) 276-7285

SECTION 2

PRODUCT/INGREDIENTS

INGREDIENTS	CAS#	CONCEN	TRATION
Denatured Ethanol	Mixture	100	%weight
Ethanol	64-17-5	95 - 98	%weight
Unleaded Gasoline	Mixture	2 - 5	%weight
Toluene	108-88-3	0 - 1.5	%weight
Xylene, mixed isomers	1330-20-7	0 - 1.5	%weight
Benzene	71-43-2	0 - 0.25	%weight
Ethyl Benzene	100-41-4	0 - 0.27	%weight
Miscellaneous Hydrocarbons		0 - 2.5	%weight

NOTE: Content of Gasoline components will vary; Individual components may be present from trace amounts up to the maximum shown.

SECTION 3

HAZARDS IDENTIFICATION

EMERGENCY OVERVIEW

Appearance & Odor: Clear liquid, Alcohol odor,

Health Hazards: Causes severe eye irritation. May be harmful or fatal if swallowed. Do not induce vomiting. May cause aspiration pneumonitis. May cause CNS depression.

Physical Hazards: Material is extremely flammable and heavier than air. Vapors may travel across the ground and reach remote ignition sources causing a flashback fire danger.

NFPA Rating (Health, Fire, Reactivity): 1, 3, 0

Hazard Rating: Least - 0 Slight - 1 Moderate - 2 High - 3 Extreme - 4

Inhalation:

In applications where vapors (caused by high temperature) or mists (caused by mixing or spraying) are created, breathing

Denatured Ethanol

MSDS# 5708MU

Page: 1 of 13

may cause a mild burning sensation in the nose, throat and lungs. Breathing of high vapor concentrations may cause CNS depression, evidenced by dizziness, light-headedness, headache, nausea, drowsiness, and loss of coordination. Continued inhalation may result in unconsciousness.

Eye Irritation:

Severely irritating to the eyes causing pain, redness, swelling and blurred vision.

Skin Contact:

Prolonged or repeated skin contact can cause defatting and drying of the skin which may result in a burning sensation and a dried, cracked appearance.

Ingestion:

This material may be harmful or fatal if swallowed. Ingestion may result in vomiting; aspiration (breathing) of vomitus into lungs must be avoided as even small quantities may result in aspiration pneumonitis. Generally considered to have a low order of acute oral toxicity.

Other Health Effects:

Carcinogenic in animal tests. Known human carcinogen. See Section 11. Material is suspected of causing cancer in laboratory animals. See Section 11. Material may cause birth defects and/or miscarriages. See Section 11. Refer to Section 11, Toxicological Information, for specific information on the following effects:

Developmental Toxicity, Genotoxicity

Primary Target Organs:

The following organs and/or organ systems may be damaged by overexposure to this material and/or its components: Cardiovascular System, Blood/Blood Forming Organs, Kidney, Liver

Signs and Symptoms:

Irritation as noted above. Aspiration pneumonitis may be evidenced by coughing, labored breathing and cyanosis (bluish skin); in severe cases death may occur. Damage to blood-forming organs may be evidenced by: a) easy fatigability and pallor (RBC effect), b) decreased resistance to infection (WBC effect), c) excessive bruising and bleeding (platelet effect). Kidney damage may be indicated by changes in urine output or appearance, pain upon urination or in the lower back or general edema (swelling from fluid retention). Liver damage may be indicated by loss of appetite, jaundice (yellowish skin and eye color), fatigue and sometimes pain and swelling in the upper right abdomen.

For additional health information, refer to section 11.

SECTION 4

FIRST AID MEASURES

Inhalation:

Move victim to fresh air and provide oxygen if breathing is difficult. Get medical attention. If the victim has difficulty breathing or tightness of the chest, is dizzy, vomiting or unresponsive, give 100% oxygen with rescue breathing or CPR as required and transport to the nearest medical facility.

Skin:

Flush exposed area with water and follow by washing with soap if available. If redness, swelling, pain and/or blisters occur, transport to the nearest medical facility for additional treatment.

Eve:

Immediately flush eyes with large amounts of water for at least 30 minutes, by the clock, while holding eyelids open. Transport to nearest medical facility for additional treatment.

Denatured Ethanol MSDS# 5708MU

Page: 2 of 13

Ingestion:

DO NOT take internally. Do NOT induce vomiting. If vomiting occurs spontaneously, keep head below hips to prevent aspiration of liquid into lungs. Get medical attention. In general no treatment is necessary unless large quantities are swallowed, however, get medical advice. Have victim rinse mouth out with water, then drink sips of water to remove taste from mouth.

Note to Physician:

If more than 2.0ml/kg body weight has been ingested and vomiting has not occurred, emesis should be induced with supervision. Keep victim's head below hips to prevent aspiration. If symptoms such as loss of gag reflex, convulsions, or unconsciousness occur before emesis, gastric lavage using a cuffed endotracheal tube should be considered.

SECTION 5

FIRE FIGHTING MEASURES

Flash Point [Method]: <10 °F/<-12.22 °C [Approximate Setaflash Closed Cup]

Flammability in Air: 1.3%V - 7.6 %volume

Extinguishing Media:

Use water fog, foam, dry chemical or carbon dioxide (CO2) to extinguish flames. Do not use a direct stream of water. Material will float and can be re-ignited on surface of water.

Fire Fighting Instructions:

DANGER! EXTREMELY FLAMMABLE. Clear fire area of all non-emergency personnel. Only enter confined fire space with full bunker gear, including a positive pressure, NIOSH-approved, self-contained breathing apparatus. Cool surrounding equipment, fire-exposed containers and structures with water. Container areas exposed to direct flame contact should be cooled with large quantities of water (500 gallons water per minute flame impingement exposure) to prevent weakening of container structure.

Unusual Fire Hazards:

Vapors are heavier than air accumulating in low areas and traveling along the ground away from the handling site. Do not weld, heat or drill on or near container. However, if emergency situations require drilling, only trained emergency personnel should drill.

SECTION 6

ACCIDENTAL RELEASE MEASURES

Protective Measures:

DANGER! EXTREMELY FLAMMABLE! Eliminate potential sources of ignition. Handling equipment must be bonded and grounded to prevent sparking.

Spill Management:

Dike and contain spill.

FOR LARGE SPILLS: Remove with vacuum truck or pump to storage/salvage vessels.

FOR SMALL SPILLS: Soak up residue with an absorbent such as clay, sand or other suitable material. Place in non-leaking container and seal tightly for proper disposal.

Reporting:

U.S. regulations require reporting releases of this material to the environment which exceed the reportable quantity to the National Response Center at (800)424-8802.

Denatured Ethanol

MSDS# 5708MU

Page: 3 of 13

SECTION 7

HANDLING AND STORAGE

Precautionary Measures:

Wash with soap and water before eating, drinking, smoking, applying cosmetics, or using toilet. Launder contaminated clothing before reuse. Properly dispose of contaminated leather articles such as shoes or belts that cannot be decontaminated. Avoid heat, open flames, including pilot lights, and strong oxidizing agents. Use explosion-proof ventilation to prevent vapor accumulation. Ground all handling equipment to prevent sparking. Do not siphon gasoline by mouth; harmful or fatal if swallowed. Avoid contact with eyes, skin and clothing. Wash thoroughly after handling.

For use as a motor fuel only. Do not use as a cleaning solvent or for other non-motor fuel uses.

Handling:

Surfaces that are sufficiently hot may ignite liquid material. Material is extremely flammable and heavier than air. Vapors may travel across the ground and reach remote ignition sources causing a flashback fire danger.

Keep containers closed when not in use. WARNING! The flow of gasoline through the pump nozzle can produce static electricity, which may cause a fire if gasoline is pumped into an ungrounded container. To avoid static buildup, place approved container on the ground. Do not fill container in vehicle or truck bed. Keep nozzle in contact with container while filling. Do not use automatic pump handle (latch-open) device. Keep all storage vessels closed. Material will ignite when exposed to air. Air trapped within the storage container may be removed by placing dry ice in the container prior to closing. Turn off all battery operated portable electronic devices (examples include: cellular phones, pagers and CD players) before operating gasoline pump. Use only with adequate ventilation.

Storage:

Do not store in open or unlabeled containers. Store in a cool, dry place with adequate ventilation. Keep away from open flames and high temperatures.

Keep liquid and vapor away from heat, sparks and flame. Extinguish pilot lights, cigarettes and turn off other sources of ignition prior to use and until all vapors have dissipated. Use explosion-proof ventilation indoors and in laboratory settings.

Container Warnings:

Keep containers closed when not in use. Containers, even those that have been emptied, can contain explosive vapors. Do not cut, drill, grind, weld or perform similar operations on or near containers.

SECTION 8

EXPOSURE CONTROLS/PERSONAL PROTECTION

Chemical	Limit	TWA	STEL	Ceiling	Notation
Benzene	ACGIH TLV	0.5 ppmv	2.5 ppmv		Skin
Benzene	OSHA PEL	1 ppmv	5 ppmv		
Ethanol	ACGIH TLV	1000 ppmv			
Ethyl Alcohol	OSHA PEL	1000 ppmv			
Gasoline	ACGIH TLV	300 ppmv	500 ppmv		
Gasoline	OSHA PEL - 1989(revoked)	300 ppmv	500 ppmv		
Toluene	ACGIH TLV	50 ppmv			Skin
Toluene	OSHA PEL	200 ppmv		300 ppmv	
Toluene	OSHA PEL - 1989(revoked)	100 ppmv	150 ppmv		
Toluene	SHELL	50 ppmv			

Denatured Ethanol

MSDS# 5708MU

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	INTERNAL			
xylene (o-, m-, p- isomers)	OSHA PEL	100 ppmv		
xylene (o-, m-, p- isomers)	OSHA PEL - 1989(revoked)	100 ppmv	150 ppmv	
Xylene (o-, m-, p-isomers)	ACGIH TLV	100 ppmv	150 ppmv	

Decomposition Product	Limit	TWA	STEL	Ceiling	Notation
Carbon dioxide	ACGIH - TLV	5000 ppmm	30000		
		[ppmm		
Carbon dioxide	OSHA - PEL		30000		
			ppmm		
Carbon dioxide	OSHA -	10000			
	PEL_IS	ppmm			
Carbon monoxide	OSHA - PEL	35 ppmv		200 ppmv	

Decomposition Product	Method	Condition
Carbon dioxide	Combustion	
Carbon monoxide	Combustion	

Exposure Controls

Provide adequate ventilation to control airborne concentrations below the exposure guidelines/limits.

Personal Protection

Personal protective equipment (PPE) selections vary based on potential exposure conditions such as handling practices, concentration and ventilation. Information on the selection of eye, skin and respiratory protection for use with this material is provided below.

Eye Protection:

Chemical Goggles - If liquid contact is likely., or Safety glasses with side shields

Skin Protection:

Use protective clothing which is chemically resistant to this material. Selection of protective clothing depends on potential exposure conditions and may include gloves, boots, suits and other items. The selection(s) should take into account such factors as job task, type of exposure and durability requirements.

Published literature, test data and/or glove and clothing manufacturers indicate the best protection is provided by: Neoprene, or Nitrile Rubber

Respiratory Protection:

If engineering controls do not maintain airborne concentrations to a level which is adequate to protect worker health, an approved respirator must be worn. Respirator selection, use and maintenance should be in accordance with the requirements of the OSHA Respiratory Protection Standard, 29 CFR 1910.134.

Types of respirator(s) to be considered in the selection process include:

For Vapors: Air Purifying, R or P style prefilter & organic cartridge, NIOSH approved respirator. Full face air supplied respirator if oxygen level is reduced below 19.5 %. Self-contained breathing apparatus for use in environments with unknown concentrations or emergency situations.

Denatured Ethanol MSDS# 5708MU

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SECTION 9

PHYSICAL AND CHEMICAL PROPERTIES

Appearance & Odor: Clear liquid. Alcohol odor.

Substance Chemical Family: Alcohol

Boiling Point	173 °F Approximate	Flammability in Air	1.3 %volume - 7.6 %volume
Flash Point	< 10 °F Approximate [Setaflash Closed Cup]	Specific Gravity	0.79
Stability	Stable	Vapor Density	> 1
Viscosity	< 1.4 cSt @ 100 °F		

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REACTIVITY AND STABILITY

Stability:

Material is stable under normal conditions.

Conditions to Avoid:

Avoid heat, sparks, open flames and other ignition sources.

Materials to Avoid:

Avoid contact with strong oxidizing agents.

Hazardous Decomposition Products:

Thermal decomposition products are highly dependent on combustion conditions. A complex mixture of airborne solids, liquids and gases will evolve when this material undergoes pyrolysis or combustion. Aldehydes, Carbon Monoxide, Carbon Dioxide, Unidentified organic compounds, Peroxide, Styrene oxideand other unidentified organic compounds may be formed upon combustion.

SECTION 11

TOXICOLOGICAL INFORMATION

Acute Toxicity

TEST	Result	OSHA Classification	Material Tested
Dermal LD50	>2 g/kg(Rabbit)	Non-Toxic	Based on components(s)
Eye Irritation	Variable [Rabbit]	Irritating	Based on components(s)
Inhalation LC50	>16,000 ppmv(Rat)	Non-Toxic	Based on components(s)
Oral LD50	>5 ml/kg(Rat)	Non-Toxic	Based on components(s)

Carcinogenicity:

Gasoline has been tested by API in a long-term inhalation test in mice and rats. There was an increased incidence of liver cancer in female mice. Male rats had a dose related increase in kidney tumors. This effect was due to formation of alpha-2u-globulin in the rats. This material is not formed in humans and is therefore not considered relevant.

Carcinogenicity Classification

Denatured Ethanol MSDS# 5708MU

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2

Chemical Name	NTP	IARC	ACGIH	OSHA
Denatured Ethanol	No	Yes	No	No
Benzene	Yes	Carcinogen (1)	A1	Yes
Ethyl Benzene	No	Possible Carcinogen (2B)	A3	No
Toluene	No	Not Classifiable (3)	A4	No
Unleaded Gasoline	No	Possible Carcinogen (2B)	A3	No

Carcinogenicity	Chronic inhalation of wholly vaporized gasoline produced kidney tumors in male rats and liver tumors in female mice. The kidney tumors have been shown to develop through a unique mechanism involving Alpha-2u globulin. This protein is not present in humans making the kidney tumors irrelevant to potential human health risks. Origin of the female mouse liver tumors is less understood, leaving their significance for human risks uncertain. Prolonged and repeated exposure to high concentrations (10s to 100s ppm) of benzene may cause serious injury to blood-forming organs, is associated with anemia (depletion of blood cells) and is linked to the later development of acute myelogenous leukemia (AML) in humans. A recent chronic bioassay of ethylbenzene by the NTP produced clear evidence of carcinogenicity in male rats based on kidney tumor increase. Other animal tumors possibly associated with ethylbenzene include testicular adenomas in male rats, kidney tumors in female rats, lung tumors in male mice and liver tumors in female mice. Toluene is not known to be mutagenic or carcinogenic although available human and experimental animal data are limited and insufficient to assess carcinogenic potential.
Cardiovascular System	While there is no evidence that workplace exposure to acceptable levels of toluene vapors (e.g., the TLV) have produced cardiac effects in humans, high concentrations may cause cardiac sensitization and sudden lethality has been reported from habitual sniffing of solvents or glue. Animal studies have confirmed the sensitizing effects. Sensitization may lead to fatal changes in heart rhythms. Hypoxia or injection of adrenalin-like agents may enhance this effect. Thickening of heart blood vessels has been reported in animals exposed to xylene.
Developmental Toxicity	Daily exposure of pregnant rats to unleaded gasoline vapor at concentrations up to 9000 ppm resulted in no detectable maternal or developmental toxicity. Developmental toxicity studies of xylenes showed embryolethal/toxic and teratogenic effects with maternal toxicity. Many case studies involving abuse during pregnancy implicate toluene as a developmental toxicant. Studies in laboratory animals have shown developmental effects comparable to those reported in humans, but the effects were generally associated with maternal toxicity. Ethanol ingestion during pregnancy has been reported to cause birth defects in some infants.
Genotoxicity	Unleaded gasoline was tested for genetic activity in tests using microbial cells, cultured mammalian cells and rats (bone marrow) and was judged to be negative in every case. Toluene was negative in the Ames assay and negative for chromosomal aberrations and sister-chromatid exchanges in human lymphocytes and in an in vitro test using hamster cells. Mouse lymphoma test results for toluene were inconclusive.
Blood/Blood Forming Organs	Blood effects were seen in rats following prolonged and repeated oral exposure to a mixture of xylenes containing ethylbenzene.
Kidney	Long-term inhalation of wholly vaporized gasoline caused increased kidney weight and

Denatured Ethanol MSDS# 5708MU

	progressive nephropathy (tissue damage) in male rats. In rats exposed orally to a xylene mixture also containing ethylbenzene, males developed hyaline droplet changes and females showed evidence of early chronic nephropathy. Intentional abuse of toluene vapors by 'glue-sniffers' has been associated with damage to the kidneys.
Liver	Inhalation of gasoline vapor increased liver weights, urinary excretion of ascorbic acid, and hepatic enzyme activity in male rats. Liver weight increases were seen in rats dosed orally for 90 days with a xylene mixture also containing ethylbenzene. Reversible liver damage has been reported in persons exposed to toluene by solvent abuse. Prolonged and repeated consumption of ethanol has been shown to cause liver damage in animals and cirrhosis in humans.
Neurotoxicity	Rats receiving prolonged and repeated exposure to high doses of xylene have shown hearing loss. Prolonged and repeated exposures to high toluene concentrations (mixed solvent) have resulted in hearing loss in laboratory animals. There have also been reports of hearing damage in humans overexposed to toluene and other solvents, however, these effects and their possible relationship to noise exposure remain uncertain. Intentional inhalation ('glue-sniffing') and resulting overexposure to toluene vapors has been linked to brain injury.
Sensitization	Gasoline and component petroleum streams blended to produce it were tested in animal studies and found not to cause skin sensitization.
Systemic Toxicity	Laboratory animals exposed to prolonged and repeated doses of xylenes by various routes have shown effects in liver, kidneys, lungs, spleen, heart, blood and adrenals. Persons on disulfiram (Antabuse(R)) therapy should be aware that the ethyl alcohol in this product is hazardous to them just as is alcohol from any source. Disulfiram reactions (vomiting, headache and even collapse) may follow ingestion of small amounts of alcohol and have also been described from skin contact.

SECTION 12	ECOLOGICAL INFORMATION
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Environmental Impact Summary:

There is no ecological data available for this product.

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SECTION 13	DISPOSAL CONSIDERATIONS

RCRA Information:

Under RCRA, it is the responsibility of the user of the material to determine, at the time of the disposal, whether the material meets RCRA criteria for hazardous waste. This is because material uses, transformations, mixtures, processes, etc. may affect the classification. Refer to the latest EPA, state and local regulations regarding proper disposal.

SECTION 14	TRANSPORT	INIECHENACIE	INI	
OLUTION 14		HAI OLIMATIO	71 4	

US Department of Transportation Classification

Proper Shipping Name: Alcohols, N.O.S.

Denatured Ethanol MSDS# 5708MU

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Technical Names (s):

Ethanol, Petroleum Distillate

Identification Number:

UN1987

Hazard Class/Division:

3 (Flammable Liquid)

Packing Group:

- 11

Marine Pollutant % of Total:

Marine Pollutant: Marine Polluntant based on the presence of >10% hydrocarbons listed in 49 CFR 172.101, appendix B; main constituents Trimethylbenzene and Naphthalene.

Emergency Response Guide #127

International Air Transport Association

Hazard Class/Division:

3 (Flammable Liquid)

Identification Number:

UN1987

Packing Group:

Ш

Proper Shipping Name:

Alcohols, N.O.S. (Contains Ethanol and Gasoline)

Technical Name(s):

Ethanol, Gasoline

International Maritime Organization Classification

Hazard Class/Division:

3 (Flammable Liquid)

Identification Number:

UN1987

Packing Group:

П

Proper Shipping Name:

Alcohols, N.O.S.

Technical Name(s):

Ethanol, Gasoline

SECTION 15	ON 15	SECT
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REGULATORY INFORMATION

Federal Regulatory Status

OSHA Classification:

Product is hazardous according to the OSHA Hazard Communication Standard, 29 CFR 1910.1200.

Comprehensive Environmental Release, Compensation & Liability Act (CERCLA):

Benzene

RQ 10 lbs

Reportable Spill => 4096.961421 lbs

or 682.53 gal

Ozone Depleting Substances (40 CFR 82 Clean Air Act):

This material does not contain nor was it directly manufactured with any Class I or Class II ozone depleting substances.

Superfund Amendment & Reauthorization Act (SARA) Title III:

There are no components in this product on the SARA 302 list.

SARA Hazard Categories (311/312):

Immediate Health	Delayed Health	Fire	Pressure	Reactivity
YES	YES	YES	NO	NO

SARA Toxic Release Inventory (TRI) (313):

Denatured Ethanol MSDS# 5708MU

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2

Toluene, Benzene

Toxic Substances Control Act (TSCA) Status:

All component(s) of this material is(are) listed on the EPA/TSCA Inventory of Chemical Substances.

Other Chemical Inventories:

Australian AICS, Chinese Inventory, European EINECS, Japan ENCS, Korean Inventory, Philippines PICCS,

State Regulation

The following chemicals are specifically listed by individual states; other product specific health and safety data in other sections of the MSDS may also be applicable for state requirements. For details on your regulatory requirements you should contact the appropriate agency in your state.

California Safe Drinking Water and Toxic Enforcement Act (Proposition 65).

WARNING: This product contains a chemical(s) known to the State of California to cause cancer.

WARNING: This product contains a chemical(s) known to the State of California to cause birth defects or other reproductive harm.

New Jersey Right-To-Know Chemical List:

, ,		
Benzene (71-43-2)	0 - 0.25 %weight	Carcinogen
Benzene (71-43-2)	0 - 0.25 %weight	Mutagen
Benzene, Methyl- (108-88-3)	0 - 1.5 %weight	
Ethanol (64-17-5)	95 - 98 %weight	
Xylenes (1330-20-7)	0 - 1.5 %weight	

Pennsylvania Right-To-Know Chemical List:

Benzene (71-43-2)	0 - 0.25 %weight	Spec Haz Sub/Env Hazardous
Benzene, dimethyl- (1330-20-7)	0 - 1.5 %weight	Environmental Hazard
Benzene, Methyl- (108-88-3)	0 - 1.5 %weight	Environmental Hazard
Ethanol (64-17-5)	95 - 98 %weight	

SECTION 16

OTHER INFORMATION

Revision#: 2

Review Date: 01/04/2006 **Revision Date:** 04/14/2003

Revisions since last change (discussion): This Material Safety Data Sheet (MSDS) has been reviewed to fully comply with the guidance contained in the ANSI MSDS standard (ANSI Z400.1-1998). We encourage you to

take the opportunity to read the MSDS and review the information contained therein.

SECTION 17

LABEL INFORMATION

READ AND UNDERSTAND MATERIAL SAFETY DATA SHEET BEFORE HANDLING OR DISPOSING OF PRODUCT. THIS LABEL COMPLIES WITH THE REQUIREMENTS OF THE OSHA HAZARD COMMUNICATION STANDARD (29

MSDS# 5708MU Denatured Ethanol

Page: 10 of 13

CFR 1910.1200) FOR USE IN THE WORKPLACE. THIS LABEL IS NOT INTENDED TO BE USED WITH PACKAGING INTENDED FOR SALE TO CONSUMERS AND MAY NOT CONFORM WITH THE REQUIREMENTS OF THE CONSUMER PRODUCT SAFETY ACT OR OTHER RELATED REGULATORY REQUIREMENTS.

PRODUCT CODE(S): 02704, 05482

Denatured Ethanol

DANGER!

EXTREMELY FLAMMABLE. VAPORS MAY EXPLODE. CAUSES SEVERE EYE IRRITATION. OVEREXPOSURE TO VAPORS CAN CAUSE CNS DEPRESSION. ASPIRATION HAZARD IF SWALLOWED - CAN ENTER LUNGS AND CAUSE DAMAGE. CONTAINS BENZENE WHICH IS A CANCER HAZARD - LINKED TO DEVELOPMENT OF ACUTE MYELOGENOUS LEUKEMIA. LONG-TERM EXPOSURE TO GASOLINE VAPORS HAS CAUSED CANCER IN LABORATORY ANIMALS. The following organs and/or organ systems may be damaged by overexposure to this material and/or its components.

MAY CAUSE DAMAGE TO: Cardiovascular System, Blood/Blood Forming Organs, Kidney, Liver

Refer to Section 11, Toxicological Information, for specific information on the following effects: **Developmental Toxicity, Genotoxicity**

Precautionary Measures:

Avoid heat, sparks, open flames and other ignition sources. Avoid breathing of vapors, fumes, or mist. Do not take internally. Use only with adequate ventilation. Keep container closed when not in use. Wash thoroughly after handling.

FIRST AID

Inhalation: Move victim to fresh air and provide oxygen if breathing is difficult. Get medical attention. DO NOT attempt to rescue victim unless proper respiratory protection is worn. If the victim has difficulty breathing or tightness of the chest. is dizzy, vomiting or unresponsive, give 100% oxygen with rescue breathing or CPR as required and transport to the nearest medical facility.

Skin Contact: Flush exposed area with water and follow by washing with soap if available. If redness, swelling, pain and/or blisters occur, transport to the nearest medical facility for additional treatment.

Eye Contact: Immediately flush eyes with large amounts of water for at least 30 minutes, by the clock, while holding eyelids open. Transport to nearest medical facility for additional treatment.

Ingestion: DO NOT take internally. Do NOT induce vomiting. If vomiting occurs spontaneously, keep head below hips to prevent aspiration of liquid into lungs. Get medical attention. Have victim rinse mouth out with water, then drink sips of water to remove taste from mouth. In general no treatment is necessary unless large quantities are swallowed, however. get medical advice.

FIRE

In case of fire, Use water fog, foam, dry chemical or carbon dioxide (CO2) to extinguish flames. Do not use a direct stream of water. Material will float and can be re-ignited on surface of water.

SPILL OR LEAK

Dike and contain spill.

FOR LARGE SPILLS: Remove with vacuum truck or pump to storage/salvage vessels.

FOR SMALL SPILLS: Soak up residue with an absorbent such as clay, sand or other suitable material. Place in

MSDS# 5708MU Denatured Ethanol Page: 11 of 13

Shell/Motiva 0008425

non-leaking container and seal tightly for proper disposal.

CONTAINS: Ethanol, 64-17-5; Unleaded Gasoline, Mixture; Toluene, 108-88-3; Xylene, mixed isomers, 1330-20-7; Benzene, 71-43-2; Ethyl Benzene, 100-41-4; Miscellaneous Hydrocarbons,

NFPA Rating (Health, Fire, Reactivity): 1, 3, 0

TRANSPORTATION

US Department of Transportation Classification

Proper Shipping Name:

Alcohols, N.O.S.

Technical Names (s):

Ethanol, Petroleum Distillate

Identification Number:

UN1987

Hazard Class/Division:

3 (Flammable Liquid)

Packing Group:

-11

Marine Pollutant % of Total:

Marine Pollutant: Marine Polluntant based on the presence of >10% hydrocarbons listed in 49 CFR 172.101, appendix B; main constituents Trimethylbenzene and Naphthalene.

Emergency Response Guide #127

California Safe Drinking Water and Toxic Enforcement Act (Proposition 65).

WARNING: This product contains a chemical(s) known to the State of California to cause cancer.

WARNING: This product contains a chemical(s) known to the State of California to cause birth defects or other reproductive harm.

CAUTION: Misuse of empty containers can be hazardous. Empty containers can be hazardous if used to store toxic, flammable, or reactive materials. Cutting or welding of empty containers might cause fire, explosion or toxic fumes from residues. Do not pressurize or expose to open flames or heat. Keep container closed and drum bungs in place.

Name and Address

Motiva Enterprises LLC P.O. Box 4540 Houston, TX 77210-4540

ADMINISTRATIVE INFORMATION

MANUFACTURER ADDRESS: Motiva Enterprises LLC, P.O. Box 4540, Houston, TX. 77210-4540

THE INFORMATION CONTAINED IN THIS DATA SHEET IS BASED ON THE DATA AVAILABLE TO US AT THIS TIME, AND IS BELIEVED TO BE ACCURATE BASED UPON THAT: IT IS PROVIDED INDEPENDENTLY OF ANY SALE OF THE PRODUCT, FOR PURPOSE OF HAZARD COMMUNICATION. IT IS NOT INTENDED TO CONSTITUTE PRODUCT PERFORMANCE INFORMATION, AND NO EXPRESS OR IMPLIED WARRANTY OF ANY KIND IS MADE WITH RESPECT TO THE PRODUCT, UNDERLYING DATA OR THE INFORMATION CONTAINED HEREIN. YOU ARE URGED TO OBTAIN DATA SHEETS FOR ALL PRODUCTS YOU BUY, PROCESS, USE OR DISTRIBUTE, AND ARE ENCOURAGED TO ADVISE THOSE WHO MAY COME IN CONTACT WITH SUCH PRODUCTS OF THE INFORMATION CONTAINED HEREIN.

Denatured Ethanol

MSDS# 5708MU

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TO DETERMINE THE APPLICABILITY OR EFFECT OF ANY LAW OR REGULATION WITH RESPECT TO THE PRODUCT, YOU SHOULD CONSULT WITH YOUR LEGAL ADVISOR OR THE APPROPRIATE GOVERNMENT AGENCY. WE WILL NOT PROVIDE ADVICE ON SUCH MATTERS, OR BE RESPONSIBLE FOR ANY INJURY FROM THE USE OF THE PRODUCT DESCRIBED HEREIN. THE UNDERLYING DATA, AND THE INFORMATION PROVIDED HEREIN AS A RESULT OF THAT DATA, IS THE PROPERTY OF MOTIVA ENTERPRISES LLC AND IS NOT TO BE THE SUBJECT OF SALE OR EXCHANGE WITHOUT THE EXPRESS WRITTEN CONSENT OF MOTIVA ENTERPRISES LLC.

44322-12060-100R-01/04/2006

Denatured Ethanol

MSDS# 5708MU



Safety Data Sheet

HiTEC 6591S Fuel Additive

MSDS no.

H6591S

HiTEC is a trademark owned by Afton Chemical Corporation or one of its subsidiaries.

Product and company identification

Product use

Petrochemical industry: Fuel additive.

Date of issue/Revisions

17 November 2010

In case of emergency - Chemical

+1-800-403-0044 (US & Canada)

+1-804-648-7727 (International)

+32-2-507-20-64 (Europe)

+81 345 789 341 (Japan)

+65 3158-1074 (Asia Pacific)

+86 10 5100 3039 (China)

+61 2801 44558 (Australia)

Manufacturer / Supplier

Afton Chemical Corporation

500 Spring St.

Richmond, VA 23219

Telephone number: +1-804-788-5800

Afton Chemical Limited Euro-Tech Centre

London Road, Bracknell, Berkshire

RG12 2UW, England

Telephone Number: +44 1344 304141 msds@aftonchemical.com

In Singapore:

Afton Chemical Asia Pte. Ltd.

111 Somerset Road

#09-05

TripleOne Somerset

Singapore 238164

Telephone number: +65 3732 0822

Fax: +65 3737 4123

2. Hazards identification

Notice to reader

Afton operates a world-wide system for hazard communication. Some hazards shown in Section 2 may apply to non-EU countries and may not result in classification and labeling in the EU. Please see Sections 3 and 15 for country specific classification information, and Section 11 for additional details.

Europe: The product is classified as dangerous according to Directive 1999/45/EC and its amendments.

Australia: HAZARDOUS SUBSTANCE. DANGEROUS GOODS.

Primary hazards and critical effects

: Warning.

CAUSES RESPIRATORY TRACT, EYE AND SKIN IRRITATION.

Physical/chemical hazards

: COMBUSTIBLE. - United States and Canada

FLAMMABLE. - European Union VAPOR MAY CAUSE FLASH FIRE.

Environmental hazards

: Toxic to aquatic organisms. May cause long-term adverse effects in the aquatic environment.

Hazardous Material Information System (U.S.A.)

Health 1
Fire hazard 2
Reactivity 0

3. Composition/information on ingredients

Note: see section 8 for occupational exposure limits and section 11 for LC50/LD50 information

Substance/Preparation

: Preparation

Ingredient name

CAS no.

Conc. (% w/w) EU Classification

<u>WHMIS</u> Regulated? 91-20-3

4. First aid measures

Inhalation

Naphthalene

: If inhaled, remove to fresh air. If not breathing, give artificial respiration. If breathing is difficult, give oxygen. Get medical attention immediately.

0.1 - 0.5

Carc. Cat. 3; R40

Xn; R22 N; R50/53 Yes.

Ingestion

: If affected person is fully conscious, give one glass of water to drink. Never give anything by mouth to an unconscious person. Get medical attention if symptoms appear.

Skin contact

: In case of contact, immediately flush skin with plenty of water for at least 15 minutes while removing contaminated clothing and shoes. Get medical attention immediately.

Eye contact

: In case of contact, immediately flush eyes with plenty of water for at least 15 minutes. Get medical attention immediately.

5. Fire-fighting measures

Extinguishing media

: In case of fire, use water spray (fog), foam, dry chemical or CO2.

Fire-fighting procedures

: Fire-fighters should wear positive pressure self-contained breathing apparatus (SCBA) and full turnout

Fire/explosion hazards

: COMBUSTIBLE. - United States and Canada FLAMMABLE. - European Union

VAPOR MAY CAUSE FLASH FIRE. Vapors may accumulate in low or confined areas or travel a considerable distance to a source of ignition and flash back. Runoff to sewer may create fire or explosion

Hazardous decomposition products

Decomposition products may include the following materials:

carbon dioxide carbon monoxide

Flash point

: Closed cup: 44°C (111.2°F) [Pensky-Martens. Closed cup]

6. Accidental release measures

Personal precautions

: Immediately contact emergency personnel. Eliminate all ignition sources. Keep unnecessary personnel away. Use suitable protective equipment (section 8). Follow all fire-fighting procedures (section 5). Do not touch or walk through spilled material.

Environmental precautions and clean-up methods

If emergency personnel are unavailable, contain spilled material. For small spills, add absorbent (soil may be used in the absence of other suitable materials) and use a non-sparking or explosion-proof means to transfer material to a sealable, appropriate container for disposal. For large spills, dike spilled material or otherwise contain material to ensure runoff does not reach a waterway. Place spilled material in an appropriate container for disposal. Avoid contact of spilled material with soil and prevent runoff entering surface waterways.

Note: see section 1 for emergency contact information and section 13 for waste disposal.

7. Handling and storage

Handling

Avoid contact with eyes, skin and clothing. Keep container closed. Use only with adequate ventilation. Avoid breathing vapor or mist. Keep away from heat, sparks and flame. To avoid fire or explosion, dissipate static electricity during transfer by grounding and bonding containers and equipment before transferring material. Use explosion-proof electrical (ventilating, lighting and material handling) equipment. Wash thoroughly after handling.

Storage

Keep container in a well-ventilated area. Keep container tightly closed and sealed until ready for use. Avoid all possible sources of ignition (spark or flame).

8. Exposure controls/personal protection

Engineering controls

Provide exhaust ventilation or other engineering controls to keep the airborne concentrations of vapors below their respective threshold limit value.

Personal protective equipment

Respiratory system

: Use appropriate respiratory protection if there is the potential to exceed the exposure limit(s).

Skin and body

• Where contact is likely, wear chemical resistant gloves, a chemical resistant suit, and boots. Additional body garments should be used based upon the task being performed.

Hands

: Hand Protection: Wear chemical resistant gloves. Nitrile gloves of minimum thickness 0.4 mm have an expected breakthrough time of 30 minutes or less when in frequent contact with the product. Due to variable exposure conditions the user must consider that the practical use of a chemical-protective glove in practice may be much shorter than the permeation time above. Manufacturer's directions for use, especially about the minimum thickness and the minimum breakthrough time, must be observed. This information does not replace suitability tests by the end user since glove protection varies depending on the conditions under which the product is used.

Eves

: Safety goggles are considered minimum protection. Goggles with a face shield may be necessary depending on quantity of material and conditions of use.

Occupational exposure limits

Ingredient name	OEL United States	OEL Canada	OEL Europe	OEL Australia
1) Benzene, 1,2,4-trimethyl-	ACGIH (United States, 1999).	(Canada).	EH40 (UK) (Europe).	ACGIH (United States, 1999).
	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm
2) Benzene, 1,3,5-trimethyl-	ACGIH (United States, 1999).	(Canada).	EH40 (UK) (Europe).	ACGIH (United States, 1999).
	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm
3) Xylene	ACGIH (United States, 1996).	(Canada).	EH40 (UK) (Europe, 2002). Absorbed	NOHSC (Australia, 2003).
	TWA: 100 ppm	TWA: 100	through skin. TWA: 50 ppm	STEL: 80 ppm
	STEL: 150 ppm OSHA (United States). TWA: 100 ppm	STEL: 150	8 hour(s). STEL: 100 ppm 15 minute(s).	15 minute(s).
4) Cumene	ACGIH (United States, 1994). Absorbed through skin.	(Canada). Absorbed through skin.	EH40 (UK) (Europe). Absorbed through skin.	NOHSC (Australia, 2003). Absorbed through skin.
	TWA: 50 ppm	TWA: 50 ppm	TWA: 25 ppm 8 hour(s).	TWA: 25 ppm 8 hour(s).
	OSHA (United States, 1989). Absorbed through skin. TWA: 50 ppm		EH40 (UK) (Europe, 2002). Absorbed through skin. TWA: 125 mg/m³ 8 hour(s). STEL: 250 mg/m³ 15 minute(s).	STEL: 75 ppm 15 minute(s).
5) Benzene, 1,2,3-trimethyl-	ACGIH (United States, 1999). TWA: 25 ppm	(Canada). TWA: 25 ppm	ACGIH (United States, 1999).	ACGIH (United States, 1999).
6) Naphthalene	ACGIH TLV (United States). Absorbed through skin. TWA: 10 ppm STEL: 15 ppm OSHA PEL (United States).	ACGIH TLV (United States). Absorbed through skin. TWA: 10 ppm STEL: 15 ppm	TWA: 25 ppm ACGIH TLV (United States). Absorbed through skin. TWA: 10 ppm STEL: 15 ppm	TWA: 25 ppm ACGIH TLV (United States). Absorbed through skin. TWA: 10 ppm STEL: 15 ppm

TWA: 10 ppm

9. Physical and chemical properties

Physical state and Appearance : Liquid.

Colors

Color : Clear. Light Amber.

Density : Not determined.

Specific gravity : 0.9151 @ 15.6°C

Viscosity : 19 cSt at 40°C

Auto-ignition temperature : Not determined

Flash point : Closed cup: 44°C (111.2°F) [Pensky-Martens. Closed cup]

10. Stability and reactivity

Stability : The product is stable.

Materials to avoid : Strong oxidizing and reducing agents.

Conditions to avoid : High temperatures, sparks, and open flames.

11. Toxicological information

Routes of entry : Skin, Eyes, Ingestion, and Inhalation.

Target organs: Contains material which may cause damage to the following organs: blood, kidneys, lungs, liver, heart,

gastrointestinal tract, upper respiratory tract, immune system, skin, eyes, central nervous system (CNS).

Acute effects

Inhalation : Irritating to respiratory system.

Ingestion

Ingestion may cause gastrointestinal irritation and diarrhea.

Skin contact : Irritating to skin.

Eye contact : Irritating to eyes.

Adverse effects : - Adverse symptoms may include the following:: In the presence of slight maternal toxicity, fetotoxic effects have been observed in the offspring of rats exposed by inhalation to Solvent Naphtha (petroleum) light aromatic.

- Adverse symptoms may include the following:: This product contains trimethylbenzene. Literature data indicate

that long-term inhalation exposure causes blood effects in laboratory animals.

- Adverse symptoms may include the following:: Central nervous system, liver, kidneys, and blood effects by inhalation and heart beat irregularity (arrythmia) and heart beat - increase. High exposures to xylene in some animal studies, often at levels toxic to the mother, affected embryo/fetal development. The significance of this finding to humans is not known. Xylene vapour has caused occupational skin sensitization in humans.

- Adverse symptoms may include the following:: liver, kidneys, lungs, and heart effects by dermal route and immune system effects by ingestion route. Not a developmental toxicant when administered dermally. Weak

carcinogenic liver response was observed in mice, but not rats.

Product/ingredient name	ACGIH	IARC	EPA	NIOSH	NTP	OSHA	EU	
Xvlene	Δ4	_	_	_	_	_	_	

Toxicity data

Product/ingredient name Solvent naphtha (petroleum), light aromatic	Result LD50 Oral LD50 Oral LD50 Oral	Species Rat Rat Rat	Dose 8400 mg/kg 5000 mg/kg 2900 mg/kg	Exposure - -
Benzene, 1,2,4-trimethyl-	LD50 Dermal LD50 Oral LD50 Oral	Rabbit Rat Rat	3160 mg/kg 5000 mg/kg 3400 to 6000 mg/kg	- -
	LC50 Inhalation Vapor	Rat	18000 mg/m³	4 hours
Benzene, 1,3,5-trimethyl-	LC50 Inhalation Vapor	Rat	24000 mg/m ³	4 hours
N-Propylbenzene Xylene	LD50 Oral LD50 Dermal LD50 Oral LC50 Inhalation	Rat Rabbit Rat Rat	6040 mg/kg >14100 mg/kg 4300 mg/kg 5000 to 8500	- - - 4 hours
Cumene	Vapor LD50 Dermal LD50 Oral	Rabbit Mouse Rat	ppm 10578 mg/kg 12750 mg/kg 1400 mg/kg	-

HiTEC 6591S Fuel Additive	In Case of Emerger 507-20-64 (Eu)	1CY +7-8UU-4U3-	-0044 (US/Canada) +1-80	14-648-1121 (INTI) †3	Z-Z- Page: 5//
	LC50 Inhalation Vapor	Rat	8000 ppm	4 hours	
2-Ethyl hexanol	LD50 Dermal	Rabbit	1970 mg/kg	-	
ř	LD50 Dermal	Rabbit	1700 mg/kg	-	
	LD50 Oral	Rat	2000 to 5000 mg/kg	76.	
	LD50 Oral	Mouse	2000 to 3800	**	

Guinea pig

Other information

: Not available.

12. Ecological information

: Toxic to aquatic organisms. May cause long-term adverse effects in the aquatic environment. Based on calculation.

mg/kg 1900 mg/kg

>227 ppm

6 hours

Environmental fate : This product contains components which may be persistent in the environment.

LD50 Oral

Vapor

LC50 Inhalation

13. Disposal considerations

Waste handling and disposal

: Waste must be disposed of in accordance with federal, state and local environmental control regulations.

14. Transport information

Regulatory information	UN number	Proper shipping name	Class	Packing group	Label	Additional information
DOT Classification	UN1993	Combustible liquids, n.o.s. (Xylene, Petroleum distillates)	3		<u>&</u>	-
TDG Classification	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	I	8	-
ADR/RID Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	I		Tunnel code (D/E)
IMDG Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	I		- Marine pollutant
IATA-DGR Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3			-
ADG Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	1		-

Notice to reader

The above transport information is provided to assist in the proper classification of this product and may not be suitable for all shipping conditions.

15. Regulatory information

EU regulations

Hazard symbol(s)



Irritant, Dangerous for the environment

HiTEC 6591S Fuel Additive In Case of Emergency +1-800-403-0044 (US/Canada) +1-804-648-7/27 (Intt) +32-2- Page: 6// 507-20-64 (Eu)

Risk phrases

: R10- Flammable

R36/37/38- Irritating to eyes, respiratory system and skin.

R67- Vapors may cause drowsiness and dizziness.

R51/53- Toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.

Safety phrases

: S16- Keep away from sources of ignition - No smoking.

S23- Do not breathe vapor.

S36/37/39- Wear suitable protective clothing, gloves and eye/face protection. S57- Use appropriate containment to avoid environmental contamination.

Contains

Solvent naphtha (petroleum), light aromatic

265-199-0

US regulations

SARA 313 toxic chemical notification and release reporting (w/w%)

: Benzene, 1,2,4-trimethyl-

Xylene Cumene 10 - 19.9 1 - 4.9 1 - 4.9

SARA 311/312 Hazardous Categorization

: SARA 311/312 MSDS distribution - chemical inventory - hazard identification: Fire hazard, Immediate

(acute) health hazard, Delayed (chronic) health hazard

RQ (Reportable quantity)

: CERCLA: Hazardous substances.: Xylene: 100 lbs. (45.4 kg); CUMENE: 5000 lbs. (2270 kg); Ethylbenzene: 1000 lbs. (454 kg); Naphthalene: 100 lbs. (45.4 kg); STYRENE: 1000 lbs. (454 kg); Toluene: 1000 lbs. (454 kg); Benzene: 10 lbs. (4.54 kg); P-XYLENE: 100 lbs. (45.4 kg); Acetaldehyde: 1000 lbs. (454 kg); FURAN: 100 lbs. (45.4 kg); Propylene oxide: 100 lbs. (45.4 kg); o-XYLENE: 1000 lbs. (454 kg); DI-SEC-OCTYL PHTHALATE: 100 lbs. (45.4 kg); MALEIC ANHYDRIDE: 5000 lbs. (2270 kg);

State - California Prop. 65

: This product contains the following ingredients for which the State of California has found to cause cancer, birth

defects or other reproductive harm, which would require a warning under the statute:

Naphthalene Ethylbenzene Toluene Benzene

DI(2-ETHYLHEXYL) PHTHALATE

Furan

Propylene oxide Acetaldehyde

Canadian regulations

WHMIS (Classification)

: Class B-3: Combustible liquid with a flash point between 37.8°C (100°F) and 93.3°C (200°F).

Class D-2A: Material causing other toxic effects (Very toxic). Class D-2B: Material causing other toxic effects (Toxic).

International Inventory Status

United States (TSCA) : All components are listed or exempted.

Canada : All components are listed or exempted.

Europe : All components are listed or exempted.

Japan (ENCS) : All components are listed or exempted.

Australia (NICNAS) : At least one component is not listed.

Korea (ECL) : All components are listed or exempted.

China (IECSC) : At least one component is not listed.

Philippines (PICCS) : All components are listed or exempted.

16. Other information

PREPARATION INFORMATION

Validated by HS&E Department (Tel: +1 804 788 5800) on 11/17/2010.

Date of printing

: 11/18/2010.

Indicates information that has changed from previously issued version.

Notice to reader

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ADDRESS CONTACT INFORMATION

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In Singapore: Afton Chemical Asia Pte. Ltd. 111 Somerset Road #09-05 TripleOne Somerset Singapore 238164 Telephone number: +65 3732 0822

Fax: +65 3737 4123

In Australia: Afton Chemical Asia Pacific Company Level 9, 20 Berry Street North Sydney, NSW 2060 Australia Telephone number: +61 2801 44558 Business Hours: 9:00am - 5:00pm

Full text of R-phrases appearing in section 3:

In Europe:
Afton Chemical Limited
Euro-Tech Centre
London Road, Bracknell, Berkshire
RG12 2UW, England
Telephone Number: +44 1344 304141
msds@aftonchemical.com

In Japan:
Afton Chemical Japan Corporation,
Tsukuba Technical Center
5-9-4, Tokodai, Tsukuba-shi,
Ibaraki-ken 300-2635, Japan
Telephone number: +81 29 847 1061

In China: Afton Chemical Trading (Beijing) Co., Ltd. Room 808 China World Office 2 No. 1 Jian Guo Men Wai Avenue Beijing 100004 China Telephone number: +86 10 6505 5945

: R10- Flammable.

R40-Limited evidence of a carcinogenic effect.

R20- Harmful by inhalation. R22- Harmful if swallowed.

R20/21- Harmful by inhalation and in contact with skin.

R65- Harmful: may cause lung damage if swallowed.

R37- Irritating to respiratory system.

R38- Irritating to skin.

R36/38- Irritating to eyes and skin.

R37/38- Irritating to respiratory system and skin.

R36/37/38- Irritating to eyes, respiratory system and skin.

R66- Repeated exposure may cause skin dryness or cracking.

R67- Vapors may cause drowsiness and dizziness.

R50/53- Very toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.

R51/53- Toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.

* * * END OF MSDS * * *



Safety data sheet

Keropur® AP 205 20M

Revision date: 2009/04/07 Version: 1.0

Page: 1/6

(30339574/SDS GEN US/EN)

1. Substance/preparation and company identification

Company BASE CORPORATION 100 Campus Drive Florham Park, NJ 07932 24 Hour Emergency Response Information CHEMTREC: 1-800-424-9300

BASF HOTLINE: 1-800-832-HELP

Synonyme:

Keropur AP 205 20M, Puredd AP 205 20M

2. Composition/information on ingredients

CAS Number

Content (W/W)

1330-20-7

80.46% 18.63 %

Chamical name NJTSRN 489909-5625 PC

100-41-4

3.91 %

Xylene elhylbenzene

3. Hazard Identification

Emergency overview

WARNING: COMBUSTIBLE LIQUID. CAUSES SKIN IRRITATION.

May cause initiation.
MAY CAUSE RESPIRATORY TRACT IRRITATION.

CONTAINS MATERIAL WHICH CAN CAUSE NERVOUS SYSTEM DAMAGE, CONTAINS MATERIAL WHICH CAN CAUSE LIVER DAMAGE, CONTAINS MATERIAL WHICH CAN CAUSE KIDNEY DAMAGE.

Harmful: may cause lung damage if swallowed.

Avoid contact with the skin, eyes and clothing.

Avoid inhalation of mists/vapours.

Provide local exhaust ventilation to control vapouralmists. Wear NIOSH-certified chemical goggles.

Wear chemical resistant protective gloves.

Wear protective ciothing.

Eye wash fountains and safety showers must be easily accessible.

Potential health effects

Primary routes of exposure

Routes of entry for solids and liquids include eye and skin contact, ingestion and inhalation, Routes of entry for gases include inhalation and eye contact. Skin contact may be a route of entry for liquified gases.

Acute toxicity:

Information on: Xylene

Aspiration of xylene may result in chemical preumonitis, pulmonary edema and hemontrage, ingestion and skin absorption may lead to CNS depression, symptoms may include neusea, dizziness and blurred vision.

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(30339574/SDS_GEN_US/EN)

irritation:

Information on: Xylene

Eye contact with xylene may result in reversible demage, and demaditis may result from skin contact.

Repeated dose toxicity:

Information on: Xylene

The chronic effects of overexposure to xylene include possible liver and kitney demage. A mixture of o, m, and p-xylenes was tereloganic and embryo toxic to mice by the oral route; however, these effects were accompanied by maternal toxicity. Rats exposed to 1000 mg/m3 by inhalation exhibited no teratogenic effects; however, minor skeletal abnormalities occurred.

4. First-ald measures

General advice:

Remove contaminated clothing.

f inhaled:

Keep patient calm, remove to fresh air. Assist in breathing if necessary. Seek medical attention if necessary.

li on skin;

Wash affected areas thoroughly with soap and water. Seek medical attention.

If in ayes:

in case of contact with the eyes, rinse immediately for at teast 15 minutes with plenty of water. If imitation develops, seek medical attention.

if swallowed

immediately rinse mouth and then drink plenty of water, do not induce vomiting, seek medical attention.

Never induce vomiting or give anything by mouth if the victim is unconscious or having convulsions. Seek medical attention.

5. Fire-fighting measures

Flash point:

31.1 °0

(ASTM 093)

Hazarda during fire-fighting:

Irritant gases/vapours, combustible vapours

Protective equipment for fire-fighting:

Firefighters should be equipped with self-contained breathing apparatus and turn-out geer.

Further Information:

Do not allow to onler drains or waterways. Approach with extreme caution.

NFPA Hazard codes:

Healin: 2

Fire: 2

Reactivity: 0

Special

6. Accidental release measures

Personal precautions:

Use breathing apparatus if exposed to vapours/dust/serosof. Do not get in eyes, on skin, or on ciothing. Take appropriate protective measures.

Environmental precaulions:

Do not discharge into drains/surface waters/groundwater.

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Version: 1.0

(30339574/SDS_GEN_US/EN)

Cleenup:

Dispose of absorbed material in accordance with regulations.

For large amounts: Pick up with inent absorbent material (e.g. sand, earth etc.). Spills should be contained and placed in suitable containers for disposal.

Further information:

Pack in lightly closed containers for disposal.

7. Handling and storage

Hendilma

General advice:

Keep away from sources of Ignifion - No smoking. Handle and open container with care. Keep container lightly sealed.

Protection against fire and explosion:

Vapours may form ignitable mixture with air. Avoid all sources of ignition; heat, sparks, open flame. Avoid extreme heat. Empty containers may contain flammable residue. The product is combustible.

Storage

General advice:

Keep container tightly closed and dry; store in a cool place. Avoid all sources of ignition: heat, sparks, open flame.

Storage incompatibility:

General: Segregate from acids and bases. Segregate from oxidizing agents.

8. Exposure controls and personal protection

Components with workplace control parameters

Xylena

OSHA

PEL 100 ppm 435 mg/m3 ;

ethylbenzena

ACGIH OSHA TWA value 100 ppm; STEL value 150 ppm; PEL 100 ppm 435 mg/m3;

ACGIH

TWA value 100 ppm; STEL value 125 ppm;

Advice on system design:

Provide adequate exhaust ventilation to control work place concentrations.

Personal protective equipment

Hend protection:

West chemical resistant protective gloves., Consult with glove manufacturer for testing data.

Eye protection:

Tightly fitting safety gaggles (chemical gaggles).

Body protection:

Body protection must be chosen depending on activity and possible exposure, e.g. head protection, apron, protective boots, chemical-protection sult.

General eafety and hygiene measures:

Avoid prolonged and/or repeated contact with the skin. Avoid Inhalation of vapour. Do not get in eyes, on skin, or on clothing. Avoid all routes of exposure liceuring ingestion, skin absorption and inhalation. Keep away from food, drink and animal feeding stoffs. Take off immediately all contaminated dething. Handle in accordance with good industrial hygiene and safety practice.

Revision date : 2009/04/07

Version: 1.0

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(30339674/SDS_GEN_US/EN)

9. Physical and chemical properties

Ottour:

Colour:

amino-like colouriess to yellowish

pH value:

10.1

pour point Boiling point: -43 °C

165°C

(1,013 bar)

(1%(m))

Vapour pressure:

< 5 mmHg 0.8976 g/cm3 (20 °C) (15 °C) (ISO 2811-3)

Oensity: Viscosity, kinematic:

13.9 mm2/s

partly soluble

Solubility in water:

Solubility (qualifative):

sovent(s): hydrocarbons,

10. Stability and reactivity

Hazardous reactions:

The product is chemically stable.

Corresion to metale:

No corrosive effect on metal.

11. Toxicological information

Acute toxicity

LD50/rat > 2,000 mg/kg

Literature data.

Skin initation:

rabbit: irritant.

Eye irritation:

rabbit; non-initant

Chronic toxicity

Other Information:

The product has not been lested. The statements on toxicology have been derived from the properties of the individual components.

12. Ecological Information

Environmental fate and transport

Biodegradation;

Evaluation:

The product is not very soluble in water and can thus be removed from water mechanically in suitable effluent treatment plants.

Environmental toxicity

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(30339674/SDS_GEN_US/EN)

Acute and prolonged toxicity to fish: zebra fish/LC50 (98 h): 10 - 100 mg/l

Toxicity to microorganisms: bacterium/EC10 (0.5 h): 1,400 mg/l

Inhibition of dagradation activity in activated studge is not to be anticipated during correct introduction of low concentrations.

Other ecotoxicological advice:

The product has not been leated. The statements on acotoxicology have been derived from the properties of the individual components.

13. Disposal considerations

Wasia disposal of substance:

Dispose of in accordance with national, state and local regulations.

Container disposal:

WARNING: Empty containers may still contain hazardous residue.

14. Transport information

Land transport

USDOT

Hezard class:

Packing group: ID number:

III

Hazard label:

UN 1993

Proper shipping name:

FLAMMABLE LIQUIO, N.O.S. (contains XYLENE, ETHYLBENZENE)

Sea transport

IMDG

Hazard class:

Packing group:

D number. Hazard label: UN 1993

Marine pollutant:

Proper shipping name:

FLAMMABLE LIQUID, N.O.S. (contains XYLENE, ETHYLBENZENE)

Air transport IATA/ICAO

Hezard class:

Packing group: ID number:

UN 1993

Hazard label:

Proper shipping name:

FLAMMABLE LIQUID, N.O.S. (contains XYLENE, ETHYLSENZENE)

15. Regulatory Information

Federal Regulations

Registration status:

TSCA, US

released / listed

Safety data sheet

Keropur® AP 205 20M

Revision date : 2009/04/07

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Version: 1.0

(30339574/SDS_GEN_US/EN)

OSHA hazard category: IARC 1, 2A or 2B carcinogen, Chronic target organ effects reported, Acute target organ effects reported, ACGIH TLV established, Skin and/or eye intent. Combustale Liquid

SARA hazard categories (EPCRA 311/312): Acute, Chronic, Fire

SARA 313:

CAS Number 100-41-4 Chemical name

100-41-4 1330-20-7 ethylbenzene Xviene

over Aye

State regulations

State RTK

CAS Number 1330-20-7 100-41-4 Chemica) name Xylena

ethylbenzene

State RTK MA, PA MA, NJ, PA

CA Prop. 88:

THIS PRODUCT CONTAINS A CHEMICAL(S) KNOWN TO THE STATE OF CALIFORNIA TO CAUSE CANCER AND BIRTH DEFECTS OR OTHER REPRODUCTIVE HARM.

16. Other information

HMIS III rating

Health; 2a

Flammabilky: 2

Physical hazard: 0

HMIS uses a numbering scale ranging from 0 to 4 to indicate the degree of inezerd. A value of zero means that the substance possesses easentially no hezerd; a rating of four indicates high hezerd.

Local contact information prod_reg@basf.com

Keropur is a registered trademark of BASF Corporation or BASF SE IMPORTANT: WHILE THE DESCRIPTIONS, DESIGNS, DATA AND INFORMATION CONTAINED HEREIN ARE PRESENTED IN GOOD FAITH AND BELIEVED TO BE ACCURATE, IT IS PROVIDED FOR YOUR GUIDANCE ONLY. BECAUSE MANY FACTORS MAY AFFECT PROCESSING OR APPLICATION/USE, WE RECOMMEND THAT YOU MAKE TESTS TO DETERMINE THE SUITABILITY OF A PRODUCT FOR YOUR PARTICULAR PURPOSE PRIOR TO USE. NO WARRANTIES OF ANY KIND, EITHER EXPRESSED OR IMPUED, INCLUDING WARRANTIES OF MERCHANTABILITY OR FITNESS FOR A PARTICULAR PURPOSE, ARE MADE REGARDING PRODUCTS DESCRIBED OR DESIGNS, DATA OR INFORMATION MAY BE USED WITHOUT INFRINGING THE INTELLECTUAL PROPERTY RIGHTS OF OTHERS. IN NO CASE SHALL THE DESCRIPTIONS, INFORMATION, DATA OR DESIGNS PROVIDED BE CONSIDERED A PART OF OUR TERMS AND CONDITIONS OF SALE. FURTHER, YOU EXPRESSLY UNDERSTAND AND AGREE THAT THE DESCRIPTIONS, DESIGNS, DATA, AND INFORMATION FURNISHED BY BASF HEREUNDER ARE GIVEN GRATIS AND BASF ASSUMES NO OBLIGATION OR LIABILITY FOR THE DESCRIPTION, DESIGNS, DATA AND INFORMATION GIVEN OR RESULTS OBTAINED, ALL SUCH BEING GIVEN AND ACCEPTED AT YOUR RISK.



Safety Data Sheet

MSDS no.

NEMO1121

Product and company identification

Product use

Petrochemical industry: Fuel additive.

Date of issue/Revisions

NEMO 1121

19 April 2011

In case of emergency - Chemical

+1-800-403-0044 (US & Canada)

+1-804-648-7727 (International)

+32-2-507-20-64 (Europe)

+81 345 789 341 (Japan)

+65 3158-1074 (Asia Pacific)

+86 10 5100 3039 (China)

+61 2801 44558 (Australia)

Manufacturer / Supplier

Afton Chemical Corporation 500 Spring St.

Richmond, VA 23219

Telephone number: +1-804-788-5800

Afton Chemical Limited Euro-Tech Centre

London Road, Bracknell, Berkshire

RG12 2UW, England

Telephone Number: +44 1344 304141

msds@aftonchemical.com

In Singapore: Afton Chemical Asia Pte. Ltd. 111 Somerset Road #09-05 TripleOne Somerset Singapore 238164

Telephone number: +65 3732 0822

Fax: +65 3737 4123

HAZARDS IDENTIFICATION

Notice to reader

Afton operates a world-wide system for hazard communication. Some hazards shown in Section 2 may apply to non-EU countries and may not result in classification and labeling in the EU. Please see Sections 3 and 15 for country specific classification information, and Section 11 for additional details.

The product is classified as dangerous according to Directive 1999/45/EC and its amendments. Australia: HAZARDOUS SUBSTANCE, DANGEROUS GOODS.

Primary hazards and critical effects

: Warning.

CAUSES RESPIRATORY TRACT, EYE AND SKIN IRRITATION.

ASPIRATION HAZARD IF SWALLOWED.

Physical/chemical hazards

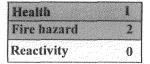
: COMBUSTIBLE. - United States and Canada

FLAMMABLE. - European Union VAPOR MAY CAUSE FLASH FIRE.

Environmental hazards

: Toxic to aquatic organisms. May cause long-term adverse effects in the aquatic environment.

Hazardous Material **Information System** (U.S.A.)



Composition/information on ingredients

Note: see section 8 for occupational exposure limits and section 11 for LC50/LD50 information

Substance/Preparation

: Preparation

Ingredient name

CAS no.

Conc. (% w/w) EU Classification

WHMIS Regulated? 64742-94-5

4. First aid measures

Inhalation

: If inhaled, remove to fresh air. If not breathing, give artificial respiration. If breathing is difficult, give oxygen. Get medical attention immediately.

0.5 - 0.99

Xn; R65

R66, R67 N; R51/53 Yes.

Ingestion : DO NOT induce vomiting. If vomit

: DO NOT induce vomiting. If vomiting occurs naturally, have victim lean forward to reduce risk of aspiration. If affected person is fully conscious, give one glass of water to drink. Never give anything by mouth to an unconscious person. Get immediate medical attention.

Skin contact : In case of contact, immediately flush skin with plenty of water for at least 15 minutes while removing contaminated

clothing and shoes. Get medical attention immediately.

Eye contact : In case of contact, immediately flush eyes with plenty of water for at least 15 minutes. Get medical attention immediately.

Solvent naphtha (petroleum), heavy aromatic

5. Fire-fighting measures

Extinguishing media: In case of fire, use water spray (fog), foam, dry chemical or CO2.

Fire-fighting procedures : Fire-fighters should wear positive pressure self-contained breathing apparatus (SCBA) and full turnout

gear.

Fire/explosion hazards : COMBUSTIBLE. - United States and Canada FLAMMABLE. - European Union

VAPOR MAY CAUSE FLASH FIRE. Vapors may accumulate in low or confined areas or travel a considerable distance to a source of ignition and flash back. Runoff to sewer may create fire or explosion

hazard.

Hazardous decomposition products : Decomposition products may include the following materials:

carbon dioxide carbon monoxide

Flash point : Closed cup: 44°C (111.2°F) [Pensky-Martens. Minimum]

6. Accidental release measures

Personal precautions: Immediately contact emergency personnel. Eliminate all ignition sources. Keep unnecessary personnel away. Use suitable protective equipment (section 8). Follow all fire-fighting procedures (section 5). Do not touch or walk through spilled material.

Environmental precautions and clean-up methods

: If emergency personnel are unavailable, contain spilled material. For small spills, add absorbent (soil may be used in the absence of other suitable materials) and use a non-sparking or explosion-proof means to transfer material to a sealable, appropriate container for disposal. For large spills, dike spilled material or otherwise contain material to ensure runoff does not reach a waterway. Place spilled material in an appropriate container for disposal. Avoid contact of spilled material with soil and prevent runoff entering surface waterways.

Note: see section 1 for emergency contact information and section 13 for waste disposal.

Handling and storage

Handling

Avoid contact with eyes, skin and clothing. Keep container closed. Use only with adequate ventilation. Avoid breathing vapor or mist. Keep away from heat, sparks and flame. To avoid fire or explosion, dissipate static electricity during transfer by grounding and bonding containers and equipment before transferring material. Use explosion-proof electrical (ventilating, lighting and material handling) equipment. Wash thoroughly after handling.

Storage

Keep container in a cool, well-ventilated area. Keep container tightly closed and sealed until ready for use. Avoid all possible sources of ignition (spark or flame).

Exposure controls/personal protection

Engineering controls

Provide exhaust ventilation or other engineering controls to keep the airborne concentrations of vapors below their respective threshold limit value.

Personal protective equipment

Respiratory system

Use appropriate respiratory protection if there is the potential to exceed the exposure limit(s).

Skin and body

Where contact is likely, wear chemical resistant gloves, a chemical resistant suit, and boots. Additional body garments should be used based upon the task being performed.

Hands

Hand Protection: Wear chemical resistant gloves. Nitrile gloves of minimum thickness 0.4 mm have an expected breakthrough time of 30 minutes or less when in frequent contact with the product. Due to variable exposure conditions the user must consider that the practical use of a chemical-protective glove in practice may be much shorter than the permeation time above. Manufacturer's directions for use, especially about the minimum thickness and the minimum breakthrough time, must be observed. This information does not replace suitability tests by the end user since glove protection varies depending on the conditions under which the product is used.

Eyes

Safety goggles are considered minimum protection. Goggles with a face shield may be necessary depending on quantity of material and conditions of use.

Occupational exposure limits

Ingredient name	OEL United States	OEL Canada	OEL Europe	OEL Australia
1) Benzene, 1,2,4-trimethyl-	ACGIH (United States, 1999).	(Canada).	EH40 (UK) (Europe).	ACGIH (United States, 1999).
	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm
2) Benzene, 1,3,5-trimethyl-	ACGIH (United States, 1999).	(Canada).	EH40 (UK) (Europe).	ACGIH (United States, 1999).
	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm	TWA: 25 ppm
3) Xylene	ACGIH (United States, 1996).	(Canada).	EH40 (UK) (Europe, 2002). Absorbed through skin.	NOHSC (Australia, 2003).
	TWA: 100 ppm	TWA: 100	TWA: 50 ppm 8 hour(s).	STEL: 80 ppm 15 minute(s).
	STEL: 150 ppm OSHA (United States). TWA: 100 ppm	STEL: 150	STEL: 100 ppm 15 minute(s).	
4) Cumene	ACGIH (United States, 1994). Absorbed through	(Canada). Absorbed through skin.	EH40 (UK) (Europe). Absorbed through skin.	NOHSC (Australia, 2003). Absorbed through skin.
4) Cumene	ACGIH (United States, 1994).	,	Absorbed through skin. TWA: 25 ppm	2003). Absorbed through skin. TWA: 25 ppm
4) Cumene	ACGIH (United States, 1994). Absorbed through skin. TWA: 50 ppm OSHA (United States, 1989). Absorbed	through śkin. TWA: 50 ppm	Absorbed through skin. TWA: 25 ppm 8 hour(s). EH40 (UK) (Europe, 2002). Absorbed	2003). Absorbed through skin.
4) Cumene	ACGIH (United States, 1994). Absorbed through skin. TWA: 50 ppm	through śkin. TWA: 50 ppm	Absorbed through skin. TWA: 25 ppm 8 hour(s). EH40 (UK) (Europe, 2002). Absorbed through skin. TWA: 125 mg/m³ 8 hour(s).	2003). Absorbed through skin. TWA: 25 ppm 8 hour(s). STEL: 75 ppm
4) Cumene	ACGIH (United States, 1994). Absorbed through skin. TWA: 50 ppm OSHA (United States, 1989). Absorbed through skin.	through śkin. TWA: 50 ppm	Absorbed through skin. TWA: 25 ppm 8 hour(s). EH40 (UK) (Europe, 2002). Absorbed through skin. TWA:	2003). Absorbed through skin. TWA: 25 ppm 8 hour(s). STEL: 75 ppm
4) Cumene 5) Benzene, 1,2,3-trimethyl-	ACGIH (United States, 1994). Absorbed through skin. TWA: 50 ppm OSHA (United States, 1989). Absorbed through skin.	through śkin. TWA: 50 ppm	Absorbed through skin. TWA: 25 ppm 8 hour(s). EH40 (UK) (Europe, 2002). Absorbed through skin. TWA: 125 mg/m³ 8 hour(s). STEL:	2003). Absorbed through skin. TWA: 25 ppm 8 hour(s). STEL: 75 ppm

Physical and chemical properties

Physical state and Appearance: Liquid.

Specific gravity

Density

Not determined.

Viscosity

0.9193 @ 15.6C

Auto-ignition temperature

: 15.6 cSt at 40°C Not determined.

10. Stability and reactivity

Stability

: The product is stable.

Materials to avoid

: Strong oxidizing and reducing agents.

Conditions to avoid

High temperatures, sparks, and open flames.

11. Toxicological information

Routes of entry

: Skin, Eyes, Ingestion, and Inhalation.

Target organs

Contains material which may cause damage to the following organs: blood, kidneys, lungs, liver, heart, gastrointestinal tract, upper respiratory tract, immune system, skin, eyes, central nervous system (CNS).

Acute effects

Inhalation

: Irritating to respiratory system.

Ingestion

: Aspiration hazard if swallowed. Can enter lungs and cause damage. Does not meet EU R65 classification

criteria

Ingestion may cause gastrointestinal irritation and diarrhea.

Skin contact

: Irritating to skin.

Eye contact

Irritating to eyes.

Adverse effects

- Adverse symptoms may include the following:: In the presence of slight maternal toxicity, fetotoxic effects have been observed in the offspring of rats exposed by inhalation to Solvent Naphtha (petroleum) light aromatic.

- Adverse symptoms may include the following:: This product contains trimethylbenzene. Literature data indicate

that long-term inhalation exposure causes blood effects in laboratory animals.

- Adverse symptoms may include the following:: Central nervous system, liver, kidneys, and blood effects by inhalation and heart beat irregularity (arrythmia) and heart beat - increase. High exposures to xylene in some animal studies, often at levels toxic to the mother, affected embryo/fetal development. The significance of this finding to humans is not known. Xylene vapour has caused occupational skin sensitization in humans. When exposed to 1800 ppm Xylene vapor, rats experienced hearing deficits to mid-frequency range tones.

- Adverse symptoms may include the following:: liver, kidneys, lungs, and heart effects by dermal route and immune system effects by ingestion route. Not a developmental toxicant when administered dermally. Weak

carcinogenic liver response was observed in mice, but not rats.

Product/ingredient name	ACGIH	IARC	EPA	NIOSH	NTP	OSHA	EU
Xylene	A4	-	-	-	-	-	-

Toxicity data

Product/ingredient name	Result	Species	Dose	Exposure
Solvent naphtha (petroleum), light aromatic	LD50 Oral	Rat	8400 mg/kg	-
	LD50 Oral	Rat	5000 mg/kg	-
	LD50 Oral	Rat	2900 mg/kg	-
Polyether polyol	LD50 Dermal	Rabbit	>2000 mg/kg	_
• •	LD50 Oral	Rat	>5000 mg/kg	-
Benzene, 1,2,4-trimethyl-	LD50 Dermal	Rabbit	3160 mg/kg	-
•	LD50 Oral	Rat	5000 mg/kg	_
	LD50 Oral	Rat	3400 to 6000	_
			mg/kg	
	LC50 Inhalation	Rat	18000 mg/m³	4 hours
	Vapor		· ·	
Benzene, 1,3,5-trimethyl-	LC50 Inhalation	Rat	24000 mg/m ³	4 hours
•	Vapor		Ü	
N-Propylbenzene	LD50 Oral	Rat	6040 mg/kg	-
Xylene	LD50 Dermal	Rabbit	>14100 mg/kg	-
	LD50 Oral	Rat	4300 mg/kg	- ·
	LD50 Oral	Rat - Male	3523 mg/kg	-
	LC50 Inhalation	Rat	5000 to 8500	4 hours
	Vapor		ppm	
2-Ethyl hexanol	LD50 Dermal	Rabbit	1970 mg/kg	-
	LD50 Dermal	Rabbit	1700 mg/kg	-
	LD50 Oral	Rat	2000 to 5000	_
			mg/kg	
	LD50 Oral	Mouse	2000 to 3800	-
			mg/kg	
	LC50 Inhalation	Rat	>227 ppm	6 hours
	Vapor			
Cumene	LD50 Dermal	Rabbit	10578 mg/kg	-
	LD50 Oral	Mouse	12750 mg/kg	-

NEMO 1121

LC50 Inhalation Vapor Rat

8000 ppm

4 hours

Other information

: Not available.

12. Ecological information

Environmental hazards

: Toxic to aquatic organisms. May cause long-term adverse effects in the aquatic environment. Based on calculation.

Environmental fate

This product contains components which may be persistent in the environment.

13. Disposal considerations

Waste handling and disposal

: Waste must be disposed of in accordance with federal, state and local environmental control regulations.

14. Transport information

Regulatory information	UN number	Proper shipping name	Class	Packing group	Label	Additional information
DOT Classification	NA1993	Combustible liquids, n.o.s. (Xylene, Petroleum distillates)	Combustible liquid.	III		
TDG Classification	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	III	3	-
ADR/RID Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	III		Hazard identification number 30
						Special provisions 640 (E)
						Tunnel code (D/E)
IMDG Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	III		- Marine pollutant
IATA-DGR Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3	Ш		-
ADG Class	UN1993	Flammable liquid, n.o.s. (Xylene, Petroleum distillates)	3			-

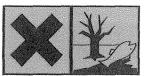
Notice to reader

The above transport information is provided to assist in the proper classification of this product and may not be suitable for all shipping conditions.

15. Regulatory information

EU regulations

Hazard symbol(s)



Irritant, Dangerous for the environment

Risk phrases

: R10- Flammable.

R36/37/38- Irritating to eyes, respiratory system and skin.

R67- Vapors may cause drowsiness and dizziness.

R51/53- Toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.

Safety phrases

S16- Keep away from sources of ignition - No smoking.

S23- Do not breathe vapor.

S36/37/39- Wear suitable protective clothing, gloves and eye/face protection. S57- Use appropriate containment to avoid environmental contamination.

Contains

NEMO 1121

Solvent naphtha (petroleum), light aromatic

265-199-0

Additional warning phrases : Contains Butanedioic acid, (tetrapropenyl)-. May produce an allergic reaction.

US regulations

SARA 313 toxic chemical notification and release reporting (w/w%)

: Benzene, 1,2,4-trimethyl-

10 - 19.9 Xylene 1 - 4.9Cumene 1 - 4.9

SARA 311/312 Hazardous Categorization

SARA 311/312 MSDS distribution - chemical inventory - hazard identification: Fire hazard, Immediate (acute) health hazard, Delayed (chronic) health hazard

RQ (Reportable quantity)

CERCLA: Hazardous substances.: Xylene: 100 lbs. (45.4 kg); CUMENE: 5000 lbs. (2270 kg); Ethylbenzene: 1000 lbs. (454 kg); Naphthalene: 100 lbs. (45.4 kg); STYRENE: 1000 lbs. (454 kg); Toluene: 1000 lbs. (454 kg); Benzene: 10 lbs. (4.54 kg); P-XYLENE: 100 lbs. (45.4 kg); o-XYLENE: 1000 lbs. (454 kg); Acetaldehyde: 1000 lbs. (454 kg); Acetaldehyd lbs. (454 kg); FURAN: 100 lbs. (45.4 kg); Propylene oxide: 100 lbs. (45.4 kg); MALEIC ANHYDRIDE: 5000 lbs. (2270 kg);

State - California Prop. 65

This product contains the following ingredients for which the State of California has found to cause cancer, birth defects or other reproductive harm, which would require a warning under the statute:

Naphthalene Ethylbenzene Toluene Benzene Furan

Propylene oxide Acetaldehyde

EPA Significant New Use Rule (SNUR)

: Polyolefin alkyl phenol alkyl amine

United States - TSCA 5(a)2 - Proposed significant new use rules

Canadian regulations

WHMIS (Classification)

Class B-3; Combustible liquid with a flash point between 37.8°C (100°F) and 93.3°C (200°F).

Class D-2B: Material causing other toxic effects (Toxic).

International Inventory Status

United States inventory (TSCA

: All components are listed or exempted.

Canada inventory Europe inventory

: All components are listed or exempted. : All components are listed or exempted.

Japan inventory (ENCS)

All components are listed or exempted.

Australia inventory (AICS)

: All components are listed or exempted. All components are listed or exempted.

Korea inventory (KECI) China inventory (IECSC)

All components are listed or exempted.

Philippines inventory (PICCS)

: All components are listed or exempted.

16. Other information

PREPARATION INFORMATION

Validated by HS&E Department (Tel: +1 804 788 5800) on 4/19/2011.

Date of printing

: 4/19/2011.

Indicates information that has changed from previously issued version.

This information and these recommendations are offered in good faith and believed to be correct as of the date hereof. Information and recommendations are supplied upon the condition that the recipients will make their own decision as to safety and suitability for their purposes. No representations or warranties, either expressed or implied, of merchantability, fitness for a particular purpose, or of any other nature, are made with respect to the product or the information and recommendations. Afton makes no representation as to completeness or accuracy. In no event will Afton be responsible for damages of any nature whatsoever resulting from the use or reliance upon the information and recommendations.

ADDRESS CONTACT INFORMATION

In the United States and Canada: Afton Chemical Corporation 500 Spring St. Richmond, VA 23219 Telephone number: +1-804-788-5800

In Singapore:
Afton Chemical Asia Pte. Ltd.
111 Somerset Road
#09-05
TripleOne Somerset
Singapore 238164
Telephone number: +65 3732 0822
Fax: +65 3737 4123

In Australia: Afton Chemical Asia Pacific Company Level 9, 20 Berry Street North Sydney, NSW 2060 Australia Telephone number: +61 2801 44558

Business Hours: 9:00am - 5:00pm

Full text of R-phrases appearing in section 3:

In Europe:
Afton Chemical Limited
Euro-Tech Centre
London Road, Bracknell, Berkshire
RG12 2UW, England
Telephone Number: +44 1344 304141
msds@aftonchemical.com

In Japan:
Afton Chemical Japan Corporation,
Tsukuba Technical Center
5-9-4, Tokodai, Tsukuba-shi,
Ibaraki-ken 300-2635, Japan
Telephone number: +81 29 847 1061

In China: Afton Chemical Trading (Beijing) Co., Ltd. Room 808 China World Office 2 No. 1 Jian Guo Men Wai Avenue Beijing 100004 China Telephone number: +86 10 6535 0000

: R10- Flammable.

R20- Harmful by inhalation.

R20/21- Harmful by inhalation and in contact with skin. R65- Harmful: may cause lung damage if swallowed.

R37- Irritating to respiratory system.

R38- Irritating to skin.

R36/38- Irritating to eyes and skin.

R37/38- Irritating to respiratory system and skin. R36/37/38- Irritating to eyes, respiratory system and skin.

R66- Repeated exposure may cause skin dryness or cracking.

R67- Vapors may cause drowsiness and dizziness.

R51/53- Toxic to aquatic organisms, may cause long-term adverse effects in the aquatic environment.

* * * END OF MSDS * * *

MATERIAL SAFETY DATA SHEET

MSDS Number: 400454M - 1

24 Hour Emergency Assistance: CHEMTEL

(877) 276-7283

General Assistance Number: (877)

276-7285

SECTION 1

PRODUCT IDENTIFICATION

MATERIAL IDENTITY: RBOB - Sewaren

COMPANY ADDRESS: Motiva Enterprises, LLC, P.O. Box 4540, Houston, TX. 77210-4540

SECTION 2 PRODUCT/INGREDIENTS CAS# CONCENTRATION **INGREDIENTS** Gasoline (Conventional, CARB and RFG) Mixture 100 %volume Miscellaneous Hydrocarbons Mixture 0 - 50 %volume 1330-20-7 0 - 25 %volume Xylene, mixed isomers Toluene 108-88-3 0 - 25 %volume 1,2,4-Trimethyl Benzene (Pseudocumene) 95-63-6 0-5 %volume Styrene 100-42-5 0-4 %volume 71-43-2 0 - 4 %volume Benzene Ethyl Benzene 100-41-4 0-3 %volume 110-54-3 0 - 3 %volume Hexane Cyclohexane 110-82-7 0 - 1 %volume Naphthalene 91-20-3 0 - 1 %volume Methyl Tert-Butyl Ether (MTBE) 1634-04-4 0 - 15 %volume Ethyl Tert-Butyl Ether (ETBE) 637-92-3 0 - 18.5 %volume Tert-Amyl Methyl Ether (TAME) 994-05-8 0 - 18.6 %volume Diisoproply Ether (DIPE) 108-20-3 0-2 %volume

NOTE: Content of Gasoline components will vary; Individual components may be present from trace amounts up to the maximum shown.

SECTION 3

HAZARDS IDENTIFICATION

EMERGENCY OVERVIEW

Appearance & Odor: Bronze color, clear & bright liquid. Hydrocarbon odor.

Health Hazards: May be harmful or fatal if swallowed. Do not induce vomitting. May cause aspiration pneumonitis. May cause CNS depression.

Physical Hazards: Material is extremely flammable and heavier than air. Vapors may travel across the ground and reach remote ignition sources causing a flashback fire danger.

NFPA Rating (Health, Fire, Reactivity): 1, 3, 0

Hazard Rating: Least - 0 Slight - 1 Moderate - 2 High - 3 Extreme - 4

Inhalation:

May cause irritation to the nose, throat and respiratory tract. Breathing of high vapor concentrations may cause CNS depression, evidenced by dizziness, light-headedness, headache, nausea, drowsiness, and loss of

coordination. Continued inhalation may result in unconsciousness.

Eve Irritation:

May be irritating to the eyes causing a burning sensation, redness, swelling and/or blurred vision.

Skin Contact:

May be irritating to the skin causing a burning sensation, redness and/or swelling. Prolonged or repeated skin contact can cause defatting and drying of the skin which may result in a burning sensation and a dried, cracked appearance.

Ingestion:

This material may be harmful or fatal if swallowed. Ingestion may result in vomiting; aspiration (breathing) of vomitus into lungs must be avoided as even small quantities may result in aspiration pneumonitis. Generally considered to have a low order of acute oral toxicity.

Other Health Effects:

Carcinogenic in animal tests. Gasoline has been tested by API in a long-term inhalation test in mice and rats. There was an increased incidence of liver cancer in female mice. Male rats had a dose related increase in kidney tumors. This effect was due to formation of alpha-2u-globulin in the rats. This material is not formed in humans and is therefore not considered relevant. It is probable that the material causes cancer in laboratory animals. Material may adversely effect male reproductive performance based on testing in laboratory animals.

This material and/or components may cause the following effects: Developmental Toxicity, Genotoxicity, Immunotoxicity, Reproductive Toxicity

Primary Target Organs:

The following organs and/or organ systems may be damaged by overexposure to this material and/or its components.

Cardiovascular System, Blood/Blood Forming Organs, Kidney, Liver, Nervous System

Signs and Symptoms:

Irritation as noted above. Aspiration pneumonitis may be evidenced by coughing, labored breathing and cyanosis (bluish skin); in severe cases death may occur. Damage to blood-forming organs may be evidenced by: a) easy fatigability and pallor (RBC), b) decreased resistance to infection (WBC effect), c) excessive bruising and bleeding (platelet effect). Kidney damage may be indicated by changes in urine output or appearance, pain upon urination or in the lower back or general edema (swelling from fluid retention). Liver damage may be indicated by loss of appetite, jaundice (yellowish skin and eye color), fatigue and sometimes pain and swelling in the upper right abdomen.

For additional health information, refer to section 11.

SECTION 4

FIRST AID MEASURES

Inhalation:

Move victim to fresh air and provide oxygen if breathing is difficult. Get medical attention. If the victim has difficulty breathing or tightness of the chest, is dizzy, vomiting or unresponsive, give 100% oxygen with rescue breathing or CPR as required and transport to the nearest medical facility.

Skin:

Remove contaminated clothing. Flush with large amounts of water for at least 15 minutes and follow by washing with soap if available. If redness, swelling, pain and/or blisters occur, transport to the nearest medical facility for additional treatment.

Eye:

Flush eyes with large amounts of water for at least 15 minutes. If redness, burning, blurred vision or swelling persist, transport to nearest medical facility for additional treatment.

Ingestion:

DO NOT take internally. Do NOT induce vomiting. If vomiting occurs spontaneously, keep head below hips to prevent aspiration of liquid into lungs. Get medical attention. In general no treatment is necessary unless large

quantities are swallowed, however, get medical advice. Have victim rinse mouth out with water, then drink sips of water to remove taste from mouth. If vomiting occurs spontaneously, keep head below hips to prevent aspiration.

Note to Physician:

If more than 2.0ml/kg body weight has been ingested and vomiting has not occurred, emesis should be induced with supervision. Keep victim's head below hips to prevent aspiration. If symptons such as loss of gag reflex, convulsions, or unconsciousness occur before emesis, gastric lavage using a cuffed endotracheal tube should be considered.

SECTION 5

FIRE FIGHTING MEASURES

Flash Point [Method]:

-40 °F/-40 °C [Tagliabue Closed Cup]

Flammability in Air:

1.3 - 7.6 %volume

Extinguishing Media:

Use water fog, foam, dry chemical or carbon dioxide (CO2) to extinguish flames. Do not use a direct stream of water. Material will float and can be re-ignited on surface of water.

Fire Fighting Instructions:

DANGER! EXTREMELY FLAMMABLE. Clear fire area of all non-emergency personnel. Only enter confined fire space with full bunker gear, including a positive pressure, NIOSH-approved, self-contained breathing apparatus. Cool surrounding equipment, fire-exposed containers and structures with water. Container areas exposed to direct flame contact should be cooled with large quantities of water (500 gallons water per minute flame impingement exposure) to prevent weakening of container structure.

Unusual Fire Hazards:

Vapors are heavier than air accumulating in low areas and traveling along the ground away from the handling site. Do not weld, heat or drill on or near container. However, if emergency situations require drilling, only trained emergency personnel should drill.

SECTION 6

ACCIDENTAL RELEASE MEASURES

Protective Measures:

DANGER! EXTREMELY FLAMMABLE! Eliminate potential sources of ignition. Handling equipment must be bonded and grounded to prevent sparking.

Spill Management:

Dike and contain spill.

FOR LARGE SPILLS: Remove with vacuum truck or pump to storage/salvage vessels.

FOR SMALL SPILLS: Soak up residue with an absorbent such as clay, sand or other suitable material. Place in non-leaking container and seal tightly for proper disposal.

Reporting:

CERCLA: Product is covered by EPA's Comprehensive Environmental Response, Compensation and Liability Act (CERCLA) petroleum exclusion. Releases to air, land, or water are not reportable under CERCLA (Superfund).

CWA: This product is an oil as defined under Section 311 of EPA's Clean Water Act (CWA). Spills into or leading to surface waters that cause a sheen must be reported to the National Response Center, 1-800-424-8802.

SECTION 7

HANDLING AND STORAGE

Precautionary Measures:

Wash with soap and water before eating, drinking, smoking, applying cosmetics, or using toilet. Launder contaminated clothing before reuse. Properly dispose of contaminated leather articles such as shoes or belts that cannot be decontaminated. Avoid heat, open flames, including pilot lights, and strong oxidizing agents. Use

explosion-proof ventilation to prevent vapor accumulation. Ground all handling equipment to prevent sparking. Do not siphon gasoline by mouth; harmful or fatal if swallowed. Avoid contact with eyes, skin and clothing. Wash thoroughly after handling.

For use as a motor fuel only. Do not use as a cleaning solvent or for other non-motor fuel uses.

Handling:

Surfaces that are sufficiently hot may ignite liquid material. Material is extremely flammable and heavier than air. Vapors may travel across the ground and reach remote ignition sources causing a flashback fire danger.

Keep containers closed when not in use. WARNING! The flow of gasoline through the pump nozzle can produce static electricity, which may cause a fire if gasoline is pumped into an ungrounded container. To avoid static buildup, place approved container on the ground. Do not fill container in vehicle or truck bed. Keep nozzle in contact with container while filling. Do not use automatic pump handle (latch-open) device. Turn off all battery operated portable electronic devices (examples include: cellular phones, pagers and CD players) before operating gasoline pump. Use only with adequate ventilation.

Storage:

Store in a cool, dry place with adequate ventilation. Keep away from open flames and high temperatures.

Keep liquid and vapor away from heat, sparks and flame. Extinguish pilot lights, cigarettes and turn off other sources of ignition prior to use and until all vapors have dissipated. Use explosion-proof ventilation to prevent vapor accumulation while in use.

Container Warnings:

Keep containers closed when not in use. Containers, even those that have been emptied, can contain explosive vapors. Do not cut, drill, grind, weld or perform similar operations on or near containers.

SECTION 8 EXPOSURE CONTROLS/PERSONAL PROTECTION

Chemical	Limit	TWA	STEL	Ceiling	Notation
Benzene	ACGIH TLV	0.5 ppmv	2.5 ppmv		Skin
Benzene	OSHA PEL	1 ppmv	5 ppmv		
Cyclohexane	ACGIH TLV	300 ppmv			
Cyclohexane	OSHA PEL	300 ppmv			
Ethyl Benzene	ACGIH TLV	100 ppmv	125 ppmv		
Ethyl Benzene	OSHA PEL	100 ppmv			
Ethyl Benzene	OSHA PEL - 1989(revoked)	100 ppmv	125 ppmv		
Gasoline	ACGIH TLV	300 ppmv	500 ppmv		
Gasoline	OSHA PEL - 1989(revoked)	300 ppmv	500 ppmv		
Isopropyl ether	ACGIH TLV	250 ppmv	310 ppmv		
Isopropyl ether	OSHA PEL	500 ppmv			
Methyl T-Butyl Ether	ACGIH TLV	40 ppmv			
N-Hexane	OSHA PEL	50 ppmv			
N-Hexane	OSHA PEL - 1989(revoked)	50 ppmv			
Naphthalene	ACGIH TLV	10 ppmm	15 ppmm		
Naphthalene	OSHA PEL	10 ppmv			
Naphthalene	OSHA PEL - 1989(revoked)	10 ppmv	15 ppmv		
Styrene	ACGIH TLV	20 ppmv	40 ppmv		

Styrene	OSHA PEL	100 ppmv		200 ppmv	
Styrene	OSHA PEL - 1989(revoked)	50 ppmv	100 ppmv		
Styrene, monomer	SHELL PEL - 1989(revoked)	50 ppmv	100 ppmv		Embryo-Fetus Policy
Toluene	ACGIH TLV	50 ppmv			Skin
Toluene	OSHA PEL	200 ppmv		300 ppmv	
Toluene	OSHA PEL - 1989(revoked)	100 ppmv	150 ppmv	·	
Toluene	SHELL SIS	50 ppmv			
Trimethyl Benzene	ACGIH TLV	25 ppmv			
Trimethyl Benzene	OSHA PEL - 1989(revoked)	25 ppmv	<u></u>		
Trimethyl Benzene	SHELL PEL - 1989(revoked)	25 ppmv			
xylene (o-, m-, p- isomers)	OSHA PEL	100 ppmv			
xylene (o-, m-, p- isomers)	OSHA PEL - 1989(revoked)	100 ppmv	150 ppmv		
Xylene (o-, m-, p-isomers)	ACGIH TLV	100 ppmv	150 ppmv		

Exposure Controls

Adequate explosion-proof ventilation to control airborne concentrations below the exposure guidelines/limits.

Personal Protection

Personal protective equipment (PPE) selections vary based on potential exposure conditions such as handling practices, concentration and ventilation. Information on the selection of eye, skin and respiratory protection for use with this material is provided below.

Eve Protection:

Chemical Goggles - If liquid contact is likely.

Skin Protection:

Use protective clothing which is chemically resistant to this material. Selection of protective clothing depends on potential exposure conditions and may include gloves, boots, suits and other items. The selection(s) should take into account such factors as job task, type of exposure and durability requirements.

Published literature, test data and/or glove and clothing manufacturers indicate the best protection is provided by: Neoprene, or Nitrile Rubber, or Polyvinyl Alcohol (PVA)

Respiratory Protection:

If engineering controls do not maintain airborne concentrations to a level which is adequate to protect worker health, an approved respirator must be worn. Respirator selection, use and maintenance should be in accordance with the requirements of the OSHA Respiratory Protection Standard, 29 CFR 1910.134.

Types of respirator(s) to be considered in the selection process include:

Supplied-Air Respirator. Air-Purifying Respirator for Organic Vapors. Self-contained breathing apparatus.

SECTION 9	PHYSICAL AND CHEMICAL PROPERTIES		
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Appearance & Odor: Bronze color, clear & bright liquid. Hydrocarbon odor.

Substance Chemical Family: Hydrocarbon

Flammability in Air	1.3 - 7.6 %volume	Flash Point	-40 °F [Tagliabue Closed Cup]
Freezing Point	-72 °F	Solubility (in Water)	Negligible
Specific Gravity	0.72 - 0.76	Stability	Stable
Vapor Density	3.5	Vapor Pressure	7 - 14.5 mmHg [Reid]
Viscosity	< 1.4 cSt Typical @ 100	Volatility	100 %volume
	of	-	

SECTION 10	REACTIVITY AND STABILITY	•

Stability:

Material is stable under normal conditions.

Conditions to Avoid:

Avoid heat, sparks, open flames and other ignition sources.

Materials to Avoid:

Avoid contact with strong oxidizing agents.

Hazardous Decomposition Products:

Thermal decomposition products are highly dependent on combustion conditions. A complex mixture of airborne solids, liquids and gases will evolve when this material undergoes pyrolysis or combustion. Aldehydes, Carbon Monoxide, Carbon Dioxide, Peroxide, Styrene oxide and other unidentified organic compounds may be formed upon combustion.

SECTION 11 TOXICOLOGICAL INFORMATION

Acute Toxicity

TEST	Result	OSHA Classification	Material Tested
Dermal LD50	>2 g/kg(Rabbit)	Non-Toxic	Based on similar material(s)
Eye Irritation	Moderate to Severe Irritation [Human]	Irritating	Based on similar material(s)
Oral LD50	>5 g/kg(Rat)	Non-Toxic	Based on similar material(s)
Skin Irritation Draize	0.98 [Rabbit, 24 HOUR(S)]	Irritating	Based on similar material(s)

Carcinogenicity:

Gasoline has been tested by API in a long-term inhalation test in mice and rats. There was an increased incidence of liver cancer in female mice. Male rats had a dose related increase in kidney tumors. This effect was due to formation of alpha-2u-globulin in the rats. This material is not formed in humans and is therefore not considered relevant.

Carcinogenicity Classification

Chemical Name	NTP	IARC	ACGIH	OSHA
Gasoline (Conventional, CARB and RFG)		Possible Carcinogen (2B)	A3	Yes
Benzene	Yes	Carcinogen (1)	A1	Yes
Ethyl Benzene		Possible Carcinogen (2B)		
Methyl Tert-Butyl Ether (MTBE)			A3	
Naphthalene			A4	
Styrene		Possible	A4	

	Carcinogen (2B)		
Toluene	Not Classifiable	A4	
	(3)	1	

	Toxic Effects - Equiva Gasoline MSDS
Carcinogenicity	Chronic inhalation of wholly vaporized gasoline produced kidney tumors in male rats and liver tumors in female mice. The kidney tumors have been shown to develop through a unique mechanism involving Alpha-2u globulin. This protein is not present in humans making the kidney tumors irrelevant to potential human health risks. Origin of the female mouse liver tumors is less understood, leaving their significance for human risks uncertain. Prolonged and repeated exposure to high concentrations (10s to 10os ppm) of benzene may cause serious injury to blood-forming organs, is associated with anemia (depletion of blood cells) and is linked to the later development of acute myelogenous leukemia (AML) in humans. A recent chronic bioassay of ethylbenzene by the NTP produced clear evidence of carcinogenicity in male rats based on kidney tumor increase. Other animal tumors possibly associated with ethylbenzene include testicular adenomas in male rats, kidney tumors in female rats, lung tumors in male mice and liver tumors in female mice. Toluene is not known to be mutagenic or carcinogenic although available human and experimental animal data are limited and insufficient to assess carcinogenic potential. Chronic inhalation of MTBE produced liver tumors in female mice and kidney tumors in male rats. These tumors are of questionable relevance to humans and further studies are being done to address their significance.
Cardiovascular System	While there is no evidence that workplace exposure to acceptable levels of toluene vapors (e.g., the TLV) have produced cardiac effects in humans, high concentrations may cause cardiac sensitization and sudden lethality has been reported from habitual sniffing of solvents or glue. Animal studies have confirmed the sensitizing effects. Sensitization may lead to fatal changes in heart rhythms. Hypoxia or injection of adrenalin-like agents may enhance this effect. Thickening of heart blood vessels has been reported in animals exposed to xylene.
Developmental Toxicity	Daily exposure of pregnant rats to unleaded gasoline vapor at concentrations up to 9000 ppm resulted in no detectable maternal or developmental toxicity. Numerous studies of benzene in experimental animals have failed to detect teratogenic effects (birth defects) even at doses of benzene toxic to the mothers. There is some evidence of fetal toxicity, but not malformations, in mice and rabbits exposed to 500 ppm and higher concentrations of benzene vapor during gestation. Ethylbenzene caused birth defects in rats but not rabbits at doses that produced toxic effects in the mothers. n-Hexane produced fetal toxicity, reduced fetal weight, in mice at maternally toxic doses. Developmental toxicity studies of xylenes showed embryolethal/toxic and teratogenic effects with maternal toxicity. Many case studies involving abuse during pregnancy implicate toluene as a developmental toxicant. Studies in laboratory animals have shown developmental effects comparable to those reported in humans, but the effects were generally associated with maternal toxicity. Exposing pregnant mice to maternally toxic MTBE levels greater than 1000 ppm produced adverse gestational and developmental effects including malformations. No developmental toxicity was seen in rabbits exposed to MTBE concentrations up to 8000 ppm. Birth defects in mice and fetotoxicity in both rats and mice were observed following maternally toxic TAME exposures. Exposure of pregnant rats to high concentrations of DIPE (3095 and 6745 ppm) by inhalation during pregnancy increased the frequency of rudimentary 14th ribs in the offspring. The effect was not seen following exposure to 430 ppm DIPE. The significance of this finding is not known.
Genotoxicity	Unleaded gasoline was tested for genetic activity in tests using microbial cells, cultured mammalian cells and rats (bone marrow) and was judged to be negative in every case. Benzene has been shown to be non-mutagenic or weakly mutagenic in a variety of in vitro (test tube) systems. It has, however, been found to cause other types of chromosome damage (micronuclei, chromosome breakage, non-dysjunctional events) in both laboratory animals and workers exposed to high doses of benzene. These effects appear to be related to one or more metabolites of benzene, possibly acting in combination. Benzene metabolites can also bind to proteins forming detectable complexes (adducts). There is limited evidence of binding to the genetic material (DNA) itself. The relationship of these effects to the causation of leukemia or tumors in experimental animals is unknown. Changes in chromosomes of lymphocytes have been identified in some studies of humans exposed to styrene. The significance of these changes is not known, and other such studies have produced negative results. Chromosomal breaks have been reported in the bone marrow cells of rats exposed to styrene by inhalation along with increased frequency of sister chromatid exchanges in alveolar macrophages, bone marrow cells and regenerating liver cells. Ethylbenzene was not mutagenic in a number of in vitro procedures. Naphthalene was negative in Ames mutagenicity and rat cell transformation assays. Cyclohexane and pseudocumene were also negative in Ames testing. Toluene was negative in the Ames assay and negative for chromosomal aberrations and sister-chromatid exchanges in human lymphocytes and in an in vitro test using hamster cells. Mouse lymphoma test results for toluene were inconclusive. MTBE was negative in several mutagenicity tests, but was positive in a mouse lymphoma test.
Blood/Blood Forming Organs	Prolonged and repeated exposure to high concentrations (10s to 100s ppm) of benzene may cause serious injury to blood-forming organs and is associated with anemia (depletion of blood cells). Repeated exposure of rabbits to high cyclohexane vapor concentrations causes a slight increase in blood clotting time. Blood effects were seen in rats following prolonged and repeated oral exposure to a mixture of xylenes containing ethylbenzene.
Immunotoxicity	Various studies of workers exposed to high levels of benzene have found impairment of both humoral (antibody) and

	cellular immunity, most notably a decrease in levels of circulating leukocytes. Many of these exposures also involve other solvents and chemicals. Animal studies with high benzene doses have reported similar effects.
Kidney	Long-term inhalation of wholly vaporized gasoline caused increased kidney weight and progressive nephropathy (tissue damage) in male rats. In rats exposed orally to a xylene mixture also containing ethylbenzene, males developed hyaline droplet changes and females showed evidence of early chronic nephropathy. Intentional abuse of toluene vapors by 'glue-sniffers' has been associated with damage to the kidneys. Long term inhalation of up to 8000 ppm MTBE vapor produced a chronic, progressive nephropathy (kidney damage) in male rats. This effect may be related to the accumulation of alpha-2u globulin and therfore specific to the male rat. (See Carcinogenicity) Increased kidney weights without evidence of tissue injury were reported in rats exposed to high, inhaled doses of TAME. Prolonged inhalation of DIPE (90 days or longer) increased kidney weights in both male and female rats. In male rats exposed to the highest concentration (7100 ppm) there was also evidence of microscopic changes (hyaline droplets) in the kidney tubules resembling those produced by exposure to gasoline.
Liver	Inhalation of gasoline vapor increased liver weights, urinary excretion of ascorbic acid, and hepatic enzymeactivity in male rats. Liver weight increases were seen in rats dosed orally for 90 days with a xylene mixture also containing ethylbenzene. Reversible liver damage has been reported in persons exposed to toluene by solvent abuse. Liver weight increases without evidence of tissue injury were seen in rats exposed to greater than 500 ppm TAME by inhalation for four weeks. Prolonged inhalation of DIPE (90 days or longer) increased liver weights in both rats and rabbits. In rabbits and in male rats exposed to 7100 ppm there was also evidence of microscopic changes in the liver tissue.
Nervous System	Inhalation of MTBE vapors at high concentrations (above 800 ppm) induced reversible central nervous system depression in rats. Inhalation of TAME at concentrations greater than 250 ppm produced reversible sedation in rats and mice.
Neurotoxicity	Inhalation exposure to high n-hexane concentrations has resulted in peripheral neuropathy in rodents and also in human workers. Rats receiving prolonged and repeated exposure to high doses of xylene have shown hearing loss. Prolonged and repeated exposures to high toluene concentrations (mixed solvent) have resulted in hearing loss in laboratory animals. There have also been reports of hearing damage in humans overexposed to toluene and other solvents, however, these effects and their possible relationship to noise exposure remain uncertain. Intentional inhalation ('glue-sniffing') and resulting overexposure to toluene vapors has been linked to brain injury. Rats exposed repeatedly to high concentrations of styrene vapor also developed hearing deficits.
Reproductive Toxicity	Inhalation of high n-hexane concentrations resulted in testicular and epididymal lesions in laboratory animals. Animal studies on benzene have shown testicular effects and alteration in reproductive cycles.
Sensitization	Gasoline and component petroleum streams blended to produce it were tested in animal studies and found not to cause skin sensitization.
Systemic Toxicity	Studies on n-hexane in laboratory animals have shown mild, transitory effects on the spleen and blood (white blood cells) and evidence of nasal tract and lung damage. Chronic exposure to vapors of a mixture containing 50% pseudocumene (and possibly contaminated with benzene) caused decreased weight gain and blood changes (lymphopenia and neutrophilia), liver, lung, spleen, kidney, and bone marrow effects in rats. Microscopic changes in the lung, including congestion, hemorrhage, edema, exudation, and leukocyte infiltration were observed in rats and guinea pigs following acute inhalation of styrene. In fatally exposed animals, pulmonary congestion, edema, and necrosis of the kidney and liver were reported. Repeated exposure to high vapor concentrations of cyclohexane caused minor microscopic liver and kidney changes in rabbits. Laboratory animals exposed to prolonged and repeated doses of xylenes by various routes have shown effects in liver, kidneys, lungs, spleen, heart, blood and adrenals.

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ECOLOGICAL INFORMATION

Environmental Impact Summary: There is no ecological data available for this product.

SECTION 13	DISPOSAL CONSIDERATIONS

RCRA Information:

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D001 (Ignitable Hazardous Waste) D018 (Toxicity, Benzene > 0.5 mg/l)

Under RCRA, it is the responsibility of the user of the material to determine, at the time of the disposal, whether the material meets RCRA criteria for hazardous waste. This is because material uses, transformations, mixtures. processes, etc. may affect the classification. Refer to the latest EPA, state and local regulations regarding proper disposal.

SECTION 14

TRANSPORT INFORMATION

US Department of Transportation Classification

Proper Shipping Name:

Gasoline

Identification Number:

UN1203

Hazard Class/Division:

3 (Flammable Liquid)

Packing Group:

11

Marine Pollutant % of Total:

100 %weight

Marine Pollutant: Marine Polluntant based on the presence of >10% hydrocarbons listed in 49 CFR 172.101,

appendix B; main constituents Trimethylbenzene and Naphthalene.

Per 49 CFR 130.5, containers of 3500 gallon capacity or greater transported by road or rail are excepted from 49 CFR 172.303(L)(2) if shipping papers contain the word 'OIL'; exceptions are not applicable to shipments by

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SECTION 15

REGULATORY INFORMATION

Federal Regulatory Status

OSHA Classification:

Product is hazardous according to the OSHA Hazard Communication Standard, 29 CFR 19.10.1200.

Ozone Depleting Substances (40 CFR 82 Clean Air Act):

This material does not contain nor was it directly manufactured with any Class I or Class II ozone depleting substances.

Superfund Amendment & Reauthorization Act (SARA) Title III:

There are no components in this product on the SARA 302 list.

SARA Hazard Categories (311/312):

Immediate Health	Delayed Health	Fire	Pressure	Reactivity
YES	YES	YES	NO	NO

SARA Toxic Release Inventory (TRI) (313):

Xylene (mixed isomers), Styrene, 1,2,4-Trimethylbenzene, Toluene, Naphthalene, Methyl Tert-Butyl Ether, N-Hexane, Ethylbenzene, Cyclohexane, Benzene

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Toxic Substances Control Act (TSCA) Status:

All component(s) of this material is(are) listed on the EPA/TSCA Inventory of Chemical Substances.

Other Chemical Inventories:

Australian AICS, Chinese Inventory, European EINECS, Japan ENCS, Korean Inventory, Philippines PICCS

State Regulation

The following chemicals are specifically listed by individual states; other product specific health and safety data in other sections of the MSDS may also be applicable for state requirements. For details on your regulatory requirements you should contact the appropriate agency in your state.

California Safe Drinking Water and Toxic Enforcement Act (Proposition 65):

The chemical identified with this code, Reproductive Toxin is known to the state of California to cause birth defects or other reproductive harm. The chemical identified with this code, Carcinogen & Reproduction Toxin, is known to the state of California to cause both cancer and birth defects or other reproductive harm.

Benzene (71-43-2) 0 - 4 %volume Carcinogen/Reproduction Toluene (108-88-3) 0 - 25 %volume Reproduction

New Jersey Right-To-Know Chemical List:

co, mgm ro mich chemical fich				
Benzene (71-43-2)	0 -	4	%volume	Carcinogen
Benzene (71-43-2)	0 -	4	%volume	Mutagen
Benzene, Methyl- (108-88-3)	0 -	25	%volume	_
Cyclohexane (110-82-7)	0 -	1	%volume	
Ethylbenzene (0851)	0 -	3	%volume	
Methyl Tert-Butyl Ether (1634-04-4)	0 -	15	%volume	
Naphthalene (1322)	0 -	1	%volume	
Propane, 2,2'-oxybis- (108-20-3)	0 -	2	%volume	
Styrene (100-42-5)	0 -	4	%volume	Mutagen
Xylenes (1330-20-7)	0 -	25	%volume	

Pennsylvania Right-To-Know Chemical List:

Benzene (71-43-2)	0 -	4	%volume	Spec Haz Sub/Env Hazardous
Benzene, dimethyl- (1330-20-7)	0 -	25	%volume	Environmental Hazard
Benzene, ethenyl (100-42-5)	0 -	4	%volume	Environmental Hazard
Benzene, Ethyl- (100-41-4)	0 -	3	%volume	Environmental Hazard
Benzene, Methyl- (108-88-3)	0 -	25	%volume	Environmental Hazard
Cyclohexane (110-82-7)	0 -	1	%volume	Environmental Hazard
Methyl Tert-Butyl Ether (1634-04-4)	0 -	15	%volume	Environmental Hazard
Naphthalene (91-20-3)	0 -	1	%volume	Environmental Hazard
Propane, 2,2'-oxybis- (108-20-3)	0 -	2	%volume	

SECTION 16

OTHER INFORMATION

Revision#: 1

Revision Date: 10/11/2000

Revisions since last change (discussion): This Material Safety Data Sheet has been changed to include new information on the potential carcinogenicity of component Ethylbenzene and to add Diisopropyl Ether (DIPE) as a

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component. We encourage you to take the opportunity to reread the sheet and review the information contained. Changes have occurred in the following Sections: 2, 11, 15.

SECTION 17

LABEL INFORMATION

READ AND UNDERSTAND MATERIAL SAFETY DATA SHEET BEFORE HANDLING OR DISPOSING OF PRODUCT. THIS LABEL COMPLIES WITH THE REQUIREMENTS OF THE OSHA HAZARD COMMUNICATION STANDARD (29 CFR 1910.1200) FOR USE IN THE WORKPLACE. THIS LABEL IS NOT INTENDED TO BE USED WITH PACKAGING INTENDED FOR SALE TO CONSUMERS AND MAY NOT CONFORM WITH THE REQUIREMENTS OF THE CONSUMER PRODUCT SAFETY ACT OR OTHER RELATED REGULATORY REQUIREMENTS.

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DANGER!

EXTREMELY FLAMMABLE. VAPORS MAY EXPLODE. OVEREXPOSURE TO VAPORS CAN CAUSE CNS DEPRESSION. MAY CAUSE SKIN AND EYE IRRITATION. ASPIRATION HAZARD IF SWALLOWED - CAN ENTER LUNGS AND CAUSE DAMAGE. CONTAINS BENZENE WHICH IS A CANCER HAZARD - LINKED TO DEVELOPMENT OF ACUTE MYELOGENOUS LEUKEMIA. LONG-TERM EXPOSURE TO GASOLINE VAPORS HAS CAUSED CANCER IN LABORATORY ANIMALS. PROLONGED OR REPEATED SKIN CONTACT MAY CAUSE OIL ACNE OR DERMATITIS.

MAY CAUSE DAMAGE TO: Cardiovascular System, Blood/Blood Forming Organs, Kidney, Liver, Nervous System

Precautionary Measures: Avoid heat, sparks, open flames and other ignition sources. Do not take internally. Use only with adequate ventilation. Avoid contact with eyes, skin and clothing. Keep container closed when not in use. Wash thoroughly after handling.

FIRST AID

Inhalation: Move victim to fresh air and provide oxygen if breathing is difficult. Get medical attention. If the victim has difficulty breathing or tightness of the chest, is dizzy, vomiting or unresponsive, give 100% oxygen with rescue breathing or CPR as required and transport to the nearest medical facility.

Skin Contact: Remove contaminated clothing. Flush with large amounts of water for at least 15 minutes and follow by washing with soap if available. If redness, swelling, pain and/or blisters occur, transport to the nearest medical facility for additional treatment.

Eye Contact: Flush eyes with large amounts of water for at least 15 minutes. If redness, burning, blurred vision or swelling persist, transport to nearest medical facility for additional treatment.

Ingestion: DO NOT take internally. Do NOT induce vomiting. If vomiting occurs spontaneously, keep head below hips to prevent aspiration of liquid into lungs. Get medical attention. If vomiting occurs spontaneously, keep head below hips to prevent aspiration. Have victim rinse mouth out with water, then drink sips of water to remove taste from mouth. In general no treatment is necessary unless large quantities are swallowed, however, get medical advice.

FIRE

In case of fire, Use water fog, foam, dry chemical or carbon dioxide (CO2) to extinguish flames. Do not use a direct stream of water. Material will float and can be re-ignited on surface of water.

SPILL OR LEAK

Dike and contain spill.

FOR LARGE SPILLS: Remove with vacuum truck or pump to storage/salvage vessels.

RBOB - Sewaren MSDS # 400454M-1 Page of

FOR SMALL SPILLS: Soak up residue with an absorbent such as clay, sand or other suitable material. Place in non-leaking container and seal tightly for proper disposal.

CONTAINS: Miscellaneous Hydrocarbons, Mixture; Xylene, mixed isomers, 1330-20-7; Toluene, 108-88-3; 1,2,4-Trimethyl Benzene (Pseudocumene), 95-63-6; Styrene, 100-42-5; Benzene, 71-43-2; Ethyl Benzene. 100-41-4; Hexane, 110-54-3; Cyclohexane, 110-82-7; Naphthalene, 91-20-3; Methyl Tert-Butyl Ether (MTBE), 1634-04-4; Ethyl Tert-Butyl Ether (ETBE), 637-92-3; Tert-Amyl Methyl Ether (TAME), 994-05-8; Diisoproply Ether (DIPE), 108-20-3

NFPA Rating (Health, Fire, Reactivity): 1, 3, 0

TRANSPORTATION

US Department of Transportation Classification

Proper Shipping Name:

Gasoline UN1203

 \parallel

Identification Number:

Hazard Class/Division:

3 (Flammable Liquid)

Packing Group:

100 %weight

Marine Pollutant % of Total:

Marine Pollutant: Marine Pollutant based on the presence of >10% hydrocarbons listed in 49 CFR 172.101,

appendix B; main constituents Trimethylbenzene and Naphthalene.

Per 49 CFR 130.5, containers of 3500 gallon capacity or greater transported by road or rail are excepted from 49 CFR 172.303(L)(2) if shipping papers contain the word 'OIL'; exceptions are not applicable to shipments by water.

Emergency Response Guide # 128

CAUTION: Misuse of empty containers can be hazardous. Empty containers can be hazardous if used to store toxic, flammable, or reactive materials. Cutting or welding of empty containers might cause fire, explosion or toxic fumes from residues. Do not pressurize or expose to open flames or heat. Keep container closed and drum bungs in place.

Name and Address

Motiva Enterprises, LLC

P.O. Box 4540

Houston, TX 77210-4540

TRANSPORTATION EMERGENCY

CHEMTEL (877) 276-7283

HEALTH EMERGENCY

CHEMTEL (877) 276-7283

ADMINISTRATIVE INFORMATION

COMPANY ADDRESS: Motiva Enterprises, LLC, P.O. Box 4540, Houston, TX. 77210-4540

Company Product Stewardship & Regulatory Compliance Contact: Ken Darmer

Phone Number: (281) 874-7982

MSDS FAX-BACK Phone Number: (877) 276-7285

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According to OSHA Hazard Communication Standard, 29 CFR 1910.1200

1. MATERIAL AND COMPANY IDENTIFICATION

Material Name

: BR Reformulated Gasoline with EtOH

Uses

: Fuel for spark ignition engines designed to run on unleaded

fuel.

Manufacturer/Supplier

: Motiva Enterprises LLC

PO BOX 4540

Houston, TX 77210-4540

USA

MSDS Request

: 877-276-7285

Emergency Telephone Number

Spill Information

: 877-242-7400

Health Information

: 877-504-9351

2. COMPOSITION/INFORMATION ON INGREDIENTS

Chemical Identity	CAS No.	Concentration
Gasoline		90.00 - 100.00 %
Ethanol	64-17-5	0.00 - 10.00 %

Contains Alkanes, Cycloalkanes, Alkenes and Aromatic Hydrocarbons, Mixture.

Contains 1,2,4 Tri-methyl-benzene, CAS# 95-63-6.

Contains Styrene, CAS # 100-42-5.

Contains Benzene, CAS #71-43-2.

Contains Toluene, CAS # 108-88-3.

Contains Ethylbenzene, CAS # 100-41-4.

Contains n-Hexane, CAS # 110-54-3.

Contains Xylene (Mixed Isomers), CAS # 1330-20-7.

Contains Naphthalene, CAS # 91-20-3. Contains Cyclohexane, CAS# 110-82-7.

3. HAZARDS IDENTIFICATION

Emergency Overview

Appearance and Odour : Bronze. Clear, bright liquid. Hydrocarbon.

Health Hazards : Harmful: may cause lung damage if swallowed. Irritating to

skin. Vapours may cause drowsiness and dizziness. A component or components of this material may cause cancer. This product contains benzene which may cause leukaemia (AML - acute myelogenous leukaemia). May cause MDS

(Myelodysplastic Syndrome).

Safety Hazards : Extremely flammable. The vapour is heavier than air, spreads

along the ground and distant ignition is possible. Electrostatic charges may be generated during handling. Electrostatic

discharge may cause fire.

Environmental Hazards : Toxic to aquatic organisms, may cause long-term adverse

effects in the aquatic environment.

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1910.1200

Health Hazards

Inhalation

: Vapours may cause drowsiness and dizziness. Slightly irritating

to respiratory system.

Skin Contact

: Irritating to skin.

Eye Contact Ingestion

: Moderately irritating to eyes.

: Harmful: may cause lung damage if swallowed.

Other Information : Possibility of organ or organ system damage from prolonged

exposure; see Chapter 11 for details. Target organ(s):

Blood-forming organs.
Peripheral nervous system.

May cause heritable genetic damage. Possible risk of harm to the unborn child. A component or components of this material may cause cancer. This product contains benzene which may cause leukaemia (AML - acute myelogenous leukaemia). May

cause MDS (Myelodysplastic Syndrome).

Signs and Symptoms

Skin irritation signs and symptoms may include a burning sensation, redness, swelling, and/or blisters. If material enters lungs, signs and symptoms may include coughing, choking, wheezing, difficulty in breathing, chest congestion, shortness of breath, and/or fever. The onset of respiratory symptoms may be delayed for several hours after exposure. Breathing of high vapour concentrations may cause central nervous system (CNS) depression resulting in dizziness, light-headedness, headache, nausea and loss of coordination. Continued inhalation may result in unconsciousness and death. Damage to blood-forming organs may be evidenced by: a) fatigue and anemia (RBC), b) decreased resistance to infection, and/or excessive bruising and bleeding (platelet effect). Peripheral nerve damage may be evidenced by impairment of motor function (incoordination, unsteady walk, or muscle weakness in the extremities, and/or loss of sensation in the arms and legs). Eye irritation signs and symptoms may include a burning sensation and a temporary redness of the eye. Auditory system effects may include temporary hearing loss and/or ringing in the

Aggravated Medical Conditions

Pre-existing medical conditions of the following organ(s) or organ system(s) may be aggravated by exposure to this material: Blood-forming organs. Peripheral nervous system.

Environmental Hazards

Toxic to aquatic organisms. May cause long-term adverse effects in the environment. Unlike other gasoline components,

ethanol is miscible with water.

Additional Information

: This product is intended for use in closed systems only.

4. FIRST AID MEASURES

Inhalation

: Remove to fresh air. If rapid recovery does not occur, transport to nearest medical facility for additional treatment.

Skin Contact

Remove contaminated clothing. Immediately flush skin with large amounts of water for at least 15 minutes, and follow by washing with soap and water if available. If redness, swelling,

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Eye Contact

Ingestion

According to OSHA Hazard Communication Standard, 29 CFR 1910.1200

pain and/or blisters occur, transport to the nearest medical facility for additional treatment. When using high pressure equipment, injection of product under the skin can occur. If high pressure injuries occur, the casualty should be sent immediately to a hospital. Do not wait for symptoms to develop. Flush eyes with water while holding eyelids open. Rest eyes for

30 minutes. If redness, burning, blurred vision, or swelling persist transport to the nearest medical facility for additional

treatment.

If swallowed, do not induce vomiting: transport to nearest

medical facility for additional treatment. If vomiting occurs spontaneously, keep head below hips to prevent aspiration. If any of the following delayed signs and symptoms appear within the next 6 hours, transport to the nearest medical facility: fever greater than 101° F (38.3°C), shortness of breath, chest

congestion or continued coughing or wheezing.

Advice to Physician Treat symptomatically. Persons on disulfiram (Antabuse®)

therapy should be aware that the ethyl alcohol in this product is

hazardous to them just as is alcohol from any source.

Disulfiram reactions (vomiting, headache and even collapse) may follow ingestion of small amounts of alcohol and have also

been described from skin contact.

5. FIRE FIGHTING MEASURES

Clear fire area of all non-emergency personnel.

Flash point Upper / lower

-40 °C / -40 °F (ASTM D-93 / PMCC) : 1.3 - 7.6 %(V)

Flammability or **Explosion limits**

Auto ignition temperature

> 250 °C / 482 °F

Hazardous combustion products may include: A complex Specific Hazards

mixture of airborne solid and liquid particulates and gases (smoke). Carbon monoxide. Unidentified organic and inorganic compounds. The vapour is heavier than air, spreads along the ground and distant ignition is possible. Will float and can be

reignited on surface water.

Suitable Extinguishing

Media

Foam, water spray or fog. Dry chemical powder, carbon dioxide, sand or earth may be used for small fires only.

Unsuitable Extinguishing Media

Do not use direct water jets on the burning product as they could cause a steam explosion and spread of the fire.

Simultaneous use of foam and water on the same surface is to

be avoided as water destroys the foam.

Protective Equipment for

Firefighters

Additional Advice

Proper protective equipment including breathing apparatus must be worn when approaching a fire in a confined space. Keep adjacent containers cool by spraying with water. If

possible remove containers from the danger zone. If the fire cannot be extinguished the only course of action is to evacuate immediately. Contain residual material at affected sites to prevent material from entering drains (sewers), ditches, and

waterways.

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6. ACCIDENTAL RELEASE MEASURES

Avoid contact with spilled or released material. Immediately remove all contaminated clothing. For guidance on selection of personal protective equipment see Chapter 8 of this Material Safety Data Sheet. For guidance on disposal of spilled material see Chapter 13 of this Material Safety Data Sheet. Observe the relevant local and international regulations. Avoid contact with skin, eyes and clothing. Evacuate the area of all non-essential personnel. Ventilate contaminated area thoroughly. If contamination of sites occurs remediation may require specialist advice. Ensure electrical continuity by bonding and grounding (earthing) all equipment. Take precautionary measures against static discharges.

Protective measures

: Vapour can travel for considerable distances both above and below the ground surface. Underground services (drains, pipelines, cable ducts) can provide preferential flow paths. Do not breathe fumes, vapour. Take measures to minimise the effects on groundwater. Contain residual material at affected sites to prevent material from entering drains (sewers), ditches, and waterways. Shut off leaks, if possible without personal risks. Remove all possible sources of ignition in the surrounding area. Use appropriate containment (of product and fire fighting water) to avoid environmental contamination. Prevent from spreading or entering drains, ditches or rivers by using sand, earth, or other appropriate barriers. Attempt to disperse the vapour or to direct its flow to a safe location for example by using fog sprays. Take precautionary measures against static discharge. Ensure electrical continuity by bonding and grounding (earthing) all equipment.

Clean Up Methods

For large liquid spills (> 1 drum), transfer by mechanical means such as vacuum truck to a salvage tank for recovery or safe disposal. Do not flush away residues with water. Retain as contaminated waste. Allow residues to evaporate or soak up with an appropriate absorbent material and dispose of safely. Remove contaminated soil and dispose of safely. For small liquid spills (< 1 drum), transfer by mechanical means to a labelled, sealable container for product recovery or safe disposal. Allow residues to evaporate or soak up with an appropriate absorbent material and dispose of safely. Remove contaminated soil and dispose of safely.

Additional Advice

Notify authorities if any exposure to the general public or the environment occurs or is likely to occur. Local authorities should be advised if significant spillages cannot be contained. Maritime spillages should be dealt with using a Shipboard Oil Pollution Emergency Plan (SOPEP), as required by MARPOL Annex 1 Regulation 26. U.S. regulations may require reporting releases of this material to the environment which exceed the reportable quantity (refer to Chapter 15) to the National Response Centre at (800) 424-8802. Under Section 311 of the Clean Water Act (CWA) this material is considered an oil. As such, spills into surface waters must be reported to the National Response Centre at (800) 424-8802. This material is covered by EPA's Comprehensive Environmental Response,

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Compensation and Liability Act (CERCLA) Petroleum Exclusion. Therefore, releases to the environment may not be reportable under CERCLA.

7. HANDLING AND STORAGE

General Precautions

Avoid breathing vapours or contact with material. Only use in well ventilated areas. Wash thoroughly after handling. For guidance on selection of personal protective equipment see Chapter 8 of this Material Safety Data Sheet. Use the information in this data sheet as input to a risk assessment of local circumstances to help determine appropriate controls for safe handling, storage and disposal of this material. Air-dry contaminated clothing in a well-ventilated area before laundering. Properly dispose of any contaminated rags or cleaning materials in order to prevent fires. Prevent spillages. Turn off all battery operated portable electronic devices (examples include: cellular phones, pagers and CD players) before operating gasoline pump. Do not use as a cleaning solvent or other non-motor fuel uses. Contaminated leather articles including shoes cannot be decontaminated and should be destroyed to prevent reuse. For comprehensive advice on handling, product transfer, storage and tank cleaning refer to the product supplier.

Handling

When using do not eat or drink. Extinguish any naked flames. Do not smoke. Remove ignition sources. Avoid sparks. Never siphon by mouth. The vapour is heavier than air, spreads along the ground and distant ignition is possible. Avoid exposure.

Storage

: Drum and small container storage: Keep containers closed when not in use. Drums should be stacked to a maximum of 3 high. Packaged product must be kept tightly closed and stored in a diked (bunded) well-ventilated area, away from, ignition sources and other sources of heat. Use properly labelled and closeable containers. Take suitable precautions when opening sealed containers, as pressure can build up during storage. Tank storage: Tanks must be specifically designed for use with this product. Bulk storage tanks should be diked (bunded). Locate tanks away from heat and other sources of ignition. Cleaning, inspection and maintenance of storage tanks is a specialist operation, which requires the implementation of strict procedures and precautions.

Product Transfer

Electrostatic charges may be generated during pumping. Electrostatic discharge may cause fire. Ensure electrical continuity by bonding and grounding (earthing) all equipment. Restrict line velocity during pumping in order to avoid generation of electrostatic discharge (<= 1 m/sec until fill pipe submerged to twice its diameter, then <= 7 m/sec). Avoid splash filling. Do NOT use compressed air for filling, discharging, or handling operations. Wait 2 minutes after tank filling (for tanks such as those on road tanker vehicles) before opening hatches or manholes. Wait 30 minutes after tank filling (for large storage tanks) before opening hatches or manholes.

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Recommended Materials

For containers, or container linings use mild steel, stainless steel. Aluminium may also be used for applications where it does not present an unnecessary fire hazard. Examples of suitable materials are: high density polyethylene (HDPE), polypropylene (PP), and Viton (FKM), which have been specifically tested for compatibility with this product. For container linings, use amine-adduct cured epoxy paint. For seals and gaskets use: graphite, PTFE, Viton A, Viton B. Some synthetic materials may be unsuitable for containers or

Unsuitable Materials

container linings depending on the material specification and intended use. Examples of materials to avoid are: natural rubber (NR), nitrile rubber (NBR), ethylene propylene rubber (EPDM), polymethyl methacrylate (PMMA), polystyrene, polyvinyl chloride (PVC), polyisobutylene. However, some may be suitable for glove materials.

Container Advice

Containers, even those that have been emptied, can contain explosive vapours. Do not cut, drill, grind, weld or perform similar operations on or near containers. Gasoline containers

must not be used for storage of other products.

Additional Information

Ensure that all local regulations regarding handling and storage

facilities are followed.

8. EXPOSURE CONTROLS/PERSONAL PROTECTION

Occupational Exposure Limits

Material	Source	Туре	ppm	mg/m3	Notation
Gasoline, low boiling point naphtha	ACGIH	TWA	300 ppm		
Gasoline, low boiling point naphtha	ACGIH	STEL	500 ppm		
Toluene	ACGIH	TWA	20 ppm		
Toluene	OSHA Z1A	TWA	100 ppm	375 mg/m3	
Toluene	OSHA Z1A	STEL	150 ppm	560 mg/m3	
Toluene	OSHA Z2	TWA	200 ppm		
Toluene	OSHA Z2	Ceiling	300 ppm		
Toluene	OSHA Z2	MAX. CONC	500 ppm		
Xylene, mixed isomers	ACGIH	TWA	100 ppm		
Xylene, mixed isomers	ACGIH	STEL	150 ppm		
Xylene, mixed isomers	OSHA Z1	PEL	100 ppm	435 mg/m3	

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Xylene, mixed	OSHA Z1A	TWA	100 ppm	435 mg/m3	
isomers					
Xylene, mixed	OSHA Z1A	STEL	150 ppm	655 mg/m3	
isomers			1.000		
Ethanoi	ACGIH	STEL	1,000 ppm	4.000	
Ethanol	OSHA Z1	PEL	1,000 ppm		
Ethanol	OSHA Z1A	TWA	1,000 ppm	1,900 mg/m3	
1,2,4- Trimethylbe nzene	ACGIH	TWA	25 ppm		
1,2,4- Trimethylbe nzene	OSHA Z1A	TWA	25 ppm	125 mg/m3	
Ethylbenze ne	ACGIH	TWA	20 ppm		
Ethylbenze ne	OSHA Z1	PEL	100 ppm	435 mg/m3	
Ethylbenze ne	OSHA Z1A	TWA	100 ppm	435 mg/m3	
Ethylbenze ne	OSHA Z1A	STEL	125 ppm	545 mg/m3	
n-hexane	ACGIH	TWA	50 ppm		
n-hexane	ACGIH	SKIN_DES			Can be absorbed through the skin.
n-hexane	OSHA Z1	PEL	500 ppm	1,800 mg/m3	
n-hexane	OSHA Z1A	TWA	50 ppm	180 mg/m3	
Benzene	ACGIH	TWA	0.5 ppm		
Benzene	ACGIH	STEL	2.5 ppm		
Benzene	ACGIH	SKIN_DES			Can be absorbed through the skin.
Benzene	OSHA	TWA	1 ppm		
Benzene	OSHA	STEL	5 ppm	<u> </u>	
Benzene	OSHA	OSHA_ACT	0.5 ppm	·	
Benzene	OSHA Z1A	TWA	1 ppm		
Benzene	OSHA Z1A	STEL	5 ppm		
Benzene	SHELL IS	TWA	0.5 ppm	1.6 mg/m3	
Benzene	SHELL IS	STEL	2.5 ppm	8 mg/m3	
Benzene	OSHA Z2	TWA	10 ppm		
Benzene	OSHA Z2	Ceiling	25 ppm		
Benzene	OSHA Z2	MAX. CONC	50 ppm		
Cyclohexan e	ACGIH	TWA	100 ppm		
Cyclohexan e	OSHA Z1	PEL	300 ppm	1,050 mg/m3	
Cyclohexan e	OSHA Z1A	TWA	300 ppm	1,050 mg/m3	·
Naphthalen e	ACGIH	TWA	10 ppm		

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Naphthalen e	ACGIH	STEL	15 ppm		
Naphthalen e	ACGIH	SKIN_DES			Can be absorbed through the skin.
Naphthalen e	OSHA Z1	PEL	10 ppm	50 mg/m3	
Naphthalen e	OSHA Z1A	TWA	10 ppm	50 mg/m3	
Naphthalen e	OSHA Z1A	STEL	15 ppm	75 mg/m3	
Styrene	ACGIH	TWA	20 ppm		
Styrene	ACGIH	STEL	40 ppm		
Styrene	OSHA Z1A	TWA	50 ppm	215 mg/m3	
Styrene	OSHA Z1A	STEL	100 ppm	425 mg/m3	
Styrene	OSHA Z2	TWA	100 ppm		
Styrene	OSHA Z2	Ceiling	200 ppm		
Styrene	OSHA Z2	MAX. CONC	600 ppm		

Additional Information

: Shell has adopted as Interim Standards the OSHA Z1A values that were established in 1989 and later rescinded. SHELL IS is the Shell Internal Standard. Skin notation means that significant exposure can also occur by absorption of liquid through the skin and of vapour through the eyes or mucous membranes.

Biological Exposure Index (BEI) - See reference for full details

Material	Determinant	Sampling time	BEI	Reference
Toluene	toluene in Urine	Sampling time: End of shift.	0.03 mg/l	ACGIH BEL (01 2010)
Toluene	toluene in Blood	Sampling time: Prior to last shift of work week.	0.02 mg/l	ACGIH BEL (01 2010)
Toluene	o-Cresol, with hydrolysis in Creatinine in urine	Sampling time: End of shift.	0.3 mg/g	ACGIH BEL (01 2010)
Xylene, mixed isomers	Methylhippuric acids in Creatinine in urine	Sampling time: End of shift.	1.5 g/g	ACGIH BEL (01 2010)
Ethylbenzene	Sum of mandelic acid and phenylglyoxylic acid in Creatinine in urine	Sampling time: End of shift at end of work week.	0.7 g/g	ACGIH BEL (01 2010)
Ethylbenzene	Ethyl benzene in End-exhaled air	Sampling time: Not critical.		ACGIH BEL (01 2010)

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n-hexane	2,5-Hexanedion, without hydrolysis in Urine	Sampling time: End of shift at end of work week.	0.4 mg/l	ACGIH BEL (01 2010)
Benzene	S- Phenylmercaptu ric acid in Creatinine in urine	Sampling time: End of shift.	25 μg/g	ACGIH BEL (01 2010)
Benzene	t,t-Muconic acid in Creatinine in urine	Sampling time: End of shift.	500 µg/g	ACGIH BEL (01 2010)
Styrene	styrene in Venous blood	Sampling time: End of shift.	0.2 mg/l	ACGIH BEL (01 2010)
Styrene	Mandelic acid plus phenylglyoxylic acid in Creatinine in urine	Sampling time: End of shift.	400 mg/g	ACGIH BEL (01 2010)

Exposure Controls

: The level of protection and types of controls necessary will vary depending upon potential exposure conditions. Select controls based on a risk assessment of local circumstances. Appropriate measures include: Use sealed systems as far as possible. Adequate explosion-proof ventilation to control airborne concentrations below the exposure guidelines/limits. Local exhaust ventilation is recommended. Eye washes and showers for emergency use.

Personal Protective Equipment Respiratory Protection

Personal protective equipment (PPE) should meet recommended national standards. Check with PPE suppliers.

If engineering controls do not maintain airborne concentrations to a level which is adequate to protect worker health, select respiratory protection equipment suitable for the specific conditions of use and meeting relevant legislation. Check with respiratory protective equipment suppliers. Where air-filtering respirators are suitable, select an appropriate combination of mask and filter. Where air-filtering respirators are unsuitable (e.g. airborne concentrations are high, risk of oxygen deficiency, confined space) use appropriate positive pressure breathing apparatus. All respiratory protection equipment and use must be in accordance with local regulations. Respirator selection, use and maintenance should be in

accordance with the requirements of the OSHA Respiratory

Protection Standard, 29 CFR 1910.134.

Hand Protection

Personal hygiene is a key element of effective hand care. Gloves must only be worn on clean hands. After using gloves, hands should be washed and dried thoroughly. Application of a non-perfumed moisturizer is recommended. Suitability and durability of a glove is dependent on usage, e.g. frequency and duration of contact, chemical resistance of glove material,

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glove thickness, dexterity. Always seek advice from glove suppliers. Contaminated gloves should be replaced.

Eye Protection

: Chemical splash goggles (chemical monogoggles).

Protective Clothing

: Chemical resistant gloves/gauntlets, boots, and apron (where

risk of splashing).

9. PHYSICAL AND CHEMICAL PROPERTIES

Appearance

: Bronze. Clear, bright liquid.

Odour На

: Hydrocarbon. : Not applicable.

Freezing Point

: -58 °C / -72 °F

Flash point

: -40 °C / -40 °F (ASTM D-93 / PMCC)

Upper / lower Flammability

: 1.3 - 7.6 %(V)

or Explosion limits

Auto-ignition temperature

: > 250 °C / 482 °F

Specific gravity

: 0.72 - 0.76

Density

: ca. 0.78 g/cm3 at 15 °C / 59 °F

Water solubility

: Negligible.

Kinematic viscosity

: < 1 mm2/s at 40 °C / 104 °F

Vapour density (air=1)

10. STABILITY AND REACTIVITY

Stability

Stable under normal conditions of use.

Conditions to Avoid

Avoid heat, sparks, open flames and other ignition sources.

Materials to Avoid

Strong oxidising agents.

Products

Hazardous Decomposition : Hazardous decomposition products are not expected to form during normal storage. Thermal decomposition is highly

dependent on conditions. A complex mixture of airborne solids, liquids and gases, including carbon monoxide, carbon dioxide and other organic compounds will be evolved when this material undergoes combustion or thermal or oxidative

degradation.

11. TOXICOLOGICAL INFORMATION

Basis for Assessment

: Information given is based on product testing, and/or similar

products, and/or components.

Acute Oral Toxicity

: Low toxicity: LD50 >2000 mg/kg , Rat

Aspiration into the lungs when swallowed or vomited may

cause chemical pneumonitis which can be fatal.

Acute Dermal Toxicity

Low toxicity: LD50 >2000 mg/kg , Rabbit

Acute Inhalation Toxicity

Low toxicity: LC50 >20 mg/l / 1.00 h, Rat

High concentrations may cause central nervous system depression resulting in headaches, dizziness and nausea; continued inhalation may result in unconsciousness and/or

death.

Skin Irritation

Irritating to skin.

Eye Irritation **Respiratory Irritation** Moderately irritating to eyes (but insufficient to classify). Based on human experience, breathing of vapours or mists may cause a temporary burning sensation to nose, throat and

Material Safety Data Sheet

Carcinogenicity

According to OSHA Hazard Communication Standard, 29 CFR 1910.1200

lungs.

Sensitisation : Not expected to be a sensitiser.

Repeated Dose Toxicity : Kidney: caused kidney effects in male rats which are not

considered relevant to humans

Blood-forming organs: repeated exposure affects the bone

marrow. (Benzene)

Peripheral nervous system: repeated exposure causes

peripheral neuropathy in animals. (n-hexane)

Mutagenicity : May cause heritable genetic damage. (Benzene)

Mutagenicity studies on gasoline and gasoline blending streams have shown predominantly negative results.

: Known human carcinogen. (Benzene)

May cause leukaemia (AML - acute myelogenous leukemia).

(Benzene)

Inhalation exposure to mice causes liver tumours, which are

not considered relevant to humans.

Material	:	Carcinogenicity Classification
Gasoline, low boiling point	:	ACGIH Group A3: Confirmed animal carcinogen with unknown
naphtha		relevance to humans.
Gasoline, low boiling point	:	IARC 2B: Possibly carcinogenic to humans.
naphtha		
Xylene, mixed isomers	:	ACGIH Group A4: Not classifiable as a human carcinogen.
Xylene, mixed isomers	:	IARC 3: Not classifiable as to carcinogenicity to humans.
Toluene	:	ACGIH Group A4: Not classifiable as a human carcinogen.
Toluene	:	IARC 3: Not classifiable as to carcinogenicity to humans.
Ethanol	:	ACGIH Group A4: Not classifiable as a human carcinogen.
Ethylbenzene	:	ACGIH Group A3: Confirmed animal carcinogen with unknown
-		relevance to humans.
Ethylbenzene	:	IARC 2B: Possibly carcinogenic to humans.
Benzene	:	ACGIH Group A1: Confirmed human carcinogen.
Benzene	:	NTP: Known carcinogen.
Benzene	:	IARC 1: Carcinogenic to humans.
Benzene	:	OSHASP: Cancer hazard.
Naphthalene	:	ACGIH Group A4: Not classifiable as a human carcinogen.
Naphthalene	•	NTP: Anticipated carcinogen.
Naphthalene	:	IARC 2B: Possibly carcinogenic to humans.
Styrene	:	ACGIH Group A4: Not classifiable as a human carcinogen.
Styrene	:	NTP: Reasonably anticipated to be a human carcinogen.
Styrene	:	IARC 2B: Possibly carcinogenic to humans.

Reproductive and Developmental Toxicity

: Causes foetotoxicity at doses which are maternally toxic.

(Toluene)

May impair fertility at doses which produce other toxic effects.

(n-hexane)

Many case studies involving abuse during pregnancy indicate that toluene can cause birth defects, growth retardation and

learning difficulties. (Toluene)

Ethanol, a component of this material, may cause birth defects

and/or miscarriages following high oral doses.

Additional Information : Exposure to very high concentrations of similar materials has been associated with irregular heart rhythms and cardiac

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According to OSHA Hazard Communication Standard, 29 CFR

arrest.

Prolonged and repeated exposures to high concentrations have resulted in hearing loss in rats. Solvent abuse and noise interaction in the work environment may cause hearing loss.

(Toluene)

Abuse of vapours has been associated with organ damage and

death. (Toluene)

May cause MDS (Myelodysplastic Syndrome). (Benzene)

12. ECOLOGICAL INFORMATION

Incomplete ecotoxicological data are available for this substance.

Acute Toxicity : Toxic: LL/EL/IL50 1-10 mg/l (to aquatic organisms) (LL/EL50

expressed as the nominal amount of product required to

prepare aqueous test extract).

Fish : Expected to be toxic: LL/EL/IL50 1-10 mg/l

Aquatic Invertebrates : Expected to be toxic: LL/EL/IL50 1-10 mg/l : Expected to be toxic: LL/EL/IL50 1-10 mg/l

Microorganisms : Expected to be harmful: LL/EL/IL50 10-100 mg/l

Mobility : Floats on water. Evaporates within a day from water or soil

surfaces. Large volumes may penetrate soil and could contaminate groundwater. Contains volatile constituents.

Persistence/degradability : Major constituents are expected to be inherently

biodegradable. The volatile constituents will oxidize rapidly by

photochemical reactions in air.

Bioaccumulation : Expected to be inherently biodegradable. Contains

constituents with the potential to bioaccumulate.

Other Adverse Effects : Films formed on water may affect oxygen transfer and damage

organisms.

13. DISPOSAL CONSIDERATIONS

Material Disposal : Recover or recycle if possible. It is the responsibility of the

waste generator to determine the toxicity and physical properties of the material generated to determine the proper waste classification and disposal methods in compliance with applicable regulations. Waste arising from a spillage or tank cleaning should be disposed of in accordance with prevailing regulations, preferably to a recognised collector or contractor. The competence of the collector or contractor should be established beforehand. Do not dispose into the environment, in drains or in water courses. Do not dispose of tank water bottoms by allowing them to drain into the ground. This will

result in soil and groundwater contamination.

Container Disposal : Drain container thoroughly. After draining, vent in a safe place

away from sparks and fire. Residues may cause an explosion hazard. Do not, puncture, cut, or weld uncleaned drums. Send to drum recoverer or metal reclaimer. Do not pollute the soil,

water or environment with the waste container.

Local Legislation : Disposal should be in accordance with applicable regional,

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According to OSHA Hazard Communication Standard, 29 CFR 1910.1200

national, and local laws and regulations. Local regulations may be more stringent than regional or national requirements and must be complied with.

14. TRANSPORT INFORMATION

US Department of Transportation Classification (49CFR)

Identification number

UN 1203 Gasohol

Proper shipping name Class / Division

3

Packing group

П

Emergency Response Guide

128

No.

Additional Information

Oil: This product is an oil under 49CFR (DOT) Part 130. If shipped by rail or highway in a tank with a capacity of 3500 gallons or more, it is subject to these requirements. Mixtures or solutions containing 10% or more of this product may also

be subject to this rule.

IMDG

Identification number

UN 1203

Proper shipping name

GASOLINE

Class / Division Packing group

Ш

Marine pollutant:

Yes

IATA (Country variations may apply)

Identification number

UN 1203

Proper shipping name

Gasoline

Class / Division

3

Packing group

Ш

15. REGULATORY INFORMATION

The regulatory information is not intended to be comprehensive. Other regulations may apply to this material.

Federal Regulatory Status

Additional Information

IARC has classified gasoline exhaust emissions as a Class 2B carcinogen - possibly carcinogenic to humans. Steps should be taken to prevent personal exposure to gasoline exhaust emissions.

Comprehensive Environmental Release, Compensation & Liability Act (CERCLA)

BR Reformulated Gasoline with

Reportable quantity: 100 lbs

According to OSHA Hazard Communication Standard, 29 CFR

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1910.1200

Material Safety Data Sheet

EtOH()

Gasoline, low boiling point naphtha () Reportable quantity: 100 lbs

Xylene, mixed isomers (1330-20-7) Reportable quantity: 100 lbs

Toluene (108-88-3) Reportable quantity: 1000 lbs

Ethanol (64-17-5) Reportable quantity: 100 lbs

Ethylbenzene (100-41-4) Reportable quantity: 1000 lbs

n-hexane (110-54-3) Reportable quantity: 5000 lbs

Benzene (71-43-2) Reportable quantity: 10 lbs

Naphthalene (91-20-3) Reportable quantity: 100 lbs

Cyclohexane (110-82-7) Reportable quantity: 1000 lbs

Styrene (100-42-5) Reportable quantity: 1000 lbs

Shell classifies this material as an "oil" under the CERCLA Petroleum Exclusion, therefore releases to the environment are not reportable under CERCLA.

Clean Water Act (CWA) Section 311

Xylene, mixed isomers (1330-20-7) Reportable quantity: 100 lbs

Toluene (108-88-3) Reportable quantity: 1000 lbs

Ethylbenzene (100-41-4) Reportable quantity: 1000 lbs

Benzene (71-43-2) Reportable quantity: 10 lbs

Naphthalene (91-20-3) Reportable quantity: 100 lbs

Cyclohexane (110-82-7) Reportable quantity: 1000 lbs

Styrene (100-42-5) Reportable quantity: 1000 lbs

Under Section 311 of the Clean Water Act (CWA) this material is considered an oil. As such, spills into surface waters must be reported to the National Response Centre at (800) 424-8802.

SARA Hazard Categories (311/312)

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1910.1200

Material Safety Data Sheet

Immediate (Acute) Health Hazard. Delayed (Chronic) Health Hazard. Fire Hazard.

SARA Toxic Release Inventory (TRI) (313)

Xylene, mixed isomers (1330-20-7)
Toluene (108-88-3)
1,2,4-Trimethylbenzene (95-63-6)
Ethylbenzene (100-41-4)
n-hexane (110-54-3)
Benzene (71-43-2)
Naphthalene (91-20-3)
Cyclohexane (110-82-7)
Styrene (100-42-5)

State Regulatory Status

Lietad

California Safe Drinking Water and Toxic Enforcement Act (Proposition 65)

This product contains a chemical known to the State of California to cause cancer. Known to the State of California to cause birth defects or other reproductive harm.

New Jersey Right-To-Know Chemical List

Yylene mixed isomers (1330-20-7)

Aylerie, mixeu isomers (1350-20-7)	Listea.
Toluene (108-88-3)	Listed.
Ethanol (64-17-5) 1,2,4-Trimethylbenzene (95-63-6)	Listed. Listed.
Ethylbenzene (100-41-4)	
n-hexane (110-54-3)	Listed. Listed.
Benzene (71-43-2)	Listed.
Naphthalene (91-20-3)	Listed.
Cyclohexane (110-82-7)	Listed.
Styrene (100-42-5)	Listed.

Pennsylvania Right-To-Know Chemical List

Gasoline, low boiling point naphtha ()	Listed.
Xylene, mixed isomers (1330-20-7)	Environmental hazard.
	Listed.
Toluene (108-88-3)	Environmental hazard.
,	Listed.
Ethanol (64-17-5)	Listed.

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According to OSHA Hazard Communication Standard, 29 CFR

Material Safety Data Sheet

1,2,4-Trimethylbenzene (95-63-6)

Environmental hazard.

Listed.

Ethylbenzene (100-41-4)

Environmental hazard.

Listed.

n-hexane (110-54-3)

Listed.

Benzene (71-43-2)

Special hazard.

Special nazard. Environmental hazard.

Listed.

Naphthalene (91-20-3)

Environmental hazard.

Listed

Cyclohexane (110-82-7)

Environmental hazard.

Listed.

Styrene (100-42-5)

Environmental hazard.

Listed.

16. OTHER INFORMATION

Additional Information

This document contains important information to ensure the safe storage, handling and use of this product. The information in this document should be brought to the attention of the person in your organisation responsible for advising on safety

matters.

NFPA Rating (Health,

Fire, Reactivity)

MSDS Version Number

: 1, 3, 0

: 6.0

MSDS Effective Date

09/09/2011

MSDS Revisions

A vertical bar (|) in the left margin indicates an amendment from the previous version.

MSDS Regulation

The content and format of this MSDS is in accordance with the OSHA Hazard Communication Standard, 29 CFR 1910.1200.

Uses and Restrictions

This product must not be used in applications other than those recommended in Section 1, without first seeking the advice of

the supplier.

This product is not to be used as a solvent or cleaning agent;

for lighting or brightening fires; as a skin cleanser.

This product is designed only to suit automotive applications and no provision is made for the requirements of aviation applications.

MSDS Distribution

The information in this document should be made available to

all who may handle the product.

Disclaimer

The information contained herein is based on our current knowledge of the underlying data and is intended to describe the product for the purpose of health, safety and environmental requirements only. No warranty or guarantee is expressed or implied regarding the accuracy of these data or the results to

be obtained from the use of the product.

BR Reformulated Gasoline with EtOH

MSDS# 401740M

Version 6.0

Effective Date 09/09/2011

According to OSHA Hazard Communication Standard, 29 CFR

1910.1200

Material Safety Data Sheet

Enterprisea LLC Schedule - Distribution Motiva Testing. Terminals



PQ-Schedule-1	Revision 5 (Motiva 2)	Page 1
Date Revised: 2/22/10	Review: Annual Review	Owner: Motiva Product Quality
Written by: Mary Beth Kinman	Reviewed by Aisha Albimani	Approved by: Mary Beth Kinman/ Del Wood

							Frequ	ency
Product	Location	Analyses	ASTM Method	Terminal Release Specifications	Sample	Sample Retain	Summer - VOC RVP/VOC BD	Winter- Non-VOC
EPA RBOB	P/L Receipts	Retain Sample	N/A		As Required	15 days	As required per LOP	As required per LOP
deligenment description	Marine receipts	Retain Sample	N/A	Review incoming COA prior to unloading	Vessel testing is coordinated by the Supply group	15 days	Every Receipt	Every Receipt
	Terminal Tanks (See Note 1)	RVP, Upper	D 5191	See Annual RVP/VOC Guidelines and Requirements	1 quart Upper Third	None	Every Receipt	Not Required
		RVP, Lower	D 5191	See Annual RVP/VOC Guidelines and Requirements	1 quart Lower Third	None	Every Receipt	Not Required
		API Gravity Appearance	D4052 D4176	Report (See Note 2) Clear and Bright @ 65-80°F	1 quart composite for these tests	15 days	Every Receipt Every Receipt	Every Receipt Every Receipt
	Terminal Tanks Blend Down	RVP, Top 1'	D 5191	See Annual RVP/VOC Guidelines and Requirements	1 quart at 1' Level	None	Blend-down Only	Not Required
	Period	VOC, Top 1' VOC, Upper VOC, Lower	Complex Model	See Annual RVP/VOC Guidelines and Requirements. Requirements are: 25% min reduction in Region 1, 23.4% min reduction in Region 2, and 21.4% min reduction in Region 2 Adjusted	1 quart at 1' Level 1 quart Upper Third 1 quart Lower Third		Blend- down Only. Per blend down letter. VOC samples to be sent to 3 rd Party lab for VOC certification	Not Required
EPA RFG Gasoline	Random Outbound Truck	% Ethanol	D5845	Petrospec Result 9.7 +/- 0.5 % Ethanol	All Level Truck Sample	None	Weekly during ethanol process and for a perio months or until terminal conformance to blend 9 One truck on one Lane schedule to include ever (See Note 5)	d of no less than 3 can demonstrate 6. (See Note 4) . Use a random
	Terminal Rack	% Ethanol (See Note 3)		10.0 ± 0.5% max by TMS Meter Blend Ratio Check.	N/A	None	Daily/ Folio	Daily/Folio

Note 1: VRU return tank shall be tested for RVP weekly during summer VOC control period.

Note 2: Max +/- 0.7 °API difference from reported value if COA is available.

Note 3: Daily/ folio terminal ethanol and product inventory reconciliation must be performed to determine % ethanol.

Note 4: Any change or modification that may impact the blending system shall be reviewed by Motiva PQ Analyst to determine if an additional testing period is required to check conformance to blend %.

Note 5: At the end of 3 months, send the truck data sheets and the Petrospec SQC chart to Motiva PQ Analyst for review. Be sure the meter throughput ratio check blend and out of spec BOL printing is configured and functioning properly for ethanol specification.



			ASTM			Sample	Testing F	requency
Product	Location	Analyses	Metho d	Terminal Release Specifications	Sample	Retain	Summer – VOC	Winter- Non-VOC
Conventional	P/L Receipts	Retain Sample	N/A		As Required	15 days	As required per LOP	As required per LOP
(CBOB, Suboctane and full octane gasoline)	Marine Receipts	RVP	D5191	Review incoming COA prior to unloading	Vessel testing is coordinated by the Supply group	15 days	Every Receipt	Every Receipt
	Terminal Tanks	RVP, Upper	D 5191	See Annual RVP/VOC Guidelines and Requirements	1 quart Upper Third	None	Every Receipt	Not Required
	(See Note 1)	RVP, Lower	D 5191	See Annual RVP/VOC Guidelines and Requirements	1 quart Lower Third	None	Every Receipt	Not Required
		API Gravity Appearance	D4052 D4176	Report (See Note 2) Clear and Bright	1 quart composite. for these tests	15 days	Every Receipt Every Receipt	Every Receipt Every Receipt
	Terminal Tanks Blend down Period	RVP, Top 1'	D 5191	See Annual RVP/VOC Guidelines and Requirements	1 quart of 1' Level	None	Blend-down Only	Not Required
All Oxygenated Conventional Gasoline	Random Outbound Truck	%Ethanol	D5845	Petrospec Result 9.7 +/- 0.5 % Ethanol	All Level Truck Sample	N/A	Weekly during ethanol Implementation process and for a period of no less than 3 months or until terminal can demonstrate conformance to blend %. (See Note 4)	
							One truck on one Lane. schedule to include ever (See Note 5)	y meter on each Lane
	Terminal Rack	%Ethanol (See Note 3)		10.0 ± 0.5% max by TMS Meter Blend Ratio Check	N/A	N/A	Daily/Folio	Daily/Folio

Note 1: VRU return tank shall be tested for RVP weekly during summer RVP control period.

Note 2: Max +/- 0.7 °API difference from reported value if COA is available.

Note 3: Daily/ folio terminal ethanol and product inventory reconciliation must be performed to determine % ethanol.

Note 4: Any change or modification that may impact the blending system shall be reviewed by Motiva PQ Analyst to determine if an additional testing period is required to check conformance to blend %.

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Note 5: At the end of 3 months, send the truck data sheets and the Petrospec SQC chart to Motiva PQ Analyst for review. Be sure the meter throughput ratio check blend and out of spec BOL printing is configured and functioning properly for ethanol specification.

	Location				ļ		Freq	uency
Product		l "	ASTM AS	Terminal Release Specifications	Sample	Sample Retain	Summer – VOC RVP/VOC BD	Winter- Non-VOC
Butane	Terminal Tanks (See Note 1)				Special sample cylinder	None		One sample at every 350,000 to a max of 500,000 gallons of butane received or one sample every 3 months, whichever is more frequent per tank.
New Installations Of Butane		(See Note 2)	definition of the second secon					

Note 1: Terminal changes sample cylinder and sends sample cylinder to Texon for testing.

Note 2: On new installations of butane a risk based sampling and testing procedure must be completed prior to start up to determine the sampling and testing required.

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			ASTM			Sample	Testing F	requency
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer - VOC	Winter- Non-VOC
Neat Ethanol	Import vessel	ASTM D4806		Must meet ASTM D4806 specifications for fuel grade ethanol applicable to the state.	Volumetric Composite	15 days	Every Import	Every Import
	Blending Skid For addition of Denaturant (See Note 1)	API Gravity	D4052	45.9-46.8° API Specification Range (specific gravity = 0.7937-0.7977)	15 minutes After start Of Blend	As required	Every Import	Every Import
Denatured Ethanol	Hub Terminals (Distributors of Ethanol)	API Gravity Appearance Ethanol Methanol Washed Gum Inorganic Chloride Copper Water Acidity PHe Sulfate Sulfur	D4052 D4176 D5501 D5501 D381 D7319 D1688 E1064 D1613 D6423 D4806	45.5 – 49.0 ° API Specification Range Clear & Bright, Free of Particulate 92.1 % Volume Minimum 0.5 % Volume Maximum 5.0 mg/100ml Maximum 10 ppmw Maximum or 8 mg/l Maximum 0.1 mg/Kg Maximum 1.0 % Volume Maximum 0.007% Weight Maximum 6.5 – 9.0 pH Range 4 ppmv Maximum for states which adopt current ASTM version. 30 ppmw Sulfur (current ASTM version)	All level or Volumetric Composite of tank	15 days	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt

Note 1: Target denaturant injection rate to meet IRS Farm Bill regulation max 2.50%.

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			ASTM			Sample	Testing Fr	equency
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer - VOC	Winter- Non-VOC
Denatured Ethanol	Truck Receipts	Appearance API Gravity	D4176 D4052	Clear and Bright @ 65-80°F 45.5 – 49.0 °API Target Range	4 oz Minimum Of all Truck Compartments	None	Every Receipt Every Receipt	Every Receipt Every Receipt
	Rail Receipts	Appearance API Gravity	D4176 D4052	Clear and Bright @ 65-80°F 45.5 – 49.0 °API Target Range	4 oz Minimum Of each Rail Car	Retain Until the Tank Is Released Or 15 days	Every Receipt Every Receipt	Every Receipt Every Receipt
	Barge Receipts	Appearance API Gravity Water	D4176 D4052 E1064	Clear and Bright @ 65-80°F 45.5 – 49.0 °API Target Range Max 1.0 % volume	4 oz Minimum Of each Compartment	15 days	Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt
	Terminal Tanks	API Gravity Appearance Ethanol Methanol Water	D4052 D4176 D5501 D5501 E1064	45.5 – 49.0 °API Target Range Clear and Bright @ 65-80°F 92.1 % Volume Minimum 0.5 % Volume Maximum Max 1.0 % volume, Third Party lab	Volumetric Composite	15 days	Once/Month/Tank Once/Month/Tank Once/Month/Tank Once/Month/Tank Once/Month/Tank	Once/Month/Tank Once/Month/Tank Once/Month/Tank Once/Month/Tank Once/Month/Tank

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			ASTM			Sample	Testing	Frequency
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter
Ultra Low Sulfur Diesel Marine (See N	P/L Receipts	API Gravity Haze Flashpoint Sulfur	D4052 D4176 D93 D7039	Report only Max 3 Min 125 °F Max 15 ppmw	1 quart during 1st 15 minutes of P/L receipt	15 days if QA issue is found	Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt
	Marine Receipts (See Note 1)	API Gravity Haze Flashpoint Sulfur	D4052 D4176 D93 D7039	Report only Max 3 Min 125 °F Max 15 ppmw	1 quart during 1st 30 minutes of marine receipt	15 days if QA issue is found	Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt
	Terminal – Tanks	API Gravity Haze Flashpoint Sulfur Conductivity	D4052 D4176 D93 D7039 D2624	Report only Max 2 Min 125 °F (Pipelines may have higher Specification) Max 15 ppmw Min 80pS/m (if tank contains additive) (See Note 2)	1 quart Composite	15 days	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt
	Terminal - Rack	Conductivity	D2624	Min 50pS/m (If additive added at rack)	1 quart All Level	None	Once/Week/Rack	Once/Week/Rack
Oversite Program	Southwest Research Institute (See note 3)	HFRR Lubricity Sulfur	D6079 D5453	Terminal will send one sample each month to Southwest Research Institute for testing in boxes Supplied. Results tracked by PQ Analyst.	1 quart All Level	15 days Southwest Research Inst.	Once/Month/Rack Or tank - where Lubricity added	Once/Month/Rack Or tank - where Lubricity added

Note 1: Review incoming COA prior to unloading. Vessel testing is coordinated by the Supply group.

Note 2: If <80pS/m at tank, test at rack to be sure Conductivity is at specification of a min 50pS/m.

Note 3: Terminal will send one sample each month to Southwest Research Institute for testing in boxes supplied. Results are tracked by PQ Analyst. All results are in the PQ Livelink folder. (Lubricity max 520um and Sulfur max 15ppm).

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		•	ASTM			Sample	Testing	Frequency
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter
EPA	P/L Receipts	API Gravity	D4052	Report only	1 quart during	15 days if	Every Receipt	Every Receipt
Low		Haze	D4176	Max 3	1st 15 minutes	QA issue	Every Receipt	Every Receipt
Sulfur		Flashpoint	D93	Min 125 °F	of P/L receipt	ls found	Every Receipt	Every Receipt
	Marine Receipts	API Gravity	D4052	Report only	1 quart during	15 days if	Every Receipt	Every Receipt
	(See Note 1)	Haze	D4176	Max 3	1st 30 minutes	QA issue	Every Receipt	Every Receipt
	1` '	Flashpoint	D93	Min 125 °F	of Marine receipt	is found	Every Receipt	Every Receipt
	Terminal – Tanks	API Gravity	D4052	Report only	1 quart Composite	15 days	Every Receipt	Every Receipt
		Haze	D4176	Max 2			Every Receipt	Every Receipt
		Flashpoint	D93	Min 125 °F (Pipelines may have higher specification)			Every Receipt	Every Receipt
		Sulfur	D7039	Max 500 ppmw			Every Receipt	Every Receipt
		Conductivity	D2624	Min 80pS/m (if tank contains additive) (See Note 3)			Every Receipt	Every Receipt
		*Kinematic Viscosity @ 40°C	D445	1.9-4.1 mm2/S at 40°C			Every Receipt	Every Receipt
		*Cetane Index	D976	Min 40			Every Receipt	Every Receipt
		*Cetane Index	D4737B	Min 40			Every Receipt	Every Receipt
		*T90 * (See Note 2)	D85	540 – 640 °F			Every Receipt	Every Receipt
	Terminal - Rack	Conductivity	D2624	Min 50pS/m (additive added at rack)	1 quart All Level	None	Once/Week/Rack	Once/Week/Rack
	Telfilliai - Rack	Conductivity	D2024	Will Soponii (additive added at rack)	i quait All Level	None	Oncerveennack	Office) Week/Nack
Oversite Program	Southwest Research Institute	HFRR Lubricity (See Note 4)	D6079	Terminal will send one sample each month to Southwest Research Institute for testing in boxes supplied. Results tracked by PQ Analyst.	1 quart All Level	Ship to Southwest Research Institute (15 days)	Once/Month/Rack Or tank - where Lubricity added	Once/Month/Rack Or tank - where Lubricity added

Note 1: Review incoming COA prior to unloading. Vessel testing is coordinated by the Supply group

Note 2: These tests (marked with *) must be done if transmix is upgraded to LSD.

Note 3: If <80pS/m at tank, test at rack to be sure Conductivity is at specification of a min 50pS/m.

Note 4: Terminal will send one sample each month to Southwest Research Institute for testing in boxes supplied. Results are tracked by PQ Analyst. All results are in the PQ Livelink folder. (Lubricity max 520um).

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			ASTM			Sample	Testing	Frequency
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter
EPA High Sulfur Diesel	P/L Receipts	API Gravity Haze Flashpoint	D4052 D4176 D93	Report only Max 3 Min 125 °F	1 quart during 1st 15 minutes of P/L receipt	15 days	Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt
	Marine Receipts (See Note 1)	API Gravity Haze Flashpoint	D4052 D4176 D93	Report only Max 3 Min 125 °F	1 quart during 1st 30 minutes of Marine receipt	15 days	Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt
	Terminal – Tanks	API Gravity Haze Flashpoint Conductivity	D4052 D4176 D93 D2624	Report only Max 2 Min 125 °F (Pipelines may have higher Specification Min 80pS/m (if tank contains additive) (See Note 2)	1 quart all Composite for all tests.	15 days	Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt
	Terminal - Rack	Conductivity	D2624	Min 50pS/m (additive added at rack)	1 quart All Level	None	Once/Week/Rack	Once/Week/Rack

Note 1: Review incoming COA prior to unloading. Vessel testing is coordinated by the Supply group **Note 2**: If <80pS/m at tank, test at rack to be sure Conductivity is at specification of a min 50pS/m.

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			ASTM			Sample	Testing F	requency
Product	Location	Analyses	Method	Terminal Acceptance/Release Specifications	Sample	Retain	Summer	Winter
Biodiesel B100/B99	Truck Receipts	API Gravity Appearance Flash point	D4052 D4176 LEL Reading (See Note 1)	Max +/- 0.7° API difference from COA Clear and Bright <1% * * If LEL >1% perform Flash point D93 Min 125 °F to check for gross gasoline contamination	1 quart all level	None	Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt
	Rail Receipts	API Gravity Appearance	D4052 D4176	Max +/- 0.7° API difference from COA Clear and Bright	1 quart	Retain until tank released or 15 days	Every Receipt Every Receipt	Every Receipt Every Receipt
	Terminal Tanks (Contract Lab) (See Note 2)	Kinematic Viscosity @ 40°C Acid Number Oxidation Stability Water Content	D445 D664 EN14112 D6304	1.9 – 6.0 mm²/s Max 0.50 % Wt. Min 6 hours Max 0.04 % Vol. (Max 400 ppmw)	1 quart composite	15 days	Once/Month Once/Month Once/Month Once/Month	Once/Month Once/Month Once/Month Once/Month
		Micro organism activity or Hy-Lite Kit	Microbmonitor or equivalent kit D7463	Max 4000 cfu/L or slight growth Max 2000 RLU	1 quart with bacon sampler		Once/Quarter	Once/Quarter
	Terminal Tanks (Terminal)	API Gravity	D4052	Max +/- 0.7° API difference from COA	1 quart composite	15 days	Once/Month	Once/Month
•		Haze Sulfur Flash point	D4176 D5453 or D7039 D93	Max 2 Max 10 ppmw Min 125 °F			Once/Month Once/Month Once/Month	Once/Month Once/Month Once/Month

Note 1: Contact Product Quality Analyst to discuss if delivery trucks are dedicated biodiesel written in contract – may not need to do LEL reading. Note 2: Send a copy of monthly and quarterly results to Product Quality Analyst.

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			ASTM			Sample	Testing I	requency
Product	Location	Analyses	Method	Terminal Acceptance/Release Specifications	Sample	Retain	Summer	Winter
B5 Diesel	Terminal Tank	Conductivity	D2624	Min 80pS/m (if tank contains additive) (See Note 3)	1 quart	15 days	Each Receipt	Each Receipt
(See Note 1)		B2-B5 Content	EN14078/D7371	B5: 4.5 vol% to 5.5 vol% Up to B5: 2 vol% up to 5.5 vol%			Each Receipt	Each Receipt
	Terminal – Rack	Conductivity	D2624	Min 50pS/m (if additive added at rack)	1 quart All Level	15 days	Once/Week/Rack	Once/Week/Rack
		HFRR Lubricity	D6079	Max 520 μm (0.520 mm)	1 quart All Level		Once/Month/Rack	Once/Month/Rack
		B2-B5 Content (See Note 2)	% biodiesel	B5: 4.5 vol% to 5.5 vol% Up to B5: 2 vol% up to 5.5 vol% by TMS Meter Blend Ratio check	N/A	None _.	Daily/Folio	Daily/Folio

Note 1: If biodiesel contains <2% B99/B100 lubricity additive is required.

Note 2: Daily/ folio terminal biodiesel and biodiesel blends inventory reconciliation must be performed to determine % biodiesel.

Note 3: If <80pS/m at tank, test at rack to be sure Conductivity is at specification of a min 50pS/m.

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			ASTM			Sample	Testing F	requency
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter
	P/L Receipts into Terminal	API Gravity Appearance	D4052 D4176	37–51°API (See Note 1) Clear and Bright	1 quart after P/L Switch	None	Every Receipt Every Receipt	Every Receipt Every Receipt
		API Gravity Appearance Flashpoint MSEP Millipore * Aqua-Glo * Conductivity	D4052 D4176 D56 D3948 D2276 D3240 D2624	37–51°API (See Note 1) Clear and Bright Min 105 °F Shell, industry 100 °F Min 85 MSEP Alert @ A – B – G 6 Max 15 ppm incoming Report	1 quart during 1st 15 minutes At P/L manifold * line sample	None	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt
		API Gravity Appearance Flashpoint MSEP Millipore * Aqua-Glo * Conductivity	D4052 D4176 D56 D3948 D2276 D3240 D2624	37–51°API (See Note 1) Clear and bright Min 105 °F Shell, industry 100 °F Min 85 MSEP Alert @ A – B – G 6 Max 15 ppm incoming Report	1 quart during 1st ½ of receipt At the P/L Manifold * line sample	None	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt
		API Gravity Appearance Flashpoint MSEP	D4052 D4176 D56 D3948	37–51°API (See Note 1) Clear and Bright Min 105 °F Shell, industry 100 °F Min 85 MSEP	1 quart during last 15 minutes At P/L manifold	None	Retain for testing if receipt tank is off-spec	Retain for testing If receipt tank is off-spec

Note 1: Max +/- 0.7 °API difference from reported value if COA is available.

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			ASTM			Sample	Testing Frequency	
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter
	Marine Receipts into terminal	Quantity Temperature Water	N/A N/A Visual	Report Report No Free Water	1 quart each compartment	None	Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt
		API Gravity Appearance Flashpoint MSEP	D4052 D4176 D56 D3948	37 – 51 Max. 0.7difference from reported CoA Clear and Bright Min 105 °F Shell, industry 100 °F Min 85 MSEP (See Note 1)	1 quart each compartment 1 quart composite	30 days	Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt
		API Gravity Appearance Flashpoint MSEP	D4052 D4176 D56 D3948	37 – 51 Max. 0.7difference from reported CoA Clear and Bright Min 105 °F Shell, industry 100 °F Min 85 MSEP (See Note 1)	1 quart at start Of receipt At shore side connecting flange	None	Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt
		API Gravity Appearance Flashpoint MSEP Millipore * Aqua-Glo * Conductivity	D3240 D4176 D56 D3948 D2276 D4052 D2624	37 – 51 Max. 0.7difference from reported CoA Clear and Bright Min 105 °F Shell, industry 100 °F Min 85 MSEP (See Note 1) Alert @ A – B – G 6 Max 15 ppm incoming Report (See Note 1)	1-quart in 1st 30 minutes Of receipt At shore side connecting flange	None	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt
		API Gravity Appearance Flashpoint MSEP Millipore * Aqua-Glo * Conductivity	D4052 D4176 D56 D3948 D2276 D3240 D2624	37 – 51 Max. 0.7difference from reported CoA Clear and Bright Min 105 °F Shell, industry 100 °F Min 85 MSEP (See Note 1) Alert @ A – B – G 6 Max 15 ppm incoming Report	1 quart at shore side Connecting Flange at mid-point Of receipt	None	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt

Note 1: Incoming overseas Marine Receipts may contain SDA (Static Dissipator Additive). This causes low MSEP results and measurable conductivity. Filtration is required before tank re-certification and going to rack.

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			ASTM			Sample	Testing Frequency		
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter	
Jet-A Ter	Terminal – Tanks	API Gravity, Upper * API Gravity, Middle* API Gravity, Lower*	D4052	37 – 51 Max. 0.7difference from reported CoA if available or max 0.7 difference from each level	1 gallon upper, middle and lower third of tank	None	Every Receipt	Every Receipt	
	Full ASTM D1655	Appearance * Haze * Flashpoint * Saybolt Color Existent Gum Corrosion Freeze Point Distillation, 10% Distillation, 50% Distillation, 90% Distillation, EP JFTOT @ 260°C Total Acidity Aromatics Mercaptans Total Sulfur Viscosity @ -4°F Net BTU's Smoke Point MSEP *	D4176 D4176 part2 D56 D 156 D 381 D 130 D 2386 D 86 D 86 D 86 D 86 D 3241 D 3242 D 1319 D 3227 D 2622 D 445 D 4529 D1322 D3948	Clear and Bright Max 1 Min 105 °F Shell, industry 100 °F (Pipeline Specifications may be different) Report Max 7.0 mg/100ml rating Max 1b Min -40 °F (minus 40 °F) Max 400 °F Report Report Report Max 572 °F Max 25 mm Hg Pressure & 3 Tube Rating Max 0.1 % Max 25 % Max 0.0030 % wt. Max 0.30 % wt. Max 8.0 Min 18400 BTU/lb Min 25 or Min 18 if Naphthalenes are < 3.0 Min 85 MSEP (See Note 1)	1 gallon composite * These field test must be completed at the terminal prior to recertification	30 days	Every Receipt Every Receipt	Every Receipt Every Receipt	

Note 1: Incoming overseas Marine Receipts may contain SDA (Static Dissipator Additive). This causes low MSEP results and measurable conductivity. Filtration is required before tank re-certification and going to rack.

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			ASTM			Sample	Testing	Frequency
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter
·	Terminal Filters	Aqua-Glo * Millipore * MSEP	D3240 D2276 D3948	Max 10 ppm incoming A-2, B-2 or G-2 or better Min 85 MSEP	1-quart at Inlet To pre-filter * line sample	30 days	Weekly Weekly Weekly	Weekly Weekly Weekly
		Conductivity Aqua-Glo * Millipore * MSEP	D2624 D3240 D2276 D3948	Within 30 CU of Automated CU Meter Max 10 ppm outgoing Alert @ A – B –G2 Min 85 MSEP	1-quart at outlet of filter/ separator * line sample	30 days	Weekly Weekly Weekly Weekly	Weekly Weekly Weekly Weekly
	Terminal – Rack	Conductivity Millipore * Aqua-Glo *	D2624 D2276 D3240	50 – 600 pS/m (Automated CU Meter) Alert @ A – B – G 2 Max 10 ppm outgoing	1-quart at truck rack sample point * line sample	15 days None None	Weekly Daily Daily	Weekly Daily Daily
	Transport Trucks Shipment	White Bucket	Visual	Clear and bright, free from particulates. No visible free or suspended water and no evidence of red dye	1 quart composite	15 days	Every truck	Every truck

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			ASTM			Sample	Testing Frequency		
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter	
Product AvGas 100 LL	Railcar Receipt (See Note 1)	API Gravity Color Appearance Particulates Free Water	D 1298 D 2392 D4176 Visual Visual	Max 0.7difference from reported value on CoA Blue Clear and Bright Free of Particulates None	1 Qt Amber White Bucket White Bucket White Bucket White Bucket	30 days None None None None	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	
	Truck Receipt	API Gravity Color Appearance Particulates Free Water	D 1298 D 2392 D4176 Visual Visual	Max 0.7difference from reported value on CoA Blue Clear and Bright Free of Particulates None	1 Qt Amber White Bucket White bucket White bucket White bucket	30 days None None None None	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	
	Tank Analyses (See Note 2)	API Gravity Color Appearance Particulates Free Water	D 1298 D 2392 D4176 Visual Visual	Max 0.7difference from reported value on CoA Blue Clear and Bright Free of Particulates None	1 Qt Amber White Bucket White bucket White bucket White bucket		Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt Every Receipt	

Note 1: Check the seals and grade plate of the railcar upon arrival. Review the CoA and check each receipt for compliance to the specifications in ASTM D910 prior to unloading the railcar.

Note 2: The terminal must supply a Release Certificate for each truck load of AvGas 100 that leaves the terminal.

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			ASTM			Sample	Testing Frequency		
Product	Location	Analyses	Method	Terminal Release Specifications	Sample	Retain	Summer	Winter	
Ма	P/L Receipts	API Gravity Appearance	D4052 D4176	Max 0.7 difference from reported if CoA is available Clear and Bright	1 quart during 1st 15 minutes at P/L manifold	None	Every Receipt Every Rec Every Receipt Every Rec		
	Marine Receipts	API Gravity Appearance	D4052 D4176	Max 0.7 difference from reported if CoA is available Clear and Bright	1-quart in 1 st 30 minutes at shore side connecting flange	None	Every Receipt Every Receipt	Every Receipt Every Receipt	
	Terminal Tanks	API Gravity Appearance Flashpoint MSEP	D4052 D4176 D56 D3948	Max 0.7 difference from reported if CoA is available Clear and Bright Min 105 °F Min 75	1 quart composite	30 days	Every Receipt Every Receipt Every Receipt Every Receipt	Every Receipt Every Receipt Every Receipt Every Receipt	

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Operations Data Files Herbicide MSDS's



ALLIGARE 90

NONIONIC LOW-FOAM WETTER/SPREADER SURFACTANT

Alkylpolyoxethylene and derivatives and humectant	90.0%
Other Ingredients:	10.0%
TOTAL:	00.0%

KEEP OUT OF REACH OF CHILDREN CAUTION!/PRECAUCIÓN!

Si usted no entiende la etiqueta, busque a alguien para que se la explique a usted en detalle. (If you do not understand the label, find someone to explain it to you in detail.)

Precautionary Statements: Do not take internally. Avoid skin contact. May cause skin and eye irritation.

FIRST AID

Call a poison control center or doctor immediately for treatment advice.

If Swallowed: Have person sip a glass of water if able to swallow. Do not induce vomiting unless told to do so by a poison control center or doctor. Do not give anything by mouth to an unconscious person.

If on Skin or Clothing: Take off contaminated clothing. Rinse skin immediately with plenty of water for 15-20 minutes.

If Inhaled: Move person to fresh air. If person is not breathing, call 911or an ambulance, then give artificial respiration, preferably mouth to mouth if possible.

If in Eyes: Hold eye open and rinse slowly and gently with water for 15-20 minutes. Remove contact lenses if present, after the first 5 minutes, then continue rinsing eye. Have the product container with you when calling a poison control center or doctor, or going for treatment.

SN: 001A-072307

Distributed By: Alligare, LLC 13 N. 8th Street, Opelika, AL 36801

IN CASE OF EMERGENCY, CALL CHEMTREC UNITED STATES: 1-800-424-9300 INTERNATIONAL: 1-202-483-7616

Alligare 90 13 N 8th Street Opelika, AL 36801 MATERIAL SAFETY DATA SHEET

1. PRODUCT IDENTIFICATION

TRADEMARK OR PRODUCT NAME: Alligare 90

SYNONYMS: None, mixture

CHEMICAL FAMILY: Nonionic Surfactant

GENERIC DESCRIPTION: Nonionic Surfactant Blend
MOLECULAR WEIGHT: Not applicable, mixture

2. HAZARDOUS INGREDIENTS

OSHA REGULATED

COMPONENT

CAS. NO

WT%

EXPOSURE LIMITS

None

Maximum of 1 ppm Ethylene Oxide (EO) (75-21-8) May be present in the product. The OSHA PEL and ACGIH TLV for EO is 1 ppm. (EO Statement for any formula containing a component that is ethoxylated-REMOVE THIS INSTRUCTION and change paragraph to Black)

3. EFFECTS OF OVEREXPOSURE

INHALATION: Inhalation not likely. Mist may cause irritation of the respiratory tract.

SKIN CONTACT: Brief contact is not irritating. Prolonged contact may cause redness.

EYE CONTACT: Slightly irritating. May cause redness, irritation.

INGESTION: May cause abdominal discomfort, nausea, vomiting and diarrhea.

OTHER HEALTH EFFECTS: None

The above listed potential effects of overexposure are based on actual data, results of studies performed upon similar compositions, component data, and/or expert review of the product. Overexposure to any chemical may result in enhancement of pre-existing and adverse medical condition and allergic reactions.

4. EMERGENCY FIRST AID

CALL A POISON CONTROL CENTER OR DOCTOR IMMEDIATELY FOR TREATMENT ADVICE.

IF SWALLOWED: Have person sip a glass of water if able to swallow. Do not induce vomiting unless told to do so by a poison control center or doctor. Do not give anything by mouth to an unconscious person.

IF ON SKIN OR CLOTHING: Take off contaminated clothing. Rinse skin immediately with plenty of water for 15-20 minutes.

IF INHALED: Move person to fresh air. If person is not breathing, call 911 or an ambulance, then give artificial respiration, preferably mouth to mouth if possible.

IF IN EYES: Hold eye open and rinse slowly and gently with water for 15-20 minutes. Remove contact lenses if present, after the first 5 minutes, then continue rinsing eye. Have the product container with you when calling a poison control center or doctor, or going for treatment.

5. REACTIVITY DATA

STABILITY: () unstable (x) stable

INCOMPATIBILITY (MATERIALS TO AVOID): Avoid strong oxidizing and reducing agents.

HAZARDOUS DECOMPOSITION PRODUCTS: Burning can produce carbon monoxide and/or carbon dioxide

HAZARDOUS POLYMERIZATION: () may occur (x) will not occur

CONDITIONS TO AVOID: Open flame or extreme heat.

6. PHYSICAL PROPERTIES

APPEARANCE AND ODOR: Light, golden liquid

BOILING POINT: NA

SPECIFIC GRAVITY: (Water=1) 1.03 +/- .05

VAPOR DENSITY: NA VAPOR PRESSURE: NA

EVAPORATION RATE: (butyl acetate = 1) NA

SOLUBILITY IN WATER: Soluble

7. NFPA HAZARD RATING (National Fire Protection Association

Flammability

Health: Exposure could cause irritation but only minor residual injury even if no treatment is given.

Health 1 0 Instability

Flammability: Exposure could cause irritation but only minor residual injury even if no treatment is given...

Special Hazard

Instability: Normally stable, even under fire exposure conditions, and are not reactive with water.

8. FIRE AND EXPLOSION HAZARD INFORMATION

FLASHPOINT: >200 °F
FLAMMABLE LIMITS: NA

EXTINGUISHING MEDIA: Foam, Water fog, Dry chemical, ABC fire extinguisher.

SPECIAL FIRE FIGHTING PROCEDURES: Self-contained positive breathing apparatus and protective clothing should be worn.

UNUSUAL FIRE HAZARD: None known

9. SPECIAL PRECAUTIONS

HANDLING AND STORAGE: Use with adequate ventilation. Wash thoroughly after handling. Keep away from heat, sparks and flames.

OTHER PRECAUTIONS: Keep in original container tightly closed. Do not reuse empty container. Avoid contact with eyes, skins, and clothing. Do not store with food, feed, or other material to be used or consumed by humans or animals.

10. SPECIAL PROTECTION INFORMATION

RESPIRATORY PROTECTION: Appropriate to chemical.

VENTILATION: Adequate ventilation. PROTECTIVE GLOVES: Impervious.

EYE PROTECTION: Wear chemical safety goggles. Do not wear contact lenses.

11. SPILL OR LEAK PROCEDURES

SPILLS OR RELEASES: If material is released or spilled wear eye and skin protection. Floor may be slippery; use care to avoid falling. Contain spill immediately with inert materials (e.g. sand, earth). Avoid discharge to natural waters. Transfer liquids and solid diking material to suitable containers for recovery or disposal.

WASTE DISPOSAL: Do not contaminate water, food or feed by storage or disposal. Dispose of in an approved waste disposal facility in accordance with all Federal, State, and Local Regulations.

CONTAINER DISPOSAL: Offer container for recycling or dispose of in a sanitary landfill or by other procedures approved by local regulations.

12. REGULATORY INFORMATION

COMPOUNDS WHICH REQUIRE REPORTING UNDER SARA TITLE III

Sara Regulated Compounds

Section

CAS NO.

Percent

None Known

13. OTHER INFORMATION

WARNINGI This product contains a detectable amount of ethylene oxide, which is known to the State of California to cause cancer and/or reproductive toxicity.

Ethoxylated products may contain residual amounts of ethylene oxide (EO) which can accumulate in the container headspace and be released into the ambient environment. This process is enhanced when the product is agitated, as during tank car loading and unloading, and blending operations. Ethylene oxide causes tumors in laboratory animals. The Occupational Safety and Health Administration (OSHA) Permissible Exposure Level (PEL) for EO is 1 ppm for an eight-hour time weighted average exposure. The standard regulates occupational exposure to EO from all sources, including products containing residual EO. It is the responsibility of the employer to comply with OSHA ethylene oxide standard (29) CFR 1910.1047).

The recommendation for safe handling and protection procedures is believed to be generally sultable for the standard uses of this compound. However, each user should identify his intended uses of this material and determine whether they are appropriate. All data included in this document is released as typical values and should not be utilized to determine the suitability of this material for a particular use or purpose. No warranty, either expressed or implied, is hereby made, nor do we give permission, inducement, or recommendations to practice any patented invention without a license. All data is offered for consideration, investigation, and verification purposes only.

Alligare Diuron 80DF

Alligare, LLC

Emergency Phone: Chemtrec 800-424-9300

Effective Date: May 08, 2007

1. PRODUCT AND COMPANY IDENTIFICATION

PRODUCT NAME: Alligare Diuron 80DF DESCRIPTION: A dry-flowable herbicide.

EPA Reg. No.: 81927-12

COMPANY IDENTIFICATION:

Alligare, LLC 13 North 8th Street Opelika, AL 36801

2. COMPOSITION / INFORMATION ON INGREDIENTS

Ingredient

Chemical Name

Formula C₉H₁₀Cl₂N₂O CAS#

Composition

Diuron

3-(3,4-dichlorophenyl)-1,1-dimethylurea

330-54-1

80%

3. HAZARD IDENTIFICATION

Health Hazards: Harmful if swallowed. Causes moderate eye irritation.

Physical Hazards: May release irritating or toxic fumes if burned.

Environmental Hazards: Do not apply directly to water, or to areas where surface water is present, or to intertidal areas below the mean high water mark. Do not contaminate water by cleaning of equipment or disposal of wastes. Do not apply when weather conditions favor drift from areas treated. Cover or incorporate spills.

4. FIRST AID

Have the product container or label with you when calling a poison control center or doctor, or going for treatment. You may also contact 1-800-424-9300 for emergency medical treatment information.

IF ON SKIN OR CLOTHING: Take off contaminated clothing. Rinse skin immediately with plenty of water for 15-20 minutes. Call a poison control center or doctor for treatment advice.

IF IN EYES: Hold eye open and rinse slowly and gently with water for 15-20 minutes. Remove contact lenses, if present, after the first 5 minutes, then continue rinsing eye. Call a poison control center or doctor for treatment advice.

IF SWALLOWED: Call a poison control center or doctor immediately for treatment advice. Have person sip a glass of water if able to swallow. Do not induce vomiting unless told to do so by a poison control center or doctor. Do not give anything by mouth to an unconscious person.

5. FIRE-FIGHTING MEASURES

Flash point: Not combustible.

Flammable Limits (LFL-UFL): N/A

Fire and Explosion Hazards: May thermally decompose in fire releasing irritating and toxic fumes. Extinguishing Medium: Foam, CO₂, dry chemical, or water spray (water stream may spread flames). Fire Fighting Equipment: Firefighters should be equipped with self-contained positive pressure

breathing apparatus and turnout gear.

Fire Fighting Instructions: Evacuate area of all unnecessary personnel and fight fire from a safe distance upwind. Contain contaminated water / firefighting water; do not allow to enter drains or waterways. Foam or dry chemical fire extinguishing systems are preferred to prevent environmental damage from excessive water runoff.

NFPA Ratings: Health - 2 / Flammability - 0 / Reactivity - 0

6. ACCIDENTAL RELEASE MEASURES

Personal Precautions: Isolate area and keep unnecessary and unprotected personnel from entering. Wear suitable personal protective clothing and equipment as described in Section 8 of this document. Extinguish sources of ignition nearby and downwind and ensure adequate ventilation.

Environmental Precautions: Do not discharge into soil / subsoil or into drains / surface water / groundwater.

Large Spills: Dike spillage and recover and retain as much free liquid as possible for reuse. Pick up remainder with suitable absorbent material. If spilled on the ground, the affected area should be excavated to a depth of 1 - 2 inches. Place into suitable containers for reuse or disposal in a licensed facility. After removal, thoroughly clean contaminated area with water. Collect wash water for approved disposal. Make sure that tools and equipment are adequately decontaminated.

7. HANDLING AND STORAGE

Handling: Wear appropriate personal protective clothing and equipment (see Section 8 below). Use only in a well-ventilated area. Avoid contact with eyes or clothing. Wash thoroughly with soap and water after handling. Wash hands before eating, drinking, chewing gum, using tobacco, or using the toilet. Remove clothing immediately if pesticide gets inside. Then wash thoroughly and put on clean clothing.

Storage: Keep out of reach of children and animals. Store product in original container only, away from other pesticides, fertilizer, food, or feed.

8. EXPOSURE CONTROLS / PERSONAL PROTECTION

Pesticide Applicators and Workers: Refer to the product label attached to the product.

Engineering Controls: Workplace should be equipped with a shower and eye-wash station.

Personal Protective Equipment (PPE):

Handlers must wear long-sleeved shirt and long pants, chemical-resistant gloves made of any waterproof material (such as polyethylene or polyvinylchloride), dust / mist respirator, shoes plus socks.

Follow manufacturer's instructions for cleaning/maintaining PPE. If no such instructions for washables, use detergent and hot water. Keep and wash PPE separately from other laundry.

9. PHYSICAL AND CHEMICAL PROPERTIES

Physical State: Off-white granules

Odor: Slightly sweet

pH: 8.4 - 8.6

Bulk Density: 0.62 g/mL (5.17 lbs/gal)

Solubility: Soluble

10. STABILITY AND REACTIVITY

CHEMICAL STABILITY: Stable under normal use and storage conditions. May decompose if heated.

CONDITIONS TO AVOID: Excessive heat. SUBSTANCES TO AVOID: None known.

HAZARDOUS REACTIONS: This product is chemically stable and no hazardous reactions should occur

if stored and handled as prescribed / indicated.

HAZARDOUS DECOMPOSITION PRODUCTS: When thermally decomposed, may release hazardous and / or toxic furnes (hydrogen chlorides, exides of carbon and nitrogen).

3

11. TOXICOLOGICAL INFORMATION

ACUTE ORAL TOXICITY LD₅₀ (rat): 1,879 mg/kg) ACUTE DERMAL TOXICITY LD₅₀ (rabbit): > 5,000 mg/kg ACUTE INHALATION TOXICITY

LC₅₀ (rat): > 2.03 mg/L

EYE IRRITATION: Mildly Irritating **SKIN IRRITATION:** Non-irritating

SKIN SENSITIZATION: Not a contact sensitizer

CARCINOGENICITY:
ACGIH: Not Listed
IARC: Not Listed
NTP: Not Listed
OSHA: Not Listed

MUTAGENIC TOXICITY: No data available.

REPRODUCTIVE TOXICITY: No data available.

12. ECOLOGICAL INFORMATION

Do not apply directly to water, to areas where surface water is present, or to intertidal areas below the mean high water mark. Do not contaminate water when disposing of equipment washwaters. Do not contaminate water used for irrigation or domestic purposes.

13. DISPOSAL CONSIDERATIONS

Do not contaminate water, food or feed by disposal.

PESTICIDE DISPOSAL: Do not contaminate water, food, or feed by storage or disposal. Wastes resulting from the use of this product may be disposed of on site or at an approved waste disposal facility.

CONTAINER DISPOSAL: Do not reuse container. Completely empty bag into application equipment. Then dispose of empty bag in a sanitary landfill, or incineration; if allowed by State and local authorities, by burning. If burned, stay out of smoke.

14. TRANSPORT INFORMATION

Containers < 125 lbs: Not Regulated by DOT -

Containers ≥ 125 lbs:

DOT PROPER SHIPPING NAME: UN3077, Environmentally Hazardous Substance, Solid, N.O.S.

(Diuron 80%), 9, PG III

REPORTABLE QUANTITY: 100 lbs.

DOT EMERGENCY RESPONSE GUIDE: 171

MARINE POLLUTANT: No

15. REGULATORY INFORMATION

FIFRA -

All pesticides are governed under the Federal Insecticide, Fungicide, and Rodenticide Act. The regulatory information presented below is pertinent only when this product is handled outside of the normal use and application as a pesticide.

SARA Title III – Section 302 Extremely Hazardous Substances Not listed

1

SARA Title III - Section 311/312 Hazard Categories

Immediate, Delayed

SARA Title III - Section 312 Threshold Planning Quantity

The threshold planning quantity (TPQ) for this product treated as a mixture is 10,000 lbs. This product contains no ingredients with a TPQ of less than 10,000 lbs.

SARA Title III - Section 313 Reportable Ingredients

Diuron (80%) CAS#: 330-54-1

CERCLA -

Diuron – 100 lbs. (≥ 125 lbs. of product)

California Prop 65 Status -

This product contains a substance (Diuron) known to the state of California to cause cancer.

16. OTHER INFORMATION

This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the MSDS contains all of the information required by CPR.

DISCLAIMER:

THE INFORMATION IN THIS MSDS IS BASED ON DATA AVAILABLE AS OF THE REVISION DATE GIVEN HEREIN, AND BELIEVED TO BE CORRECT. CONTACT ALLIGARE, LLC TO CONFIRM IF YOU HAVE THE MOST CURRENT MSDS. JUDGMENTS AS TO THE SUITABILITY OF THE INFORMATION HEREIN FOR THE INDIVIDUAL'S OWN USE OR PURPOSES IS NECESSARILY THE INDIVIDUAL'S OWN RESPONSIBILITY. ALTHOUGH REASONABLE CARE HAS BEEN TAKEN IN THE PREPARATION OF SUCH INFORMATION, ALLIGARE, LLC EXTENDS NO WARRANTIES, MAKES NO REPRESENTATIONS, AND ASSUMES NO RESPONSIBILITY AS TO THE ACCURACY OR SUITABILITY OF SUCH INFORMATION FOR APPLICATION TO THE INDIVIDUAL'S PURPOSES OR THE CONSEQUENCES OF ITS USE.

This Material Safety Data Sheet (MSDS) serves different purposes than and DOES NOT REPLACE OR MODIFY THE EPA-APPROVED PRODUCT LABELING (attached to and accompanying the product container). This MSDS provides important health, safety, and environmental information for employers, employees, emergency responders and others handling large quantities of the product in activities generally other than product use, while the labeling provides that information specifically for product use in the ordinary course.

MATERIAL SAFETY DATA SHEET Glyphosate 4 Plus Herbicide

Emergency Phone: Chemtrec 800-424-9300 Effective Date: February 13, 2007

1. PRODUCT AND COMPANY IDENTIFICATION

PRODUCT NAME: Glyphosate 4 Plus

Active Ingredient: Glyphosate (in the form of its isopropylamine salt)

Chemical Name: N-(phosphonomethyl)glycine

Chemical Formula: Ĉ₆H₁₇N₂O₅P

COMPANY IDENTIFICATION:

Alligare, LLC 13 North 8th Street Opelika, KS 36801

2. COMPOSITION / INFORMATION ON INGREDIENTS

Glyphosate Isopropylamine Salt

CAS No. 38641-94-0

41.0%

3. HAZARD IDENTIFICATION

EMERGENCY OVERVIEW

Causes moderate eye irritation. Harmful if swallowed or inhaled. Avoid breathing vapor or spray mist. Avoid contact with eyes, skin or clothing.

POTENTIAL HEALTH HAZARDS:

EYE-

Moderate eye irritant. Undiluted product may cause pain, redness and

tearing.

SKIN -

May be slightly irritating to the skin.

INGESTION -

No more than slightly toxic and no significant adverse health effects are expected to develop if a small amount (less than a mouthful) is swallowed.

POTENTIAL PHYSICAL HAZARDS:

May react with metals such as galvanized or mild steel to produce hydrogen gas, potentially forming a highly combustible gas mixture.

4. FIRST AID

IF IN EYES: Hold eye open and rinse slowly and gently with water for 15-20 minutes. Remove contact lenses, if present, after the first 5 minutes, then continue rinsing eye. Call a poison control center or doctor for treatment advice.

IF SWALLOWED: Call a poison control center or doctor immediately for treatment advice. Have person sip a glass of water if able to swallow. Do not induce vomiting unless told to do so by a poison control center or a doctor.

IF INHALED: Move person to fresh air. If person is not breathing, call 911 or an ambulance, then give artificial respiration (preferably by mouth-to-mouth) if possible.

IF ON SKIN OR CLOTHING: Take off contaminated clothing. Rinse skin immediately with plenty of water for 15-20 minutes. Call a poison control center or doctor for treatment advice.

Have the product container or label with you when calling a poison control center or doctor, or going for treatment. You may also contact 1-800-424-9300 for emergency medical treatment information..

5. FIRE-FIGHTING MEASURES

Flash point: Will not flash

Flammable Limits (LFL-UFL): N/A

Fire and Explosion Hazards: During a fire, product may generating irritating or toxic gasses

through thermal decomposition.

Means of Extinction: Use water spray, foam or dry chemical.

Fire Fighting Instructions: Evacuate area and fight fire from a safe distance. Approach from upwind to avoid hazardous vapors and decomposition products. A foam or dry chemical fire extinguishing system is preferred to prevent environmental damage from excessive water run off. If water is used, avoid heavy hose streams. If possible, dike and collect water used to fight fire to prevent/minimize run off.

Firefighting Equipment: Self-contained breathing apparatus with full face piece. Wear full firefighting turn-out gear (Bunker gear).

Hazardous Combustion Products: Carbon monoxide, nitrogen oxides, phosphorous oxides.

6. ACCIDENTAL RELEASE MEASURES

Clean up spills immediately. Isolate and post spill area. Wear protective clothing and personal protective equipment as prescribed in Section 8 "Exposure Controls/Personal Protection". Keep unprotected persons and animals out of area.

SMALL SPILL: Absorb spill with inert material such as dry sand, vermiculite or fuller's earth, then place in a chemical waste container.

LARGE SPILL: Dike large spills using absorbent or impervious material such as clay or sand. Recover and contain as much free liquid as possible for reuse. Allow absorbed material to solidify and scrape up for disposal. After removal, scrub the area with detergent and water and neutralize with dilute alkaline solutions of soda ash or lime.

7. HANDLING AND STORAGE

Keep out of reach of children and animals. Do not contaminate other pesticides, fertilizers, water, food or feed by storage or disposal. Wash thoroughly after handling this product.

Store above 10°F (-12°C) to keep product from crystallizing.

8. EXPOSURE CONTROLS / PERSONAL PROTECTION

Engineering Controls: To keep exposure to airborne contaminants below exposure limits, proper ventilation is required when handling or using this product. Local mechanical exhaust ventilation may be required. Facilities storing or using this material should be equipped with an eyewash facility and a safety shower.

Eyewear: Safety goggles are recommended when mixing, loading or cleaning equipment.

Clothing: All pesticide handlers must wear a long-sleeved shirt and long pants and shoes plus socks.

Gloves: Waterproof gloves are recommended when mixing, loading or cleaning equipment. NOTE: Remove clothing immediately if pesticide gets inside. Then wash thoroughly and put on clean clothing.

9. PHYSICAL AND CHEMICAL PROPERTIES

Appearance: Clear yellow to amber liquid

Odor: Slight amine odor

pH: 4.4

Flashpoint (PMA-4): N/A Specific Gravity: 1.17 g/ml Solubility in Water: Emulsifies

10. STABILITY AND REACTIVITY

CONDITIONS TO AVOID: Avoid temperatures above 115°F (46°C) and below 25°F (-5°C) CHEMICAL STABILITY: Product is normally stable. However, product may decompose if

heated.

HAZARDOUS DECOMPOSITION PRODUCTS: Heat and fire may result in thermal decomposition and the release of nitrogen oxides, phosphorous oxides and carbon monoxide.

INCOMPATIBILITY WITH OTHER MATERIALS: Strong oxidizers and bases, mild and galvanized steel.

POLYMERIZATION: Will not occur.

11. TOXICOLOGICAL INFORMATION

ACUTE ORAL TOXICITY

Oral LD₅₀ (rat): > 5,000 mg/kg

ACUTE DERMAL TOXICITY

Dermal LD₅₀ (rat, male): > 5,000 mg/kg

ACUTE INHALATION TOXICITY

Inhalation LC₅₀ (rat): > 2.5 mg/L

EYE IRRITANT

Rabbit - Moderate

SKIN IRRITATION

Rabbit - Mild

SENSITIZATION

Guinea pig - Non-Sensitizer

MEDICAL CONDITIONS AGGRAVATED BY EXPOSURE: None known.

CARCINOGENICITY:

ACGIH:

Not listed

IARC:

Not listed

NTP:

Not listed

OSHA:

Not listed

MUTAGENIC DATA: No evidence of mutagenic effects during in vivo and in vitro assays.

ADDITIONAL DATA: None.

12. ECOLOGICAL INFORMATION

ENVIRONMENTAL DATA: Do not apply directly to water, to areas where surface water is present or to intertidal areas below the mean high water mark. Do not contaminate water when cleaning equipment or disposing of equipment washwaters.

MAMMILIAN TOXICITY

This product is considered to be relatively nontoxic to dogs and other domestic animals; however, ingestion of this product or large amounts of freshly sprayed vegetation may result in temporary gastrointestinal irritation (vomiting, diarrhea, colic, etc.). If such symptoms are observed, provide the animal with plenty of fluids to prevent dehydration. Call a veterinarian if symptoms persist for more than 24 hours.

FISH TOXICITY

96 hour LC₅₀, Rainbow trout – 8.2 µg/L (technical)

96 hour LC₅₀, Bluegill – 5.8 μg/L (technical)

AVIAN TOXICITY

Oral LD₅₀, Bobwhite quail -- > 3,800 mg/kg (technical)

BEE TOXICITY: Non-toxic.

13. DISPOSAL CONSIDERATIONS

PESTICIDE DISPOSAL: Wastes resulting from the use of this product that cannot be used or chemically reprocessed should be disposed of in a landfill approved for pesticide disposal or in accordance with applicable Federal, state or local procedures. Emptied container retains vapor and product residue. Observe all labeled safeguards until container is cleaned, reconditioned, or destroyed.

CONTAINER DISPOSAL: For plastic containers, triple rinse (or equivalent). Then offer for recycling or reconditioning, or puncture and dispose of in a sanitary landfill, or incineration, or, if allowed by state and local authorities, by burning. If burned, stay out of smoke.

For refillable containers, do not reuse the container except for refill in accordance with a valid Alligare Repackaging or Toll Repackaging Agreement. If not refilled or returned to the authorized repackaging facility, triple rinse container, then puncture and dispose of in a sanitary landfill, or by incineration or, if allowed by state and local authorities, by burning. If burned, stay out of smoke.

For bulk containers, triple rinse (or equivalent) and wash with appropriate cleaners before reusing.

14. TRANSPORT INFORMATION

DOT PROPER SHIPPING NAME: Not regulated by DOT.

DOT HAZARD CLASS OR DIVISION: N/A

DOT UN/NA NUMBER: N/A
DOT PACKING GROUP: N/A
REPORTABLE QUANTITY: None
MARINE POLLUTANT: Not Listed

DOT EMERGENCY RESPONSE GUIDE: N/A

15. REGULATORY INFORMATION

FIFRA -

All pesticides are governed under the Federal Insecticide, Fungicide, and Rodenticide Act. The regulatory information presented below is pertinent only when this product is handled outside of the normal use and application as a pesticide.

OSHA HAZARD COMMUNICATION STANDARD STATUS: Not Regulated

SARA Title III - Section 302 Extremely Hazardous Substances

Not listed

SARA Title III - Section 311/312 Hazard Categories

Immediate

SARA Title III - Section 312 Threshold Planning Quantity

The threshold planning quantity (TPQ) for this product treated as a mixture is 10,000 lbs. This product contains no ingredients with a TPQ of less than 10,000 lbs.

SARA Title III - Section 313 Reportable Ingredients

None

CERCLA -

None

CALIFORNIA PROP 65 STATUS -

Not listed

16. OTHER INFORMATION

This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the MSDS contains all of the information required by CPR.

DISCLAIMER:

Alligare, LLC (the Company) warrants that this product conforms to the chemical description on the label in all material respects and is reasonably fit for the purpose referred to in the directions for use, subject to the exceptions noted below, which are beyond the Company's control. To the extent consistent with applicable law, the Company makes no other representation or warranty, express or implied, concerning the product, including no implied warranty of merchantability or fitness for a particular purpose. No such warranty shall be implied by law, and no agent or representative is authorized to make any such warranty on the Company's behalf.

To the extent consistent with applicable law, the exclusive remedy against the Company for any cause of action relating to the handling or use of this product is a claim for damages, and in no event shall damages or any other recovery of any kind exceed the price of the product which caused the alleged loss, damage, injury or other claim. To the extent consistent with applicable law, under no circumstances shall the Company be liable for any special, indirect, incidental or consequential damages of any kind, including loss of profits or income, and any such claims are hereby waived. Some states do not allow the exclusion or limitation of incidental or consequential damages.



SUPER MARKING DYE

SUPERSEDES: NONE

SECTION 1: PRODUCT AND COMPANY IDENTIFICATION

PRODUCT NAME:

SUPER MARKING DYE

MANUFACTURER:

ADDRESS:

Alligare, LLC. 13 N. 8th Street, Opelika, AL 36801

CHEMTREC PHONE:

US: 1-800-424-9300

International: 1-202-483-7616

CHEMICAL NAME:

Proprietary mixture

CHEMICAL FAMILY:

CHEMICAL FORMULA: Mixture

Colorant

Aquatic colorant

PRODUCT USE:

SECTION 1 NOTES:

INGREDIENT

None

SECTION 2: HAZARDOUS INGREDIENTS

SARA 313 % WT/% VOL REPORTABLE OSHA STEL ACGIH

Ceiling TWA

MSDS DATE: 4/17/08

STEL

CAS NO.

SECTION 2 NOTES: None

SECTION 3: HAZARDS IDENTIFICATION

ROUTES OF ENTRY:

Eyes, skin, ingestion, inhalation

POTENTIAL HEALTH EFFECTS

EYES:

May cause irritation and redness

SKIN:

May cause irritation and redness

INGESTION:

May cause nausea, abdominal discomfort and diarrhea

INHALATION:

Spray mist may be irritating to lungs

ACUTE HEALTH HAZARDS: None beyond above

CHRONIC HEALTH HAZARDS:

Repeated or extremely prolonged exposure may cause minor tissue damage

MEDICAL CONDITIONS GENERALLY AGGRAVATED BY EXPOSURE: Existing dermatitis may be exacerbated.

CARCINGGENICITY

OSHA: No

ACGTH: No

NTP: No TARC: NO

OTHER: NO

SECTION 3 NOTES: None

SECTION 4: FIRST AID MEASURES

If in Eyes: Hold eye open and rinse slowly and gently with water for 15-20 minutes. Remove contact lenses if present, after the first 5 minutes, then continue rinsing eye. Have the product container with you when calling a poison control center or doctor, or going for treatment.

If on Skin or Clothing: Take off contaminated clothing. Rinse skin immediately with plenty of water for 15-20 minutes.

If Swallowed: Have person sip a glass of water if able to swallow. Do not induce vomiting unless told to do so by a poison control center or doctor. Do not give anything by mouth to an unconscious person.

If Inhaled: Move person to fresh air. If person is not breathing, call 911 or an ambulance, then give artificial respiration, preferably mouth to mouth if possible.

NOTES TO PHYSICIANS OR FIRST AID PROVIDERS:

SECTION 4 NOTES: None

PAGE 1 OF 4



SUPER MARKING DYE

MSDS DATE: 4/17/08 SUPERSEDES: NONE

SECTION 5: FIRE-FIGHTING MEASURES

FLAMMABLE LIMITS IN AIR, UPPER: Unknown LOWER: Unknown

FLASH POINT:

F: >200 C: >93

METHOD USED:

PMCC

AUTOIGNITION TEMPERATURE:

F: Unknown C: Unknown

NFPA HAZARD CLASSIFICATION

HEALTH: 1

FLAMMABILITY: 0

REACTIVITY:

OTHER: -

EXTINGUISHING MEDIA:

Cool surrounding area.

SPECIAL FIRE FIGHTING PROCEDURES:

None

UNUSUAL FIRE AND EXPLOSION HAZARDS: None

HAZARDOUS DECOMPOSITION PRODUCTS:

None

SECTION 5 NOTES: Product is extremely soluble in water and will turn water blue but is safe for aquatic

SECTION 6: ACCIDENTAL RELEASE MEASURES

ACCIDENTAL RELEASE MEASURES:

Small spills: Absorb with appropriate absorbent material or mop.

Large spills: Dike area and absorb with appropriate absorbent material.

SECTION 6 NOTES:

SECTION 7: HANDLING AND STORAGE

HANDLING AND STORAGE: Store in a cool, dry place. Do not store near strong oxidizers.

SECTION 7 NOTES:

SECTION 8: EXPOSURE CONTROLS/PERSONAL PROTECTION

VENTILATION :

Normal ventilation will be adequate

RESPIRATORY PROTECTION:

None required

EYE PROTECTION:

Chemical goggles

SKIN PROTECTION:

Wear rubber gloves

OTHER PROTECTIVE CLOTHING OR EQUIPMENT:

Wear long sleeves and pants

WORK HYGIENIC PRACTICES:

None

EXPOSURE GUIDELINES:

None

SECTION 8 NOTES:

Product will stain skin but if washed off immediately, will cause no damage

PAGE 2 OF 4



SUPER MARKING DYE

SECTION 9: PHYSICAL AND CHEMICAL PROPERTIES

APPEARANCE:

Deep blue

ODOR:

None

PHYSICAL STATE:

Liquid

PH AS SUPPLIED:

~4 - 5

pH (Other): Unknown BOILING POINT:

Unknown Unknown

۳. Unknown

MELTING POINT:

C: Unknown

FREEZING POINT:

Unknown

Unknown

VAPOR PRESSURE (mmHg):

6

C:

Unknown Unknown

VAPOR DENSITY (AIR = 1):

G

F: Unknown

Unknown

SPECIFIC GRAVITY (H20 = 1):

~1.14

68 · C: 20

EVAPORATION RATE:

Slower than standard

BASIS (butyl acetate=1):

SOLUBILITY IN WATER: Soluble

VISCOSITY:

Unknown

F: C:

SECTION 9 NOTES:

None

SECTION 10: STABILITY AND REACTIVITY

STABILITY:

Stable X

Unstable

CONDITIONS TO AVOID (STABILITY):

None known

INCOMPATIBILITY (MATERIAL TO AVOID): Strong oxidizers

HAZARDOUS DECOMPOSITION OR BY-PRODUCTS:

None known

HAZARDOUS POLYMERIZATION:

Will not occur

CONDITIONS TO AVOID (POLYMERIZATION): None known

SECTION 10 NOTES:

SECTION 11: TOXICOLOGICAL INFORMATION

TOXICOLOGICAL INFORMATION:

Not available

SECTION 11 NOTES:

None

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MSDS DATE: 4/17/08 SUPERSEDES: NONE



SUPER MARKING DYE

SECTION 12: ECOLOGICAL INFORMATION

ECOLOGICAL INFORMATION:

Not available

SECTION 12 NOTES:

None

SECTION 13: DISPOSAL CONSIDERATIONS

WASTE DISPOSAL METHOD:

May be absorbed and landfilled or disposed of according to all laws and

MSDS DATE: 4/17/08 SUPERSEDES: NONE

regulations.

RCRA HAZARD CLASS:

Not regulated

SECTION 13 NOTES:

None

SECTION 14: TRANSPORT INFORMATION

U.S. DEPARTMENT OF TRANSPORTATION

PROPER SHIPPING NAME:

Not regulated

HAZARD CLASS: ID NUMBER: PACKING GROUP: LABEL STATEMENT:

OTHER AGENCIES:

None

SECTION 14 NOTES:

SECTION 15: REGULATORY INFORMATION

U.S. FEDERAL REGULATIONS

TSCA (TOXIC SUBSTANCE CONTROL ACT): No

CERCLA (COMPREHENSIVE RESPONSE COMPENSATION, AND LIABILITY ACT): Not regulated

SARA TITLE III (SUPERFUND AMENDMENTS AND REAUTHORIZATION ACT):

311/312 HAZARD CATEGORIES:

Not listed

313 REPORTABLE INGREDIENTS:

Not listed

STATE REGULATIONS:

INTERNATIONAL REGULATIONS:

None

SECTION 15 NOTES:

None

SECTION 16: OTHER INFORMATION

OTHER INFORMATION:

PREPARATION INFORMATION:

Prepared on 4/17/08

DISCLAIMER:

The recommendation for safe handling and protection procedures is believed to be generally suitable for the standard uses of this compound. However, each user should identify his intended uses of this material and determine whether they are appropriate. All data included in this document is released as typical values and should not be utilized to determine the suitability of this material for a particular use or purpose. No warranty, either expressed or implied, is hereby made, nor do we give permission, inducement, or recommendations to practice any patented invention without a license. All data is offered for consideration, investigation and verification purposes only. verification purposes only.

Alligare, LLC., 13 N. 8th Street, Opelika, AL 36801

PAGE 4 OF 4

MATERIAL SAFETY DATA SHEET SFM Extra™ Herbicide

Alligare, LLC

Emergency Phone: Chemtrec 800-424-9300

Effective Date: February 1, 2007

EPA Reg. No. 81927-5

1. PRODUCT AND COMPANY IDENTIFICATION:

PRODUCT NAME:

SFM Extra™

DESCRIPTION:

Dispersible granule herbicide.

COMPANY IDENTIFICATION:

Alligare, LLC 13 North 8th Street Opelika, AL 36801 888-255-4427

2. COMPOSITION / INFORMATION ON INGREDIENTS:

Ingredient	ChemicalName	Formula	CAS#	Composition
Sulfometuron-methyl	Methyl 2-[[[[(4,6-dimethyl-2-pyrimidinyl)amino]- carbonyl]amino]sulfonyl]benzoate	C15H16N4O5 S	74222-97-2	56.25%
Metsulfuron-methyl	Methyl 2-[[[(4-methoxy-6-methyl-1,3,5-triazln-2-yl) aminol-carbonyllaminolsulfonyilbenzoate	C14H15N5O6S	74223-64-6	15.0%

3. HAZARD IDENTIFICATION

HAZARDS TO HUMANS AND DOMESTIC ANIMALS: Harmful if absorbed through skin. Causes moderate eye irritation. Avoid contact with skin, eyes, or clothing.

POTENTIAL HEALTH EFFECTS:

- Eye contact may cause eye irritation with tearing, pain and / or blurred vision.
- Repeated dermal contact may cause skin irritation with itching, burning, redness, swelling or rash.
- Ingestion of high doses of Sulfometuron Methyl may lead to red blood cell destruction.

ENVIRONMENTAL HAZARDS: This herbicide is injurious to plants at extremely low concentrations. Nontarget plants may be adversely affected from drift and run-off. Do not apply directly to water, or to areas where surface water is present or to intertidal areas below the mean high water mark. Do not contaminate water when disposing of equipment wash water.

4. FIRST AID

IF ON SKIN OR CLOTHING: Take off contaminated clothing. Rinse skin immediately with water for 15-20 minutes. Call a poison control center or doctor for treatment advice.

IF IN EYES: Hold eye open and rinse slowly and gently with water for 15-20 minutes. Remove contact lenses, if present, after the first 5 minutes, then continue rinsing eye. Call a poison control center or doctor for treatment advice.

5. FIRE-FIGHTING MEASURES

Flash point: N/A

Flammable Limits (LEL): 0.092 g/L Fire and Explosion Hazards: None known.

Means of Extinction: Use water spray, carbon dioxide, foam or dry chemical.

Fire Fighting Instructions: Evacuate area. If area is exposed to fire and conditions permit, allow fire to burn itself out. Dike runoff and do not allow runoff to enter sewers, storm drains or waterways.

Thoroughly decontaminate firefighting equipment after use.

Firefighting Equipment: Self-contained breathing apparatus with full face piece and full bunker gear.

Hazardous Combustion Products: May produce irritating / toxic gasses and vapors.

6. ACCIDENTAL RELEASE MEASURES

Clean up spills immediately observing the precautions in Section 8 of this MSDS. Isolate the hazard area and keep unnecessary and unprotected personnel from entering. Prevent material from contaminating soil or from entering sewage and drainage systems and bodies of water.

SMALL SPILLS: Scoop up material and place in a container for reuse or disposal. Clean contaminated floors and objects thoroughly with water, observing all environmental regulations.

LARGE SPILLS: Avoid creating a dust cloud and take all possible measures to reduce airborne dust. Vacuum, shovel or sweep up material and place in a container for reuse or disposal. After removal, flush contaminated area thoroughly with water, observing all environmental regulations.

7. HANDLING AND STORAGE

Do not allow to come into contact with skin, eyes and clothing. Remove and wash contaminated clothing before reuse. Wash thoroughly with soap and water after handling and before eating, drinking, chewing gum, using tobacco or using the toilet.

Store in a cool, dry place and in such a manner as to prevent cross contamination with other pesticides, fertilizers, food, and feed. Store in original container and out of the reach of children, preferably in a secured storage area.

8. EXPOSURE CONTROLS / PERSONAL PROTECTION

Engineering Controls: Facilities storing or utilizing this material should be equipped with an eyewash station and a safety shower.

Protective Clothing: Long-sleeved shirt, long pants and shoes plus socks.

General: Wash thoroughly with soap and water after handling. Discard clothing and other absorbent materials that have been heavily contaminated with this product; do not reuse them. Follow the manufacturer's instructions for cleaning and maintaining PPE. If no such instructions for washables exist, use detergent and hot water. Keep and wash PPE separately from other laundry.

9. PHYSICAL AND CHEMICAL PROPERTIES

Appearance: Fine light-tan powder

Odor: Faint sulfur odor

pH: 5.0 - 6.3

Bulk Density: 0.64 - 0.74 g/ml Flashpoint (PMA-4): N/A Solubility in Water: Insoluble

10. STABILITY AND REACTIVITY

CONDITIONS TO AVOID: Stable under normal use and transportation situations.

HAZARDOUS DECOMPOSITION PRODUCTS: Data not available.
INCOMPATIBILITY WITH OTHER MATERIALS: None known.

POLYMERIZATION: Will not occur.

11. TOXICOLOGICAL INFORMATION

ACUTE ORAL TOXICITY Oral LD_{so} (rat): > 5,000 mg/kg ACUTE DERMAL TOXICITY

Dermal LD₅₀ (rat): > 5,000 mg/kg ACUTE INHALATION TOXICITY

Inhalation LC₅₀ (rat): > 5.3 mg/L

EYE IRRITANT

Rabbit - Mildly irritating

SKIN IRRITATION

Rabbit - Slight to mildly irritating

SENSITIZATION

Guinea Pig - Not a contact sensitizer

MEDICAL CONDITIONS AGGRAVATED BY EXPOSURE: None known.

CARCINOGENICITY:

ACGIH: Not listed IARC: Not listed NTP: Not listed OSHA: Not listed

MUTAGENIC DATA: No evidence of mutagenic effects during in vivo and in vitro assays.

ADDITIONAL DATA: Not known to cause reproductive or birth defects at normal exposure levels.

12. ECOLOGICAL INFORMATION

This herbicide is injurious to plants at extremely low concentrations. Nontarget plants may be adversely affected from drift and run-off. Do not apply directly to water, or to areas where surface water is present or to intertidal areas below the mean high water mark. Do not contaminate water when disposing of equipment wash water.

13. DISPOSAL CONSIDERATIONS

Do not contaminate water, food or feed by disposal.

PESTICIDE DISPOSAL: Pesticide wastes are toxic. Improper disposal of excess pesticide, or rinsate is a violation of Federal Law. If these wastes cannot be disposed of by use according to label instructions, contact your State Pesticide or Environmental Control Agency, or the Hazardous Waste Representative at the nearest EPA Regional Office for guidance.

CONTAINER DISPOSAL: Triple rinse (or equivalent). Then offer for recycling or reconditioning, or puncture and dispose of in a sanitary landfill, or incineration, or, if allowed by state and local authorities, by burning. If burned, stay out of smoke.

14. TRANSPORT INFORMATION

DOT PROPER SHIPPING NAME: Not Regulated by DOT

DOT HAZARD CLASS OR DIVISION: N/A

4

DOT UN/NA NUMBER: N/A
DOT PACKING GROUP: N/A
REPORTABLE QUANTITY: N/A
MARINE POLLUTANT: Not Listed

DOT EMERGENCY RESPONSE GUIDE: N/A

15. REGULATORY INFORMATION

FIERA -

All pesticides are governed under the Federal Insecticide, Fungicide, and Rodenticide Act. The regulatory information presented below is pertinent only when this product is handled outside of the normal use and application as a pesticide.

SARA Title III – Section 302 Extremely Hazardous Substances

Not Listed

SARA Title III - Section 311/312 Hazard Categories

Immediate

SARA Title III - Section 312 Threshold Planning Quantity

N/A

SARA Title III - Section 313 Reportable Ingredients

None

CERCLA -

Not Listed

CALIFORNIA PROP 65 STATUS -

Not Listed

16. OTHER INFORMATION

This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the MSDS contains all of the information required by CPR.

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Brooklyn Residuals
1997-2011

NEWTOWN CREEK RFI - TOTAL RESIDUALS SHIPPED 1997-2011

Totals - 2,333,256 lbs. or 1,166 tons

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FACILITY ID	MANIFEST NO	RIPR NO	TRANS	PHILIP SERVICES,	TSDF Date	SHIP Num =	RESIDUAL TYPE	STREAM DESC	#	CONT.	AMT	UNITS	LBS	TONS
58603	37931	83085	EQ-NORTHEA	REPUBLIC DIV	08/05/10	DOT027	DOT-HAZARDOUS	ASBESTOS, NON-FRIABLE	1 0	см	3.5	Т	7000	3.5
				PHILIP SERVICES,	55,55,55									
58603	37932	83085	EQ-NORTHEA	REPUBLIC DIV	08/05/10	DOT027	DOT-HAZARDOUS	ASBESTOS, NON-FRIABLE	10	СМ	1.09	T	2180	1.09
58603	129		FRANKLIN	NORTHLAND ENVIRONMENTAL, INC.	07/18/01	NH5180	NON-HAZARDOUS	BLASTING GRIT W/ EPOXY COAT	1 [ОМ	800	Р	800	0.4
58603	219		FRANKLIN	NORTHLAND ENVIRONMENTAL, INC.	08/01/01	NH0015	NON-HAZARDOUS	BLASTING GRIT	2 [DM	1600	Р	1600	0.8
58603	408	<u></u>	FRANKLIN	NORTHLAND ENVIRONMENTAL, INC.	10/19/01	NH0015	NON-HAZARDOUS	BLASTING GRIT	12 [ОМ	9600	Р	9600	4.8
58603	415		FRANKLIN	NORTHLAND ENVIRONMENTAL, INC.	10/19/01	NH0001	NON-HAZARDOUS	SOIL (CUTTINGS/BORING)	1 [DM	400	Р	400	0.2
58603	853		FREEHOLD	REPUBLIC ENV SYS (PA), INC.	11/12/02	NH0015	NON-HAZARDOUS	BLASTING GRIT	1 0	СМ	10	Т	0	0
58603	904		FRANKLIN	NORTHLAND ENVIRONMENTAL, INC.	01/23/03	NH0015	NON-HAZARDOUS	BLASTING GRIT	6 [DM	3500	Р	3500	1.75
58603	1508	56304	EQ-NORTHEA	CASIE ECOLOGY OIL SALVAGE, INC	12/22/06	NH0015	NON-HAZARDOUS	BLASTING GRIT	9 [OM	6300	Р	6300	3.15
58603	20393	78389	AUCHTER-NJ	CASIE ECOLOGY OIL SALVAGE, INC	06/26/09	NH5154	NON-HAZARDOUS	HOSES, OLD/USED	1 (СМ	2000	Р	2000	1
58603	32736		LORCO	CASIE ECOLOGY OIL SALVAGE, INC	05/17/00	NH0022	NON-HAZARDOUS	SOIL WITH GASOLINE	3 [DM	1200	Р	1200	0.6
58603	50105		SJ	SAFETY-KLEEN (TS), INC.	01/07/97	NH5066	NON-HAZARDOUS	BLASTING GRIT AND SOIL	10	CM	20	Υ	33686.9	16.84345
58603	52252-A	-	MANGIARDI	CWA, INC.	08/24/99	NH0022	NON-HAZARDOUS	SOIL WITH GASOLINE	1 [DT	30.2	Т	0	0
58603	52252-B		MANGIARDI	CWA, INC.	08/24/99	NH0022	NON-HAZARDOUS	SOIL WITH GASOLINE	1 0	DT	30.4	Т	.0	0
58603	52252-C		MANGIARDI	CWA, INC.	08/24/99	NH0022	NON-HAZARDOUS	SOIL WITH GASOLINE	1 [DT	29.4	τ	0	0
58603	52252-D		MANGIARDI	CWA, INC.	08/24/99	NH0022	NON-HAZARDOUS	SOIL WITH GASOLINE	1 [DT	15.7	Т	0	0
58603	53683		LORCO	CASIE ECOLOGY OIL SALVAGE, INC	12/04/00	NH0015	NON-HAZARDOUS	BLASTING GRIT	5 [DM	2000	Р	2000	1

1997-2011

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FACILITY ID	MANIFEST NO	RIPR NO	TRANS	DISPOSER	TSDF Date	SHIP Num	RESIDUAL TYPE	STREAM DESC	#	CONT.	AMT	UNITS	∴ LBS .	TONS
E9603	F7244	26274	FO NE	PHILIP SERVICES,	00/25/02	NUEGO	NON HAZARROUG	CDEAT CARROLL	4	61.4	40.0			
58603	57241	26274	EQ-NE	REPUBLIC DIV PHILIP SERVICES,	08/25/03	NH5033	NON-HAZARDOUS	SPENT CARBON	1	CM	12.3	T	0	(
58603	57241 A	26274	EQ-NE	REPUBLIC DIV	08/21/03	NH5033	NON-HAZARDOUS	SPENT CARBON	1	см	7	Т	0	(
				PHILIP SERVICES,										
58603	57241 B	26274	EQ-NE	REPUBLIC DIV	01/05/04	NH5033	NON-HAZARDOUS	SPENT CARBON	6	CF	2.3	Т	0	(
				ALCOSTI II AAAG										
58603	57672	28096	EQ-NE	NORTHLAND ENVIRONMENTAL, INC.	09/25/03	NH5045	NON-HAZARDOUS	FILTERS, GASOLINE	1	DM	100	Р	400	0.2
30003	37072	28030	EQ-NE	MICHIGAN DISPOSAL	09/23/03	NH3043	NON-HAZARDOOS	FILTERS, GASOLINE	. 4	Divi	400	<u> </u>	400	0.2
58603	57869	29059	EQ-NE	WASTE TREAT.	02/09/04	NH5096	NON-HAZARDOUS	TANK WIPER SEAL	8	DM	800	Р	800	0.4
				AARON OIL COMPANY,										
58603	59202	35220	EQ-NE	INC.	07/29/04	NH5151	NON-HAZARDOUS	FILTERS, USED OIL METAL	1	DM	200	Р	200	0.3
				NORTHAND										
58603	60240	39928	EQ-NE	NORTHLAND ENVIRONMENTAL, INC.	02/11/05	NH0015	NON-HAZARDOUS	BLASTING GRIT	2	DM	2200	P	2200	1.3
30003	00240	33320	EQTIVE	MICHIGAN DISPOSAL	02/11/03	14110012	11011-HAZAIIDOOS	DEASTING GRIT	3	DIVI	2200	<u> </u>	2200	1
58603	61828	47747	EQ-NE	WASTE TREAT.	11/10/05	NH0015	NON-HAZARDOUS	BLASTING GRIT	14	DM	10000	P	10000	į
														·
				NORTHLAND										
58603	62077	88815	EQ-NORTHEA	ENVIRONMENTAL, INC.	07/05/11	NH0015	NON-HAZARDOUS	BLASTING GRIT	4	DM	2000	P	2000	
58603	63463	55278	EQ-NORTHEA	CASIE ECOLOGY OIL SALVAGE, INC	09/07/06	NH0015	NON-HAZARDOUS	BLASTING GRIT	25	DM	20000	D	20000	10
	03 103	332,0	EQ NORTHEX	Sitevital, into	03/07/00	14110013	TOTTTAZARDOGS	BLASTING GITT	2.7	DIVI	20000	<u>'</u>	20000	
				NORTHLAND										
58603	77642	90334	EQ-NORTHEA	ENVIRONMENTAL, INC.	10/14/11	NH5277	NON-HAZARDOUS	SLUDGE, STRIP DRAIN	2	DM	400	P	400	0.2
E0603	77700	70605	50 1100 7117	INTERNATIONAL					_			_		
58603	77700	79625	EQ-NORTHEA	PETROLEUM CORP.	09/15/09	RC0068	NON-HAZARDOUS	USED OIL	1	Π	250	G	2085.1	1.04255
58603	907565	83647	LORCO	LORCO PETROLEUM	05/20/10	NH0001	NON-HAZARDOUS	SOIL (CUTTINGS/BORING)	6	DM	3000	Р	3000	1.5
		-		CASIE ECOLOGY OIL	,,									
58603	907579	81885	LORCO	SALVAGE, INC	01/14/10	NH5474	NON-HAZARDOUS	SOIL W/ GASOLINE & DIESEL	10	DM	5000	Р	5000	2.5
10 7 <u>8 -</u>		t váli	160 (164-) 7 (24 (244)				0 2 CEPECIA		Property.			136,000		- 116 - 116
58603	75228	Contractors	LAIDLAW-M	SAFETY-KLEEN (TS), INC.	11/26/96	RCRA5059	RCRA-HAZARDOUS	ABSORBENT MATERIAL WITH PET.		DM	55	G	458.7	0.2293
58603	75608	146	LAIDLAWTRN	SAFETY-KLEEN (TS), INC.	02/12/98	RCRA5078	RCRA-HAZARDOUS	ABSORBENT MAT. W/ GASOLINE	P46-848	DM	55	G	458.7	0.2293
		14		PURE EARTH RECYCLING		4.46								(%) oy e aliasa
58603	7805213JJK	85170	EQ-NORTHEA	(NJ), INC.	09/22/10	RCRA6387	RCRA-HAZARDOUS	PAINT CHIPS	1	DF	5	P	5	0.002
F0600				CASIE ECOLOGY OIL	/ /						[-			
58603	43		FRANKLIN	SALVAGE, INC	04/30/01	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	1	DM	150	Р	150	0.075

NEWTOWN CREEK RFI - TOTAL RESIDUALS SHIPPED

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Totals - 2,333,256 lbs. or 1,166 tons

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FACILITY ID	MANIFEST NO	RIPR NO	TRANS	DISPOSER	TSDF Date	SHIP Num	RESIDUAL TYPE	STREAM DESC	#	CONT.	AMT	UNITS	LBS	TONS
1	-			AARON OIL COMPANY,										
58603	143		FRANKLIN	INC.	07/16/01	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	1	DM	100	P	100	0.05
58603	427		FRANKLIN	AARON OIL COMPANY,	40/24/04	BB000C3	DECOVEDADIS	ADCODDENTAMAT IN/ CACOLINE			100		400	0.05
38003	427		FRANKLIN	INC. AARON OIL COMPANY,	10/24/01	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE ABSORBENTS W/ PETROLEUM	1	DM	100	P	100	0.05
58603	530		FRANKLIN	INC.	04/03/02	RP0125	RECOVERABLE	PROD	1		300	₽	300	0.15
				AARON OIL COMPANY,										
58603	572		FRANKLIN	INC.	04/03/02	RP0051	RECOVERABLE	FILTERS, GASOLINE	1	DM	300	P	300	0.15
				AARON OIL COMPANY,										
58603	656		FRANKLIN	INC.	07/25/02	RP0051	RECOVERABLE	FILTERS, GASOLINE	2		500	Р	500	0.25
58603	671		FRANKLIN	AARON OIL COMPANY, INC.	07/25/02	RP0099	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	6	DM	3600	D	3600	1.8
- 50005	0,1		TIV WWICH	AARON OIL COMPANY,	07/25/02	111 0033	RECOVERABLE	SEODGE, OIL, WATER SEI ARATOR		DIVI	3000	<u>'</u>	3000	1.0
58603	852		FRANKLIN	INC.	12/05/02	RP0051	RECOVERABLE	FILTERS, GASOLINE	12	DM	2400	P	2400	1.2
								·						
58603	27445	82042	LORCO	LORCO PETROLEUM	02/04/10	RP0001	RECOVERABLE	GROUNDWATER - GASOLINE	1	DM	60	G	500.42	0.25021
58603	13863	67280		CASIE ECOLOGY OIL SALVAGE, INC	02/28/08	RP0125	RECOVERABLE	ABSORBENTS W/ PETROLEUM PROD	,	DM	200	D	200	0.1
30003	13803	07280		CASIE ECOLOGY OIL	02/28/08	NFU123	RECOVERABLE	PROD		DIVI	200	<u> </u>	200	0.1
58603	14588	56893		SALVAGE, INC	11/08/06	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	18	DM	900	G	7506	3.753
58603	14598	57039	LORCO	LORCO PETROLEUM	11/22/06	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	4	DM	200	G	1668	0.834
58603	14902	57044	LODGO	CASIE ECOLOGY OIL	44/27/06	DD0435	0500/5048/5	ABSORBENTS W/ PETROLEUM			2000	D	2000	
36003	14902	37044	LORCO	SALVAGE, INC INTERNATIONAL	11/27/06	RP0125	RECOVERABLE	PROD	4	DM	2000		2000	
58603	151300	84546	EQ-NORTHEA	PETROLEUM CORP.	07/13/10	RP0044	RECOVERABLE	SLUDGE, TANK BOTTOM	1	TT	2000	G	16680.6	8.3403
														
58603	16195	90607	LORCO	LORCO PETROLEUM	08/29/11	RP0118	RECOVERABLE	WATER/DIESEL/ GASOLINE	1	П	385	G	3211	1.6055
50000	16240	F.C.002	ALICUTED ALL	LODGO DETROUELINA	44 (00 (00		2500/5049/5	S	_		<u>-</u>	_	0566	. 700
58603	16340	56892	AUCHTER-NJ	LORCO PETROLEUM	11/02/06	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	11	П	1147	G	9566	4.783
58603	16341	56892	AUCHTER-NJ	LORCO PETROLEUM	11/01/06	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	1	 	1400	G	11676	5.838
58603	16691	56892	AUCHTER-NJ	LORCO PETROLEUM	11/02/06	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	1	TT	900	G	7506	3.753
F0.000	105-1											_		
58603	19674	70608	AUCHTER-NJ	LORCO PETROLEUM CASIE ECOLOGY OIL	06/25/08	FLD268	RECOVERABLE	FUEL OIL AND WATER	1	Π	3050	G	25437	12.7185
58603	19969	74102	AUCHTER-NJ	SALVAGE, INC	01/08/09	RP0044	RECOVERABLE	SLUDGE, TANK BOTTOM	1	СМ	9.42	т	18840	9.42
					02,00,00	111 0044	TE OUT ENTINEE				3.72		200-10	3.72
58603	20391	78639	AUCHTER-NJ	LORCO PETROLEUM	06/29/09	RP0132	RECOVERABLE	SLUDGE, DIESEL TANK BOTTOM	1	π	1300	G	10842	5.421

NEWTOWN CREEK RFI - TOTAL RESIDUALS SHIPPED 1997-2011

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FACILITY ID	MANIFEST NO	RIPR NO	TRANS	DISPOSER	TSDF Date	SHIP Num	RESIDUAL TYPE	STREAM DESC	# CONT.	AMT	UNITS	LBS	TONS
58603	20772	80867	AUCHTER-NJ	LORCO PETROLEUM	11/04/09	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	1 177	2100	G	17514.6	8.7573
58603	20815	81613	AUCHTER-NJ	LORCO PETROLEUM	12/18/09	RP0044	RECOVERABLE	SLUDGE, TANK BOTTOM	1 TT	2800	G	23352.8	11.6764
58603	21602	82248	AUCHTER-NJ	LORCO PETROLEUM	02/04/10	RP0115	RECOVERABLE	ETHANOL AND WATER	1 77	403	G	3361.1	1.68055
58603	21949	64566	LORCO	CASIE ECOLOGY OIL SALVAGE, INC	10/24/07	RP0125	RECOVERABLE	ABSORBENTS W/ PETROLEUM PROD	2 DM	200	Р	200	0.1
58603	22500	89808	EQ-NORTHEA	LORCO PETROLEUM	08/03/11	RP0078	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1 17	5200	G	43369.5	21.68475
58603	26145	76543	LORCO	CASIE ECOLOGY OIL SALVAGE, INC	03/18/09	RP0125	RECOVERABLE	ABSORBENTS W/ PETROLEUM PROD	5 DM	250	Р	250	0.125
58603	269329	83373	EQ-NORTHEA	PETROLEUM CORP.	04/22/10	RP0044	RECOVERABLE	SLUDGE, TANK BOTTOM	1 17	1400	G	11676.4	5.8382
58603	274700	83934	EQ-NORTHEA	PETROLEUM CORP.	05/28/10	RP0118	RECOVERABLE	WATER/DIESEL/ GASOLINE	1 TT	4800	G	40033.3	20.01665
58603	274705	84317	EQ-NORTHEA	PETROLEUM CORP.	06/24/10	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	1 TT	5156	G	43002.5	21.50125
58603	40439		MILLER	AARON OIL COMPANY, INC.	11/03/97	NH5129	RECOVERABLE	SLUDGE, PETRO. PDX TK BOTTOM	1 TT	955	G	7964.7	3.98235
58603	53102		FRANKLIN	AARON OIL COMPANY, INC.	03/02/00	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1 77	4697	G	39173	19.5865
58603	53132		FRANKLIN	AARON OIL COMPANY, INC.	04/03/00	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	1 DM	1	D	458.7	0.22935
58603	53302		FRANKLIN	AARON OIL COMPANY, INC.	06/19/00	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	1 DM	55	G	458.7	0.22935
58603	53528		FRANKLIN	AARON OIL COMPANY, INC.	08/01/00	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1 177	3000	G	25020	12.51
58603	53606		FRANKLIN	AARON OIL COMPANY, INC.	09/18/00	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	1 DM	250	Р	250	0.125
58603	53685		FRANKLIN	AARON OIL COMPANY, INC.	07/14/00	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1 TT	4144	G	34561	17.2805
58603	54016		FRANKLIN	BRIDGEPORT TERMINAL	02/16/01	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1 177	5370	G	44785.8	22.3929
58603	56604	23204	FRANKLIN	INC.	05/07/03	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	3 DM	1000	Р	1000	0.5
58603	56606	23215	FRANKLIN	AARON OIL COMPANY, INC.	05/07/03	RP00062	RECOVERABLE	ABSORBENT MAT. W/GASOLINE	4 DM	1600	Р	1600	0.8
58603	56829	24162	FRANKLIN	AARON OIL COMPANY, INC.	05/07/03	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	3 DM	750	Р	750	0.375

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FACILITY ID	MANIFEST NO	RIPR NO	TRANS	DISPOSER	TSDF Date	SHIP Num	RESIDUAL TYPE	STREAM DESC	* # #	CONT.	AMT	UNITS	LBS	TONS
1				AARON OIL COMPANY,				1						
58603	57162	26067	FRANKLIN	INC.	07/17/03	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	1	DM	150	P	150	0.075
				U.S. FILTER RECOVERY		-		[
58603	57197	26205	EQ-NE	SERVICES	07/02/03	RP0044	RECOVERABLE	SLUDGE, TANK BOTTOM	1	П	5179	G	43192.9	21.59645
				AARON OIL COMPANY,										
58603	57425	26995	EQ-NE	INC.	08/28/03	RP0051	RECOVERABLE	FILTERS, GASOLINE	2	DM	400	Р	400	0.2
				AARON OIL COMPANY,				_			i			
58603	57673	28188	EQ-NE	INC.	10/15/03	RP00062	RECOVERABLE	ABSORBENT MAT. W/ GASOLINE	3	DM	600	P	600	0.3
				AARON OIL COMPANY,						_ 2 .		_		
58603	57870	29060	EQ-NE	INC.	10/15/03	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	1	DM	50	G	417	0.2085
50500	57074	20004	50.45	AARON OIL COMPANY,	10/15/00		2500/524215	ABSORBENTS W/ PETROLEUM				_		
58603	57871	29064	EQ-NE	INC.	10/15/03	RP0125	RECOVERABLE	PROD	2	DM	400	<u>P</u>	400	0.2
F9603	50027	34450	FO NE	U.S. FILTER RECOVERY	05/04/04	DD0070	DECOVEDABLE	TANK DOTTONA WATER CASOUNE	1	I T T T	2015	_	240174	15 00055
58603	59037	34459	EQ-NE	SERVICES AARON OIL COMPANY,	05/04/04	RP0078	RECOVERABLE	TANK BOTTOM WATER - GASOLINE ABSORBENTS W/ PETROLEUM	1	TT	3815	G	31817.1	15.90855
58603	59203	35222	EQ-NE	INC.	07/29/04	RP0125	DECOMEDABLE	PROD	7	DM	1050	Р	1050	0 535
36003	39203	33222	EQ-IVE	U.S. FILTER RECOVERY	07/29/04	RPU123	RECOVERABLE	PROD		DM	1050	Р	1050	0.525
58603	60184	39824	EQ-NE	SERVICES	11/10/04	RP0078	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1	π	4370	G	36445.8	18.2229
38003	00184	33024	LQ-NL	U.S. FILTER RECOVERY	11/10/04	KF0078	RECOVERABLE	TANK BOTTOW WATER - GASOLINE	<u></u>	11	4370	<u> </u>	30443.8	10.2223
58603	60208	41504	EQ-NE	SERVICES	01/14/05	RP0078	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1	TT	1335	G	11133.9	5.56695
30003	00200	41304	LQTIL	AARON OIL COMPANY,	01/14/03	111 0078	NECOVENABLE	ABSORBENTS W/ PETROLEUM		11	1555		11133.3	3.30033
58603	60239	39927	EQ-NE	INC.	01/12/05	RP0125	RECOVERABLE	PROD	3	DM	600	Р	600	0.3
	00203	000_/		AARON OIL COMPANY,	01,11,00	111 0123	11200121111022	ABSORBENTS W/ PETROLEUM			000			0.0
58603	60781	42789	EQ-NE	INC.	03/31/05	RP0125	RECOVERABLE	PROD	4	DM	800	Р	800	0.4
				U.S. FILTER RECOVERY	10,00,00				<u> </u>					
58603	61062	43871	EQ-NE	SERVICES	04/12/05	RP0078	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1	ТТ	3720	G	31024.8	15.5124
				AARON OIL COMPANY,			· 4·· <u>· ·</u> · ·	ABSORBENTS W/ PETROLEUM						
58603	61826	47745	EQ-NE	INC.	09/29/05	RP0125	RECOVERABLE	PROD	4	DM	800	Р	800	0.4
				AARON OIL COMPANY,				ABSORBENTS W/ PETROLEUM						
58603	63367	54363	EQ-NORTHEA	INC.	07/13/06	RP0125	RECOVERABLE	PROD	4	DM	800	P	800	0.4
	,			CASIE ECOLOGY OIL					_			_		
58603	78390	78390	EQ-NORTHEA	SALVAGE, INC	06/25/09	RP0130	RECOVERABLE	SLUDGE, OIL/WATER SEPARATOR	2	DM	110	G	917.4	0.4587
				CASIE ECOLOGY OIL				ABSORBENTS W/ PETROLEUM				·		
58603	79955	79955	EQ-NORTHEA	SALVAGE, INC	09/23/09	RP0125	RECOVERABLE	PROD	4	DM	1200	Р	1200	0.6
				AARON OIL COMPANY,				ABSORBENTS W/ PETROLEUM	—					
58603	80022	90333	EQ-NORTHEA	INC.	10/19/11	RP0125	RECOVERABLE	PROD	7	DM	700	Р	700	0.35
58603	84761	84761	EQ-NORTHEA	LORCO PETROLEUM	07/23/10	RP0118	RECOVERABLE	WATER/DIESEL/ GASOLINE	1	ТТ	5250	G	43786.5	21.89325
							,			_		_		
58603	85065	85065	EQ-NORTHEA	LORCO PETROLEUM	07/30/10	RP0118	RECOVERABLE	WATER/DIESEL/ GASOLINE	1_	Π	3000	G	25020.8	12.5104

93886 C021935 GAS1 GAS2	66820 62036	EQ-NORTHEA LORCO	SIEMENS WATER TECHNOLOGIES COR CASIE ECOLOGY OIL SALVAGE, INC	TSDF Date 02/05/08	SHIP Núm RP0118	RESIDUAL TYPE	STREAM DESC	# CONT.	TMA	UNITS	LBS	TONS
C021935 GAS1			TECHNOLOGIES COR CASIE ECOLOGY OIL	02/05/08	RP0118	25001521215						(
C021935 GAS1			CASIE ECOLOGY OIL	02/05/08	RP0118				j			1
GAS1	62036	LORCO	1			RECOVERABLE	WATER/DIESEL/ GASOLINE	1 TT	5000	G	41700	20.85
GAS1	02030	LORCO	ISALVAGE IN	07/05/07	DD0135	DECOVEDADLE	ABSORBENTS W/ PETROLEUM	2 5 4	750	D	750	0.375
			or terride, into	07/05/07	RP0125	RECOVERABLE	PROD	3 DM	750	Р	750	0.375
CASS	-	DSI	SHELL-IL	01/28/98	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1 TT	4310	G	35945.4	17.9727
GA32		DSI	SHELL-IL	03/31/98	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1П	5022	G	41883.5	20.94175
GAS3		DSI	SHELL-IL	04/21/98	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1П	5232	G	43634.9	21.81745
GAS4		DSI	SHELL-IL	05/26/98	RP0002	RECOVERABLE	TANK BOTTOM WATER - GASOLINE	1 TT	4665	G	38906.1	19.45305
			CASIE ECOLOGY OIL				ABSORBENTS W/ PETROLEUM					
NHZ36374	59296	LORCO		03/20/07	RP0125	RECOVERABLE	PROD	3 DM	500	Р	500	0.25
491		FRANKLIN	INC.	12/20/01	RP0017	RECYCLED	FILTERS USED OIL METAL	1 DM	300	Р	300	0.15
16695	56308	LORCO	LORCO PETROLEUM	11/23/06	RC0014	RECYCLED-NON	USED OIL FILTERS	1 DM	50	Р	50	0.025
21491	64567	LORCO	LORCO PETROLEUM	10/16/07	RC0014	RECYCLED-NON	USED OIL FILTERS	1 DM	350	Р	350	0.175
			SOIL SAFE, INC -							٠		
250	84009	EQ-NORTHEA		06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	28.24	T	56480	28.24
258	84009	EQ-NORTHEA	BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	31.18	Т	62360	31.18
259	84009	EQ-NORTHEA	SOIL SAFE, INC - BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	29.99	т	59980	29.99
		-	SOIL SAFE, INC -									
261	84009	EQ-NORTHEA	BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	27.97	T	55940	27.97
262	84009	EQ-NORTHEA	SOIL SAFE, INC - BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	24.92	т	49840	24.92
			SOIL SAFE, INC -								13.	
263	84009	EQ-NORTHEA	BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	33.06	Т	66120	33.06
			1 '									
301	84009	EQ-NORTHEA		06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	29.58	Т	59160	29.58
383	84009	FO-NORTHFA	1 .	06/10/10	BC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DM	33.75	т	66500	33.25
	5.005	EQ HORITIEA		00/10/10	1100022	NECT CLED-NOW	SOLE WITH GASOLINE	TIDIVI	33.23		00300	33.23
392	84009	EQ-NORTHEA	BRIDGEPORT	06/21/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	26.73	т	53460	26.73
438	84009	EU-NUBTHEV	SOIL SAFE, INC -		BC0022		SOIL WITH GASOLINE			т	56700	28.35
JIH	GAS3 GAS4 IZ36374 491 16695 21491 250 258 259 261 262 263 301 383	GAS3 GAS4 IZ36374 59296 491 I.6695 56308 I.1491 64567 I.500 I.6095 GAS3 DSI GAS4 DSI Z36374 59296 LORCO 491 FRANKLIN L6695 56308 LORCO 21491 64567 LORCO 250 84009 EQ-NORTHEA 258 84009 EQ-NORTHEA 259 84009 EQ-NORTHEA 261 84009 EQ-NORTHEA 262 84009 EQ-NORTHEA 263 84009 EQ-NORTHEA 301 84009 EQ-NORTHEA 383 84009 EQ-NORTHEA	DSI SHELL-IL	DSI	DSI	DSI	DSI SHELL-IL D4/21/98 RP0002 RECOVERABLE TANK BOTTOM WATER - GASOLINE	DSI	DSI SHELI-IL D4/21/98 RP0002 RECOVERABLE TANK BOTTOM WATER - GASOLINE 1 TT 5232	DSI SHELI-IL D4/21/98 RP0002 RECOVERABLE TANK BOTTOM WATER - GASOLINE 1 TT 5232 G	DSI SHELL-IL 0.4/21/98 RP0002 RECOVERABLE TANK BOTTOM WATER - GASOLINE 1 TT 5232 G 43634.9	

NEWTOWN CREEK RFI - TOTAL RESIDUALS SHIPPED 1997-2011

Totals - 2,333,256 lbs. or 1,166 tons

FACILITY ID	MANIFEST NO	RIPR NO	TRANS	DISPOSER :	TSDF Date	SHIP Num	RESIDUAL TYPE	STREAM DESC	# CONT.	AMT 🕮	UNITS	LBS	TONS
				SOIL SAFE, INC -									
58603	440	84009	EQ-NORTHEA	BRIDGEPORT	06/21/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	26.12	T	52240	26.12
58603	443	84009	EQ-NORTHEA	SOIL SAFE, INC - BRIDGEPORT	06/21/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	23.03	т	46060	23.03
30003	. 713	01003	EQ NONTIEA	SOIL SAFE, INC -	00/21/10	NCOUZZ	NECTOLED NON	JOIL WITH GASSEINE	101	25.05	<u> </u>	1 10000	
58603	484	84009	EQ-NORTHEA	BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	30.07	Т	60140	30.07
				SOIL SAFE, INC -									
58603	487	84009	EQ-NORTHEA	BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	27.84	T	55680	27.84
	_			SOIL SAFE, INC -					-				
58603	6	84009	EQ-NORTHEA	BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	25.03	<u> </u>	50060	25.03
58603	61827	47746	EQ-NE	AARON OIL COMPANY, INC.	09/29/05	RC0014	RECYCLED-NON	USED OIL FILTERS	1 DM	300	P	300	0.15
38003	01027	47740	EQ-NE	AARON OIL COMPANY,	09/29/03	NC0014	RECICLED-NON	OSED OIL FILTERS	1,0101	300	F	300	0.13
58603	63368	54364	EQ-NORTHEA	INC.	07/13/06	RC0014	RECYCLED-NON	USED OIL FILTERS	1 DM	200	Р	200	0.1
58603	C018532	59295	LORCO	LORCO PETROLEUM	03/16/07	RC0014	RECYCLED-NON	USED OIL FILTERS	1 DM	100	P	100	0.05
				SOIL SAFE, INC -							_		
58603	L4-7165	83319	EQ-NORTHEA	BRIDGEPORT SOIL SAFE, INC -	04/23/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	28.67	T	57340	28.67
58603	L4-7165 1	84009	EQ-NORTHEA	BRIDGEPORT	06/10/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	27.87	Т	55740	27.87
30003	£4-7103 I	04003	LONORTHLA	SOIL SAFE, INC -	00/10/10	110022	RECICLED-NON	JOIL WITH GASCLINE	101	27.07		33740	27.07
58603	L4-7165-2	83319	EQ-NORTHEA	BRIDGEPORT	04/23/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	29.66	Т	59320	29.66
		· · ·		SOIL SAFE, INC -									
58603	L4-7165-3	83319	EQ-NORTHEA	BRIDGEPORT	04/23/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	29.06	T'	58120	29.06
				SOIL SAFE, INC -									
58603	L4-7165-4	83319	EQ-NORTHEA	BRIDGEPORT	04/23/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	29.54	T	59080	29.54
58603	L4-7165-5	83319	EQ-NORTHEA	SOIL SAFE, INC - BRIDGEPORT	04/23/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	28.4	т .	56800	28.4
30003	L4-7103-3	03313	EQNORTIEA	SOIL SAFE, INC -	04/23/10	RCOOZZ	NECTCEED NON	SOLE WITH GASSEINE	101	20.4	•	30000	
58603	L4-7165-6	83319	EQ-NORTHEA	BRIDGEPORT	04/23/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	30.88	Т	61760	30.88
				SOIL SAFE, INC -									
58603	L4-7165-7	83319	EQ-NORTHEA	BRIDGEPORT	04/23/10	RC0022	RECYCLED-NON	SOIL WITH GASOLINE	1 DT	29.58	T	59160	29.58
58603	NHZ56111	67279	LORCO	LORCO PETROLEUM	02/25/08	RC0014	RECYCLED-NON	USED OIL FILTERS	1 DM	200	Ρ	200	0.1
-												2,333,256	THE STATE OF THE S
												lbs.	tons

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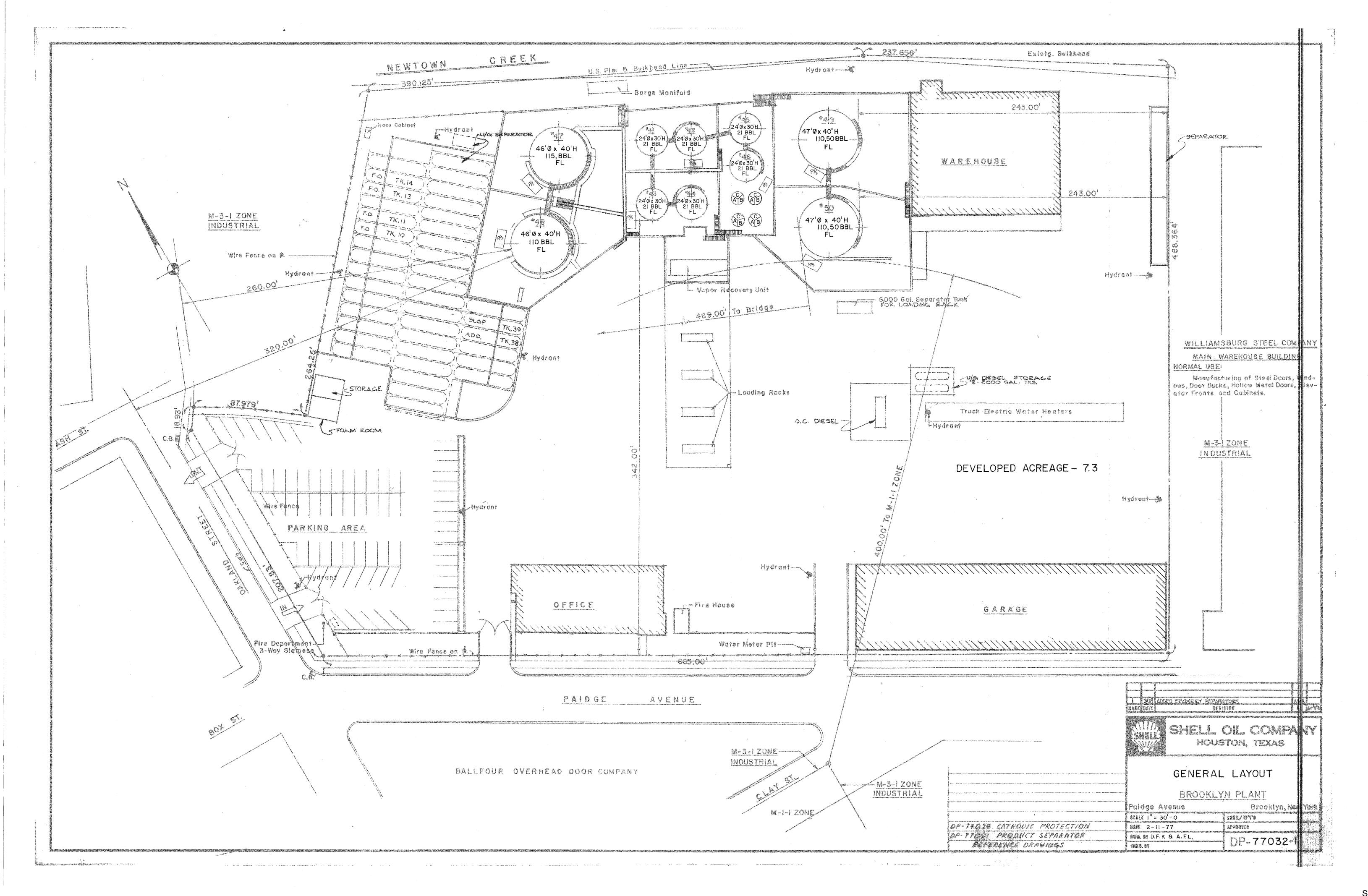
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58603-1977-02-11-FIG-01 (General

Layout - Brooklyn Plant - Shell).pdf



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Filename:

58603-2000-11-01-OTH-01 (Oil Water

Separator Results - Camin).pdf

Nov-01-00 01:19P Camin Cargo Control Corp. 1 908 862 2545

P.03

Camin Cargo Control, Inc.



Cargo Surveys Loss Control Consultation Analytical Testing Members Of API-ASTM Approved by US Customs and New York Morcantile Exchange

BRANCHES:

South Jessel-Philadelphia Boston New England Pasedens, Tense Coppy Chrish, Tenss Poli Adhan, Taxas Colfo Considor Dominious Parpuble Collegan allow-Monco Panizas

HEADQUARTERS:

New York - North Jersey 230 Marion Avenue Linden, New Jersey 07036 Tel: (908) 523-0616 Hax: (908) 862-2545

e-mail: cadm@eamincargo.com

CERTIFICATE OF QUALITY

Reported To : Steve Majid

Customer : Motiva Enterprise Brooklyn

25 Paidge Ave.

Brooklyn

NY 11222

FIIR No.

: 2000100038 Report Date : 11/01/2000

Location

: Oil/ water separator

Matrix

: Wastewater Date Sampled : 10/19/2000

Time Collected: 08:30:00 Date Received : 10/19/2000

Lab No. Sample IC	Laboratory Test	Method	Results	Units	MDL
29334026	Oil & Greese	1664 A	2.1	mġ/L	1.00
29334027	MTBE	EPA 602	2692	ug/L	1,00
	pH	150.1	7.45	១ដ	0.01

Page 1

11-01-00 13:58 TO:EQUIVA SVS

NYLAB ID# 10516

FROM: 7183837970

P02

MOTIVA ENTERPRISES LLC
SHELL & TEXACO WORKING TOGETHER
25 PAIDGE AVENUE
BROOKLYN, NY 11222
1-718-383-4066 ext. 10
FAX 1-718-383-7970

E AX IRANSMITTAL SHEET

NAME: DAVE
FIRM/DEPARTMENT:
FAX NUMBER:
FROM: 11-1-00 Should.
TOTAL NUMBER OF PAGES INCLUDING TRANSMITTAL SHEET
DATE:
COMMENTS: SEE Attached Brooklyn
October results

DOCUMENT INFO

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DocID:

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Filename:

58603-2009-11-17-PER-01 (SPDES Permit

0006131 Expires 1-31-15).pdf

New York State Department of Environmental Conservation Division of Environmental Permits

Programs and Systems, 4th Floor

625 Broadway, Albany, NY 12233-1750

Phone: (518) 402 -9167 • Fax: (518) 402-9168

Website: www.dec.ny.gov

NOV 1 7 2009



James W. Lintz
Motiva Enterprises LLC
25 Paidoo Avenue

25 Paidge Avenue Brooklyn, NY 11222-1281 **FACILITY INFORMATION**

NAME: Motiva Marketing Terminal

LOCATION: New York (C)

COUNTY: Kings

SPDES NO: NY 000 6131

DEC ID NO.: 2-6101-00105/00019

Dear SPDES Permittee:

Enclosed please find a validated NOTICE/RENEWAL APPLICATION/PERMIT form renewing your State Pollutant Discharge Elimination System (SPDES) permit for the referenced facility. This validated form, together with the previously issued permit (see issuance date of this permit in Part 3 of the NOTICE/RENEWAL APPLICATION/PERMIT form), and any subsequent permit modifications constitute authorization to discharge wastewater in accordance with all terms, conditions and limitations specified therein.

The instructions and other information that you received with the NOTICE/RENEWAL APPLICATION/PERMIT package fully described procedures for renewal and modification of your SPDES permit under the Environmental Benefit Permit Strategy (EBPS). As a reminder, SPDES permits are renewed at a central location in Albany in order to make the process more efficient. All other concerns with your permit such as applications for permit modifications, permit transfers to a new owner, name changes, and other questions should be directed to the Regional Permit Administrator at the following address:

John Cryan NYS DEC Region 2 47-40 21st Street 1 Hunters Point Plaza Long Island City, NY 11101-5407 (718) 482-4997

If you have already filed an application for modification of your permit, it will be processed separately through our regional office. If you have questions concerning this permit renewal, please contact Lindy Sue Czubernat at (518) 402-9165.

Sincerely,

Chief Permit Administrator

Enclosure

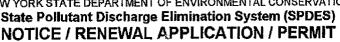
cc:

RPA

RWE

BWP

NEW YORK STATE DEPARTMENT OF ENVIRONMENTAL CONSERVATION State Pollutant Discharge Elimination System (SPDES)





Please read ALL instructions on the back before completing this application form. Please TYPE or PRINT clearly in ink.

PART 1 - NOTICE

Permittee Contact Name, Title, Address

Facility and SPDES Permit Information

MOTIVA ENTERPRISES LLC

MARIO D'ANTONIO. JAMES W. LINTZ

25 PAIDGE AVE

BROOKLYN

NY 11122-1281

MOTIVA MARKETING TERMINAL Name:

Ind. Code: 5171 County: KINGS

2-6101-00105/00019 DEC No.:

SPDES No.: NY 000 6131 02/01/2010 **Expiration Date:** Application Due By: 08/05/2009

Are these name(s) & address(es) correct? if not, please write corrections above.

The State Pollutant Discharge Elimination System Permit for the facility referenced above expires on the date indicated. You are required by law to file a complete renewal application at least 180 days prior to expiration of your current permit. Note the "Application Due By" date above.

CAUTION: This short application form and attached questionnaire are the only forms acceptable for permit renewal. Sign Part 2 below and mail only this form and the completed questionnaire using the enclosed envelope. Effective April 1, 1994 the Department no longer assesses SPDES application fees.

If there are changes to your discharge, or to operations affecting the discharge, then in addition to this renewal application, you must also submit a separate permit modification application to the Regional Permit Administrator for the DEC region in which the facility is located, as required by your current permit. See the reverse side of this page for instructions on filing a modification request.

PART 2 - RENEV	VAL APPLICATION
	mation provided on this form and all attachments submitted berewith is true to shable as a Class A misdemeanor pursuant to section 210.45 of the Penal Law.
JAMES W. LINTZ	TERMINAL COMPLEX MANAGER
Name of person signing application (see instructions on back)	Title 2
Janes White	7/20/09
Signature	Date
PART 3 - PERMIT (Below	this line - Official Use Only)
Effective Date: 2/1/10 Expiration Date: 1/31/13 William R. Adriance	NYSDEC - Division of Environmental Permits Address: Bureau of Environmental Analysis
Permit Administrator	625 Broadway, Albany, NY 12233-1750
William K. Adriance N	IOV 1 7 2009
Signature	Date
constitute authorization to discharge wastewater in accorda previously issued valid permit, modifications thereof or issued a	his facility issued $\frac{2}{L}/\frac{0.5}{0.5}$ and subsequent modifications ince with all terms, conditions and limitations specified in the spart of this permit, including any special or general conditions valve the Department's authority to initiate a modification of this

permit on the grounds specified in 6NYCRR §621.14, 6NYCRR §754.4 or 6NYCRR §757.1 existing at the time this permit is issued or which arise thereafter.

General Conditions dated



Please enter the numbers from your current permit:

DEC Number 2 - 10101 - 00105 00012

SPDES Number: NY

000 6131

SPDES RENEWAL APPLICATION QUESTIONNAIRE

THIS PAGE MUST BE COMPLETED AND RETURNED WITH YOUR COMPLETED APPLICATION Please TYPE or PRINT neatly using adequate pressure to make ALL copies legible. Keep a copy for your records. M NO YES . 1. Has the SPDES permit for your facility been modified in the past 5 years 2. Dischargers who use, manufacture, store, handle or discharge toxic or hazardous pollutants are subject to industrial Best Management Practices (BMP) plan requirements for toxic or hazardous substances. A BMP plan prevents or minimizes the potential for release of pollutants to receiving waters from such ancillary industrial activities, including material storage areas; plant site runoff; in-plant transfer; process and material storage areas; loading and unloading operations, and sludge and waste disposal areas. Does your facility conduct anciliary activities as described above, which are not covered by BMP requirements in your current permit? ☐ YES M NO Please indicate which of the following best describes the situation at your facility. None of the concerns on the "Self Evaluation List" seem to apply to my facility at this time and I will not be applying for a modification of the SPDES permit in the foreseeable future. Yes, some of the items on the "Self Evaluation List" have led me to believe that the permit for this facility needs to be modified. I already have a complete modification application pending with the Department. Yes, some of the items on the "Self Evaluation List" have led me to believe that the SPDES permit for this facility may need to be Modified. I have requested the appropriate forms by phone OR I have completed and attached the "Request For SPDES Application Forms" (included in this renewal package) to allow me to submit a permittee-initiated Modification application. See The "Request For SPDES Application Forms" page for a toll free 800 number. X The items on the "Self Evaluation List" have left me unable to conclude whether my permit needs to be modified at this time. I am reporting the following general concerns about my permit: ATTACHED DESCRIPTION <u>Changes</u>

DISTRIBUTION:

Regional Water Engineer Regional Permit Administrator Central Office (BWP) · 20-2 (1/89)

NEW YORK STATE DEPARTMENT OF ENVIRONMENTAL CONSERVATION State Pollutant Discharge Elimination System (SPDES) DISCHARGE PERMIT





	·
Industrial Code: 5171	SPDES Number: NY - 0006131
Discharge Class (CL): 01	DEC Number: 2-6101-00105/00019
Toxic Class (TX): T	Effective Date (EDP): 02/01/00
Major Drainage Basin: 17	Expiration Date (ExDP): 02 / 01 / 05
Sub Drainage Basin: 02	Modification Date(s):
Water Index Number: LIS-4	Attachment(s): General Conditions (Part II)Date:11/90
Compact Area: ISC	
York State and in compliance with the Clean Water Act as "the Act"). PERMITTEE NAME AND ADDRESS	h Title 8 of Article 17 of the Environmental Conservation Law of New as amended, (33 U.S.C. Section 1251 et. seq.) (hereafter referred to Attention: R.S Bailey, Regional Mgr. NE
Name: Motiva Enterprises LLC	
Street: Two Shell Plaza, P.O. Bo	ox 2099
City: Houston	State: TX Zip Code: 77252-2099
is authorized to discharge from the facility described be	₩.:
FACILITY NAME AND ADDRESS	
Name: Motiva Marketing T	Perminal
Location (C,T,V): New York (C)	County: Kings
Facility Address: 25 Paidge Ave.	
City: Brooklyn	State: NY Zip Code: 11222-1281
NYTM - E: 588.5	NYTM - N: 4 510 .
From Outfall No.: 001 at Latitude	
into receiving waters known as: Newtown	
and; (list other Outfalls, Receiving Waters & Water Class	
01A Newtown Creek (Via (001) SD
•	
in accordance with the effluent limitations, monitoring re (Part I) and General Conditions (Part II) of this permit.	equirements and other conditions set forth in Special Conditions
DISCHARGE MONITORING REPORT (DMR) MAILING	G ADDRESS
NATIONAL SECTION AND ASSESSMENT OF THE SECTION ASSESSMENT OF THE SECTI	
Malling Name: Motiva Enterprises	3 LLC
Street: 25 Paidge Avenue City: Brooklyn	Otto: 1777 - 77- Out - 11000 1001
Responsible Official or Agent:	State: NY Zip Code: 11222-1281
Trouponoisie Children of Agents.	Phone: (718)383-4066
permittee shall not discharge after the expiration date u	e shall expire on midnight of the expiration date shown and the nless this permit has been renewed, or extended pursuant to law. Ite, the permittee shall apply for a permit renewal no less than 180
	Permit Administrator:
T. Burns, Div. Of Water	John F. Cryan
Hon. R. Giuliani, Mayor of NYC	Address: 47-40 21st St., 2nd Floor
NYC DOH & DEP	Long Island City, NY 11101 (718) 482-4997
Interstate Sanitation Commission	Signature Date: 12/17/99
U.S. EPA, Reg. II & Edison, NJ	John J. Lymn
NYS DEC Div. of Water, BMCP & BMP	

91-20-2a (1/89)

SPDES No.: NY 000 6131

Part 1, Page __ 2 of __ 9

FINAL EFFLUENT LIMITATIONS AND MONITORING REQUIREMENTS	·
During the period beginning EDP	
and lasting until EDP + 5 yrs.	
and the state of t	of balance

the discharges from the permitted facility shall be limited and monitored by the permittee as specified below:

				Monito	Minimum ring Requirements
Outfall Number &	Discha	rge Limitations		/leasurement	Sample
Effluent Parameter	Daily Avg.	Daily Max.	Units Fred	Uency	Type
001 - Storm Water Runoff					
Flow	NA	Monitor	GPD	Monthly	Instantaneous
Oil & Grease	NA NA	15	mg/l	Monthly	Grab
pH (range)	(6.0 - 9.0)		\$U's	Monthly	Grab
MTBE	NA	Monitor	mg/l	Monthly	Grab
01A - Hydrostatic Test Water					
Flow	NA	Monitor	GPD	Each Discha	arge ² Instantaneous
Oil & Grease	NA	15	mg/l	Each Discha	arge Grab(s)
pH (range)	(6.0 - 9.0)		SÚ's	Each Discha	arge ² Grab(s)
Benzene	NA	0.020	mg/l	Each Discha	
Toluene	NA	0.020	mg/l	Each Discha	arge ² Grab(s)
Xylenes (Total)	NA	0.020	mg/l	Each Discha	arge ² Grab(s)
Ethylbenzene	NA	0.020	mg/l	Each Discha	arge ² Grab(s)
Chlorine, Total Residuals	NA	0.10	mg/l	Each Discha	arge ² Grab(s)
MTBE	NA	Monitor	mg/l	Each Discha	arge ² Grab(s)

- 1. Tanks being hydrostatically tested must be free of product and cleaned. The Regional Water Engineer must be informed at least two business days prior to the discharge of tank test water.
- 2. Any discharge of tank test water must be done under the direct supervision of plant personnel. Samples from the tank must be taken prior to discharge from various levels within the tank (Top, middle and bottom). If sampling shows conformance with effluent limitations, discharge may be initiated. If effluent limitations are not attained, additional measures must be implemented to attain compliance prior to initiation of discharge.

A visual check of the discharge must be made for the presence of oil and floating substances. Data associated with tank test water shall be kept, along with the log of visual observations, for a period of three years and be made available to department personnel upon request.

The discharge of tank test water must be done in a manner that minimizes erosion of soil or sediment and does not cause flooding in the area of discharge. It must be done in a manner that minimizes the impact on the fisheries.

3	Only required when	chiarinated water is used	in tank teeting

91-20-2g (1/96)

SPDES No.: NY 000 6131

Part 1, Page 3 of 9

ACTION LEVEL REQUIREMENTS (TYPE!)

The parameters listed below have been reported present in the discharge but at levels that currently do not require technology or water quality based limits. Action levels have been established which, if routinely or excessively exceeded, will result in reconsideration and/or development of technology or water quality based limits.

Routine action level monitoring results, if not provided for on the Discharge Monitoring Report (DMR) form, shall be appended to the DMR for the period during which the sampling was conducted. If submission of DMR's is not required by this permit, the results shall be maintained in accordance with instructions on the RECORDING, REPORTING AND MONITORING page of this permit.

If any of the action levels is exceeded, the permittee shall undertake a short-term, high-intensity monitoring program for the parameter(s). Samples identical to those required for routine monitoring purposes shall be taken on each of at least three consecutive operating and discharge days and analyzed. Results shall be expressed in terms of both concentration and mass, and shall be submitted no later than the end of the second month following the month when the action level was first exceeded. Results may be appended to the DMR or transmitted under separate cover to the addresses listed on the RECORDING, REPORTING AND MONITORING page of this permit. If levels higher than the actions levels are confirmed the results shall constitute an application for permit modification and the permit may be reopened for consideration of revised action levels or effluent limits.

The permittee is not authorized to discharge any of listed parameters at levels which may cause or contribute to a violation of water quality standards.

Outfall Number & Effluent Parameter	Action Level	Units	Minimum Monitorin Measurement Frequency	g Requirements Sample Type
001 Storm Water Runoff				
Benzene	0.10	mg/l	Quarterly	Grab
Toluene	0.10	mg/l	Quarterly	Grab
Xylenes (Total)	0.10	mg/l	Quarterly	Grab
Ethylbenzene	0.10	mg/t	Quarterly	Grab

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Prohibitions:

Consistent with Department policy dilution is prohibited as a substitute for treatment. Except where expressly authorized to do so by an applicable Categorical Standard or the Commissioner or his duly authorized representative, no Industrial User shall ever increase the use of process water or, in any other way, attempt to dilute a discharge as a partial or complete substitute for adequate treatment to achieve compliance with a permit effluent limitation requirement.

No discharge of tank water bottoms and/or any industrial or manufacturing process wastewater effluents are permitted. Included in the effluents categorized as industrial process effluents are wastewaters resulting from vehicle maintenance or washing operations. Washing operations are those cleaning operations which involve the use of detergents or other emulsifying chemicals.

Tank water bottoms, vehicle maintenance and washing wastewaters are not likely to be effectively treated by gravity separation alone and therefore are not permitted to be discharged. After review of an Engineering Submission for the treatment of tank bottoms and/or maintenance and/or washing wastewaters these prohibitions may be altered.

Waste or wastewater generated at locations other than at this facility are not permitted to be treated at of discharged from this facility.

NOTES:

This SPDES permit is not to be construed as altering obligations of the permittee under 6NYCRR Part 613, i.e. 613.3(c)6(iii) Storm water which collects within the secondary containment system must be controlled by a manually operated pump or siphon, or gravity drain pipe which has two manually controlled dike valves operable from the outside of the dike. All pumps, siphons and valves must be properly maintained and kept is good condition. if gravity drain pipes are used, all dike valves must be locked in a closed position except when the operator is in the process of draining ... water from the diked area. The only exceptions shall be those expressly authorized by the Commissioner or his duly authorized representative.

A visual check for oil or floating substances must be made and logged prior to the initiation of any discharge from an impoundment or a discharge controlled by a normally closed valve. The log of visual observations shall be maintained at the facility for a period of at least three years and must be made available to the Department upon request.

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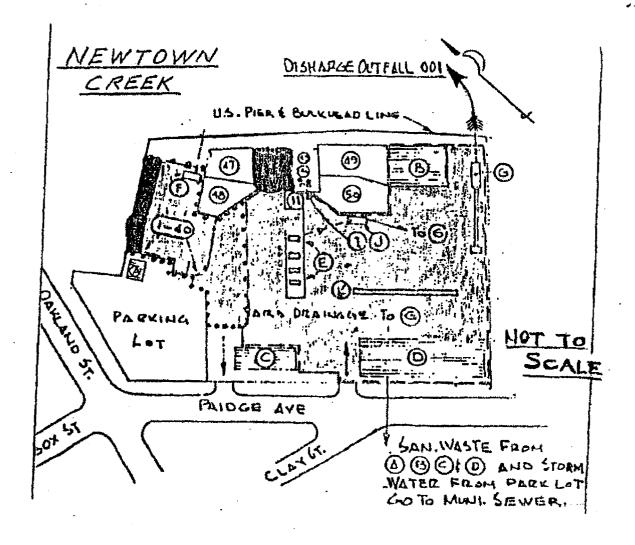
DEFINITIONS OF DAILY AVERAGE AND DAILY MAXIMUM

The daily average discharge is the total discharge by weight or in other appropriate units as specified herein, during a calendar month divided by the number of days in the month that the production or commercial facility was operating. Where less than daily sampling is required by this permit, the daily average discharge shall be determined by the summation of all the measured daily discharges in appropriate units as specified herein divided by the number of days during the calendar month when measurements were made.

The daily maximum discharge means the total discharge by weight or in other appropriate units as specified herein, during any calendar day.

MONITORING LOCATIONS

The permittee shall take samples and measurements, to comply with the monitoring requirements specified in this permit, at the location(s) indicated below: (Show sampling locations and outfalls with sketch or flow diagram as appropriate) for 001 from treatment system effluent flow prior to discharge to Newtown Creek. Sampling of hydrostatic test water (01A) shall be from the tank, pipe, etc...contents prior to discharge via 001.



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SPECIAL CONDITIONS - BEST MANAGEMENT PRACTICES

- 1. The permittee shall develop and implement a Best Management Practices (BMP) plan, to prevent, or minimize the potential for, release of significant amounts of toxic or hazardous pollutants to the waters of the State through plant site runoff; spillage and leaks; sludge or waste disposal; and storm water discharges including, but not limited to, drainage from raw material storage. Completed BMP plans shall be submitted to the Regional Water Engineer within six months of EDP.
- 2. The permittee shall review all facility components or systems (including material storage areas; in-plant transfer, process and material handling areas; loading and unloading operations; storm water, erosion, and sediment control measures; process emergency control systems; and sludge and waste disposal areas) where toxic or hazardous pollutants are used, manufactured, stored or handled to evaluate the potential for the release of significant amounts of such pollutants to the waters of the State. In performing such an evaluation, the permittee shall consider such factors as the probability of equipment fallure or improper operation, cross-contamination of storm water by process materials, settlement of facility air emissions, the effects of natural phenomena such as freezing temperatures and precipitation, fires, and the facility's history of spills and leaks. For hazardous pollutants, the list of reportable quantities as defined in 40 CFR, Part 117 may be used as a guide in determining significant amounts of releases. For toxic pollutants, the relative toxicity of the pollutant shall be considered in determining the significance of potential releases.

The review shall address all substances present at the facility that are listed as toxic pollutants under Section 307(a)(1) of the Clean Water Act or as hazardous pollutants under Section 311 of the Act or that are identified as Chemicals of Concern by the Industrial Chemical Survey.

- 3. Whenever the potential for a significant release of toxic or hazardous pollutants to State waters is determined to be present, the permittee shall identify Best Management Practices that have been established to minimize such potential releases. Where BMPs are inadequate or absent, appropriate BMPs shall be established. In selecting appropriate BMPs, the permittee shall consider typical industry practices such as spill reporting procedures, risk identification and assessment, employee training, inspections and records, preventive maintenance, good housekeeping, materials compatibility and security. In addition, the permittee may consider structural measures (such as secondary containment and erosion/sediment control devices and practices) where appropriate.
- 4. Development of the BMP plan shall include sampling of waste stream segments for the purpose of toxic "hot spot" identification. The economic achievability of technology-based end-of-pipe treatment will not be considered until plant site "hot spot" sources have been identified, contained, removed or minimized through the imposition of site specific BMPs or application of internal facility treatment technology.
- 5. The BMP plan shall be documented in narrative form and shall include any necessary plot plans, drawings or maps. Other documents already prepared for the facility such as a Safety Manual or a Spill Prevention, Control and Countermeasure (SPCC) plan may be used as part of the plan and may be incorporated by reference. USEPA guidance for development of stormwater elements of the BMP is available in the September 1992 manual "Storm Water Management for Industrial Activities," USEPA Office of Water Publication EPA 832-R-92-006 (available from NTIS, (703)487-4650, order number PB 92235969). A copy of the BMP plan shall be maintained at the facility and shall be available to authorized Department representatives upon request. As a minimum, the plan shall include the following BMP's:

a. BMP Committee b. Reporting of BMP Incidents c. Risk Identification & Assessment d. Employee Training	e. f. g. h.	Inspections and Records Preventive Maintenance Good Housekeeping Materials Compatibility	i. - - -	Security Spill prevention & response Erosion & sediment control Management of runoff
a. Employee raining	n.	Materials Compatibility	i.	Management of runoff

- The BMP plan shall be modified whenever changes at the facility materially increase the potential for significant releases
 of toxic or hazardous pollutants or where actual releases indicate the plan is inadequate.
 - A "not apot" is a segment of an industrial facility; including but not limited to soil, equipment, material storage areas, sewer lines etc.; which contributes elevated levels of problem pollutants to the wastewater and/or storm water collection system of that facility. For the purposes of this definition, problem pollutants are substances for which end of pipe treatment to meet a water quality or technology requirement may, considering the results of wastestream segment sampling, be deemed unreasonable. For the purposes of this definition, an elevated level is a concentration or mass loading of the pollutant in question which is sufficiently higher than the end of pipe concentration of that same pollutant so as to allow for an economically justifiable removal and/or isolation of the segment and/or B.A.T. treatment of wastewaters emanating from the segment.

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- (e) All requirements of the Discharge Notification Act, including public repository requirements, are waived for any outfall meeting any of the following circumstances, provided Department notification is made in accordance with (f):
 - (i) such sign would be inconsistent with any other state or federal statute;
 - such sign could only be located in an area that is damaged by ice or flooding due to a one-year storm or storms of less severity;
 - (iii) Instances in which the outfall to the receiving water is located on private or government property which is restricted to the public through fencing, patrolling, or other control mechanisms. Property which is posted only, without additional control mechanisms, does not qualify for this provision;
 - (iv) instances where the outfall pipe or channel discharges to another outfall pipe or channel, before discharge to a receiving water; or
 - (v) instances in which the discharge from the outfall is located in the receiving water, two-hundred or more feet from the shoreline of the receiving water.
- (f) If the permittee believes that any outfall which discharges wastewater from the permitted facility meets any of the walver criteria listed in (e) above, notification (form enclosed) must be made to the Department's Bureau of Water Permits, Central Office, of such fact, and, provided there is no objection by the Department, a sign and DMR repository for the involved outfall(s) are not required. This notification must include the facility's name, address, telephone number, contact, permit number, outfall number(s), and reason why such outfall(s) is waived from the requirements of discharge notification. The Department may evaluate the applicability of a waiver at any time, and take appropriate measures to assure that the ECL and associated regulations are complied with,

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RECORDING, REPORTING AND ADDITIONAL MONITORING REQUIREMENTS

- The permittee shall also refer to the General Conditions (Part II) of this permit for additional information concerning a) monitoring and reporting requirements and conditions.
- The monitoring information required by this permit shall be summarized, signed and retained for a period of three years from the date of the sampling for subsequent inspection by the Department or its designated agent. Also;
 - [X] (If box is checked) monitoring information required by this permit shall be summarized and reported by submitting completed and signed Discharge Monitoring Report (DMR) forms for each ____ month report period to the locations specified below. Blank forms are available at the Department's Albany office listed below. The first reporting period begins on the effective date of this permit and the reports will be due no later than the 28th day of the month following the end of each reporting period.

Send the original (top sheet) of each DMR page to:

Department of Environmental Conservation Division of Water Bureau of Watershed Compliance Programs 50 Wolf Road Albany, New York 12233-3506

Phone: (518) 457-3790

Send the first copy (second sheet) of each DMR page to:

Department of Environmental Conservation Regional Water Engineer Region 2 1 Hunters Point Plaza 47-40 21st St. Long Island City, NY 11101-5407

- A monthly "Wastewater Facility Operation Report..." (form 92-15-7) shall be submitted (if box is checked) to the [] Regional Water Engineer and/or [] County Health Department or Environmental Control Agency listed above.
- Noncompliance with the provisions of this permit shall be reported to the Department as prescribed in the attached General Conditions (Part II).
- Monitoring must be conducted according to test procedures approved under 40 CFR Part 136, unless other test procedures have been specified in this permit.
- If the permittee monitors any pollutant more frequently than required by this permit, using test procedures approved under 40 CFR Part 136 or as specified in this permit, the results of this monitoring shall be included in the calculations and recording on the Discharge Monitoring Reports.
- Calculations for all limitations which require averaging of measurements shall utilize an arithmetic mean unless otherwise specified in this permit.
- h) Unless otherwise specified, all information recorded on the Discharge Monitoring Report shall be based upon measurements and sampling carried out during the most recently completed reporting period.
- Any laboratory test or sample analysis required by this permit for which the State Commissioner of Health issues certificates of approval pursuant to section five hundred two of the Public Health Law shall be conducted by a laboratory which has been issued a certificate of approval. Inquiries regarding laboratory certification should be sent to the Environmental Laboratory Accreditation Program, New York State Health Department Center for Laboratories and Research, Division of Environmental Sciences, The Nelson A. Rockefeller State Plaza, Albany, New York 12201.



Integrated Contingency Plan

ANNEX 1.... FACILITY AND LOCALITY INFORMATION [DIAGRAMS / MAPS]

This Section contains the drawings and diagrams for the Brooklyn Terminal that are listed below:

- Figure 1.1 Topographic Map
- Figure 1.2 Facility Site Diagram
- Figure 1.3 Evacuation Diagram
- Figure 1.4 Site Drainage Flow Diagram
- Figure 1.5 Environmental Sensitivity Mapping
- Figure 1.6 Dock Diagram

Figure 1.1 Topography Map

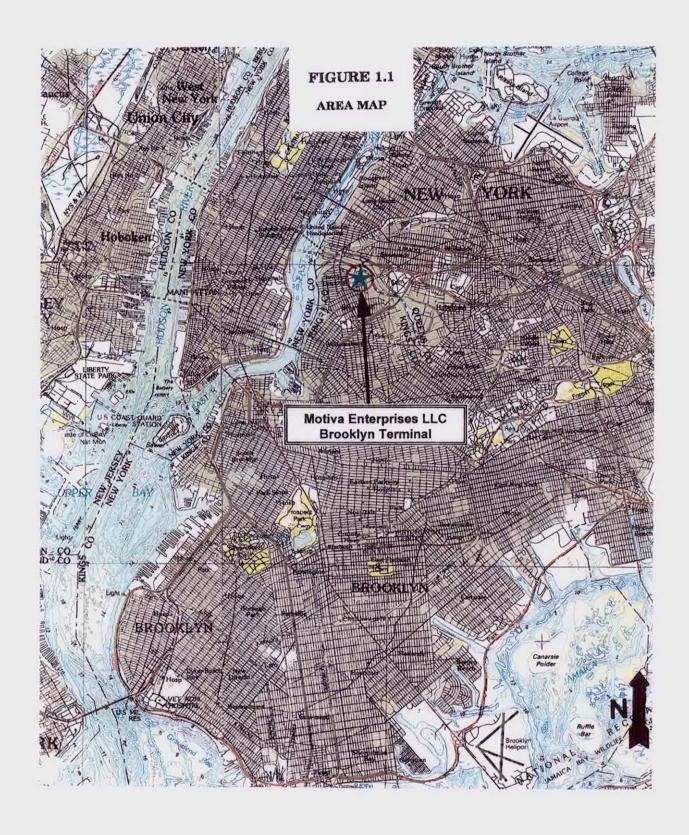
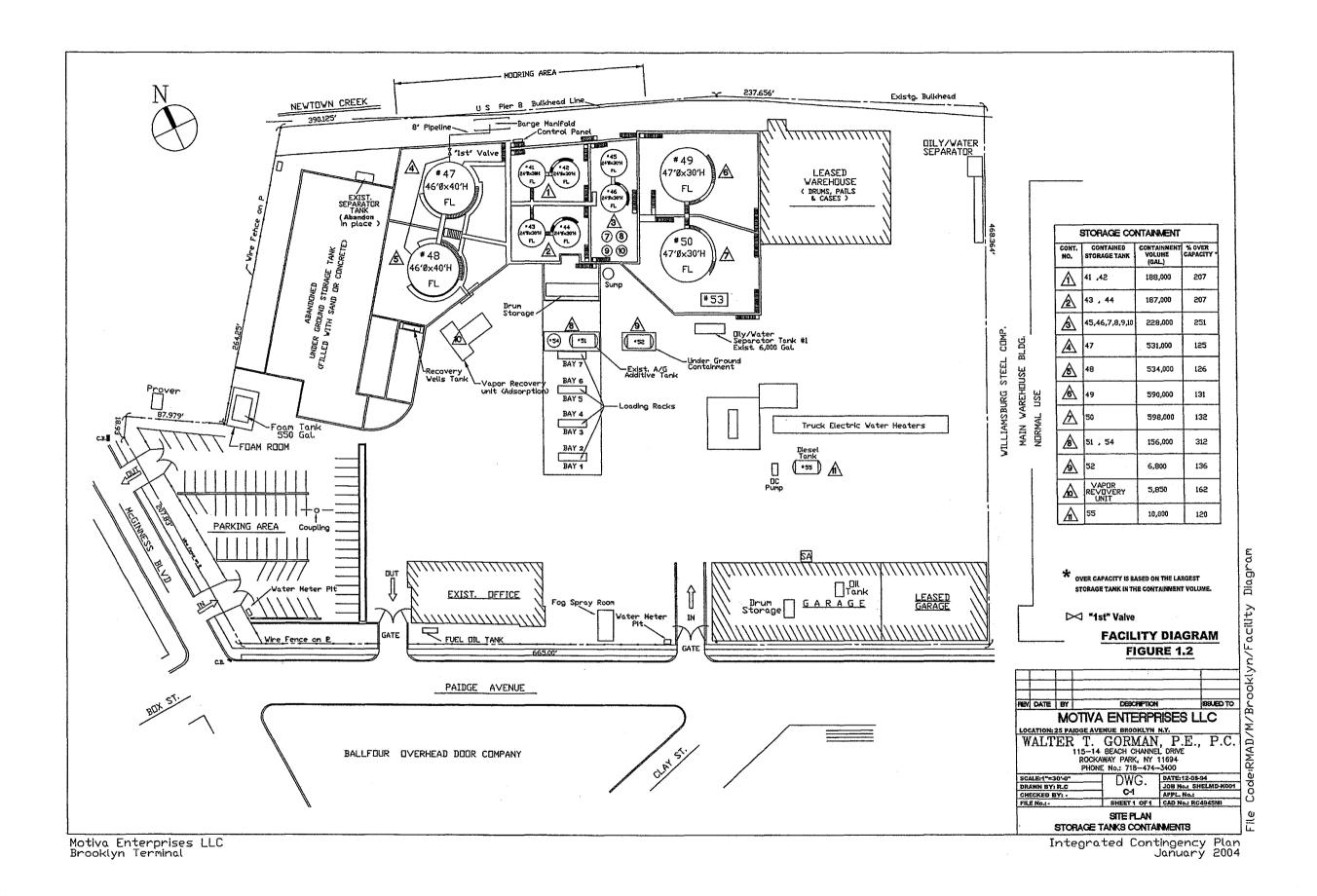


Figure 1.2 Facility Site Diagram



Shell/Motiva 0008547

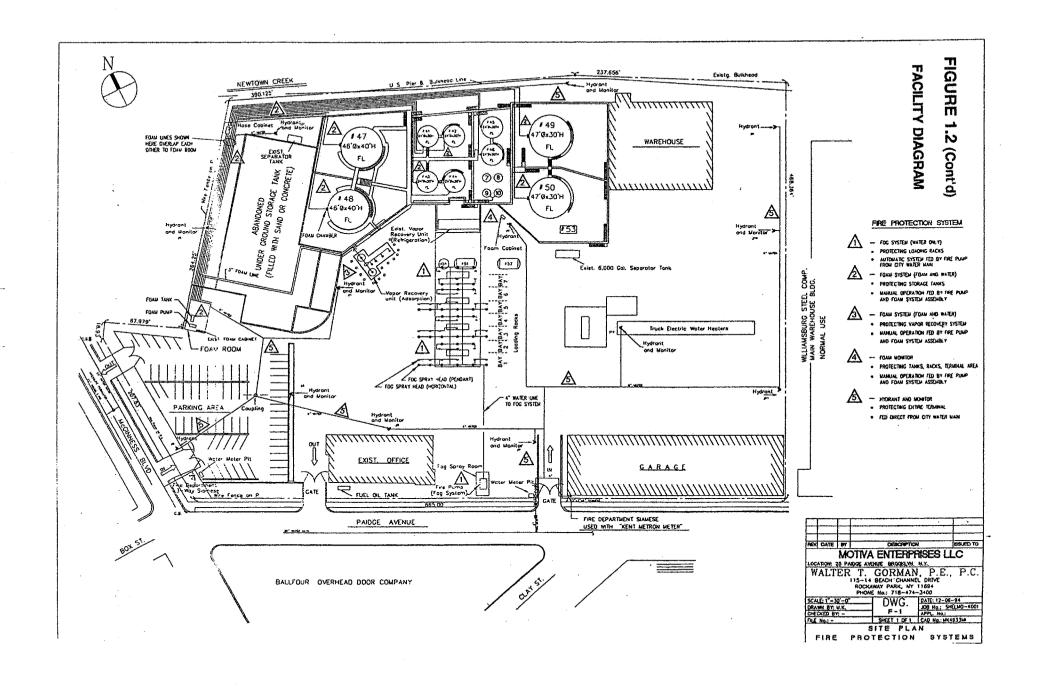


Figure 1.3 Evacuation Diagram

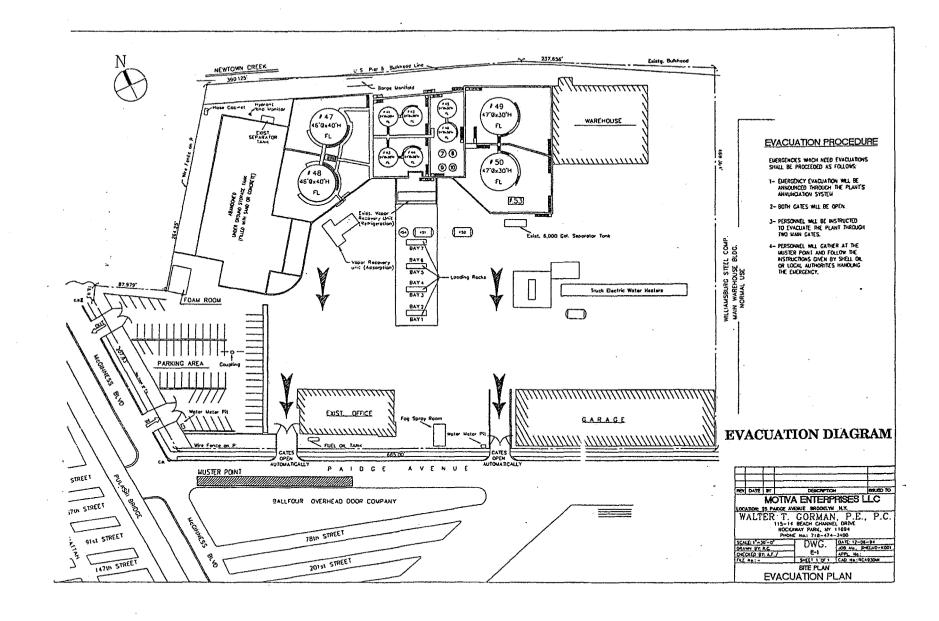
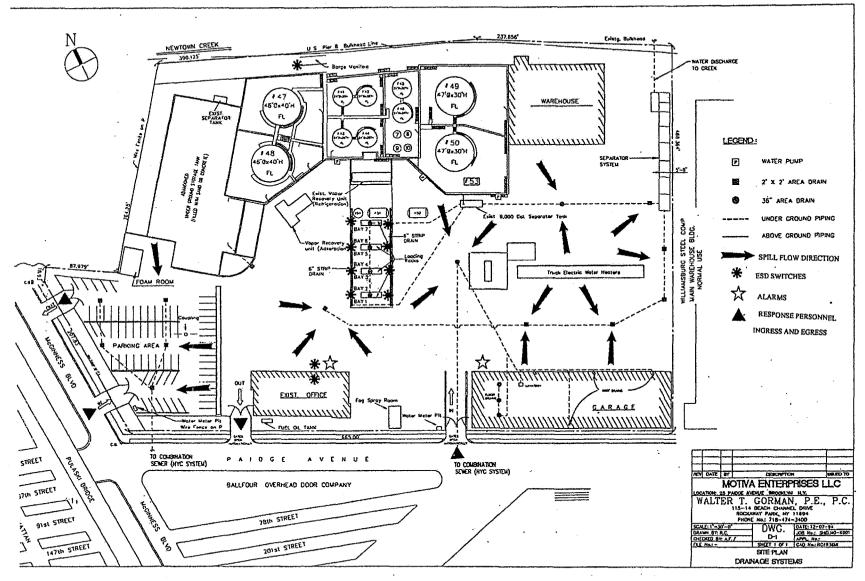


Figure 1.4 Site Drainage Flow Diagram



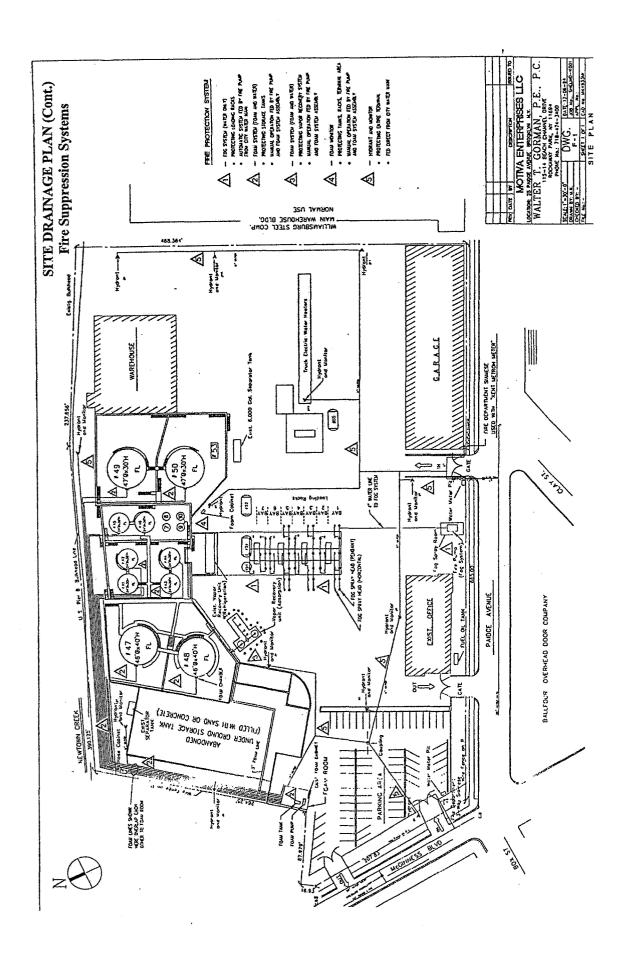
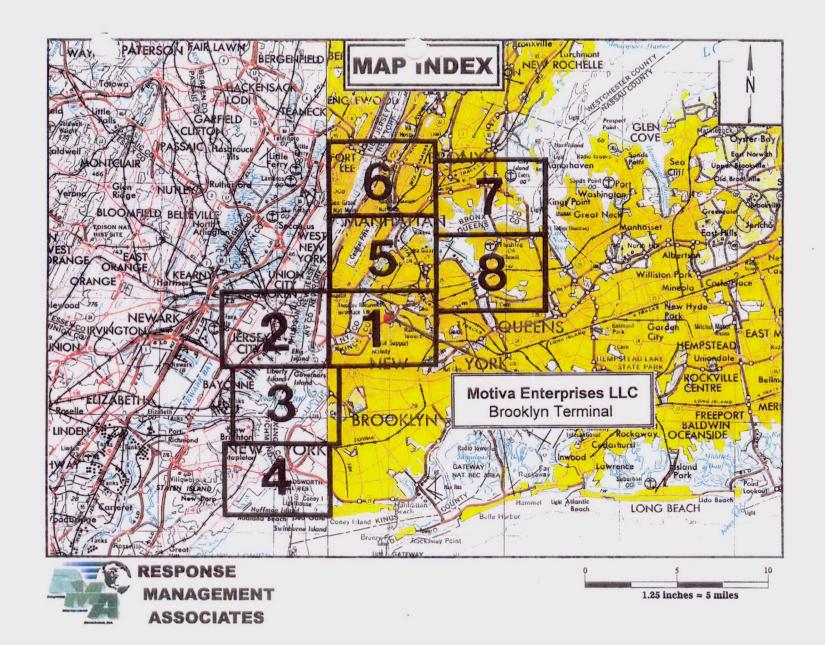
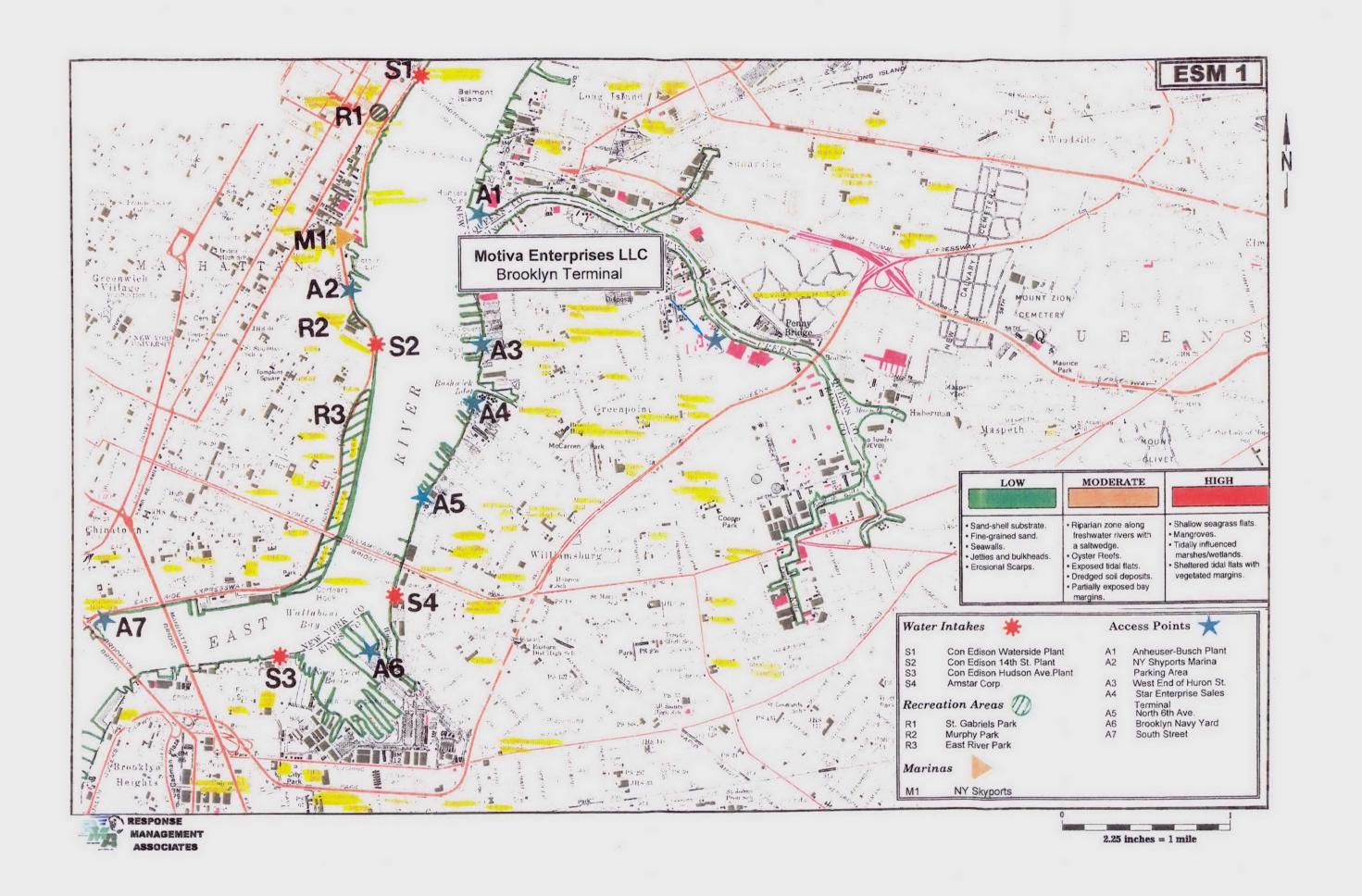
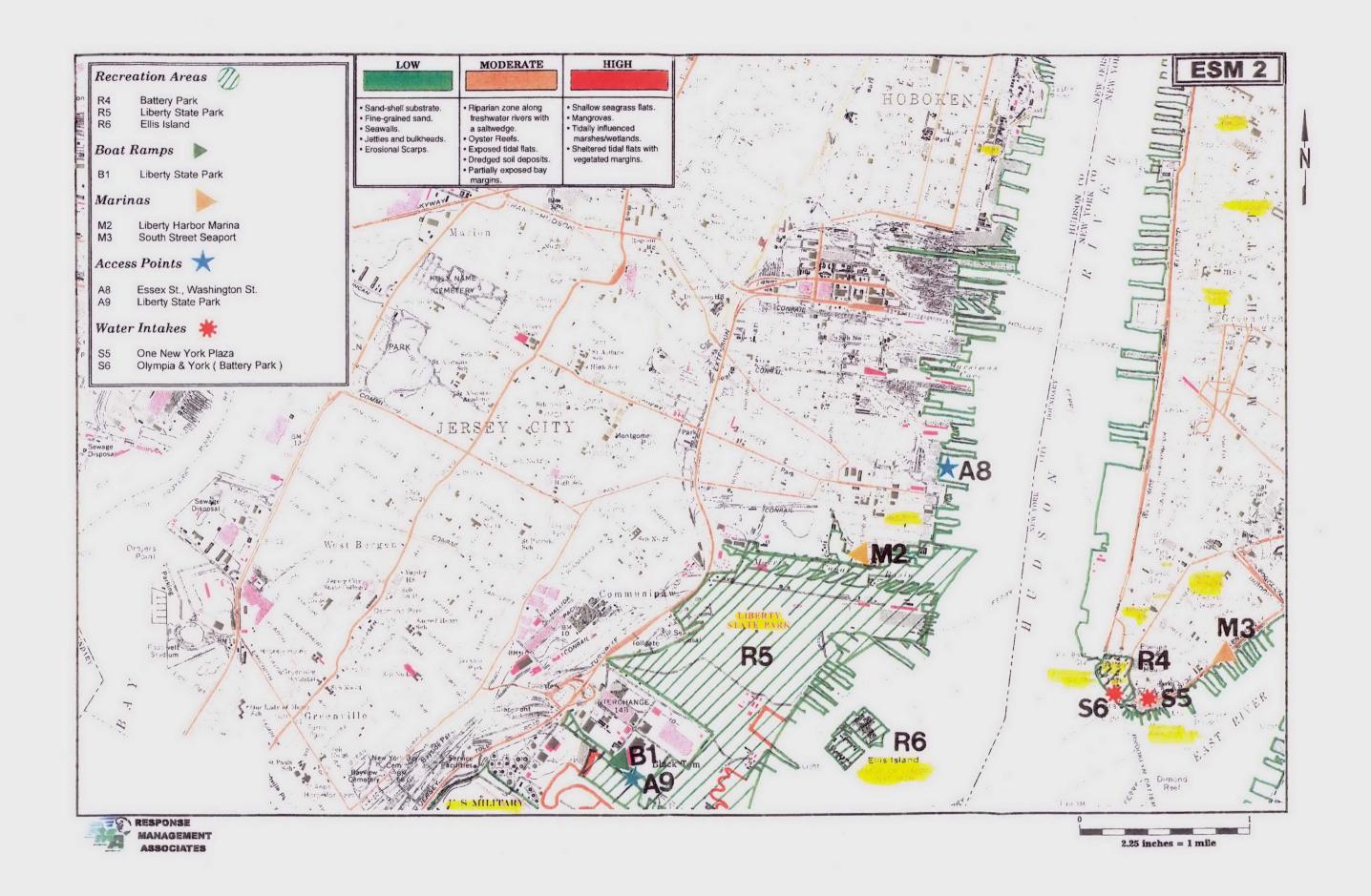
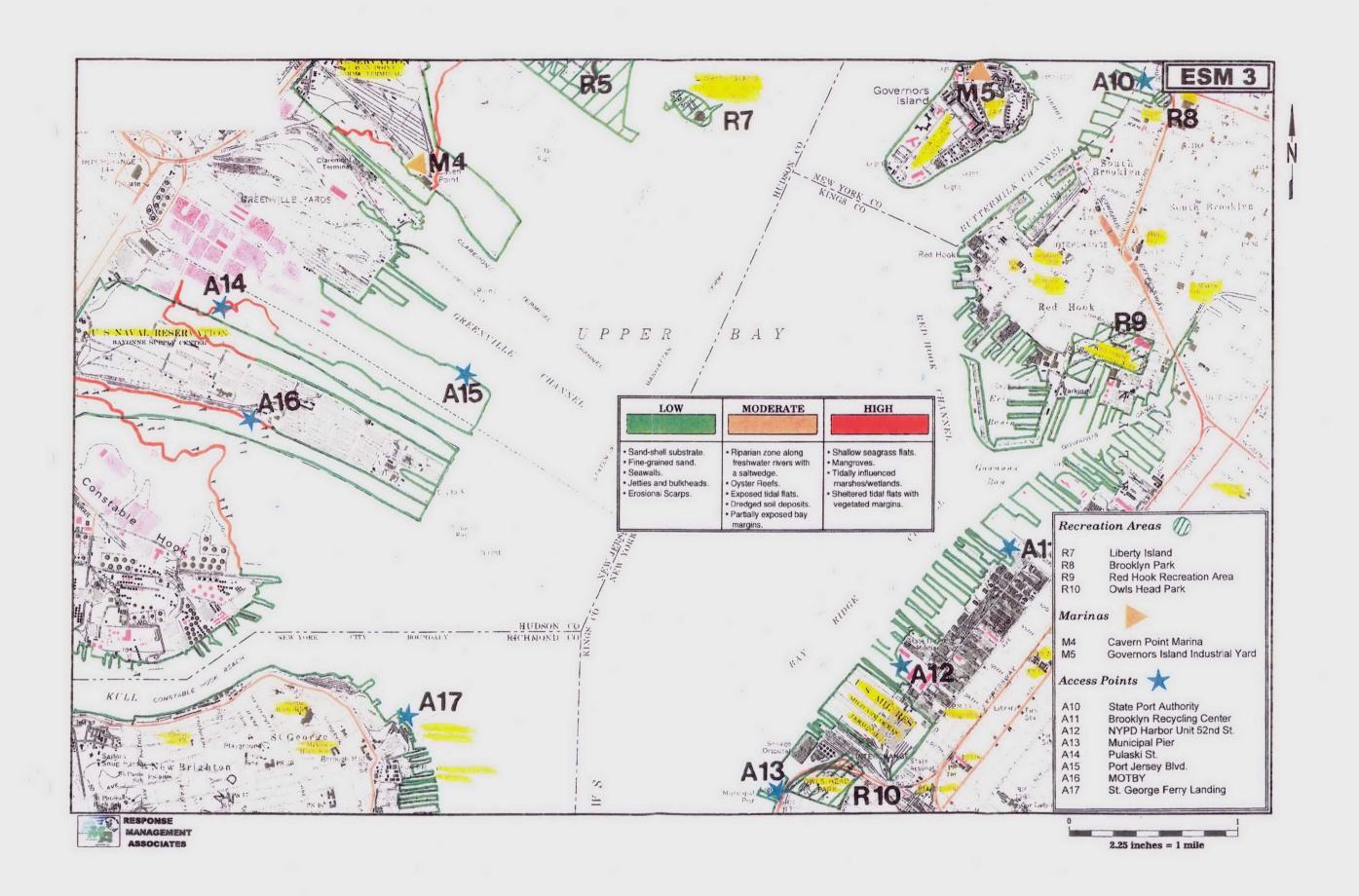


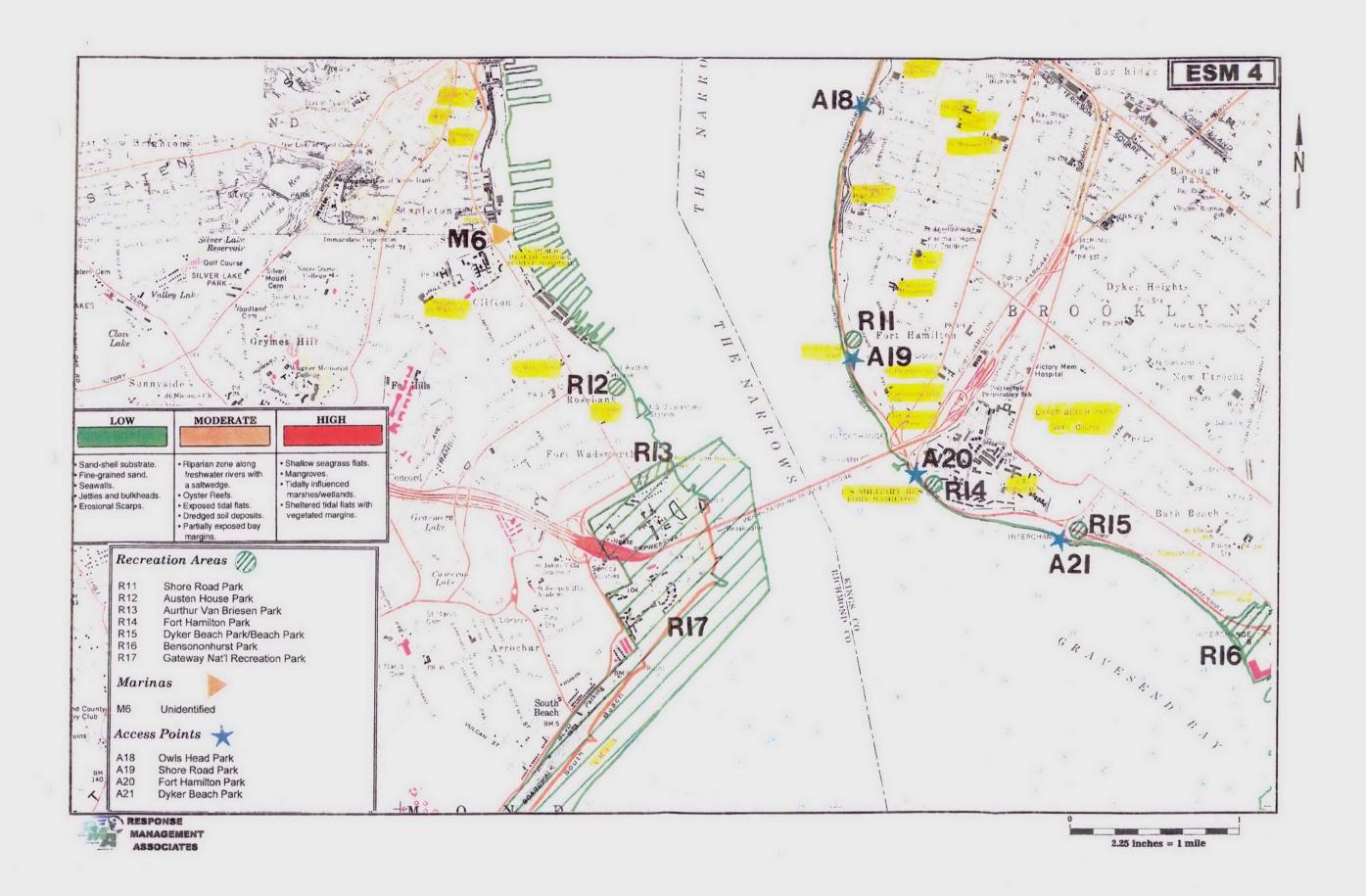
Figure 1.5 Environmental Sensitivity Mapping

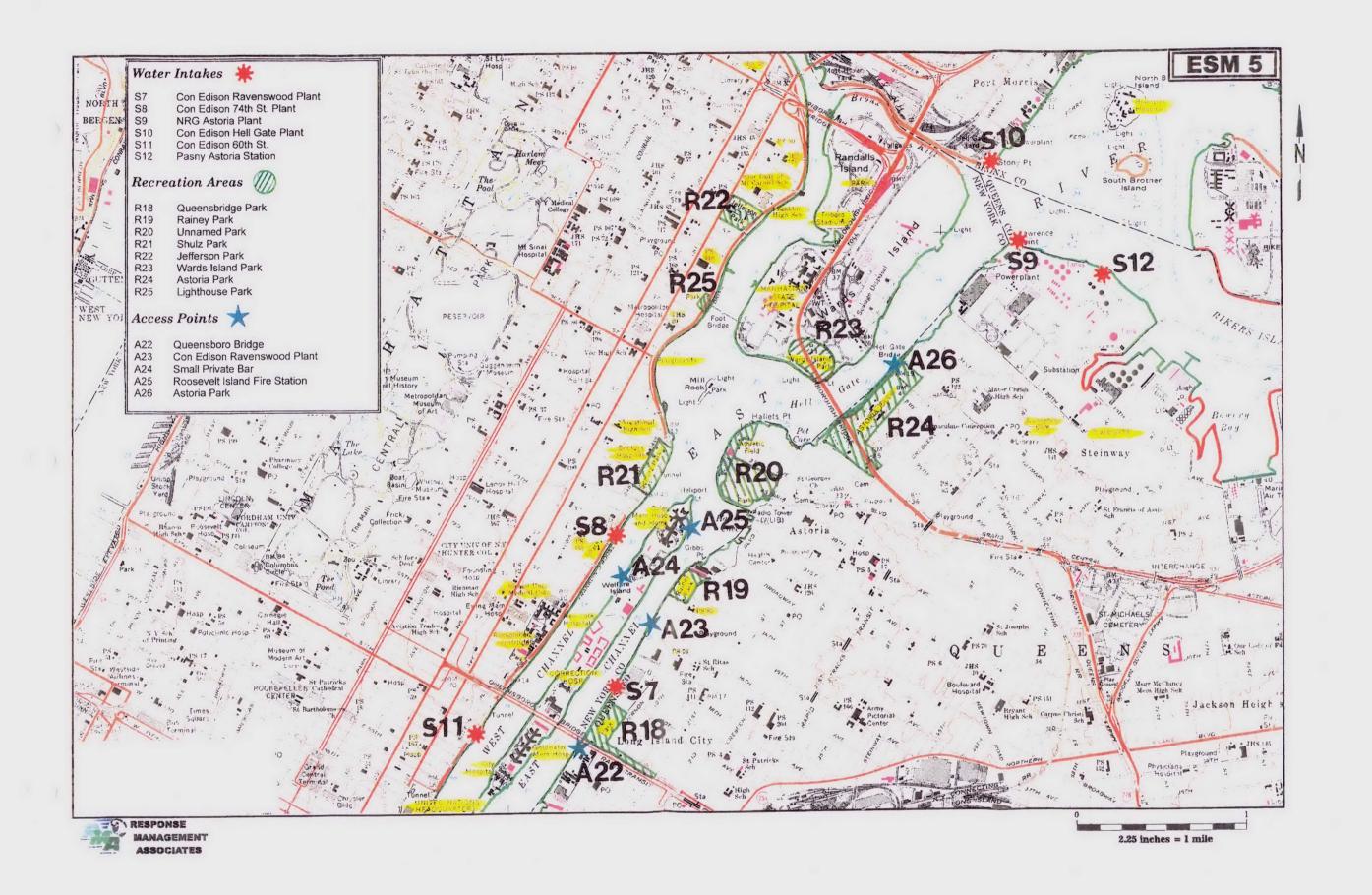


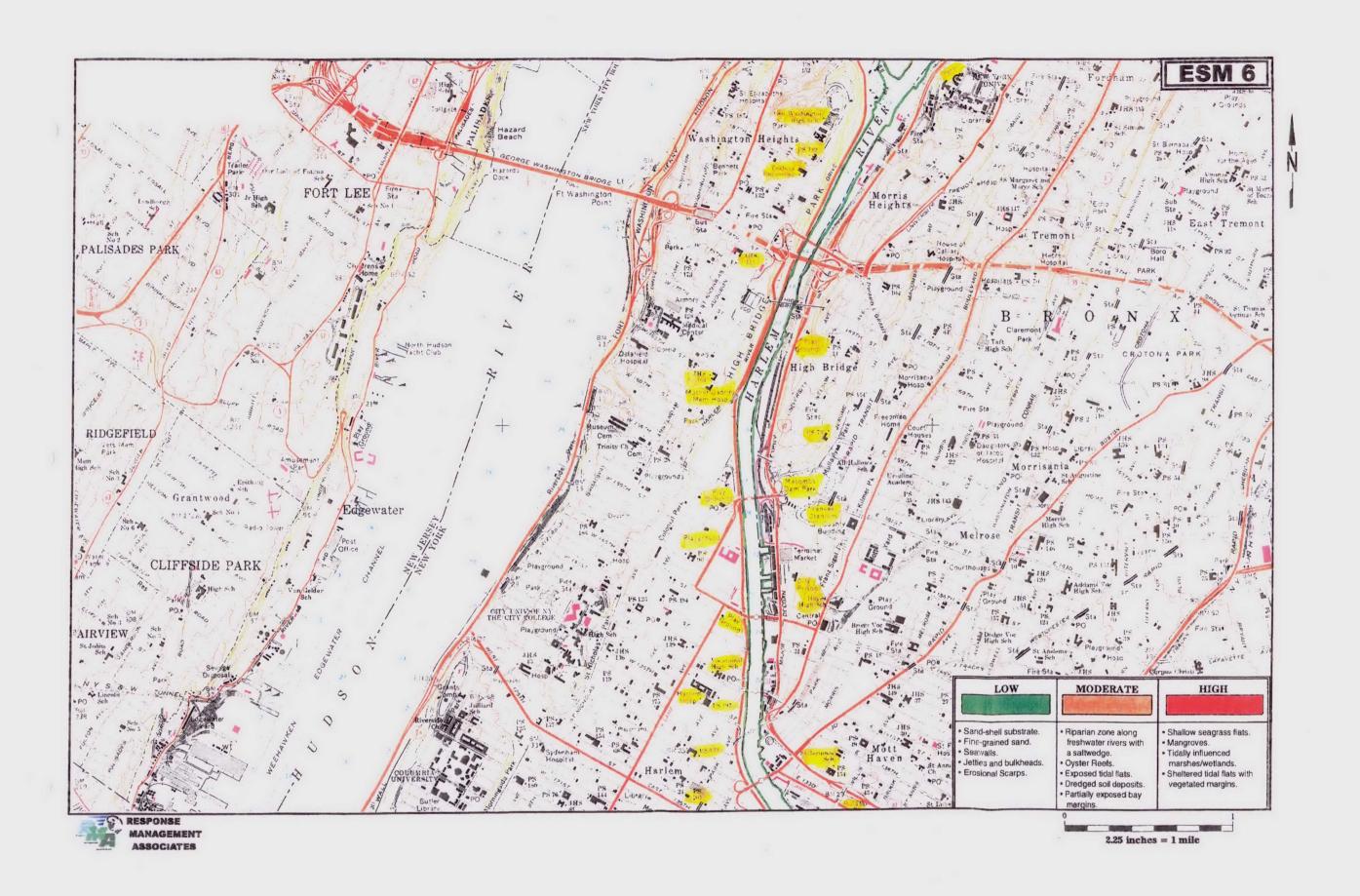


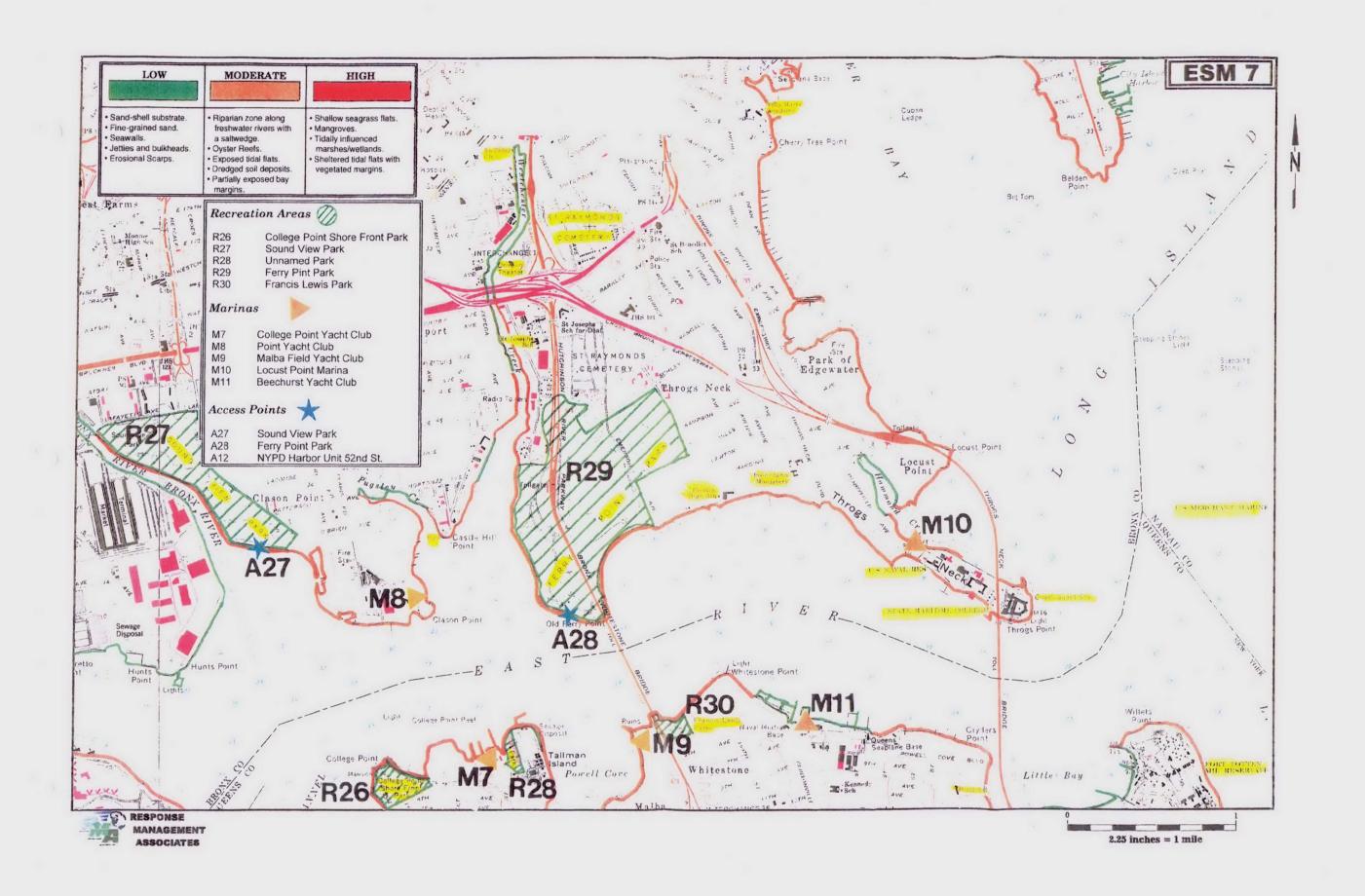












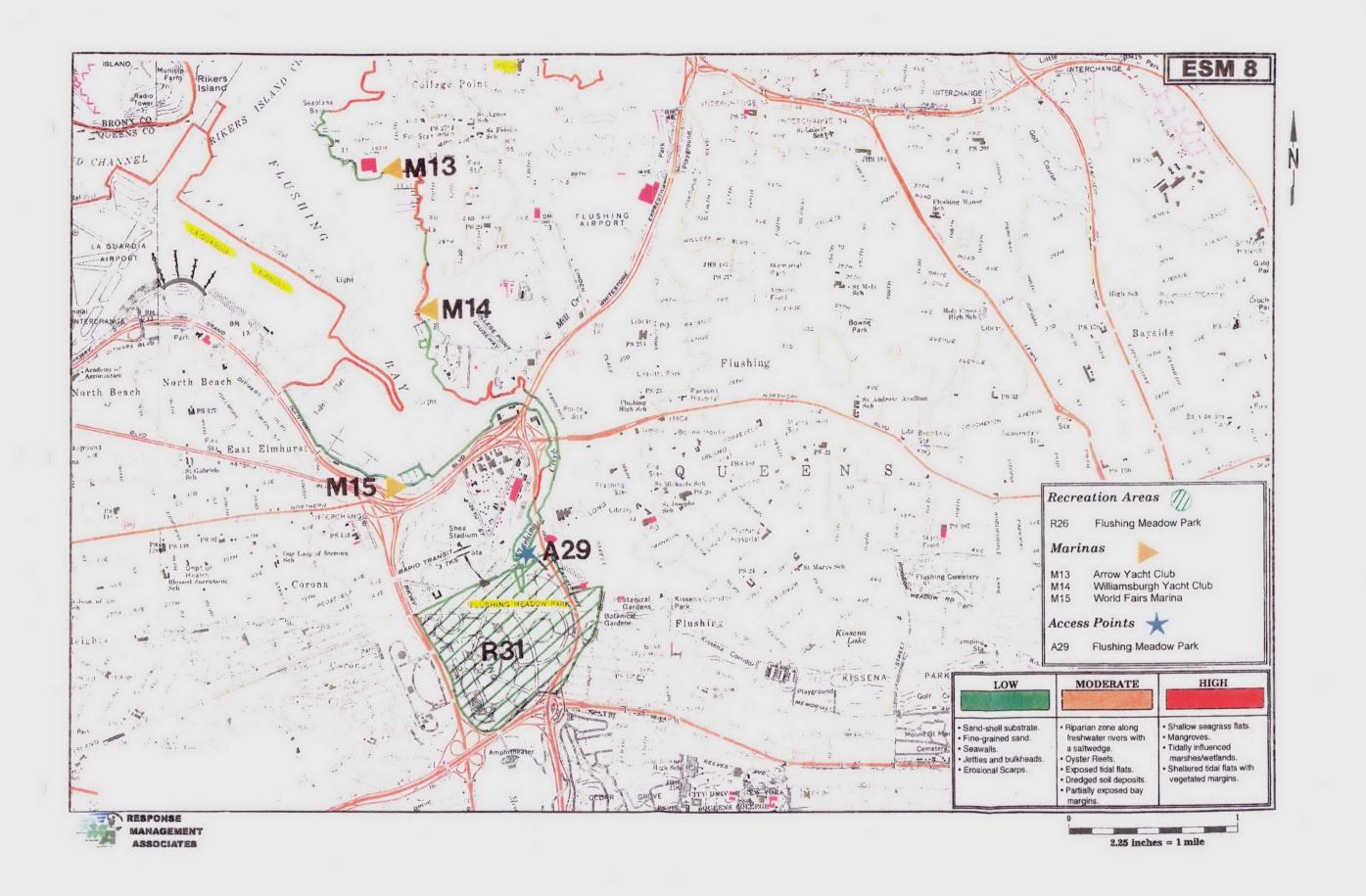
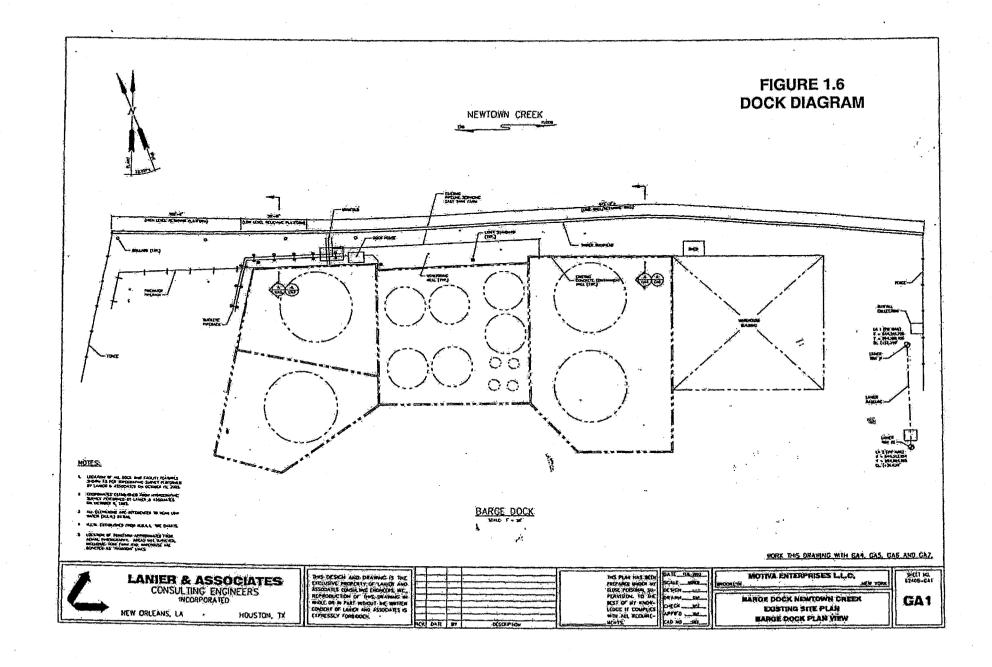
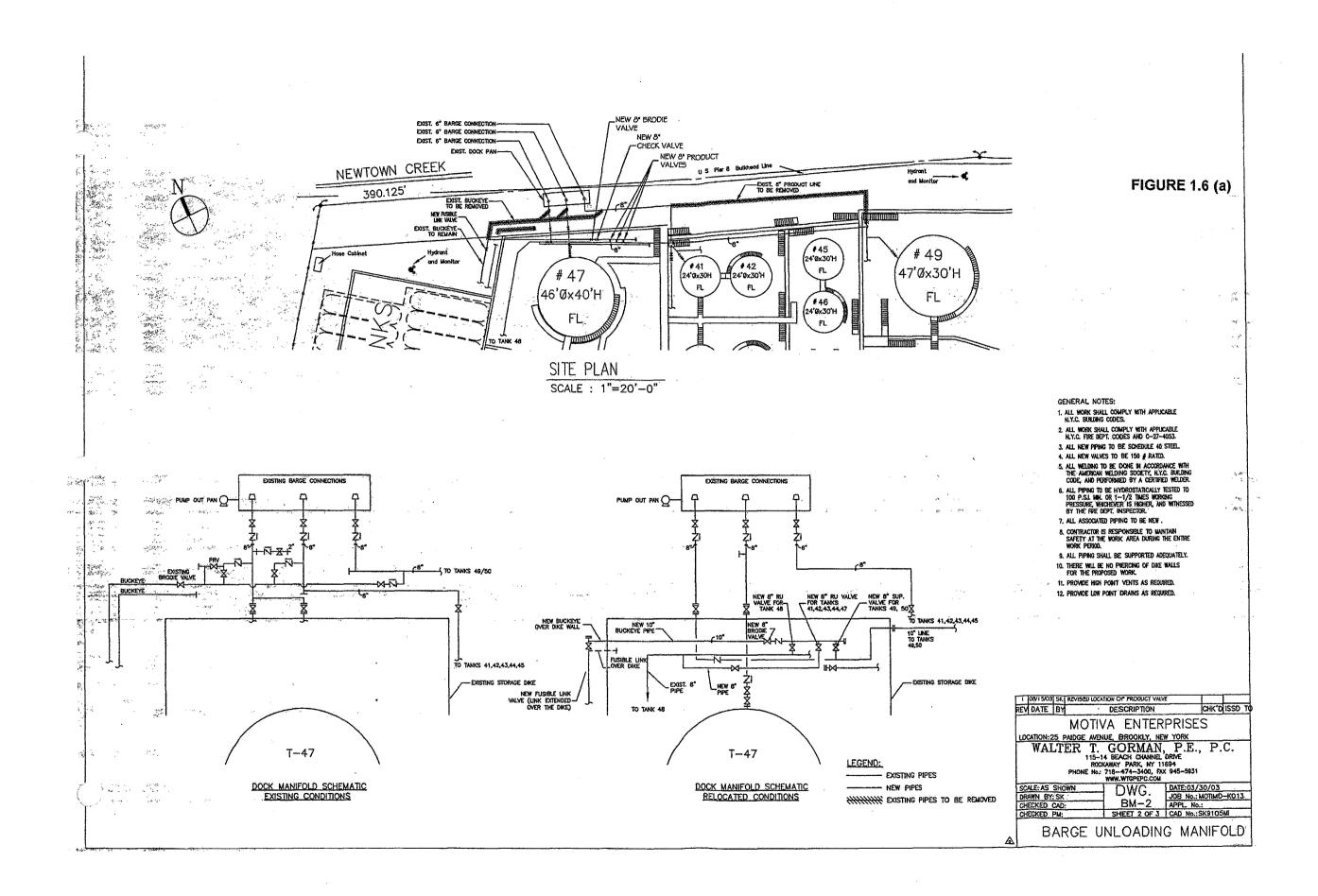


Figure 1.6 - Dock Diagram





ANNEX 2.....NOTIFICATIONS

2.1..... EMERGENCY RESPONSE INFORMATION

The information in this section describes what will be needed in an emergency involving the discharge of petroleum products or a combination of hazardous substances and petroleum products.

- a) Internal Notifications: In the event of a spill, the spill observer will immediately sound the emergency alarm and notify the Qualified Individual (QI) or the Alternate Qualified Individual (AQI). The QI / AQI will make further Internal Notifications, as appropriate, depending upon to size and / or severity of the incident, by calling the Regional Manager; Manager, LSDR/HSE and Emergency Management, and Communications Officer. The QI / AQI may call the Motiva Enterprises LLC Emergency Management, Preparedness, and Response for support if necessary.
- b) Community Notifications: If community notification and / or evacuation is necessary, the local Police Department will be contacted. The Local Area Evacuation Plan (LAEP) will be activated. The Company's Communications Officer will assist with radio and television announcements.

With assistance of the Local Emergency Planning Committee, the Fire Department, the Oil Spill Response Contractor, and the Red Cross, areas downstream of the incident will be alerted of the situation.

c) Federal and State Agency Notifications: The Incident Commander (QI / AQI) will ensure that all notifications are carried out in a timely manner. The following agencies should be notified as soon as possible:

United States Coast Guard – Local Marine Safety Office *National Response Center *Federal Environmental Protection Agency

State Agencies

*When calling the National Response Center or the EPA, include the following statement:

"This call fulfills any reporting obligations we may have, if any, pursuant to applicable laws and regulations including, but not limited to the Toxic Substances Control Act, Section 8 (e)."

2.1.1..... Emergency Notification Phone List

The Emergency Notification Telephone Numbers are provided in the Core Plan. The Facility Response Team members and telephone numbers are listed in the same section.

2.1.1.1.... How to Report a Spill

The instructions on how to report a spill and the Spill Notification Form are contained in the Core Plan.

It is the intent of the Facility personnel to notify the appropriate authorities and Company personnel of a spill as soon as possible. This will be done even if the spill reporting is for information purposes only and no assistance is required.

Motiva Enterprises LLC has a standing policy that all reportable spills will be reported as soon as practical.

All spills will be accompanied by a written report that will be forwarded to the Regional Manager for the assigning of an incident number. This form is used to track all spills, releases and discharges.

SITE SAFETY PLAN

I. G	eneral - Spill / Rel	ease						
☐ Land	☐ Air	☐ Water	□ +	IAZMAT	Othe	r:		
Facility:								
Location:		······································	···				·	
Objectives:	:_ 							
Operationa	l Period: Date				-	Time:	to _	
	azards to be Eva						•	
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	xygen Deficient/Enri		∐ Cher	nical/MSDS	S #			
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III. Weat				1 (000 0011	interito)			
		Tido:				Motor To	mnaratura:	
Skies Temperati	······································	Tide: Current:					mperature:	
•	ocity:					Current	rirection:	
		Wind Direction	JII		5			
	rol Measures	. 4	Λ.					
DCCOII						<u> </u>		
Ventilation	n:	☐ Mechanic					Continuous:	☐ No ☐ Yes
 Flagman/\\	/atchman:							
			······································					
V. To	esting & Monitori					ACCE	PTABLE ENTRY CON	
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	xygen Level		-	•	19.5 –	22.0% in air*	< 19.5% or 22.0% in air*	<16.0 or ≥ 23.5% in air
	EL			ery	< 10%	in air	≥ 10.0 but < 20.0% in air†	≥ 20.0% in air
	ydrogen Sulfide		eve	ery				
	enzene			ery	< 10 pp	om	≥ 10 but < 100 ppm	≥ 100 ppm
	OC:	∐Y ∐N □Y □N		ery	< 1 ppr		≥ 1 but < 3000 ppm	≥ 3000 ppm
	ther:	i	600	ery			andard(s) *Acceptable for 5325 f when LEL is greater than 10% in a	
VI. R	equired Personal	Protective E	auipme	nt (Check fo	or require	ed use)		
General		Respiratory					Footwear	Clothing
☐ Hard Hat	☐ Safety Glasses			☐ Ear Plugs		Leather	☐ Steel-toes	☐ FR Coveralls
	•	00D/ 0/ til 2ill0		☐ Ear Muffs		☐ Rubber	☐ Rubber	☐ Level A
☐ Safety Harr	ness Goggles	☐ Air Line						
☐ Safety Harr	ness Goggles Face-shield	☐ Air Line ☐ Air Purifying (F		☐ Combination	on	☐ Nitrile	☐ Hip-boots	☐ Level B
☐ Safety Harr	ness Goggles	☐ Air Line		☐ Combination	on	☐ Nitrile ☐ PVC	☐ Hip-boots ☐ Chemical Resistant	☐ Level B ☐ Level C
□ Safety Harr □ PFD	ness Goggles Face-shield Tinted Lens	☐ Air Line ☐ Air Purifying (F		☐ Combination	on	☐ Nitrile	☐ Hip-boots ☐ Chemical Resistant	☐ Level B
□ Safety Harr □ PFD Any other s	ness ☐ Goggles ☐ Face-shield ☐ Tinted Lens special PPE:	☐ Air Line ☐ Air Purifying (F Cartridge Type: []ov □H	☐ Combination	on	☐ Nitrile ☐ PVC	☐ Hip-boots ☐ Chemical Resistant	☐ Level B ☐ Level C
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□ Safety Harr □ PFD Any other s VII. Er Emergency Fire Depart Ambulance	Goggles Face-shield Tinted Lens Special PPE: mergency Inform Contact Person: tment:	☐ Air Line ☐ Air Purifying (F Cartridge Type: [ation and Res	scue Se	□ Combination		□ Nitrile □ PVC □ Contact by Contact by Contact by	☐ Hip-boots ☐ Chemical Resistant ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐	☐ Level B ☐ Level C ☐ Level D
☐ Safety Harr ☐ PFD Any other s VII. En Emergency Fire Depart Ambulance Hospital:	Goggles Face-shield Tinted Lens Special PPE: mergency Inform Contact Person: tment:	☐ Air Line ☐ Air Purifying (F Cartridge Type: [ation and Re	Scue Se	☐ Combination		□ Nitrile □ PVC □Contact by _ Contact by _ Contact by _ Contact by	☐ Hip-boots ☐ Chemical Resistant ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐	☐ Level B ☐ Level C ☐ Level D
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☐ Safety Harr ☐ PFD Any other s VII. Er Emergency Fire Depart Ambulance Hospital: Rescue Ser If not provided	Goggles Face-shield Tinted Lens Special PPE: mergency Inform Contact Person: tment: Fruices:	☐ Air Line ☐ Air Purifying (F Cartridge Type: [ation and Res	Scue Se	Combination		□ Nitrile □ PVC □Contact by _ Contact by _ Contact by _ Contact by	Hip-boots Chemical Resistant	☐ Level B ☐ Level C ☐ Level D

X. Comments or Special Work Procedures											
			<u></u>								
C. Report All Injuries Im	mediate	ly - "No	tify Site	Safety	Officer"						
Radio Channel:	Radio Channel: Radio Frequency: Telephone No										
Call 911 if life threatening											
XI. Monitoring Results	Zone								T		
	Time							-			
Oxygen	Level										
	Ву										
	Time										
LEL	Level										
	Ву		_								
	Time		_						<u></u>		
Hydrogen Sulfide	Level										
	Ву										
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Equipment: Type:			Mnfter: _ Mnfter: _			Cal Cal	ibration / ibration /	Expiration: Expiration:			

XII		Wo	ork	Are	a Di	agı	am																			
Ple	ase	inclu	ıde	wina	dire	ctio	n, e	xclus	sion z	zone,	supp	ort z	one,	deco	n ar	ea ar	nd sig	nifica	nt lan	dmar	ks.					
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I hereby acknowledge and authorize the above work to be performed in accordance with the conditions outlined on this permit. If the work procedures or conditions change creating any unsafe conditions, then this permit is void and work is to be suspended. I understand and affirm that the conditions of this work permit will be followed prior to and during entry into a confined space. I also agree to order the work to be stopped and the confined space evacuated in the event that conditions of the permitted work area fail to meet the permit requirements.

EMP&R NOTIFICATION LOG

Person on the EMP&R staπ to whom you relayed this emergency information:					
Name: Phone:() Time:: AM or PM (circle or	ne) Time Zone: EST or CST				
Document any calls or actions that you take in regard to this Emergency Call (including calls where you leave a message):					
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ANNEX 3.a RESPONSE TEAMS

3.a.....INTRODUCTION

This section describes organizational features and duties of the Local Response Team (LRT) and the Tier II and III Response Team. The Tier II and III Team are managed by Emergency Management (EM).

The key to an effective emergency response is a rapid, coordinated, tiered response by the affected unit/facility, AWAY Team, and/or National Response Team, consistent with the magnitude of an incident.

The Local Response Team will provide first response to an incident at a Facility. Emergency Management (EM)-managed Teams will respond, to the degree necessary, to incidents exceeding local capability and when requested. If additional assistance is needed, the Local Incident Commander will activate the EM-managed Teams, which may include:

- An AWAY Team
- A National Response Team (NRT)
- The Houston Support Center (HSC)
- A Corporate Emergency Response Team (CERT)
- The SOP US/Motiva Crisis Management Team (CMT)

Shell & Motiva Response Teams use the NIMS Incident Command System (ICS) to manage emergency response activities. Because ICS is a management tool that is readily adaptable to incidents of varying magnitude, it will be used for all emergency incidents. Staffing levels will be adjusted to meet specific response team needs, based on incident size, severity, and type of emergency.

An explanation of ICS and the roles and responsibilities for primary members of the Local Response Team is provided in Annex 3.a.5.

3.a.1....LOCAL RESPONSE TEAM

The first Alliance person on scene will function as the person-in-charge until relieved by an authorized/trained supervisor who will then assume the position of Incident Commander (IC). Transfer of command may take place as more senior management respond to the incident. For response operations within the control of the Local Response Team, the role of IC will typically be assumed and retained by Terminal Management.

The number of positions/personnel required to staff the Local Response Team will depend on the size and complexity of the incident. The duties of each position may be performed by the IC directly or delegated, as the situation demands.

The IC is always responsible for directing the response activities and will assume the duties of all the primary positions until the duties can be delegated to other qualified personnel.

Refer to the job descriptions detailed in this annex for the primary response team positions.

A complete ICS organization is shown in Figure 3.3. The LRT should try to fill the positions and request additional support from the Emergency Management, Preparedness, and Response Team to fill/back up all of the remaining positions, <u>as the incident dictates</u>. Telephone reference is provided in the Core Plan.

3.a.2....EM-MANAGED RESPONSE TEAMS

Motiva management resources available for incident response include:

- A National Response Team
- AWAY Team
- Houston Support Center (HSC)
- Corporate Emergency Response Team (CERT)
- SOP US/Motiva Crisis Management Teams

3.a.2.1 National Response Team

Motiva has resources through one National Response Team (Figure 3.1) that covers incidents that require a Tier III response.

A National Response Team, once fully staffed, is designed to cover all aspects of a comprehensive and prolonged incident response. During a prolonged response, additional personnel from within the Company may be cascaded in, and more than one level within the Team may be involved to sustain 24-hour operations.

3.a.2.2 National Response Team Organization

The National Response Team is organized according to Incident Command System principles (Figure 3.2). Led by Unified Command, the team includes the following principal components:

- Command Staff
- Operations
- Planning

- Logistics
- Finance

The complete ICS organization of the National Team is shown in Fig. 3.3.

3.a.2.3 Membership

The National Team is staffed by specially trained personnel from various Shell and Motiva business units as well as consultants.

3.a.2.4 AWAY Team

The AWAY Team is a component of the National Response Team, and is composed of designated, Houston-based personnel from various Shell and Motiva departments. Upon activation, the AWAY Team will preliminarily:

- Assess the magnitude of the incident and its potential impact;
- Estimate the level of effort necessary for minimizing its impact; and
- Depart to the scene of an incident from the Shell Corporate Hanger at Houston Bush Intercontinental Airport as soon as possible typically within two hours after being activated.

Once on scene, the AWAY Team will use the Incident Command System to:

- Manage the incident response; or
- Support the Local Team by integrating with the local response organization, providing liaison to government agencies and the news media, supporting or taking over any duties mutually agreed to, and helping keep the HSC and the SOP US/Motiva CMT informed.

The AWAY Team organization is shown in Figure 3.3.

3.a.2.5 Houston Support Center

When activated, the Houston Support Center (HSC) will be staffed to provide 24-hour Facility support, including managing field activities from the HSC until the AWAY Team and/or National Team arrives on scene.

For vessel incidents, the HSC will be the initial command post and Spill Management Team until an AWAY Team and/or National Team arrives and a new Incident Command Post is established. Once this is complete, the HSC will support the incident until no longer needed.

The basic HSC organization is shown in Figure 3.4.

3.a.2.6 Corporate Emergency Response Team

The Corporate Emergency Response Team (CERT) is a cross functional team of emergency responders from the operating business units. CERT members possess skills in one or more of the following areas:

- Incident Command
- Safety Officer

- Medical Unit Leader
- Operations Skill Pool
 - Fire fighting leadership
 - Hazardous materials response
 - Rescue
 - Planning Section Chief

CERT members may be activated to respond to any non-oil spill emergency. In the event ICS support positions are required that are external to the CERT, personnel from the National Response Team will fill those positions.

3.a.2.7 Shell Oil Products US/Motiva Crisis Management Teams

The SOP US/Motiva Crisis Management Teams manage crisis-related issues at the SOP US/Motiva Executive Leadership level. The Teams provide guidance on issues that have the potential to significantly impact the Company's reputation or operations, or pose a significant legal, regulatory, or financial liability.

The appropriate CEO, in accordance with the SOP US/Motiva Crisis Management Plan, will activate the SOP US/Motiva Crisis Management Team.

3.a.3.....RESPONSE TEAM TRAINING

Shell and Motiva require that all response personnel, including contractors and casual labor, have the appropriate training necessary to serve on a response team during an emergency. Local team members will receive training in the Facility Response Plan.

Each Local Response Team Member should review the Facility Response Plan whenever the Member's job position or responsibilities change under the Plan. A copy of this Plan will be available at all times to Team Members.

3.a.3.1 HAZWOPER (29 CFR 1910.120)

Federal and state regulations require that response team members maintain up-to-date HAZWOPER training necessary to function in their assigned positions. At a minimum, Motiva employees will receive "First Responder Operations Level" training. All "contract" personnel responding to a Shell or Motiva incident must be certified in accordance with the applicable HAZWOPER training requirements of 29 CFR 1910.120.

3.a.3.2 Incident Command System

Response team members will receive ICS training, and may also receive supplemental training in other related general topics.

3.a.3.3 Volunteers

Motiva will not use volunteers for response to an incident, if no Company provisions exist to train them. Volunteers may be used by government response entities, as allowed by applicable policies/ procedures.

3.a.3.4 Training Records

Training records for local team members are available, if needed, according to Federal, state, and local government requirements.

3.a.4....RESPONSE TEAM EXERCISES

Local and National Team members, government agencies, contractors, and other resources must participate in response exercises required by Federal, state, or local regulations and as detailed in the "National Preparedness for Response Exercise Program (PREP) Guidelines." Shell and Motiva will conduct <u>announced</u> and <u>unannounced</u> drills to maintain compliance, and each plan-holder must conduct at least one exercise annually.

The following table lists the triennial exercise cycle for facilities (see PREP Guidelines for full details).

	T	riennial Cycle				
Total Number	Frequency	Exercise Type/Description				
12	Quarterly	QI Notification Exercise				
6	Semi-Annual	Equipment Deployment Exercise (Facility-owned equipment)				
3	Annual	Response Team Tabletop Exercise				
3	Annual	Equipment Deployment Exercise (facilities with OSRO-owned equipment)				
3	Annual	Unannounced Exercise (not a separate exercise) Actual response can be considered as an unannounced exercise.				
NOTE: All response plan components must be exercised at least once in the Cycle.						

3.a.4.1..... Quarterly QI Notification Exercise

- <u>Scope:</u> Exercise communication between Facility personnel and the QI(s) and/or designated alternate(s). At least once each year, one of the notification exercises should be conducted during non-business hours.
- Objective: Contact must be made with a QI or designated alternate, as identified in the Plan.
- <u>General:</u> All personnel receiving notification shall respond to the notification and verify their receipt of the notification. Personnel who do not respond should be contacted to determine whether or not they received the notification.

3.a.4.2..... Semi-Annual Equipment Deployment Exercise (for facilities with response equipment)

- <u>Scope:</u> Deploy and operate Facility response equipment identified in the response plan. The equipment to be deployed must include the following, at a minimum:
 - 1,000 feet of representative type of boom;
 - One of each type of skimming system; or
 - The equipment necessary to respond to the Facility's Small/Average Most Probable Discharge (AMPD), whichever is less.
- <u>Objective:</u> Demonstrate personnel's ability to deploy and operate response equipment. Ensure that the response equipment is in proper working order.
- General: The Facility may take credit for actual equipment deployment to a spill, or for training sessions, as long as the activities are properly documented.

3.a.4.3.....Annual Equipment Deployment Exercise (OSRO-owned equipment)

- <u>Review:</u> The Facility should determine that the OSRO(s) has completed
 the equipment deployment exercise requirements and has maintained the
 necessary documentation. The OSRO may deploy equipment at any
 location, so long as it occurs within an operating environment similar to the
 Facility's.
- <u>Scope:</u> OSRO must deploy and operate response equipment identified in the response plan. The equipment to be deployed must include the following, at a minimum:
 - 1,000 feet of representative type of boom.
 - One of each type of skimming system.

• <u>Objective:</u> OSRO must demonstrate the ability of the personnel (OSRO) to deploy and operate response equipment (OSRO). Ensure that the response equipment (OSRO) is in proper working order.

3.a.4.4... Annual Response Team Tabletop Exercise

- <u>Scope:</u> Exercise the response team's organization, communication, and decision- making in managing a spill response. Each team identified within the plan must conduct an annual Response Team Tabletop Exercise.
- Objective: Exercise the response team in a review of the following:
 - Knowledge of the Plan.
 - Proper notifications.
 - Communications system.
 - Ability to access an OSRO.
 - Coordination of internal spill response personnel.
 - Review of the transition from a local team to a regional team.
 - Ability to effectively coordinate response activity with the National Response System (NRS) infrastructure.
 - Ability to access information in the Area Contingency Plan.
- **General:** A minimum of one Response Team Tabletop Exercise in a triennial cycle will involve a Worst-Case Discharge scenario.

3.a.4.5..... Exercise Documentation

- All exercises should be documented and maintained at the Facility; documentation should specify:
 - - The type of exercise;
 - Date and time of the exercise:
 - A description of the exercise;
 - The objectives met in the exercise;
 - The components of the response plan exercised; and
 - Lessons learned.

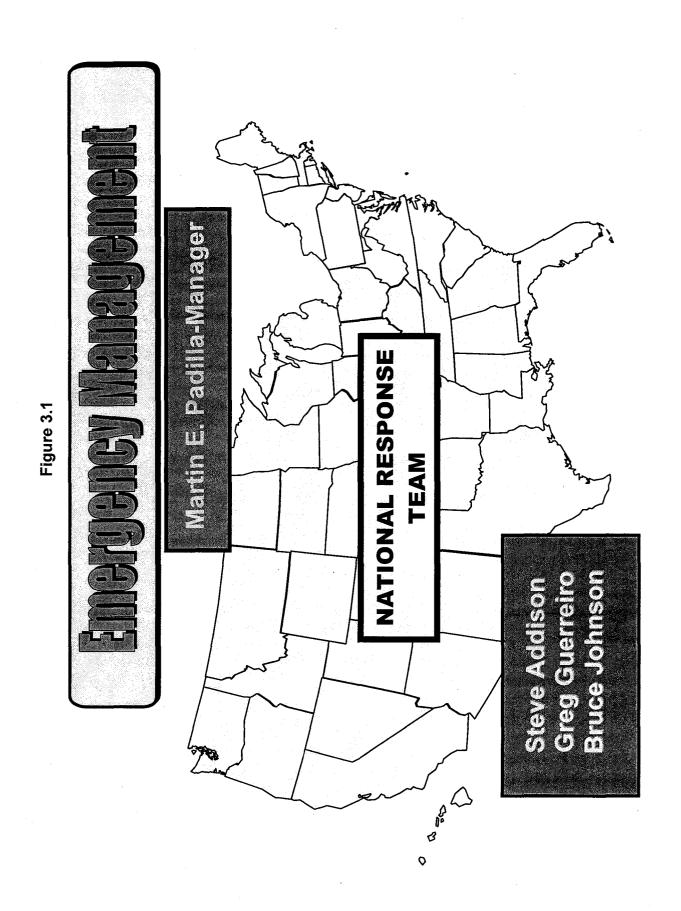


Figure 3.2

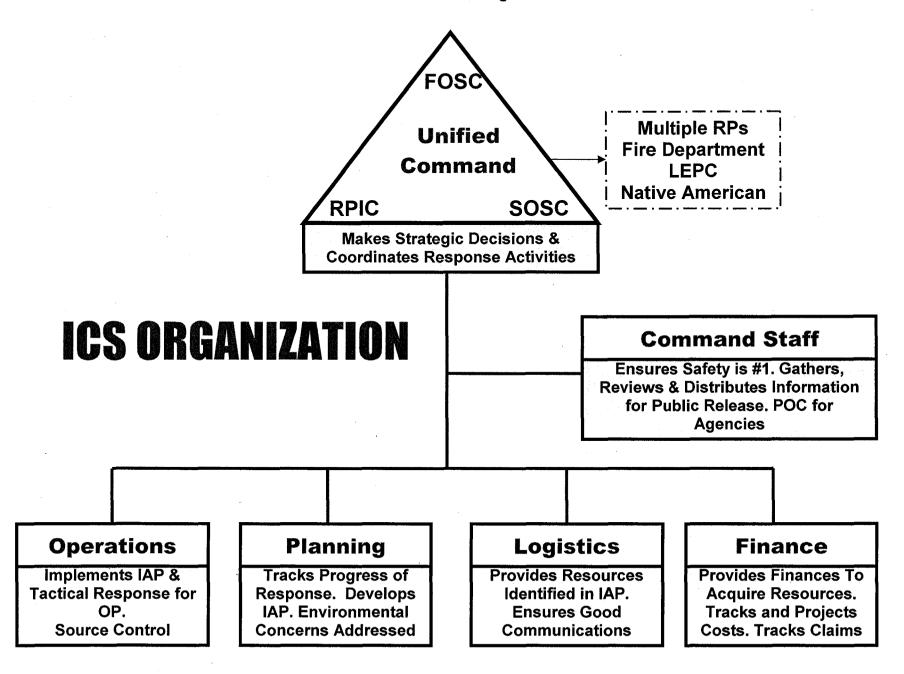
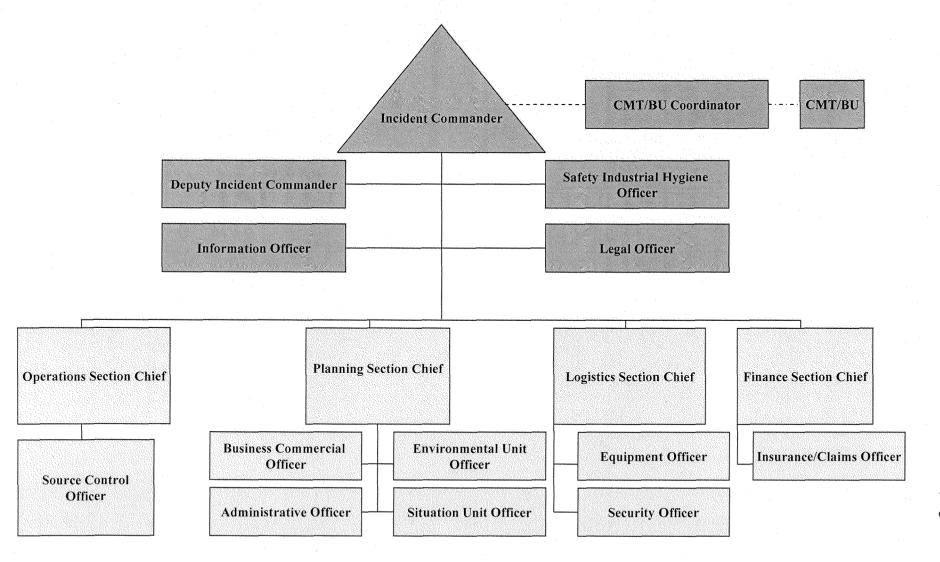


Figure 3.3



Figure 3.4

HSC Organization (ICS)



3.a.5....JOB DESCRIPTIONS

3.a.5.1 Local On-Scene Commander / Qualified Individual

The local On-Scene Commander (OSC) coordinates the activities of all personnel involved with administrative, technical, containment and clean-up operations at the spill scene and is designated as the Motiva Enterprises LLC QI. The local OSC assigns responsibility to various persons to act, but has final authority for any on-scene decision and, as such, is designated as the Motiva Enterprises LLC QI. A minimum of two people is required for 24-hour operation. However, one should be designated as the Senior Company Representative.

Scope of Responsibility

The local OSC is responsible for the implementation, effectiveness, and cost of the entire oil spill clean-up operation. This individual has complete authority over clean-up personnel at the spill scene. Typical, the local OSC will respond as follows to a spill incident:

Start Up

- ◆ Upon notification of an incident, the local OSC decides the initial start-up strategy and conducts a site investigation.
- Call out selected members of the Oil Spill Response Team.
- ◆ Consult with appropriate response team members to develop strategy for continuing response and any salvage operation.
- Establish and implement response priorities.
- Authorize procurement of equipment, manpower, and services identified to be necessary.
- Keep senior management informed of situation.
- ♦ Attend press/local audience conference(s) using agreed releases as basis for response.
- Notify government agencies of proposed activities.

Daily

- Hold a planning meeting with advisors and the Oil Spill Response Team.
- Meet with government agencies to obtain agreement on acceptable levels of response and environmental cleanup.
- ◆ Conduct a site inspection to make sure objectives are being accomplished.

- ◆ Meet with media representatives upon request of the Communications Officer.
- Evaluate and adjust response priorities.
- ◆ Transmit an updated situation report and press release to Senior Management.
- Maintain a log of these activities.

Periodic

- ◆ Authorize procurement of additional equipment, manpower, and services, as required.
- ♦ Approve invoices not delegated to support personnel for payment.
- ◆ Attend press/local audience conferences at the request of the Communications Officer.

Stand Down

- Ensure that the Support Coordinator, before leaving site, is provided with a copy of any notes or observations made by team members during the operation for use at the post-incident stewardship meeting.
- ◆ Convene post-incident stewardship meeting approximately four (4) weeks after stand down.
- Monitor training programs.
- Monitor the Oil Spill Response Team structure.

Points to Consider

- 1. Oil Spill cooperatives and contractors may be the best source for immediate equipment needs.
- 2. Provide frequent press statements and public meetings, when appropriate, to keep the public informed.
- 3. Plan for the worst-case situation when emergencies occur.

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4. During emergencies, many people become instant experts. Always require consultants and technical personnel to support their recommendations with proven examples and data.

3.a.5.2Field Operations Coordinator (Terminal Employee)

The Field Operations Coordinator is in charge of the field operations relating to the oil spill cleanup and, as such, is designated Alternate Qualified Individual (AQI). The AQI delegates responsibility to a number of field supervisors and superintendents and communicates frequently with the local OSC with updates on the various phases of the operations. The AQI also identifies the future requirements of his staff and arranges for more equipment and/or personnel as required.

Scope of Responsibility

The AQI is responsible for all field operations in the clean-up of the oil spill, including the following:

Start Up

- ◆ At the incident location, prepares input to and attends the local OSC's strategy and start-up planning meeting.
- Supervises the implementation of the agreed response plan.
- Evaluates the situation at the oil spill site to assess amount of oil to be removed and methods to be employed. Works with the Environmental and Regulatory Agency Advisors to establish if cleanup is to be attempted; if so, where and to what degree.

Daily

- Prepares for and attends the local OSC's planning meeting.
- Maintains regular radio contact with the local OSC.
- Monitors the effectiveness of containment, cleanup, and disposal operations—modifies these as necessary.
- Monitor effectiveness of procedures/equipment employed; makes recommendations to the local OSC as appropriate.
- ♦ Monitors the effectiveness of shore clean-up operations; makes recommendations, as appropriate, to the local OSC.
- Maintains a log of all of these activities.

<u>Periodic</u>

 Assumes control of the total incident response in the absence of the local OSC.

Stand Down

- Provides the Support Coordinator, before leaving site, with a copy of any notes or observations made during the operation for use at the postincident stewardship meeting.
- ◆ Agrees with relevant government/local authorities that acceptable stand down conditions exist on each cleaned up site.
- Monitors developments in containment and recovery techniques and equipment.
- ◆ Maintains an up-to-date register of specialists in oil containment and recovery.

3.a.5.3 Environmental / Safety Advisor

The Environmental / Safety Advisor is familiar with the ecological effects of oil, dispersants, and the clean-up operations on the flora and fauna in the spill area. This individual may recommend against certain types of clean-up operations in environmentally sensitive areas where the effects due to the clean-up operation may be more severe than the effects of oil. The Environmental / Safety Advisor estimates the trajectory of the oil spill and determines priorities for cleanup.

The Environmental / Safety Advisor is an expert in the performance of booms, skimmers, sorbents, etc. This individual knows which equipment works best under the particular conditions of the spill and will advise on the purchase, rental, or other acquisition of the most cost-effective clean-up equipment. The Environmental / Safety Advisor recommends the methods to be used to contain and recover the oil. This individual's activities are coordinated with those of the Field Operations Coordinator.

The Environmental / Safety Advisor is also knowledgeable in ways and means to temporarily store and ultimately dispose of the recovered oil. He or she will advise on the most cost effective and, in coordination with the Law Department, legal ways to hold large quantities of recovered oil and debris while awaiting its proper disposal. This individual will also determine the best way to dispose of the recovered oil (e.g., incineration, burial, recycling, etc.).

The Environmental / Safety Advisor should be well-versed in safe operation practices and have a basic knowledge of first aid. He or she will identify potential safety problems at the spill site and communicate this information to the field forces. All first aid and medical treatment operations come under his or her jurisdiction.

Scope of Responsibility

The Environmental/Safety Advisor is responsible for continuously assessing damage and potential damage to the environment and reporting to the local OSC. In addition, he or she is:

- Responsible for providing expertise as to the optimum methodology for the containment and recovery of oil for the conditions that exist.
- Responsible for providing expertise in disposing of recovered oil and oiled debris in a safe and efficient manner acceptable to local authorities.
- Responsible for providing expertise on the safe practices to be followed in all operations for the oil spill cleanup.
- ♦ Responsible for maximizing protection of sensitive habitats and wildlife protection/rehabilitation efforts.

Start Up

- At the incident location, prepare input to and attend the local OSC's strategy and start-up planning meeting.
- Evaluate the situation at the spill site; assess damage and potential damage to environment.
- ◆ Apply for any manpower or specialist resources needed to conduct monitoring/investigation work.
- Coordinate the efforts for rescuing oiled wildlife.
- ♦ Work with fish and game agencies to identify wildlife habitats and seasons with high population densities.
- Recommend wildlife habitats for protection.
- Invoke existing contractor to handle potentially dangerous wildlife.
- ♦ Contract with wildlife specialists for bird rescue and protection.
- Identify local facilities for wildlife rehabilitation.
- Request company funding to lease rehabilitation facilities.
- Request zoos to provide homes for recovering animals.
- Set up facilities for collecting and disposing of animal carcasses.
- Arrange for environmental specialists to collect data and identify impact to:
 - Water and air quality.
 - Human health.

- ♦ Assess the impacts of various response techniques on the environment.
- ♦ Meet with the Federal Regional Response Team and environmental agencies to learn their concerns about environmental impacts.
 - Determine which permits are required and prepare and submit applications. Seek waivers as appropriate.
 - Prepare environmental guidelines for the local OSC and contractors.
 - At the incident location prepare input to, and attend the local OSC's strategy and start-up planning meeting.
- Evaluate the situation at the oil spill site to assess the amount of oil to be removed and methods to be employed for containment and recovery.
- ♦ Consult local, state, and federal requirements for waste storage, transportation, and disposal requirements.
- Obtain local authority approval for the disposal of recovered oil and oiled debris.
- Work with Field Operations Coordinator to estimate storage capacity needed for recovered oil and oiled debris.
- ◆ Contact terminals or chemical plants near the spill area to see if they have capacity to temporarily store recovered oil.
- ♦ Identify regional waste disposal facilities and determine procedures for waste acceptance.
- ◆ Determine, with the Field Operations Coordinator, the extent of manpower, equipment, and services necessary to execute plans.
- Establish contact with local emergency/medical services.
- Establish first aid posts.
- Establish instruction and training facilities for contract labor.

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Coordinate implementation of permit to work system.

Daily

- Attend the local OSC's planning meeting.
- Monitor the effects of clean-up operations on the local ecology, and report to the local OSC.
- Maintain contact with local ecology experts in order to take full account of local factors and to brief them on clean-up strategies.
- Monitor field-sampling operations.

- ♦ Keep records of number of oiled animals:
 - dead
 - spotted
 - collected
 - rehabilitated and released
- Provide supervision for wildlife centers set up for the emergency.
- Record oiled animal sightings on wall map.
- ◆ Update list of environmental and commercial resources impacted and threatened by the spill.
- Coordinate with all regulatory agencies.
- ♦ Monitor the effectiveness of clean-up operations and equipment employed. Make recommendations as appropriate to the local OSC and Field Operations Coordinator.
- ♦ Assist the Incident Operations Coordinator in agreeing with local authorities that prescribed clean-up standards have been achieved.
- Monitor recovery and disposal; make recommendations, as appropriate, to the local OSC and Field Operations Coordinator.
- ◆ Supervise activities for recovered oil transportation, storage, and disposal.
- Monitor recovered oil and waste handling activities to make sure that regulatory requirements are satisfied.
- Maintain logs to document the following:
 - Quantity and types of equipment deployed for containment and recovery.
 - Quantity and types of material stored.
 - Storage locations for recovered materials.
 - Disposal sites used for recovered materials.
- ◆ Attend the Field Operations Coordinator's planning meeting.
- ♦ Monitors the effectiveness of security, safety, and medical care arrangements and modifies these as necessary.
- Hold a planning meeting with senior safety personnel.
- Monitor clean-up operations and advise the Field Operations Coordinator immediately should it be necessary to halt any activity. (The Environmental / Safety Advisor has authority to halt any activities that contravene legal or company requirements.)

- ◆ Examine (or prepare) operating and safety instructions for all equipment and products delivered to site to ensure that instructions are relayed to, and understood by, operators.
- ♦ Monitor the effectiveness of instruction and training facilities implemented.
- Maintain a log of all of these activities.
- ◆ Check OSHA training certification documents and ensure all personnel involved in spill cleanup has the required HAZWOPER training.

Periodic

- ◆ Conduct aerial surveillance to locate endangered wildlife habitats threatened by spill.
- ♦ Hire consultants to research response and problems for similar emergencies.
- ◆ Provide input that will help the local OSC to establish priorities for shoreline protection.
- ◆ Advise the Field Operations Coordinator of the quantity of recovered oil on hand that can be recycled.
- ◆ Advise the Field Operations Coordinator of the permits needed for waste disposal, storage, or transportation.
- Investigate, report, and record all accidents.
- Attend induction/debriefing of contractors.

Stand Down

- Provide the Support Coordinator, before leaving site, with a copy of any notes or observations, made during the operation, for use at the post-incident stewardship meeting.
- ◆ Maintain awareness of significant developments concerning the environmental impact of oil pollution.
- ♦ Hold and maintain an up-to-date register of national ecological specialists.
- Stand down equipment/manpower/specialist local services.

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- Issue a final status report.
- Monitor developments in containment and recovery techniques and equipment.

- ◆ Agree with relevant government/local authorities that acceptable stand down conditions exist on each cleaned up site.
- Monitor developments in shore clean-up techniques and equipment.
- Monitor developments in disposal/storage techniques.
- Maintain an up-to-date record of licensed disposal/storage sites.
- Maintain an up-to-date list of licensed waste haulers.

Points to Consider

- ◆ The potential for environmental impacts constantly changes as winds shift spill movement.
- Do not release rehabilitated wildlife to areas that will be impacted by oil slicks.
- ◆ Animals will ingest oil when they preen themselves. This will contribute to high mortality rates.
- ♦ Eagles, bears, and other scavengers will eat oiled animals; therefore, oiled animals should be removed as soon as possible.
- ♦ Shellfish and bottom fish samples may be needed. If oil enters commercial or subsistence areas for these fish, work with regulatory agencies to determine if closure is warranted.
- Do not bury recovered oil or oil contaminated debris.
- ◆ Environmental permits may be required to burn or incinerate oil-contaminated material.
- Emulsified oil should be treated with emulsion breakers before storage.
- ◆ Oil contaminated booms and other damaged equipment may require disposal.

3.a.5.4 Support Coordinator (Terminal Employee)

Scope of Responsibility

The Support Coordinator is responsible for all security matters; for establishing, operating, and maintaining an effective communications network; for locating, purchasing and expediting the materials and services required for the Oil Spill Response Team; and for maintaining a complete and accurate record of all events that occur.

Start Up

- Convey stocks of security passes to site.
- Establish access control and arrange for site security
- ◆ Establish access control to base control point/ field control point/ equipment depots/ recovered material collection points.
- ◆ Contact local area telephone company requesting additional telephone lines.
- Establish communications network.
- Set up telephone system for Field Command Post.
- If necessary, arrange for initial catering/janitorial services required with Field Operations Coordinator, and establish availability of such services and hotel accommodations in locality.
- ♦ If necessary, establish ad hoc field food services (sandwiches/drinks from local caterers, etc.)
- Convey pre-prepared stock of purchase order forms, open order files, and stock cards to support services field control point.
- Arrange for necessary manpower resources to perform tasks in own area.
- Process approved requests for materials and services.
- Set up procedures to authorize and account for expenditures.
- ◆ Process purchase order numbers to authorized contractors, merchants, and vendors.
- Check time sheets of contractors to verify accuracy.
- Distribute pre-printed logbooks to team members.
- Maintain a display of oil spill management data on the walls of the command and/or operations center(s).
- Assist Local On-Scene Commander as required.
- Set up historical log to record daily events
- Set up record keeping system for:
 Companies and agencies offering assistance.
 Calls to Local On-Scene Commander.
 Correspondence

Daily

- Attend the Local On-Scene Commander's meeting.
- Hold planning meeting with security personnel.
- Monitor effectiveness of security plan.
- Maintain liaison with police.
- Maintain radio network.
- Maintain communications network for operation and security.
- Check:
 - System power source.
 - Tape recorders for conferences.
 - Cameras, films, & video equipment.
 - Battery chargers
- Receive, verify, and process invoices.
- Conduct inspections to make sure items received meet specifications for items ordered.
- Maintain log.
- Attend Local On-Scene Commander's planning meeting as recording secretary.
- File all documents.
- Maintain shift logs which document: (Obtain information from Field Operations Coordinator)
 - Number of pieces and types of equipment deployed.
 - Number of contractor personnel employed
 - Consultants employed.
 - Company personnel on-site.

Periodic

- Investigate any security incidents.
- Maintain close liaison with local police.
- Attend induction/debriefing of contractors.
- Schedule maintenance for communications network.
- Provide training for using communication equipment.
- On continuous basis, process approved applications for materials and services.

- Keep records of equipment purchased and issued to contractors.
- Submit daily/weekly report of expenses.
- ♦ Recommend termination for contractors and consultants that are no longer needed.
- ◆ Prepare weekly chronological report for Local On-Scene Commander.
- Collect log/note books from team members.
- ◆ Collect purchase orders, work orders, and contracts for the Local On-Scene Commander's signature.

Stand Down

- Maintain a stock of pre-prepared security passes.
- Develop and maintain a security plan.
- Recall all equipment and record return.
- ◆ Collect from other team members copies of all notes, logs, and/or observations made during the operation for use at the post-incident stewardship meeting.
- ◆ Prepare full chronological report for Local On-Scene Commander.
- ♦ Stand down equipment, manpower, and local services.
- ◆ On completion of operation, arrange for equipment and materials to be returned to contractors.

Points to Consider

- ◆ Determine the radio frequencies in concert with USCG, EPA, and contractors.
- ◆ Determine communications that will be needed for all groups participating in clean-up operations.
- ◆ Encourage personnel using the communication network to practice proper radio protocol.
- ◆ Review vendors' invoices, as there may be attempts to overcharge for emergency services.
- ◆ Fixed-fee contracts for services and labor are in the Company's best interest.
- Make sure that the contract scope for materials and services is well defined.
- Ask vendors for quantity discounts and discounts for prompt payment.

1

◆ Industry oil spill cooperatives require equipment to be returned in good condition. Most equipment exposed to spilled oil is difficult to return to its pre-spill condition; therefore, it may be necessary to purchase and replace equipment borrowed from cooperatives.

- ◆ If the 30-day lease rate for equipment equals 75 percent of the purchase cost of new equipment, it may be better to buy new equipment.
- ♦ Contractors may provide oiled or poor equipment and charge new equipment rates.
- ♦ When possible, purchase materials and supplies from local merchants.
- ◆ Encourage best management practices relating to the purchase or leasing of equipment and manpower.

3.a.5.5.....Hazardous Waste Contingency Plan Job Descriptions:

- <u>Terminal Superintendent</u> Coordinates storage, inspection, transportation and disposal of hazardous waste related to the operations of the Facility. In the event of a spill, the Qualified Individual shall serve as Incident Commander and Administrator of the Response Plan.
- <u>Terminal Supervisor</u> Coordinates storage, inspection, transportation and disposal of hazardous waste related to the operations of the Facility.
- <u>Terminal Operator</u> Coordinates storage and inspection of hazardous waste containers in the designated waste accumulation area at the Facility.
- **Environmental Coordinator** Coordinates waste characterization, storage, transportation, and disposal of hazardous waste relating to Facility operations and remediation of groundwater at the Facility.

ANNEX 3b., COMMAND

3.b.1...... Qualified Individual and Duties

The Qualified Individual (QI) and the AQI (whether Terminal Superintendent, Administrative Assistant or a Terminal Operator) shall have full authority including access to Company funding and contracting authority to implement spill response actions. The QI/AQI shall communicate immediately with the appropriate regulatory personnel, Company personnel and any necessary spill response contractor to ensure a timely and reasonable response to a release. The QI/AQI shall insure that notification of National Response Center, required under regulations implementing CWA Section 311(b) is complete. Arrangements will be made at all times to ensue that either one or the other (QI/AQI) is available on a 24-hour basis and is able to arrive at the Facility in a reasonable amount of time.

Specifically, in the event of a release the QI/AQI shall perform the following sections:

A Qualified Individual is required to:

- A) Be available on a 24-hour basis:
- B) Speak fluent English;
- C) Be located in the United States;
- D) Be familiar with the implementation of the Response Plan;
- E) Be trained in the responsibilities of the qualified individual under the Response Plan;
- F) Be provided a document by the owner/operator designating them as a qualified individual and specifying their full authority to—
 - (1) Activate and engage in contracting with oil spill removal organization(s) and other response related resources identified in the Plan;
 - (2) Act as a liaison with the predesignated Federal On-Scene Coordinator (OSC); and
 - (3) Obligate funds required to carry out response activities.

If the QI is also the IC, vital duties include:

- A) Activate internal alarms and hazard communications systems to notify all Facility personnel,
- B) Notify all response personnel, as needed,
- C) Identify the character, exact source, amount, and extent of the release, as well as the other items needed for notification,
- D) Notify and provide necessary information to the appropriate Federal, State, and local authorities with designated response rolls, including the National Response Center, State Emergency Response Commission, and Local Emergency Planning Committee,
- E) Assess the interaction of the spilled substance with water and or other substances stored at the Facility and notify response personnel at the scene of that assessment,
- F) Assess the possible hazards to human health and the environment due to the release. This assessment must consider both the direct and indirect effects of the release (i.e., the effects of any toxic, irritating, or asphyxiating gases that may be generated, or the effects of any hazardous surface water runoffs from water or chemical agents used to control fire and heat-induced explosions),
- G) Assess and implement prompt removal actions to contain and remove the substance released.
- H) Coordinate rescue and response actions as previously arranged with all response personnel,
- I) Use authority to immediately access Company funding to initiate cleanup activities, and
- J) Direct cleanup activities until properly relieved of the responsibility.

3.b.1.1... NIMS ICS Command Aspects

The Incident Command System (ICS) is used to manage an emergency incident or a non-emergency incident. It can be used equally well for both small and large situations.

The system has considerable internal flexibility. It can grow or shrink to meet differing needs. This makes it a very good cost-effective and efficient management system. The system can be applied to a wide variety of emergency and non-emergency situations.

The Command Post will be located in the Terminal Office Building, if possible. The first alternate Command Post will be one of the warehouses located on the Facility property.

3.b.2...... Internal and External Communications

Internal Communications

In the event of a spill, field personnel will immediately notify the Qualified Individual (QI) or the Alternate Qualified Individual (AQI) verbally or via two-way radio. All of the field personnel have two-way radios and QI/AQI has access to a radio at the Facility. The QI/AQI will immediately activate the emergency shut off switch and activate the exit gate to open. The emergency shut off will shut down all the pumps in the Facility including the loading rack pumps. The QI/AQI will inform all personnel via telephone or verbally of the emergency and why evacuation is necessary. If necessary the QI/AQI will assign someone to guard the gate area.

After the employees are told of the emergency and if evacuation is necessary, they should proceed to the gates of escape via evacuation routes (Figure 1.2) and wait for further instructions. In case of a power failure, the pumps will automatically be shut down and the entrance and exit gates can be opened by removing the motor box cover and releasing the clutch at which time the gates can be opened manually.

- For minor emergency evacuation, employees should walk to the reassembly area at the entrance on Paidge Avenue and await further instructions.
- If a Facility evacuation is called for, an alternative command post will be set up at the Long Island Sales Terminal.
- Area and Community Evacuation Plans have been discussed in Core Plan, Section 1.1.6.

If tanks or tank trucks of gasoline or diesel are involved in a fire, isolate for at least one half mile in all directions.

Procedures to account for employees (roll call):

- Employees must stay together on any evacuation.
- Employees are not to leave an evacuation point until their supervisor has accounted for them.

External Communication

For public notification and evacuation, the Facility could obtain the assistance of the Police, the Fire Department and the LEPC. Community evacuation may be facilitated by the use of emergency sirens, media broadcast, PA systems, bullhorns and/or door-to-door notification by police, fire departments and other city employees.

Motiva Enterprises LLC's goal is to keep the public informed in the event of an emergency involving the safety of individuals and/or property. In the event of such an emergency, the Senior Company Official present shall designate a qualified person to handle inquiries from the press. The person so designated, hereafter called "Media Contact", shall gather facts available, including what happen, when, where and the current situation.

In replying to initial questions from the media, the Media Contact should say that the Company would issue a statement as soon as the facts can be obtained.

The Media Contact will immediately notify the nearest Motiva Enterprises LLC Communications Representative of the emergency. The Communications Representative will then take over and prepare all press releases and coordinate community and employee family needs. He or She will handle all public affairs matters with the Incident Commander.

3.b.3..... Safety

The safety of all responders is the most important object in the incident command system. Motiva Enterprises LLC Safety Coordinator will work closely with all other safety officers to ensure that proper procedures are followed. During the "clean-up" phase of the response, Motiva Enterprises LLC's permit program will be followed.

Company Personnel

Workers who have received "First Responder Operations Level" training as outlined by OSHA 29 CFR 1910.120(q)(6)(ii) may respond for the purpose of protecting nearby persons, property or the environment from the effects of the release. Their only response shall be defensive in nature without actually trying to approach the point of release to stop it. Their function shall be to contain the release from a safe distance, keep it from spreading, and prevent exposures. They shall not engage in any activity that would present an actual or potential inhalation hazard from the spilled material, which would require the use of respiratory protection.

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Contractor Personnel

The spill contractor will furnish a **Site Specific Safety and Health Plan** before engaging in a clean-up operation. This document shall be on all hazardous waste site jobs. It must be kept up-to-date and be present for review by employees, contractors, subcontractors, federal, state and local authorities. Pre-entry briefings should be held prior to initiating any site activity and the Site Safety and Health Plan reviewed.

The Safety Officer will be responsible for the following:

- All responders and contractors have credentials demonstrating appropriate OSHA HAZWOPER training.
- A safe perimeter is maintained throughout the response. This will include inspection of air monitoring equipment.
- All ignition sources have been identified and neutralized.
- A Site Safety and Health Plan is in effect for the entire operation.
- That proper PPE is being used as identified in the Site Safety and Health Plan.
- Decontamination is being conducted by all responders.

3.b.4..... Liaison

An incident at the Facility will activate the notification process. The Local Response Team will work closely with the local agencies and the emergency management utilizing the Incident Command System.

If the response exceeds the capability of the local response team, the Qualified Individual will request the assistance of the Emergency Management, Preparedness, and Response Regional Team.

ANNEX 3c... ICS OPERATIONS

3.c.1..... OPERATIONAL RESPONSE OBJECTIVES

Motiva Enterprises LLC will operate its Facility and implement this Plan to be protective of human health and the environment.

In general, the Qualified Individual will take the following actions:

- Investigate any and all reports of leaks or spills to determine what actions need to be taken and what actions can be taken immediately to mitigate the leaks.
- In the event of a major spill, determine whether or not the spill can be stopped, halted, or contained by simple immediate actions that can be performed with safety.
- Close the Facility for the duration of the emergency. If required, or if fire or explosion potential is high, contact the local law enforcement and the state police to evacuate the area and to block off the potentially affected highways. The approved Local Emergency Planning Committee evacuation plan will be followed as it pertains to evacuations.
- Notify the appropriate emergency response agencies and activate the Spill Response Plan.
- ♦ Contact the contractors listed in Core Plan 1.1.2 for immediate assistance on spill response and supplies.
- ◆ The personnel identified in Annex 3.A will be involved in directing the activities of the spill response team and contractors for the site.
- Begin activities to recover spilled material.
- Determine a location on the site that can be used to stage equipment and a second location on the site where contaminated soil can be stored safely. If large volumes of contaminated soil are anticipated, the preferred method of decontamination of the soil is by on-site incineration. An off-site staging area for the incinerator may have to be developed to maintain a low fire hazard.

3.c.2...... DISCHARGE CONTROL & ASSESSMENT / MONITORING

The response actions to a spill are dependent on the magnitude of the spill. The necessary equipment, products, and personnel for spill response vary depending on the quantity of the discharge. This section describes general guidance for handling spills as well as specific plans for dealing with small, medium, and worst-case discharge scenarios. The following general guidance must be observed by all persons working with spilled materials.

3.c.2.1.... Diesel Fuel Spills

The fire danger from diesel fuels is moderate. Diesel fuels float on water and caution should be used in working with or near the fuels because of their flammability and vapors. Exposure to or inhalation of diesel fuels can be hazardous to health. The preferred response for cleanup of diesel fuels is containment of the fuels and recovery. However, extreme caution should be exercised in order to assure that the area is safe and free of explosive vapors prior to commencement of containment and recovery activities. Sensitive environmental areas should be protected immediately by use of floating booms to ensure that diesel fuels do not intrude into those areas.

NOTE: Personnel safety is the primary consideration in any emergency. Avoid excessive exposure to liquid and vapors. These procedures are considerations only. Actual circumstances may dictate that procedures followed may differ somewhat from those listed below.

- Identify the source and stop discharge if possible.
- Use an explosimeter and other air sampling equipment to assure areas are safe to enter for continued response operations.
- If the spill occurs in the tank farm, every effort must be made to block any drainage to ditches in order to prevent product from reaching the waterway.
- Contain and isolate the spill. Monitor containment for effectiveness.
- ◆ Advise neighboring operations of any threat to their property or personnel.
- Determine the direction and expected duration of spill movement.

◆ If the spill enters the waterway, review the location of any environmentally sensitive areas identified in Annex 1. Determine which of these may be threatened by the spill and direct the Oil Spill Cleanup Contractor (COOP), if applicable, to proceed with boom and skimmers to these locations. Take appropriate actions as indicated on the response maps and initiate recovery actions.

3.c.2.2.... Gasoline Spills

The presence of gasoline poses extremely high potential for explosion and fire. Gasoline floats on water and gasoline vapors can travel substantial distances and generate explosions. Exposure to gasoline or its vapors can cause a narcotic effect and can pose a severe health hazard. In the event of a gasoline spill, the preferred remediation strategy is to knock down or disperse the vapors and allow the product to evaporate until the fire hazard has passed. Gasoline vapors are heavier than air and will settle in low places. Also, gasoline vapors may travel long distances due to wind action.

Environmentally sensitive areas should be protected by temporary dikes or diversionary booms. The areas near the vapor cloud must be evacuated if the danger of fire or explosion is to be minimized.

NOTE: Personnel safety is the primary consideration in any emergency. Avoid excessive exposure to liquid and vapors. These procedures are considerations only. Actual circumstances may dictate that procedures followed may differ somewhat from those listed below.

- Identify the source and stop discharge if possible.
- ◆ Use explosimeter and other air sampling equipment to assure that areas are safe to enter for continued response operations.
- ♦ Eliminate sources of vapor cloud ignition. Use waterfog to knock down vapors and disperse material.
- Stay upwind and evacuate nonessential personnel.
- ◆ Advise neighboring operations of any threat to their property or personnel.
- Determine the direction and expected duration of spill movement.
- ♦ If the spill enters the waterway, review the location of any environmentally sensitive areas identified in Annex 1. Determine which of these may be threatened by the spill and direct the COOP (if applicable) to proceed to those areas with boom to divert any remaining spilled product.

3.c.2.3.... Ethanol Spill

Many of the procedures set out for Diesel and Gasoline spills should be used during an Ethanol incident. Personnel 00safety is the primary consideration in any emergency. Avoid excessive exposure to liquid and vapors.

In case of an Ethanol fire:

◆ Use Alcohol Resistant (AR) foams for incidents since Ethanol will absorb and break down other firefighting foams rendering them ineffective and it takes copious amounts of water to extinguish an Ethanol fire.

For Ethanol leaks or spills:

- The absorbent material used should be resistant to alcohol.
- ♦ Initiate proper air monitoring equipment (i.e., Combustible Gas Indicator (CGI) and Flame Ionizing Detector (FID) or MultiRAE Plus Five-Gas Air Monitoring Instrument; Photo Ionizing Detector (PID). Must review response factors prior to using PID, and establish hot, warm and cold zones.
- ◆ Absorb or cover with dry earth, sand or other non-combustible material and transfer to containers.
- Use clean non-sparking tools to collect absorbed material.
- ◆ Take necessary firefighting response actions ensuring minimal PPE is worn.

3.c.3...... CONTAINMENT AND DRAINAGE PLANNING

Drainage from the aboveground diked storage area is pumped out over the concrete dike walls in accordance with NYFD requirements. Air pumps (200 gpm capacity) equipped with hard pipe suction and discharge are pumped to the rack separator then to the final separator prior to discharge through Outfall 001.

The final separator is a "French weir type" that utilizes flow-through processing before discharging to Outfall 001. The separator is equipped with a mechanical shut-off valve inside the separator between the oil compartment and the water/oil mixture section that will be closed when the oil compartment is full. This valve prevents flow through until the oil is pumped out of the separator.

The pipeline manifold/receiving and barge unloading area drainage evaporates or percolates into the ground except for the barge hose catch pan that is piped to Tank 48.

The discharge from the paved yard area catch basins, the own consumption fuel area, T/T parking area, warehouse loading platform, garage drains (excluding wash bay), truck pump off arm, and pump out from the VRU goes to the final separator and discharge Outfall 001.

Drainage from the employee parking lot and the drainage from the wash bay drain in the garage is to the City sanitary sewer. Stormwater drainage from other areas of the Facility is not controlled as it is either non-point sources and/or originate off non-spill potential areas.

3.c.4..... RECOVERY

The response contractor will use vac trucks and explosion-proof pumps to recover the spilled material. The Facility storage tanks can be used to store recovered product provided there is adequate ullage. Otherwise, contractors will use temporary storage containers to transport and store recovered material. This subject is covered in further detail in Annex 3.d.5.

3.c.5...... DECONTAMINATION AND MEDICAL TREATMENT

In the event of a response at the Facility, contractors will be used to handle decontamination of equipment and personnel. However, if the normal work clothing of Facility personnel becomes contaminated at the onset of a release, the contaminated personnel should:

- Remove the contaminated clothing immediately.
- Shower with soap and water as soon as possible.
- ◆ See a physician as soon as possible, and be sure to provide Material Safety Data Sheets (MSDSs) to anyone treating the affected persons.

All emergency responders exiting the contaminated area must go through a decontamination station in accordance with incident management procedures.

Emergency responders will not take any personal protective equipment (PPE) or other equipment from the site until it has been properly decontaminated. If the equipment cannot be decontaminated, it must stay on site.

The local fire and police departments will coordinate with the local emergency medical service (EMS) to provide emergency medical treatment and transportation.

3.c.6.....SALVAGE

Salvage operations for aboveground tanks will be conducted by qualified contractors hired by Motiva Enterprises LLC. No salvage operations will be conducted if unsafe conditions exist.

ANNEX 3d...ICS-PLANNING

3.d.1 INTIAL TACTICAL DEPLOYMENT STRATEGY

TACTICAL DEPLOYMENT

The release into adjacent waterways could potentially be devastating to both the environment and human interests. The NY/NJ ACP has identified for the region exceptional points of interest, recommended boom strategy and deployment locations. The following locations are deemed **PRIORITY** in the booming strategy:

- 1. If tide is heading **North East**, use NY/NJ ACP ESM Maps #4 and #3, in that order.
 - a. Map #4 Booming Priority

SENSITIVE AREA MAP #4					
CODE	SENSITIVE AREA NAME				
B80	RIVERWALK COVE				
M36	SOUTH ST SEAPORT				
M37	SKYPORT INC MARINA				
P1	*CON-EDISION*				
P2	*BROOKLYN UNION GAS*				
R6	WALLABOUT BAY (BROOKLYN NAVY YARD)				
R91	NEWTOWN CREEK				
W1	AMSTAR CORP 2 ND AND KENT ST 15'				
W4	CON-EDISON EAST RIVER 25'				
W5	CON-EDISON HUDSON AVE 20'				
W7	CON-EDISON WATERSIDE 20'				
W17	UNITED NATIONS 9'				

b. Map #3 Booming Priority

	SENSITIVE AREA MAP #3				
CODE	SENSITIVE AREA NAME				
A62	*NORTH BROTHER ISLAND*				
A68	*SOUTH BROTHER ISLAND*				
B76	OAK POINT RAIL SITE				
B79	HALLETS COVE				
C45	BRONX RIVER				
R11	WARDS ISLAND PSYCH HOSPITAL				
W2	CON-EDISON ASTORIA 48'				
W6	CON-EDISON RAVENWOOD 20'				
W9	CON-EDISON 74 TH ST 20'				
W11	PASNY ASTORIA STATION 20'				
W34	CON-EDISON 60 TH ST 8'				

- 2. If tide is heading **South West**, use NY/NJ ACP ESM Maps #4 and #7, in that order
 - a. Map #4 Booming Priority

SENSITIVE AREA MAP #4				
CODE	SENSITIVE AREA NAME			
B80	RIVERWALK COVE			
M36	SOUTH ST SEAPORT			
M37	SKYPORT INC MARINA			
P1	*CON-EDISION*			
P2	*BROOKLYN UNION GAS*			
R6	WALLABOUT BAY			
	(BROOKLYN NAVY YARD)			
R91	NEWTOWN CREEK			
W1	AMSTAR CORP 2 ND AND KENT ST 15'			
W4	CON-EDISON EAST RIVER 25'			
W5	CON-EDISON HUDSON AVE 20'			
W7	CON-EDISON WATERSIDE 20'			
W17	UNITED NATIONS 9'			

b. Map #7 Booming Priority

	SENSITIVE AREA MAP #7
CODE	SENSITIVE AREA NAME
A72	LIBERTY STATE PARK
B8	LIBERTY ISLAND
В9	MOTBY
B67	ELLIS ISLAND
M4	NORTH COVE YACHT CLUB
M7	LIBERTY HARBOR MARINA
M8	NEWPORT YACHT CLUB
M16	GOVENORS ISLAND INDUSTRIAL YARD
M36	SOUTH ST SEAPORT
P3	*NYNEX TELEPHONE LINES*
P4	*CON-EDISON*
P5	*CON-EDISON*
P6	*CON-EDISON*
P7	*BUCKEYE PIPELINE CO.*
P8	*BROOKLYN UNION GAS*
P9	*TRANSCONTINENTAL GAS*
R2	AMERADA HESS
R3	ST GEORGE FUEL PIER
R6	WALLABOUT BAY (BROOKLYN NAVY YARD)
R7	ATLANTIC BASIN
R8	ERIE BASIN
R9	CON-EDISON NARROWS
R90	GOWANUS CANAL
R92	OWLS HEAD PARK (CONCERT BLOCKS)
W4	CON-EDISON EAST RIVER
W5	CON-EDISON HUDSON AVE 20'
W10	WORLD TRADE CENTER 10'
W15	ONE NEW YORK PLAZA 9'
W16	OLYMPIA & YORK (BATTERY PARK) 20'

Utilization of the above approved tactical plans and the NY/NJ ACP will quickly allow the guidance of OSROs and cleanup efforts.

There is no permanent boom located at the Brooklyn Dock. The OSROs are under contract to provide the needed supplies in the event of an incident.

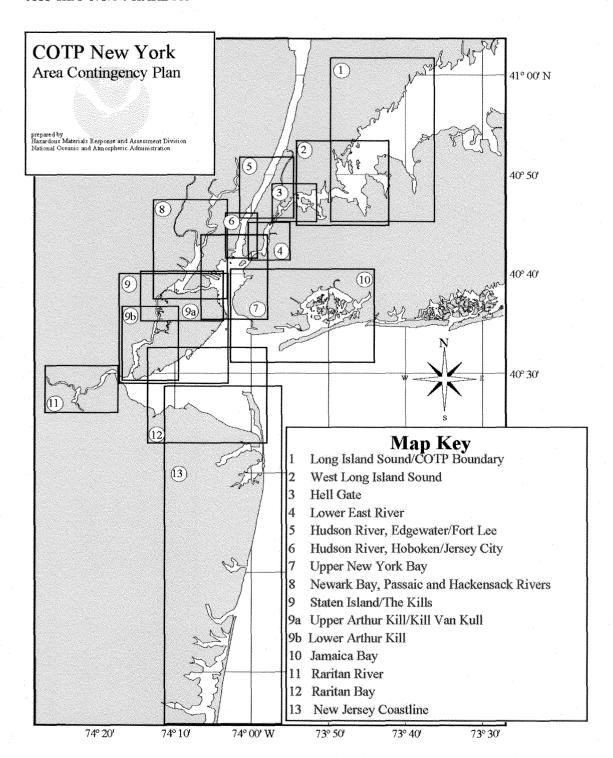
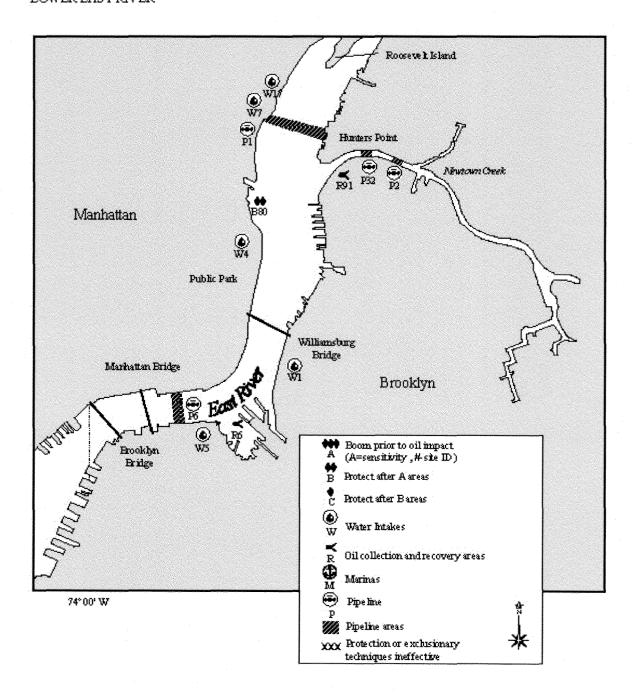
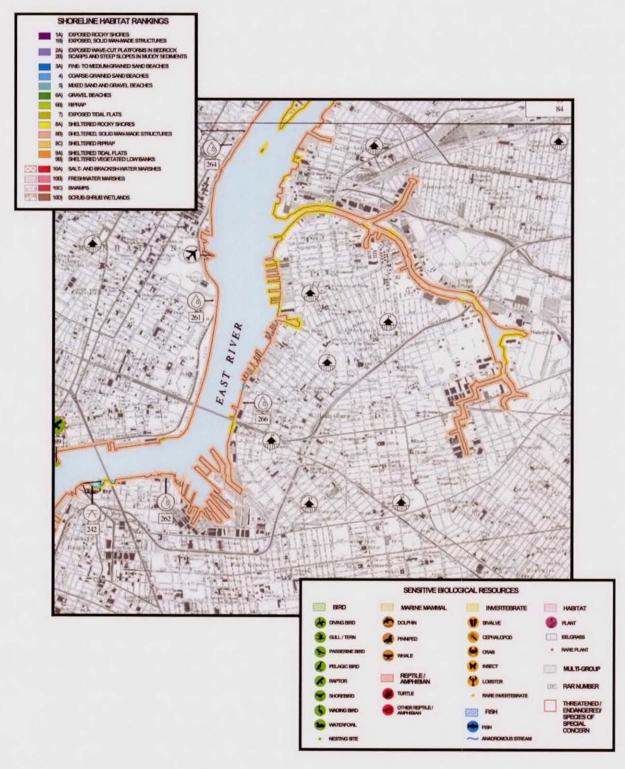


FIGURE 1



E-V-E MAP 4

MAP 4: ENVIRONMENTAL SENSITIVITY INDEX (ESI) LOWER EAST RIVER



STRATEGY MATRIX **REV: 20 NOV 98** LOWER EAST RIVER

SENSITIVE AREA MAP 4 CODE SENSITIVE AREA NAME		BOOM METHOD/ MIN BOOM LENGTH IN FT		STAGING SITE MAP CODE PHONE NUMBER		ACT/ ESS
B80	RIVERWALK COVE	P			E/\$	B/V
M36	SOUTH ST SEAPORT	P/D	3000	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	\$	B/V
M37	SKYPORT INC MARINA	P/D	300	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	\$	B/V
Pl	*CON-EDISION*	*	*	ELECTRICAL LINES 212-580-6763	\$	В
P2	*BROOKLYN UNION GAS*	*	*	24" GAS LINE 718-403-2921	\$	В
R6	WALLABOUT BAY (BROOKLYN NAVY YARD)	R	1500	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	Е	B/V
R91	NEWTOWN CREEK	P/R	1500	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	Е	B/V
W1	AMSTAR CORP 2 ND AND KENT ST 15'	P/D	1300	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441 N.Y.C. MARINE FIRE DEPT. 718-494-4269	\$	B/V
W4	CON-EDISON EAST RIVER 25'	P/D	1300	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441 N.Y.C. MARINE FIRE DEPT. 718-494-4269	E/\$	В
W5	CON-EDISON HUDSON AVE 20'	P/D	1300	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	E/\$	В
W7	CON-EDISON WATERSIDE 20'	P/D	1300	SKYPORT INC MARINA (M37) 212-686-4548	E/\$	В
W17	UNITED NATIONS 9'	P/D	1700		E/\$	B/V

NOTES: WATER INTAKE SIZES ARE LISTED AFTER SENSITIVE AREA NAME

BOOMING METHOD D = DEFLECT

P = PROTECT

R = RECOVER

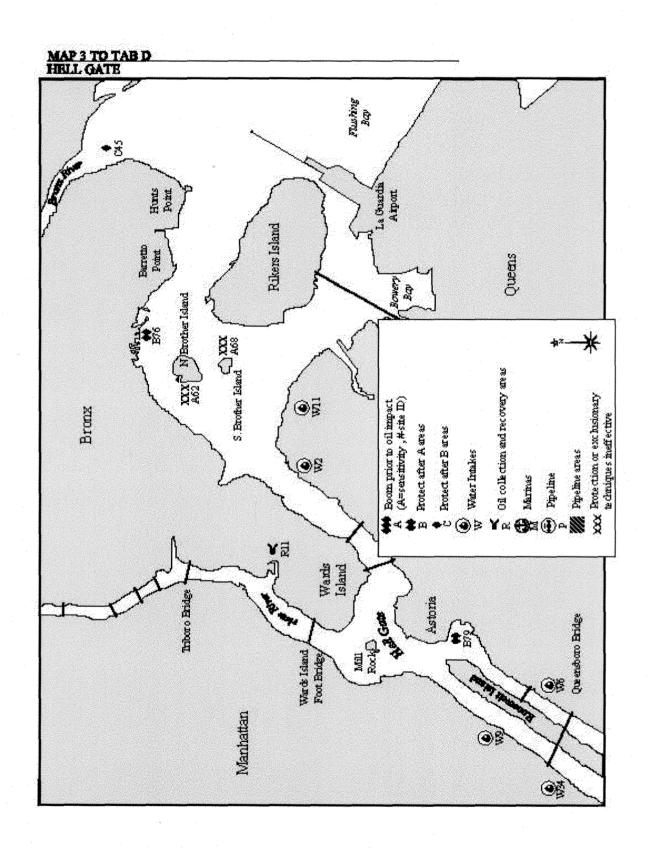
IMPACT

E = ENVIRONMENTAL

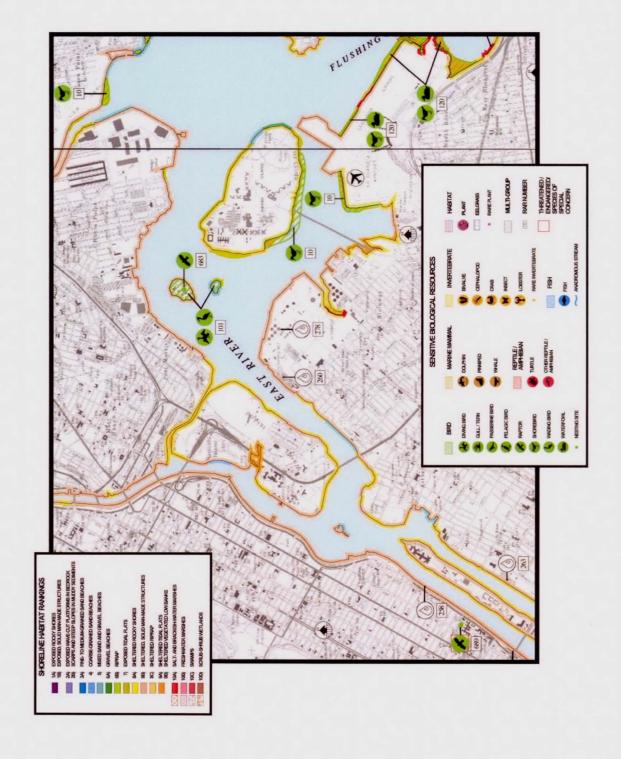
\$ = ECONOMIC

ACCESS

B = BOAT V = VEHICLE



E-V-D MAP 3



STRATEGY MATRIX REV: 20 NOV 98 HELL'S GATE

SENSITIVE AREA MAP 3 CODE SENSITIVE AREA NAME		BOOM METHOD/ MIN BOOM LENGTH		STAGING SITE MAP CODE PHONE NUMBER		IMPACT/ ACCESS	
CODE		IN FT	(H				
A62	*NORTH BROTHER ISLAND *	P			Е	В	
A68	*SOUTH BROTHER ISLAND *	P			E	В	
B76	OAK POINT RAIL SITE	P/D	500		\$	B/V	
B79	HALLETS COVE	P			E	В	
C45	BRONX RIVER	P	700		Е	В	
R11	WARDS ISLAND PSYCH HOSPITAL	R	1000		Е	B/V	
W2	CON EDISON ASTORIA 48'	P/D	1300		E/\$		
W6	CON-EDISON	P/D	1300	BROOKLYN NAVY YARD DEVELOPMENT	E/\$	В	
	RAVENWOOD 20'	l		CORP 718-852-1441			
W9	CON-EDISON 74 TH ST 20'	P/D	1300		E/\$	B/V	
W11	PASNY ASTORIA STATION 20'	P/D	1300		E/\$	B/V	
W34	CON-EDISON 60 TH ST 8'	P/D	1300	WRIGHT ISLAND MARINA (M17) 914-235-8013	E/\$	B/V	

NOTES: *FOR SENSITIVE AREAS A62 AND A68 DEFLECT OR RECOVER OIL BEFORE IMPACT*
WATER INTAKE SIZES ARE LISTED AFTER SENSITIVE AREA NAME

BOOMING METHOD

D = DEFLECT

P = PROTECT

R = RECOVER

IMPACT

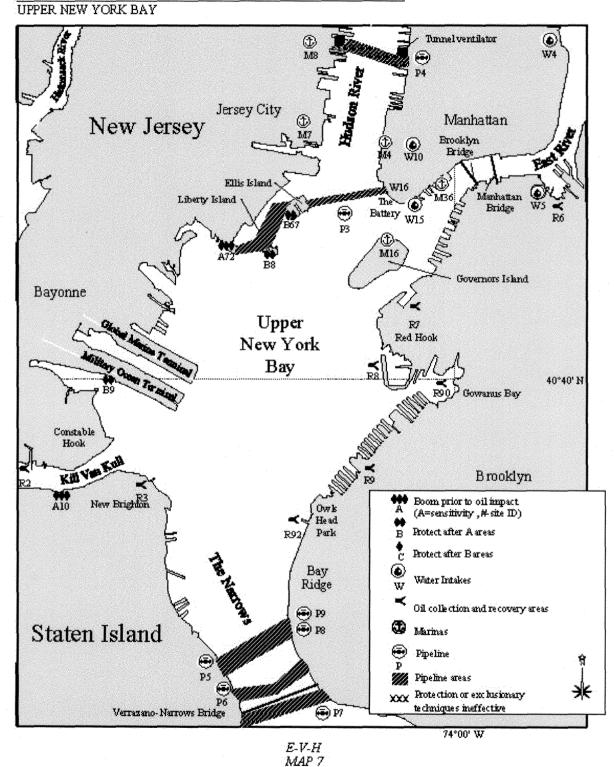
E = ENVIRONMENTAL

\$ = ECONOMIC

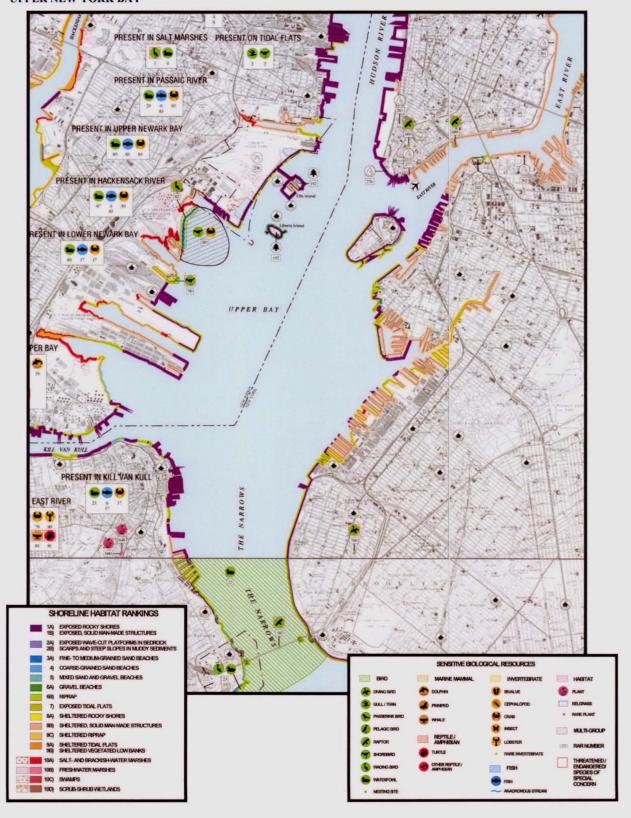
ACCESS

B = BOAT

V = VEHICLE



UPPER NEW YORK BAY



STRATEGY MATRIX **REV: 20 NOV 98** UPPER NEW YORK BAY

SENSITIVE AREA MAP 7		BOOM METHOD/ MIN BOOM		STAGING SITE MAP CODE PHONE NUMBER		IMPACT/ ACCESS	
CODE	ODE SENSITIVE AREA NAME LENGTH IN FT						
A72	LIBERTY STATE PARK	P/D	3500	LIBERTY STATE PARK (A72) 718-243-0199	E/\$	B/V	
B8	LIBERTY ISLAND	P/D	4500	LIBERTY HARBOR MARINA (M45) 201-451-1000 (908-221-1938 NIGHT)	E/\$	В	
B9	MOTBY	P/D/R	5000	MOTBY (B9) 201-451-1000 (908-221-1938 NIGHT)	E/\$	B/V	
B67	ELLIS ISLAND	P/D/R	6000	LIBERTY HARBOR MARINA (M45) 201-451-1000 (908-221-1938 NIGHT)	E/\$	В	
M4	NORTH COVE YACHT CLUB	P	500	NORTH COVE YACHT CLUB (M4) 212-938-9000	\$	B/V	
M7	LIBERTY HARBOR MARINA	P/D	300		\$	B/V	
M8	NEWPORT YACHT CLUB	P/D	300	NEWPORT YACHT CLUB (M8) 201-626-5550 (718-885-0617 NIGHT)	\$	B/V	
M16	GOVENORS ISLAND INDUSTRIAL YARD	P/R	700	GOVENORS ISLAND INDUSTRIAL YARD (M16) 212-668-7936	\$	B./V	
M36	SOUTH ST SEAPORT	P/D	3000	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	\$	B/V	
P3	*NYNEX TELEPHONE LINES*	*	*	TELEPHONE LINES	\$	В	
P4	*CON-EDISON*	*	*	ELECTRIC POWER LINES 212-580-6763	\$	В	
P5	*CON EDISON*	*	*	OIL STATIC LINE 212-580-6763	\$	В	
P6	*CON EDISON*	*	*	THREE 24" GAS/ELECTRIC LINES 212-580-6763	\$	В	
P7	*BUCKEYE PIPELINE CO*.	*	*	10" GAS LINE 718-656-5746	\$	В	
P8	*BROOKLYN UNION GAS*	*	*	TWO 24" GAS LINES 718-403-2921	\$	В	
P9	*TRANSCONTINENTAL GAS*	*	*	24" NATURAL GAS LINE 908-862-8600	\$	В	
R2	AMERADA HESS	R	900		\$	B/V	
R3	ST GEORGE FUEL PIER	R	1000		\$	В	
R6	WALLABOUT BAY (BROOKLYN NAVY YARD)	R	1500	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	E/\$	B/V	
R7	ATLANTIC BASIN	R	1500		Е	В	
R8	ERIE BASIN	R	300	RED HOOK MARINE TERMINAL 718-875-0777	E	В	
R9	CON-EDISON NARROWS	R			\$	В	
R90	GOWANUS CANAL	P/R	1800	RED HOOK MARINE TERMINAL 718-875-0777	E	В	
R92	OWLS HEAD PARK (CONCERT BLOCKS)	P/R	1000	PIER 69 BROOKLYN	Е	B./V	
W4	CON-EDISION EAST RIVER	P/D	1300	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441	\$	B/V	
W5	CON-EDISON HUDSON AVE 20'	P/D	1300	BROOKLYN NAVY YARD DEVELOPMENT CORP 718-852-1441 N.Y.C. MARINE FIRE DEPT. 718-494-4269	\$	В	
W10	WORLD TRADE CENTER 10'	P/D	1300	LIBERTY HARBOR MARINA (M45) 201-451-1000 (908-221-1938 NIGHT)	\$	В	
W15	ONE NEW YORK PLAZA 9'	P/D	1300	LIBERTY HARBOR MARINA (M45) 201-451-1000 (908-221-1938 NIGHT)	\$		
W16	OLYMPIA & YORK (BATTERY PARK) 20'	P/D	1300	USCG LICENSING AND EXAMS BRANCH 212-668-4970	\$	В	

NOTES: WATER INTAKE SIZES ARE LISTED AFTER SENSITIVE AREA NAME DO NOT ANCHOR AROUND PIPELINE AREAS

BOOMING METHOD

D = DEFLECT P = PROTECT

R = RECOVER

IMPACT

1 1

E = ENVIRONMENTAL

\$ = ECONOMIC

ACCESS

B = BOAT V = VEHICLE

3.d.2......VULNERABILITY ANALYSIS

EFFECTS ON HUMAN HEALTH AND PUBLIC WELFARE

A release of petroleum products in substantial quantity to the environment from the Motiva Terminal in Brooklyn, NY could pose a threat to human health and public welfare.

The immediate vicinity of the spill site should be evacuated to reduce risk of injury from either overexposure or fire and explosion.

A spill from the largest tank would be a non-persistent oil (Group 1). For non persistent oil discharged into tidal waters, the planning distance is 5 miles from the Facility down current ebb tide and to the point of maximum tidal influence or 5 miles, whichever is less, during flood tide. Any release from the piping at the dock has the potential to directly impact Newtown Creek. Site overflow drainage would most likely gently flow east on the Facility's property. Drainage from the employee parking lot and the wash bay drain in the garage is to the City Sanitary and Sewer System.

Actions to contain a spill affecting Newtown Creek and the East River and to prevent exposure to populated areas should include protection of marinas, local industry and other properties on the waterfront where the public may be at risk.

3.d.2.1 Water Intakes

The Facility is located approximately one-half mile to the east of the East River. In the event of a discharge with impact to the river, there are various industrial downstream water intakes that may be potentially impacted. Upon determining that a spill could reach an industrial intake, the Facility should be contacted and boom should be used to protect the intake.

Water Intake	Distance from Facility
Con Edison – Waterside Plant	1.25 mile NW (approximate)
Con Edison – 14 th Street Plant	1.50 mile SW (approximate)
Con Edison – Hudson Ave. Plant	4.00 mile SW (approximate)
Con Edison – Ravenswood Plant	2.25 mile NE (approximate)
Con Edison – 74 th St. Plant	3.00 mile NE (approximate)
Con Edison – Astoria Plant	6.50 mile NE (approximate)
Con Edison – Hell Gate Plant	6.50 mile NE (approximate)

3.d.2.2 Schools

Miscellaneous primary and secondary schools are located within the city limits. The schools are situated in all directions from the Facility. Those in the immediate vicinity include:

School Name	Distance from Facility
St. Theresa's School	1.00 mile NE (approximate)
Public School	1.00 mile NE (approximate)
Queens Vocational High School	1.00 mile NE (approximate)
Aviation High School	1.00 mile NE (approximate)

Any evacuation efforts for these schools will be coordinated with the local emergency assistance agencies (police department, fire department, etc.). Additional detail on the schools within the area of the Facility is included on the maps in Figure 1.1.

3.d.2.3 Medical Facilities

Medical Facility	Distance from Facility
St. John's Hospital	0.75 miles N (approximate)
Greenpoint Hospital	1.10 miles S (approximate)
VA Hospital	1.60 miles W (approximate)

Any evacuation efforts for these schools will be coordinated with the local emergency assistance agencies (police department, fire department, etc.). Additional detail on the medical facilities within the area of the Facility is included on the maps in Figure 1.1.

3.d.2.4 Residential Areas

Residential population begins within a quarter-mile of the Facility and continues outward in all directions. The coverage area of these residential areas is not continuous; rather it is broken up by commercial areas.

Any evacuation efforts for these areas will be coordinated with the local emergency assistance agencies (police department, fire department, etc.). Additional detail on the residential areas within the area of the Facility is included on the maps in Figure 1.1.

3.d.2.5 Businesses

The immediate area surrounding the Facility is for the most part commercialized. The listing of businesses in the area is extensive and not included here for update purposes.

Any evacuation efforts for these areas will be coordinated with the local emergency assistance agencies (police department, fire department, etc.). Additional detail on the general layout of businesses within the area of the Facility is included on the maps in Figure 1.1.

3.d.2.6 Fish and Wildlife, Wetlands, and other Sensitive Environments

The shoreline and general environment in the area of the Facility is highly commercialized. The wildlife population is limited.

Flora and fauna are always present and are sensitive to the effects of a pollution incident. All environmental areas deserve protection from pollution, but they must be prioritized during a response so as to protect the most sensitive and susceptible areas to pollution.

Marsh and wetland habitats exist in the area of the Facility and are identified on the maps in Annex 1. The size and diversity of the wetland environments vary with season and year.

During a response situation, the USFWS and applicable state agencies should be contacted for information regarding wetlands and other sensitive environments. Upon contact, the agencies will be able to:

- Identify and establish priorities for fish and wildlife, wetlands, and other sensitive environments requiring protection from any direct or indirect effects from a discharge.
- Identify potential environmental effects on fish and wildlife, wetlands, and other sensitive environments resulting from removal actions or countermeasures.

3.d.2.7 Lakes and Streams

Newtown Creek and the East River could be impacted. Other lakes, streams, and rivers that may be potentially impacted by a discharge originating at the Facility are identified on the maps in Annex 1.

3.d.2.8 Endangered Flora and Fauna

The endangered flora and fauna that may be potentially impacted by a discharge originating at the Facility are listed below.

These species for Kings County, New York include:

Species		Status
Amaranth, Seabeach	·	Endangered
Bat, Indiana		Endangered

These species for the State of New York include:

Species	Status
Indiana Bat	Endangered
Karner Blue Butterfly	Endangered
Bald Eagle	Threatened
American Peregrine Falcon	Endangered
Piping Plover	Endangered & Threatened
Chittenango Ovate Amber Snail	Threatened
Roseate Tern	Endangered
Bog Turtle	Threatened
Dwarf Wedgemussel	Endangered

3.d.2.9 Recreational Areas

The recreational areas most likely to be potentially impacted by a discharge originating at the Facility include:

Recreational Area	Distance from Facility
St. Gabriels Park	1.50 mile NW (approximate)
Murphy Park	1.50 mile W (approximate)
East River Park	1.75 mile W (approximate)
Queensbridge Park	2.00 mile NE (approximate)
Rainey Park	3.00 mile NE (approximate)
Shulz Park	4.00 mile NE (approximate)
Unnamed Park	4.00 mile NE (approximate)
Lighthouse Park	5.00 mile NE (approximate)
Wards Island Park	5.50 mile NE (approximate)
Astoria Park	5.50 mile NE (approximate)
Jefferson Park	6.00 mile NE (approximate)
Battery Park	6.50 mile SW (approximate)
Liberty State Park	7.50 mile SW (approximate)
Éllis Island	7.50 mile SW (approximate)

1

Any evacuation efforts for these areas will be coordinated with the local emergency assistance agencies (police department, fire department, etc.). The media could also be used to issue public warnings if appropriate.

3.d.3......ANALYSIS OF THE POTENTIAL FOR A SPILL

The potential for a significant spill at the Facility is minimal due to the spill prevention measures that are in place and the operating procedures followed by Facility personnel. The potential for a spill of sufficient magnitude to escape the Facility is very remote due to the spill mitigation measures inherent in the Facility design. To date, there have been no reportable spills at this Facility.

All of the containment areas have sumps that route rainwater and spills should they occur to the separator system on the east side of the Facility. Furthermore, all the containment areas are adequately sized to contain the volume of the largest tanks in each of the areas. Storage tank details, including age, are provided in Annex 7.

Spill prevention measures include a number of discharge detection methods and various inspection procedures described further in Annex 7.

Facility operating procedures are defined in the Plant Procedures Manual. All personnel responsible for Facility operations are qualified. New personnel receive on-the-job training working with experienced operating personnel as well as training in the areas of safety, spill prevention, emergency response, and applicable pollution prevention laws, rules and regulations. They become qualified prior to assuming unsupervised operating responsibilities. The Facility is under continuous operation and is always attended by responsible operators.

Spill mitigation measures include Facility designs intended to direct releases to containment areas where they can be promptly controlled and cleaned up.

In the event that a spill does escape the Facility across and off the boundary lines not adjacent to Newtown Creek (south or west sides), the spill would travel along Paidge Avenue or McGinniss until it reaches a stormwater drain which would act as a conduit to the creek.

The New York City area is not subject to excessive damage from inclement weather such as tornadoes, hurricanes, floods, or tropical storms. The area is subject to snowstorms during the winter months but none have resulted in reportable spills. To date, no reportable spills have occurred at the Facility.

3.d.4......RESOURCES REQUIRED FOR SPILL RESPONSE

Resources required for spill response are based on the following calculations of planning volumes.

Non-Marine Transportation Related Portion of the Facility - EPA Final Rule

Worst-Case Discharge

For a Facility adjacent to navigable waters, 100% of the capacity of the largest single aboveground storage tank within a secondary containment area. (100% of 10,714 bbls = 10,714 bbls).

WCD = 10,714 bbls

The Facility shall identify sufficient response resources, by contract or other approved means, to respond to a worst-case discharge to the maximum extent practicable. The response resources shall, as appropriate, include:

- Oil recovery devices with an effective daily recovery capacity equal to the lesser of 50% of the WCD or the response caps. If the daily recovery rate exceeds the applicable contracting caps (seeTable) then the Facility must identify additional resources equal to twice the cap or the amount necessary to reach the calculated planning volume.
- Temporary storage capacity equal to twice the daily recovery capacity.
- At least 20% of the on-water response equipment should be capable of operating in water of 6 feet or less depth.
- Containment boom for oil collection and containment and for protection of areas of environmental sensitivity or economic importance.
- Identify resources capable of responding to a shoreline clean-up opeation involving the calculated volume of oil and emulsified oil that might impact the affected shoreline.
- Response resources with fire fighting capabilities and an individual assigned to work with the Fire Department.

Remediation and cleanup equipment is available from the cleanup contractors. Storage and recovery for oils for a worst-case spill is also available within the Facility. The cleanup may be enhanced by use of special detergent compounds or bio-enhancement compounds.

Contaminated soils will be removed from the surface of the ground and from the banks of waterways and will be thermally processed to remove contamination.

Medium Discharge

The lesser of 36,000 gallons or 10% of the capacity of the largest aboveground storage tank. (10,714 * 10% = 1,071: 36,000/42 = 857 bbls)

MD = 857 bbls

- Oil recovery devices with an effective daily recovery capacity equal to 50% of the Medium/Maximun Most Probable Discharge volume must be capable of arriving on scene within 12 hours.
- Sufficient quantity of containment boom must arrive within 12 hours for oil collection and containment and for protection of fish and wildlife and sensitive environments, as appropriate.
- Temporary storage capacity equal to twice the daily recovery capacity must be available.

Remediation equipment is available from the OSROs. In the event of a spill, at least one of the OSROs would respond within one hour. The anticipated response would include trenching and drilling to collect contaminated groundwater. Also, sorbents and vac trucks would be utilized to recover spilled product on the ground.

Small Discharge

A volume less than or equal to 2,100 gallons (2100/42 = 50 bbls)

SD = 50 bbls

The Facility shall identify sufficient resources, by contract or other approved means, to respond to a small discharge. The response resources shall, as appropriate, include:

- 1,000" of containment boom and a means of deploying it within one (1) hour of the discovery of a spill.
- Oil recovery devices with an effective daily recovery capacity equal to the amount of oil discharged in a Small Discharge or greater which is available at the Facility within two (2) hours of the detection of an oil discharge.

1

 Oil storage capacity for recovered oily material equivalent to twice the effective daily recovery rate.

Remediation equipment is available from the OSROs. In the event of a spill, at least one of the OSROs would respond within one hour. A small discharge at the loading rack would probably not warrant involvement from OSROs since the spill would be automatically routed to the Facility drainage system.

Planning Volume

Refer to the worksheet at the end of Annex 8 showing calculations used to determine the planning volume and on-water recovery capacity. The worksheet gives Tier 1 (6 hours), Tier 2 (30 hours) and Tier 3 (54 hours) recovery capacities.

To achieve a recovery capacity for <u>Tier 1</u> of 321 bbls/day, one weir type skimmer would be required. The nameplate capacity of this skimmer is 285 bbls/hr which equates to 1,368 bbls/day effective daily recovery. To sustain continuous operations, two vac trucks along with the necessary boom should also arrive on site with in 6 hours.

The <u>Tier 2</u> recovery requirement is 536 bbls/bay. This is met with the single skimmer deployed in response to the Tier 1 requirement.

The <u>Tier 3</u> recovery requirement is 857 bbls/day. This is met with the single skimmer deployed in response to the Tier 1 requirements. These numbers are to be used for planning response resources.

The above equipment and resources would be supplied by local contractors, co-ops (if any), and the MSRC.

3.d.5SPECIFIC SPILL SCENARIOS

3.d.5.1 Factors Affecting Spill Response for Small and Medium Discharge Scenarios

3.d.5.1.1. Size of Spills

Consideration of the resources planned for spill response is based on the evaluation of a release of 857 Bbls of gasoline to the Newtown Creek. A small **discharge** of 50 bbls, or less will require a similar response for containment but would not require as much recovery and cleanup resources as the 857 bbl spill event. The evaluation of the resources required for an 857 bbl spill event is detailed below.

3.d.5.1.2... Proximity to Downgradient Wells, Waterways, and Drinking Water Intakes

No drinking water intakes or water wells are located within the vicinity of the Facility.

3.d.5.1.3... Proximity to Fish and Wildlife and Sensitive Environments

There are several sensitive environments and receptors in the immediate area of the Facility (See Figures 1.1 and 1.4). Contamination of sensitive environments is highly unlikely since the capacity of the loading rack sump is designed to contain the capacity of any tank truck that uses the rack.

3.d.5.1.4... Likelihood that Spill Will Travel Offsite

In the event that a spill occurred at the rack, it would immediately be routed to an oil/water separator. If containment was breached, overflow drainage would most likely gently flow east on the Facility's property. Drainage from the employee parking lot and the wash bay drain in the garage is to the City Sanitary & Sewer System. Any release from the piping at the dock has the potential to directly impact Newtown Creek.

3.d.5.1.5 ... Location of Material Spilled (Receiving Surface)

Spills in the truck loading rack area could land on the concrete truck loading rack pad. Small discharges in the diked areas of the Facility could land on the gravel/clay dike basins.

3.d.5.1.6 ... Material Discharged

The materials that could be discharged in the event of a spill include any of the materials in the Facility. These materials include fuel oil, gasoline, diesel and additives. The most likely materials that could be discharged is gasoline because it is handled in the greatest volumes.

3.d.5.1.7 ... Weather and Aquatic Conditions

The Brooklyn Terminal is on the coast of New York. Seasonal impediments to cleanup may include occasional winds, hurricanes, and seasonally high rainfall. It is not likely that response actions for a small/medium discharge would be influenced by adverse weather conditions since the loading rack is covered.

3.d.5.1.8 ... Availability of Remediation Equipment

For calculation purposes, 80% of the spilled oil would be lost to the environment due to evaporation, dissolution and natural dispersion in the water, 10 % of the spilled oil would reach shoreline features through movement of the oil on the water, and 20% of the spilled oil would be required to be recovered on the water.

Where possible, skimming locations would operate on a 12 to 24 hours per day basis. For the calculation of oil recovered, only 20% of the rated capacity of the skimmer will be used to allow for inefficiencies in encountering oil at the skimmer, manpower effectiveness, etc.

Equipment and resources would be supplied by local contractors, co-ops (if any), and the MSRC based on conditions during an actual spill response.

3.d.5.1.9 ... Probability of Chain Reaction Failures

There is little or no probability that chain reaction failures could occur. The sump is large enough to contain the entire volume of the largest tanker truck compartment. However, special precautions would have to be taken to avoid accidental sparks from igniting the spilled product.

3.d.5.1.10. Direction of Spill Pathway

The path of the spill is discussed in the Vulnerability Analysis in Annex 3.d.1. A goal to complete top priority boom sites in the first twelve (12) hours requires the following, both for this particular event and according to the evaluation of the sensitive areas prior to the spill. It is assumed that for a spill of this nature that a request would be made to close the River to general traffic and that it may be approved by the USCG.

3.d.5.2 Factors Affecting Spill Response For Worst-Case Discharge Scenario

Consideration of the resources planned for spill response is based on the earlier evaluation showing a worst-case discharge of 10,714 bbls of gasoline to Newtown Creek. The recovery operations would start by following the above scenario. The evaluation of response resources for the worst-case discharge is discussed above under planning volumes.

3.d.5.2.1 ... Size of Spills

The factors that affect spill response are relatively dependent of the size of a spill. The generation of a worst-case spill at the Facility would shut down the Facility for the duration of the spill event or until it has been determined that there is no danger from fire and explosion.

3.d.5.2.2 ... Proximity to Downgradient Wells

There are no wellhead protection areas in the immediate area of the Facility. Most local residences are believed to be on municipal water.

3.d.5.2.3 ... Proximity to Fish and Wildlife and Sensitive Environments

Sensitive Environments are identified in the maps in Annex 1.

3.d.5.2.4 ... Likelihood that Spill Will Travel Offsite

In the event of a worst-case spill involving the aboveground storage tanks, the spill should be contained inside the dike walls.

3.d.5.2.5 ... Location of Material Spilled (Receiving Surface)

In the event of a worst-case spill, the spill will contaminate the surface of the ground and will run on to concrete and paved surfaces in the area as well as into the soils.

3.d.5.2.6 ... Material Discharged

For the worst-case spill, the material probably will be a non-persistent gasoline. Contamination of the shorelines will be anticipated. Provisions for staging several areas for contaminated soil to be placed will be designated by the QI. Motiva will evaluate all available resources with the Federal On-Scene Commander in the unified command and employ those resources deemed necessary. The Motiva Eastern Regional Response Team will be notified and will be available to provide supplemental resources.

3.d.5.2.7 ... Weather and Aquatic Conditions

Weather and aquatic conditions will be considered regarding the cleanup efforts for the worst-case spill.

3.d.5.2.8 ... Availability of Remediation Equipment

Remediation and cleanup equipment is available from the cleanup contractors. Storage and recovery for oils for a worst-case spill is also available within the Facility. The cleanup may be enhanced by use of special detergent compounds or bio-enhancement compounds. Contaminated soils will be removed from the surface of the ground and from the banks of the rivers and will be thermally processed to remove contamination. The extent of petroleum contamination will be determined by using a photoionization detection meter and by visual inspection.

3.d.5.2.9 ... Probability of Chain Reaction Failures

The probability of a chain reaction failure is considered slight to non-existent. The tanks are not manifolded together.

3.d.5.2.10. Direction of Spill Pathway

This is discussed in Annex 3.d.1. Any release from the piping at the dock has the potential to directly impact Newtown Creek. Site overflow drainage would most likely gently flow east on the Facility's property. Drainage from the employee parking lot and the wash bay drain in the garage is to the City Sanitary & Sewer System.

3.d.6 SPILL MOVEMENT ESTIMATES

Immediate action after a spill can minimize potential impact damage since the spill will move with time and result in contamination of a greater area. Oil moves across the surface of the water as a result of wind and current; therefore, it is important to have knowledge of tides, currents, prevailing winds, and other factors which will permit the prediction of how and where a slick will move.

Trajectory Analysis

Oil slicks move as a result of wind and water currents. It is commonly assumed that oil slicks move with the wind at approximately 3 to 4 percent of the wind velocity. When the wind velocity is low or wind is absent, the slick will tend to move with the current at about the same velocity and in the same direction as the current. When the wind is blowing, the slick will be affected by both water and wind forces. If the wind direction is opposite to the current, the wind can reduce or reverse the water velocity at the surface.

Aerial surveillance provides the most effective means of determining spill size and movement. Frequent helicopter and/or fixed wing aircraft overflights may not, however, be possible or available; in which case, spill movement must be calculated using the available data and surface observations.

Tidal Current Charts / Tables

The National Oceanic & Atmospheric Administration (NOAA) in cooperation with the National Ocean Service (NOS) post tidal current predictions on website (http://tidesandcurrents.noaa.gov) for Narrows, New York Harbor. Sensitivity should be given to the fact that these charts are estimates and will vary. Currents will also fluctuate due to rainfall in the area.

3.d.7 DISPOSAL PLANS/HAZARDOUS WASTE

For proper disposal of waste, please contact your Field Environmental Representative or your Waste Disposal Coordinator for guidance.

3.d.7.1 General Description of Disposal Plans

The principal items that will be recovered are contaminated soil and contaminated water and oils mixtures. It is not anticipated that the Facility will be able to recover gasoline unless the gasoline stays within the diked areas of the Facility and unless it is of sufficient depth to permit recovery by pumping into a tank or truck trailer.

3.d.7.1.1 ... Recovery of Spilled Materials

All liquids recovered from spills will be assumed to be hazardous wastes, subject to RCRA storage standards. These materials will generally be in the form of recovered liquids pumped from the oil-water separators, slop tanks, or from skimmers. These materials will be handled by various recovery and disposal contractors and will be manifested to licensed hazardous wastes treatment storage and disposal facilities (TSDF) for disposal.

3.d.7.1.2 ... Disposal of Spill Contaminated Materials

All solid cleanup materials that have been in contact with gasoline, diesel fuels, or other products will be placed into a 55-gallon drum or other suitable metal container and appropriately labeled as hazardous wastes until the materials have been analyzed.

If the analysis indicates that the wastes are non-hazardous, the hazardous waste labels will be removed.

If the material is determined by analysis to be hazardous waste, the container of spill-contaminated solids will be manifested as either a D001 (flammable hazardous waste) or as a D018 (hazardous waste containing benzene), depending upon the amount of flammable material in the cleanup materials. These materials will be manifested, stored and disposed of as hazardous wastes.

All soils contaminated with oils and gasolines will be handled and stored in accordance with State of New York regulations for petroleum-contaminated soils.

All individuals responsible for generating any spill control materials shall contact the Environmental Supervisor at the Facility, the Terminal Superintendent, or the Complex Manager for instructions on the placement, labeling, and manifesting for each drum.

3.d.7.1.3 ... Disposal of Contaminated Soils

Contaminated soils will be collected and stored for treatment. Motiva has national contracts with companies that dispose of petroleum-contaminated materials. Contaminated soils will be excavated and moved to a staging area for further evaluation. After determination of the best type of decontamination, the soils will be sent to a soil recycling company for disposal by incineration, thermal processing, or by composting, depending upon state regulations.

3.d.7.1.4 ... Disposal of Contaminated Equipment and Materials

In the event of a petroleum spill, some of the cleanup equipment will be contaminated with gasoline or diesel fuel. Both can be removed from most equipment, except porous surfaces such as wood, by washing with detergent, soap, and water. Most contaminated equipment will be moved to a spill recovery staging area at a location selected by the OSC and washed. The wash waters and rinse waters will be collected for treatment and/or disposal.

3.d.7.1.5 ... Disposal of Contaminated Personal Protective Equipment

Personal protective equipment that may be used on this project may include splash suits and disposable Tyvek[®] suits. If these materials become contaminated and cannot be cleaned up by washing, they will be drummed and sent off for incineration disposal to one of the approved disposal sites.

3.d.7.1.6 ... Disposal of Contaminated Decontamination Solutions

Decontamination solutions will be treated in one of several ways. With the approval, the solutions could be sent to the wastewater treatment system for disposal. If not, the wastewaters will be pumped through activated carbon to remove the petroleum products. If the water meets the NPDES permit limits, it will be discharged. Otherwise, alternative disposal arrangements will be made.

3.d.7.1.7 ... Disposal of Contaminated Adsorbents Solutions

It is not envisioned that any adsorbent solutions would be used on a spill at this Facility. If any adsorbent solutions are used, they will be recovered and drummed and disposed of as a D001 or D018 hazardous wastes.

3.d.7.1.8 ... Disposal of Contaminated Spent Chemical Solutions

A number of various types of chemical solutions may be used on this project but the specifics are unknown at this time. The principal use of these chemical solutions would be to remove petroleum from the cleanup and recovery equipment.

If these types of solutions are used, they will drummed, analyzed after collection, and disposed of in accordance with appropriate hazardous or non-hazardous waste regulations.

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3.d.7.2 Manifesting Shipments of Hazardous Wastes

All waste materials from cleanups are assumed to be hazardous wastes unless testing of the materials indicates otherwise. All materials from cleanups will be manifested to a licensed hazardous waste disposal transporter and disposed at a licensed hazardous waste disposal facility.

3.d.7.3 Locations of Companies Accepting Spill Contaminated Materials

Motiva has national contracts for waste disposal with companies that dispose of petroleum in incineration facilities.

3.d.8 COORDINATION WITH NATURAL RESOURCE TRUSTEES

Motiva will conduct bilateral natural resource damage assessments (NRDA) with the state. Motiva Enterprises LLC will provide a qualified contract toxicologist and expert in NRDA investigations (see contractor list in the Core Plan.)

Annex 3e, Page 1

ANNEX 3e... ICS-LOGISTICS

3.e.1...... MEDICAL NEEDS OF RESPONDERS

The contractor will supply a Site Safety and Health Plan before work begins.

Any personnel requiring emergency medical attention will be evacuated immediately from the spill area. Qualified personnel only will give first aid and stabilize individual needing assistance. To provide first-line assistance to field personnel in case of illness or injury, the following items will be made immediately available by contractor:

First-aid Kit

Portable Emergency Eye Wash

Supply of Clean Water

If actual or suspected serious injury occurs, these steps will be followed:

Remove the exposed or injured person from immediate danger.

Render first aid, if necessary; decontaminate affected personnel after critical first aid is given.

Obtain paramedic services or transport by air or ground ambulance to hospital (listed in Core Plan 1.1.2).

3.e.2..... SITE SECURITY

3.e.2.1.... Fencing

The Facility is surrounded by a chain-link fence. The Facility gates are closed at all times except when traffic requires entry or exit. Access is by loading card or access card.

Trucks may be loaded at the truck loading rack 24 hours per day, 7 days per week. Because of this continuous activity, the Facility has implemented a system of security that permits access only to authorized drivers and trucks.

3.e.2.2.... Locked Valves

Valve security at the Facility is maintained in several ways. Inactive valves are chained or locked in the closed position.

Annex 3e, Page 2

3.e.2.2.... Locked Valves (Cont'd)

In the tank farm area, all tank water withdrawal valves are locked and closed when not in use. All basin drain valves, where installed, are closed, chained, and locked when not in use. When the basin drain valves are operated, the water in the basin is inspected by an employee prior to operation of the valve. If a visible sheen or other condition indicating the presence of oil or gasoline is present, the valves are not operated.

3.e.2.3.... Pump Controls

Deliveries from the product storage tanks to trucks are controlled by the Terminal Automation System. The drivers can only gain access to the Facility by inserting a pre-coded card. Once inside the Facility, the driver cannot turn on the product pumps to load the vehicle unless the card is inserted into the loading rack card reader. Only approved drivers are assigned the pre-coded cards.

3.e.2.4.... Capping and Blanking Valves

All loading connections that are not in use are capped, blind flanged, or otherwise secured to prevent an oil leakage.

3.e.2.5.... Facility Lighting

The Facility has security lighting at the loading rack and the storage tank area. These lights provide illumination that is sufficient to detect any acts of vandalism, discharges, or releases. The lights are turned on automatically.

3.e.2.6.... Security Guards - Site Control

Site security and access will be the responsibility of the Complex Manager. During an emergency, access will be limited to those persons who are authorized and have proper training. This responsibility will be delegated to the local law enforcement agency or contract security identified in Core Plan, Section 1.1.2.

3.e.3...... COMMUNICATIONS

The Facility utilizes intrinsically safe UHF radios that meet Class 1 Division 1, Group D requirements. In the event of a response, the Facility radios will be supplemented by the contractor resources based on the circumstances. ICS 205 form will be used to provide all radio frequency assignments as prepared by the Communications Unit Leader and given to the Planning Section Chief. (A copy of the form is provided at the end of the Annex.) In addition, the Terminal Office has landlines and cellular telephones, fax machines, and computers to contact personnel assigned to the incident.

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3.e.4...... TRANSPORTATION

Tank trucks and helicopters are available through the list of contractors provided in the Core Plan, Section 1.1.2.

3.e.5...... PERSONNEL SUPPORT

Meals and housing can be provided by area hotels listed in Core Plan, Section 1.1.6.1.

3.e.6...... EQUIPMENT MAINTENANCE AND SUPPORT

Contractors will be relied upon for equipment maintenance and support.

1. Incident Name		2. Operational l	Period (Date / Time)	INCIDENT RADIO COMMUNICATIONS PLAN ICS 205-CG	
		From:	To:		
3. BASIC RADIO CHANNE			· · · · · · · · · · · · · · · · · · ·	.	
SYSTEM / CACHE	CHANNEL	FUNCTION	FREQUENCY	ASSIGNMENT	REMARKS
		<u> </u>			
					·
	-				
	·				
		•			, , , , , , , , , , , , , , , , , , , ,
. Prepared by: (Communi	cations Unit)			Date / Time	
NCIDENT RADIO CO	MMUNICATIONS	S PLAN		· · · · · · · · · · · · · · · · · · ·	ICS 205-CG (Rev.07/04)

Annex 3f, Page 1

ANNEX 3f ... ICS-FINANCE / PROCUREMENT / ADMINISTRATION

3.f.1...... RESOURCE LIST / RESPONSE EQUIPMENT / SUPPORT EQUIPMENT / CONTRACTING

The Facility maintains only minimal quantities of spill response material in the response trailer. The majority of the spill response materials are available from the contractors. Motiva Enterprises LLC has spill response assistance contracts with the contractors shown in Core Plan, Section 1.1 of this Plan. The Emergency Management, Preparedness, and Response Regional Team can provide procurement and manpower coordinators who will obtain materials, equipment, and manpower from contractors. (See organization chart listed in Annex 3.a) Facility personnel are prohibited from responding to spills as they are only trained to the first responders operations level.

Company personnel who have received first responder operations level training [as outlined by OSHA 29 CFR 1910.120(q)(6)(ii)] may respond for the purpose of protecting nearby persons, property, or the environment from the effects of the release. Their only response will be defensive in nature without actually trying to approach the point of release to stop it. Their function will be to contain the release from a safe distance and keep it from spreading. They will not engage in any activity that would present an actual or potential inhalation hazard from the spilled material that would require the use of respiratory protection.

3.f.2..... PERSONNEL MANAGEMENT

When large numbers of workers are needed, the oil spill contractor will supply skilled and unskilled personnel. They will also supply technical people as needed. The Emergency Management, Preparedness, and Response Regional Team can also assign specific duties for team members to carry out when an oil spill occurs.

3.f.3...... CLAIMS PROCEDURES

The Emergency Management, Preparedness, and Response Regional Team can provide claims personnel who will handle the processing of claims on site. The claims coordinator will contact the local media and publish a toll free 800 number for claimants to call. (See organization chart listed in Annex 3.a).

Annex 3f, Page 2

3.f.4...... COST DOCUMENTATION

The Emergency Management, Preparedness, and Response Regional Team will provide a Comptroller and Auditor to control and document costs. (See organization chart listed in Annex 3.a)

ANNEX 4.... INCIDENT DOCUMENTATION

4.1..... POST-ACCIDENT INVESTIGATION

4.1.1..... Purpose of Follow-Up

A critique following an oil spill response is beneficial to evaluate the actions taken or omitted. Recommendations and modifications to the ICP should be made to prepare for the possibility of another oil spill. Requests for a post incident critique will only be made by a Company attorney. It is recommended that all discussions be attended by a Company attorney who should also review all reports prior to finalization.

4.1.2..... Outline of Post-Spill Critique

Outlined below are items a team composed of outside people knowledgeable in oil spill response and key members of the response teams (including a Company attorney) may wish to examine. These questions are intended as guidelines only; many other questions are likely to be appropriate at each stage of a critique.

4.1.2.1....Detection

- Was the spill detected promptly?
- How was it detected?
- ♦ By whom?
- Could it have been detected earlier? How?
- ◆ Are any instruments or procedures available to consider which might aid in spill detection?

4.1.2.2....Notification

- Were proper procedures followed in notifying government / agencies?
- Were notifications prompt?
- Was management notified promptly?
- Was management response appropriate?
- Was Motiva Enterprises LLC notified promptly?
- ♦ If so, why, how, and who? If not, why not?

4.1.2.3....Assessment / Evaluation

- Was the magnitude of the problem assessed correctly at the start?
- What means were used for this assessment?
- Are any guides or aids needed to assist spill evaluation?
- What sources of information were available on winds and on water currents?
- Is our information adequate?
- Was this information useful (and used) for spill trajectory forecasts?
 Were such forecasts realistic?
- Do we have adequate information on oil properties?
- ◆ Do we need additional information on changes of oil properties with time (i.e., as a result of weathering and other processes)?
- ♦ Could the assessment have been speeded up or should it have been?
- What about mobilization of manpower resources?
- Was the local oil spill cooperative used appropriately?
- How could this be improved?
- ♦ Was it appropriate to mobilize Motiva resources; if so, was the mobilization promptly initiated?
- What other corporate resources are available and have they been identified and used adequately?

4.1.2.4....Response-Strategy

- Is there an adequate spill response plan for the location?
- Is it flexible enough to cope with unexpected spill events?
- ◆ Does the Plan include clear understanding of local environmental sensitivities?
- What was the initial strategy for response to this spill?
- Is this strategy defined in the spill plan?
- ♦ How did the strategy evolve and change during this spill and how were these changes implemented?

- ♦ What caused such changes?
- ♦ Are improvements needed? More training?

4.1.2.5....Responses-Resources Used

- ♦ What resources were mobilized?
- How were they mobilized?
- ♦ How did resource utilization change with time? Why?
- Were resources used effectively?
 - Contractors
 - Government agencies
 - Company resources
 - Cooperatives
 - Volunteers
 - Consultants
 - Other (e.g., bird rescue centers)
- What changes would have been useful?
- Do we have adequate knowledge of resource availability?
- Do we have adequate knowledge of waste disposal capabilities?

4.1.2.6....Response-Effectiveness

- Was containment effective and prompt?
- How could it have been improved?
- Should the location or the local cooperative have additional resources for containment?
- ♦ Was recovery effective and prompt?
- How could it have been improved?
- ◆ Should the location or the local cooperative have additional resources for recovery of spilled oil?
- Was contaminated equipment disposed of promptly and safely?
- ♦ Was there adequate in-house oil separation, recovery, and disposal?

- ♦ How could it have been improved?
- Were adequate outside disposal resources available?

4.1.2.7....Command Structure

- ♦ Who was initially in charge of spill response?
- What sort of organization was initially set up?
- ♦ How did this change with time? Why?
- ♦ What changes would have been useful?
- Was there adequate surveillance?
- Should there be any changes?
- Were communications adequate?
- What improvements are needed (in hardware, procedures, etc.)?
- Was support from financial services adequate? Prompt?
- Should there be any changes?
- ♦ Is more planning needed?
- Should financial procedures be developed to handle such incidents?

4.1.2.8....Measurement

- Was there adequate measurement or estimation of the volume of oil spilled?
- ♦ Was there adequate measurement or estimation of the volume of oil recovered?
- Was there adequate measurement or estimation of the volume of oil disposed of?
- Should better measurement procedures be developed for either phase of operations?
- ♦ If so, what would be appropriate and acceptable?

4.1.2.9....Government Relations

- What are the roles and effects of the various government agencies that were involved?
- ♦ Was there a single focal point among the government agencies for contact?
- ◆ Should there have been better focus of communications to the agencies?
- Were government agencies adequately informed at all stages?
- Were too many agencies involved?
- ♦ Were any changes needed in procedures to manage government relations?
- Examples of affected U.S. agencies (there may be others):
 - Coast Guard
 - Environmental Protection Agency
 - National Oceanographic Atmospheric Administration
 - Department of Fish and Wildlife
 - State Parks
 - Harbors and Marinas
 - States
 - Cities
 - Counties
- Was there adequate agreement with the government agencies on disposal methods?
- ♦ Was there adequate agreement with the government agencies on criteria for cleanup?
- How was this agreement developed?
- Were we too agreeable with the agencies in accepting their requests for specific action items (e.g., degree of cleanup)?
- ◆ Should there be advance planning of criteria for cleanup aimed at specific local environmentally sensitive areas? (Such criteria should probably also be designed for different types of oils.)

4.1.2.10..Public Relations

- ♦ How were relations with the media handled?
- What problems were encountered?
- Are improvements needed?
- ♦ How could public outcry have been reduced? Was it serious?
- ♦ Would it be useful to undertake a public information effort to educate reporters about oil and its effects if spilled?
- ◆ These areas should be investigated shortly after the incident to assure that actions taken are fresh in peoples' minds.

4.2..... FACILITY SPILL HISTORY

This section presents a discussion of spill events that have occurred at the Brooklyn Terminal during the past 5 years as required by the OPA 90 under 40 CFR 112.20. To date, the Facility has not been at fault for any reportable oil spills, as defined in 40 CFR Part 110.

After emergency notifications, all spills that occur at the Facility are reported to the Regional Manager. The EMP&R Notification Log is an environmental incident tracking form and is used to track all spills, releases, and discharges. A formal log of the reportable spill incidents is kept in this manual maintained at the Terminal Office.

This Integrated Contingency Plan is updated as necessary with a copy of pages from the current Spill Control Log. A copy of a typical log page is presented here in Annex 4. Copies of spill records and the remedial actions taken to prevent an occurrence of a spill incident are also maintained in a Spill Control Log, which is kept in the Terminal Office. A copy of the Casualty / Loss Incident reports are also placed in this file after each spill control incident, along with an analysis of the causes of the incident and the preventive measures taken to control it. This file is kept in the Terminal Office and is updated as required.

4.2.... Continued

Elements required on the spill history record.

Date of discharge.	
Location of discharge.	
Discharge cause(s).	
Material(s) discharged.	
Amount discharged.	
Amount of discharge that reached navigable waters.	
Amount recovered.	
Effectiveness and capacity of secondary containment.	
Clean-up actions taken.	
Steps taken to reduce possibility of recurrence.	
Total storage capacity of the tank(s) or impoundment(s) from which the material discharged.	
Enforcement actions.	
Effectiveness of monitoring equipment.	
Description of how spill was detected.	

ANNEX 5..... TRAINING AND EXERCISE DRILLS

5.1..... FACILITY DRILLS AND EXERCISES

Alert drills, as required by the Clean Water Act (CWA) Section 311(j)(5), are part of the response plan and are recorded in the PREP Documentation Log that is kept in the Terminal Office. During the drills, actions taken by the response team, both predicted and unpredicted, are noted and reviewed.

5.1.1...... Description of Exercises and Evaluation Procedures

The Facility follows the National Preparedness for Response Exercise Program (PREP) Guidelines for responding to the evaluation and exercises requirements embodied in the OPA 90 regulations. This Facility uses a combination of both internal and external exercises to comply with the preparedness and training portions of the PREP guidelines. The internal exercises include:

- ♦ QI notification exercises
- ◆ Spill Management Team Tabletop Exercises

Additionally, the Facility conducts area exercises in cooperation with Motiva staff and with the participation of other Industry response teams.

- ◆ The QI Notification Exercises include quarterly notification of the various QIs and AQIs at the terminal.
- ◆ The spill management team tabletop exercises consist of annually conducted spill drills with the local spill management team.
- ◆ The OSRO equipment deployment exercises are conducted by the OSROs under contract by Motiva. These OSROs are asked to provide documentation that they have complied with the annual equipment deployment exercises. Because the Facility personnel are neither permitted nor qualified to provide emergency response activities, all emergency response is performed through OSROs.
- Within a triennial cycle, the Facility and Motiva conduct the following minimum number of drills:
 - Twelve–QI notification exercises conducted quarterly.
 - Three—spill management team tabletop exercises. One of these involves a worst-case scenario and is conducted annually in conjunction with the local spill management team.

- Three—unannounced exercises conducted annually that are more than QI notifications. These exercises vary in size and scope. Actual response can be considered as an unannounced exercise.
- OSRO–equipment deployment exercises (required of OSROs on an annual basis).
- Company equipment deployment exercises (semiannual). Note:
 As stated in Core Plan 1.1.4, the Facility does not have response equipment and relies on OSRO contractors. Absorbents, shovels, rakes, gloves, and flash lights are maintained onsite for routine maintenance and housekeeping purposes and not for spill response.

5.1.2..... PREP Guideline Compliance

This Facility is in compliance with the PREP guidelines and exercises. The supporting documentation for the compliance with the PREP guidelines is maintained in the Terminal Office files.

5.1.3...... QI Notification and Spill Management Team Tabletop Drill Exercises

The QI notification exercises are conducted quarterly. The Spill Management Team Exercises are conducted annually. Documentation of the drills is kept in the Terminal Office files.

5.1.4...... QI Notification Drill Logs

The logs of the drills are maintained in the Terminal Office files. The logs are maintained for a period of five (5) years.

5.1.5...... Spill Management Team Tabletop Exercise Logs

Spill Management Team Tabletop Exercise Logs are maintained in the Terminal Office files. The drill logs, that include self-evaluation of the exercise, are available by request of the Complex Manager. The logs are maintained for a period of five (5) years.

Motiva has committed to compliance with training requirements and drill requirements as outlined in the PREP Guidelines.

5.1.6...... Government-Initiated Unannounced Exercises

Government-initiated unannounced exercises are designed to give the agency with primary regulatory oversight over a particular industry the opportunity to evaluate on a random basis, the response preparedness of that industry. Motiva will participate in a government-initiated unannounced exercise as directed.

5.2..... TRAINING AND MEETING LOGS

5.2.1 Personnel Training and Qualifications

The Complex Manager determines the qualifications of various personnel and assignments.

This Section contains a description of the qualifications and the personnel's training that is conducted at the Facility.

5.2.2..... Personnel Qualification and Training

5.2.2.1.... Demonstrated Ability Requirements

No person is allowed to operate the storage and handling equipment of this Facility until he / she has read and understands the operating procedures outline in this Plan for that person's scope of activity and has demonstrated ability to operate such equipment in the prescribed manner.

No employee of this Facility is permitted to operate the storage, processing or handling equipment unless that person can demonstrate to the Complex Manager the following:

- ◆ An ability to handle the Facility non-transportation related equipment.
- ♦ Thorough knowledge of the grade and name of all products handled.
- Knowledge of capacities of all storage tanks and products assigned.
- ◆ Ability to gauge tank level and temperature and convert barrels to gallons.
- Knowledge of location and operation of all piping and valves.
- Knowledge of location and operation of all safety equipment.
- ♦ Knowledge of emergency shutdown system.
- Knowledge of location and operation of communication method with shipping facility.
- ♦ Knowledge of all operation and spill contingency procedures outlined in this Plan.

Special training sessions dedicated to this Plan will be held as deemed necessary for present and future implementation.

5.2.2.2... Designated Individual Responsible for Training

The Complex Manager is responsible for personnel training. The Complex Manager ensures that no unqualified personnel are permitted to perform work. Additionally, the Complex Manager provides the opportunity for selected individuals to attend specialized training classes on pertinent subjects. Some of these classes may include HAZWOPER and refresher training, and other specialized training.

5.2.2.3.... Training Programs

The Facility personnel are instructed in the operation and maintenance of equipment at the Facility. The instruction includes the prevention of discharges, spills, or releases of oil, applicable pollution control regulations and the contents of the Facility SPCC Plan. No person is allowed to operate equipment or receive products at the Facility until he or she is thoroughly trained and has demonstrated an ability to handle the assignments.

The training received by all personnel including classroom instruction, safety and environmental briefings, on-the-job training with a supervisor, periodic formal reviews of the operating instructions and procedures used at the Facility is maintained as part of their personnel records.

All personnel are instructed when new procedures are introduced or when any procedures are modified. Training and retraining is also performed when new equipment is introduced in the Facility.

In addition to the Facility training, employees have received HAZWOPER training to the level of First Responder- Operations.

5.2.3...... Discharge Prevention Meeting Logs

Motiva conducts periodic safety meetings at this Facility. These meetings include various health and safety matters as well as discussions of spill prevention and cleanup and the importance of employee awareness, visual observation, and prompt response in preventing spills. At least once a year, the safety meetings will highlight and describe known discharges and any recently developed precautionary measures. The minutes of the safety meetings are maintained in the Terminal Office files.

5.2.4...... National Preparedness For Response Exercise Program (PREP)

MOTIVA ENTERPRISES, L. L. C. TRIENNIAL CYCLE OF EXERCISING THE ENTIRE RESPONSE PLAN

Fill in the dates exercises were conducted in the spaces provided below:

QI Notification Exercises ¹	Spill Management Team Table Top Exercises ²			
1.	1.			
2	2			
3.	3			
4				
5	Unannounced Exercises			
6				
7.	1.			
8.	2.			
9.	3.			
10				
11	Facility-Owned Equipment			
12	Deployment Exercises			
OSRO Equipment Deployment	1. N/A			
Exercises	2. N/A			
	3. N/A			
1	4. N/A			
2.	5. N/A			
3.	6. N/A			
V.	V. (W/)			

NOTES:

Complete documentation of drills or actual emergency responses is located in the Terminal Office PREP Documentation Log.

SAMPLE ONLY

¹One of these a year must be conducted during off-duty hours

²One within a three-year cycle must include a Worst-Case Discharge Scenario

INTERNAL EXERCISE DOCUMENTATION FORM

Quarterly QI Notification Exercise

1.	Date performed:
2.	Exercise or actual response?
3.	Terminal initiating exercise:
4.	Name of person notified:
5.	Time initiated:
6.	Method used to contact: Telephone, Pager, Radio, Other
7.	Description of notification procedure:
8.	Identify which of the 15 core components of your response plan were exercised during this particular exercise: Notification, Communications, Documentation.
	Certifying Signature

Retain this form for a minimum of five (5) years for EPA or three (3) years for USCG/PHMSA/BOEMRE.

INTERNAL EXERCISE DOCUMENTATION FORM

SPILL MANAGEMENT TEAM TABLETOP EXERCISE AND QI NOTIFICATION DRILL

 1.	Date performed:
••	Buto ponemicu.
2.	Exercise or actual response?
	If an exercise, announced or unannounced?
3.	Location of tabletop:
4.	Time started:
ᢇ.	Time started:
	•
5.	Response Plan scenario used (check one):
	Average most probable discharge.
	Maximum most probable discharge.
	Worst case discharge.
	Size of simulated spill.
6.	Describe how the following objectives were exercised:
	a) Spill management team's knowledge of oil spill response plan:
	b) Proper notifications:
	c) Communications system:

USCG/PHMSA/BOEMRE.

Annex 5, Page 8

Spill Management Team Tabletop Exercise (continued)

	d) Spill Management Team's a organizations:	bility to access contracted oil sp	ill removal
	e) Spill Management Team's abi Coordinator, State and applica	lity to coordinate spill response with ble agencies:	n On-Scene
	f) Spill Management Team's a information in the Area Conting	bility to access sensitive site an gency Plan:	d resource
7.	Identify which of the 15 core com during this particular exercise:	ponents of your Response Plan wer	e exercised
8.	Attach description of lesson(s) leacorrective measures.	rned and person(s) responsible for	follow up of
	Certifying Signature	Date	

Retain this form for a minimum of five (5) years for EPA or three (3) years for

(OSRO Certifications are in Annex 11.)

ANNEX 6..... RESPONSE CRITIQUE / PLAN REVIEW / MODIFICATION PROCESS

6.1..... AMENDMENT BY OWNER OR OPERATOR

SPILL PREVENTION, CONTROL AND COUNTERMEASURE PLAN REQUIREMENTS (40 CFR §112.4 & 112.5):

a. Review Frequency

As the owner or operator of this Facility, a review and evaluation of the Spill Prevention, Control, and Countermeasure portion of this Plan will be conducted within six (6) months of any change in Facility design, construction, operation or maintenance that materially affects the Facility's potential for discharge of oil into or upon the navigable water of the United States or adjoining shore lines, or at least every five years. Any technical amendment(s) will be implemented as soon as possible but not later than six (6) months. Changes requiring amendment to this Plan include, but are not limited to:

- Commission or decommission of tanks;
- Replacement, reconstruction, or movement of tanks;
- Reconstruction, replacement, or installation of piping systems;
- ♦ Construction or demolition that might alter secondary containment structures; or
- ◆ Revision of standard operation or maintenance procedures at the facility.

b. Required Amendments

The owner or operator of this Facility will amend the Spill Prevention, Control, and Countermeasure portion of this Plan within six (6) months of its review to include more effective prevention and control technology if such technology will significantly reduce the likelihood of a spill event from the Facility and if such technology has been field proven at the time of the review.

c. Plan Certification

The Spill Prevention, Control, and Countermeasure portion of this Plan will not satisfy the requirements of 40 CFR 112 unless certified by a Registered Professional Engineer. The Engineer must: (1) be familiar with the requirements and provisions of 40 CFR 112; (2) he or his agent have examined the facility; (3) attest that the Plan is prepared in accordance with "good engineering practices", including consideration of

applicable industry standards; (4) procedures for required inspections and testing have been established and with the requirements of this part and (5) attest that the Plan is adequate for the facility. Certification for the Spill Prevention, Control, and Countermeasure portion of this Plan can be found in Annex 8, Section 8.2.2. This Plan must be re-certified by a Registered Professional Engineer whenever there is significant modification (i.e. technical amendment) of the Plan.

d. Submission and Modification

Availability

As the owners or operators of this Facility, Motiva Enterprises LLC will maintain a complete copy of this Spill Prevention, Control, and Countermeasure portion of this Plan at the Facility and will make the Plan available to the Regional Administrator or authorized representative of the Environmental Protection Agency for on-site review during normal working hours. A complete copy is maintained at the Facility because the Facility is manned at least four hours a day.

Submission to Regional Administrator

In the event that this Facility discharges more than 1,000 gallons of oil into or upon the navigable waters of the United States or adjoining shorelines in a single event, or discharges more than 42 gallons of oil upon the navigable waters of the United States or adjoining shorelines in two reportable spill events within any twelve month period, the owner or operator of this Facility will submit the following information to the Regional Administrator of the Environmental Protection Agency within 60 days.

- 1. Name of facility
- 2. Name of owner / operator
- 3. Location of facility
- 4. Maximum storage or handling capacity of the facility and normal daily throughput
- 5. Corrective action
- 6. Description and maps of facility
- 7. Cause of such discharge including failure analysis of the system
- 8. Additional prevention measures taken or contemplated
- 9. Other information as required by the RA pertinent to the Plan or discharge.

EPA FACILITY RESPONSE PLAN REQUIREMENTS 40 CFR § 112.20(d) & (g)

a. Review Frequency

The facility response plan must be reviewed periodically to ensure compliance with the ACP and NCP.

b. Required Amendments

Revisions to the response plan must be submitted to the Regional Administrator within 60 days when there is a change that may materially affect the response to a Worst-Case Discharge. These changes include the following: 1) facility configuration that significantly affects the information included in the Plan; 2) oil stored, handled or transported that affects the response resources; 3) names or capability of the OSROs; and 4) facility response plan procedures.

USCG REVIEW AND UPDATE PROCEDURES

a. Conditions Requiring Changes:

- Relocation or replacement of portions of the Facility (including the pipeline) which in any way substantially affect the information included in this Plan, such as a change to the Worst Case Discharge volume.
- ◆ Emergency response procedures.
- A change in the listings of economically important or environmentally sensitive areas identified in the applicable ACP in effect six (6) months prior to the Plan review.
- ♦ Change in the Facility's configuration that materially alters the information included in the Plan.
- ♦ Change in the type of oil handled, stored, or transferred that materially alters the required response resources.
- ◆ A change in the name of the Oil Spill Removal Organization (OSRO).
- ◆ Material change in capabilities of the Oil Spill Removal Organization(s) (OSROs) that provide equipment and personnel.
- Any other change that materially affect the implementation of the Plan.

b. Submission of Revisions

USCG requires changes to be submitted to them in a timely manner to the MSO (in duplicate). The plan review must occur within one (1) month of the anniversary date of the USCG approval letter. If NO CHANGES are required, the Facility will submit a letter to the USCG stating "NO CHANGES REQUIRED".

6.2....RECORD OF CHANGES

Include record of changes here.

Date	Page	Description of Change
May 2003	Entire Plan	Conversion of FRP to ICP
Nov 2003	Table of Contents, Pgs. 2, 5, 9, 10; Introduction, Pg. 1; Core Plan, Pgs. 20 thru 23; Annex 1, Pg.1 and Figure 1.6; Annex 2, Pgs. 3 thru 12; Annex 5, Pgs. 1, 2; Annex 6, Pgs. 3, 4; Annex 8, Pgs. 1, 33 thru 38; insert behind Annex 11, Pg. 3	USCG requested revisions
Jan 2004	Table of Contents, Pgs. 2, 8, 9; Introduction, Pgs. 1, 5; Annex 1, Figure 1.2; Annex 6, Pg. 4; Annex 8, Pgs. 21(a), 21(b), 33 thru 39; Annex 11	Additional USCG changes
April 2004	Table of Contents, Pg. 10; Introduction, Pgs. 2, 3, 5; Core Plan, Pgs. 4, 6, 7; Annex 1, insert Figure 1.6(a) (Barge Unloading Manifold diagram); Annex 3d, Pgs. 1, 10, 11; Annex 6, Pg. 4; Annex 7, Pgs. 1, 2, 3, 25 – 31; Annex 8, Pgs. 2, 26, 40	Contact numbers and addresses update, miscellaneous changes
Aug 2004	Core Plan, Pgs. 3, 4, 10, 15 thru 17; Annex 5, Pgs. 2 thru 4; Annex 6, Pg. 4; Annex 7, Pgs. 2, 3, Annex 8, Pg. 14; Annex 11, Pgs. 1 thru 3, Replace inserts behind page 6, Replace PREP Certification Page and add inserts for Clean Harbors Cooperative. Insert PREP Certification Page for Marine Spill Response Corp., Insert Miller Environmental group PREP before Miller contract. Insert Clean Venture PREP before Clean Venture contract dated June 20, 2000.	EPA Review
Jan 2006	Table of Contents, Pgs. 2 thru 11; Introduction, Pg. 5; Core Plan, Pgs. 3 thru 7; Annex 3a; Annex 6, Pg. 4; Annex 8, Pgs. 31, 32; Annex 9, Pg. 2	Personnel changes and global changes
April 2006	Introduction, Pg 5; Core Plan, Pgs 3, 4, 6, Annex 6, Pg 4; Annex 11, PREP Certification for OSROs	Personnel and contact numbers updated and PREP Certification
March 2008	Table of Contents, Pgs. 9, 10; Introduction, Pgs. 1, 5; Core Plan, Pgs. 2, 3, 4, 6, 9, 14, 17, 19; Annex 2, Pg. 1; Annex 3a, Pgs. 12, 24; Annex 3b, Pgs. 1 thru 4; Annex 3d, Pg. 14; Annex 3e, Pg. 2; Annex 3f, Pgs. 1, 2; Annex 5, Pgs. 2, 3, 4, 6, 8; Annex 6, Pg. 4; Annex 7, Pgs. 20, 21; Annex 8, Pgs. 3, 22; Annex 9, Pgs. 1, 7, 8 thru 28 replaced by 7 thru 16	Personnel, titles, and contact numbers updated; revised Annex 9 to remove threat of violence that is better covered in the Facility Security Plan (FSP).
April 2008	Introduction, Pg. 5; Core Plan, Pg. 4; Annex 6, Pg. 4	Update Corporate personnel information
June 2008	Table of Contents, Pgs 3 thru 5; Introduction, Pg. 5; Core Plan, Pgs. 4, 5; Annex 2, Pg. 1; Annex 3d, Pgs.1 thru 19 (retain maps at end of Annex); Annex 6, Pg. 4; Annex 8, Pg. 23; Annex 12, Pgs. 8, 9	EPA Response, Tactical Assessment; Corporate personnel update
June 2009	Table of Contents, Pgs. 3, 10; Introduction, Pgs. 1, 5; Core Plan, Pgs. 2 thru 4, 6, 9; Annex 2, remove Pgs. 3 thru 12-insert Pgs. 3 thru 7; Annex 3a, Pgs. 8, 12, 13, 23, 24; Annex 3c, Pgs. 4, 5; Annex 3d, Pg. 3; Annex 4, remove Pgs. 7,8, add Pg. 7; Annex 6, Pgs. 4, 5; Annex 8, Pg. 10; Annex 9, Pgs. 1, 2, Annex 11, Pg. 7, add PREP Certification behind appropriate banner page; after Pg. 29, add Ethanol MSDS	Personnel changes; title update; PREP and MSDS added
Oct 2009	Introduction, Pgs. 2, 3, 5; Core Plan, Pgs. 3, 4, 6, 22; Annex 1, Pg. 7; Annex 6, Pg. 4; Annex 7, Pgs. 1 thru 4, 8, 9, 11, 16; Annex 8, Pg. 2	Update of Ownership and Miscellaneous revisions
Feb 2010	Table of Contents, Pgs. 6, 8; Introduction, Pg. 5; Core Plan, Pgs. 3, 4, 6; Annex 6, Pg. 4; Annex 8, Pgs. 1, 22a; Annex 11, Pg. 3; insert 2009 PREP Certifications and banner pages	OSRO changes and global revisions
Aug 2010	Table of Contents, Pgs. 3, 10; Introduction, Pg. 5; Core Plan, Pgs. 4, 9, 22; Annex 3c, Pgs. 4 thru 6; Annex 6, Pg. 4; Annex, 7 Pgs. 1 thru 5, 10 thru 19; 32 and insert; Annex 8, Pgs. 19, 21, 24 thru 27; Annex 11, insert Ken's Marine contract and 2009 PREP; insert Miller Environmental Group contract	Personnel change, and global revisions; contracts; SPCC update

6.2....RECORD OF CHANGES

Include record of changes here.

Date	Page	Description of Change
Nov 2010	Table of Contents, Pg. 3; Introduction, Pg. 5; Core Plan, Pgs. 6, 11, 19, 20; Annex 3.e, Pg. 2, add Form ICS 205-CG; Annex 5, Pgs. 5, 6, 8; Annex 6, Pgs. 5, 6; Annex 8, Pgs. 34, 39; Annex 12, Pg. 10	Response to USCG request for information and global changes
Mar 2011	Introduction, Pg. 5; Annex 6, Pg. 5; Annex 8, Pgs. 34 thru 42 & insert USCG Cross Ref. (33 CFR 154.1045); Annex 11, insert Aerial Oil Tracking Resources	USCG updates
April 2011	Introduction, Pg. 1, 5; Core Plan, Pg. 3 thru 8; Annex 6, Pg. 5	Personnel Update
August 2011	Table of Contents, Pg. 10; Introduction, Pg. 5; Core Plan, Pg. 4; Annex 6, Pg. 5	Personnel Update
. 17		

6.3..... EMPLOYEE'S REVIEW OF THE INTEGRATED CONTINGENCY PLAN / SPCC PLAN

For a list of employees who are familiar with and review the ICP and the SPCC, see the Training Records, "Training Sign-In Sheets".

ANNEX 7..... PREVENTION

7.1..... HAZARD EVALUATION

7.1.1..... Potential for Contamination

The potential for contamination offsite is considered very slight. Each aboveground tank is contained in a concrete dike structure with concrete floors. The greatest potential for contamination is at the Dock facility where transfers occur over water.

7.1.2..... Tank Farm

Table 7-1 lists all tanks present at the Brooklyn Terminal including the substance stored. The prefix "A" indicates an aboveground tank and the prefix "B" indicates a below ground tank. The table indicates the tank type, the year originally installed; maximum volume in gallons, the possible types of failure, the prediction of flow rate and the direction of flow for all tanks. Surface impoundments are not used for product storage at this Facility. The words "tank" and "container" can be used interchangeably in the document.

7.1.3...... Estimates of Quantity of Oils Potentially Discharged

The estimates of the quantity of oils potentially discharged are shown in Table 7-1.

The Facility is a bulk storage terminal handling several types of petroleum products. The Facility receives petroleum from Buckeye Pipeline, truck, or incidental barge. The Facility stores it and transfers it to customers through the truck loading rack.

The potential for release of gasoline during a pipeline or barge receipt is dependent upon the rate at which material is pumped from the pipeline or vessel. The Facility receives products from either the pipeline or from a vessel at a maximum delivery rate of 5,400 barrels per hour.

7.1.4..... Possible Spill Pathways

The Facility is located in Brooklyn, New York on the shore of Newtown Creek. Any release from the piping at the Dock has the potential to directly impact Newtown Creek.

Site overflow drainage would most likely gently flow northeast on the Facility's property. Drainage from the employee parking lot and the washbay drain in the garage is to the City Sanitary and Sewer System.

TABLE 7-1 DESCRIPTION OF ABOVEGROUND AND **BELOW GROUND STORAGE TANK STORAGE**

Tank or Source ID*	Substance Stored	Tank Type or Surface Area	Year Installed	Type of Failure	Maximum Volume (gallons)	Containment Capacity (gallons)
A41	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	188,184 ¹
A42	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	
A43	Gasoline	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	187,782²
A44	Gasoline	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	
A45	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	240,859 ³
A46	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	
A47	Gasoline	Int. Floating Roof	1960	Overflow, rupture, leak	442,062	519,886 ⁴
A48	Gasoline	Int. Floating Roof	1960	Overflow, rupture, leak	445,126	490,187 ⁴
A49	Gasoline	Int. Floating Roof	1969	Overflow, rupture, leak	484,042	992,332 ⁴
A50	Gasoline	Int. Floating Roof	1969	Overflow, rupture, leak	483,790	
A51	oos	Horizontal	1987	Overflow, rupture, leak	5,000	15, 625 ⁵
A54	Puradd Gas Additive	Cone Roof	1993	Overflow, rupture, leak	5,000	

Note: Based on Tank inspections both internal and external, and prevention measures in place, the potential for a

A = aboveground tank B = belowground tank

Prediction of rate of flow-pinpoint leak to catastrophic collapse Direction of Flow - Northeast

Note¹: These tanks are within the same containment.

Note²: These tanks are within the same containment.

Note³: These tanks are within the same containment.

Note⁴: These tanks are contained within their own containment area.

Note⁵: These tanks are contained within their own containment area.

TABLE 7-1 DESCRIPTION OF ABOVEGROUND AND BELOW GROUND STORAGE TANK STORAGE (Cont'd)

Tank or Source ID*	Substance Stored	Tank Type or Surface Area	Year Installed	Type of Failure	Maximum Volume (gallons)	Containment Capacity (gallons)
A53	Slop Tank	Horizontal	1993	Overflow, rupture, leak	6,000	598,000 ⁴
A55	oos	Horizontal	1999	Overflow, rupture, leak	10,000	12,000 ⁶
A7	oos	Horizontal	1945	Overflow, rupture, leak	9,600	228,000 ³
A8	oos	Horizontal	1945	Overflow, rupture, leak	9,600	228,000 ³
A9	Ultrazol Gas Additive	Horizontal	1945	Overflow, rupture, leak	9,600	228,000 ³
A10	Nemo	Horizontal	1945	Overflow, rupture, leak	9,600	228,000 ³
Talentana	0	THER POTEN	ITIAL SPI	LLSOURC	ES	rien Destruction
A Recovery Well Tank	Petroleum Contact Water	Horizontal	1999	Overflow, rupture, leak	275	560
Rack Separators	Petroleum Contact Water	Horizontal	1940s	Overflow, rupture, leak	6,000	N/A
B Final Separator	Petroleum Contact Water	Horizontal	1940s	Overflow, rupture, leak	25,000	N/A
B 52	Rack Water Containment	Horizontal with cement vault		Overflow, rupture, leak	4,000	6,800

Note: Based on Tank inspections both internal and external, and prevention measures in place, the potential for a discharge is remote.

- A = aboveground tank B = belowground tank
- Prediction of rate of flow-pinpoint leak to catastrophic collapse Direction of Flow - Northeast
- Note¹: These tanks are within the same containment.

 Note²: These tanks are within the same containment.

- Note: These tarks are within the same containment.

 Note⁴: These tanks are within the same containment.

 Note⁴: These tanks are contained within their own containment area.

 Note⁵: These tanks are contained within their own containment area.
- Note⁶ This tank is contained within a vault.

TABLE 7-1 DESCRIPTION OF ABOVEGROUND AND BELOW GROUND STORAGE TANK STORAGE (Cont'd)

OTHER POTENTIAL SPILL SOURCES							
Tank or Source ID*	Substance Stored	Tank Type or Surface Area	Year Installed	Type of Failure	Maximum Volume (gallons)	Containment Capacity (gallons)	
Loading Rack(s)/ Transfer Area(s)	Petroleum Products	N/A	Various	Valve Failure; Leak	N/A	Catch Basins	
Pipeline/ Pumps	Petroleum Products	N/A	Various	Receiving	N/A	Tank/Catch Basins	
Vapor Recovery Unit	Condensate/ Glycol	N/A	Unknown	Maintenance	110	110	
Garage/ Used Oil	Used Oil	Horizontal	1988	Overflow, rupture, leak	280	400	
Water Collection	Petroleum Contact Water 7@700 gal. tanks	Horizontal	Various	Overflow, rupture, leak	4,900	> 700 gal. (inside dike walls)	
Prover	Gasoline/ Distillates	Steel	Unknown	Overflow, rupture, leak	1,000	> 1,000 (use under truck rack)	
		40	DRUMS				
Lessee Storage Areas	Various Petroleum Products	Drums, Pails, Cases		Overflow, rupture, leak	50,000	Inside Building	
Drum Storage Area	Glycol/Red Dye	Drums 4@ 55 gals.		Overflow, rupture, leak	220	6,800	
Satellite Accumulation Area	Petroleum Debris	Drums 1@ 55 gals.		Overflow, rupture, leak	55	755 gal (inside truck rack)	
Garage/ Grease	Grease Oil	Drums 6@ 55		Overflow, rupture, leak	330	> 55 gal (inside warehouse)	

- A = aboveground tank B = belowground tank
- Prediction of rate of flow-pinpoint leak to catastrophic collapse Direction of Flow - Northeast
- Note¹: Note²: These tanks are within the same containment.
- These tanks are within the same containment.

- Note: These tanks are within the same containment.

 Note: These tanks are within the same containment.

 Note: These tanks are contained within their own containment area.

 These tanks are contained within their own containment area.
- Note⁶: This tank is contained within a vault.

7.1.5..... Diked Areas

All aboveground storage tanks at the Brooklyn Terminal are completely surrounded by containment dikes. Spills from the storage tanks or related product and pipeline will be contained within the diked areas and pumped out over the dike walls in accordance with NYFD requirements. Air pumps equipped with hard pipe suction are used to transfer accumulated precipitation to the oil/water separator system prior to discharge through Outfall 001.

The Facility's truck loading rack, truck pump-off area, and additive unloading is equipped with curbs, roof and strip drains designed to hold the contents of the largest single compartment on a tank truck. The spill containment system drains to a 4,000-gallon underground tank. The tank is emptied as needed and the material is transported off site for disposal. The additive unloading and truck pump-off areas are located adjacent to the truck loading rack.

Discharges from paved yard area catch basins, tank truck parking area, warehouse loading platform, garage drains (excluding wash bay), and pump out from the VRU goes to the final separator prior to discharge through Outfall 001.

The final separator is equipped with a mechanical shut-off valve that prevents flow through until the oil is pumped out of the separator. Treated water from the separator is discharged under the Facility's SPDES permit.

Drawings of the spill control drainage plan for the Facility are shown in the Core Plan, Figure 1.4 and in Annex 1. These drawings indicate the general arrangement of the fixed facilities that will prevent the release of oil and petroleum to the environment.

7.1.6..... Undiked Areas

The major portion of the tank farm piping is run in the tank farm containment area or in the protected truck loading rack area. The remaining piping is run aboveground and over the protected truck loading rack area and asphalt yard area. All other drainage of the paved area flows toward catch basin drains located throughout the Facility that ultimately drains to the final separator and processed prior to discharge.

7.1.7..... Schematic Drawing of Facility

A schematic drawing of the Brooklyn Terminal with all tanks labeled is provided in the Core Plan, Figure 1.2, and in Annex 1, Figure 1.2.

Comment [J1]: Used againin 7 1.8.4

Comment [aeh2R1]:

Comment [aeh3]: storage - was removed.

Storage denotes product kept until needed. A UST is also registered.

Comment [J4]: Is there a word missing here?

7.1.8...... Procedures for Routine Handling of Products

The Brooklyn Terminal has a number of established procedures in use for truck loading and transfer operations. The Facility receives products from either pipeline or barge at an average delivery rate of 5,400 barrels per hour for gasoline.

7.1.8.1.... Loading (Receiving) Procedures

To provide a dependable safeguard against tank overfilling, each of the storage tanks receiving product is equipped with a two-stage high-level alarm system. In an overfill situation, both a visual and audible alarm is set off, followed by a third high-high alarm which will automatically close the valve on the receiving line to effectively shut off the transfer of product into the tank and prevent an overfill. The primary alarm is set at 90% fill capacity and with a visual white light; secondary alarm at 95% fill capacity with an amber light and shut down audible alarm, and the tertiary alarm is at 98% fill capacity with a red light and shut down alarm. The Buckeye Pipeline is equipped with an automatic shut down system if a high-high (secondary or tertiary) alarm is received, while the dock operation has manual shut down devices during product receipts.

The Facility has secondary containment around each storage tank that is described in Annex 7.2. This dike has sufficient capacity to contain any expected overflow or tank rupture.

No person is allowed to handle the receipt of products unless he or she has been thoroughly trained and has demonstrated the ability to perform these procedures. Additional details on employee training are contained in Annex 5 of this Plan.

a. Preparation of Tanks Prior to Pipeline or Vessel Receipt

Prior to the receipt of product, the tank(s) are manually gauged and a product storage tank temperature taken. The exact time the gauge was taken, depth of water, (if any), the product depth, and temperature are entered in the Facility gauge worksheet. The person taking this gauge will initial the gauge worksheet. The gauger will calculate the headroom in the storage tank(s) scheduled for receipt to ensure the tank(s) will hold the amount of the receipt.

The designated responsible person for the Facility will arrange to open the manifold receiving valves and the tank receiving valves. Receipt valves and high level alarms are tested.

Other procedures for receipt by pipeline or vessel are specified in the Operations Manual.

b. Procedures During Receipt of Product

The following descriptions are general in nature and for informational purposes only. The Facility's operating procedures and instructions govern the receipt of product. These procedures are maintained in the Terminal Office.

Qualified personnel will be on duty during receipt of product. These personnel receive periodic refresher instructions on the correct procedures to use during product transfer. The person in charge of receipt of the product follows local Facility procedures for receipt of product.

After product has started to flow, the qualified person walks the pipeline to the receiving tank checking for leaks. At the tank, the automatic gauge is checked to assure product is flowing into the proper tank.

During the tank receipt, the person in charge will calculate a rough gauge (final height) for the receiving tank. Thereafter, the person in charge of the receipt will check the tank gauge (product level) at least once an hour.

If the tank is to be filled to near capacity, it will be gauged more often when the tank is nearly full. The qualified person will remain on watch on the platform of the tank (or other suitable observation location) during the last half hour of pumping. After each hourly gauge, the receiving lines will be walked to check for leaks.

If more than one tank is on a delivery line, the tank not receiving product will be gauged prior to start of delivery and at the first hourly gauge to make sure there is no leak in its valve or confusion in quantities received that could possibly cause an overfill of the tank.

c. After pumping procedures

After completion of the receipt, external valves on the delivery line will be closed. The tank will be manually gauged and measured for water and the temperature of the produce will be accurately measured at the midpoint of the product. This information will be recorded in the gauge worksheet along with the time receipt was completed. The qualified person will initial the entries in the gauge worksheet for identification.

d. Communications During Receipt

(1) When product is received by marine transport - On barge receipts, visual and oral communication is maintained between the vessel's hose watch and the Facility's hose watch. Product to be received, pumping rate and batch size are reviewed prior to start-up. Adequate sets of portable, intrinsically safe transceiver radios are available and used, that enables direct communication between pumping station or vessel, hose watch and tank watch.

7.1.8.1 Loading (Receiving) Procedures (Cont'd)

d. Communications During Receipt (Cont'd)

(2) When product is received by pipeline, the person responsible for the receipt maintains the frequent communication with the pipeline company. Meanwhile, another person is constantly gauging the tanks while communicating via intrinsically safe radios with personnel in the office. Any changes (such as type of product, quantity, amount of room in the tank, the need for pipeline wash, and other appropriate information) are exchanged between the pipeline and the Facility.

7.1.8.2.... Tank Truck Procedures

a. Receipt of Product by Tank Truck

Receipt of product by tank truck is scheduled by Facility personnel. The procedures covering the receipt of product by tank truck are specified in the *Terminal Operations Manual*. Those procedures and Facility operating procedures and instructions control the receipt of product. The following description is for the purposes of information only. The procedures and instructions are maintained in the Terminal Office.

Preparation includes assignment of qualified personnel to receive the product. The truck unloading area is maintained free of obstacles. Should any accidental discharge occur, the area is graded to discharge into strip drains that go to a primary separator and then to the final separator prior to discharge.

- A fire extinguisher is maintained at the pump-off spot.
- Only qualified employees are permitted to pump-off transport trucks.
 These individuals are trained in the prescribed loading / unloading procedure for tank trucks according to instructions in the training manual.
- The transport truck is attended at all times during the unloading process to provide instant shut down in case of an emergency.
- All pump-off lines are capped, all valves kept closed, and the tank valve locked except when in use.
- No mobile storage tanks are at the Facility.

7.1.8.3.... Tank Truck Loading Procedures Using the Loading Rack

a. Transfer of Product Into Tank Trucks

The Facility uses an automated system for the transfer of product into tank trucks. The system is designed to prevent spills and overfills. As an additional precaution against spills, the drivers are permitted to use the truck rack control system and have received instruction from Motiva on the correct procedures to use in accessing the system, safety precautions, and spill reporting.

7.1.8.3.... Tank Truck Loading Procedures Using the Loading Rack (Cont'd)

a. Transfer of Product Into Tank Trucks (Cont'd)

The general procedures for operation of the truck rack control system are found in the *TMS System User Manual* located in the Terminal Office.

Only authorized truck drivers can gain access to the loading rack by presenting an authorization card and entering a unique driver code number (PIN).

The trucks are bottom loaded at this Facility. The trucks are equipped with a loading bar or brake locks that lock the brakes and prevent the truck from starting.

The drivers are instructed to carefully inspect vehicles to make sure that bottom valves are not leaking. Trucks are occasionally spot inspected. In the event that a vehicle fails inspection the truck will be barred from the Facility until the necessary repairs have been completed.

The automatic loading equipment also verifies that the driver has connected the grounding, overfill protection equipment, and vapor connection. This ensures that the truck is properly grounded to reduce the potential for static electrical discharges and that the truck overfilling protection equipment is properly operating. While loading, drivers must hold a "dead man" button or pumps will shut down and product will not flow to the truck.

When the driver completes loading he or she proceeds to the Bill of Lading printing area, obtains the Bill of Lading, opens the automatic gate, and leaves the Facility. Once the truck is loaded, the driver has custody of the shipment and is responsible for safe delivery of the product. Despite the fact that the driver is still inside the Facility gates, the driver is responsible for the shipment, and any spills that occur at that point will be considered transportation related.

b. Specific Procedures in Use for Truck Loading

Specific procedures in use for truck loading at the Facility are described in the *Terminal Operations Manual* and in specific terminal operating procedures. These are kept in the Terminal Office files.

- The Facility has specific safety procedures that include requirements for trucks to park away from the loading rack when awaiting the opportunity to load product.
- Loading will be stopped during severe electrical storms.
- Smoking permitted in designed areas.

7.1.8.3.... Tank Truck Loading Procedures Using the Loading Rack (Cont'd)

b. Specific Procedures in Use for Truck Loading

- Under no circumstances will a truck in the process of loading be left unattended or will it be parked at the rack unattended.
- All truck lights, heaters, accessories, and non-operating electrical equipment will be turned off before entering the loading area, and will only be turned on after leaving.
- Any stalled trucks will be towed away from rack prior to repairs.
 Booster batteries will be connected more than 100 feet away.
- · All DOT regulations will be followed.

7.1.8.4.... Facility Tank Truck Loading and Unloading Facilities

a. Description of Drainage and Barrier Systems

The Facility's truck loading rack has a drainage system that is designed to hold the contents of the largest single compartment on a tank truck. The spill containment system has a cement slab with drain inlets and strip drains connected to a 4,000-gallon underground tank. The truck pump-off and additive unloading areas are also located within the loading rack area. The additive unloading area utilizes the same containment system as the loading rack. The holding tank is emptied as needed.

The truck rack is covered by a large canopy to minimize rainwater collecting at the rack. Any liquid (water, melted snow or hydrocarbon) that falls beneath the canopy flows by gravity to a sub surface holding tank where it is manually emptied via a vacuum truck.

b. Disconnect Protection Systems

All trucks that load at the Facility have either a locking bar or other interlocking system to prevent the truck from being moved while the vapor recovery and/or loading hoses are still connected to the truck. All trucks are also equipped with over-fill protection and are grounded to ensure further safety. Truck over-fill protection is tested annually by the carrier for every truck and records are kept in the Terminal Office.

c. Examination of Bottom Drains on Vehicles

The drivers are instructed to carefully inspect vehicles to make sure that bottom valves are not leaking. In the event that a bottom valve is discovered leaking, the truck will be barred from the Facility until the necessary repairs have been completed.

Shell/Motiva 0008674

7.1.8.4 Facility Tank Truck Loading and Unloading Facilities (Cont'd)

d. Overfill Protection System

The overfill protection system shall be checked for proper operation prior to loading.

7.2..... SECONDARY CONTAINMENT

7.2.1..... Dikes and Dike Capacity

The Facility tanks are surrounded by dikes that have a capacity in excess of the largest of the tanks plus an allowance for rainfall. The total storage capacity of the tank farm containment area is adequate to contain the largest tank (450,000 gallons) and has enough volume for a rainfall allowance.

The volumetric capacity of the containment areas has been prepared by David Martin, Motiva Enterprises, and RPMS Engineers.

7.2.2..... Dike Integrity

Diked areas are sufficiently imperious to contain spilled oil. Containment walls and floors are fully intact and have no permeable voids. The tank farm containment dikes are constructed of concrete. The additive tanks are contained within concrete containments or contained within underground containment areas.

7.2.3 Curbing

The other principal area that could result in a release of petroleum is the truck loading rack. The loading rack has curbs to direct any potential spilled product to flow by gravity to a sub-surface holding tank where it is manually emptied via a vacuum truck. The loading rack containment system is substantially larger than the largest single compartment that could spill on the rack.

7.2.4...... Culverts, Gutters or Other Drainage Systems

The Facility removes tank water bottoms by transferring it into water collection tanks, then the water is pumped to a holding tank and the product is returned to storage. The tank is contained within a concrete containment dike that is adequately sized to contain the entire contents of the tank plus sufficient freeboard.

Dock drainage procedures (booming equipment and drip pans) are covered in the Dock Operations Manual.

7.2.5..... Retention Ponds

This Facility does not have a retention pond.

7.2.6..... Sorbent Materials

All sorbents used for spill response will be supplied by contracted OSROs.

7.2.7...... Positive Controls to Prevent Drainage From Diked Areas

The positive controls used to prevent drainage from diked storage areas include procedural controls and equipment to prevent the discharge of oils from all areas of this Facility.

- The preferred method of removal of accumulated stormwater is by natural evaporation provided that the accumulation does not damage the equipment / structures or inhibit operations conducted within the containment area.
- In the event that drainage of an area becomes necessary due to accumulated stormwater, the containment area air pumps equipped with hard-pipe suction and discharges are pumped to the oil/water separator outside the diked area then to the final separator prior to discharge through Outfall 001. If a visible sheen or other condition indicating the presence of oil or gasoline is present, the valves are not operated.
- In the tank farm area, all tank water withdrawal valves are closed and locked when not in use. All basin drain valves, where installed, are closed and locked when not in use. When the basin drain valves are operated, the water in the basin is inspected by an employee prior to operation of the valve.
- Accumulated water is visually inspected for oil and / or oil product contamination (sample procedures and documentation forms are provided in Annex 7) and discharged only if no contamination is observed.
- The Facility does not have an effluent treatment facility.
- In the event that drainage of contaminated liquids from a containment area is required, the use of a vacuum truck, pump, or other means will be evaluated for the removal.

7.2.8..... Disapproval of Flapper-Type Drain Valves

Flapper-type drain valves are not used in this Facility.

7.2.9...... Drainage from Undiked Areas

This topic is discussed in detail in Annex 7.1.6.

7.3...... BULK STORAGE INSTALLATION

7.3.1..... Material Compatibility Standards

The Facility's bulk oil and oil product storage tanks have been designed in accordance with industry standards. The tanks have the following design characteristics:

- ◆ Tanks are constructed of a material that is compatible with the oil and petroleum products stored and the conditions of storage.
- Tanks are operated within "Safe Fill" levels positioned below the established capacity limits of the tank.
- A conversion of tanks or construction of a new tank for Ethanol is constructed at regulatory standards. A Management of Change for the standard is completed to cover an Ethanol change.

7.3.2..... Secondary Containment Sufficiency

A discussion of the secondary containment sufficiency for this Facility is presented in Annex 7.2 above.

7.3.3...... Drainage Bypass Systems

The Facility does not have a bypass system for Facility drainage.

7.3.4...... Underground Metallic Storage Tanks

There is one underground storage tank at this Facility. The tank is registered, within a cement vault, and provided with cathodic protection.

7.3.5...... Partially Buried Metallic Storage Tanks

There are no partially buried metallic storage tanks at this Facility.

7.3.6...... Integrity Testing Standards for Aboveground Storage Tanks

The tank integrity and testing standards are discussed in Section 7.10.

7.3.7..... Internal Heating Coils

There are no internal heating coils in any of the Facility tanks.

7.4...... DISCUSSION OF FAIL SAFE ENGINEERING AND DESIGN STANDARDS

As far as practical, the Facility has been engineered to fail-safe engineering standards. The fail-safe provisions include, but are not limited to:

 Automated truck loading rack system that allows the loading of trucks with maximum safety.

- The use of large loading rack roof to minimize the entry of rainwater into the loading rack.
- The use of audio high-level alarms on all tanks that receive product from the pipeline or vessel.
- ◆ The use of tank dikes to prevent petroleum from flowing from the Facility property.
- Tank inventory is maintained by the Alliance Distribution Measurement Policy.
- The policy manual is a separate document located at the Terminal Office.

7.4.1..... High Liquid Level Alarms

Motiva Enterprises LLC petroleum storage tanks have high liquid level alarms that have audible signal to detect high levels during filling operations. Upon hearing a high-level alarm, Facility Personnel will check the tank and tank level to verify its contents and integrity. This Facility also has valves with fusible link cut-offs to stop a high-flow event. Alarms are tested on a regular basis.

Tank high-level alarms and gauging devices are tested by pulling alarms and verifying manual versus automatic gauges prior to every receipt by the Terminal Operators. Tank high-level alarms are inspected by a certified electrician annually. Tank high-level calculations are reviewed and verified annually by Terminal Management.

7.4.2..... Emergency Shut-off Devices

The Buckeye Pipeline will shut down flow to the Facility immediately upon receiving a high-high (secondary or tertiary) level alarm. Upon receiving the high-high level alarm, the Buckeye Pipeline will automatically close pipeline valves to the Facility. The pipeline can shut down flow within five minutes in an emergency.

7.4.3...... Direct Communications Between Facility and Pipeline

The Terminal Operator and the Buckeye Pipeline Operator communicate verbally before each receipt. For attended receipts, communication is maintained after flow has started and at the completion of each receipt.

7.4.4...... Fast Response Gauging Systems

The Facility uses quick response manual gauges that enable the Terminal Operator to determine the level in each of the tanks. The tank gauges are float-style gauges.

7.4.5..... Visible Oil Leaks

Cleanup of all oil leaks starts on discovery and will be completed in a safe and expedient manner. An oil leak is considered cleaned up when there are no visible traces of oil or petroleum on the ground.

7.4.6..... Mobile or Portable Oil Storage Tanks

Mobile or portable oil storage tanks may be brought on-site during various operations. These portable tanks will be positioned or located so as to prevent spilled oil from reaching navigable waters. The largest mobile/portable container will be provided with containment plus sufficient freeboard for precipitation.

7.5..... FACILITY TRANSFER OPERATIONS

7.5.1..... Buried Piping

Below ground piping is cathodically protected and coated to reduce corrosion.

The cathodic protection system is monitored monthly and the values for impressed voltages are recorded.

The cathodic protection system is checked annually by technically competent personnel. Copies of the reports are maintained in the Terminal Office for a minimum of five (5) years.

All underground product transfer piping is tested periodically. Copies of the reports are maintained in the Terminal Office.

When a section of buried pipe is exposed, it is carefully examined for deterioration and corrective action taken as necessary.

Buried piping installed or replaced after August 16, 2002 will be provided with a protective wrapping and coating and cathodic protection.

7.5.2..... Aboveground Piping

All aboveground valves and pipelines are regularly examined during operating personnel rounds. During these examinations, operating personnel assess the general condition and necessity for corrective actions of the pipelines.

7.5.3..... Out-of-Service Piping

Out-of-service pipelines will be capped or blind flanged and marked to its origin in the event that a Facility pipeline is removed from service or is placed in standby status for an extended time. Any out-of-service piping has had the product removed and the piping has been blind flanged or capped off.

7.5.4..... Design of Piping Supports to Reduce Abrasion

All piping supports are visually inspected to ensure that any abrasion is quickly detected. The aboveground piping is supported on a transverse horizontal pipe to minimize contact and abrasion. Where appropriate, special wearing shoes are welded on to the underside of pipes to further reduce abrasion potential in areas of high pipeline movement.

7.5.5..... Inspections

The Facility conducts a number of different types of inspections. A discussion of inspections and tests is presented in Annex 7, Section 7.7. Pipeline inspections are part of the Facility's Daily Inspection. Sample Inspection Checklist(s) are included at the end of this Annex.

7.5.6...... Warning Signs for Vehicular Traffic

Warning signs for vehicular traffic are prominently placed at strategic locations throughout the Facility. These signs warn all vehicles entering the Facility about the dangers related to the aboveground piping or other oil transfer operations. The signs include instruction for use of the loading rack, spill notification directions, and entrance and exit.

7.6..... NORMAL DAILY THROUGHPUT

The normal daily throughput for the Brooklyn Terminal is 840,000 gallons. When demand and, subsequently, daily throughput increase, the potential release volumes increase. This increase typically occurs in the summer.

7.7...... DISCHARGE DETECTION BY PERSONNEL

A spill or release can be discovered by visual inspection. The initial response actions described in Core Plan, Section 1.1.7.1 will be implemented if any spills are detected.

7.7.1..... Visual Inspection

The Terminal Operator examines the tanks and the equipment in the tank farm daily to ensure that there are no visible leaks in the tanks or piping system.

All visible tanks, lines, flanges, pumps, and other equipment are examined on a routine basis for indications of leaks, drips, sweating, etc. Repair of any such item is handled on a priority basis. Inspections include gauge hatch covers, manhole covers, gaskets, and foundations.

The exposed surfaces of the tanks, pipelines, and all equipment are inspected visually for the presence of discoloration or blistering that could indicate that the exterior paint is failing, or that the tank is leaking at a seam or through a pinhole. When any discoloration or blistering is observed, the tank or pipeline is repaired or replaced.

Other records of visual inspections that are made on a periodic basis, such as the internal floating roof seals, are kept in the Terminal Office on a dedicated form.

Motiva Enterprises LLC employs contractors to perform maintenance at the Facility. The maintenance is performed as required.

7.7.2...... Facility Self Inspection

The following is a partial list of the inspections that are made periodically at the Facility. Complete files on the results of these inspections are maintained by the Facility and are retained for a period of five (5) years. The following list is for example only and addresses only those items that are important to the operation and spill control issues at the Facility.

TYPICAL FACILITY INSPECTIONS

ltem	Description of Inspection or Test-Repair if defective
The second comparison of the property of the second comparison of the s	ADING RACK
Fire Extinguishers at all locations in the	Check for full charge / recharge where needed
Facility	Oncok for fail Gharge / recharge where needed
All loading arms on the loading rack	Visually Check for leaks, counter balance operations,
7 th loading aims on the loading rack	dry brake coupler seal, jaws, swing stops, adjust where
	required.
Truck Flush Equipment	Visually Check joints, swivels, couplers, and movement
	freedom
All Flow Control Valves and Meters	Inspect micro-switch screws and O-rings for leaks
All Turbine Flow Meters	Inspect and Check
All Temperature Probes	Re-calibrate
All Pressure Gauges	Inspect for operation / leaks
All Strainers	Inspect
Grounding Devices at lanes on loading rack	Inspect and Check
Overfill Device	Check Operation and status lights. Check to ensure
	bypass switch is locked in on position.
Vapor Flow Sensors	Physical check of successful operation during loading.
Rack Junction Boxes, Electrical	Check
Intercom	Check ·
Seals and gaskets	Visually inspect all piping, valves, fitting and
Ť	component connections, seals, gaskets and valve
	pacing for leakage or looseness
Meter Presets	Check function, ensure seals in place
TRUCK UI	NLOADING SYSTEM
Pump motor	Check for leaks
Air Eliminator	Check for leaks
Temperature Probe	Re-calibrate, Check for leaks
Water Draw Off Valves	Check for leaks, valves closed, splash blocks in-place
Pressure Gauges	Check for operation, leaks
Pump off hoses	Check for leaks
STORAGI	TANK FACILITIES
Tanks	Inspect roof devices, openings, for security and
	labeled. Observe domes and roofs for damage.
Water Draw Off Valves	Ensure valves closed and locked, check for leaks
Tank Level Gauges	Check for free movement, level transmitters
Tank Thermometers	Check for calibration
Tank Hi-Level Alarm	Manually Check audible alarm activation
Tank Level Transmitter	Compare readings and re-calibrate
Tank Motor Operated Valves	Completely check operation
Tank Hand Operated Valves	Check for leaks, operation
Tank Safety Control Valve	Check Operation
Product Pump Motor	Inspect for leaks, check operation
Tank Relief Valves	Check operation
Pressure Gauges	Check
Seals / Gaskets / Vitualic Couplings	Check for leaks
Tank Wall & Drains	Visual Inspection
Oil-Water Separator	Visual Inspection
Manifold Area	Thorough check of all valves, visual inspection,
	lubricate as required
Pipeline Signal Control Panel	Check for correct operation & pipeline signals

TYPICAL FACILITY INSPECTIONS (Cont'd)

ltem	Description of Inspection or Test-Repair if defective
-	SECURITY SYSTEMS
Perimeter Fence	Visual Inspection
Perimeter Gates	Check for locks and chains
Signs and Signboards	Check to ensure that warning signs, notices, instructions, and "Stop Here" lines are not obstructed and that they are secure and legible
Facility Area Lighting	Visually check lighting and ensure that lights are operating and are aimed for maximum illumination

The Facility maintains the records described below:

- 1. Records of Pressure Tests on Piping
- 2. Records of Meter Calibrations
- 3. Records of Repairs made to Facility
- 4. Environmental Records, including
 - a. Inspections of all water outfalls and water analyses
 - b. Environmental records of any and all groundwater testing
 - c. Personnel Training Records
 - d. Waste disposal manifests
 - e. Tank Cleaning and inspection records
 - f. Other records required by permits
- 5. Product reconciliation and tank testing records
- 6. Reports on cathodic protection testing and inspections
- 7. Records of key and lock assignments
- 8. Records of safety meetings

7.7.3..... Other Procedures

7.7.3.1.... Pressure Testing of All Pipelines

Motiva Enterprises LLC periodically tests all pipelines in the Facility. The work is performed by an outside contractor and reports of each pressure test are kept in the Terminal Office files for a minimum of five (5) years.

7.7.3.2.... Tank Testing

The Facility conducts periodic tank testing to ensure tank integrity. The tests are indirect, but are indications of the tank soundness.

7.7.3.3.... Cathodic Protection Testing

All steel tanks and lines are protected by an impressed current cathodic protection system. In order to protect the tanks and the pipelines, the system is inspected annually by technically qualified personnel.

7.7.3.4.... Soundness Testing and Inspection

- The containers are visually inspected by operating personnel for signs of deterioration, leaks, or the accumulation of liquids inside the containment areas.
- Each storage container is inspected according to Company policy, as required by age, condition, and service. The monthly tank inspection records are maintained in a separate file at the Facility.
- Motiva Supporting Documentation Refer to Tank and Pressure Vessel Inspection and Maintenance Manual for details.
- Based on these conditions, the aboveground storage containers are professionally inspected and non-destructive thickness testing is performed.
- All aboveground storage tanks are included in the scope of this inspection and maintenance document. This includes small tanks, additive tanks, water tanks, horizontal tanks, UL-142 tanks, API 650 tanks, vapor tanks, pressure vessel, etc.
- Inspection/testing records are retained in a separate file at the Facility for a minimum period of five (5) years or longer based on industry standard of Corporate policy. (Industry standard is to retain records for the life of the tank).
- If a field-constructed aboveground container undergoes a repair, alteration, reconstruction, or change in service that might affect the risk of a discharge or failure due to brittle fracture, the container will be evaluated.
- Drums or totes brought on-site are built or tested to the standard(s) or in-process inspection and testing procedures established by the drum manufacturer or the drum recycler, as applicable.
- While on-site, the drums or totes will be visually examined at least monthly.

7.7.3.5.... Product Justification Record

Several types of records are kept in the Facility. These records are examined on a daily basis.

A daily record is kept of the amount of product in storage in the tanks, products shipped through the truck loading rack, and products received from pipelines and vessels.

A bulk stock loss record is maintained at the Facility and balanced monthly. The bulk stock loss record is used to compare the actual variations, both gross and net, of product to the amount that is reasonably anticipated. Any variances in the records are immediately investigated.

7.7.3.6.... Locks and Seal Assignments

The Facility maintains a log of current key assignments, locks, and security seals.

7.7.3.7.... Written Procedures for Inspection

Written procedures have been developed for this Facility and a record of the inspections, signed by the appropriate inspector, is kept in the Terminal Office files. Sample forms are also located at the end of Annex 7.

7.7.3.8.... Record Retention Policy

Records of inspections must include each container, secondary containment, and item of response equipment at the Facility. The records of inspections must be cross-reference to retention location.

Inspection of response equipment is a requirement under 40 CFR 112.7(e). Facility self-inspection requires two-steps; (1) a checklist of things to inspect; and (2) a method of recording the actual inspection and its findings. Facility Response Plan records must be kept for five (5) years. The SPCC records are retained for three (3) years. Industry standards are that tank inspection records be retained for the life of the tank. Records are maintained in the Terminal Office.

7.8...... APPLICABLE MORE STRINGENT STATE DISCHARGE PREVENTION RULES AND REGULATIONS

♦ 6 New York Code of Rules and Regulations, §610-614.

		PIP	ELINE (CHECKLIST			Sun L	
<u> 1965-1961 († 2016)</u> 1	LTA:	V:	3890.5e . 06	PRODU	CT:	HRe Gase	gular Un oline	leaded
Receipt Assigned	d to:	Tender No:		HDiesel		HSu _l Gaso	oer Unie	aded
Name:				HAvjet		HPre Gase	mium Ui oline	nleaded
Relief:				Quantity		Barrels		Gallons
Assistant:				Height:		Split Tanks		
H 1. Checked H	igh Level Alarms H	Yes H No		Н 3. Си	t Off Loading R	ack Meters		
H 2. Notify Pipel	line Company			H 4. Ga	uged Tanks			
TANK NUMBER	TEMPERATURE (DEGREES F)	PRODUCT HEIGHT (INCHES)	WAT (INCH		NK TO BE FILLED	CHECK HEA VALVE**		ALL VALVES CLOSED
				H Yes				
				H Yes				1
**Any exception.	notify Supervisor (note:	s)	1	11 1 63	11140		1	
H 6. Check Bat H 7. Check All	ipeline Delivery Station tch Delivery Detail with Tank Valves on Same I	Operator Header	lephone	Number:				
H 8. Compute / H 9. Receipt St	Approximate Gauge for	After Receipt				Ft.		
H Check	Header line-up / leaks	<i>w</i>			Gauge Operato		HNo	
	ine Sample: ine – Check Auto Gaug	(time) e			anks Same Hea Sample and Lo			
H 10. Read and	Record Hourly Gauge,	Walk Lines, Ched		ler. H Gravi	ty and Flashpoi			
H 11. At First Hourly Gauge, check all gauges on all tanks connected to the same header. H 12. If tank is to be filled, ask for assistance last 30 minutes of pumping.								
	to be filled, ask for assis to be filled, maintain ste							
H 14. After Rec	eipt is Completed:	•		g .				
	ed and Cleared Pipeline	(1	time)		d Tank Valves(
	l Header Valve al Gauge - Cut Rack Mo	otors		H Kead	and Logged Ai	uto Gauges & Tim	e	
TANK NUMBER	TEMPERATURE			WATER (INCHES)	sA			LSAMPLE ESTED
			40ga				HYes•	and the second s
							HYes	•
						***************************************	HNo	
							HYes•	,
H 16. Log All Data in Gauge Book H Sign with Date and Time								
	esponsibility Reassigne	ed:						
Name: Name:				ate: ate:		Time Time		
Receipt Complet	ed By:			Date:	····		Time:	
				- Onles				

Sample Only

DAILY CHECKLIST	MOTIVA-ENTERPRISES LLC		
	FACILITY REGISTRATION NUMBER 2-1940		
	25 PAIDGE AVE, BROOKLYN, NY 11222		
	23 1 21005 245, 0100016114, 141 11222		
DATE// SHIFT	PERFORMED BY:		
YARD		TIME	STATUS
ļ 	CUMULATION / CREEK FOR SHEEN	THALE	312703
CHECK YARD FOR UNSAFE CON			
CHECK PERIMETER FENCING AN			
MTY GARBAGE PAILS	B Clotting		
CHECK FOG ROOM / FOAM ROOF	A HEATEGR AND DIDING		
}	· · · · · · · · · · · · · · · · · · ·	_	
DRAIN AIR COMPRESSOR YES	NO		
COMMENTS			
DOCK TANK FARM 41-42-43	-44-45-46-47-48-49-50-51-52-53-54-55-9-10	TIME	STATUS
	TORS, FOR UNSAFE CONDITIONS / LEAKS	1	10,,,,,
	IPING, COUPLINGS, FLANGES FOR LEAKS		
CHECK STAIRWAYS / CROSSOVE			
RECEIVING BARGE OR PIPELINE			
CHECK DOCK LINES FOR PRODU			
CHECK DOCK SYSTEM FOR DISC			
	IS OF DEBRIS, EROSION, CRACKS,		***
DISCOLORATION, SIGNS OF SPIL			
COMMENTS			
OWNER O			
	•		
,			
•			
Ĺ			
		TIME	STATUS
VAPOR RECOVERY		TIME	STATUS
DRAIN VAPOR LINE EACH SHIFT	TZ	_	
USE CHECKLIST ONCE PER WEE			
CHECK FOR LEAKS, PRESSURES	, DNSAFE CONDITIONS		,
COMMENTS	The state of the s		
•			
RACKS		TIME	STATUS
CLOSEOUT		1	10111100
CHECK ADDITIVE	SC LEAVO		
CHECK FOR UNSAFE CONDITION			
GROUND CABLES / AIR HOSE OF			
LOADING ARMS / COUPLER CON	DITION ON THE		
COMMENTS			1
MOTIEV SUPERVISOR OF ANY	POOR CONDITIONS IMMEDIATELY		
ACTION SUPERVISOR OF ANT	, CON CONDITIONS IMMEDIATES		
2: C. C. C. C. C. C. C. C. C. C. C. C. C.	POOD IN STATUS		
PLEASE INSERT G = GOOD P =	FOUR IN STATUS		

DIKE DRAINAGE MONTHLY LOG REPORT

DAY OF MONTH	TIME START	TIME FINISH	ZONE NUMBER	VISIBLE SHEEN	OPERATOR ON DUTY
	,				
					A I A W
				•	
					à

ZONE #1 TANKS 47-48 ZONE #2 TANKS 41-42-43-44.

ZONE #3 TANKS 45-46 REAR OF TANKS 40-50

ZONE #4 FRONT OF TANKS 49-50 ZONE #5 OLD UNDERGROUND TANK
FARM

MUST INSPECT ZONE BEFORE PUMPING. IF A SHEEN IS PRESENT DO

NOT PUMP THAT ZONE.

MOTIVA BROOKLYN T	ERMINAL REVISED DIKE VOLUM	IE CALCULATIONS		
By: David O. Martin, Project Coordinator				
Tank No (s):	41/42	Comments		
Dike volume in gallons (from Walter Gorman Calculations)	188,183.93			
Overflow fill volume of largest tank:	88,978.00	Tank 42		
Gallons per foot of smaller tank:	3,360.00	Tank 41		
Avg. dike wall height:	6.912			
Displacement of other tank:	23,224.32	=gallons per foot of smaller tank X avg. dike wall height		
Misc displacement (pipes, pumps, etc)	3,763.68	Assume 2%		
Containment Percentage:	162%	'OK'		

MOTIVA BROOKLYN TERMINAL REVISED DIKE VOLUME CALCULATIONS					
Ву:	David O. Martin, Project Coordinate	or			
Tank No (s):	43/44	Comments			
Dike volume in gallons (from Walter Gorman Calculations)	187,781.5765				
Overflow fill volume of largest tank:	88,912.00	Tank 44			
Gallons per foot of smaller tank:	3,360.00	Tank 43			
Avg. dike wall height:	6.870				
Displacement of other tank:	23,083.20	=gallons per foot of smaller tank X avg. dike wall height			
Misc displacement (pipes, pumps, etc)	3,755.63	Assume 2%			
Containment Percentage:	162%	'ok'			

MOTIVA BROOKLYN	TERMINAL REVISED DIKE VOLUM	E CALCULATIONS
By:	David O. Martin, Project Coordinato	r
Tank No (s):	45/46/7/8/9/10	Comments
Avg. Dike Height:	6.95	
Dike Length:	109.00	
Dike width:	42.00	
Dike Area:	31817.10	
Basin 1 Area	141.67	
Basin 2 Area	125.00	
Basin 3 Area	116.67	
Total Area:	32200.43	
Dike volume in gallons :	240,859.2413	
Overflow fill volume of largest tank:	96,061.00	Tank 45
Gallons per foot of Tank 46	3,360.00	Tank 46
Gallons per foot of Tank 9	647.69	
Gallons per foot of Tank 10	647.69	
Avg. dike wall height:	6.950	
Displacement of Tank 46	23,352.00	=gallons per foot of smaller tank X avg. dike wall height
Divide correct of Tauly 0/42		Active floor of tanks are 50" above dike floor. Area below floor is open for product to enter. Tanks 7 @ 8 are out-of-service and open and will allow
Displacement of Tanks 9/10	2,450.43	product to enter.
Misc displacement (pipes, pumps,		
etc)	4,817.18	Assume 2%
Containment Percentage:	190%	'OK'

Integrated Contingency Plan April 2004

MOTIVA BROOKLYN TERMINAL REVISED DIKE VOLUME CALCULATIONS					
Ву:	By: David O. Martin, Project Coordinator				
Tank No (s):	47	Comments			
Dike volume in gallons (from Walter Gorman Calculations)	519,885.8233				
Overflow fill volume of largest tank:	442,064.00	Tank 47			
Gallons per foot of smaller tank:		N/A			
Avg. dike wall height:	9.260				
Displacement of other tank:	-	=gallons per foot of smaller tank X avg. dike wall height			
Misc displacement (pipes, pumps, etc)	10,397.72	Assume 2%			
Containment Percentage:	115%	'ОК'			

Integrated Contingency Plan April 2004

MOTIVA BROOKLYN TERMINAL REVISED DIKE VOLUME CALCULATIONS					
By:	By: David O. Martin, Project Coordinator				
Tank No (s):	48	Comments			
Dike volume in gallons (from Walter Gorman Calculations)	490,186.6977				
Overflow fill volume of largest tank:	445,126.00	Tank 48			
Gallons per foot of smaller tank:		N/A			
Avg. dike wall height:	6.912				
Displacement of other tank:	-	=gallons per foot of smaller tank X avg. dike wall height			
Misc displacement (pipes, pumps, etc)		Assume None			
Containment Percentage:	110%	'ok'			

MOTIVA BROOKLYN TERMINAL REVISED DIKE VOLUME CALCULATIONS					
By:	David O. Martin, Project Coordinator				
Tank No (s):	49/50 Comments				
Tank 49 Dike volume in gallons (from Walter Gorman Calculations)	497,662.4868				
Tank 50 Dike volume in gallons (from Walter Gorman Calculations)	494,669.5702				
Tank 49 & 50 combined dike volume (connected by overflow)	992,332.0570				
Overflow fill volume of largest tank:	484,039.00	Tank 42			
Gallons per foot of smaller tank:	12,978.00	Tank 41_			
Avg. dike wall height:	8.080				
Displacement of other tank:	104,862.24	=gallons per foot of smaller tank X avg. dike wall height			
Displacement of Tank 53 (horiz. Waste) in gallons:	6,000.00	Max capacity			
Misc displacement (pipes, pumps, etc)	9,893.39	Assume 2%			
Containment Percentage:	164%	'OK'			

Integrated Contingency Plan April 2004

MOTIVA BROOKLYN TER	RMINAL REVISED DIKE VOLUME CA	LCULATIONS		
By: David O. Martin, Project Coordinator				
Tank No (s):	51/54	Comments		
Dike volume in gallons (from Walter Gorman Calculations)	15,625.22			
Overflow fill volume of largest tank:	6,000.00	Tank 51		
Gallons per foot of smaller tank:		N/a		
Avg. dike wall height:	5.400			
Displacement of other tank:	6,000.00	=Max cap. In gallons		
Misc displacement (pipes, pumps, etc)	312.50	Assume 2%		
Containment Percentage:	127%	'OK'		

Motiva Enterprises LLC Brooklyn Terminal Integrated Contingency Plan August 2010

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CONTAINMENT VOLUME CALCULATIONS

ANNEX 8.....REGULATORY COMPLIANCE / CROSS REFERENCE

The following pages contain information required by the regulations that act as documentation, authorization, or certification. Additionally, there are matrices with the specific regulatory requirement, and its corresponding section or page number.

8.1.1 Response Plan Cover Sheet
8.1.2 Facility Substantial Harm Classification
8.1.3 Determination of Worst-Case Discharge
8.1.4 EPA Expanded Cross-Reference
8.2 SPILL PREVENTION, CONTROL, AND COUNTERMEASURE PLAN
8.2.1 Legal Requirements for Preparation and Implementation Applicability
8.2.2 Professional Engineer's Certification and Approval
8.2.3 Terminal Management Certification
Log of Plan Review and Amendments
8.2.4 Qualified Individuals Authority to Initiate Oil Spill Response
8.2.4 Qualified Individuals Authority to Initiate Oil Spill Response 8.2.5 Spill Prevention, Control, and Countermeasure Cross-Reference
8.2.5 Spill Prevention, Control, and Countermeasure Cross-Reference
8.2.5 Spill Prevention, Control, and Countermeasure Cross-Reference
8.2.5 Spill Prevention, Control, and Countermeasure Cross-Reference 8.3 HAZARDOUS WASTE CONTINGENCY PLAN 8.3.1 Distribution Letter to Local Agencies
8.2.5 Spill Prevention, Control, and Countermeasure Cross-Reference 8.3 HAZARDOUS WASTE CONTINGENCY PLAN 8.3.1 Distribution Letter to Local Agencies 8.3.2 Regulatory Cross-Reference

8.1.1.....Response Plan Cover Sheet

This cover sheet will provide EPA with basic information concerning the facility. It must accompany a submitted facility response plan. Explanations and detailed instructions can be found in Appendix F of 40 CFR 112.20. Please type or write legibly in black or blue ink. Public reporting burden for the collection of this information is estimated to vary from 1 hour to 270 hours per response in the first year, with an average of 5 hours per response. This estimate includes time for reviewing instructions searching existing data sources, gathering the data needed, and completing and reviewing the collection of information. Send comments regarding the burden estimate of this information, including suggestions for reducing this burden to: Chief, Information Policy Branch, PM-223, US Environmental Protection Agency, 401 M St., SW, Washington, DC 20460; and to the office of Information and Regulatory Affairs, Office of Management and Budget, Washington, DC 20503.

GENERAL INFORMATION			
Owner / Operator of Facility: Motiva Enterprises LLC			
Facility Name:	Brooklyn Terminal		
Facility Address (street address or route):	25 Paidge Avenue		
City, State, US Zip code:	Brooklyn, NY 11222-1281		
Facility Phone Number:	718-383-4066		
Latitude (Degrees: North):	Longitude (Degrees: West)		
40° 44' 15" N	74° 56' 45" W		
Degrees, minutes, seconds	Degrees, minutes, seconds		
Dun & Bradstreet Number: North American Industry Classification System			
#023838670	(NAICS) Code: 424710		
Largest above-ground Fuel Maximum Storage Capacity Storage Tank Capacity			
(Gallons): 450,000 (Gallons): 2,358,600			
Number of Aboveground Fuel Storage Tanks: <u>18</u>	Worst-case Discharge Amount (Gallons) 450,000		
Facility Distance to Navigable Water. Mar	k the appropriate line.		
0-1/4 mile X 1/4 - 1/2 mile 1/2 - 1 mile >1 mile >1 mile			

Does the facility have a total oil storage capacity greater than or equal to 1 million gallons and, within any storage area, does the facility lack secondary containment that is sufficiently large to contain the capacity of the largest aboveground oil storage tank plus sufficient freeboard to allow for precipitation? YES			f Substantial Harm Criteria or from vessels and does the facility have a total oil 42, 000 gallons?
within any storage area, does the facility lack secondary containment that is sufficiently large to contain the capacity of the largest aboveground oil storage tank plus sufficient freeboard to allow for precipitation? YES	YES _	X	NO
Does the facility have a total oil storage capacity greater than or equal to 1 million gallons and is the facility located at a distance (as calculated using the appropriate formula in Appendix C or a comparable formula) such that a discharge from the facility could cause injury to fish and wildlife and sensitive environments? YESX	within any contain th	y storage area, does the facility la he capacity of the largest aboveg	ack secondary containment that is sufficiently large to
is the facility located at a distance (as calculated using the appropriate formula in Appendix C or a comparable formula) such that a discharge from the facility could cause injury to fish and wildlife and sensitive environments? YESX	YES		NOX
Does the facility have a total oil storage capacity greater than or equal to 1 million gallons and is the facility located at a distance (as calculated using the appropriate formula in Appendix C or a comparable formula) such that a discharge from the facility would shut down a public drinking water intake? YES	is the fac a compar	cility located at a distance (as calc rable formula) such that a dischar	culated using the appropriate formula in Appendix C or
is the facility located at a distance (as calculated using the appropriate formula in Appendix C or a comparable formula) such that a discharge from the facility would shut down a public drinking water intake? YES	YES _	X	NO
Does the facility have a total oil storage capacity greater than or equal to 1 million gallons and has the facility experienced a reportable oil spill in an amount greater than or equal to 10, 000 gallons within the last 5 years? YES	is the fac a compar	cility located at a distance (as calc rable formula) such that a dischar	culated using the appropriate formula in Appendix C or
has the facility experienced a reportable oil spill in an amount greater than or equal to 10, 000 gallons within the last 5 years? YES	YES		NO X
CERTIFICATION I certify under penalty of law that I have personally examined and am familiar with the information submitted in this document, and that based on my inquiry of those individuals responsible for obtaining information, I believe that the submitted information is true, accurate, and complete. Signature: Name: James W. Lintz Please type or print Title: Metropolitan Complex Manager	has the fa	acility experienced a reportable o	
I certify under penalty of law that I have personally examined and am familiar with the information submitted in this document, and that based on my inquiry of those individuals responsible for obtaining information, I believe that the submitted information is true, accurate, and complete. Signature: Name: James W. Lintz Please type or print Title: Metropolitan Complex Manager	YES		NOX
submitted in this document, and that based on my inquiry of those individuals responsible for obtaining information, I believe that the submitted information is true, accurate, and complete. Signature: Name: James W. Lintz Please type or print Title: Metropolitan Complex Manager		CE	ERTIFICATION
Name: James W. Lintz Please type or print Title: Metropolitan Complex Manager	submitted	d in this document, and that base	d on my inquiry of those individuals responsible for
Please type or print Title: Metropolitan Complex Manager	Signature	e:	
	Name:		
Date:	Title:	Metropolitan Complex Manage	<u>r</u>
	Date:		

8.1.2...... Facility Substantial Harm Classification

(This page reserved for substantial harm classification from EPA)

8.1.3...... Determination of Worst-Case Discharge

INSTRUCTIONS

The calculation of a worst-case discharge is used for emergency planning purposes and is required in 112.20 (h)(5)(A) for facility owners and operators who must prepare a response plan. When planning for the amount of resources and equipment necessary to respond to the worstcase discharge planning volume, adverse weather conditions should be taken into consideration. Owners and operators should determine the facility's worst-case discharge from either Part A for onshore storage facilities or Part B for onshore production facilities. The worksheet integrates a facility's use of secondary containment and its proximity to navigable waters. For production facilities, the presence of exploratory wells, production wells, and storage tanks must be considered in the calculation. Part B takes these additional factors into consideration and provides steps for their inclusion in the total worst-case volume. defined in this part, onshore oil production facilities may include all wells, flow lines, separation equipment, storage facilities, gathering lines, and auxiliary non-transportation related-equipment and facilities in a single geographical oil or gas field operated by a single operator. Although a potential worst-case volume is dependent on the risk parameter that results in the higher volume.

Marine transportation-related transfer facilities that contain fixed onshore structures used for bulk oil storage are jointly regulated by both EPA and the U.S. Coast Guard (USCG) and are termed "complexes". Because the USCG also requires response plans from transportation-related facilities to address a worst-case discharge of oil, a separate calculation for the worst-case discharge volume for USCG facilities is included in Annex 3.D.3 and done according to 33 CFR §154.1029. All complexes must compare both calculations for worst-case discharge derived by EPA and USCG and plan for whichever volume is greater.

PART A WORST-CASE DISCHARGE CALCULATION FOR ONSHORE STORAGE FACILITIES

Part A of this worksheet is to be completed by owners or operators of SPCC-regulated facilities (excluding oil production facilities) if the facility meets the criteria as presented in Appendix C to this part or if it is determined by the RA that the facility could cause substantial harm to the environment.

If you are an owner or operator of a production facility, please proceed to Part B.

A.1 .	SINGLE TANK FACILITIES
	For facilities containing only one aboveground storage, the worst-case volume equals the capacity of the storage tank. - FINAL WORST-CASE VOLUME: N/A GAL - Do not proceed further.
A.2.	SECONDARY CONTAINMENT - MULTIPLE TANK FACILITIES Are all aboveground storage tank or groups of aboveground storage tanks at the facility without adequate secondary containment? N(Y/N)
A.2.1	If the answer is yes, the final worst-case volume equals the total aboveground oil storage capacity at the facility. (1) -FINAL WORST-CASE VOLUME: N (Y/N) (2) -Do not proceed any further.
A.2.2	If the answer is no, calculate the total aboveground capacity of tanks without adequate secondary containment. If all aboveground storage tanks or groups of aboveground storage tanks of the facility have adequate secondary containment, ENTER "0" (zero).
A.2.3	Calculate the capacity of the largest single aboveground oil storage tank within an adequate secondary containment area or the combined capacity of a group of aboveground oil storage tanks permanently manifolded together, whichever is greater, PLUS THE VOLUME FROM QUESTION A2.
	FINAL WORST-CASE VOLUME450,000 GAL

1

[&]quot;Storage facilities" represent all facilities subject to this part, excluding oil production facilities.

² Secondary containment is defined in 112.7(e)(2) of the current rule. Acceptable methods and structures for containment are given in 112.7 (c)(1) of the current rule.

³ All complexes that are jointly regulated by EPA and the USCG must also calculate the worst-case discharge planning volume for the transportation related portion of the facility and plan for which ever volume is greater.

PART B: WORST-CASE DISCHARGE PLANNING VOLUME CALCULATION FOR ONSHORE PRODUCTION FACILITIES

Part B of this worksheet is to be completed by owners or operators of SPCC-regulated oil production facilities if they meet the criteria presented in Appendix C to this part, or if it is determined by the RA that the facility could cause harm. A production facility consists of all wells (producing and exploratory) and related equipment in a single geographical oil or gas field operated by a single operator.

B.1 SINGLE-TANK FACILITIES

- B.1.1 For facilities containing only one aboveground oil storage tank, the worst-case discharge planning volume equals the capacity of the aboveground oil storage tank plus the production volume of the well with the highest output at the facility. If adequate secondary containment (sufficiently large to contain the capacity of the aboveground oil storage tank plus sufficient freeboard to allow for precipitation) exists for the storage tank, multiply the capacity of the tank by 0.8.
- B.1.2 For facilities with production wells produced by pumping, if the rate of the well with the highest output is known and the number of days the facility is unattended can be predicted, then the production volume is equal to the pumping rate of the well multiplied by the greatest number of days the facility is unattended.
- B.1.3 If the pumping rate of the well with the highest output is estimated or the unattended is estimated then the production volume is determined from the pumping rate of the well multiplied by 1.5 times the greatest number of days that the facility has been or is expected to be unattended.
- B.1.4 Attachment D-1 to this appendix provides methods for calculating the production volume for explanatory wells and production wells producing under pressure.
- (1) FINAL WORST-CASE VOLUME: N/A GAL
- (2) Do not proceed further.

B.2 SECONDARY CONTAINMENT - MULTIPLE TANK FACILITIES

Are all aboveground storage tanks or groups of aboveground storage tanks at the facility without adequate secondary containment? <u>No.</u> The Brooklyn Terminal does provide for secondary containment.

- B.2.1 If the answer is yes, the final worst-case volume equals the total aboveground oil storage capacity without adequate secondary containment plus the volume of the well with the highest output at the facility.
- (1) For facilities with production wells producing by pumping. If the rate of the well with the highest output is known and the number of days the facility is unattended can be predicted, then the production volume is equal to the pumping rate of the well multiplied by the greatest number of days the facility is unattended.

- (2) If the pumping rate of the well with the highest output is estimated or the maximum number of days the facility is unattended is estimated, the production volume is determined from the pumping rate of the well multiplied by 1.5 times the greatest number of days that the facility has been or is expected to be unattended.
- (3) Attachment D-1 to this appendix provides methods for calculating production volumes for exploratory wells and production wells producing under pressure.
 - (A) FINAL WORST-CASE VOLUME: N/A GAL
 - (B) Do not proceed further.
- B.2.2 If the answer is no, calculate the total aboveground capacity of tanks without adequate secondary containment. If all aboveground storage tanks or groups of aboveground storage tanks at the facility have adequate secondary containment, ENTER "0" (zero).

______0___GAL

- B.2.3 Calculate the capacity of the largest single aboveground oil storage tank with an adequate secondary containment area or the combined capacity of a group of aboveground oil storage tanks permanently manifolded together, whichever is the highest, PLUS THE VOLUME FROM QUESTION B.2.6(b). Attachment D-1 provides methods for calculating the production volumes for exploratory wells and production wells producing under pressure.
 - (A) FINAL WORST-CASE VOLUME: N/A GAL
 - (B) Do not proceed further.

TABLE 1 TO APPENDIX E RESPONSE RESOURCE OPERATING CRITERIA OIL RECOVERY DEVICES

Operating Environment	Sig	Sea State		
River		≤1 foot		1
Inland		≤3 feet		2
Great Lakes		≤4 feet		2-3
Ocean		≤6 feet		3-4
	ВО	OM USE		
Boom Property	River	Inland	Great Lakes	Ocean
Significant Wave Height	<1	<3	<4	≤6
Sea State	1	2	2-3	3-4
Boom height - in. (draft) plus freeboard)	10-18	18-42	18-42	≥42
Reserve Buoyancy to Weight Ratio	2:1	2:1	2:1	3:1 to 4:1
Total Tensile Strength - lbs.	4,500	15-20,000	15-20,000	≥20,000
Skirt Fabric Tensile Strength - lbs.	200	300	300	500
Skirt Fabric Tear Strength - lbs.	100	100	100	125

TABLE 3 EMULSIFICATION FACTORS FOR OIL PRODUCT GROUPS

NON-PERSISTENT OIL	
GROUP 1	1.0
PERSISTENT OIL	
GROUP 2	2.5
GROUP 3	3.0
GROUP 4	1.8

TABLE 4
ON-WATER OIL RECOVERY RESOURCE MOBILIZATION FACTORS

Operating Area	<u>Tier 1</u>	Tier 2	Tier 3
River & Canals	.30	.40	.60
Inland / Nearshore / Great Lakes	.15	.25	.40
Offshore	.10	.165	.21

Note: These mobilization factors are for total resources mobilized; not incremental resources.

TABLE 5 RESPONSE CAPABILITY CAPS BY GEOGRAPHIC AREA

February 18, 1993 All except rivers, canals, Great Lakes	<u>Tier 1</u> 10K	<u>Tier 2</u> 20K	<u>Tier 3</u> 40K
Great Lakes	5K	10K	20K
Rivers & Canals	1,500	3,000	6,000
February 18, 1998 All except rivers, canals, & Great Lakes	12.5K	25K	50K
Great Lakes	6.35	12.3	25
Rivers & Canals	1,875	3,750	7,500

Note: The caps show cumulative overall effective daily recovery rate, not incremental increases. This table updated to conform to EPA Final Rule 40 CFR 112-July 1, 1994.

TABLE 2
REMOVAL CAPACITY PLANNING TABLE

Spill Location	Nearshore / Inland			River 3 days		
Sustainability of on-water recovery	4 days					
Oil Group	% Natural Dissipation	% Recovered Floating Oil	% Oil Onshore	% Natural Dissipation	% Recovered Floating Oil	% Oil Onshore
1 Nonpersistent Oils	80	20	10	80	10	10
2 Light Crudes and Fuels	50	50	30	40	15	45
3 Medium Crudes and Fuels	30	50	50	20	15	65
4* Heavy Crudes, Fuel Residuals	10	50	70	5	20	75

For planning purposes, non-petroleum oil must be considered a Group 4 persistent oil.

Attachment 8.1.3.1

Worksheet for Determining Planning Volume for Response Resources for Worst-case Discharge Brooklyn Terminal

	odiid illioliiladioi.					
p (A) Ca	alculate Worst-Cas	e Discharge	in barrel	s (Appendi)	k D)	10,714
p (B) Oi	il Group** (Table 3	and Section	1.2 of th	is Appendix	()	1
p(C) Ge	eographic Area (ch	oose one)	X /			or Rivers and Canals
t to Natu 80	ral Dissipation	,	red Float 20 (D2)	ing Oil	% Oil	Onshore 10 (D3)
p (E1) Oı	n-Water Recovery	Step ((D2) x Ste 100	<u>ep (A)</u>		2,143
p (E2) Oı	n-Shore Recovery	Step ((D3) x Ste 100	<u>ep (A)</u>		1,071
p (F) Er	mulsification Factor	(Table 3)				1.00
p (G) Oı	n-Water Oil Recove	ery Resource	e Mobiliza	ation Factor	r (Table 4)
Tie	er 1	Tie	er 2			Tier 3
0.	15	0.:	25			0.40
(G	61)	(G	62)			(G3)
	p (A) Cap (B) Of p (C) Go (D) P (E1) Of p (E2) Of p (F) Er p (G) Of Ti O.	p (A) Calculate Worst-Case p (B) Oil Group** (Table 3 p (C) Geographic Area (ch p (D) Percentages of Oil (Total to Natural Dissipation 80 (D1) p (E1) On-Water Recovery p (E2) On-Shore Recovery p (F) Emulsification Factor	p (B) Oil Group** (Table 3 and Section p (C) Geographic Area (choose one) p (D) Percentages of Oil (Table 2) to Natural Dissipation % Recover 80 (D1) p (E1) On-Water Recovery Step (Part of the Control of the Contro	p (A) Calculate Worst-Case Discharge in barrels p (B) Oil Group** (Table 3 and Section 1.2 of the p (C) Geographic Area (choose one) p (D) Percentages of Oil (Table 2) t to Natural Dissipation 80 20 (D1) (D2) p (E1) On-Water Recovery Step (D2) x Stere 100 p (E2) On-Shore Recovery Step (D3) x Stere 100 p (F) Emulsification Factor (Table 3) p (G) On-Water Oil Recovery Resource Mobilization Tier 1 Tier 2 0.15 0.25	p (A) Calculate Worst-Case Discharge in barrels (Appendix p (B) Oil Group** (Table 3 and Section 1.2 of this Appendix p (C) Geographic Area (choose one) X	p (A) Calculate Worst-Case Discharge in barrels (Appendix D) p (B) Oil Group** (Table 3 and Section 1.2 of this Appendix) p (C) Geographic Area (choose one) X Nearshore / Inland / Great Lakes p (D) Percentages of Oil (Table 2) t to Natural Dissipation % Recovered Floating Oil % Oil 80 20 (D1) (D2)

1 1

^{**} Facilities storing multiple groups of oil should prepare a separate worksheet for each group that comprises 10% or more of the volume of the facility. All oil volumes or all oils must be totaled for percentage determinations.

Attachment 8.1.3.1 (continued)

Worksheet for Determining Planning Volume for Response Resources for Worst Case Discharge (continued)

Part II On-Water Recovery Capacity (barrels / day)

Tier 1		Tier 2	Tier 3
321		536	857
Step (E1) x	(Step (F) x Step (G1)	Step (E1) x (Step (F) x Step (G2)	Step (E1) x (Step(F) x Step (G3)
Part III	Shoreline Cleanu	p Volume (barrels / day	1,071
Part IV		ity By Geographic Area (Table 5) to be contracted for, barrels / day)	Step (E2) x (Step(F)
•	Tier 1	Tier 2	Tier 3
	12,500	25,000	50,000
	(J1)	(J2)	(J3)
Part V	Amount needed to (barrels / day)	o be identified, but not contracted fo	<u>r in advance</u>
	Tier 1 0	Tier 2	Tier 3 0
Part II	Гier I - Step (J1)	Part II Tier 2 - Step (J2)	Part II Tier 3 - Step (J3)

1 1

NOTE: To convert to gallons / day, multiply Part II-Part V by 42.

8.1.4..... EPA Expanded Cross-Reference (40 CFR 112.20)

BASED ON APPENDIX F FACILITY-SPECIFIC RESPONSE PLAN

		LOCATION
1.1 E	mergency Response Action Plan (ERAP) consisting of:	EUGATION
1.	Qualified Individual Information	Core Plan
2.	Emergency Notification Phone List	Core Plan
3.	Spill Response Notification Form	Core Plan
4.	Response Equipment List and Location	Core Plan 1.1.4.1 Annex 3.e.6 OSRO dependent
5.	Response Equipment Testing & Development	Core Plan 1.1.4.1 Annex 3.e.6 OSRO dependent
6.	Facility Equipment Testing & Deployment	Core Plan
7.	Evacuation Plan	Core Plan, Diagram in Annex
8.	Immediate Actions	Core Plan
9.	Facility Actions	Core Plan
1.2 Fac	cility Information including:	
1.	Facility Name and Location	Introduction 1.2
2.	Latitude and longitude	Introduction 1.2
3.	Location and drainage to a Wellhead Protection Area	Introduction 1.2
4.	Owner / Operator Information	Introduction 1.2
5.	Qualified Individual name with authority to implement the Plan	Introduction 1.2, Core Plan 1.1.2
6.	Date of oil storage start-up	Introduction 1.2
7.	Description of current facility operations	Introduction 1.2
8.	Dates and types of substantial expansions	Introduction 1.2
1.3 Em	ergency Response Information including:	
1.	Notification Phone List & Notification Form	Core Plan 1.1.2, 1.1.3, Annex 2
2.	Equipment List	Core Plan; 1.1.4
3.	Equipment Testing / Deployment	Core Plan 1.1.4.1, Annex 3.e.6, OSRO dependent, Annex 11
4.	Personnel	Core Plan, Annex 3a
5.	Evacuation Plan	Core Plan 1.1.6, Annex 1, Figure 1.3
6.	Qualified Individual Duties	Annex 3a, 3b
1.4 Haz	zard Evaluation including:	
1.4	.1. Hazard Identification	Annex 7.1
	List each aboveground tank and below ground tank.	Table 7.1
	3.a. Identify each tank or SI that stores oil or hazardous materials.	Table 7.1
	3.b&c. Substance, quantity stored.	Table 7.1
	3.d. Tank type / surface, area; year.	Table 7.1

3.e.	Maximum capacity.	LOCATION Table 7.1
3.e. 3 f.	Record of tank failures / causes.	Table 7.1
4.	Schematic drawing using above information on tanks.	Annex 1, Figure 1.2
5.	Description of Facility Operations:	Annex 7
	 Description of loading and unloading of transportation vehicles that risk the release of oil during transfer processes. Include all transfer processes for trucks, railroad cars, vessels. 	Annex 7.1.8
	υ Identify operations that may present a risk of release.	Annex 7.1
	υ Secondary containment volume associated with each tank and transfer point at the facility.	Annex 7.2
	ບ Normal daily throughput and effect on potential release volumes that a negative or positive change in that throughput may	Annex 7.6
	rability Analysis: Potential effects to human health, rty, environment of spill.	
1. Wa	ter intakes	Annex 3.d
2. Sc	hools	Annex 3.d
3. Me	edical facilities	Annex 3.d
4. Re	esidential areas	Annex 3.d
5. Bu	sinesses	Annex 3.d
6. We	tlands and environmentally sensitive areas	Annex 3.d
7. Fis	sh and wildlife	Annex 3.d
8. La	kes and streams	Annex 3.d
9. En	dangered flora and fauna	Annex 3.d
10. Re	ecreational areas	Annex 3.d
11. Tra	ansportation routes (air, land, water)	Annex 3.d
12. Uti	ilities	Annex 3.d
	onomically sensitive areas including: terrestrially sensitive vironments, aquatic environments, and unique habitats.	Annex 3.d
	sis of the Potential for a Spill based on these factors:	
ს Tan	k age,	Table 7.1, Annex 3d
υ Spil	l history,	Annex 4.2; 3d
υ Hor	izontal range of spill, and	Annex 3.d.4
n Vuit	nerability to natural disaster.	Annex 3.d.1

	LOCATION
.4.4 Spill History description including:	
1. Date of spill	Annex 4.2
2. Cause,	Annex 4
3. Material spilled,	Annex 4
4. Amount in gallons,	Annex 4
Amount that reached navigable waters,	Annex 4
Effectiveness and capacity of secondary containment,	Annex 4
7. Clean-up actions taken,	Annex 4
Steps taken to reduce recurrence,	Annex 4
Total storage capacity of tanks or impoundments from which spill occurred.	Annex 4
10. Enforcement actions,	Annex 4
11, Effectiveness of monitoring equipment, and	Annex 4
12, Description of how each spill was detected.	Annex 4
5 Response Scenarios information needed:	
1.5.1 Small spill / Medium Spill	Core Plan, Annex 3.d.4
υ Response equipment to be used for each scenario.	Core Plan, Annex 3.d.4
υ Mitigation and response actions to be used in each scenarios.	Core Plan, Annex 3.d.4
1.5.2 Worst-case scenario	Core Plan, Annex 3.d.4
.6 Discharge Detection Systems including text on:	
1.6.1 Procedures and equipment used to detect spills, and types of spill detection by personnel	Annex 7.4-7.7
1.6.2 Automated spill detection and frequency of inspection of all systems	Annex 7.4 - 7.5.5; 7.7.1; 7.7.2
7 Plan Implementation covering:	
1.7.1 Response resources for small, medium, worst-case spills.	Annex 3.d; 3.d.3.3 - 3.d.5
1.7.1.1 Emergency plans of spill response	Core Plan, Annex 3.c; 3.d; 3.d.3.3 - 3.d.5
1.7.1.2 Additional response training	Core Plan, Annex 3.c; 3.d; 3.d.3.3 - 3.d.5
1.7.1.3 Additional contracted help	Core Plan, Annex 3.c; 3.d; 3.d.3.3 - 3.d.5
1.7.1.4 Access to additional response equipment / experts	Core Plan, Annex 3.c
1.7.1.5 Ability to implement the Plan including response training and practice drills	Annex 3.c.2; Annex 5
Disposal plans-description of how and where the facility intends to recover, reuse, decontaminate, or dispose of materials after a spill	Annex 3.d.5

	T
	LOCATION
1.7.3 Containment and drainage planning including:	Annex 3.c.3; Annex 7.1.5, 7.2
1.7.3.1 Available volume of containment	Annex 7 - Table 7.1; Annex 7.2.1
1.7.3.2 Route of drainage from storage and transfer areas,	Annex 7.1.5; Drainage Diagram in Annex 1
1.7.3.3 Construction materials of drainage troughs	NA
1.7.3.4 Type and number of valves and separators used in the drainage system,	Annex 7.1.5
1.7.3.5 Sump pump capacities	Annex 7.1.5
1.7.3.6 The containment capacity of weirs and booms, location of all,	NA
1.7.3.7 Other cleanup materials	OSRO dependent
1.8 Self-Inspection, Drills / Exercises and Response Training	
1.8.1 Facility self-inspection, including checklists and records of inspection, meeting logs, etc.	Annex 7.7.1
1.8.1.1 Tank Inspection	Annex 7.7
1.8.1.2 Response Equipment Inspection	Annex 7.7
1.8.1.3 Secondary Containment Inspection	Annex 7.7
1.8.2 Facility Drills / Exercises	Annex 5
υ Internal Exercise	Annex 5
υ QI notification drills	Annex 5
ບ Spill Management Team Tabletop Exercise	Annex 5
υ Equipment Deployment Exercise	Annex 5
ບ Unannounced Drills	Annex 5
υ External Exercises	Annex 5
υ Area Exercises	Annex 5
1.8.3 Response Training	Annex 5
1.8.3.1 Personnel Response Training Logs	Annex 5
1.8.8.2 Discharge Prevention Meeting Logs	Annex 5
1.9 Diagrams and Plot Plans of the facility:	
1.9.1 Detailed Plot Plan	Core Plan 1.1.8; Annex 1, Figure 1.2
1.9.2 Site Drainage Plan Diagram	Annex 1
1.9.3 Site Evacuation Diagram	Annex 1
1,10 Security including:	
1.10.1 Emergency cut-off locations	Annex 3.e.2.3 Annex 1, Figure 1.2, Annex 7.4.2
1.10.2 Enclosures (e.g., fencing)	Annex 3.e.2.1

	LOCATION
1.10.3 Guards, their duties, day and night,	Annex 3.e.2.6, Core Plan 1.1.6.3
1.10.4 Lighting,	Annex 3.e.2.5
1.10.5 Valve and pump locks	Annex 3.e.2.2
1.10.6 Pipeline	Annex 3.e.2
2.0 Response Plan Cover Sheet Information including:	
υ Facility Name	Annex 8.1.1
υ Facility Address	Annex 8.1.1
υ Facility Phone Number	Annex 8.1.1
υ Latitude and Longitude	Annex 8.1.1
υ Dun & Bradstreet Number	Annex 8.1.1
υ Standard Industrial Classification (SIC) Code	Annex 8.1.1
υ Largest Oil Storage Tank Capacity	Annex 8.1.1
υ Maximum Oil Storage Capacity	Annex 8.1.1
υ Number of Oil Storage Tanks	Annex 8.1.1
υ Worst-Case Discharge Amount	Annex 8.1.1
υ Facility Distance to Navigable Water	Annex 8.1.1
υ Applicability of Substantial Harm Criteria	Annex 8.1.1
υ Certification	Annex 8.1.1

8.2..... SPILL PREVENTION CONTROL AND COUNTERMEASURE (40 CFR 112.7)

8.2.1..... Legal Requirements for Preparation and Implementation Applicability

This is a Spill Prevention, Control, and Countermeasure Plan to be used by the Brooklyn Terminal in responding to and reporting a petroleum discharge or substantial threat of a petroleum discharge into the navigable waters or adjoining shorelines of the United States or the State of New York. The requirement for this Plan is found in the Code of Federal Regulations, Title 40, Part 112.

This Plan has been developed to fully address the regulatory requirements of the Federal Spill Prevention, Control and Countermeasure Regulation; U. S. EPA Final Rule for Oil Pollution Prevention; Non-Transportation Related On-Shore and Off-Shore Facilities (40 CFR 112 – as amended on November 13, 2009). When accompanied by the OPA-90 Plan, this document and the OPA-90 Plan fulfill the requirements of 40 CFR Part 112.

All facilities that have the potential to discharge harmful quantities of oil into or onto the navigable waters of the United States, which have more than 1,320 gallons of aboveground storage, or a total underground storage capacity which exceeds 42,000 gallons are required to have a Spill Prevention, Control, and Countermeasure Plan. This facility meets those criteria. Harmful quantities of oil are defined in 40 CFR 110 as a visible sheen on the surface of the water or shoreline, or which are in excess of permit quantities for those facilities that have a limit in their facility NPDES Permit.

As the owners or operators of this Facility, Motiva Enterprises LLC will maintain a complete copy of this Spill Prevention, Control, and Countermeasure portion of this Plan at the Facility and will make the Plan available to the Regional Administrator or authorized representative of the Environmental Protection Agency for on-site review during normal working hours. A complete copy is maintained at the Facility because the Facility is manned at least four (4) hours per day. A complete copy is maintained at the Facility because the Facility is manned at least four hours a day.

In the event that this facility discharges more than 1,000 gallons of oil into or upon the navigable waters of the United States or adjoining shorelines in a single event, or discharges more than 42 gallons of oil upon the navigable waters of the United States or adjoining shorelines in two reportable spill events within any twelve month period, the owner or operator of this facility will submit the following information to the Regional Administrator of the Environmental Protection Agency within 60 days.

1

- 1. Name of facility
- 2. Name of owner / operator
- 3. Location of facility
- 4. Maximum storage or handling capacity of the Facility and normal daily throughput
- 5. Corrective action and countermeasures including description of equipment repairs and replacements
- 6. Description and maps of facility
- 7. Cause of such discharge including failure analysis of the system
- 8. Additional prevention measures taken or contemplated
- 9. Other information as required by the RA pertinent to the Plan or discharge

8.2.2...... Professional Engineer's Certification and Approval

PROFESSIONAL ENGINEER CERTIFICATION

By means of this Professional Engineer Certification, I hereby attest to the following:

- I am familiar with the requirements of 40 CFR Part 112 and have verified that this Plan has been prepared in accordance with the requirements of this Part.
- I or my agent have visited and examined the Facility(s).
- I have verified that this Plan has been prepared in accordance with good engineering practice, including consideration of applicable industry standards.
- I have verified that the required inspection and testing procedures have been established as described in Annex 7.
- I have verified that the Plan is adequate for the Facility.
- My certification of this Plan in no way relieves the owner/operator of the Facility(s) of their duty to prepare and fully implement the Plan in accordance with the requirements of 40 CFR Part 112. I in no way assume any liability of whatsoever kind of nature by my certification.
- The owner/operator, by "Management Approval" located on the following page, acknowledges this certification and the compliance measures described herein.
- This certification is limited to the sections referenced in the Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.7) cross reference table located in Section 8.2.5.

(Seal)



Date: _____**SEP 23 2010**

Registered Professional Engineer

Robert P. Perla, P.E. RPMS Consulting Engineers

State of New York

Registration No: 054709

8.2.3...... Terminal Management Certification

MAN	NAGEMENT APPROVAL
Owner/Operator responsible for Facility: • Facility Name and Location:	Motiva Enterprises LLC Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222-1281
	proves this Plan and acknowledges that the elements mplemented, including a commitment to expend money and cleanup oil spills.
This page may be used for the initial management and/or change of design	al Management Approval or for subsequent change of ated person accountable.
This SPCC Plan will be implemented	as herein described.
Signature: Janus W. L	Designated person accountable for oil spill prevention at the Facility:
Name: James W. Lintz	Name: James W. Lintz
Date: 4-10-08	Title: Metropolitan Complex Mgr
Title: Metropolitan Complex Mgr	
	•
This SPCC Plan will be implemented a	as herein described.
Signature:	Designated person accountable for oil spill prevention at the Facility:
Name:	Name:
Date:	Title:
Title:	
•	
This SPCC Plan will be implemented a	as herein described.
Signature:	Designated person accountable for oil spill prevention at the Facility:
Name:	Name:
Date:	Title:
Title:	

Annex 8, Page 22a

8.2.3...... Terminal Management Certification (Cont'd)

LOG OF PLAN REVIEW AND AMENDMENTS

NON TECHNICAL AMENDMENTS

Non-technical amendments are not certified by a Professional Engineer.

Examples of changes include, but are not limited to, phone numbers, name changes, or any non-technical text change(s).

TECHNICAL AMENDMENTS

- Technical amendments are certified by a Professional Engineer.
- Examples of changes include, but are not limited to, commissioning or decommissioning containers; replacement, reconstruction, or movement of containers; reconstruction, replacements, or installation of piping systems; construction or demolition that might alter secondary containment structures; changes or product or service; or revision of standard operation or maintenance procedures at a Facility.
- An amendment made under this section will be prepared within six (6) months of the change and implemented as soon as possible but not later than six (6) months following preparation of the amendment.

MANAGEMENT REVIEW

Management will review this SPCC Plan at least each five (5) years and document the review on the form below.

Review/ Amend Date,	Signature	Amend Plan (will/will not)	Description of Review Amendment	Affected Page(s)	P.E. Certification (Y/N)
3/1/10.	Twite	> 10			<u> </u>

8.2.4 Qualified Individuals Authority to Initiate Oil Spill Response – 10/98

Pursuant to the Oil Pollution Act of 1990 (OPA), State Oil Spill Response laws and Federal and State regulations under Federal and State Oil Spill Response statutes, authority to sign Notices of Federal Interest for an Oil Pollution Incident (or their equivalent), Notices of State Interest for an Oil Pollution Incident (or their equivalent), designation of responsible party for an oil spill, authority to approve witness statements, and authority to initiate oil spill response activities is hereby assigned and delegated to persons occupying and acting in the capacity of the positions as specified below in accordance with such facilities' Oil Spill Response Contingency Plans and/or the Company's Regional Response Teams.

- 1. At marketing terminals: Terminal Manager, Complex Manager, Superintendents, or in their absence, Assistance Terminal Managers, Terminal Supervisors, Terminal Operators, Regional Managers, Regional Response Team On-Scene Coordinator.
- 2. For all other locations: Manager, LSDR/HSE and Emergency Management, or any officer of the Company. Any employee of the Company serving on the Regional Response Teams or performing work required by the Regional Response Plans has necessary authority to perform their work in accordance with the objectives established with the Alliance of Shell and Saudi Refining, Inc. Limitations on approval amounts are governed by Motiva's Delegation of Authority.

8.2.5 Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference

40 CFR § 112	BRIEF DESCRIPTION	SECTION
112.3	Requirements for preparation and implementation of Spill Prevention Control and Countermeasure Plan	
(a,b,c)	Owners or operators and could reasonably be expected to have a discharge oil as describedmust prepare and implement a Plan	Sec. III, Annex 8.2.1
(d)	A licensed Professional Engineer must review and and certify a Plan for it to be effective	Sec. III, Annex 8.2.2 (PE Certification)
(e)	Maintain a complete copy of the Plan at the facility if the facility is normally attended at least 4 hours per day, or at the nearest field office	Sec. III Annex 8.2.1
112.5	Amendment of Spill Prevention Control and Countermeasures Plans by owners or operators	
(a)	Amend the SPCCwhen there is a change in facility design, construction, operation or maintenance which materially affects the facility's potential for the discharge of oil	Sec. III, Annex 8.2.3.a
(b)	complete a review and evaluation of the SPCC at least once every five years amend the SPCC within six months of the reviewimplement within six months of preparation of any amendment.	Sec. III, Annex 8.2.3.a
(c)	Have a Professional Engineer certify any technical amendment	Sec. III, Annex 8.2.2
112.7	Guidelines for the preparation and implementation of a Spill Prevention Control and Countermeasures Plan	M-1-10
	must prepare a Planhave full approval of managementin writing.	Sec. 1 Introduction 1.1 Sec. III, Annex 8.2.3
	If the plan calls for additional facilities or procedures, methods, or equipment not yet fully operational, these items should be discussed in separate paragraphs, and the details of installation and operational start-up should be explained separately.	
	follow the sequence specified (or cross-reference)	Sec. III, Annex 8.2.5
(a)(2)	Comply with all applicable requirements in this part [or] state reasons for non-conformance and describe alternate methods	Sec. III, Annex 8.2.1
(a)3)	Describe physical layout and include diagram	Sec. I, Intro. 1.2.7; Sec. II, Core Plan, Figure 1.2; Sec. III Annex 1 Fig 1.2
(a)(3)(i)	[address in your Plan] the type of oil in each container and its capacity	Sec. III. Annex 7 Table 7-1
(a)(3)(ii)	discharge prevention measures including routine handling of products	Sec. III. Annex 7.1.8
(a)(3)(iii)	Drainage or discharge controls and procedures for control of a discharge	Sec. III. Annex 7.1.5, 7.1.6, 7.2.7
(a)(3)(iv)	Countermeasures for discharge discovery, response, and cleanup (both facility's and contractor)	Sec. II, Core Plan 1.1.7
(a)(3)(v)	Methods of disposal of recovered materials	Sec. III, Annex 3.d.6
(a)(3)(vi)	Contact list and phone numbers	Sec. II, Core Plan 1.1.2
(a)(4)	Relate information [on a discharge]	Sec. II, Core Plan 1.1.3
(a)(5)	Organize portions of the Plan that will make them readily usable	Core Plan, Section Dividers
(b)	Where experience indicates a reasonable potential for equipment failureinclude a prediction	Sec. III, Annex 7 Table 7-1

8.2.5...... Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference (Cont'd)

40 CFR § 112	BRIEF DESCRIPTION	SECTION
(c)(1)	Onshore facilities.	Sec. III, Annex 7.2.
(c)(1)(i)	Dikes, berms or retaining walls sufficiently impervious to contain spilled oil	Sec. III, Annex 7.2.2
(c)(1)(ii)	Curbing	Sec. III, Annex 7.2.3
(c)(1)(iii)	Culverting, gutters or other drainage systems	Sec. III, Annex 7.2.4
(c)(1)(iv)	Weirs, booms or other barriers	N/A
(c)(1)(v)	Spill diversion ponds	Sec. III, Annex 7.2.5
(c)(1)(vi)	Retention ponds	Sec. III, Annex 7.2.5
(c)(1)(vii)	Sorbent materials	Sec. III, Annex 7.2.6
(c)(2)	Offshore Facilities.	
(c)(2)(i)	Curbing, drip pans	N/A
(c)(2)(ii)	Sumps and collection systems	N/A
(d)	If you determine that the installation of structures or equipment listed in paragraphs (c) and (h)(1) of this sectionis not practicableclearly explain in your Planand provide	
(d)(1)	A strong oil spill contingency plan following40 CFR 109.	Entire Plan
(d)(2)	A written commitment of manpower, equipment and materials required to expeditiously control and remove any harmful quantity of oil discharged.	Sec. III, Annex 8.2.3
(e)	Inspections and records	
,	in accordance with written procedures that you or the certifying engineer developwith the SPCC Plan for a period of three years.	Sec. III, Annex 7.7.2, 7.7.3.8
(f)	Personnel, training and spill prevention procedures	
(f)(1)	train your oil-handling personnel in the operation and maintenance of equipment to prevent the discharges	Sec. III, Annex 5.2.2
(f)(2)	Designate a personaccountable for oil spill prevention	Sec. III, Annex 8.2.3
(f)(3)	Schedule and conduct spill prevention briefingshighlight and describe known spill dischargesor failures, malfunctioning components, and recently developed precautionary measures.	Sec. III, Annex 5.2.3
(g)	Security (excluding oil production facilities)	Sec. III, Annex 3.3.2
(h)	Facility tank car and tank truck loading/unloading rack	
(h)(1)	Where loading/unloading area drainage does not flow into a catchment basin or treatment facility designed to handle discharges, use a quick drainage systemdesign any containment system to hold at least maximum capacity of any single compartment of a tank car or tank truck loaded or unloaded at the facility.	Sec. III, Annex 7.1.8.4
(h)(2)	Provide an interlocked warning light or physical barrier system, warning signs, wheel chocks, or vehicle break to prevent vehicular departure before complete disconnect of flexible or fixed oil transfer lines.	Sec. III, Annex 7.1.8.4.b
(h)(3)	Prior to filling and departure of any tank car of tank truck, closely inspect for discharges the lowermost drain and all outlets of such vehicles should be closely examined for leakage, and if necessary, that they are tightened, adjusted, or replaced to prevent liquid leakage while in transit.	Sec. III, Annex 7.1.8.4.c
(i)	If a field-constructed aboveground container undergoes a repair, alteration, reconstruction, or change in service that might affect the risk of a discharge or failure due to brittle fractureevaluate the container for risk	Sec. III, Annex 7.7.3.4
(i)	In additioninclude a complete discussion of conformance with applicable requirementsor any more stringent, with State rules, regulations and guidelines.	Sec. III, Annex 7.8

8.2.5...... Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference (Cont'd)

40 CFR § 112	BRIEF DESCRIPTION	SECTION
(k)	Qualified Oil-filled Operation Equipment	
(k)(1)	Qualification Criteria – Reportable Discharge History: The owner or operatorthat has had no discharges as described in § 112.1(b) from any oil-filled operational equipment; and	N/A
(k)(2)	Alternative Requirements to General Secondary Containment. If secondary containment is not provided for qualified oil-filled operational equipment pursuant to paragraph (c) of this section, the owner or operator of a facility with qualified oil-filled operational equipment must:	N/A
(k)(2)(i)	Establish and document the facility procedures for inspections or a monitoring program to detect equipment failure and/or a discharge; and	N/A
(k)(2)(ii)	Unless you have submitted a response plan under § 112.20, provide in your Plan the following:	N/A
(k)(2)(ii)(A)	An oil spill contingency plan following the provisions of part 109 of this chapter,	N/A
(k)(2)(ii)(B)	A written commitment of manpower, equipment, and materials required to expeditiously control and remove any quantity of oil discharged that may be harmful.	N/A
112.8	Spill Prevention, Control, and Countermeasure Plan requirements for onshore facilities (excluding production facilities)	
(a)	Meet the general requirements for the Plan listed under § 112.7, and	
(b)(1)	Restrain drainage from diked storage areas by valves or other positive means to prevent a spillinto the drainage system or inplant effluent treatment system, except where plan systems are designed to handle such leakage. You may empty diked areas by pumps or ejectors; however you must be manually activate these pumpsand inspect the condition of the accumulation before starting	Sec. III, Annex 7.2.7, 7.2.8
(b)(2)	Use valves of manual, open-and-closed design If facility drainage drains directly into water courseyou must inspect and drain uncontaminated retained stormwater, as provided inparagraphs (c)(3)(ii)(iii), and (iv).	Sec. III, Annex 7.2.7, 7.2.8
(b)(3)	Design facility drainage systems from undiked areas to flow into ponds, lagoons or catchment basins, designed to retain oil or return it to the facility. You must not locate catchment basins in areas subject to periodic flooding.	Sec. III, Annex 7.1.6
(b)(4)	Ifnot engineered as in paragraphs (b)(3), equip the final discharge of all ditches with a diversion system that wouldretain the oil in the facility.	Sec. III, Annex 7.1.6
(b)(5)	Where drainage waters are treated in more than one treatment unit provide two "lift" pumps and permanently install at least one of the pumps. Whatever techniques are used, facility drainage systems engineer to prevent a discharge as described in § 112.1(b) in case there is an equipment failure or human error	Sec. III, Annex 7.2.7
(c)	Bulk storage containers (onshore)	
(c)(1)	Not use a container for the storage of oil unless its material and construction are compatible with the material stored and conditions of storage	Sec. III, Annex 7.3.1
(c)(2)	Construct all bulk storage container installations so that you provide a secondary means of containment for the entire contents of the largest single container plus sufficient freeboard to allow for precipitation. You must ensure that diked areas are sufficiently impervious to contain discharged oil.	Sec. III, Annex 7.2.1, 7.2.2
(c)(3)	Not allow drainage of uncontaminated rainwater from the diked area into a storm drain or discharge of an effluent discharge into an open water course, lake, or pond, bypassing the in-plant treatment system unless you:	Annex 7.2.7
(c)(3)(i)	Normally keep the bypass valve sealed closed.	Sec. III, Annex 7.2.7
(c)(3)(ii)	Inspect the retained rainwater to ensure that its presence will not cause a discharge as described in § 112.1(b).	Sec. III, Annex 7.2.7
(c)(3)(iii)	Open the bypass valve and reseal it following drainageunder responsible supervision.	Sec. III, Annex 7.2.7

8.2.5...... Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference (Cont'd)

40 CFR § 112	BRIEF DESCRIPTION	SECTION
(c)(3)(iv)	Keep adequate records of such events.	Sec. III, Annex 7.2.7
(c)(4)	Protect any completely buried metallic storage tank installed on or after January 10, 1974 from corrosion by coatings or cathodic protection	Sec. III, Annex 7.3.4
(c)(5)	Not use partially buried metallic tanks for the storage of oil should be avoided, unless the buried section of the shell is adequately coated	Sec. III, Annex 7.3.5
(c)(6)	Test each aboveground container for integrity testing on a regular Keep comparison records In additionfrequently inspect the outside of the container for signs of deterioration, discharges, or accumulation of oil inside diked areas. Records of inspections and tests kept under usual and customary business practices will suffice for the purposes of this paragraph.	Sec. III, Annex 7.7
(c)(7)	Control leakage through defective internal heating coils by monitoring the steam return and exhaust lines	Sec. III, Annex 7.3.7
(c)(8)	Engineer or update each container installation in accordance with good engineering practice to avoid discharges (and) provide at least one of the following devices:	
(c)(8)(i)	High liquid level alarms with an audible or visual signal at a constantly attended operation or surveillance station. In smaller facilities, an audible air vent may suffice.	Sec. III, Annex 7.4.1
(c)(8)(ii)	High liquid level pump cutoff devices set to stop flow at a predetermined container content level.	Sec. III, Annex 7.4.2
(c)(8)(iii)	Direct audible or code signal communication between the container gauger and the pumping station.	Sec. III, Annex 7.4.3
(c)(8)(iv)	A fast response system for determining the liquid level of each bulk storage container such as digital computers, telepulse, or direct vision gauges.	Sec. III, Annex 7.4.4
(c)(8)(v)	You must regularly test liquid level sensing devices to ensure proper operation.	Sec. III, Annex 7.4.1
(c)(9)	Observe effluent treatment facilities frequently enough to detect possible system upsets that could cause a discharge	Sec. III, Annex 7.4.1
(c)(10)	Promptly correct visible discharges which result in a loss of oil from container includingseam, gaskets, piping, pumps, valves	Sec. III, Annex 7.4.5
(c)(11)	Position or locate mobile or portable oil storage container to prevent a discharge as described in § 112.1(b)furnish a secondary means of containmentfor the largest single compartment or container with sufficient freeboard.	Sec. III, Annex 7.4.6
(d)	Facility transfer operations, pumping, and facility process	
(d)(1)	Provide buried piping installed or replaced on or after August 16, 2002, with a protective wrapping and coatingcathodically protect. If a section of buried line is exposedcarefully inspect it for deterioration. If you find corrosion damage, you must undertake additional examination and corrective action as indicated	Sec. III, Annex 7.5.1
(d)(2)	Cap or blank-flange the terminal connectionand mark it as to origin when piping is not in service, or in standby service for an extended time.	Sec. III, Annex 7.5.3
(d)(3)	Properly design pipe supports to minimize abrasion and corrosion and allow for expansion and contraction.	Sec. III, Annex 7.5.4
(d)(4)	Regularly inspect all aboveground valves, piping, and appurtenancesalso conduct integrity and leak testing on buried piping at the time of installation, modification, construction, relocation, or replacement.	Sec. III, Annex 7.7.1
(d)(5)	Warn all vehicles entering the facility to be sure that no vehicle will endanger above ground piping or other oil transfer operations.	Sec. III, Annex 7.5.6

- 8.3..... HAZARDOUS WASTE CONTINGENCY PLAN (40 CFR 265 SUBPART D)
- 8.3.1..... Distribution Letter to Local Agencies

September 30, 2001

To: Distribution List

Re: 40 CFR 265 Subpart D Hazardous Waste Contingency Plan

This document is being provided to meet the requirements of 40 CFR 265 Subpart D requiring hazardous waste facilities to provide a contingency plan for responding to fires, explosions, or any unplanned sudden or non-sudden release of hazardous waste or hazardous waste constituents to air, soil, or surface water.

This regulation allows for the amendment of an existing emergency or contingency plan to address the release of a hazardous waste. The document being provided to you is the Hazardous Waste Contingency Plan (HWCP) for the Motiva Enterprises LLC Brooklyn Terminal. This plan represents the pertinent information that would be necessary to respond to an incident at the Facility, or similarly, treat victims of any incident at the Facility. For the Brooklyn Terminal, hazardous materials generated from the facility will be petroleum-based products. Material Safety Data Sheets (MSDS) for products that are stored and handled at the Facility have also been included to aid in the response effort.

The intent of this regulation is to ensure that local responders have an understanding of the facilities with which they are dealing in the event of an emergency. The Oil Spill Response Plan was prepared under the guidelines of the Oil Pollution Act of 1990 (OPA-90) and provides large quantities of information regarding Facility operations. This HWCP represents the initial actions and information that would be needed for a response from any of the local responders or emergency services. By additionally providing MSDS sheets for products handled at the Facility we believe we are meeting the intent of the regulation.

Please maintain this document as a record of the actions that will be taken to minimize hazards to human health or the environment from fires, explosions or any unplanned release of hazardous waste.

Nassau County Emergency Management Attn: Inspector Tom Skelly 140 15th Street Mineola, NY 11501

Lawrence Fire Department Emergency Coordinator 75 Washington Avenue Lawrence, NY 11559

Nassau County Fire Marshall's Office Emergency Coordinator 899 Jerusalem Avenue Uniondale, NY 11553 Nassau County Medical Center Emergency Coordinator 2201 Hempstead Turnpike East Meadow, NY 11554

Nassau County Police Dept. Emergency Coordinator 1699 Broadway Hewlett, NY 11557

Malverne Fire Dept. Emergency Coordinator 1 Britton Circle Malverne, NY 11565

At this time, it is our intentions that this document will be updated when significant changes in chemical storage result in a change in emergency strategy. Please retain this letter as an introduction to this document. If additional information is needed, please contact the Terminal Manager at 516-371-4780.

Sincerely,

George O'Connor Health and Safety Representative

Attachments

c: Nassau County Emergency Management
Lawrence Fire Department
Malverne Fire Dept.
Nassau County Medical Center
Nassau County Police Department
Nassau County Fire Marshall's Office

8.3.2..... Regulatory Cross-Reference

(Hazardous Waste Contingency Plan Cross Reference 40 CFR 265 Subpart D)

HWCP 40 CFR 265 Subpart D	Located in ICP
265.52(a). Implementation Actions.	Core Plan 1.1.7
265.52(c). Arrangements with local agencies.	Core Plan 1.1.6.4
265.52(d). Names, addresses, numbers of Emergency Response Coordinators (Qualified Individuals)	Core Plan 1.1.2
265.52(e). Listing of emergency equipment:	Core Plan
Fire extinguishing systems	1.1.4.5
Spill control equipment, communications	1.1.4.4
Alarms	1.1.4.4, 1.1.6.1
Decontamination equipment	1.1.7.16
265.52(f). Evacuation Plan.	Core Plan 1.1.6
265.16 (d)(2) Job Descriptions	Annex 3.a.5

8.4..... HAZARDOUS WASTE OPERATIONS EMERGENCY RESPONSE PLAN (29 CFR 1920.120)

8.4.1..... Regulatory Cross-Reference

CROSS REFERENCE FOR HAZARDOUS WASTE OPERATIONS EMERGENCY RESPONSE PLAN AND THE FACILITY RESPONSE PLAN (OPA '90)

	Motiva Enterprises LLC HAZWOPER Plan (29 CFR 1910.120(q)(2)(i-xiii)	Location in Core Plan (ERAP) & Integrated Contingency Plan
1.0	Pre-Emergency Planning and Coordination with Outside Parties (q)(2)(i)	Hone, Taking Day, Heer is gasting to be specified to the second section of the second section of the second sec
	1.1 Hazardous Substances Stored At facility*	Core Plan 1.1; Annex 7, Table 7.1
	1.2 Foreseeable types of incidents*	Core Plan 1.1.7.1; Annex 1, Figure 1.2
	1.3 Plot Plan*	Core Plan 1.1.8; Annex 1, Figure 1.2
	1.4 Pre-emergency planning and coordination*	Core Plan 1.1.6.1-1.1.6.4
2.0	Personnel Roles and Training (q)(2)(ii)	Core Plan 1.0 - Introductory Note; Annex 3.a.5; Annex 5; Annex 11.2
3.0	Communications and Notifications (q)(2)(ii)	Core Plan 1.1.1, 1.1.2 - Notification Lists; Core Plan 1.1.4.3; Annex 9.1.2, 9.2
4.0	Emergency Recognition and Prevention (q)(2)(iii)	Core Plan 1.1; 1.1.7.1; Annex 9
5.0	Safe Distances and Places of Refuge (q)(2)(iv)	Core Plan 1.1.6.1; Annex 9.6.7
6.0	Evacuation Routes and Procedures (q)(2)(vi)	Core Plan 1.1.6.1, 1.1.6.2, 1.1.8, Figure 1.3; Annex 1, Figure 1.3
7.0	Site Security and Control (q)(2)(v)	Core Plan 1.1.6.3; Annex 9
8.0	Decontamination (q)(2)(vii)	Core Plan 1.1.7.16
9.0	Emergency Medical Treatment and First Aid (q)(2)(viii)	Core Plan 1.1.7.16
10.0	Emergency Response Notifications (q)(2)(ix)	Core Plan 1.1.1 - 1.1.3, 1.1.4.4, 1.1.6.1,1.1.7.1; Annex 9.2
11.0	Emergency Response Procedure (q)(2)(ix)	1.1.7 - Immediate Actions; Annex 9
12.0	Personal Protective Equipment (q)(2)(xi)	Core Plan 1.0 - Introductory Note, 1.1.4.1
13.0	Review Process (q)(2)(x)	Core Plan 1.1.7.3

8.5...... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030) Final Rules

33 C	FR §154.1030	LOCATION
(a)	The plan must be written in English.	Entire Plan
(b)	A response plan must be divided into the sections listed in this paragraph and formatted in the order specified herein unless noted otherwise. It must also have some easily found marker identifying each section listed below. The following are the sections and subsections of a facility response plan:	TOC, Tabs and Annex 8.5
<u> </u>	(1) Introduction and plan contents.	Section I, 1.1
l	(2) Emergency response action plan:	Section II Core Plan, 1.1
	(i) Notification procedures.	Section II Core Plan, 1.1.2 and 1.1.3
	(ii) Facility's spill mitigation procedures.	Section II Core Plan, 1.1.7
	(iii) Facility's response activities.	Section II Core Plan, 1.1.7.4
<u> </u>	(iv) Fish and wildlife and sensitive environments.	Section III Annex 3
	(v) Disposal plan.	Section III Annex 3.d.6
	(3) Training and Exercises:	Section III Annex 5
	(i) Training procedures.	Section III Annex 5.2
	(ii) Exercise procedures.	Section III Annex 5.1
	(4) Plan review and update procedures.	Section III Annex 6
	(5) Appendices.	
 	(i) Facility-specific information.	Section I, 1.2
<u> </u>	(ii) List of contacts.	Section II Core Plan, 1.1.2
	(iii) Equipment lists and records.	Section II Core Plan, 1.1.4
ļ	(iv) Communications plan.	
	(v) Site-specific safety and health plan.	Section II Core Plan, 2.1.1.1
ļ	(vi) List of acronyms and definitions.	and Section III Annex 3.b.3 Section III Annex 12
ļ	(vii) A geographic-specific appendix for each zone in which a mobile	N/A
	facility operates.	
(c)	The required contents for each section and subsection of the plan are contained in §§ 154.1035, 154.1040, and 154.1041, as appropriate.	Section III Annex 8.5
(d)	The sections and subsections of response plans submitted to the COTP must contain at a minimum all the information required in §§154.1035, 154.1040, and 154.1041, as appropriate. It may contain other appropriate sections, subsections, or information that are required by other Federal, State, and local agencies.	Section III Annex 8.5 and Annex 10
(e)	For initial and subsequent submission, a plan that does not follow the format specified in paragraph (b) of this section must be supplemented with a detailed cross-reference section to identify the location of the applicable sections required by this subpart.	Section III Annex 8.5
(f)	The information contained in a response plan must be consistent with the National Oil and Hazardous Substances Pollution Contingency Plan (NCP) (40 CFR part 300) and the Area Contingency Plan(s) (ACP) covering the area in which the facility operates. Facility owners or operators shall ensure that their response plans are in accordance with the ACP in effect 6 months prior to initial plan submission or the annual plan review required under § 154.1065(a). Facility owners or operators are not required to, but may at their option, conform to an ACP which is less than 6 months old at the time of plan submission.	Section I, 1.1

8.5........... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1035) Final Rules

CFR §154.10	35	LOCATION
(a)(1)	Facility's address, phone, fax.	Introduction 1.2
(a)(2)	Facility's location	Introduction 1.2
(a)(3)	24 hour contact	Core Plan 1.1.2
(a)(4)	Table of Contents	After Cover Page
(a)(5)	Cross Reference	Annex 8
(a)(6)	Record of Changes	Annex 6.2
(b)(1)(i)	Notification Procedures	Core Plan; Annex 2
` / / / /	(A) Facility personnel, OSROs, qualified individuals	,
	(B) Federal, State, local agencies	
(b)(1)(ii)	Notification Form	Core Plan
(b)(2)(i)	Spill mitigation procedures	Core Plan; Annex 3.d
	(A) Average most probable discharge	·
	(B) Maximum most probable discharge	
	(C) Worst case discharge	
	(D) Worst case discharge from the non-transportation	
	related Facility	
(b)(2)(ii)	Prevention procedures	Core Plan, Annex 7
	(A) Failure of transfer apparatus	
	(B) Tank overfill	
	(C) Tank failure	
	(D) Piping rupture	
	(E) Piping leak	
	(F) Explosion / Fire	
	(G) Equipment failure	
(b)(2)(iii)	Listing of equipment	Core Plan; Annex 3.d
(b)(3)(i)	Facility personnel's responsibilities for response	
(b)(3)(ii)	Qualified Individual's responsibilities	Annex 3.a
(b)(3)(iii)	Corporate management response team's organizational	Annex 3.a-3.f
	structure	
	(A) Command and control	
ĺ	(B) Public information	
	(C) Safety	l
	(D) Liaison with governmental agencies	
	(E) Spill operations	
	(F) Planning	
i	(G) Logistics support (H) Finance	
(b)(3)(iv)	Oil Spill Removal Organizations	Core Plan
(b)(3)(iv)	(A) Equipment and supplies to meet§154.1045,	Cole Flair
	(A) Equipment and supplies to meet § 154. 1645, §154.1047 or	
	(B) Trained personnel necessary to continue	
	operationfirst 7 days of the response.	
(b)(3)(v)	include job descriptions for each spill management team	Annex 3.a.5
(5)(5)(4)	member within the organizational structuremust include	Ailliox J.a.J
	the responsibilities and duties of each spill management	
i	team member in a response action.	
	team member in a response action.	

8.5.......... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1035) Final Rules (Cont'd)

CFR §154.103	5 (Cont'd)	LOCATION
(b)(3)(vi)	For facilities that handle, store, or transport group II through group IV petroleum oils, and that operate in waters where dispersant use in pre-authorized, this subsection of the plan must also separately list the resource providers and specific resources, including appropriately trained dispersant-application personnel, necessary to provide the dispersant capabilities required in the subpart. All resources providers and resources must be available by contract or other approved means as described in § 154.1028(a). The dispersant resources to be listed within this section must include the following:	N/A
(b)(3)(vi)(A)	Identification of each primary dispersant staging site to be used by each dispersant-application platform to meet the requirements of this subpart	N/A
(b)(3)(vi)(B)	Identification of the platform type, resource-providing organization, location, and dispersant payload for each dispersant-application platform identified. Location data must identify the distance between the platform's home base and the identified primary dispersant staging site for this section.	N/A
(b)(3)(vi)(C)	For each unit of dispersant stockpile required to support the effective daily application capacity (EDAC) of each dispersant-application platform necessary to sustain each intended response tier of operation, identify the dispersant product resource provider, location, and volume. Location data must include the stockpile's distance to the primary staging sites where the stockpile would be loaded onto the corresponding platforms.	N/A
(b)(3)(vi)(D)	If an oil spill removal organization has been evaluated by the Coast Guard, and its capability is equal to or exceeds the response capability needed by the owner or operator, the section may identify only the oil spill removal organization, and not the information required in paragraphs (b)(3)(vi)(A) through (b)(3)(vi)(C) of this section.	N/A
(b)(3)(vii)	This subsection of the plan must also separately list the resource providers and specific resources necessary to provide aerial oil tracking capabilities requir4ed in this subpart. The oil tracking resources to be listed within this section must include the following: (A) The identification of a resource provider; and (B) Type and location of aerial surveillance aircraft that are ensured available, through contract or other approved means, to meet the oil tracking requirements of § 154.1045(j).	Annex 11
(b)(3)(viii)	For mobile facilities that operate in more than one COTP zone, the plan must identify the oil spill removal organization and the spill management team in the applicable geographic-specific appendix. The oil spill removal organization(s) and the spill management team discussed in paragraph (b)(3)(iv) or this section must be included for each COTP zone in which the facility will handle, store, or transport oil in bulk.	N/A

8.5...... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1035) Final Rules (Cont'd)

CFR §154.103	35 (Cont'd)	LOCATION
(b)(3)(ix)	For mobile facilities that operate in more than one COTP	N/A
	zone, the plan must identify the oil spill removal	
	organization and the spill management team in the	
	applicable geographic-specific appendix. The oil spill	
	removal organization(s) and the spill management team	
	discussed in paragraph (b)(3)(iv)(A) of this section must be	
	included for each COTP zone in which the facility will	
	handle, store, or transport oil in bulk.	
(b)(4)(i)	List areas of economic importance and environmental sensitivity	Annex 3.d
(b)(4)(ii)	For a worst case discharge	Annex 3.d, Annex 1
	(A) List areas of economic importance and environmental sensitivity	, uniox old, , uniox i
	(B) Response actions to protect these areas	
	(C) Map showing locations	
(b)(4)(iii)	For a worst case discharge identify appropriate equipment	Section 11 Core Plan,
	and required personnel to protect above mentioned areas	1.1.4, 1.1.5
(b)(4)(iii)(A)	Identify the appropriate equipment and required personnel	Annex 3
	to protect all fish and wildlife and sensitive environments	
(b)(4)(iii)(B)	Calculate the distances required byby selecting one	~====
(1) (4) (**) (5) (method described	O Black
(b)(4)(III)(B)(1) Distances calculated	Core Plan, Annex 3
(b)(4)(iii)(B)(2	A spill trajectory or model may be substituted for distances	
(b)(4)(iii)(B)(3	3) The procedures contained in the Environmental	
(*)(*)(*)(*)	Protection Agency's regulationsmay be substituted for	
	distances	
(b)(4)(iii)(C)	Based on historicalCOTP may require the additional fish	
	and wildlife and sensitive environments	
(b)(5)	Disposal Plan	Annex 3.d.7
(c)(1)	Training Procedures	Annex 5.2.2.3.
	Facility Personnel	Annex 5.2.2.
	• QI/AQI	Introduction 1.2.5; Annex 5.2.2.1.
	Members of Spill Management Team	Annex 5.1.3, 5.1.5
	OSHA Training Requirements	Introduction p. 1; Annex 5.2.2.3.
	Method of training for volunteers	Annex 3.e.5; Annex 3.f.2
	Training Records Maintained	Annex 5.2.2
	Location of Training Records	Annex 5.2.2
(c)(2)	Exercise Procedures	Annex 5
(c)(3)	Training and exercises	Annex 5
(d)	Plan review and update	Annex 6
(e)(1)	Facility specific information	Intro 1.2
(e)(1)(i)	Facility plan showing moorings, transfer locations, control stations, safety equipment; location and capacity of all	Annex 1
	piping and storage tanks.	

1

8.5...... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1035) Final Rules (Cont'd)

CFR §154.10	35 (Cont'd)	LOCATION
(e)(1)(ii)	Description of number of vessels that can transfer to simultaneously	Intro 1.2
(e)(1)(iii)	Location of first valve separating transportation-related portion of facility from non-T-R	Annex 1
(e)(1)(iv)	MSDS	Annex 11
(e)(2)(i)	Means to contact qualified individual and alternates	Core Plan 1.1.2
(e)(2)(ii)	Means to contact OSROs	Core Plan 1.1.2
(e)(2)(iii)	Means to contact Federal, State and Local Agencies	Core Plan 1.1.2
(e)(3)	Equipment List & records	Core Plan
(e)(3)(i)	For responding to Average Most Probable Discharge	Core Plan; Annex 3.d
(e)(3)(ii)	For responding to a Worst Case Discharge	Core Plan; Annex 3.d
(e)(3)(iii)	USCG classification of OSROs. For organizations not classified, list equipment including: (A) Nameplate information (B) Effective daily recovery rate (C) Boom height and type of end connectors (D) Type of spill for which equipment will be used (E) Total daily capacity for storage / disposal (F) Communication equipment (G) Location of equipment (H) Date of last inspection	Core Plan 1.1.4.3
(e)(4)	Communication Plan	Core Plan; Annex 3.b
(e)(5)	Site Specific Safety & Health Plan	Annex 3.b.3
(e)(6)	List of Acronyms	Annex 12

8.5...... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1045) Final Rules

CFR §154.104	5	LOCATION
(a)	facility that handlesGroup I through Group IV petroleum oils	
(a)(1)	criteria in Table 1identification of appropriate equipment	
(a)(2)(i)(v)	ice conditions; debris;other appropriate	
(a)(3)(i)(ii)		
(b)(1)(3)	Response equipment must	
(c)	identify response resourcesaverage most probable discharge	Core Plan, Annex 3.d, Annex 8
(c) (1)	1,000 feet of containment boom or two times the length of the largest vesseland the means of deploying and anchoring the boom within 1 hour of the detection of a spill;	Core Plan, Annex 3.d, Annex 8
(c) (2)	recovery devices and oil storage capacity within 2 hours	Core Plan, Annex 3.d, Annex 8
(d)	identify response resourcesmaximum most probable discharge	Core Plan, Annex 3.d, Annex 8
(d)(1)	include sufficient containment boom, oil recovery devices, and storage capacity for any recovery of up to the maximum most probable discharge planning volume	Annex 3.d, Annex 8
(d) (2)	resources must be appropriate for each group of oil	Core Plan, Annex 3.d, Annex 8
(d) (3)	must be positionedarrivescene of a discharge	
(d)(3)(i)	within the specified times	Annex 8
(d)(3)(ii)	In higher volume port areaswithin 6 hours	Annex 8
(d)(3)(iii)	In all other locations,within 12 hours	Annex 8
(d)(4)	COTP may impose additional operational restrictions	
(e)	identify the response resourcesworst case discharge	Annex 8
(e)(1)	The location must be suitable to meet the response times identified	Annex 8
(e)(2)	The response resources must be appropriate for	
(e)(2)(i)	The volume of the facilities worst case discharge	Core Plan, Annex 3.d, Annex 8
(e)(2)(ii)	Group(s) of oilhandles, stored or transported by the facility; and	Core Plan, Annex 3.d, Annex 8
(e)(2)(iii)	The geographic area(s) in which the facility operates.	Core Plan, Annex 3.d, Annex 8
(e)(3)	sufficient boom, oil recovery devices, and storage capacity to recover the worst case discharge planning volumes.	Core Plan, Annex 3.d, Annex 8
(e)(4)	quantity of response resourcesto responseto the worst case discharge to the maximum extent practicable.	Core Plan, 3.f.1, 3.d
(e)(5)	The following percentages of the response equipmentmust be capable of operating in waters of 6 feet or less depth.	
(e)(5)(i)	Offshore – 10 percent	N/A
(e)(5)(ii)	Nearshore/inland/Great Lakes/rivers and canals – 20 percent.	Core Plan, Annex 3.d

8.5.......... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1045) Final Rules (Cont'd)

CFR §154.1	045 (Confd)	LOCATION
(e)(6)	COTP may impose additional operational restrictions	
(f)	Response equipmentmust be capable of arriving on scene within the times specified in this paragraph	Core Plan, Annex 3.d, Annex 8
(g)	response equipment identified for Tier 1 plan credit must be capable of being mobilized and en route to the scene of a discharge within 2 hours of notification	Core Plan, Annex 3.d, Annex 8
(g)(1)	Either directly or through the qualified individual; and	Core Plan, Annex 3.d, Annex 8
(g)(2)	Within 30 minutes of a discovery	Annex 3.d, Annex 8
(h)	Response resources identified for Tier 2 and Tier 3 plan credit must be capable of arriving on scene within the time specified	Annex 3.d, Annex 8
(i)	The owner or operator of a facility that handles, stores, or transports groups II through IV petroleum oils within the inland, nearshore, or offshore areas where preauthorization for dispersant use exists must identify in their response plan, and ensure the availability of, through contract or other approved means, response resources capable of conducting dispersant operations within those areas.	N/A
(i)(1)	Dispersant response resources must be capable of commencing dispersant-application operations at the site of a discharge within 7 hours of the decision by the Federal On-Scene Coordinator to use dispersants.	N/A
(i)(2)	Dispersant response resources must include all of the following:	N/A
(i)(2)(i)	Sufficient volumes of dispersants for application as required by paragraph (i)(3) of this section. Any dispersants identified in a response plan must be of a type listed on the National Oil and Hazardous Substances Pollution Contingency Plan Product Schedule (which is contained in 40 CFR part 300, and available online from the U.S. Government Printing Office).	N/A
(i)(2)(ii)	Dispersant-application platforms capable of delivering and applying the dispersant on a discharge in the amounts as required by paragraph (i)(3) of this section. At least 50 percent of each EDAC tier requirement must be achieved through the use of fixed-wing, aircraft-based application platforms. For dispersant-application platforms not detailed within the DMP2, adequacy of performance criteria must be documented by presentation of independent evaluation materials (e.g., field tests and reports of actual use) that record the performance of the platform.	N/A

8.5...... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1045) Final Rules (Cont'd)

CFR §154.10	045 (Cont'd)	LOCATION
(i)(2)(iii)	Dispersant-application systems that are consistent in design with, and are capable of applying dispersants within, the performance criteria in ASTM F1413-07 (incorporated by reference, see § 154.106). For dispersant-application systems not fully covered by ASTM F1413-07, such as fire monitor-type applicators, adequacy of performance criteria must be documented by presentation of independent evaluation materials (e.g., laboratory tests, field tests, and reports of actual use) that record the design of performance specifications.	N/A
(i)(2)(iv)	Dispersant-application personnel trained in and capable of applying dispersants according to the recommended procedures contained within ASTM F1737-07 (incorporated by reference, see § 154.106).	N/A
(i)(3)	Dispersant stockpiles, application platforms, and other supporting resources must be available in the quantity and type sufficient to treat a facility's worst-case discharge (as determined by using the criteria in appendix C, section 8) or in quantities sufficient to meet the requirements in Table 154.1045(i) of this section, whichever is the lesser amount.	N/A
(j)	The owner or operator of a facility handling Groups I through IV petroleum oil as a primary cargo must identify in the response plan, and ensure the availability through contract or other approved means, of response resources necessary to provide aerial oil tracking to support oil spill assessment and cleanup activities. Facilities operating exclusively on inland rivers are not required to comply with this paragraph. Aerial oil tracking resources must:	Annex 11
(j)(1)	Be capable of arriving at the site of a discharge in advance of the arrival of response resources identified in the plan for tiers 1, 2, and 3 Worst-Case Discharge response times, and for a distance up to 59 nautical miles from shore (excluding inland rivers).	Annex 11
(j)(2)	Be capable of supporting oil spill removal operations continuously for three 10-hour operational periods during the initial 72 hours of the discharge;	Annex 11
(j)(3)	Include appropriately located aircraft and personnel capable of meeting the response time requirement for oil tracking from paragraph (j)(1) of this section; and	Annex 11
(j)(4)	Include sufficient numbers of aircraft, pilots, and trained observation personnel to support oil spill removal operations, commencing upon initial assessment, and capable of coordinating on-scene cleanup operations, including dispersant and mechanical recovery operations. Observation personnel must be trained in:	Annex 11

8.5...... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1045) Final Rules (Cont'd)

CFR §154.104	45 (Cont'd)	LOCATION
(j)(4)(i)	The protocols of oil-spill reporting and assessment, including estimation of slick size, thickness, and quantity; and	Annex 11
(j)(4)(ii)	The use of assessment techniques in ASTM F1779-08 (incorporated by reference, see §154.106), and familiar with the use of other guides, such as NOAA's "Open Water Oil Identification Job Aid for Aerial Observation," and NOAA's "Characteristic Coastal Habitats" guide	Annex 11
(k)	identify response resources with firefighting capability	Annex 9.5
(k) (l)	identify equipment and required personnel to protect fish and wildlife and sensitive environments.	Core Plan, Annex 3.d
(l)(1)	the identified response resources must include the quantities of boom sufficient to protect	Annex 3.d, Annex 6
(l)(2)	resources and response methods must be consistent with the ACP in effect 6 months prior to initial plan submission or the annual plan review	Annex 3.d, Annex 6
(m)	The response plan for a facility that handles, stores, or transports Groups I through IV petroleum oils must identify an oil spill removal organization(s) with response resources that are available	Core Plan, Annex 3.d, Annex 8
(m)(1)	Except as required in paragraph (I)(2) shoreline clean-up response resources required must be determined as described in Appendix C of this part.	Annex 3.d
(m)(2)	resources and response methods must be consistent with the ACP in effect 6 months prior to initial plan submission or the annual plan review	Annex 3.d, Annex 6
(n)	Appendix C quantity of response resources for the maximum most probable discharge volume, and for each worst case discharge response tier.	Annex 3.d
(n)(1)	Included in Appendix C of this part is a cap that recognizes the practical and technical limits of response capabilities	Annex 3.d
(n)(2)	Appendix C of this part lists the caps that will apply in February 18, 1998facility whose estimated recovery capacity exceeds caps shall identify sources of additional equipment equal to twice the cap or the amount necessary to reach the calculated planning volume, whichever is lower.	Annex 3.d
(o)(1)(5)	The Coast Guard will initiate a review of cap increases and other requirements contained within this subpart	wa

8.5.......... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1050 and §154.1055) (Cont'd)

CFR §154.1	050	LOCATION
(a)	Must identify the training to be provided to each individual with responsibilities under the plan.	Annex 5
(b)	A facility owner or operator shall ensure the maintenance of records sufficient to document training of facility personnel	Annex 5.2
(c)	Where applicable, a facility owner or operator shall ensure that an oil spill removal organization identified in a response plan to meet the requirements of this subpart maintain records sufficient to document training	Annex 5.1.1
(d)	The facility owner or operator remains responsible for ensuring that all private response personnel are trained to meet the Occupational Safety and Health Administration (OSHA) standards for emergency response operations in 29 CFR 1910.120.	Introduction 1.1
CFR §154.1	055	LOCATION
(a)(1)	Qualified individual notification exercises	Annex 5
(a)(2)	Spill management team tabletop exercises	Annex 5
(a)(3)(i)	Equipment deployment exercisesfacility owned and operated.	Annex 5
(a)(3)(ii)	Equipment deployment exercisesoil spill removal organization equipment.	Annex 5
(a)(4)	Emergency procedures exercises (optional)	Mill first year page

ANNEX 9..... COMPANY EMERGENCY PLAN AND REPORTING PROCEDURES

9.1..... CORPORATE EMERGENCY REPORTING

9.1.1 Guidelines

Houston Office personnel and appropriate affiliates are to be promptly notified and be kept informed of unusual events and reportable incidents occurring at our marketing facilities or involving Motiva owned product or property handled or operated by others. This procedure must be carefully followed to ensure that Headquarters personnel receive the required information. Information on how to effectively communicate with the news media during an emergency situation is provided in Annex 3.b.2.

9.1.2..... Reporting Incidents Internally

To report incidents internally, take the following actions:

- 1. If the situation warrants potential use of resources from Emergency Management, Preparedness, and Response (EMP&R), call their 24 hr. hotline immediately at (877) 242-7400 to report incidents. When notification is made to or assistance is requested from Emergency Management, Preparedness, and Response (EMP&R), notification information should be documented on the EMP&R Notification Log.
 - Collect the information requested on the Spill Response Notification Form (located in the Core Plan) prior to calling the Emergency Management, Preparedness, and Response Team.
- 2. Contact the Regional Manager and the Manager, LSDR/HSE and Emergency Management within 24 hours (7 days a week).
- 3. If the reportable event involves a spill or an impact to the community, a written event investigation report (Investigation Report*) will be provided, within 10 calendar days, to the Regional Manager and the Manager, LSDR/HSE and Emergency Management.

*NOTE: Exceptions to the Investigation Report will be made for sensitive matters which may need to be investigated under the attorney-client work product privilege. Contact Legal immediately where circumstances warrant. Advise the above contacts accordingly. On rare occasions an incident (e.g., certain process safety incidents) may require additional time to complete the investigation. The Manager, LSDR/HSE and Emergency Management is authorized to extend the reporting requirements where appropriate.

The event Investigation Report should address the facts of the matter and specifically discuss what preventative steps will be taken to help prevent a similar occurrence. The report should provide sufficient detail to enable others to learn from the experience.

Other reportable environmental events will not require a written followup report unless specifically requested.

- 4. For environmental incidents that are reportable to the National Response Center (NRC) pursuant to various federal laws, notify NRC at 1-800-424-8802 upon discovery of the environmental incident. If required by law, you must also contact local and State agencies in a timely manner to report certain environmental incidents.
- 5. Fatalities or incidents resulting in the hospitalization of three (3) or more Motiva employees must be initially reported orally by telephone or in person to the nearest OSHA area office within eight hours. Facilities can either call the nearest OSHA area office or call the OSHA 24-hour toll free telephone number at 1-800-321-OSHA (6742). The report must relate the circumstances of the accident, the number of fatalities and hospitalizations, and the extent of any injuries. The OSHA area director may require additional reports, in writing or otherwise, concerning the accident. Although the regulation does not require the employer to confirm in writing the oral or in person report to OSHA, Motiva facilities should work with the Motiva Legal Department to prepare a confirmation letter to send to OSHA.

9.1.3..... Incident Investigation

Investigation of incidents qualifying for emergency reporting should be coordinated with the Law Department. Do not delay required regulatory or insurance company reporting.

Subject to the requirement to coordinate incident investigations with the Law Department for environmental incidents, injury accidents, and property damage / product loss, a full Incident Report detailing the known factors, confirmed causes, costs, and actions taken to address the incident must be submitted to the Houston Office within ten (10) working days of the start date of an incident investigation that does not require any testing, sampling, or other activities that require more than 10 working days to complete. For incident investigations that require testing, sampling, or other activities that cannot reasonably be completed in ten (10) working days, the incident report must be submitted within thirty (30) working days of the start of date of the incident.

9.1.3.1.... Environmental

Environmental incidents should be reported if any one of the following conditions is present:

- 1. Any spill, discharge, or migration that threatens significant ecological damage or poses a threat to employee or public welfare.
- 2. Any incident that may have serious legal repercussions, such as the threat of legal action against the Company or an employee, the imposition of a significant penalty, or cleanup operations being taken over by a governing agency.
- Any significant or potential side effects such as hazardous materials, petroleum products, or chemicals reaching a drinking water source, entering a public sewer system, or entering into basements of buildings or homes.
- 4. Any significant public reaction or news media coverage which has or may reflect on the Company's reputation.

9.1.3.2.... Accidents, Property Damage, Security, and Unfavorable Publicity

The following incidents should be reported:

Injury accidents (employees, contractors, or third parties) requiring hospitalization or a fatality.

Property damage, product loss, or other unusual happening (fires, explosions, power failures) where the losses or costs are expected to exceed \$50,000.

Any act of criminal violence resulting in serious injury or fatality, bomb threats, death threats, group demonstrations, wildcat strikes, or unexpected picketing, whether actual, threatened or potential, that could impact on Company operations, facilities, or personnel.

Any incident or event likely to result in significant unfavorable public reaction or news media coverage that is not covered within other categories.

9.1.4..... Handling the News Media

Motiva seeks to be a cooperative, forthright, and a responsible corporate citizen. In keeping with this, it is our goal to keep the public informed in the event of an emergency involving the safety of individuals or property.

9.2 EMP&R NOTIFICATION LOG			
Person on the EMP&R staff to whom	you relayed this emergency information:		
Name: Phone:() Time:: AM or PM (circle or	ne) Time Zone: EST or CST		
Document any calls or actions that you take in regard to this Emergency Call (including calls where you leave a message):			
Follow-up call:	Time Called:		
	·		
Follow-up call:	Time Called:		
, . 			
	·		
Follow-up call:	Time Called:		
Follow-up call:	Time Called:		

9.3....LOCAL EMERGENCY PLAN

9.3.1...... General Emergencies and Disasters

9.3.1.1 Introduction

The objective of this Plan is to prepare for a general emergency and in so doing provide for the safety of Company personnel, protect Company property, and maintain the ability to continue operations.

9.3.1.2.... Authority to Activate Plan

This Plan may be activated by the designated Qualified Individual or the designated Alternate Qualified Individual. The individual activating the Plan shall assume responsibility for its complete execution until such time as relieved by higher authority.

9.3.1.3.... Emergency Agencies and Control Center

When deemed necessary, persons listed on the emergency notification phone list (Core Plan 1.1.2) may be summoned.

9.3.2..... Natural Disasters

9.3.2.1 Floods

Floods may result from an unusually heavy rain following a long period of wet weather or a sudden spring thaw with, or without, rainfall. They may be caused by hurricanes with heavy rainfall and exceptionally high tides in coastal areas. Tidal waves may also flood coastal areas or areas adjacent to large inland lakes. Generally, there is ample advance warning of these conditions and as warranted, the following preparations should be considered:

- 1. Disconnect the main electrical switch, shut the main valve in the gas service line and water line, if any. Determine whether connections on sanitary sewer would be blocked to prevent back up (storm sewer drains should not be blocked).
- 2. Clear the yard of all loose items that could float away. Store empty drums inside a building and secure them against floating. Underground tanks in yard storage should be filled with water or otherwise anchored to prevent floating and sealed to prevent product or other contaminate from escaping.
- 3. Store carton packages above anticipated flood level or remove them to a safe place.
- 4. Remove motors and other electrical equipment and store them above anticipated flood level.

- 5. Remove automotive equipment, including forklift trucks and other motorized portable equipment, to a safe place.
- 6. Make sure that vertical tanks and large pipelines (8" and over) are filled, preferably with product. Safety requires maintaining the product level in the tanks at least 10" above the highest anticipated flood level. If sufficient product is not available, water should be used. However, water should be admitted to the tanks and lines only as a last resort, and only in sufficient quantities to keep ahead of the flood rise. Horizontal tanks that would be below flood-water level should be filled an anchored.
- 7. Close and lock product line valves.
- 8. Consideration should also be given to protection of Company funds and records. If deemed necessary on account of expected high water, valuable papers and funds should be removed from the safe to be stored elsewhere for safekeeping.
- 9. If possible, file cabinets should be elevated to a height above the expected flood level. If this is not possible, the contents of the file drawers that are subject to flood damage should be removed, tied securely in bundles and stored temporarily at a height above the expected high water level. In the same manner, see that correspondence and records in desk drawers are removed if in danger of loss or damage.
- 10. Pump out the oil collection compartment of open-top oil / water separators so flood waters do not impact the compartment causing a release to the lands or waters.

9.3.2.2.... Hurricanes

In the event of an approaching hurricane, the following precautions should be taken:

- 1. Clear the yard area of all loose items, empty drums, etc., that blow around and cause further damage.
- 2. Close all doors and windows.
- 3. Tape and / or board up windows and brace large windows.
- 4. Brace all large outside doors securely.
- 5. Small diameter (10' to 12') vertical or horizontal tanks should be at least half filled with product. If product is low, water should be added, only as a last resort.

6. Take precautions as listed above for impending flood if hurricane warnings indicate this emergency.

9.3.2.3.... Tornadoes

Generally, there is little warning of tornado conditions, from 15 minutes to an hour and a half. However, insofar as time permits, the same preparation should be made as indicated above for hurricanes, giving preference in the order listed. A tornado may follow a period of intense ground heat. The first indication of its approach may be a combination of thick dark storm clouds and heavy rainfall or hail. When such signs appear in tornado areas, it is important to maintain contact with local weather reporting agencies.

9.3.2.4....Earthquakes

Brooklyn is in Zone 2 - Moderate Damage Area.

9.3.2.5.... Cleanup

After any emergency has passed, facilities should be returned to operating condition as soon as possible. However, in doing so, certain precautions should be observed:

- 1. Do not touch loose wires under any circumstances until they have been checked out by a qualified electrician. They may be electrically charged.
- 2. Do not turn on main electrical switch until the entire system has been checked out (if any part was flooded) by a qualified electrician.
- 3. Do not operate any electrical equipment until thoroughly dried out and checked (if flooded) by a qualified electrician.
- 4. Check thoroughly all product lines and tanks for leaks or any other evidence of damage.
- 5. Check entire Facility for possible damage.
- 6. Prepare accident report, if necessary.

9.3.3..... Media

All contact with the press or other media will be made by the Complex Manager or a Motiva Communications Representative listed in the Core Plan. All contacts should adhere to the Company's public policy statements and follow existing guidelines.

9.3.4..... Emergency Oversight

When this Plan is activated, the Complex Manager will direct all "outside" activities and all "inside" activities. Those handling administrative duties will stand ready to secure and protect the Company funds and records, and stand ready to assist as directed by the Complex Manager. The Terminal Operator on duty will act as telephone coordinator and liaison with Emergency Agencies.

9.3.5..... First Aid

Local Emergency Medical Services will be contacted by calling 911. If required, a First Aid Station will be established in the Terminal Office.

9.3.6..... Special Matters

9.3.6.1.... Criminal Complaints and Arrests

Under long-standing Company policy no employee, on behalf of the Company, may sign a criminal complaint, institute a criminal action or cause the arrest of anyone unless prior approval of the Legal Department has been obtained. Of course, if a Federal or State Law Enforcement officer desires to sign the complaint or file charges in accordance with his statutory authority and duty, he should be encouraged to do so.

9.3.6.2.... Subsequent Investigations

All contacts with investigating authorities during their subsequent investigations of these types of emergencies should be made only through the Company's Security Representatives. Therefore, any inquiries made by public authorities in connection with any post investigations should be referred to them. However, personnel should cooperate in developing for the Security Representatives any information they may deem to be desirable to furnish the investigating authorities.

9.3.6.3.... Conduct of Employees

Emphasis should always be on the side of preventing undesirable publicity; and, except in self-defense:

NO PHYSICAL FORCE SHOULD BE USED AGAINST OTHER PERSONS AT ANY TIME!!

9.3.6.4.... Bomb Threat Checklist

NI OCE DE LE TURBLE	THE PERSON NAMED IN COLUMN 1		CONTROL OF A PLANTAGE OF A STATE
Name Of Person Receiving Threat	re dimine 😤 Title		Phone No.
CONTRACTOR AND ADDRESS OF THE PARTY OF THE P			
CONTROL OF THE PARTY OF THE PAR			
. B . T			
Date Threat Received Time Thre	at Received Re	ported To	Phone No.
, Date (1110at) (0001, 00)	AND THE PROPERTY OF THE PROPER		
			AND THE RESIDENCE OF THE PARTY

	going to explode?	EXACT WORDII		EAT
3. What does it look	like?			
4. What kind of boml	b is it?	***		
5. What will cause it	to explode?			
6. Did you place the	bomb?	····		
7. Why?		· · · · · · · · · · · · · · · · · · ·	**************************************	
8. What is your name	e?			
9. What is your addr	ess and phone?			
The following rea	quire opinions, perceptio	ns and judgments. Please	give your first in	npression.
Caller was:	[] Male	[] Female	[] Adult	[] Child
Estimated age:	[] Pre-teen	[] Teenage	[] 20-40	[1] Other
Caller's Speech:	[] Accent	[] Heavy	[] Slight	[] Other
	[] Spanish	[] German	[] German	[] Other
	[] Southern	[] Northern	[] New York	[] Other
Caller's Voice:	[] Fast	[] Slow	[] Excited	[] Angry
	[] Slurred	[] Quite	[] Nasal	[] Slang
	[] Impediment	[] Well Spoken	[] Other	
Background Sound:	[] Animals	[] Railroad	[] Aircraft	[] Street
	[] Other (describe)			

1

9.4..... DEMONSTRATIONS

9.4.1..... Introduction

Security procedures to be activated in respect to demonstrations have three objectives:

- 1. Protection of Company employees and property.
- 2. Protection of business visitors and their property.
- 3. Continuity of operations.

In the Company's performance of service to the public, constructive communications are encouraged, but communications which take the form of group demonstrations conducted on Company property not only are not constructive but pose a serious threat to the personal safety of employees and probable harm to Company property.

Since these demonstrations could come at any time, with or without warning, to effectively cope with such an emergency, a threat plan of action for each Company facility must be placed in readiness. Guidelines for the development of a plan to meet this type of emergency, including an outline of the actions to be taken, are set out below.

9.4.2..... Authority to Activate Plan

This Plan may be activated by the designated Qualified Individual or the designated Alternate Qualified Individual.

The individual placing the Plan into effect will remain responsible for all activity until relieved by higher authority. Exercising good judgment and without over-reacting, the individual activating the Plan will take all measures necessary to accomplish the three objectives first mentioned.

The highest local authority present, or the Complex Manager if present, will act as Company spokesperson in the event a meeting with the demonstrators is indicated. He / she shall be familiar with Company's public policy statements and the Emergency Reporting Procedures.

The highest local authority present, the Complex Manager or the Motiva Enterprises LLC Communications Representative, will act as spokesperson with the media.

9.4.3..... Emergency Agencies

When deemed necessary, persons listed on the emergency notification phone list (Core Plan, Section 1.1.2) may be summoned.

9.4.4..... Notification

Any individual observing or receiving notice, verbal or written, of an actual or proposed demonstration shall immediately notify the QI/AQI or the Senior Terminal Operator.

If received or noted after hours, and after consideration of first protecting Company employees and forestalling damage to property, every effort will be made to notify the above by telephone.

All employees in the Facility will be notified in person of what action is being taken and what countermeasures, if any, should be taken. If it becomes necessary to evacuate the Facility, a communications post will be established by the Complex Manager and employees may call there for current instructions.

A Control Center will be established in the Terminal Office, if possible. All activities will be directed by the senior person in charge from the Control Center.

9.4.5..... Action Steps

9.4.5.1 Entrances

If time allows, all entrances to the Facility, except one, should be locked or blocked so that the demonstrators will be required to enter through only one door. However, predesignated personnel with keys should be posted at all such locked entrances so that all doors may be quickly opened if personnel evacuation becomes necessary.

9.4.5.2.... Dangerous Materials

Gates to all fenced areas should be locked and employees positioned where they can warn of points where flammable or other dangerous materials are kept.

9.4.5.3.... Alerting Personnel

All personnel in the Facility should be alerted and kept advised of all developments by the communication means set out in the Plan.

9.4.5.4.... Restricted Areas

Company and other selected personnel will be stationed at every building door, entrance / exit gate, and the truck loading rack (if remote from the office) and advise non-employees that the area is not open to the public. However, no physical force should be used to restrain or resist outsiders.

9.4.5.5.... Files and Desks

If it appears that the protest or demonstration may become unruly or access to restricted areas may be attempted, all desks should be cleared and all desks, files and cabinets locked as directed by the person in charge.

9.4.5.6.... Fire Equipment

Personnel shall be prepared to take up positions where they will be able to readily man hand held fire equipment only. If necessary, the local Fire Department will be summoned by calling 911 by Facility personnel, as directed by the Fire Emergency Plan.

9.4.5.7 First Aid

Local Emergency Medical Services will be contacted by calling 911. If required, a First Aid Station will be established in the Terminal Office.

9.4.6...... Instructions for Contact with Demonstrators

9.4.6.1.... Clarification

At the outset, the exact reason for and purpose of the groups visit should be requested and such information conveyed immediately to the person in charge.

9.4.6.2.... Restrict to Lobby

Efforts should be made to keep demonstrators outside of the Facility or, if they gain entrance, in the lobby or reception area - but by request only. Do not attempt to use force.

9.4.6.3 Heckling

Do not debate with, taunt, heckle or harass protesters in any manner.

9.4.6.4.... Group Representatives

If possible, the group should be persuaded to designate one (or only a few) person to represent it and it should be suggested that the meeting be held in a separate closed room.

9.4.6.5.... Spokesperson Conduct

The Company spokesperson should always be accompanied by at least two other Company employees (if available), should decline to have his or her conversation recorded, should not pose for pictures, and should not express personal opinions. However, NO attempt to confiscate cameras, film, recorders or any personal articles should be made. The spokesperson should listen courteously, engage in no debate, and answer questions only in terms of authorized Company statements. NO MORE.

9.4.6.6.... Unruly Demonstrations

If the demonstration becomes disruptive or if the group refuses to leave after the Company spokesperson considers the interview at an end, the police should be summoned to the Facility. The Company employee in charge of the emergency should then decide whether the disruptive actions are of such severity as to warrant a request for removal by the police.

9.4.6.7 Evacuation

If demonstrators begin to intentionally damage or destroy Company property, Company personnel are to be immediately evacuated from the affected area and police action should be immediately requested to protect persons and property.

9.4.6.8.... Criminal Complaints and Arrests

Under a long-standing Company policy, no employee, on behalf of the Company, may sign a criminal complaint, institute a criminal action or cause the arrest of anyone unless prior approval of the Legal Department is obtained. Of course, if a Federal or State Law Enforcement Officer desires to sign the complaint or file charges in accordance with his statutory authority and duty, he should be encouraged to do so.

9.4.6.9.... Restraint by Employees

Emphasis should always be on the side of avoiding provocation or disturbance and preventing undesirable publicity. Except when self-defense becomes necessary, NO PHYSICAL FORCE SHOULD BE USED BY EMPLOYEES AT ANY TIME.

COMMON SENSE, CALMNESS AND DISCRETION SHOULD PREVAIL AT ALL TIMES!!

9.5..... FIRE EMERGENCY PLAN

9.5.1..... Introduction

The objective of this Plan is to prepare for a fire emergency and in so doing, provide for the safety of Company personnel, protect Company property, and maintain the ability to continue operations.

Facility personnel will take no action or risk to themselves or other to fight a fire, except when the fire is in the incipient stages where hand-held fire extinguishers may be used by Facility personnel.

Facility personnel will not endanger themselves or others in any way.

No employee shall enter a burning building to fight a fire.

9.5.2..... Authority to Activate Plan

This Plan may be activated by the designated Qualified Individual, the designated Alternate Qualified Individual or any other Facility employee. The individual activating the Plan shall assume responsibility for its complete execution until such time as relieved by higher authority.

9.5.3..... Emergency Agencies and Control Center

When deemed necessary, persons listed on the emergency notification phone list (Core Plan, Section 1.1.2) may be summoned.

9.5.4......In the Event of a Fire

The person observing the fire will sound the nearest alarm and notify the Terminal Office to notify the local Fire Department by calling 911.

All truck loading at the truck loading rack will cease.

Facility personnel will direct the evacuation of all trucks to a safe location outside of the Facility facility. All drivers will remain with their trucks. If starting vehicles will present an ignition hazard, vehicles will not be moved.

If the fire is at the truck loading rack, Facility personnel will stand by the foam system control actuator and initialize the foam system if the automatic system for the loading rack should fail.

If a Facility employee is on duty, providing that it is safe to do so, a Facility employee will close all tank and pipeline valves and shut off all power to the product pumps.

Facility personnel will ensure that all of the entrance / exit gates are open for emergency vehicles.

Facility personnel, as may be available, will be assigned to the entrance / exit gates to deny access to anyone other that emergency vehicles (Police, Fire, and Ambulance). Without placing themselves in danger, Facility employees may assist emergency response vehicles stopping traffic on East Avenue to allow entrance / exit of trucks and emergency vehicles to / from the Facility.

All non-Company personnel will be directed to leave the Facility taking their personal vehicles with them, if safe to do so.

Facility personnel and / or selected individuals arriving at or returning to the Facility will report to the Qualified Individual for instructions. The QI will be the designated liaison with the Fire Department.

If possible, company funds and / or records will be secured or removed from the Facility to a safe location.

If possible, a Facility employee or selected individual will handle all telephone traffic.

9.5.5.....Fire Evacuation Plan

A detailed Facility evacuation plan and Evacuation Diagram is located in the Core Plan and in Annex 1. The diagram depicts the location of the emergency evacuation routes, fire extinguishers, and fire alarm pull stations.

9.5.6.....Fire Safety Equipment

9.5.6.1....Fire Alarm Switches

See diagrams in Annex 1.

9.5.6.2....Truck Loading Rack Foam System

The truck loading rack is protected by a foam system that is activated automatically by fire sensor equipment located on the under side of the loading rack roof.

The truck loading rack foam system may be activated manually from the Terminal Operator's office or from the foam room.

9.5.6.3.....Tank Farm Foam System

Each tank in the tank farm is protected by a foam system that is activated manually with zone control. To activate, the Operator must open the appropriate foam valve that corresponds to the tank and turn on the foam pump.

9.5.6.4....Portable Fire Extinguishers

Portable fire extinguishers are located at various locations throughout the Facility. A location listing is found in the Core Plan.

9.5.6.5.....Fire Blankets

There are fire blankets located on each lane of the loading rack, one at the pump off station, two in the shop and one in the warehouse.

9.5.7...... Predetermined Reassembly Locations

If it becomes necessary to evacuate the Facility due to imminent danger, all Facility employees, contractors, drivers, and visitors will safely and quickly proceed to the "Fire Drill Area" located between the main office and warehouse. All employees and visitors will be accounted for by the designated person in charge. All employees and visitors will remain in this area until directed otherwise by the designated person in charge.

COMMON SENSE SHOULD PREVAIL AT ALL TIMES

BE CALM AT ALL TIMES - DO NOT RUN - DO NOT PANIC

Follow the instruction from the designated person in charge or from such civil authorities that are on the scene

ANNEX 10... STATE REQUIREMENTS

ANNEX 10

NEW YORK SPILL PREVENTION REPORT (6NYCRR 598.1(k))

TABLE

		Pursuant to <u>598.1</u>		<u>Section</u>
, , ,	Information Current Registration Application and Certificate Management Approval and Certification Name & Signature of qualified person who prepared the Report (NYS Professional Engineer or Qualified Person)	(k)(2)i (k)(2)ii (k)2)iv	Annex	x 10, Attachment 1 x 8, Section 8.2.3 x 10, Attachment 2
	Map Locations and identification of tanks, transfer stations & piping	(k)(2)iii	Annex	· 1
Summar	ry of Releases During Past Five Years	(k)(2)v	Annex	4, Section 4.2
Identific	ation and Assessment of Causes of Releases	(k)(2)vi	Annex	7, Section 7.1
Complia	nce Status	(k)(2)vii	Annex	10, Attachment 3
Inspection	ons	(K)(2)viii		etion Program described in Annex tion 7.5.4, 7.7.1, 7.7.2, 7.7.3
(General Daily			of Shift Checklist and SPCC list located at the end of Annex 7
	Monthly			ly inspections are performed, gh not required under this section
	Annual		(1)	Annual inspections of cathodic protection systems are performed and maintained in a separate report. Reports are maintained on site Tanks, secondary containment systems, and equipment are inspected daily – See Forms in Annex 7
F	Five-Year	·	Five-Y on site	ear inspection records maintained
Financia	l Responsibility (If applicable)	(k)(2)ix	N/A – reques	will be provided to NYSDEC upon

Spill Response Plan	(k)(2)x	Core Plan, Annexes 1, 2, 3, 4, 5, 7, 8 & 9
Discussion and Assessment of Equivalent Equipment, Method, or Practice (If applicable)	(k)(3)	N/A
Site Assessment and Findings (If applicable)	(k)(4)	N/A
Spill Reporting Form		Core Plan, Section 1.1.3
Written Procedures for the Prevention of Mixing of Incompatible Substances (If applicable)	598.4(b)(7)	N/A – Storage/handling of petroleum products and fuel additives does not present a compatibility concern under this section (all materials are compatible)

ATTACHMENT 1

REGISTRATION APPLICATION AND RECERTIFICATION

ATTACHMENT 2

SPILL PREVENTION REPORT (SPR) CERTIFICATION

I certify that I have acquired, through education and/or related practical experience, knowledge of the physical sciences, technology and principles of storing and handling hazardous substances as it relates to this Facility.

I have examined the Facility, and being familiar with the provisions of 6 NYCRR Parts 595, 596, 597, 598, and 599, attest that this Spill Prevention Report has been prepared in accordance with requirements therein.

James W. Lintz	
Name of Qualified Person	Signature of Qualified Person
Dete	
Date:	

ATTACHMENT 3

SAMPLE COMPLIANCE STATUS CHECKLIST

11	LOCAL REQUIREMENTS
	Attachment 1
	Attachment 2
	Attachment 3
11.1	OSRO Classifications
	OSRO contracts
	AMPD Checklist
11.2	Response Team Job Description
11.3	Material Safety Data Sheets







New York State Department of "vironmental Conservation CHEMICAL BULK STO, AGE CERTIFICATE

625 Broadway, 11th Floor, Albany, NY 12233-7020 Phone: 518-402-9553

Region 2
One Hunters Point Plaza, 1s .oor
47-40 21st Street, L.I. City, NY 11101-6454
(718) 482-6454

				(110) 402-040	, -	
TANK	DATE	TANK LOCATION	CAPACITY	HAZARDOUS	% HAZ	CHEMICAL
NUMBER	INSTALLED	AND TYPE	(GALLONS)	SUBSTANCE	SUBST	ABSTRACT#
10	01/01/1945	AST - Steel/Carbon Steel/Iron	10,000			
	^ :			XYLENE (MIXED)	3.00	1330-20-7
51	10/01/1990	AST - Steel/Carbon Steel/Iron	5,000			
				XYLENE (MIXED)	17.00	1330-20-7
52	12/01/1990	AST - Steel/Carbon Steel/Iron	4,000			
				XYLENE (MIXED)	17.00	1330-20-7
54	10/01/1993	AST - Steel/Carbon Steel/Iron	5,014			
				XYLENE (MIXED)	17,00	1330-20-7
9	04/01/1945	AST - Steel/Carbon Steel/Iron	10,000		. 212	
				XYLENE (MIXED)	27.00	1330-20-7

OWNER:

MOTIVA ENTERPRISES, LLC

1100 LOUISIANA STREET, SUITE 2200 HOUSTON, TX 77002

OPERATOR: MOTIVA ENTERPRISES LLC

(718) 383-4066

EMERGENCY JAMES W. LINTZ CONTACT: (718) 383-4066

ISSUED BY:

Commissioner

Alexander B. Grannis

CBS NUMBER:

2-000209

DATE ISSUED:

11/03/2008

EXPIRATION DATE:

11/30/2010

FEE PAID:

\$ 625.00

SITE:

MOTIVA ENTERPRISES LLC

25 PAIDGE AVENUE

BROOKLYN, NY 11222

MAILING CORRESPONDENCE:

JAMES W. LINTZ

MOTIVA ENTERPRISES LLC

25 PAIDGE AVENUE

BROOKLYN, NY 11222

As an authorized representative of the above named facility, I hereby certify that the information on this form is true and correct. Additionally, I recognize that I am responsible for assuring that this facility is in compliance with all sections of ECL Article 40 and 6 NYCRR Parts 595, 596, 597, 598, and 599, not just those cited helow.

-- The facility must be re-registered if there is a transfer of ownership.

-- The facility has maintained it's requirements relating to daily, monthly, annual and five year inspections as required by Part 598.7 and has has it's SPR annually updated as required by Part 598.1(k).

-- The Department must be notified within 3 business days prior to adding, replacing, reconditioning, or permanently closing a stationary tank.

- This certificate must be signed and posted on the premises at all times. Posting must be at the tank, at the entrance of the facility, or the main office where the storage tanks are located.

-- Any person with knowledge of a spill, leak or discharge must report the incident to DEC within two hours (1-800-457-7362).

Signature of Representative/Owner Date

MES (J. Lintz, Matropolitan Complex Manne and Title of Authorized Representative/Owner (Please Print)

Print Date: 11/3/2008

THIS REGISTRATION CERTIFICATE IS NON-TRANSFERABLE

Page 1 of

NEW YORK STATE CHEMICAL BULK STORAGE INSPECTION REPORT

Rev. 8/28/06 Cbscklst 2005

CBS# 2 -000 209 or Unregistered Inspec	ction numbe	ər	Date 10/20		Cbscklst 2005
Site Name Motiva Enterprises LLC - Brooklyn Terminal	Owner Nam Owner Addi	Motiva Enterprises LLC ress 1100 Louisiana St, 9	· · · · · · · · · · · · · · · · · · ·		
Site Contact Frank Signoriello	Owner Cont	Houston, TX 77002 tact James Lintz	<u>'</u>		
730,000,3000,	Phone Numl	740,000,4000			
		718-383-7970			
Front Oleon Stelle OMER Const.	Email Addre	Instrument the second sections	ent.com		
of site Map Datum GIS: E N Loca SITE Representative NYSDEC Inspector Self-assessment	ation 3. At	1. ^T	Visitor parkin	ng 2.€	
I. GENERAL		YES	NO	<u>) </u>	X
1. All regulated tanks at this site are registered [§596.2(a)]?		Y			
2. Is the registration certificate posted at the facility [\$596.2(g)]?		Υ			110745
3. Is registration information current & correct [\$596.2(f)]?		Tank 52 should be removed			4.44
II. SPILL PREVENTION REPORT (SPR) A. Preparation of the SPR		YES	NO		X
4. Does facility have an SPR [§598.1(k)(1)]? Y/N Date:		Incorporated in ICP, last update 10/2010			-0.0
Has SPR been updated annually or Whenever a significant release occu When a substantial modification was made. Y/N/X	arred or	Υ			
6. Does the SPR contains a copy of current registration application & certifi [§598.1(k)(2)(i)]? Y/N	icate.	Υ			100 m
7. Current approval of management [§598.1(k)(2)(ii)]? Y/N		.Y			1
Current site map [§598.1(k)(2)(iii)]? Locate/identify tanks, transfer static connecting piping Y/N	ions,	Υ			
9. Preparer's name and signature [§598.1(k)(2)(iv)]? Y/N		Y			
10. Listing and description of spills for past 5 years [\$598.1(k)(2)(v)]? Y/f	N	Y			
11. An assessment of causes of spills, leaks, and releases for past 5 years §598.1(k)(2)(vi)]? Y/N		NA NO SPILLS IN 5 YRS		·	
12. SPR contain a spill response plan [\$598.1(k)(2)(x)]? Y/N/1 (incomplet	te)	Y in ICP			1.7
B. Periodic Inspections of Tank/Piping and Record keeping §598.1(k)(2 §598.6 &§598.8]	2)(viii) ,		14. 23.33 14. 23.33		1661 500 A
13. Is weekly monitoring performed between the tank/pipe and the secondar containment system for: a. UST [; \$598.6(b)(2)]? Y/N/X	гу	NA no USTS			

b. Underground piping [§599.15(b); §598.6(c)(1); §598.5(a)]? Can be in combination with: inventory with annual tightness test; vapor wells; gw wells; auto tank gauging; equiv. Y/N/X	NA no underground pipinf	
14. UST Systems - Monthly Inspections Monthly visual is performed [\$598.6(a)(1)]? Y/N/X/1 (records not retained for 10 yrs \$598.8(a))/2 (report signed, dated, certified \$598.8(b))/3 (records not in SPR)/4(operability)	NA no USTS	
15. AST Monthly (≥10% volume beneath ground) [§598.7(b)] a. Aboveground tank - Monthly leak detection is performed [§598.7(b)]? Y/N/X/1 (records not retained for 10 yrs §598.8(a))/ 2 (report signed, dated, certified §598.8(b)/ 3 (records not in SPR)	Y records on file at terminal	
b. Underground piping - Monthly leak detection is performed [\$598.6(c);\$598.7(b);\$599.15(b)]? Y/N/ 1 (records not retained for 10 yrs \$598.8(a))/ 2 (report signed, dated, certified \$598.8(b)/ 3 (records not in SPR)	NA no underground piping	
16. UST Systems - Annual Inspections [§598.6(a)(2)] Date: a. Automatic Line Leak Detector? Y/N(not performed)/1(no records in SPR)/2(records not retained 5 yrs)/3(no cert.)/4(not operational)	NA no USTS	
 b. Cathodic Protection System for Tanks? Y/N/X(not performed)/1(no records in SPR)/2(records not retained 5 yrs)/3(no cert.)/4(not maintained to achieve protection) 	NA no USTS	
c. Cathodic Protection System for Piping? Y/N(not performed)/1(no records in SPR)/ 2(records not retained 5 yrs)/3(no cert.)/4(not maintained to achieve protection)	NA no underground piping	
17. AST Systems - Arnual Inspections [\$598.7] Date Completed: 10/20/2010 a. Aboveground Tank- (1) Visual inspections performed [\$598.7(c)(2)]? Y/N/1 (records not in SPR)	Υ	
(2) For tank subject to corrosion, cathodic protection system is inspected by qualified technician and is maintained to achieve protection [§598.7(c)(1); §598.8(a); §598.8(b) & §598.9]?Y/N (not performed)/ X(not in contact with soil)/1(no records in SPR)/2 (records not retained 5 yrs)/3 (no cert.)/4 (not maintained to achieve protection)	Not in contact with soil	
b. Aboveground Piping - (1) Visual inspections performed [§598.7(c)(2)]? Y/N/1 (records not in SPR)	Υ	
(2) For piping subject to corrosion, cathodic protection system is inspected by qualified technician and is maintained to achieve protection [§598.7(c)(1); §598.8(a); §598.8(b) & §598.9]? Y/N(not performed)/ X(not in contact with soil)/ 1 (no records in SPR)/ 2 (records not retained 5 yrs)/3 (no cert.)/ 4 (not maintained to achieve protection)	Not in contact with soil; entire terminal system is inspected annually	
18. AST Systems - 5-year Inspections [§598.7(d)] Date: 10/1/08 Aboveground tanks and piping must undergo a 5-year inspection in accordance with a consensus code, standard, or practice. An assessment & evaluation must be made of structural soundness, system tightness, corrosion, wear, foundation weakness & operability. Reports are dated, signed, & certified [§598.8(b)] & records are maintained for 10-year period [§598.8(a)]. For tanks > 10,000 gal, the inspection is certified by a NYS-licensed professional engineer. The remaining life expectancy must be determined. a. Aboveground tanks? Y/N/X/ I (not in accordance with code)/ 2 (no assessment)/ 3 (no cert)/ 4 (records not retained 10 yrs)/ 5 (no cert. for tank>10,000 g)/ 6 (records not in SPR)	5 yr Tank inspection reports on file at terminal	
b. Aboveground piping? Y/N/X/ 1(not in accordance with code)/ 2(no assessment)/3(no cert)/4(records not retained 10 yrs)/5 (records not in SPR)	Y	

19. UST Inspection - Reconditioned Tanks With Liners [\$598.6(d)]? Y/N (not inspected internally)/X/1 (not performing to design specs)/2 (no assessment)/3 (no cert.)/4 (records not retained)/5 (records not in SPR)	NA no USTs		
20. Facility report on status of compliance [§598.1(k)(2)(vii)]?	Inspection reports		
C. Tank & Piping Certifications (Apply to tanks installed on or after 2/11/95) 21. Does the SPR contain a certification statement for design and installation of tank and piping systems - a. USTs [§599.6(g)(4)& (5)]? Y/N/ X (no USTs)/1 (record not available)/2 (no records for 5 yrs)/3 (records not in SPR)	NA tanks installed prior to 1995 X, no USTs		
b. ASTs [\$599.11(f)(4) & (5)]? Y/N/ X (no ASTs)/1 (record not available)/2 (no records for 5 yrs)/3 (records not in SPR)	NA tanks installed prior to 1995		:
c. Piping [§599.16(e)(3)&(4)]? Y/N/1 (record not available)/2 (no records for 5 yrs)/3 (records not in SPR)	NA tanks installed prior to 1995		
D. Life Expectancy/Warranty 22. UST secondary containment liner - liner life expectancy is specified in the SPR [§599.4(d)]? Y/N/X	NA		
23. Useful life for UST tank design, if < 30 years, is specified in the SPR [§599.3(c)(1)]? Y/N/X	NA		Î
24. Useful life for AST tank design, if < 30 years, is specified in the SPR [§599.8(b)(1)]? Y/N/X	NA		
25. Piping life expectancy is specified in the SPR? [§599.13(a)(1)]? Y/N	NA		
E. Additional Requirements		The second	
26. Are rupture disks replaced			6.4.40
a. Every 3 years, Y/N (no option selected)/X			
b. According to manufacturer's guidelines, Y/N (no option selected)/X			
c. On the basis of operating experience [§598.9(f)]?Y/N (no option selected)/X	Υ		
27. Does SPR contain a site assessment for UST, or AST with ≥10% volume beneath ground, for { closure[§598.10(e)]}; {change-in-service [§598.10(a)(2)} or {when directed by the department[§598.1(g)(3)]} Y/N/X (not applicable)/1 (inadequate)/2 (not in SPR §598.1(k)(4) &§598.10(e)(4))	NA, no USTs		
28. If facility have written procedures to prevent deliveries to the wrong tank, are they referenced in SPR [§598.4(b)(7)]? Y/N/X (single tank with no other fill ports, or facility has mated connections)	X, in Terminal Operation Manual		
	YES NO	<u>X</u>	Т
29. Transfer station [§599.17(c)(2)]: Transfer stations must have a permanently installed secondary containment system. Containment system must have an acceptable spill containment volume; satisfy permeability to substance stored; constructed, coated, or lined with materials that are compatible with substance stored; and equipped with a sump and manually-controlled drainage system (must be locked closed). Y/X/N (no containment)/1 (not perm. installed)/2 (unacceptable cont. vol.)/ 3 (permeable)/4(not maintained)/5 (incompatible)/6 (no sump or lockable drainage valve)	Υ		
To prevent mixing of incompatible substances: [§598.4(b)(7)] 30. Does the facility have written site procedures in SPR to prevent delivery to the wrong tank, fill ports with mated connections? Y/N/X (have written procedures, or facility has single tank of any type)	X, Terminal Operation Manual		

Attachment 3

11.1 OSRO Classifications, OSRO contracts, AMPD Checklist

The following pages include the updated OSRO Classifications, contracts/PREP, and a copy of the AMPD Checklist.

CONTRACTED RESPONSE RESOURCES CLASSIFICATIONS Sector New York

USCG Classified Oil Spill Removal Organization (OSRO)							
			Facil	ity Class	ification	Level	High
OSRO Name	Response Time	Environment Type	MM	W1	W2	W3	Volume Port
Ken's Marine Services, Inc.	45 minutes	Rivers/Canals	x	х	×		Yes
		Inland	х	х	x	×	
Atlantic Response Inc.	1-1/2 hours	Rivers/Canals	х				
·		Inland	Х				
Clean Harbors Environmental Services Inc.	1 hour	Rivers/Canals	x	х	х	×	
Miller Environmental Group, Inc.	1 hour	Rivers/Canals	х	х	х	×	
(Land) Miller's Launch (Marine)		Inland	х	х	х	х	
Marine Spill Response Corporation (MSRC)	2 hours	Rivers/Canals	х	х	х	×	
(MONO)		Inland	х	х	х	х	

USCG OSRO CLASSIFICATIONS (As of October 2002)

The USCG has classified OSROs according to their response capabilities, within each Captain of the Port (COTP) zone, for vessels and for facilities in four types of environments. Response capabilities are rated MM, W1, W2, or W3 as described below.

1IM	NIMUM EQUIPME	NT REQUIR	EMENTS FOR O	SRO CL	ASSIFICATIONS	
Classification	Resource Q Guideline	uantity es ^{2,3}	Maximum Facility F Times	Response	Maximum Vessel I Times	Response
		R	ivers/Canals ¹			
	Protective Boom:	4,000*ft				
ММ	EDRC: TSC:	1,200 bbls 2,400 bbls	High Volume Ports: Other Ports:	6 hours 12 hours	High Volume Ports: Other Ports:	12 hours 24 hours
	Protective Boom:	25,000*ft				
W ¹	EDRC: TSC:	1,875 bbls 3,750 bbls	High Volume Ports: Other Ports:	12 hours 24 hours	High Volume Ports: Other Ports:	12 hours 24 hours
	Protective Boom:	25,000*ft				
W ²	EDRC: TSC:	3,750 bbls 7,500 bbls	High Volume Ports: Other Ports:	30 hours 36 hours	High Volume Ports: Other Ports:	36 hours 48 hours
	Protective Boom:	25,000*ft				
W ³	EDRC: TSC:	7,500 bbls 15,000 bbls	High Volume Ports: Other Ports:	54 hours 60 hours	High Volume Ports: Other Ports:	60 hours 72 hours
			Great Lakes			
	Protective Boom:	6,000*ft				
ММ	EDRC: TSC:	1,250 bbls 2,500 bbls	All Ports:	6 hours	All Ports:	12 hours
	Protective Boom:	30,000*ft				
W ¹	EDRC: TSC:	6,250 bbls 12,500 bbls	High Volume Ports: Other Ports:	12 hours 24 hours	High Volume Ports: Other Ports:	12 hours 24 hours
	Protective Boom:	30,000*ft				
W ²	EDRC: TSC:	12,500 bbls 25,000 bbls	All Ports:	36 hours	All Ports:	42 hours
	Protective Boom:	30,000*ft				
W ³	EDRC: TSC:	25,000 bbls 50,000 bbls	All Ports:	60 hours	All Ports:	66 hours

USCG OSRO CLASSIFICATIONS (Cont'd) (As of October 2002)

The USCG has classified OSROs according to their response capabilities, within each Captain of the Port (COTP) zone, for vessels and for facilities in four types of environments. Response capabilities are rated MM, W1, W2, or W3 as described below.

1IM	NIMUM EQUIPM	ENT REQUIR	EMENTS FOR O	SRO CL	ASSIFICATIONS	
Classification	Resource Quantity Guidelines ^{2,3}		Maximum Facility Response		Maximum Vessel Response	
The state of the s	E-minimum and the Committee of the Commi	100 mm)()	Inland ¹		Bayus istilisesso	ingertick and down track to liver
	Protective Boom:	6,000* ft				
MM	EDRC: TSC:	1,200 bbls 2,400 bbls	High Volume Ports: Other Ports:	6 hours 12 hours	High Volume Ports: Other Ports:	12 hours 24 hours
	Protective Boom:	30,000* ft				
W ¹	EDRC: TSC:	12,500 bbls 25,000 bbls	High Volume Ports: Other Ports:	12 hours 24 hours	High Volume Ports: Other Ports:	12 hours 24 hours
	Protective Boom:	30,000* ft				
W^2	EDRC: TSC:	25,000 bbls 50,000 bbls	High Volume Ports: Other Ports:	30 hours 36 hours	High Volume Ports: Other Ports:	36 hours 48 hours
	Protective Boom:	30,000* ft				
W^3	EDRC: TSC:	50,000 bbls 100,000 bbls	High Volume Ports: Other Ports:	54 hours 60 hours	High Volume Ports: Other Ports:	60 hours 72 hours
			Nearshore			
	Protective Boom:	8,000* ft	1 Sala Valamas Dantas	C h	High Volume Ports: Other Locations:	12 hours
MM	EDRC: TSC:	1,200 bbls 2,400 bbls	High Volume Ports: Other Locations:	6 hours 12 hours	(for open ocean, plus from shore)	traver time
	Protective Boom:	30,000* ft				
W ¹	EDRC: TSC:	12,500 bbls 25,000 bbls	High Volume Ports: Other Locations:	12 hours 24 hours	High Volume Ports: Other Locations:	12 hours 24 hours
	Protective Boom:	30,000* ft				
W ²	EDRC: TSC:	25,000 bbls 50,000 bbls	High Volume Ports: Other Locations:	30 hours 36 hours	High Volume Ports: Other Locations:	36 hours 48 hours
	Protective Boom:	30,000* ft	High Volume Ports:	54 hours	High Volume Ports:	60 hours
W³	EDRC: TSC:	50,000 bbls 100,000 bbls	Other Locations: (for open ocean, plus time from shore)	60 hours s travel	Other Locations: (for open ocean, plus from shore)	72 hours travel time

USCG OSRO CLASSIFICATIONS (Cont'd) (As of October 2002)

The USCG has classified OSROs according to their response capabilities, within each Captain of the Port (COTP) zone, for vessels and for facilities in four types of environments. Response capabilities are rated MM, W1, W2, or W3 as described below

19111	VIIVIUW EQUIPIVI	EN! KEQUIK	EMENTS FOR O	SRO CL	ASSIFICATIONS	
assification	Resource Quantity Guidelines ^{2,3}		Maximum Facility Response		Maximum Vessel Response Times	
**************************************		Dischart Communication (Communication Communication Communication Communication Communication Communication Co	Offshore	SECTION FLORIDA		
	Protective Boom:	8,000* ft				
MM	EDRC: TSC:	1,200 bbls 2,400 bbls	High Volume Ports: Other Ports:	6 hours 12 hours	High Volume Ports: Other Ports:	12 hou 24 hou
	Protective Boom:	15,000* ft				
W^1	EDRC: TSC:	12,500 bbls 25,000 bbls	High Volume Ports: Other Ports:	24 hours 48 hours	High Volume Ports: Other Ports:	24 hou 48 hou
	Protective Boom:	15,000* ft				
W^2	EDRC: TSC:	25,000 bbls 50,000 bbls	High Volume Ports: Other Ports:	30 hours 36 hours	High Volume Ports: Other Ports:	36 hou 48 hou
	Protective Boom:	15,000 ft				
W^3	EDRC: TSC:	50,000 bbls 100,000 bbls	High Volume Ports: Other Ports:	54 hours 60 hours	High Volume Ports: Other Ports:	60 hou 72 hou
			Open Ocean			
	Protective Boom:	0 ft				
MM	EDRC: TSC:	1,200 bbls 2,400 bbls	High Volume Ports: Other Ports:	6 hours 12 hours	High Volume Ports: Other Ports:	12 hou 24 hou
	Protective Boom:	O ft				
W^1	EDRC: TSC:	12,500 bbls 25,000 bbls	High Volume Ports: Other Ports:	6 hours 12 hours	High Volume Ports: Other Ports:	12 hou 24 hou
	Protective Boom:	0 ft.				
W ²	EDRC: TSC:	25,000 bbls 50,000 bbls	High Volume Ports: Other Ports:	30 hours 36 hours	High Volume Ports: Other Ports:	36 hou 48 hou
	Protective Boom:	0 ft				_
W^3	EDRC: TSC:	50,000 bbls 100,000 bbls	High Volume Ports: Other Ports:	54 hours 60 hours	High Volume Ports: Other Ports:	60 hou 72 hou

¹ Rivers/canals include bodies of water, including the Intracoastal Waterway and other bodies artificially created for navigation, confined within an inland area and having a project depth of 12 feet (3.66 meters).

² EDRC stands for "effective daily recovery capacity," or the calculated recovery capacity of oil recovery devices determined by using a formula that takes into account limiting factors such as daylight, weather, sea state, and emulsified oil in the recovered material.

³ TSC stands for "temporary storage capacity," meaning sufficient storage capacity equal to twice the EDRC of an OSRO. Temporary storage may include inflatable bladders, rubber barges, certified barge capacity, or other temporary storage that can be utilized on scene at a spill response and which is designed and intended for the storage of flammable or combustible liquids. It does not include vessels or barges of opportunity for which no pre-arrangements have been made. Fixed shore-based storage capacity, ensured available by contract or other means, will be acceptable.

^{*} In addition, 1,000 feet of containment boom plus 300 feet per skimming system.

OSRO CONTRACTS AND PREP CERTIFICATIONS

KEN'S MARINE SERVICES, INC.



March 5, 2010

Ken's Marine Service, Inc. 117 East 22nd Street Bayonne, NJ 07002

RE: 2009 OSRO Equipment Deployment Documentation Request

Dear PREP Coordinator:

Please document your 2009 equipment deployment exercise requirements in accordance with the National Preparedness for Response and Exercise Program (PREP) guidelines by signing and returning this form. If a contract number is not shown below, please provide the contract number that you currently show on file. If another person with your Company will certify this 2009 PREP, please mark through your name and provide the form to that person to process.

Your signature will provide certification of OSRO compliance with the PREP guidelines, whereby you have properly deployed and exercised your oil spill removal equipment during the fiscal year of 2009.

OSRO EQUIPMENT DEPLOYMENT COMPLIANCE STATEMENT

The second secon
I hereby certify that the Company has met all equipment deployment requirements for 2009 in accordan with the USCG PREP guidelines.
JOYCE LUBACH
(Printed Name)
(Signatora) / Secretary Contract No.:
(Title)
Ken's Marine Service, Inc.
(Print Company Name)
3/0/2010 (Date)/
Please fax, or most preferably email, the completed original copy of this letter immediately or by April 2010 to our Compliance Consultant.
Angela Hardy O'Brien's Response Management Inc. 6620 Cypresswood Drive, Ste. 200 Spring, TX 77379
Fax: (281) 320-9700
Email: angela.hardy@obriensrm.com
If there are any questions, please contact Angela Hardy at 281-320-9796. Your immediate attention ar response is appreciated.
Sincerely, a. Dardy
KernYLambert

55 East Paulding Drive, Suite 109-309, Dallas GA 30157

HSE Manager

Office Telephone 678-363-5921

[MOTIVA ENTERPRISES LLC]

PROCUREMENT AGREEMENT FOR SERVICES

Seller: Ken's Marine Service, Inc. Agreement #: CMD 200014 Issue Date: 06/01/2010

To Be Used For:		Commodity Codes:	
SELLER: Address 1:	Ken's Marine Service, Inc. 116 East 22 nd Street Bayonne, NJ 07002	Invoicing Information: Please mail invoice with Freight bill (when Prepaid/Add to Invoice) and bills of lading. For questions regarding payment of invoices, please call: As indicated on Buyer's Release Document.	
Attn: Telephone: Fax: Email:	Raymond Huckemeyer 201-437-3541 201-221-8578 ampd@kensmarine.net		
Ship To: A	s Per Buyer's Release	Bill To: As Per Buyer's Release	

1. Payment Terms of Net 45 days will be based on the date invoice is received. All invoices and packing slips must reference the applicable Buyer Release Document or Account Code and be forwarded to the "Bill To" address. Failure to do so may delay or prevent payment.

Delivery term:	As Per Buyer's Release
Shipping Directions:	As Per Buyer's Release
Freight Charges:	(X) Prepaid & Allowed () Prepaid/Add to Invoice () Collect

Notice: This form contains a Liability-Indennity clause. Please read carefully.

This Procurement Agreement ("Agreement"), made on 06/01/2010 ("Effective Date"), and terminating on 06/01/2013, between Motiva Enterprises LLC, a company having its principal office at 910 Louisiana Street, Houston, TX 77002 ("Buyer") and Ken's Marine Service, Inc., a company incorporated under the laws of New Jersey and having its statutory seat / principal offices at 116 East 22nd Street, Bayonne, NJ 07002 ("Seller") for the supply of Services related to emergency response and preparedness support in regards to marine and landside spills, hazardous material releases and other emergency incidents (as further described in Attachment 1 hereto). In the event of any conflict between the terms and conditions set forth in a Buyer Release Document hereunder (also referred to as Purchase Order) and this Agreement, the terms and conditions of this Agreement prevail except to the extent the terms or conditions of the Buyer Release Document or Purchase Order specifically state they supersede or amend the terms or conditions of this Agreement.

Procurement Agreement for Services CMD 200014

PART 1 - CORE PROVISIONS

1. STRUCTURE / DEFINITIONS

- 1.1 This Agreement consists of the Preamble stated above, the Core Provisions in Part 1, the General Terms and Conditions in Part 2, the Attachments in Part 3, and Schedules, if any, in Part 4.
- 1.2 Unless otherwise specified, words and phrases within this Agreement and its various Attachments and (if applicable) Schedules shall have the respective meanings set forth in the definitions provision of Part 2.

2. NOTICES

- 2.1 Any notice under this Agreement shall only be effective if given in writing in English and given in one of the methods specified in Clause 19 of the General Terms and Conditions, Part 2. Service of notice by telex, e-mail or international airmail shall not be effective.
- 2.2 For notices given to Seller:

Attention: Raymond Huckemeyer Ken's Marine Service, Inc. 116 East 22rd Street Bayonne, NJ 07002 Phone: 201-437-3541 Fax: 201-221-8578 Email: ampd@kensmarine.net

2.3 For notices given to Buyer:

Attention: Alejandro Barrella Shell Oil Products US 910 Louisiana Street Houston, TX 77002 Phone: 713-241-7382

Email: ulejandro.barrella@shell.com

3. SIGNATURES

The Parties have caused this Agreement to be duly executed in duplicate original by their respective authorized representatives.

For:	SELLER.	For:	BUYER	
	w.		\mathcal{A}	
Signature:	Rymond Had	Signature:	- Jan	_
	: PAYMOND HUCK	<i>"</i>		RNEW
	OPS. mar		MON PROWNEMEN	
Date:	5-25-10	Date:	6-8-10	

Procurement Agreement for Services CMD WHITE 300014

[MOTIVA ENTERPRISES LLC]

PROCUREMENT AGREEMENT FOR SERVICES

Seller: Miller Environmental Group, Inc. Agreement #: CMD 200013 Issue Date: 05/10/2010

To Be Used For:		Commodity Codes:	
Seller: Address 1:	Miller Environmental Group, Inc. 538 Edwards Avenue Calverton, NY 11933	Invoicing Information: Please mail invoice with Freight bill (when Prepaid/Add to Invoice) and bills of lading. For questions regarding payment of invoices, please call: As indicated on Buyer's Release Document.	
Attn: Telephone: Fax: Email:	James H. Davey 631-369-4900 x210 631-369-4909 jdavey@millerenv.com	can: As mulcated on Dayer's Release Document.	
Ship To: A	s Per Buyer's Release	Bill To: As Per Buyer's Release	

1. Payment Terms of Net 45 days will be based on the date invoice is received. All invoices and packing slips must reference the applicable Buyer Release Document or Account Code and be forwarded to the "Bill To" address. Failure to do so may delay or prevent payment.

Delivery term:	As Per Buyer's Release	
Shipping Directions:	As Per Buyer's Release	
Freight Charges:	(X) Prepaid & Allowed () Prepaid/Add to Invoice () Collect	

Notice: This form contains a Liability-Indemnity clause. Please read carefully.

This Procurement Agreement ("Agreement"), made on 05/10/2010 ("Effective Date"), and terminating on 05/10/2013, between Motiva Enterprises LLC, a company having its principal office at 910 Louisiana Street, Houston, TX 77002 ("Buyer") and Miller Environmental Group, Inc., a company incorporated under the laws of New York and having its statutory seat / principal offices at 538 Edwards Avenue, Calverton, NY 11933 ("Seller") for the supply of Services related to emergency response and preparedness support in regards to marine and landside spills, hazardous material releases and other emergency incidents (as further described in Attachment 1 hereto). In the event of any conflict between the terms and conditions set forth in a Buyer Release Document hereunder (also referred to as Purchase Order) and this Agreement, the terms and conditions of this Agreement prevail except to the extent the terms or conditions of the Buyer Release Document or Purchase Order specifically state they supersede or amend the terms or conditions of this Agreement.

Procurement Agreement for Services CMD 200013

PART 1 - CORE PROVISIONS

1. STRUCTURE/DEFINITIONS

- 1.1 This Agreement consists of the Preamble stated above, the Core Provisions in Part 1, the General Terms and Conditions in Part 2, the Attachments in Part 3, and Schedules, if any, in Part 4.
- 1.2 Unless otherwise specified, words and phrases within this Agreement and its various Attachments and (if applicable) Schedules shall have the respective meanings set forth in the definitions provision of Part 2.

2. NOTICES

- 2.1 Any notice under this Agreement shall only be effective if given in writing in Bnglish and given in one of the methods specified in Clause 19 of the General Terms and Conditions, Part 2. Service of notice by telex, e-mail or international airmail shall not be effective.
- 2.2 For notices given to Seller:

Attention: James H. Davey Miller Brivironmental Group, Inc. 538 Edwards Avenue Calverton, NY 11933 Phone: 631-369-4900 x210 Pax: 631-369-4909

Bmail: jdavey@millerenv.com

2.3 For notices given to Buyer:

Attention: Alejandro Barrella Shell Oil Products US 910 Louisiana Street Houston, TX 77002 Phone: 713-241-7382

Email: alejandro.barrella@shell.com

3. SIGNATURES

The Parties have caused this Agreement to be duly executed in duplicate original by their respective authorized representatives.

Por:	For Millen ENVIRONMENTAR GROUP, INC
Signature:	Signature:
Print Name: Actions 1. BARR	EVA Print Namo: JAMES H. DAVEY
Title: STUIDA PROWNEMENT I	MALLACCA Fille: V.P.
Date: 6-8-10	Date:

Procurement Agreement for Services CMD 200013

ATLANTIC RESPONSE INC.



March 5, 2010

Atlantic Response, Inc. 12D Connerty Court East Brunswick, NJ 08816

RE: 2009 OSRO Equipment Deployment Documentation Request

Dear PREP Coordinator:

Please document your 2009 equipment deployment exercise requirements in accordance with the National Preparedness for Response and Exercise Program (PREP) guidelines by signing and returning this form. If a contract number is not shown below, please provide the contract number that you currently show on file. If another person with your Company will certify this 2009 PREP, please mark through your name and provide the form to that person to process.

Your signature will provide certification of OSRO compliance with the PREP guidelines, whereby you have properly deployed and exercised your oil spill removal equipment during the fiscal year of 2009.

OSRO EQUIPMENT DEPLOYMENT COMPLIANCE STATEMENT

hereby certify that the Company has met all equipment deployment requirements for 2009 in accordance with the USCG PREP guidelines.
RALPH DAYKE
Printed Name)
Julia Pala
Signaluko
DRECTOR OF OPERATIONS Contract No.: 470002195
Title)
Atlantic Response, Inc.
Print Company Name)
3/11/10
Date)
Please fax, or most preferably email, the completed original copy of this letter immediately or by April 5, 2010 to our Compliance Consultant.
Angela Hardy
D'Brien's Response Management Inc. 620 Cypresswood Drive, Ste. 200
Spring, TX 77379
Fax: (281) 320-9700
Email: angela.hardy@obriensrm.com
f there are any questions, please contact Angela Hardy at 281-320-9796. Your immediate attention and esponse is appreciated.
Sincerely, A. Hardy
(erry Lambert
HSÉ Manager

55 East Paulding Drive, Suite 109-309, Dallas GA 30157

Office Telephone 678-363-5921

CLEAN HARBORS ENVIRONMENTAL SERVICES, INC.



March 5, 2010

Sour MERGER

Clean Harbors Environmental Services, Inc.

30 Joseph Street Kingston, MA 02364

Tangston, IVIV 0200

2009 OSRO Equipment Deployment Documentation Request

Dear Mr. Hickman: MeTagen;

Please document your 2009 equipment deployment exercise requirements in accordance with the National Preparedness for Response and Exercise Program (PREP) guidelines by signing and returning this form. If a contract number is not shown below, please provide the contract number that you currently show on file. If another person with your Company will certify this 2009 PREP, please mark through your name and provide the form to that person to process.

Your signature will provide certification of OSRO compliance with the PREP guidelines, whereby you have properly deployed and exercised your oil spill removal equipment during the fiscal year of 2009.

OSRO EQUIPMENT DEPLOYMENT COMPLIANCE STATEMENT

I hereby certify that the Company has met all equipment deployment requirements for 2009 in accordance with the USCG PREP guidelines.

Hawk Hickman Scott METZGER	
(Printed Name)	there, ,
(Signature)	
(Signature) Vice Parsiners (Title)	Contract No.: RESA-0001-LDC
(Title)	
Clean Harbors Environmental Services, Inc.	
(Print Company Name)	
3-9-10	
(Date)	

Please fax, or most preferably email, the completed original copy of this letter immediately or by April 5, 2010 to our Compliance Consultant.

Angela Hardy O'Brien's Response Management Inc. 6620 Cypresswood Drive, Ste. 200 Spring, TX 77379

Fax: (281) 320-9700

Email: angela.hardy@obriensrm.com

If there are any questions, please contact Angela Hardy at 281-320-9796. Your immediate attention and response is appreciated.

Sincerely

Kerry Lambert HSE Manager

55 East Paulding Drive, Suite 109-309, Dallas GA 30157

Office Telephone 678-363-5921

MILLER ENVIRONMENTAL GROUP, INC.



June 11, 2010

James H. Davey Miller Environmental Group, Inc. 538 Edwards Ave. Calverton, NY 11933

RE: 2009 OSRO Equipment Deployment Documentation Request

Dear Mr. Davey:

James H. Davey (Printed Name)

Please document your 2009 equipment deployment exercise requirements in accordance with the National Preparedness for Response and Exercise Program (PREP) guidelines by signing and returning this form. If another person with your Company will certify this 2009 PREP, please mark through your name and provide the form to that person to process.

Your signature will provide certification of OSRO compliance with the PREP guidelines, whereby you have properly deployed and exercised your oil spill removal equipment during the fiscal year of 2009.

OSRO EQUIPMENT DEPLOYMENT COMPLIANCE STATEMENT

I hereby certify that the Company has met all equipment deployment requirements for 2009 in accordance with the USCG PREP guidelines.

(Signature)	
<u>Vice President</u> Agreemen (Title)	t No.: CMD 200013
Miller Environmental Group, Inc. (Print Company Name)	
6/1 8 /10 (Date)	
Please fax, or most preferably email , the completed copy of this le Compliance Consultant.	tter immediately or by June 20, 2010 to our
Angela Hardy O'Brien's Response Management Inc. 6620 Cypresswood Drive, Ste. 200 Spring, TX 77379	
Fax: (281) 320-9700	
Email: angela.hardy@obriensrm.com	
If there are any questions, please contact Angela Hardy at 281-320-979 appreciated.	6. Your immediate attention and response is
Sincerely,	
Kerry Lambert Health and Safety Manager	

55 East Paulding Drive, Suite 109-309, Dallas GA 30157

Office Telephone 678-363-5921

[MOTIVA ENTERPRISES LLC]

PROCUREMENT AGREEMENT FOR SERVICES

Seller: Miller Environmental Group, Inc. Agreement #: CMD 200013 Issue Date: 05/10/2010

To Be Used	For:	Commodity Codes:	
Seller: Address 1:	Miller Environmental Group, Inc. 538 Edwards Avenue Calverton, NY 11933	Invoicing Information: Please mail invoice with Freight bill (when Prepaid/Add to Invoice) and bills of lading. For questions regarding payment of invoices, please call: As indicated on Buyer's Release Document.	
Attn: Telephone: Fax: Email:	James H. Davey 631-369-4900 x210 631-369-4909 jdavey@millerenv.com		

Ship To:	As Per Buyer's Rele	ase	Bill To:	As Per Buyer's Release

Payment Terms of Net 45 days will be based on the date invoice is received. All invoices and
packing slips must reference the applicable Buyer Release Document or Account Code and be forwarded to
the "Bill To" address. Failure to do so may delay or prevent payment.

Delivery term:	As Per Buyer's Release
Shipping Directions:	As Per Buyer's Release
Freight Charges:	(X) Prepaid & Allowed () Prepaid/Add to Invoice () Collect

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This Procurement Agreement ("Agreement"), made on 05/10/2010 ("Effective Date"), and terminating on 05/10/2013, between Motiva Enterprises LLC, a company having its principal office at 910 Louisiana Street, Houston, TX 77002 ("Buyer") and Miller Environmental Group, Inc., a company incorporated under the laws of New York and having its statutory seat / principal offices at 538 Edwards Avenue, Calverton, NY 11933 ("Seller") for the supply of Services related to emergency response and preparedness support in regards to marine and landside spills, hazardous material releases and other emergency incidents (as further described in Attachment 1 hereto). In the event of any conflict between the terms and conditions set forth in a Buyer Release Document hereunder (also referred to as Purchase Order) and this Agreement, the terms and conditions of this Agreement prevail except to the extent the terms or conditions of the Buyer Release Document or Purchase Order specifically state they supersede or amend the terms or conditions of this Agreement.

Procurement Agreement for Services CMD 200013

PART 1 - CORE PROVISIONS

1. STRUCTURE / DEFINITIONS

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- 1.2 Unless otherwise specified, words and phrases within this Agreement and its various Attachments and (if applicable) Schedules shall have the respective meanings set forth in the definitions provision of Part 2.

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- 2.2 For notices given to Seller:

Attention: James H. Davoy Miller Environmental Group, Inc. 538 Edwards Avenue Calverton, NY 11933 Phone: 631-369-4900 x210 Fax: 631-369-4909

Email: jdavey@millerenv.com

2.3 For notices given to Buyer:

Attention: Alejandro Barrelia Shell Oil Products US 910 Louisiana Street Houston, TX 77002 Phone: 713-241-7382

Email: alejandro.barrella@shell.com

3. SIGNATURES

The Parties have caused this Agreement to be duly executed in duplicate original by their respective authorized representatives.

Por:		For:	Millan	ENVIRON M	an tate	GROUP, INC
Signatu			ture;	7116	> ジ	
Print N	ame: Authors 1. BARNEUM	Print I	Name:	Ames H.	DAVEY	<u></u>
Tide: _	STUIDA PROCUREMENT MANAGE	Fitle:	<u>V.P</u>	<u> </u>		
Date: _	6-9-10	Date:	5-6-	16		

MARINE SPILL RESPONSE CORPORATION (MSRC)



Don Toenshoff, Jr. Executive Vice President

March 17, 2010

Mr. Martin Padilla Motiva Enterprises 910 Louisiana St. One Shell Plaza – Room 694 Houston, TX 77002-4916

Dear Mr. Padilla:

The National Preparedness for Response Exercise Program (NPREP) Guidelines requires a response planholder to ensure that Equipment Deployment Exercise requirements are met on an annual basis. The NPREP Guidelines identify the minimum amount of equipment that must be deployed in Equipment Deployment Exercises.

This letter provides documentation to you that MSRC has completed the NPREP Equipment Deployment Exercise requirements for 2009. For purposes of Equipment Deployment Exercises under NPREP, each MSRC Region is considered a separate Oil Spill Removal Organization (OSRO). MSRC is divided into four regions, Eastern (Maine – Georgia, and the Mid-Continent), Southern (Florida - Texas including Puerto Rico and the U.S. Virgin Islands), California (self-explanatory) and Pacific/Northwest (Washington, Oregon and Hawaii). MSRC has deployed, at a minimum, the NPREP required amounts of each type of boom and one of each type of skimming system in the applicable regional inventory. This equipment has been deployed, if required, in each of the three types of operating environments listed in NPREP ("River & Canal", "Inland", and "Ocean"). Each of the four MSRC Regions has met these equipment deployment requirements in 2009. In addition, each Region has conducted extensive personnel training and has maintained its equipment according to a rigid preventative and corrective maintenance schedule.

MSRC has an aerial dispersant program, which is comprised of a contracted C-130 aircraft (based in Coolidge, AZ) and a contracted King Air BE-90A aircraft (based in Stennis, MS). MSRC's Dispersant Program, including the C-130 and King Air aircraft, are frequently exercised through internal training and drills. In addition to training, the aerial dispersant spray system on each aircraft was inspected monthly in accordance with stated MMS requirements. This letter provides documentation to you that MSRC has completed these requirements.

Documentation and records of the specific information relating to MSRC Equipment Deployment Exercises and Equipment Maintenance records are maintained in each MSRC Region. Additionally, highlights of when each MSRC Region satisfied the equipment deployment requirements and when the dispersant spray system inspections were conducted are available on the MSRC website (www.msrc.org) on the Customer Access page (USER ID: skimmer / PASSWORD: transrec).

Please feel free to contact the MSRC regions directly or me at (703) 326-5610 for additional information.

Sincerely

220 Spring Street

Suite 500

Herndon, VA 20170

Telephone 703 326 5600

Fax 703 326 5660

AERIAL OIL TRACKING RESOURCES

Judith A. Roos Vice President Marketing, Customer Services & Corporate Relations (703) 326-5617

February 4, 2011

Re: Aerial Oil Tracking Resources

Dear Customer:

On February 22, 2011, the Aerial Oil Tracking requirements of 33 CFR Part 154.1035 (b)(3)(vii) for MTR Facility Response Plans (FRPs) and 33 CFR Part 155.1035(i)(11), 33 CFR Part 155.1040(j)(11), and 33 CFR Part 155.1050(l) for Vessel Response Plans (VRPs) go into effect.

For planning purposes under these regulations, the Aerial Oil Tracking resources must be capable of supporting all response operations, including: mechanical recovery, dispersant application, and in situ burning. The Marine Spill Response Corporation (MSRC) has developed the following capability in conjunction with this new regulatory requirement that our plan holder customers may cite in their response plans, along with their citation of MSRC as the resource provider:

- Aerial surveillance aircraft;
- Along with the aircraft, the pilots and trained personnel to support oil spill response operations;
- For planning purposes, these resources are capable of arriving at the site of the discharge in advance of the arrival of response resources identified for Tiers 1, 2 and 3 planning timeframes; and
- Observation personnel trained in the protocols of oil spill reporting and assessment.

Observation personnel are primarily trained MSRC employees. The other resources are available through contracts or other approved means (specifically Letters of Intent ("LOIs") or other_agreements with various aircraft providers. These services are subject to availability of aircraft and personnel. Multiple aircraft providers are listed for each geographic Captain of the Port ("COTP") Zone.

MSRC will maintain lists of the potentially available aircraft providers, along with other documentation, by COTP zones within the respective MSRC Regional Response Center. These records will be made available upon request. MSRC will periodically review this capability by COTP zone and update the documentation as appropriate.

MSRC has provided a copy of this letter to US Coast Guard Headquarters personnel responsible for VRP compliance and to COTPs within MSRC's Operations Area for their information. Customers may use this letter in their FRP or VRP as they deem appropriate.

Sincerely,

Judite a long

AMPD CHECKLIST

AMPE	Response Coverage Information for	(Company Name)
1.	AMPD response provider (check one): ☐ Plan	Holder OSRO
	If OSRO, company name(s): Expiration Date	(contract/other approved means)
	Primary Ken's Marine Service, Inc.	Open ended
	Miller Environmental Group, Inc.	Open ended
	Marine Spill Response Corporation	Open ended
	Atlantic Response, Inc.	Open ended
2.	Equipment deployment personnel are (check ☐ Located at equipment site ☐ On re	
3.	Physical location (<i>street address</i>) of AMPD equipm storage) and qualified deployment personnel.	ent (boom/skimmer/temporary
	Equipment Address (*1-hour response time):	
	Boom:	
	Equipment Address (*2-hour response time):	
	Skimmer:	
	Temporary Storage:	

^{*}Planning Assumptions: On-water speed, 5 knots; land speed, 35 miles per hour; notification/mobilization – 30 minutes.

11.2 RESPONSE TEAM JOB DESCRIPTIONS

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Command	
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ICS ROLES AND RESPONSIBILITIES

COMMON RESPONSIBILITIES

The following is a checklist applicable to all personnel in an ICS organization:

- Receive assignment, including:
 - Job assignment
 - Resource order number and request number
 - Reporting location
 - Reporting time
 - Travel instructions
 - Special communications instructions
- Upon arrival, check-in at designated check-in location.
- Receive briefing from immediate supervisor.
- Acquire work materials.
- Supervisors maintain accountability for assigned personnel.
- Organize and brief subordinates.
- Know your assigned radio frequency(s) and ensure communications equipment is operating properly.
- Use clear text and ICS terminology (no codes) in all communications.
- Complete forms and reports required of the assigned position and send to Documentation Unit.
- Maintain unit records, including Unit/Activity Log (ICS Form 214).
- Response to demobilization orders and brief subordinates regarding demobilization.

UNIT LEADER RESPONSIBILITIES

In ICS, a Unit Leader's responsibilities are common to all units in all parts of the organization. Common responsibilities of Unit Leaders are listed below.

- Review common responsibilities.
- Receive briefing from Incident Commander, Section Chief or Branch Director, as appropriate.
- Participate in incident planning meetings, as required.
- Determine current status of unit activities.
- Order additional unit staff, as appropriate.
- Determine resource needs.
- Confirm dispatch and estimated time of arrival of staff and supplies.
- Assign specific duties to staff; supervise staff.
- Develop and implement accountability, safety and security measures for personnel and resources.
- Supervise demobilization of unit, including storage of supplies.
- Provide Supply Unit Leader with a list of supplies to be replenished.
- Maintain unit records, including Unit/Activity Log (ICS Form 214).

COMMAND

Incident Commander	11
Information Officer	11
Liaison Officer	12
Safety Officer	12
Legal Officer	12

INCIDENT COMMANDER

- Assess the situation and/or obtain a briefing from the prior IC.
- Determine Incident Objectives and strategy.
- Establish the immediate priorities.
- Establish an ICP.
- Brief Command Staff and Section Chiefs.
- Review meetings and briefings.
- Establish an appropriate organization.
- Ensure planning meetings are scheduled as required.
- Approve and authorize the implementation of an IAP.
- Ensure that adequate safety measures are in place.
- Coordinate activity for all Command and General Staff.
- Coordinate with key people and officials.
- Approve requests for additional resources or for the release of resources.
- Keep agency administrator informed of incident status.
- Approve the use of trainees, volunteers, and auxiliary personnel.
- Authorize release of information to the news media.
- Ensure incident Status Summary (ICS Form 209) is completed and forwarded to appropriate higher authority.
- Order the demobilization of the incident when appropriate.

INFORMATION OFFICER

- Determine from the IC if there are any limits on information release.
- Develop material for use in media briefings.
- Obtain IC approval of media releases.
- Inform media and conduct media briefings.
- Arrange for tours and other interviews or briefings that may be required.
- Obtain media information that may be useful to incident planning.
- Maintain current information summaries and/or displays on the incident and provide information on the status of the incident to assigned personnel.

LIAISON OFFICER

- Be a contact point for Agency Representatives.
- Maintain a list of assisting and cooperating agencies and Agency Representatives.
 Monitor check-in sheets daily to ensure that all Agency Representatives are identified.
- Assist in establishing and coordinating interagency contacts.
- Keep agencies supporting the incident aware of incident status.
- Monitor incident operations to identify current or potential inter-organizational problems.
- Participate in planning meetings, providing current resource status, including limitations and capability of assisting agency resources.
- Coordinate response resource needs for Natural Resource Damage Assessment and Restoration (NRDAR) activities with the OPS during oil and HAZMAT responses.
- Coordinate response resource needs for incident investigation activities with the OPS.
- Ensure that all required agency forms, reports and documents are completed prior to demobilization.
- Coordinate activities of visiting dignitaries.

SAFETY OFFICER

- Participate in planning meetings.
- Identify hazardous situations associated with the incident.
- Review the IAP for safety implications.
- Exercise emergency authority to stop and prevent unsafe acts.
- Investigate accidents that have occurred within the incident area.
- Review and approve the medical plan.
- Develop the Site Safety Plan and publish Site Safety Plan summary (ICS Form 208) as required.

LEGAL OFFICER

- Participate in planning meetings, if requested.
- Advise on legal issues relating to in-situ burning, use of dispersants, and other alternative response technologies.
- Advise on legal issues relating to differences between Natural Resource Damage Assessment Restoration (NRADR) and response activities.
- Advise on legal issues relating to investigations.
- Advise on legal issues relating to finance and claims.
- Advise on legal issues relating to response.

OPERATIONS

Operations Section Chief	. 14
Branch Director	. 14
Division/Group Supervisor	. 14
Staging Area Manager	. 15
Air Operations Branch Director	15

OPERATIONS SECTION CHIEF

- Develop operations portion of IAP.
- Brief and assign Operations Section personnel in accordance with the IAP.
- Supervise Operations Section.
- Determine need and request additional resources.
- Review suggested list of resources to be released and initiate recommendation for release of resources.
- Assemble and disassemble strike teams assigned to the Operations Section.
- Report information about special activities, events, and occurrences to the IC.
- Respond to resource requests in support of NRDAR activities.

BRANCH DIRECTOR

- Develop with subordinates alternatives for Branch control operations.
- Attend planning meetings at the request of the OPS.
- Review Division/Group Assignment Lists (ICS Form 204) for Divisions/Groups within the Branch. Modify lists based on effectiveness of current operations.
- Assign specific work tasks to Division/Group Supervisors.
- Supervise Branch operations.
- Resolve logistic problems reported by subordinates.
- Report to OPS when: the IAP is to be modified; additional resources are needed; surplus resources are available; or hazardous situations or significant events occur.
- Approve accident and medial reports originating within the Branch.

DIVISION/GROUP SUPERVISOR

- Implement IAP for Division/Group.
- Provide the IAP to Strike Team Leaders, when available.
- Identify increments assigned to the Division/Group.
- Review Division/Group assignments and incident activities with subordinates and assign tasks.
- Ensure that the IC and/or Resources Unit is advised of all changes in the status of resources assigned to the Division/Group.
- Coordinate activities with adjacent Division/Group.
- Determine need for assistance on assigned tasks.
- Submit situation and resources status information to the Branch Director or the OPS.
- Report hazardous situations, special occurrences, or significant events (e.g., accidents, sickness, discovery of unanticipated sensitive resources) to the immediate supervisor.
- Ensure that assigned personnel and equipment get to and from assignments in a timely and orderly manner.
- Resolve logistics problems within the Division/Group.
- Participate in the development of Branch plans for the next operational period.

STAGING AREA MANAGER

- Establish Staging Area layout.
- Determine any support needs for equipment, feeding, sanitation and security.
- Establish check-in function as appropriate.
- Post areas for identification and traffic control.
- Request maintenance service for equipment at Staging Area as appropriate.
- Respond to request for resource assignments
- Obtain and issue receipts for radio equipment and other supplies distributed and received at Staging Area.
- Determine required resource levels from the OPS.
- Advise the OPS when reserve levels reach minimums.
- Maintain and provide status to Resource Unit of all resources in Staging Area.
- Demobilize Staging Area in accordance with the Incident Demobilization Plan.

AIR OPERATIONS BRANCH DIRECTOR

- Organize preliminary air operations.
- Request declaration (or cancellation) of restricted air space
- Participate in preparation of the IAP through the OPS. Insure that the air operations
 portion of the IAP takes into consideration the Air Traffic Control requirements of
 assigned aircraft.
- Perform operational planning for air operations.
- Prepare and provide Air Operations Summary Worksheet (ICS Form 220) to the Air Support Group and Fixed-Wing Bases.
- Determine coordination procedures for use by air organization with ground Branches,
 Divisions, or Groups.
- Coordinate with appropriate Operations Section personnel.
- Supervise all air operations activities associated with the incident.
- Evaluate helibase locations.
- Establish procedures for emergency reassignment of aircraft.
- Schedule approved flights of non-incident aircraft in the restricted air space area.
- Coordinate with the Operations Coordination Center (OCC) through normal channels on incident air operations activities.
- Inform the Air Tactical Group Supervisor of the air traffic situation external to the incident.
- Consider requests for non-tactical use of incident aircraft.
- Resolve conflicts concerning non-incident aircraft.
- Coordinate with FAA.
- Update air operations plans.
- Report to the OPS on air operations activities.
- Report special incidents/accidents.
- Arrange for an accident investigation team when warranted.

PLANNING

Planning Section Chief	17
Resources Unit Leader	17
Situation Unit Leader	17
Documentation Unit Leader	18
Demobilization Unit Leader	18
Environmental Unit Leader	19

PLANNING SECTION CHIEF

- Collect and process situation information about the incident.
- Supervise preparation of the IAP.
- Provide input to the IC and the OPS in preparing the IAP.
- Chair planning meetings and participate in other meetings as required.
- Reassign out-of-service personnel already on-site to ICS organizational positions as appropriate.
- Establish information requirements and reporting schedules for Planning Section Units (e.g., Resources, Situation Units).
- Determine the need for any specialized resources in support of the incident.
- If requested, assemble and disassemble Strike Teams and Task Forces not assigned to Operations.
- Establish special information collection activities as necessary (e.g., weather, environmental, toxics, etc.).
- Assemble information on alternative strategies.
- Provide periodic predictions on incident potential.
- Report any significant changes in incident status.
- Compile and display incident status information.
- Oversee preparation and implementation of the Incident Demobilization Plan.
- Incorporate plans (e.g., Traffic, Medical, Communications, Site Safety) into the IAP.

RESOURCES UNIT LEADER

- Establish the check-in function at incident locations.
- Prepare Organization Assignment List (ICS Form 203) and Organization Chart (ICS Form 207).
- Prepare appropriate parts of Division Assignment Lists (ICS Form 204).
- Prepare and maintain the ICP display (to include organization chart and resource allocation and deployment).
- Maintain and post the current status and location of all resources.
- Maintain master roster of all resources checked in at the incident.

SITUATION UNIT LEADER

- Begin collection and analysis of incident data as soon as possible.
- Prepare, post, or disseminate resource and situation status information as required, including special requests.
- Prepare periodic predictions or as requested by the PSC.
- Prepare the Incident Status Summary Form (ICS Form 209).
- Provide photographic services and maps if required.

DOCUMENTATION UNIT LEADER

- Set up work area; begin organization of incident files.
- Establish duplication service; respond to requests.
- File all official forms and reports.
- Review records for accuracy and completeness; inform appropriate units of errors or omissions.
- Provide incident documentation as requested.
- Store files for post-incident use.

DEMOBILIZATION UNIT LEADER

- Participate in planning meetings as required.
- Review incident resource records to determine the likely size and extent of demobilization effort.
- Based on the above analysis, add additional personnel, workspace, and supplies as needed.
- Coordinate demobilization with Agency Representatives.
- Monitor the on-going Operations Section resource needs.
- Identify surplus resources and probable release time.
- Develop incident check-out function for all units.
- Evaluate logistics and transportation capabilities to support demobilization.
- Establish communications with off-incident facilities, as necessary.
- Develop an Incident Demobilization Plan detailing specific responsibilities and release priorities and procedures.
- Prepare appropriate directories (e.g., maps, instructions, etc.) for inclusion in the demobilization plan.
- Distribute demobilization plan (on and off-site).
- Provide status reports to appropriate requestors.
- Ensure that all Sections/Units understand their specific demobilization responsibilities.
- Supervise execution of the Incident Demobilization Plan.
- Brief the PSC on demobilization progress.

ENVIRONMENTAL UNIT LEADER

- Participate in Planning Section meetings.
- Identify sensitive areas and recommend response priorities.
- Following consultation with natural resource trustees, provide input on wildlife protection strategies (e.g., removing oiled carcasses, pre-emptive capture, hazing, and/or capture and treatment).
- Determine the extent, fate and effects of contamination.
- Acquire, distribute and provide analysis of weather forecasts.
- Monitor the environmental consequences of cleanup actions.
- Develop shoreline cleanup and assessment plans. Identify the need for, and prepare any special advisories or orders.
- Identify the need for, and obtain, permits, consultations, and other authorizations including Endangered Species Act (ESA) provisions.
- Following consultation with the FOSC's Historical/Cultural Resources Technical Specialist identify and develop plans for protection of affected historical/cultural resources.
- Evaluate the opportunities to use various response technologies.
- Develop disposal plans.
- Develop a plan for collecting, transporting, and analyzing samples.

LOGISTICS

Logistics Section Chief	21
Service Branch Director	21
Communications Unit Leader	22
Medical Unit Leader	22
Food Unit Leader	22
Support Branch Director	23
Supply Unit Leader	23
Facility Unit Leader	23
Ground Support Unit Leader	24
Vessel Support Unit Leader	24

LOGISTICS SECTION CHIEF

- Plan the organization of the Logistics Section.
- Assign work locations and preliminary work tasks to Section personnel.
- Notify the Resources Unit of the Logistics Section units activated including names and locations of assigned personnel.
- Assemble and brief Branch Directors and Unit Leaders.
- Participate in preparation of the IAP.
- Identify service and support requirements for planned and expected operations.
- Provide input to and review the Communications Plan, Medical Plan and Traffic Plan.
- Coordinate and process requests for additional resources.
- Review the IAP and estimate Section needs for the next operational period.
- Advise on current service and support capabilities.
- Prepare service and support elements of the IAP.
- Estimate future service and support requirements.
- Receive Incident Demobilization Plan from Planning Section.
- Recommend release of Unit resources in conformity with Incident Demobilization Plan.
- Ensure the general welfare and safety of Logistics Section personnel.

SERVICE BRANCH DIRECTOR

- Determine the level of service required to support operations.
- Confirm dispatch of Branch personnel.
- Participate in planning meetings of Logistics Section personnel.
- Review the IAP.
- Organize and prepare assignments for Service Branch personnel.
- Coordinate activities of Branch Units.
- Inform the LSC of Branch activities.
- Resolve Service Branch problems.

COMMUNICATIONS UNIT LEADER

- Prepare and implement the Incident Radio Communications Plan (ICS Form 205).
- Ensure the Incident Communications Center and the Message Center is established.
- Establish appropriate communications distribution/maintenance locations within the Base/Camp(s).
- Ensure communications systems are installed and tested.
- Ensure an equipment accountability system is established.
- Ensure personal portable radio equipment from cache is distributed per Incident Radio Communications Plan.
- Provide technical information as required on:
 - Adequacy of communications systems currently in operation.
 - Geographic limitation on communications systems.
 - Equipment capabilities/limitations.
 - Amount and types of equipment available.
 - Anticipated problems in the use of communications equipment.
- Supervise Communications Unit activities.
- Maintain records on all communications equipment as appropriate.
- Ensure equipment is tested and repaired.
- Recover equipment from Units being demobilized.

MEDICAL UNIT LEADER

- Participate in Logistics Section/Service Branch planning activities.
- Prepare the Medical Plan (ICS Form 206).
- Prepare procedures for major medical emergency.
- Declare major emergency as appropriate.
- Respond to requests for medical aid, medical transportation, and medical supplies.
- Prepare and submit necessary documentation.

FOOD UNIT LEADER

- Determine food and water requirements.
- Determine the method of feeding to best fit each facility or situation.
- Obtain necessary equipment and supplies and establish cooking facilities.
- Ensure that well-balanced menus are provided.
- Order sufficient food and potable water from the Supply Unit.
- Maintain an inventory of food and water.
- Maintain food service areas, ensuring that all appropriate health and safety measures are being followed.
- Supervise caterers, cooks, and other Food Unit personnel as appropriate.

SUPPORT BRANCH DIRECTOR

- Determine initial support operations in coordination with the LSC and Service Branch Director.
- Prepare initial organization and assignments for support operations.
- Assemble and brief Support Branch personnel.
- Determine if assigned Branch resources are sufficient.
- Maintain surveillance of assigned units work progress and inform the LSC of their activities.
- Resolve problems associated with requests from the Operations Section.

SUPPLY UNIT LEADER

- Participate in Logistics Section/Support Branch planning activities.
- Determine the type and amount of supplies en route.
- Review the IAP for information on operations of the Supply Unit.
- Develop and implement safety and security requirements.
- Order, receive, distribute, and store supplies and equipment.
- Receive and respond to requests for personnel, supplies, and equipment.
- Maintain an inventory of supplies and equipment.
- Service reusable equipment.
- Submit reports to the Support Branch Director.

FACILITY UNIT LEADER

- Review the IAP.
- Participate in Logistics Section/Support Branch planning activities.
- Determine requirements for each facility, including the ICP.
- Prepare layouts of incident facilities.
- Notify Unit Leaders of facility layout.
- Activate incident facilities.
- Provide Base and Camp Managers and personnel to operate facilities.
- Provide sleeping facilities.
- Provide security services.
- Provide facility maintenance services (e.g., sanitation, lighting, clean up).
- Demobilize Base and Camp facilities.
- Maintain facility records

GROUND SUPPORT UNIT LEADER

- Participate in Support Branch/Logistics Section planning activities.
- Develop and implement the Traffic Plan.
- Support out-of-service resources.
- Notify the Resources Unit of all status changes on support and transportation vehicles.
- Arrange for and activate fueling, maintenance, and repair of ground resources.
- Maintain Support Vehicle Inventory and transportation vehicles (ICS Form 218).
- Provide transportation services, IAW requests from the LSC or Support Branch Director.
- Collect information on rented equipment.
- Requisition maintenance and repair supplies (e.g., fuel, spare parts).
- Maintain incident roads.
- Submit reports to Support Branch Director as directed.

VESSEL SUPPORT UNIT LEADER

- Participate in Support Branch/Logistics Section planning activities.
- Coordinate development of the Vessel Routing Plan.
- Coordinate vessel transportation assignments with the Protection and Recovery Branch or other sources of vessel transportation.
- Coordinate water-to-land transportation with the Ground Support Unit, as necessary.
- Maintain a prioritized list of transportation requirements that need to be scheduled with the transportation source.
- Support out-of-service vessel resources, as requested.
- Arrange for fueling, dockage, maintenance and repair of vessel resources, as requested.
- Maintain inventory of support and transportation vessels.

FINANCE/ADMINISTRATION

Finance/Administration Section Chief	26
Time Unit Leader	26
Procurement Unit Leader	27
Compensation/Claims Unit Leader	27
Cost Unit Leader	28

FINANCE/ADMINISTRATION SECTION CHIEF

- Attend planning meetings as required.
- Manage all financial aspects of an incident.
- Provide financial and cost analysis information as requested.
- Gather pertinent information from briefings with responsible agencies.
- Develop an operating plan for the Finance/Administration Section; fill supply and support needs.
- Determine the need to set up and operate an incident commissary.
- Meet with Assisting and Cooperating Agency Representatives, as needed.
- Maintain daily contact with agency(s) administrative headquarters on Finance/Administration matters.
- Ensure that all personnel time records are accurately completed and transmitted, according to policy.
- Provide financial input to demobilization planning.
- Ensure that all obligation documents initiated at the incident are properly prepared and completed.
- Brief administrative personnel on all incident-related financial issues needing attention or follow-up prior to leaving incident.

TIME UNIT LEADER

- Determine incident requirements for time recording function.
- Determine resource needs.
- Contact appropriate agency personnel/representatives.
- Ensure that daily personnel time recording documents are prepared and in compliance with policy.
- Establish time unit objectives.
- Maintain separate logs for overtime hours.
- Establish commissary operation on larger or long-term incidents as needed.
- Submit cost estimate data forms to the Cost Unit, as required.
- Maintain records security.
- Ensure that all records are current and complete prior to demobilization.
- Release time reports from assisting agency personnel to the respective Agency Representatives prior to demobilization.
- Brief the Finance/Administration Section Chief on current problems and recommendations, outstanding issues, and follow-up requirements.

PROCUREMENT UNIT LEADER

- Review incident needs and any special procedures with Unit Leaders, as needed.
- Coordinate with local jurisdiction on plans and supply sources.
- Obtain the Incident Procurement Plan.
- Prepare and authorize contracts and land-use agreements.
- Draft memoranda of understanding as necessary.
- Establish contracts and agreements with supply vendors.
- Provide for coordination between the Ordering Manager, agency dispatch, and all other procurement organizations supporting the incident.
- Ensure that a system is in place that meets agency property management requirements. Ensure proper accounting for all new property.
- Interpret contracts and agreements; resolve disputes within delegated authority.
- Coordinate with the Compensation/Claims Unit for processing claims.
- Coordinate use of impress funds, as required.
- Complete final processing of contracts and send documents for payment.
- Coordinate cost data in contracts with the Cost Unit Leader.
- Brief the Finance/Administration Section Chief on current problems and recommendations, outstanding issues, and follow-up requirements.

COMPENSATION/CLAIMS UNIT LEADER

- Establish contact with the incident SO and LO (or Agency Representatives if no LO is assigned).
- Determine the need for Compensation for Injury and Claims Specialists and order personnel as needed.
- Establish a Compensation for Injury work area within or as close as possible to the Medical Unit.
- Review Incident Medical Plan (ICS Form 206).
- Ensure that Compensation/Claims Specialists have adequate workspace and supplies.
- Review and coordinate procedures for handling claims with the Procurement Unit.
- Brief the Compensation/Claims Specialists on incident activity.
- Periodically review logs and forms produced by the Compensation/Claims Specialists to ensure that they are complete, entries are timely and accurate and that they are in compliance with agency requirements and policies.
- Ensure that all Compensation for Injury and Claims logs and forms are complete and routed appropriately for post-incident processing prior to demobilization.
- Keep the Finance/Administration Section Chief briefed on Unit status and activity.
- Demobilize unit in accordance with the Incident Demobilization Plan.

COST UNIT LEADER

- Coordinate cost reporting procedures.
- Collect and record all cost data.
- Develop incident cost summaries.
- Prepare resources-use cost estimates for the Planning Section.
- Make cost-saving recommendations to the Finance/Administration Section Chief.
- Ensure all cost documents are accurately prepared.
- Maintain cumulative incident cost records.
- Complete all records prior to demobilization.
- Provide reports to the Finance/Administration Section Chief.

11.3 Material Safety Data Sheets (MSDS)

The local COTP requires that the MSDS be kept in the OPA'90 Plan. Therefore, the MSDS for the major products stored at this Facility are in this Annex. A complete list of all MSDS is located at the Facility.

MATERIAL SAFETY DATA SHEET Revision Date: 04/14/2003

SECTION 1 PRODUCT AND COMPANY IDENTIFICATION

PRODUCT: Denatured Ethanol MSDS NUMBER: 5708M - 2

PRODUCT CODE(S): 05482

MANUFACTURER ADDRESS: Motiva Enterprises LLC, P.O. Box 4540, Houston, TX. 77210-4540

TELEPHONE NUMBERS

Spill Information: (877) 242-7400 Health Information: (877) 504-9351 MSDS Assistance Number: (877) 276-7285

SECTION 2 PRODUCT/INGREDIENTS

CAS# CONCENTRATION INGREDIENTS

Mixture 100 %weight Denatured Ethanol
64-17-5 95 - 99.99 %weight Ethanol
Mixture 0 - 4.99 %weight Unleaded Gasoline
108-88-3 0 - 1.49 %weight Toluene
1330-20-7 0 - 1.49 %weight Xylene, mixed isomers
71-43-2 0 - 0.24 %weight Benzene
100-41-4 0 - 0.26 %weight Ethyl Benzene
0 - 2.49 %weight Miscellaneous Hydrocarbons

NOTE: Content of Gasoline components will vary; Individual components may be present from trace amounts up to the maximum shown.

SECTION 3 HAZARDS IDENTIFICATION

EMERGENCY OVERVIEW

Appearance & Odor: Clear liquid. Alcohol odor.

Health Hazards: Causes severe eye irritation. May cause skin irritation. May be harmful or fatal if swallowed. Do not induce vomiting. May cause aspiration pneumonitis. May cause CNS depression.

Physical Hazards: Material is extremely flammable and heavier than air.

Vapors may travel across the ground and reach remote ignition sources causing a flashback fire danger.

NFPA Rating (Health, Fire, Reactivity): 1, 3, 0

Hazard Rating:Least - 0 Slight - 1 Moderate - 2 High - 3

Extreme - 4

Inhalation:

In applications where vapors (caused by high temperature) or mists (caused by mixing or spraying) are created, breathing may cause a mild burning sensation in the nose, throat and lungs. Breathing of high vapor concentrations may cause CNS depression, evidenced by dizziness, light-headedness, headache, nausea, drowsiness, and loss of coordination. Continued inhalation may result in unconsciousness.

Eye Irritation:

Severely irritating to the eyes causing pain, redness, swelling and blurred vision.

Skin Contact:

May be irritating to the skin causing a burning sensation, redness and/or swelling. Prolonged or repeated skin contact can cause defatting and drying of the skin which may result in a burning sensation and a dried, cracked appearance.

Ingestion:

This material may be harmful or fatal if swallowed. Ingestion may result in vomiting; aspiration (breathing) of vomitus into lungs must be avoided as even small quantities may result in aspiration pneumonitis. Generally considered to have a low order of acute oral toxicity.

Other Health Effects:

Carcinogenic in animal tests. Gasoline has been tested by API in a long-term inhalation test in mice and rats. There was an increased incidence of liver cancer in female mice. Male rats had a dose related increase in kidney tumors. This effect was due to formation of alpha-2u-globulin in the rats. This material is not formed in humans and is therefore not considered relevant. Material is suspected of causing cancer in laboratory animals. See Section 11. Material may cause birth defects and/or miscarriages. See Section 11.

Refer to Section 11, Toxicological Information, for specific information on the following effects: Developmental Toxicity, Genotoxicity

Primary Target Organs:

The following organs and/or organ systems may be damaged by overexposure to this material and/or its components:

Cardiovascular System, Blood/Blood Forming Organs, Kidney, Liver Signs and Symptoms:

Irritation as noted above. Aspiration pneumonitis may be evidenced by coughing, labored breathing and cyanosis (bluish skin); in severe cases death may occur. Damage to blood-forming organs may be evidenced by: a) easy fatigability and pallor (RBC effect), b) decreased resistance to infection (WBC effect), c) excessive bruising and bleeding (platelet effect). Kidney damage may be indicated by changes in urine output or appearance, pain upon urination or in the lower back or general edema (swelling from fluid retention). Liver damage may be indicated by loss of appetite, jaundice (yellowish skin and eye color), fatigue and sometimes pain and swelling in the upper right abdomen.

For additional health information, refer to section 11.

SECTION 4 FIRST AID MEASURES

Inhalation:

Move victim to fresh air and provide oxygen if breathing is difficult. Get medical attention. If the victim has difficulty breathing or tightness of the chest, is dizzy, vomiting or unresponsive, give 100% oxygen with rescue breathing or CPR as required and transport to the nearest medical facility.

Skin:

Remove contaminated clothing. Flush with large amounts of water for at least 15 minutes and follow by washing with soap if available. If redness, swelling, pain and/or blisters occur, transport to the nearest medical facility for additional treatment.

Eye:

Immediately flush eyes with large amounts of water for at least 30 minutes, by the clock, while holding eyelids open. Transport to nearest medical facility for additional treatment.

Ingestion:

DO NOT take internally. Do NOT induce vomiting. If vomiting occurs spontaneously, keep head below hips to prevent aspiration of liquid into lungs. Get medical attention. In general no treatment is necessary unless large quantities are swallowed, however, get medical advice. Have victim rinse mouth out with water, then drink sips of water to remove taste from mouth.

Note to Physician:

If more than 2.0ml/kg body weight has been ingested and vomiting has not occurred, emesis should be induced with supervision. Keep victim's head below hips to prevent aspiration. If symptoms such as loss of gag reflex, convulsions, or unconsciousness occur before emesis, gastric lavage using a cuffed endotracheal tube should be considered.

SECTION 5 FIRE FIGHTING MEASURES

Flash Point [Method]: -40 °F/-40 °C [Tag Flammability in Air: 1.3%V - 7.6 %volume

-40 °F/-40 °C [Tagliabue Closed Cup]

Extinguishing Media:

Use water fog, foam, dry chemical or carbon dioxide (CO2) to extinguish flames. Do not use a direct stream of water. Material will float and can be re-ignited on surface of water.

Fire Fighting Instructions:

WARNING! DANGER! EXTREMELY FLAMMABLE. Clear fire area of all non-emergency personnel. Only enter confined fire space with full bunker gear, including a positive pressure, NIOSH-approved, self-contained breathing apparatus. Cool surrounding equipment, fire-exposed containers and structures with water. Container areas exposed to direct flame contact should be cooled with large quantities of water (500 gallons water per minute flame impingement exposure) to prevent weakening of container structure.

Unusual Fire Hazards:

Vapors are heavier than air accumulating in low areas and traveling along the ground away from the handling site. Do not weld, heat or drill on or near container. However, if emergency situations require drilling, only trained emergency personnel should drill.

SECTION 6 ACCIDENTAL RELEASE MEASURES

Protective Measures:

DANGER! EXTREMELY FLAMMABLE! Eliminate potential sources of ignition. Handling equipment must be bonded and grounded to prevent sparking.

Spill Management:

Dike and contain spill.

FOR LARGE SPILLS: Remove with vacuum truck or pump to storage/salvage vessels.

FOR SMALL SPILLS: Soak up residue with an absorbent such as clay, sand or other suitable material. Place in non-leaking container and seal tightly for proper disposal.

Reporting:

U.S. regulations require reporting releases of this material to the environment which exceed the reportable quantity to the National Response Center at (800)424-8802.

CWA: This product is an oil as defined under Section 311 of EPA's Clean Water Act (CWA). Spills into or leading to surface waters that cause a sheen must be reported to the National Response Center, 1-800-424-8802.

SECTION 7 HANDLING AND STORAGE

Precautionary Measures:

Wash with soap and water before eating, drinking, smoking, applying cosmetics, or using toilet. Launder contaminated clothing before reuse. Properly dispose of contaminated leather articles such as shoes or belts that cannot be decontaminated. Avoid heat, open flames, including pilot lights, and strong oxidizing agents. Use explosion-proof ventilation to prevent vapor accumulation. Ground all handling equipment to prevent sparking. Do not siphon gasoline by mouth; harmful or fatal if swallowed. Avoid contact with eyes, skin and clothing. Wash thoroughly after handling.

For use as a motor fuel only. Do not use as a cleaning solvent or for other non-motor fuel uses.

Handling:

Surfaces that are sufficiently hot may ignite liquid material. Material is extremely flammable and heavier than air. Vapors may travel across the ground and reach remote ignition sources causing a flashback fire danger.

Keep containers closed when not in use. WARNING! The flow of gasoline through the pump nozzle can produce static electricity, which may cause a fire if gasoline is pumped into an ungrounded container. To avoid static buildup, place approved container on the ground. Do not fill container in vehicle or truck bed. Keep nozzle in contact with container while filling. Do not use automatic pump handle (latch-open) device. Keep all storage vessels closed. Material will ignite when exposed to air. Air trapped within the storage container may be removed by placing dry ice in the container prior to closing. Turn off all battery operated portable electronic devices (examples include: cellular phones, pagers and CD players) before operating gasoline pump. Use only with adequate ventilation.

Storage:

Store in a cool, dry place with adequate ventilation. Keep away from open flames and high temperatures.

Keep liquid and vapor away from heat, sparks and flame. Extinguish pilot lights, cigarettes and turn off other sources of ignition prior to use and until all vapors have dissipated. Use explosion-proof ventilation indoors and in laboratory settings.

Container Warnings:

Keep containers closed when not in use. Containers, even those that have been emptied, can contain explosive vapors. Do not cut, drill, grind, weld or perform similar operations on or near containers.

Benzene ACGIH TLV TWA: 0.5 ppmv STEL: 2.5 ppmv Notation: Skin

Benzene OSHA PEL TWA: 1 ppmv STEL: 5 ppmv Ethanol ACGIH TLV TWA: 1000 ppmv

Ethyl Alcohol OSHA PEL TWA: 1000 ppmv

Gasoline ACGIH TLV TWA: 300 ppmv STEL: 500 ppmv Gasoline OSHA PEL - 1989(revoked) TWA: 300 ppmv STEL: 500 ppmv

Toluene ACGIH TLV TWA: 50 ppmv Notation: Skin Toluene OSHA PEL TWA: 200 ppmv Ceiling: 300 ppmv

Toluene OSHA PEL - 1989(revoked) TWA: 100 ppmv STEL: 150 ppmv

Toluene SHELL INTERNAL TWA: 50 ppmv

xylene (o-, m-, p- isomers) OSHA PEL TWA: 100 ppmv

xylene (o-, m-, p- isomers) OSHA PEL - 1989(revoked) TWA: 100 ppmv STEL:

150 ppmv

Xylene (o-, m-, p-isomers) ACGIH TLV TWA: 100 ppmv STEL: 150 ppmv

Carbon dioxide ACGIH - TLV TWA: 5000 ppmm STEL: 30000 ppmm

Carbon dioxide OSHA - PEL STEL: 30000 ppmm

Carbon dioxide OSHA - PEL IS TWA: 10000 ppmm

Carbon monoxide OSHA - PEL TWA: 35 ppmv Ceiling: 200 ppmv

Combustion Carbon monoxide

EXPOSURE CONTROLS

Adequate ventilation to control airborne concentrations below the exposure guidelines/limits.

PERSONAL PROTECTION

Personal protective equipment (PPE) selections vary based on potential exposure conditions such as handling practices, concentration and ventilation. Information on the selection of eye, skin and respiratory protection for use with this material is provided below.

Eye Protection:

Chemical Goggles - If liquid contact is likely., or Safety glasses with side shields

Skin Protection:

Use protective clothing which is chemically resistant to this material. Selection of protective clothing depends on potential exposure conditions and may include gloves, boots, suits and other items. The selection(s) should take into account such factors as job task, type of exposure and durability requirements.

Published literature, test data and/or glove and clothing manufacturers indicate the best protection is provided by: Neoprene, or Nitrile Rubber

Respiratory Protection:

If engineering controls do not maintain airborne concentrations to a level which is adequate to protect worker health, an approved respirator must be worn. Respirator selection, use and maintenance should be in accordance with the requirements of the OSHA Respiratory Protection Standard, 29 CFR 1910.134.

Types of respirator(s) to be considered in the selection process include: For Vapors: Air Purifying, R or P style prefilter & organic cartridge, NIOSH approved respirator. Full face air supplied respirator if oxygen level is reduced below 19.5 %. Self-contained breathing apparatus for use in environments with unknown concentrations or emergency situations.

SECTION 9 PHYSICAL AND CHEMICAL PROPERTIES

Appearance & Odor: Clear liquid. Alcohol odor.

Substance Chemical Family: Alcohol

Appearance: Clear liquid.

Boiling Point: 173 °F Approximate

Flammability in Air: 1.3 %volume - 7.6 %volume

Flash Point: -40 °F [Tagliabue Closed Cup]

Specific Gravity: 0.79

Stability: Stable

Vapor Density: > 1

Viscosity: < 1.4 cSt @ 100 °F

SECTION 10 REACTIVITY AND STABILITY

Stability:

Material is stable under normal conditions.

Conditions to Avoid:

Avoid heat, sparks, open flames and other ignition sources.

Materials to Avoid:

Avoid contact with strong oxidizing agents.

Hazardous Decomposition Products:

Thermal decomposition products are highly dependent on combustion conditions. A complex mixture of airborne solids, liquids and gases will evolve when this material undergoes pyrolysis or combustion. Aldehydes, Carbon Monoxide, Carbon Dioxide, Unidentified organic compounds, Peroxide, Styrene oxide and other unidentified organic compounds may be formed upon combustion.

SECTION 11 TOXICOLOGICAL INFORMATION

Acute Toxicity

Dermal LD50 >2 g/kg(Rabbit) OSHA: Non-Toxic Based on components(s) Eye Irritation Variable [Rabbit] OSHA: Irritating Based on components(s) Inhalation LC50 >16,000 ppmv(Rat) OSHA: Non-Toxic Based on components(s) Oral LD50 >5 ml/kg(Rat) OSHA: Non-Toxic Based on components(s) Skin Irritation Draize 0.98 [Rabbit, 24 hour(s)] OSHA: Irritating Based on components(s)

Carcinogenicity:

Gasoline has been tested by API in a long-term inhalation test in mice and rats. There was an increased incidence of liver cancer in female mice. Male rats had a dose related increase in kidney tumors. This effect was due to formation of alpha-2u-globulin in the rats. This material is not formed in humans and is therefore not considered relevant.

Carcinogenicity Classification

Denatured Ethanol

NTP: No IARC: Yes ACGIH: No OSHA: No

Benzene

NTP: Yes IARC: Carcinogen (1) ACGIH: A1 OSHA: Yes

Ethvl Benzene

NTP: No IARC: Possible Carcinogen (2B) ACGIH: A3 OSHA: No

Toluene

NTP: No IARC: Not Classifiable (3) ACGIH: A4 OSHA: No

Unleaded Gasoline

NTP: No IARC: Possible Carcinogen (2B) ACGIH: A3 OSHA: No

Carcinogenicity

Chronic inhalation of wholly vaporized gasoline produced kidney tumors in male rats and liver tumors in female mice. The kidney tumors have been shown to develop through a unique mechanism involving Alpha-2u globulin. This protein is not present in humans making the kidney tumors irrelevant to potential human health risks. Origin of the female mouse liver tumors is less understood, leaving their significance for human risks uncertain. Prolonged and repeated exposure to high concentrations (10s to 100s ppm) of benzene may cause serious injury to blood-forming organs, is associated with anemia (depletion of blood cells) and is linked to the later development of acute myelogenous leukemia (AML) in humans. A recent chronic bioassay of ethylbenzene by the NTP produced clear evidence of carcinogenicity in male rats based on kidney tumor increase. Other animal tumors possibly associated with ethylbenzene include testicular adenomas in male rats, kidney tumors in female rats, lung tumors in male mice and liver tumors in female mice. Toluene is not known to be mutagenic or carcinogenic although available human and experimental animal data are limited and insufficient to assess carcinogenic potential.

Cardiovascular System

While there is no evidence that workplace exposure to acceptable levels of toluene vapors (e.g., the TLV) have produced cardiac effects in humans, high concentrations may cause cardiac sensitization and sudden lethality has been reported from habitual sniffing of solvents or glue. Animal studies have confirmed the sensitizing effects. Sensitization may lead to fatal changes in heart rhythms. Hypoxia or injection of adrenalin-like agents may enhance this effect. Thickening of heart blood vessels has been reported in animals exposed to xylene.

Developmental Toxicity

Daily exposure of pregnant rats to unleaded gasoline vapor at concentrations up to 9000 ppm resulted in no detectable maternal or developmental toxicity. Developmental toxicity studies of xylenes showed embryolethal/toxic and teratogenic effects with maternal toxicity. Many case studies involving abuse during pregnancy implicate toluene as a developmental toxicant. Studies in laboratory animals have shown developmental effects comparable to those reported in humans, but the effects were generally associated with maternal toxicity. Ethanol ingestion during pregnancy has been reported to cause birth defects in some infants.

Genotoxicity

Unleaded gasoline was tested for genetic activity in tests using microbial cells, cultured mammalian cells and rats (bone marrow) and was judged to be negative in every case. Toluene was negative in the Ames assay and negative for chromosomal aberrations and sister-chromatid exchanges in human lymphocytes and in an in vitro test using hamster cells. Mouse lymphoma test results for toluene were inconclusive.

Blood/Blood Forming Organs

Blood effects were seen in rats following prolonged and repeated oral exposure to a mixture of xylenes containing ethylbenzene.

Kidney

Long-term inhalation of wholly vaporized gasoline caused increased kidney weight and progressive nephropathy (tissue damage) in male rats. In rats exposed orally to a xylene mixture also containing ethylbenzene, males developed hyaline droplet changes and females showed evidence of early chronic nephropathy. Intentional abuse of toluene vapors by 'glue-sniffers' has been associated with damage to the kidneys.

Liver

Inhalation of gasoline vapor increased liver weights, urinary excretion of ascorbic acid, and hepatic enzyme activity in male rats. Liver weight increases were seen in rats dosed orally for 90 days with a xylene mixture also containing ethylbenzene. Reversible liver damage has been reported in persons exposed to toluene by solvent abuse. Prolonged and repeated consumption of ethanol has been shown to cause liver damage in animals and cirrhosis in humans.

Neurotoxicity

Rats receiving prolonged and repeated exposure to high doses of xylene have shown hearing loss. Prolonged and repeated exposures to high toluene concentrations (mixed solvent) have resulted in hearing loss in laboratory animals. There have also been reports of hearing damage in humans overexposed to toluene and other solvents, however, these effects and their possible relationship to noise exposure remain uncertain. Intentional inhalation ('glue-sniffing') and resulting overexposure to toluene vapors has been linked to brain injury.

Sensitization

Gasoline and component petroleum streams blended to produce it were tested in animal studies and found not to cause skin sensitization.

Systemic Toxicity

Laboratory animals exposed to prolonged and repeated doses of xylenes by various routes have shown effects in liver, kidneys, lungs, spleen, heart, blood and adrenals. Persons on disulfiram (Antabuse(R)) therapy should be aware that the ethyl alcohol in this product is hazardous to them just as is alcohol from any source. Disulfiram reactions (vomiting, headache and even collapse) may follow ingestion of small amounts of alcohol and have also been described from skin contact.

SECTION 12 ECOLOGICAL INFORMATION

Environmental Impact Summary:

There is no ecological data available for this product.

SECTION 13 DISPOSAL CONSIDERATIONS

RCRA Information:

Under RCRA, it is the responsibility of the user of the material to determine, at the time of the disposal, whether the material meets RCRA criteria for hazardous waste. This is because material uses, transformations, mixtures, processes, etc. may affect the classification. Refer to the latest EPA, state and local regulations regarding proper disposal.

SECTION 14 TRANSPORT INFORMATION

US Department of Transportation Classification

Proper Shipping Name: Alcohols, N.O.S. (Contains Ethanol and Gasoline)

Technical Names (s): Ethanol, Gasoline

Identification Number: UN1987

Hazard Class/Division: 3 (Flammable Liquid)

Packing Group: II

Marine Pollutant % of Total:

Marine Pollutant: Marine Polluntant based on the presence of >10% hydrocarbons listed in 49 CFR 172.101, appendix B; main constituents

Trimethylbenzene and Naphthalene. Emergency Response Guide # 127

International Air Transport Association

Hazard Class/Division: 3 (Flammable Liquid)

Identification Number: UN1987

Packing Group: II

Proper Shipping Name: Alcohols, N.O.S. (Contains Ethanol and Gasoline)

Technical Name(s): Ethanol, Gasoline

International Maritime Organization Classification

Hazard Class/Division: 3 (Flammable Liquid)

Identification Number: UN1987

Packing Group: II

Proper Shipping Name: Alcohols, N.O.S. Technical Name(s): Ethanol, Gasoline

SECTION 15 REGULATORY INFORMATION

FEDERAL REGULATORY STATUS

OSHA Classification:

Product is hazardous according to the OSHA Hazard Communication Standard, 29 CFR 1910.1200.

Comprehensive Environmental Release, Compensation & Liability Act (CERCLA): Benzene RQ 10 lbs Reportable Spill \Rightarrow 4097 lbs or 683 gal

Ozone Depleting Substances (40 CFR 82 Clean Air Act):
This material does not contain nor was it directly manufactured with any Class I or Class II ozone depleting substances.

Superfund Amendment & Reauthorization Act (SARA) Title III:

There are no components in this product on the SARA 302 list.

SARA Hazard Categories (311/312):

Immediate Health:YES Delayed Health:YES Fire:YES Pressure:NO
Reactivity:NO

SARA Toxic Release Inventory (TRI) (313):

Xylene (mixed isomers), Toluene, Ethylbenzene, Benzene

Toxic Substances Control Act (TSCA) Status: All component(s) of this material is(are) listed on the EPA/TSCA Inventory of Chemical Substances.

Other Chemical Inventories:

Australian AICS, Chinese Inventory, European EINECS, Japan ENCS, Korean Inventory, Philippines PICCS,

State Regulation

The following chemicals are specifically listed by individual states; other product specific health and safety data in other sections of the MSDS may also be applicable for state requirements. For details on your regulatory requirements you should contact the appropriate agency in your state.

California Safe Drinking Water and Toxic Enforcement Act (Proposition 65).

WARNING: This product contains a chemical(s) known to the State of California to cause cancer.

WARNING: This product contains a chemical(s) known to the State of California to cause birth defects or other reproductive harm.

New Jersey Right-To-Know Chemical List:

Benzene (71-43-2) 0 - 0.24 %weight Carcinogen Benzene (71-43-2) 0 - 0.24 %weight Mutagen Benzene, Methyl- (108-88-3) 0 - 1.49 %weight Ethanol (64-17-5) 95 - 99.99 %weight Xylenes (1330-20-7) 0 - 1.49 %weight

Pennsylvania Right-To-Know Chemical List:

Benzene (71-43-2) 0 - 0.24 %weight Spec Haz Sub/Env Hazardous Benzene, dimethyl- (1330-20-7) 0 - 1.49 %weight Environmental Hazard Benzene, Methyl- (108-88-3) 0 - 1.49 %weight Environmental Hazard Ethanol (64-17-5) 95 - 99.99 %weight

SECTION 16 OTHER INFORMATION

Revision#: 2

Revision Date: 04/14/2003

Revisions since last change (discussion): This Material Safety Data Sheet (MSDS) has been newly reviewed to fully comply with the guidance contained in the ANSI MSDS standard (ANSI Z400.1-1998). We encourage you to take the opportunity to read the MSDS and review the information contained therein.

SECTION 17 LABEL INFORMATION

READ AND UNDERSTAND MATERIAL SAFETY DATA SHEET BEFORE HANDLING OR DISPOSING OF PRODUCT. THIS LABEL COMPLIES WITH THE REQUIREMENTS OF THE OSHA HAZARD COMMUNICATION STANDARD (29 CFR 1910.1200) FOR USE IN THE WORKPLACE. THIS LABEL IS NOT INTENDED TO BE USED WITH PACKAGING INTENDED FOR SALE TO CONSUMERS AND MAY NOT CONFORM WITH THE REQUIREMENTS OF THE CONSUMER PRODUCT SAFETY ACT OR OTHER RELATED REGULATORY REQUIREMENTS.

PRODUCT CODE(S):

05482

Denatured Ethanol

DANGER!

EXTREMELY FLAMMABLE. VAPORS MAY EXPLODE. CAUSES SEVERE EYE IRRITATION. OVEREXPOSURE TO VAPORS CAN CAUSE CNS DEPRESSION. MAY CAUSE SKIN IRRITATION. ASPIRATION HAZARD IF SWALLOWED - CAN ENTER LUNGS AND CAUSE DAMAGE. CONTAINS BENZENE WHICH IS A CANCER HAZARD - LINKED TO DEVELOPMENT OF ACUTE MYELOGENOUS LEUKEMIA. PROLONGED OR REPEATED SKIN CONTACT MAY CAUSE OIL ACNE OR DERMATITIS. LONG-TERM EXPOSURE TO GASOLINE VAPORS HAS CAUSED CANCER IN LABORATORY ANIMALS.

MAY CAUSE DAMAGE TO: Cardiovascular System, Blood/Blood Forming Organs, Kidney, Liver

Refer to Section 11, Toxicological Information, for specific information on the following effects:
Developmental Toxicity, Genotoxicity

Precautionary Measures:

Avoid contact with skin and clothing. Avoid heat, sparks, open flames and other ignition sources. Avoid breathing of vapors, fumes, or mist. Do not take internally. Use only with adequate ventilation. Keep container closed when not in use. Wash thoroughly after handling.

FIRST AID

Inhalation: Move victim to fresh air and provide oxygen if breathing is difficult. Get medical attention. DO NOT attempt to rescue victim unless proper respiratory protection is worn. If the victim has difficulty breathing or tightness of the chest, is dizzy, vomiting or unresponsive, give 100% oxygen with rescue breathing or CPR as required and transport to the nearest medical facility.

Skin Contact: Remove contaminated clothing. Flush exposed area with water and follow by washing with soap if available. If redness, swelling, pain and/or blisters occur, transport to the nearest medical facility for additional treatment.

Eye Contact: Immediately flush eyes with large amounts of water for at least 30 minutes, by the clock, while holding eyelids open. Transport to nearest medical facility for additional treatment.

Ingestion: DO NOT take internally. Do NOT induce vomiting. If vomiting occurs spontaneously, keep head below hips to prevent aspiration of liquid into lungs. Get medical attention. Have victim rinse mouth out with water, then drink sips of water to remove taste from mouth. In general no treatment is necessary unless large quantities are swallowed, however, get medical advice.

FIRE

In case of fire, Use water fog, foam, dry chemical or carbon dioxide (CO2) to extinguish flames. Do not use a direct stream of water. Material will float and can be re-ignited on surface of water.

SPILL OR LEAK

Dike and contain spill.

FOR LARGE SPILLS: Remove with vacuum truck or pump to storage/salvage vessels.

FOR SMALL SPILLS: Soak up residue with an absorbent such as clay, sand or other suitable material. Place in non-leaking container and seal tightly for proper disposal.

CONTAINS: Ethanol, 64-17-5; Unleaded Gasoline, Mixture; Toluene, 108-88-3; Xylene, mixed isomers, 1330-20-7; Benzene, 71-43-2; Ethyl Benzene, 100-41-4; Miscellaneous Hydrocarbons,

NFPA Rating (Health, Fire, Reactivity): 1, 3, 0

TRANSPORTATION

US Department of Transportation Classification

Proper Shipping Name: Alcohols, N.O.S. (Contains Ethanol and Gasoline)

Technical Names (s): Ethanol, Gasoline

Identification Number: UN1987

Hazard Class/Division: 3 (Flammable Liquid)

Packing Group: II

Marine Pollutant % of Total:

Marine Pollutant: Marine Polluntant based on the presence of >10% hydrocarbons listed in 49 CFR 172.101, appendix B; main constituents

Trimethylbenzene and Naphthalene. Emergency Response Guide # 127

California Safe Drinking Water and Toxic Enforcement Act (Proposition 65).

WARNING: This product contains a chemical(s) known to the State of California to cause cancer.

WARNING: This product contains a chemical(s) known to the State of California to cause birth defects or other reproductive harm.

CAUTION: Misuse of empty containers can be hazardous. Empty containers can be hazardous if used to store toxic, flammable, or reactive materials. Cutting or welding of empty containers might cause fire, explosion or toxic fumes from residues. Do not pressurize or expose to open flames or heat. Keep container closed and drum bungs in place.

Name and Address

Motiva Enterprises LLC P.O. Box 4540 Houston, TX 77210-4540

ADMINISTRATIVE INFORMATION

MANUFACTURER ADDRESS: Motiva Enterprises LLC, P.O. Box 4540, Houston, TX. 77210-4540

Company Product Stewardship & Regulatory Compliance Contact: David Snyder Phone Number: (281) 874-7728

THE INFORMATION CONTAINED IN THIS DATA SHEET IS BASED ON THE DATA AVAILABLE TO US AT THIS TIME, AND IS BELIEVED TO BE ACCURATE BASED UPON THAT: IT IS PROVIDED INDEPENDENTLY OF ANY SALE OF THE PRODUCT, FOR PURPOSE OF HAZARD COMMUNICATION. IT IS NOT INTENDED TO CONSTITUTE PRODUCT PERFORMANCE INFORMATION, AND NO EXPRESS OR IMPLIED WARRANTY OF ANY KIND IS MADE WITH RESPECT TO THE PRODUCT, UNDERLYING DATA OR THE INFORMATION CONTAINED HEREIN. YOU ARE URGED TO OBTAIN DATA SHEETS FOR ALL PRODUCTS YOU BUY, PROCESS, USE OR DISTRIBUTE, AND ARE ENCOURAGED TO ADVISE THOSE WHO MAY COME IN CONTACT WITH SUCH PRODUCTS OF THE INFORMATION CONTAINED HEREIN.

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36914-12060-100R-04/17/2003

Annex 11 – Road Transport Emergency Response Plan

This Plan is for the Facility only; no part of it is sent to an agency.

Page 1

ROAD TRANSPORT EMERGENCY RESPONSE

for

Motiva Enterprises LLC

Purpose

The purpose this document is to provide a template of an emergency response plan covering the transportation of products (includes the loading, transport and unloading) that meets the requirements of the Road Transport Standard.

I. INTRODUCTION

This plan outlines the steps to be taken in handling various accidents involving road transport. The intent of the plan is to provide guidance on responding to the incident and thereby prevent injuries to people or damage to property and the environment.

This plan also sets forth the manner of response to discharges of petroleum products that may occur during transportation and meets the basic response plan requirements of 49 CFR 130.31(a) for a single package containing 3,500 gallons or more.

The largest single package transported in under this plan is 12,500 gallons.

Every employee likely to be involved in the implementation and control must be fully conversant with the procedures detailed in this plan.

II ACCOUNTABILITY

- 1. Management Ensure that the steps outlined in this plan are communicated and followed.
- 2. Affected Vehicle Operators (Driver) Follow and have a good understanding of the steps outlined in this plan.
- Emergency Response Contractor(s) With the assistance of the HSSE department, will clean up the hazardous materials spill and assist in the proper disposal of all contaminated materials associated with the spill. In addition, when directed, assist in contacting applicable agencies and filling out applicable reports.

- 4. Supervisor(s) Oversee and assume responsibility for the cleanup operation to ensure that the cleanup materials are properly managed and disposed of.
 - a. Contact your HSSE representative for assistance with the plan.
 - b. Notify all applicable government agencies.
- 5. HSSE Representative Assist in implementing this plan.

III GENERAL PROCEDURES (Accidents)

Note: Safety to people must come first. Employees must never take any actions that would put themselves or others in harm's way.

- Driver First Response in the Event of a Vehicle Accident or Rollover
 If driver is unhurt, he should assume initial control at the scene, and:
 - a. Switch off engine and disconnect power via the vehicle master power isolating switch (if equipped).
 - b. Ask involved parties if they need medical attention.
 - c. Call emergency services 911 (police, fire, ambulance as needed).
 - d. Verify that all valves are closed to limit the possibility of a spill.
 - e. Keep public at a safe distance.
 - f. Prevent smoking and remove sources of ignition.
 - g. Place safety triangles, cones, and fire extinguishers.
 - h. Contact supervisor or manager as soon as it is safe to do so.
 - i. Assess damage to the tanker or vehicle.
 - j. If rollover, contact a cargo tank truck specialist and tow service. If product is on board the tank truck, a pump truck will be required.

2. Road Incidents (Loss of Product or Cargo)

In addition to the items in section 11.1.4.1, drivers and/or supervisors should:

- a. Keep the public away from the area and upwind of the spill.
- b. Attempt to stop any further leakage/spillage by closing product valves or by other means if it can be done safely. "Safely" is being able to stop further leakage or spillage while not coming into contact with the spilled material. Exposure to spilled material must be minimized.
- c. Prevent leak or spillage from entering any sewer or drain by using spill pads, booms, dirt or sand bags, or by covering grating with a plastic tarp. Only deploy this material downstream of the leading edge of the spilled material and keep exposure to spilled material at a minimum.
- d. Immediately notify the Order Management Center at 1-800-990-5070. They will in turn contact the Delivery Support Manager and/or the Director of Order Management & Trucking.
- e. Under no circumstance should the driver, if unharmed, able and fit, abandon the vehicle until a responsible senior staff member of the company arrives at the scene and relieves him. The driver should keep a safe distance from any hazards.
- 3. Road Incidents (Fire Involving the Equipment on the Vehicle)

In addition to the items in section 11.1.4.1, drivers and/or supervisors should:

- a. Use fire extinguishers if small, incipient stage fire involving the vehicle or vehicle equipment occurs. Fire extinguishers should only be used by trained employees and only if it can be done without risk of injury.
- 4. Road Incidents (Fire Involving the Cargo)

In addition to the items in section 11.1.4.1, drivers and/or supervisors should:

a. Notify the fire department of the situation and the products involved. The fire department may need to find a source of fire fighting foam when petroleum products are involved.

- b. Fires involving the cargo are rarely manageable with a fire extinguisher and should not be combated by the employee.
- c. Increase the safe distance around the vehicle and avoid the smoke from the fire.

5. Road Incident (Vehicle Breakdown)

- a. Move the vehicle as far from the traveled portion of the highway as possible.
- b. Fully apply the parking brake.
- c. Place wheel blocks/chocks.
- d. Place emergency reflective triangles to warn traffic.
- e. Call your supervisor or other repair companies as directed by local procedures.
- f. The driver must remain with the vehicle at all times until help arrives.
- g. The driver should advise the public to keep clear of the vehicle and should not permit smoking or allow ignition sources near the vehicle.
- h. Depending on the circumstances, have the fire extinguishers in an easily accessible and safe place up wind of the vehicle and ready for use in an emergency.

6. Road Incidents (Hijack)

- a. Do not attempt to resist the hijacker.
- b. Gather as much information as possible about the hijackers, vehicles they may have used, direction of travel, the license plate and description of our vehicle, and the products that are in our vehicle.
- c. Call 911 to report the incident.
- d. Call your supervisor to report the incident.

7. Medical Incident Recovery Measures

Note: Employees are not trained to provide medical aid to others. First aid kits supplied on vehicles are for the use of the driver to treat his or her own injuries until medical help arrives. Employees are not expected or required to treat others and in doing so will be acting of their own accord.

- a. In the event of medical emergencies contact 911 and advise the operator of the situation.
- b. Notify your supervisor of the situation as soon as possible.

8. Annual Drills

a. Annual drills covering road transport shall be conducted by each facility. Each year, the drill should address a different type of hazard i.e. tornado, fire, bomb threat, hijacking, etc.

IV GENERAL PROCEDURES (SPILLS)

Minor Spill

In addition to the items in section III.1, drivers and/or supervisors should:

- a. Immediately stop and contain the spill at its source.
- b. Clean up the spill using supplied materials.
- c. Place all used spill response equipment/absorbents into a trash bag(s) and properly transport, dispose of, or recycle these materials according to guidance from the HSSE department. Do not transport materials from the spill site without guidance from the Environmental Group.
- d. Contact his or her supervisor/manager immediately after containing and/or cleaning up the spill and provide a description of the spill and how it was cleaned up. The spill must be reported and investigated in accordance with SOP US and Motiva Incident Notification and Investigation HSSE Standards.

2. Major Spill

In addition to the items in Section 11.1.4.1, drivers and/or supervisors should:

- a. If the likelihood of a fire or explosion exists, drivers should evacuate the immediate area and call the local fire department using 911 or an alternative emergency number.
- b. If it can be done safely, the driver should immediately stop and contain the spill at its source and keep unauthorized persons outside of the spill area. "Safely" is being able to stop further leakage or spillage while not coming into contact with the spilled material. Exposure to spilled material must be minimized.
- c. The Terminal Superintendent/Delivery Supervisor must report a Major Spill to the Shell Oil Products U.S. HSEQ Emergency Management 24 hour hot line (1-877-242-7400). This includes any amount of spill that reaches a body of water or sewer system. They will in turn contact the Delivery Support Manager. Be prepared to describe the:
 - i. Exact location of spill,
 - ii. Injuries to self and others,
 - iii. Volume of product released,
 - iv. Affected storm drains and/or water bodies,
 - v. Damage to equipment and property, and
 - vi. Name of driver and the phone number they can be reached at
- d. If additional outside assistance is needed to clean up the spill, contact the approved OSROs as listed in the Plan.
- e. The driver and/or the Emergency Response Contractor shall collect all materials used in cleaning up the spill and properly dispose or recycle these materials according to guidance from the HSSE Department.
- f. The Delivery Supervisor or Terminal Superintendent will make appropriate notifications to the National Response Center (1-800-424-8802) as required.

g. The Supervisor or Superintendent must follow up according to the requirements of the SOP US and Motiva Incident Notification and Investigation HSSE Standards.

V. TRAINING

- 1. Employees covered by this Plan shall review its contents annually.
- 2. Documentation of the initial training and refresher training will be maintained for a period of 5 years.
- 3. Those **responding** to either a hazardous material or hazardous substance spill must first have the applicable HAZWOPER training.

VI. DOCUMENT CONTROL

Training records must contain at a minimum the:

- a. Name of the instructor,
- b. Name of the student,
- c. Student's signature or equivalent,
- d. Date of the training,
- e. Materials used in the training, and
- f. Facility location where the training session was performed.

Training records will be maintained at the local office and entered into Mockingbird.

Training records will be maintained for a period of 5 years.

VII RESPONDING TO CARRIER ACCIDENTS

In the event of a significant incident involving a carrier under Motiva's operational control, it is required that a SOP US or Motiva Enterprises employee, ideally a Supervisor or Superintendent, be on site. The Company representative must initiate a timely investigation and gather information as directed by the Director of Trucking or the Manager of Delivery Support.

Significant incidents include but are not limited to:

- a. An incident of impact resulting in significant media coverage and public concern
- b. Product spill/leak/release that results in soil, surface water or potential/actual groundwater contamination.
- c. Any work-related contractor fatality occurring on or off company property.
- d. Road closures due to an incident.

The company representative will need to provide an outline of the nature and severity of the event, including the number of injuries, extent of injuries, whether hospitalization was required, involving third parties and/or the driver.

VIII VEHICLE SPILL RESPONSE EQUIPMENT LIST

Vehicle emergency equipment - each transportation vehicle with a capacity of 3,500 gallons or more will carry at a minimum:

10 Absorbent Pads

2 10' Absorbent Socks

Gloves

Disposable Bag

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IX DEFINITIONS

DOT - United States Department of Transportation

HAZWOPER - Hazardous Waste Operations and Emergency Response (OSHA Standard)

HSSE - Health, Safety, Security, and Environment Department

Land Conditions - Hills, slopes, ditches, mountains, valleys, etc.

Major Spill - A spill that may require outside assistance to remove, and/or that impacts a storm drain or body of water. All major spills must be reported to the Shell Oil Products U.S. HSEQ Emergency Management 24 hour hot line (1-877-242-7400) and follow up according to the requirements of the SOP US and Motiva Incident Notification and Investigation HSSE Standards.

<u>Note:</u> A major spill may also be a Reportable Spill (see definition). In this case, the National Response Center (1-800-424-8802) and possibly a state and/or local regulatory agency must be notified. Refer to the Core Plan at the beginning of this manual for all Agency/Emergency contact numbers.

Minor Spill – A spill that is small enough to be easily cleaned up by the driver and which does not impact a storm drain or body of water. Some states require certain minor spills to be reported. Contact your HSSE Environmental Coordinator for guidance. The spill details need to be reported via the online IRM system.

Under Operational Control – Delivering products on behalf of Shell or Motiva.

X OIL SPILL DATA LOG

Following this procedure will help facilitate emergency response operations for oil spills and other environmental concerns.

Refer to the Core Plan at the beginning of this manual for all Agency/Emergency contact numbers.

Please be prepared to provide the following information to the appropriate person or agencies: The incident's location, specific address, the closest highway mile marker to the incident, the nearest town or city, and the name and contact number of the person making the call.

City:	····	State:						
Person reporting s	pill:	Phone Nun	nber:					
Responsible party:		Phone Nun	nber:					
On scene contact:		Phone num	Phone number:					
conditions, damag	e to property and		oill, weather and land					
Surface affected:	Soil/grass □	Asphalt □	Concrete □					
Water affected	Surface □	Groundwater □	Coastal □					
Sensitive receptors	s (e.g. storm sewe	r, drainage ditch):						
Note any initial act	ions that may have	e been taken to contro	I the incident.					
	110-110-1							

Contacts Mac Response):	de and Reporting Results (Example: 911 or Shell Emergency
Contact 1: Na	ame
	Person's Name:
	Phone Number:
	Information Reported:
	Information Received (Ex: Incident Number):
	· · · · · · · · · · · · · · · · · · ·
Contact 2: Na	ame
	Person's Name:
	Phone Number:
	Information Reported:
	Information Received (Ex: Incident Number):
	Market 199

Contact 3: Na	ame
	Person's Name:
	Phone Number:
	Information Reported:
	Information Received (Ex: Incident Number):
	·
Contact 4: Na	ame
	Person's Name:
	Phone Number:
	Information Reported:
	Information Received (Ex: Incident Number):

ANNEX 12..GLOSSARY OF TERMS/ACRONYMS

This glossary contains definitions of terms that will be used frequently during the course of response operations.

Activate: The process of mobilizing personnel and/or equipment within the response organization to engage in response operations.

Activator: An individual in the response organization whose responsibilities include notifying other individuals or groups within the organization to mobilize personnel and/or equipment.

Adverse Weather: The weather conditions that will be considered when identifying response systems and equipment in a response plan for the applicable operating environment. Factors to consider include significant wave height, ice, temperature, weather related visibility, and currents within the Captain of the Port (COTP) zone in which the systems or equipment are intended to function.

Agency Representative: Individual assigned to an incident from an agency who has been delegated full authority to make decisions on all matters affecting that agency's participation in response operations.

Area Committee: As defined by Sections 311(a)(18) and (j)(4) of CWA, as amended by OPA, means the entity appointed by the President consisting of members from Federal, State, and local agencies with responsibilities that include preparing an Area Contingency Plan for the area designated by the President. The Area Committee may include exofficio (i.e., non-voting) members (e.g., industry and local interest groups).

Area Contingency Plan: As defined by Sections 311(a)(19) and (j)(4) of CWA, as amended by OPA, means the plan prepared by an Area Committee, that in conjunction with the NCP, shall address the removal of a discharge including a worst-case discharge and the mitigation or prevention of a substantial threat of such a discharge from a vessel, offshore facility, or onshore facility operating in or near an area designated by the President.

Average Most Probable Discharge: A discharge of the lesser of 50 barrels or 1% of the volume of the worst case discharge.

AWAY Team: A predesignated team from various departments in Houston, is responsible for arriving at the scene of an oil spill incident as soon as possible to provide both immediate and longer-term management of the field activities.

Barrel (bbl): Measure of space occupied by 42 U.S. gallons at 60 degrees Fahrenheit.

Bioremediation Agents: Means microbiological cultures, enzyme additives, or nutrient additives that are deliberately introduced into an oil discharge and that will significantly increase the rate of biodegradation to mitigate the effects of the discharge.

Boom: A piece of equipment or a strategy used to either contain free floating oil to a confined area or protect an uncontaminated area from intrusion by oil.

Booming Strategies: Strategic techniques which identify the location and quantity of boom required to protect certain areas. These techniques are generated by identifying a potential spill source and assuming certain conditions which would affect spill movement on water.

Bulk: Material that is stored or transported in a loose, unpackaged liquid, powder, or granular form capable of being conveyed by a pipe, bucket, chute, or belt system.

Chemical Agents: Means those elements, compounds, or mixtures that coagulate, disperse, dissolve, emulsify, foam, neutralize, precipitate, reduce, solubilize, oxidize, concentrate, congeal, entrap, fix, make the pollutant mass more rigid or viscous, or otherwise facilitate the mitigation of deleterious effects or the removal of the oil pollutant from the water. Chemical agents include biological additives, dispersants, sinking agents, miscellaneous oil spill control agents, and burning agents, but do not include solvents.

Clean-up Contractor: Persons contracted to undertake a response action to clean up a spill.

Cleanup: For the purposes of this document, cleanup refers to the removal and/or treatment of oil, hazardous substances, and/or the waste or contaminated materials generated by the incident. Cleanup includes restoration of the site and its natural resources.

Coastal Waters: For the purpose of classifying the size of discharges, means the waters of the coastal zone except for the Great Lakes and specified ports and harbors on inland rivers.

Coastal Zone: As defined for the purpose of the NCP, means all United States waters subject to the tide, United States waters of the Great Lakes, specified ports and harbors on inland rivers, waters of the contiguous zone, other waters of the high seas subject to the NCP, and the land surface or land substrata, ground waters, and ambient air proximal to those waters. The term coastal zone delineates an area of federal responsibility for response action. Precise boundaries are determined by EPA/USCG agreements and identified in federal regional contingency plans.

Coast Guard District Response Ground (DRG): As provided for by CWA sections 311(a)(20) and (j)(3), means the entity established by the Secretary of the department in which the USCG is operating within each USCG district and shall consist of: the combined USCG personnel and equipment, including firefighting equipment, of each port within the district; additional prepositioned response equipment; and a district response advisory team.

Command: The act of controlling manpower and equipment resources by virtue of explicit or delegated authority.

Command Post: A site located at a safe distance form the spill site where response decisions are made, equipment and manpower deployed, and communications handled. The Incident Commander and the On-Scene Coordinators may direct the onscene response from this location.

Communications Equipment: Equipment that will be utilized during response operations to maintain communication between the Company employees, contractors, Federal/State/Local agencies. (Radio/telephone equipment and links)

Containment Boom: A flotation/freeboard device, made with a skirt/curtain, longitudinal strength member, and ballast unit/weight designed to entrap and contain the product for recovery.

Contingency Plan: A document used by (1) federal, state, and local agencies to guide their planning and response procedures regarding spills of oil, hazardous substances, or other emergencies; (2) a document used by industry as a response plan to spills of oil, hazardous substances, or other emergencies occurring upon their vessels or at their facilities.

Contract or Other Approved Means: For OPA 90, a written contract with a response contractor; certification by the facility owner or operator that personnel and equipment are owned, operated, or under the direct control of the facility, and available

within the stipulated times; active membership in a local or regional oil spill removal organization; and/or the facility's own equipment.

Critical Areas to Monitor: Areas which if impacted by spilled oil may result in threats to public safety or health.

Cultural Resources: Current, historic, prehistoric and archaeological resources which include deposits, structures, ruins, sites, buildings, graves, artifacts, fossils, or other objects of antiquity which provide information pertaining to the historical or prehistorical culture of people in the state as well as to the natural history of the state.

Damage Assessment: The process of determining and measuring damages and injury to the human environment and natural resources, including cultural resources. Damages include differences between the conditions and use of natural resources and the human environment that would have occurred without the incident, and the conditions and use that ensued following the incident. Damage assessment includes planning for restoration and determining the costs of restoration.

Decontamination: The removal of hazardous substances from personnel and their equipment necessary to prevent adverse health effects.

Discharge: Any spilling, leaking, pumping, pouring, emitting, emptying, or dumping.

Dispersants: Means those chemical agents that emulsify, disperse, or solubilize oil into the water column or promote the surface spreading of oil slicks to facilitate dispersal of the oil into the water column.

Diversion Boom: A floatation/freeboard device, made with a skirt/curtain, longitudinal strength member, and ballast unit/weight designed to deflect or divert the product towards a pick up point, or away from certain areas.

Drinking Water Supply: As defined by Section 101(7) of CERCLA, means any raw or finished water source that is or may be used by a public water system (as defined in the Safe Drinking Water Act) or as drinking water by one or more individuals.

EM: Emergency Management. Serves as the focal point for senior management support of an incident.

Economically Sensitive Areas: Those areas of explicit economic importance to the public that due to their proximity to potential spill sources may require special protection and include, but are not limited to: potable and industrial water intakes; locks and dams; and public and private marinas.

Emergency Management: The personnel identified to staff the organizational structure identified in a response plan to manage response plan implementation.

Emergency Service: Those activities provided by state and local government to prepare for and carry out any activity to prevent, minimize, respond to, or recover from an emergency.

Environmentally Sensitive Areas: Streams and water bodies, aquifer recharge zones, springs, wetlands, agricultural areas, bird rookeries, endangered or threatened species (flora and fauna) habitat, wildlife preserves or conservation areas, parks, beaches, dunes, or any other area protected or managed for its natural resource value.

Facility: Either an onshore facility or an offshore facility and includes, but is not limited to structures, equipment, and appurtenances thereto, used or capable of being used to transfer oil to or from a vessel or a public vessel. A facility includes federal, state, municipal, and private facilities.

Facility Operator: The person who owns, operates, or is responsible for the operation of the facility.

Federal Fund: The spill liability trust fund established under OPA.

Federal Regional Response Team: The federal response organization (consisting of representatives from selected federal and state agencies) which acts as a regional body responsible for planning and preparedness before an oil spill occurs and providing advice to the FOSC in the event of a major or substantial spill.

Federal Response Plan (FRP): Means the agreement signed by 25 federal departments and agencies in April 1987 and developed under the authorities of the Earthquake Hazards Reduction Act of 1977 and the Disaster Relief Act of 1974, as amended by the Stafford Disaster Relief Act of 1988.

First Responders, First Response Agency: A public health or safety agency (e.g., fire service or police department) charged with responding to a spill during the emergency phase and alleviating immediate danger to human life, health, safety, or property.

Handle: To transfer, transport, pump, treat, process, store, dispose of, drill for, or produce.

Harmful Quantity Of Oil: The presence of oil from an unauthorized discharge in a quantity sufficient either to create a visible film or sheen upon or discoloration of the surface of the water or a shoreline, tidal flat, beach, or marsh, or to cause a sludge or emulsion to be deposited beneath the surface of the water or on a shoreline, tidal flat, beach, or marsh.

Hazardous Material: Any nonradioactive solid, liquid, or gaseous substance which, when uncontrolled, may be harmful to humans, animals, or the environment. Including but not limited to substances otherwise defined as hazardous wastes, dangerous wastes, extremely hazardous wastes, oil, or pollutants.

Hazardous Substance: Any substance designed as such by the Administrator of the EPA pursuant to the <u>Comprehensive Environmental Response</u>, <u>Compensation</u>, and <u>Liability Act</u>; regulated pursuant to Section 311 of the <u>Federal Water Pollution Control Act</u>, or discharged by the SERC.

Hazardous Waste: Any solid waste identified or listed as a hazardous waste by the Administrator of the EPA pursuant to the federal Solid Waste Disposal Act, as amended by the Resource Conservation and Recovery Act (RCRA), 42 U.S.C., Section 6901, et seq as amended. The EPA Administrator has identified the characteristics of hazardous wastes and listed certain wastes as hazardous in Title 40 of the Code of Federal Regulations, Part 261, Subparts C and D respectively.

HAZMAT: Hazardous materials or hazardous substances, exposure to which may result in adverse effects on health or safety of employees.

HAZWOPER: Hazardous Waste Operations and Emergency Response Regulations published by OSHA to cover worker safety and health aspects of response operations.

Heat Stress: Dangerous physical condition caused by over exposure to extremely high temperatures.

Hypothermia: Dangerous physical condition caused by over exposure to freezing temperatures.

Incident: Any event that results in a spill or release of oil or hazardous materials. Action by emergency service personnel may be required to prevent or minimize loss of life or damage to property and/or natural resources.

Incident Briefing Meeting: Held to develop a comprehensive, accurate, and up-to-date understanding of the incident, nature of status of control operations, and nature and status of response operations; ensure the adequacy of control and response operations; begin to organize control and response operations; and prepare for interactions with outside world.

Incident Command Post (ICP): That location at which all primary command functions are executed.

Incident Command System (ICS): The combination of facilities, equipment, personnel, procedures, and communications operating within a common organizational structure, with responsibility for the management of assigned resources at an incident.

Incident Commander (IC): The <u>one</u> individual in charge at any given time of an incident. The Incident Commander will be responsible for establishing a unified command with all on-scene coordinators.

Indian Tribe: As defined in OPA section 1001, means any Indian tribe, band, nation, or other organized group or community, but not including any Alaska Native regional or village corporation, which is recognized as eligible for the special programs and services provided by the United States to Indians because of their status as Indians and has governmental authority over lands belonging to or controlled by the Tribe.

Initial Cleanup: Remedial action at a site to eliminate acute hazards associated with a spill. An initial clean-up action is implemented at a site when a spill of material is an actual or potentially imminent threat to public health or the environment, or difficulty of cleanup increases significantly without timely remedial action. All sites must be evaluated to determine whether initial cleanup is total cleanup, however, this will not be possible in all cases due to site conditions (i.e., a site where overland transport or flooding may occur).

Initial Notification: The process of notifying necessary the Company personnel and Federal/ State/Local agencies that a spill has occurred, including all pertinent available information surrounding the incident.

Initial Response Actions: The immediate actions that are to be taken by the spill observer after detection of a spill.

Inland Area means the area shoreward of the boundary lines defined in 46 CFR part 7, except that in the Gulf of Mexico, it means the area shoreward of the lines of demarcation (COLREG lines) as defined in §80.740 through 80.850 of this chapter. The inland area does not include the Great Lakes.

Inland Waters: State waters not considered coastal waters; lakes, rivers, ponds, streams, underground water, et. al.

Inland Zone: Means the environment inland of the coastal zone excluding the Great Lakes, and specified ports and harbors on inland rivers. The term inland zone delineates an area of federal responsibility for response action. Precise boundaries are determined by EPA/USCG agreements and identified in federal regional contingency plans.

Interim Storage Site: A site used to temporarily store recovered oil or oily waste until the recovered oil or oily waste is disposed of at a permanent disposal site. Interim storage sites include trucks, barges, and other vehicles, used to store waste until the transport begins.

Lead Agency: The government agency that assumes the lead for directing response activities.

Lead Federal Agency: The agency which coordinates the federal response to incident on navigable waters. The lead federal agencies are:

- U.S. Coast Guard: Oil and chemically hazardous materials incidents on navigable waters.
- Environmental Protection Agency: Oil and chemically hazardous materials incidents on inland waters.

Lead State Agency: The agency which coordinates state support to federal and/or local governments or assumes the lead in the absence of federal response.

Loading: Transfer from Facility to vehicle.

Local Emergency Planning Committee (LEPC): A group of local representatives appointed by the State Emergency Response Commission (SERC) to prepare a comprehensive emergency plan for the local emergency planning district, as required by the Emergency Planning and Community Right-to-know Act (EPCRA).

Local Response Team: Designated Facility individuals who will fulfill the roles determined in the oil spill response plan in the event of an oil or hazardous substance spill. They will supervise and control all response and clean-up operations.

Lower Explosive Limit: Air measurement utilized to determine the lowest concentration of vapors that support combustion. This measurement must be made prior to entry into a spill area.

Marinas: Small harbors with docks, services, etc. for pleasure craft.

Medium Discharge: Means a discharge greater than 2,100 gallons (50 Bbls) and less than or equal to 36,000 gallons (85+ Bbls) or 10% of the capacity of the largest tank, whichever is less and not to exceed the WCD.

National Contingency Plan: The plan prepared under the Federal Water Pollution Control Act (33 United State Code §1321 et seq) and the Comprehensive Environmental Response, Compensation, and Liability Act of 1980 (42 United State Code § 9601 et seq), as revised from time to time.

National Pollution Funds Center (NPFC): Means the entity established by the Secretary of Transportation whose function is the administration of the Oil Spill Liability Trust Fund (OSLTF). Among the NPFC's duties are: providing appropriate access to the OSLTF for federal agencies and states for removal actions and for federal trustees to initiate the assessment of natural resource damages; providing appropriate access to the OSLTF for claims; and coordinating cost recovery efforts.

National Response System (NRS): Is the mechanism for coordinating response actions by all levels of government in support of the OSC. The NRS is composed of the NRT, RRTs, OSC, Area Committees, and Special Teams and related support entities.

National Strike Force (NSF): Is a special team established by the USCG, including the three USCG Strike Teams, the Public Information Assist Team (PIAT), and the National Strike Force Coordination Center. The NSF is available to assist OSCs in their preparedness and response duties.

National Strike Force Coordination Center (NSFCC): Authorized as the National Response Unit by CWA section 311(a)(23) and (j)(2), means the entity established by the Secretary of the department in which the USCG is operating at Elizabeth City, North Carolina, with responsibilities that include

administration of the USCG Strike Teams, maintenance of response equipment inventories and logistic networks, and conducting a national exercise program.

Natural Resource: Land, fish, wildlife, biota, air, water, ground water, drinking water supplies, and other such resources belonging to, managed by, held in trust by, appertaining to or otherwise controlled by the state, federal government, private parties, or a municipality.

Navigable Waters: As defined by 40 CFR 110.1 means the waters of the United States, including the territorial seas. The term includes:

All waters that are currently used, were used in the past, or may be susceptible to use in interstate or foreign commerce, including all waters that are subject to the ebb and flow of the tide;

Interstate waters, including interstate wetlands;

All other waters such as interstate lakes, rivers, streams (including intermittent streams), mudflats, sandflats, and wetlands, the use, degradation, or destruction of which would affect or could affect interstate or foreign commerce including any such waters;

That are or could be used by interstate or foreign travelers for recreational or other purposes;

From which fish or shellfish are or could be taken and sold in interstate or foreign commerce; and

That are used or could be used for industrial purposes by industries in interstate commerce.

All impoundments of waters otherwise defined as navigable waters under this section;

Tributaries of waters identified in paragraphs (a) through (d) of this definition, including adjacent wetlands; and

Wetlands adjacent to waters identified in paragraphs (a) through (e) of this definition: Provided, that waste treatment systems (other than cooling ponds meeting the criteria of this paragraph) are not waters of the United States.

Waters of the United States do not include prior converted cropland. Notwithstanding the determination of an area's status as prior converted cropland by any other federal agency, for the purposes of the Clean Water Act jurisdiction remains with EPA.

Nearshore Area: For OPA 90, the area extending seaward 12 miles from the boundary lines defined in 46 CFR Part 7, except in the Gulf of Mexico. In the Gulf of Mexico, it means the area extending seaward 12 miles from the line of demarcation defined in §80.740 - 80.850 of title 33 of the CFR.

Non-persistent or Group I Oil: A petroleum-based oil that, at the time of shipment, consists of hydrocarbon fractions:

- 1. At lease 50% of which by volume, distill at a temperature of 340 degrees C (645 degrees F);
- 2. At least 95% of which volume, distill at a temperature of 370 degrees C (700 degrees F).

Ocean: The open ocean, offshore area, and nearshore area as defined in this subpart.

Offshore area: The area up to 38 nautical miles seaward of the outer boundary of the nearshore area.

Oil or Oils: Naturally occurring liquid hydrocarbons at atmospheric temperature and pressure coming from the earth, including condensate and natural gasoline, and any fractionation thereof, including, but not limited to, crude oil, petroleum gasoline, fuel oil, diesel oil, oil sludge, oil refuse, and oil mixed with wastes other than dredged spoil. Oil does not include any substance listed in Table 302.4 of 40 CFR Part 302 adopted August 14, 1989, under Section 101(14) of the federal comprehensive environmental response, compensation, and liability act of 1980, as amended by P. L. 99-499.

Oil Spill Liability Trust Fund: Means the fund established under section 9509 of the Internal Revenue Code of 1986 (26 U.S.C. 9509).

Oily Waste: Product contaminated waste resulting from a spill or spill response operations.

On-Scene Coordinator (OSC): Means the federal official predesignated by the EPA or the USCG to coordinate and direct response under subpart D.

On-site: Means the areal extent of contamination and all suitable areas in very close proximity to the contamination necessary for implementation of a response action.

Open Ocean: means the area from 38 nautical miles seaward of the outer boundary of the nearshore area, to the seaward boundary of the exclusive economic zone.

Owner or Operator: Any person, individual, partnership, corporation, association, governmental unit, or public or private organization of any character.

Persistent Oil: A petroleum-based oil that does not meet the distillation criteria for a non-persistent oil. For the purposes of this Appendix, persistent oils are further classified based on specific gravity as follows:

- 1. Group II specific gravity less than .85
- 2. Group III specific gravity between .85 and less than .95
- 3. Group IV specific gravity .95 and including 1.0
- 4. Group V specific gravity greater than 1.0

Plan Holder: The plan holder is the industry transportation related facility for which a response plan is required by federal regulation to be submitted by a vessel or facility's owner or operator.

Post Emergency Response: The portion of a response performed after the immediate threat of a release has been stabilized or eliminated and cleanup of the sites has begun.

Post Emergency: The phase of response operations conducted after the immediate threat of the release has been stabilized, and cleanup operations have begun.

Primary Response Contractors or Contractors: An individual, company, or cooperative that has contracted directly with the plan holder to provide equipment and/or personnel for the containment or cleanup of spilled oil.

Qualified Individual (QI): That person or entity who has authority to activate a spill cleanup contractors, act as liaison with the "On-Scene Coordinator" and obligate funds required to effectuate response activities.

Recreation Areas: Publicly accessible locations where social/sporting events take place.

Regional Response Team (RRT): The Federal response organization (consisting of representatives from selected Federal and State agencies) which acts as a regional body responsible for overall planning and preparedness for oil and hazardous materials releases and for providing advice to the OSC in the event of a major or substantial spill.

Remove or Removal: As defined by section 311(a)(8) of the CWA, refers to containment and removal of oil or hazardous substances from the water and shorelines or the taking of such other actions as may be necessary to minimize or mitigate damage to the public health or welfare (including, but not limited to, fish, shellfish, wildlife, public and private property, and shorelines and beaches) or to the environment. For the purpose of the NCP, the term also includes monitoring of action to remove discharge.

Response Activities: The containment and removal of oil from the water and shorelines, the temporary storage and disposal of recovered oil, or the taking of other actions as necessary to minimize or mitigate damage to public health or welfare, or the environment.

Response Contractors: Persons/companies contracted to undertake a response action to contain and/or clean up a spill.

Response Guidelines: Guidelines for initial response that are based on the type of product involved in the spill, these guidelines are utilized to determine clean-up methods and equipment.

Response Plan: A practical manual used by industry for responding to a spill. Its features include: (1) identifying the notifications sequence, responsibilities, response techniques, etc. in a easy to use format; (2) using decision trees, flowcharts, and checklists to insure the proper response for spills with varying characteristics; and (3) segregating information needed during the response from data required by regulatory agencies to prevent confusion during a spill incident.

Response Resources: All personnel and major items of equipment available, or potentially available, for assignment to incident tasks on which status is maintained.

Responsible Party: Any person, owner/operator, or facility that has control over an oil or hazardous substance immediately before entry of the oil or hazardous substance into the atmosphere or in or upon the water, surface, or subsurface land of the state

Response Priorities: Mechanism used to maximize the effective use of manpower and equipment resources based upon their availability during an operational period.

Response Resources: All personnel and major items of equipment available, or potentially available, for assignment to incident tasks on which status is maintained.

Restoration: The actions involved in returning a site to its former condition.

Rivers and Canals: A body of water confined within the inland area that has a project depth of 12 feet or less, including the Intracoastal Waterway and other waterways artificially created for navigation.

Securing the Source: Steps that must be taken to stop discharge of oil at the source of the spill.

Sinking Agents: Means those additives applied to oil discharges to sink floating pollutants below the water surface.

Site Characterization: An evaluation of a cleanup site to determine the appropriate safety and health procedures needed to protect employees from identified hazards.

Site Conditions: Details of the area surrounding the facility, including shoreline descriptions, typical weather conditions, socioeconomic breakdowns, etc.

Site Safety and Health Plan: A site specific plan developed at the time of an incident that addresses:

- Safety and health hazard analysis for each operation.
- Personal protective equipment to be used.
- Training requirements for site workers.
- Medical surveillance requirements.
- Air monitoring requirements.
- Site control measures.
- Decontamination procedures.
- Emergency response procedures.
- Confined space entry procedures.

Site Security and Control: Steps that must be taken to provide safeguards needed to protect personnel and property, as well as the general public, to ensure an efficient clean-up operation.

Skimmers: Mechanical devices used to skim the surface of the water and recover floating oil. Skimmers fall into four basic categories (suction heads, floating weirs, oleophilic surface units, and hydrodynamic devices) which vary in efficiency depending on the type of oil and size of spill.

Snare Boom: Oil will adhere to the material of which this boom is made of and thus collect it.

Sorbents: Materials ranging from natural products to synthetic polymeric foams placed in confined areas to soak up small quantities of oil. Sorbents are very effective in protecting walkways, boat decks, working areas, and previously uncontaminated or cleaned areas.

Spill: An unauthorized discharge of oil or hazardous substance into the waters of the state.

Spill Observer: The first Facility individual who discovers a spill. This individual must function as the first responder and person-in-charge until relieved by an authorized supervisor.

Spill of National Significance (SONS): Means a spill which due to its severity, size, location, actual or potential impact on the public health and welfare or the environment, or the necessary response effort, is so complex that it requires extraordinary coordination of federal, state, local, and responsible party resources to contain and cleanup the discharge.

Spill Management Team: The personnel identified to staff the organizational structure identified in a response plan to manage response plan implementation.

Spill Response: All actions taken in responding to spills of oil and hazardous materials, e.g.: receiving and making notifications; information gathering and technical advisory phone calls; preparation for and travel to and from spill sites; direction of clean-up activities; damage assessments; report writing, enforcement investigations and actions; cost recovery; and program development.

Spill Response Personnel: Federal, state, local agency, and industry personnel responsible for participating in or otherwise involved in spill response. All spill response personnel will be preapproved on a list maintained in each region.

Staging Areas: Designated areas near the spill site accessible for gathering and deploying equipment and/or personnel.

State Emergency Response Commission (SERC): A group of officials appointed by the Governor to implement the provisions of Title III of the Federal Superfund Amendments and Reauthorization Act of 1986 (SARA). The SERC approves the State Oil and Hazardous Substance Discharge Prevention and Contingency Plan and Local Emergency Response Plans.

Surface Collecting Agents: Means those chemical agents that form a surface film to control the layer thickness of oil.

Surface Washing Agent: Is any product that removes oil from solid surfaces, such as beaches and rocks, through a detergency mechanism and does not involve dispersing or solubilizing the oil into the water column.

Tanker: A self-propelled tank vessel constructed or adapted primarily to carry or hazardous material in bulk in the cargo spaces.

Tidal Current Tables: Tables which contain the predicted times and heights of the high and low waters for each day of the year for designated areas.

Trajectory Analysis: Estimates made concerning spill size, location, and movement through aerial surveillance or computer models.

Transfer: Any movement of oil to, from, or within a vessel by means of pumping, gravitation, or displacement.

Trustee: Means an official of a federal natural resources management agency designated in subpart G of the NCP or a designated state official or Indian tribe or, in the case of discharges covered by the OPA, a foreign government official, who may pursue claims for damages under section 1006 of the OPA.

Underwriter: An insurer, a surety company, a guarantor, or any other person, other than an owner or operator of a vessel or facility, that undertakes to pay all or part of the liability of an owner or operator.

Unified Command: The method by which local, state, and federal agencies and the responsible party will work with the Incident Commander to:

- Determine their roles and responsibilities for a given incident.
- Determine their overall objectives for management of an incident.
- Select a strategy to achieve agreed-upon objectives.
- Deploy resources to achieve agreed-upon objectives.

Unified or Coordinated Command Meeting: Held to obtain agreement on strategic objectives and response priorities; review tactical strategies; engage in joint planning, integrate response operations; maximize use of resources; and minimize resolve conflicts.

Volunteers: An individual who donates their services or time without receiving monetary compensation.

Waste: Oil or contaminated soil, debris, and other substances removed from coastal waters and adjacent waters, shorelines, estuaries, tidal flats, beaches, or marshes in response to an unauthorized discharge. Waste means any solid, liquid, or other material intended to be disposed of or discarded and generated as a result of an unauthorized discharge of oil. Waste does not include substances intended to be recycled if they are in fact recycled within 90 days of their generation or if they are brought to a recycling facility within that time.

Waters of the U.S. - See Navigable Waters in this Glossary.

Wetlands: Those areas that are inundated or saturated by surface or groundwater at a frequency or duration sufficient to support, and that under normal circumstances do support, a prevalence of vegetation typically adapted for life in saturated soil conditions. Wetlands generally include playa lakes, swamps, marshes, bogs, and similar areas such as sloughs, prairie potholes, wet meadows, prairie river overflows, mudflats, and natural ponds (40 CFR 112.2(y)).

Wildlife Rescue: Efforts made in conjunction with Federal and State agencies to retrieve, clean, and rehabilitate birds and wildlife affected by an oil spill.

Worst Case Discharge: The largest foreseeable discharge under adverse weather conditions. For facilities located above the high water line of coastal waters, a worst case discharge includes those weather conditions most likely to cause oil discharged from the facility to enter coastal waters.

ACRONYMS

ESA

- Endangered Species Act

AC	_	Area Committee	ETA	_	Estimated Time of Arrival
AOR	-	Area of Review	FAA	_	Federal Aviation Administration
AQI	-	Alternate Qualified Individual	FACT	_	First Assessment Crisis Team
BIA	-	Bureau of Indian Affairs	FAX	_	Facsimile Machine
BLM	-	Bureau of Land Management	FCC	_	Federal Communications
BPD	-	Barrels Per Day			Commission
BOD BOEMRE	- -	Biological Oxygen Demand Bureau of Ocean Energy,	FEMA	-	Federal Emergency Management Agency
		Management, Regulation and Enforcement (replaced MMS)	FOSC FR	-	Federal On-Scene Coordinator Federal Register
вом	_	Bureau of Mines	FRDA	-	Freshwater Resource Damage
CAER	-	Community Awareness and Emergency Response		-	Assessment
СВР		Customs and Border Protection	FRF	-	Federal Revolving Fund
CERCLA	_	Comprehensive Environmental	GIS	-	Geographic Information System
OLNOLA	-	Response, Compensation and	GSA	-	General Services Administration
CFR	_	Liability Act Code of Federal Regulations	HAZWOPER	-	Hazardous Waste Operations and Emergency Response
CHEMTREC		Chemical Transportation	HHS	-	Department of Health and Human
CHLINITICE	-	Emergency Center			Services
COE	-	U. S. Army Corps of Engineers	HOPD	-	Head Office Products Distribution
CPI	-	Corrugated Plate Interceptor	IBRRC	-	International Bird Rescue Research Center
CRZ	-	Contamination Reduction Zone	IOCC	-	Interstate Oil Compact
CWA	-	Clean Water Act (Federal - Public			Commission
cws	_	Law 100-4) Community Water System	LEPC	-	Local Emergency Planning Committee
CZM	_	Coastal Zone Management	LFL	_	Lower Flammable Limit
DECON	_	Decontamination	LOSC	_	Local On-Scene Coordinator
DOS	_	Department of State	LRT	_	Local Response Team
DOT	_	Department of Transportation	MBL	_	Mobile
DRAT	_	District Response Advisory Team	MER	_	Marine Emergency Response
DRG	-	District Response Group	MMS	-	Minerals Management Service
EBS	-	Emergency Broadcast System			(replaced by BOEMRE)
EHS	-	Extremely Hazardous Substance	MMT	-	Marine Management Team
EMA	-	Emergency Management Agency	MOU	-	Memorandum of Understanding
EMS	-	Emergency Medical Service	MSDS	-	Material Safety Data Sheet
EOC	-	Emergency Operations Center	MSO	-	Marine Safety Office
EPA	-	U. S. Environmental Protection Agency	MSRC	-	Marine Spill Response Corporation
EPCRA	_	The Emergency Planning and	NCP	-	National Contingency Plan
		Community Right-to-Know Act of 1986 (Title III of SARA)	NCWS	-	Non-Community Water System
EQ	-	Environmental Quality			
ERT	-	Environmental Response Team			

NEPA	-	National Environmental Policy	RCRA	-	Resource Conservation and
		Act			Recovery Act
NIOSH	-	National Institute for Occupational Safety and Health	RECON	_	Reconnaissance
NMFS	_	National Marine Fisheries Service	REP	-	Radiological Emergency Preparedness
NOAA	_	National Oceanic and	RERT	-	Radiological Emergency
		Atmospheric Administration			Response Team
110000		(Department of Commerce)	RQ	-	Reportable Quantity
NPDES	-	National Pollution Discharge Elimination System	RRT	-	Regional Response Team
NPFC	-	National Pollution Funds Center	RSPA	-	Research and Special Programs Administration (replaced by
NPS	-	National Park Service			PHMSA)
NRC	-	National Response Center	SARA	-	Superfund Amendments and
NRDA	-	Natural Resource Damage			Reauthorization Act
		Assessment	SCBA	-	Self Contained Breathing Apparatus
NRS	-	National Response System	SDWA	_	Safe Drinking Water Act
NRT	-	National Response Team	SERC	_	State Emergency Response
NSF	-	National Strike Force	CLINO		Commission
NSFCC	-	National Strike Force Coordination Center	SIC	-	State Implementation Plan
NTNCWS		Non -Transient Non-Community	SMT	-	Spill Management Team
		Water System	SONS	-	Spill of National Significance
OPA	-	Oil Pollution Act	SOP	-	Standard Operating Procedure
OPS	-	Office of Pipeline Safety (DOT)	SPCC	-	Spill Prevention Control and
osc	-	On-Scene Coordinator	000		Countermeasures
OSHA	-	Occupational Safety and Health Administration (USDL)	SSC	-	Scientific Support Coordinator (NOAA)
OSLTF	-	Oil Spill Liability Trust Fund	STEL	-	Short Term Exposure Limits
OSPRA	-	Oil Spill Prevention and Response Act	SUPSALV	-	United States Navy Supervisor of Salvage
OSRO	-	Oil Spill Response Organization	SWD	-	Salt Water Disposal
PCB	-	Polychlorinated Biphenyls	TSCA	-	Toxic Substances Control Act
PFD	-	Personal Flotation Device	TSDF	-	Treatment, Storage or Disposal Facility
PGR	-	Pager	UCS	_	Unified Command System
PHMSA		Pipeline and Hazardous Material	USACOE	_	U.S. Army Corps of Engineers
		Safety Administration (replaced	USCG	_	U.S. Coast Guard
DIAT		RSPA)	USDA	-	U.S. Department of Agriculture
PIAT	-	Public Information Assist Team	USDL	_	U.S. Department of Labor
POLREP PPE		Pollution Report Personal Protective Equipment	USDOD	_	U.S. Department of Defense
PPM	_	Parts Per Million	USDOE	-	U.S. Department of Energy
PSD	_	Prevention of Significant	USDW	-	Underground Source of Drinking
. 00		Deterioration	HOEWO		Water
QI	-	Qualified Individual	USFWS	-	U. S. Fish and Wildlife Services
RACT	-	Reasonably Achievable Control	USGS	-	U. S. Geological Survey
		Technology	WCD	-	Worst Case Discharge
RCP	-	Regional Contingency Plan			

Section 6- Terminal Facilities

Section 6 - Terminal Facilities

(Please contact Tony Mills for any questions/clarification on this section.)

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Changes

Overview

Both the new/changed and deleted requirements are listed below. Only general descriptions are given to help the user understand the change from the previous version.

Reference	Page #	Correction / Clarification (C) or Revision (R)	Description	Revision Effective Date
	i	R	Changed the Content Owner of Section 6 to Tony Mills	11/2008
6.10.4	6-47	R	Deleted the control valve shutdown in 2-3 seconds of an overfill situation reference.	11/2008
6.10.13	6-52	R	Deleted the gate opening sequence in an Emergency Shutdown reference.	11/2008
6.14.1	6-61	R	Added requirements for sealing and padlock locations.	11/2008
6.14.3	6-62	R	Added requirement for replacing illegible or damaged seals.	11/2008
6.14.3	6-62	R	Added requirement for Terminal personnel to record Terminal security sealing activities in InControl.	11/2008
6.19.6	6-92	R	Deleted Seal Log Records section of hard copy forms. InControl now manages these functions.	11/2008
6.19.7	6-97	R	Deleted the steps for inspection of the interior of marine hoses.	11/2008

6.1 - Overview

Terminal management is responsible for the efficient use and safe operation of terminal facilities. Good housekeeping and terminal maintenance play an important role in terminal upkeep. Good housekeeping is a primary indicator of the quality and effectiveness of management.

Terminal management must have in place a system of routine checks and inspections to ensure safe, clean and efficient operations. Terminal operating personnel should perform all minor repairs and preventive maintenance tasks that fall within the scope of their regular duties and capabilities. Senior management will establish direction for handling maintenance work that requires outside assistance. See the Motiva Technical Manual or your Technical Resource for details on standards for terminal facilities. This section includes the description of equipment used in a distribution facility and the required inspections performed on such equipment. Also included are inspection procedures, frequency and appropriate forms.

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Terminal Facilities

6.2 - Terminal Inspections

6.2.1 - General

Terminal facilities must be safe for employees, the public and the environment. Management should emphasize preventive maintenance through scheduled periodic inspections that locate developing problems before failure or product leakage occurs. Documentation requirements and frequency intervals for terminal inspections are given throughout this section. InControl is the current mechanism to identify and track all required inspections.

The following are requirements for terminal inspections.

- Local terminal management has responsibility to oversee all periodic inspections to ensure good operating condition and maintenance of product quality.
- Qualified inspectors from outside the terminal can also perform terminal inspections to validate routine inspections and supplement the regular terminal inspection program.
- An API-certified inspector must perform multiyear external and internal tank inspections.

6.2.2 - Inspection Requirements

Regulatory Agency Requirements

Company policy is to comply with all laws and regulations; our inspection and maintenance standards meet or exceed those set by government agencies. The policies in this manual are not intended to contradict, in whole or in part, any governmental rulings. Regulations will take precedence if any apparent conflict arises. Terminal management must communicate such conflicts to senior management.

Documentation

Effective inspection programs require good records. InControl in conjunction with various inspection forms is the current method to document and record inspections performed.

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Terminal Facilities

Retention of Forms

The current Company Retention Schedule is available on the Company intranet on the Document Management home page (Intranet home page/Corporate Resources/Record Management). At a minimum, retention of inspection documentation must be from audit period to audit period.

API requires tank documentation (i.e. API 653 inspector forms, calculations, drawings etc.) to be retained for the life of the tank, if the tank is inspected, repaired or altered.

Housekeeping

Safe terminals are always clean terminals. Management must maintain the property and its facilities in a clean, orderly condition. Good housekeeping aids safe, clean and efficient operation and indicates good management. Non-terminal management personnel visiting terminals will view housekeeping as one of the important yardsticks to assess management of the facility.

All employees must help keep the terminal neat, clean and in good repair.

Alternatives to Company employees should be considered to maintain proper standards.

Follow OSHA rules and regulations on housekeeping requirements.

6.2.3 - Daily Visual Overall Terminal Inspection



Daily refers to days when terminals are routinely scheduled to be staffed.

Terminal management is responsible for developing and implementing an inspection program for recognizing and/or evaluating the following conditions:

- overall appearance and housekeeping
- signs of leaks
- unusual equipment noises
- odors
- security
- operational readiness
- target indication for floating suctions
- dike and roof drains
- VRU/VCU operating parameters
- safety and
- any other SPCC plan requirements.

Local terminal personnel must complete and document a daily walk through inspection which checks for conditions listed above. Daily inspections ensure safe, efficient operation and give management a better understanding of terminal operations.



Each terminal's SPCC plan requires a daily inspection.

6.2.4 - Annual Self Appraisal

In accordance with Standard 105, HSE audit program, a self-appraisal will be conducted annually/ongoing. It is a site-specific form to ensure local HS&E permits and conditions are being complied with. The Regional/Terminal Manager will coordinate scheduling of the SA during the year.

Local Management may schedule parts of the inspection throughout the year, rather than the entire inspection all at once. However all sections must be completed annually. Refer to Section 8.2.1.2, Facility Self-Assessment for more details.

6.2.5 - Assurance Reviews

Terminal and Head Office management are responsible to develop assurance and compliance systems confirming terminal personnel are using and following established procedures. Contact your Environmental Representative for assistance. For a detailed description of compliance assurance, refer to HS&E MS Standard 100. Local assurance procedures, such as those listed below, must be established as appropriate:

- random checks by plant supervisors
- plant team reviews
- · internal terminal management reviews or audits, and
- informal reviews or checks by region or head office staff.



These reviews do not require documentation.

Head Office will arrange for periodic terminal reviews to assure senior management is in compliance with company policy and governmental regulations. Assurance reviews may be independent or in conjunction with corporate compliance assurance reviews. These reviews may include:

- Management System Assurance (MSA)
- Internal/Independent HS&E Review
- Financial Audit (including Measurement Policy compliance)

6.3 - Aboveground Storage Tanks

Aboveground Storage Tanks are Distribution's largest and most important asset. As such, oversight is provided by a centralized tank inspection program. Terminal Management must be aware of scheduled tank inspections. Consult with your Project Coordinator or other Technical Resource to clarify any questions

6.3.1 - Tank Regulations

The federal government has been slow to develop and implement tank regulations. In response, many states and local municipalities are choosing to promulgate their own tank regulations.

Head Office does not follow most state or local legislative and regulatory activities, so local plants must be alert to developing regulations. In addition, plants must become part of the development process to help ensure establishment of reasonable and effective tank regulations.

All tank repairs and maintenance are to be coordinated with Local Project Coordinator and Environmental Representative.

6.3.2 - External Floating Roofs

Distribution currently uses two types of external floating roofs (EFR): pontoon and double-deck. Both of these use steel construction.

Manufacturers supply various versions of the two basic roof types that emphasize different features, such as full-liquid contact, load-carrying capacity, roof stability or pontoon arrangement. Roof fittings can contribute to evaporative loss; however, these fittings normally have design features to minimize such losses.

To convert an external floating roof to an internal floating roof, a fixed roof can be installed over the floating roof. Such fixed roofs include a cone roof and a lightweight aluminum geodesic dome. Such roofs rest on and are anchored to the tank shell. Any changes to the tank's EFR must be coordinated with Local Project Coordinator and Environmental Representative to properly account for all emissions.

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Terminal Facilities

6.3.3 - Internal Floating Roofs

Most internal floating roofs (IFR) fall into one of these categories:

- steel or aluminum pan
- aluminum pontoon or aluminum honeycomb sandwich, or
- old external floating roofs that have been converted to internal floaters.

Like external floating roofs, each of the designs has inherent design features and limitations. A few of these are cost, inherent buoyancy, corrosion resistance, durability and service life.

An alternative to the typical leg supported roof, a cable suspended roof can be installed. This cable suspended IFR is not supported by adjustable leg; it is supported by cables that run through the fixed roof. These cables can be adjusted to change the minimum operating height of the suspended roof. The advantages to a cable suspended IFR are:

- increases the tank capacity
- reduces the emissions lost through the leg openings
- does not require entering the tank to adjust roof setting
- no risk of damage to floor caused by legs

Any changes to the tank's IFR must be coordinated with Local Project Coordinator and Environmental Representative to properly account for all emissions.

6.3.4 - Procedures for All Floating Roof Systems

Consult with your Health and Safety Representative for proper equipment and procedures when descending onto the floating roof (internal or external) of a tank. Typically, descent onto the roof of an external floating roof tank constitutes entering a confined space.

Maintain product levels that prevent the roof from resting directly on the legs or supports, except when the tank is taken out of service. Head Office management must approve any exceptions to this policy.



The reasons for this policy are safety, air emissions during refilling, hazardous vapors during emptying, product loss, erosion-corrosion damage to the tank floor, and stress cracking of the floating roof.

Limit receipt line fill rates to 3 feet/second when bringing a tank into service, until the roof is floating or the product level is at least 1 foot above the fill line inlet. This fill rate must also be maintained, when floating a roof, from 3 inches below the critical zone to 3 inches above the critical zone. This limit minimizes static electricity generation and prevents roof damage (e.g. seals getting hung up, interference) and verifies appurtenances operating correctly. Consult with your Local Project Coordinator for further assistance.



Use the *Flow Rate Conversion Table for Various Pipe Sizes* (in the Appendix of Section 3) to convert rates, indicated as feet per second (fps), to gallons per minute (gpm).

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6.3.5 - Procedures to Manage Rain Water from Aboveground Tanks

All terminals with tanks that have roof drains must have a written plan for managing tank roof drains. The plan must include, but should not be limited to, the following requirements.

 The plan must ensure that the dike valves are closed before opening roof drain valves and to keep dike valves closed during the entire time roof drain valves are open.



Roof drain systems are present only on external floating roof tanks, or tanks converted to internal pans.

- The plan must assign specific responsibility and accountability to personnel for knowing and documenting the status of tank roof drain valves.
- The plan must include provisions for always keeping tank roof drain valves closed and locked unless attended drain operations are underway.
- The plan must include procedures for contacting Head Office management if a faulty roof drain is leaking or cannot be closed, to determine whether to remove the tank from service. Special documented interim operating procedures will be required until the drain can be repaired (e.g., placing portable air-operated pump on the floating roof and monitoring during rain).
- The plan must include requirements for visually inspecting roof drain valves status (open or closed) daily and document on daily walk through checklist.
- The plan must include requirements for visually inspecting for status and operability all roof and dike drain valves at least quarterly, and recording valve status in a report, log book or other record that can be reviewed for compliance.
- The plan must include requirements for conducting and documenting training for personnel with responsibility for roof draining.

6.3.6 - Tank Inspection Requirements

General

Distribution has chosen to follow the requirements of API Standard 653. API 653 is a minimum standard that covers tank inspection, repair, alteration and reconstruction.



Project Coordinator may use the *Tank Inspection and Maintenance Manual* for reference.

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Terminal Facilities

Types of API 653 Tank Inspections

There are three inspections required by API 653:

Monthly in-service inspection by a company employee at the location (See details below)

Annual external inspection by a Motiva certified API 653 tank inspector or every five years as per API 653. See your Project Coordinator for appropriate frequency.

Internal inspection by a certified API 653 tank inspector

The frequency of these inspections is based on the corrosion rate of the tank floor – both topside and underside. The actual inspection interval must be set to ensure the bottom plate minimum thicknesses at the next inspection are not less than the values listed in API 653, Table 4-1. The internal inspection interval shall never exceed 20 years.

Guidelines For Monthly Inspections

Guidelines for monthly tank inspection according to API 653 are listed below.

 The purpose of the monthly inspection is to identify any significant or major changes in the tank since the last inspection. Monthly inspections partially fulfill API 653 requirements.



DOT jurisdictional terminals must complete a yearly tank inspection. Any one of the monthly inspections will meet the requirements of this regulation therefore a separate annual tank inspection is not required. [CFR 49, Part 195.432, Paragraphs (a) and (b)]. Refer to Section 12 for definitions and information about DOT jurisdictional terminals. Currently, There are no DOT tanks owned and operated by Motiva Distribution as of current.

- Monthly inspections must be assigned to terminal operators, gaugers or other personnel who are knowledgeable about tanks, storage facility operations and products stored.
- Inspections must be documented, noting any failures or significant damage, on the "Storage Tank Monthly In Service Inspection Report" (taken from *Tank Inspection and Maintenance Manual*) in Appendix 6.19.1 or an equivalent inspection form. The completed reports must be retained at the Terminal.



Listing multiple tanks on one form for a single month is acceptable. A form with multiple months for 1 tank is not recommended because form retention is a moving window.

 Send information about any potentially serious condition (i.e., inspection report, detailed description, photos, sketches, etc.) to your technical resource. Technical support can provide technical help and will coordinate ultrasonic, external and internal inspections.

Routine in-service inspection includes a visual check of the tank's exterior surface and surrounding area for any of these deficiencies:

- Leaks Look for product on the top surface of the foundation or apron; product sheen on the ground or ground water; or seepage from rivets, seams, valves, flanges, welds or open areas of plate.
- Distortions Look for signs of inward or outward bowing of tank shell and any visible distortions in the bottom extension or roof angle.
- Settlement Check for visible settlement into the earth, sand or asphalt apron; buildup of apron material above tank bottom against the shell; and liquid drainage toward the tank.
- Corrosion Check shell, bottom extension, nozzles, manway necks and attached piping. Do not allow dirt, rocks or gravel to accumulate against the chime (shell-to-bottom joint). Normally the chime is protected by paint to prevent atmospheric, not underground exposure. Soil against the chime allows moisture migration under the uncoated tank floor, promoting corrosion.
- Foundation Look for cavities under the tank and broken, cracked or spalling concrete.
- Paint Check for cracked, blistered or rusted areas.
- Insulation (as appropriate) Check insulation for damage. Seal any penetrations through insulation to keep out water and moisture.
- Appurtenances Look for missing flange bolts and corroded bolts or welds. Note any leaks from tank appurtenances.
- Dike To prevent corrosion on the underside of the floor and on the edge
 of the floor extension (chime), maintain the slope of the dike yard so that
 rainwater flows away from the tank. Drain rainwater so it does not stand
 against the tank.
- Surrounding Area Check for damage or erosion in the dike wall, look for excess vegetation growth.

External In-Service Inspection

External in-service inspections will be done by a Motiva API 653-certified tank inspector annually. A terminal may also perform a five-year external inspection as per API 653. Both inspections are not required.

Terminal management will coordinate with technical resources to schedule and conduct these inspections.

Internal Inspections

Internal, out-of-service inspections (with 95 percent electronic floor scan) will be conducted by an API 653 certified tank inspector according to this schedule:

- Whenever a tank has been out of service more than 1 year and will be returned to service. Contact your technical resource, who will evaluate the tank, review the records and determine the need for future inspections/repairs.
- Before remaining bottom thickness has corroded to the level specified in API 653 or at least every 20 years, whichever is less. Contact your technical resource to determine which states require more frequent internal inspections than specified in API 653.



Annually, local Terminal management is to discuss and strategize tank inspections to occur in the next 12 to 18 months with their project coordinator (during this session, dock inspections and API 570 Inspections for onsite and offsite underground lines should be discussed – Reference Sections 6.8.4 and 6.11.3). Local Terminal Managers will also coordinate all tank out-of-service activities with Supply. Consideration must be taken for peak demand periods.

When tanks are scheduled out-of-service, consider allowing time for unforeseen repairs, as well as time required to clean and inspect the tank. Check the last external inspection report and tank files for suggested welding, internal lining condition and other repairs. Check with Local Project coordinator to assure all necessary work is done when out of service. Local Project Coordinator can use Tank Closure Checklist for guidance. Example of this checklist is in Appendix 6.19.2.

More and more states are passing legislation that affect storage tanks, especially regulations to comply with the Clean Air Act and secondary containment laws. Regulations may be pending that will require tank modifications while the tank is gas free. While planning an internal out-of-service inspection, consider consulting with local environmental representatives to determine whether tank modification or additions will be required in the near future. If so, consider preparing for such additions (e.g., by installing bolts, bolt holes or weld-on brackets necessary for secondary seals, wiper seals).

Refer to Section 9 for appropriate inspection intervals for internal inspections of aboveground tanks for product quality (i.e. Jet Fuel).

6.3.7 - Floating Roof Seal Systems

General

All types of floating roofs have an annular rim space between the tank shell and the roof's outer periphery to permit the roof to travel within the tank. The annular rim space must have an effective seal system to minimize evaporative losses and to meet air quality regulations. An effective seal system closes the rim space and helps to center the floating roof, but permits normal roof movement.

A seal system can consist of one or two separate seals called the primary and secondary seals. Company terminals have installed a variety of seal systems in the past; however, current construction standards recommend double-wiper seals or mechanical shoe primary and if required wiper secondary seal to meet environmental regulations (See Appendix 6.19.4).

Seal System Requirements

Federal regulations require a pan with one of two seal types for volatile (RVP>=1.5psia) products:

Liquid-mounted seals (the roof seal rides in the liquid thus allowing no vapor space)

Vapor-mounted seals (the roof seal forms a vapor barrier between the roof and tank shell)

Federal and local regulations may require inspection and repair of holes or defects in the seal system. Integrity of the vapor space enclosure is important to control evaporative loss.



Consult with Local Technical Resources and Health and Safety Representative if the seal system needs to be repaired or replaced.

6.3.8 - Primary Seals

General

This section describes the following three types of primary seals:

- mechanical (metallic) shoe seals
- resilient (nonmetallic) filled seals, and
- flexible- wiper seals.

Mechanical (Metallic) Shoe Seals

The following provides information on mechanical shoe seals.

- This seal's identifying characteristic is a light-gauge metallic band (shoes) that serves as the sliding contact with the tank shell. A mechanical device attached to the floating roof supports the metallic band and holds it against the tank shell (See Appendix 6.19.21).
- A coated fabric (the primary seal fabric) seals the rim space. Bolting or clamping the fabric from the shoes to the floating roof creates this seal.
- The specific type of primary seal fabric may vary according to the manufacturer and the kind of hydrocarbon service.
- Mechanical shoe seals usually accommodate a local variation of ±5 inches in a normal 8-inch rim space.
- Mechanical shoe seals have the longest service life (20+ years) in normal use (i.e., when the roof is continually floating). In general, the primary seal fabric may begin to show signs of aging before the metallic parts show wear. Severe corrosion may occur when using mechanical shoe seals in a corrosive product or under unusual operating conditions, such as the underside of a roof that has frequent exposure to air. Using corrosion-resistant metals or special coatings is advantageous in such cases.
- EFRs also include a weather shield. Other types of primary and secondary seals are in use or under development, but are not yet widely used.

Resilient (Nonmetallic) Filled Seals

This seal's identifying characteristic is a coated fabric envelope that contains resilient foam. The material in the envelope expands to provide a sliding contact with the tank shell (See Appendix 6.19.22).

A resilient filled seal may be either liquid mounted or vapor mounted. A liquid-mounted seal sits on the floating roof so that it touches the liquid surface. A vapor-mounted seal allows a vapor space between the liquid and the seal.

Service considerations for resilient filled seals are listed below.

- A resilient filled seal's main advantage is its flexibility to accommodate a normal variation of ±4 inches in rim space.
- Vapor-mounted seals do not control emissions as well as a liquid mounted seal, but do not deteriorate from contact with the product as quickly as a liquid-mounted seal.
- A vapor mounted seal requires a secondary seal to control emissions.

- Liquid-mounted seals significantly reduce evaporative loss since they have no rim vapor space however they deteriorate more quickly because they are in contact with product
- Liquid-mounted seals may also absorb product into the foam making tank cleaning more difficult and expensive.
- The normal life of resilient seals is typically 7-10 years.
- Projections from the shell, such as rivet heads or burrs, may cause wear and reduce the seal's service life.
- If a tank has this type of seal, consider upgrading to a mechanical (metallic) shoe seal during the next API 653 internal inspection. This will provide a longer service life (20+ years).

Flexible-Wiper Seals

This seal's identifying characteristic is an elastomeric blade that serves as a sliding contact with the tank shell (similar to the windshield wiper on a vehicle).

The flexible-wiper seal bridges the annulus between the floating roof and the tank shell and uses its own stiffness or mechanical means to push the seal against the tank shell (See Appendix 6.19.23).

Service considerations for flexible-wiper seals are listed below.

- This seal's advantage is its flexibility. The wiper is usually more flexible than a mechanical shoe seal; therefore, it may conform better to the tank shell.
- The wiper seal is mounted above the liquid to avoid potential deterioration from contact with liquid. Like resilient filled seals, the nonmetallic parts of wipers do not corrode.
- Most flexible-wiper seals accommodate a normal variation of ±4 inches in the rim space. Large-diameter tanks or those with a rim space greater than 8 inches may require special details.
- The rim vapor space of flexible-wiper seals do not control emissions as well as liquid mounted seal. Gaps between the seal and tank shell lead directly to the rim vapor space and permit more evaporative loss.
- A vapor mounted seal requires a secondary seal to control emissions.

6.3.9 - Secondary Seals

Secondary seals usually consist of fabric or elastomeric materials, sometimes with metallic or nonmetallic stiffeners to reinforce the fabric, or external attachments to guide the seal. Secondary seals generally fall into one of three categories: shoe-mounted, or rim-mounted.

Shoe-mounted secondary seals effectively reduce losses from gaps between the shoe and tank shell, but do not control losses from defects or connections in the primary seal fabric.

Rim-mounted secondary seals more effectively reduce losses because they cover the entire rim space. Rim-mounted seals make up the vast majority of secondary seals.

Mini secondary shoe seals are an alternative.

Service considerations for secondary seals are as follows.

- Some secondary seals can reverse as the floating roof reverses its direction of travel.
- A secondary seal must maintain contact with the tank shell to be effective; therefore, the roof cannot travel as close to the tank shell's top edge.
 This limitation slightly reduces the tank's working capacity.
- Properly fitted shoe-mounted secondary seals provide a good service life.
- Mini secondary seals have a significantly longer service life than the shoe-mounted and the rim mounted secondary seals.

6.3.10 - Floating Roof Seal Inspections

There are four general types of seal inspections:

- Tanks with external floating roofs require an annual close visual inspection and a seal gap measurement every 5 years for the primary seal and annually for a secondary seal (if applicable). A monthly visual inspection from the top of the tank is also required.
- Tanks with internal floating roofs require a visual inspection from the manway annually.
- Tanks at Maximum Achievable Control Technology (MACT) facilities require a 10-year seal inspection on internal floating roofs in addition to the annual manway inspection.
- Any tank taken out of service for cleaning requires a close visual seal inspection. The type of floating roof and EPA's "k" classification must be determined in order to determine any additional inspection requirements. Refer to Local Environmental Representative for assistance.



Some local and state jurisdictions have additional seal inspection requirements. Check with the environmental representative for additional requirements.

Local or contract personnel who are familiar with various seal designs and operation will perform seal inspections. Refer to Appendix 6.19.4 for procedures and suggested forms. Local Management can choose to use an equivalent form.

Information from the inspections ensures compliance with regulations and allows scheduling of seal maintenance for the coming years.

Early detection and correction of seal problems may prevent further damage, including sinking of a floating roof.

6.3.11 - Weather Shields

Most external floating roof require weather shields. The following provides information on weather shields.

- Weather shields usually have an overlapping shingle-type construction and numerous radial joints to allow for roof movement and tank shell irregularities.
- Weather shields have metallic, elastomeric or composite construction.
- A mechanical or pliable hinge connection normally attaches the weather shield to the floating roof.
- Weather shields generally extend primary seal life by protecting the fabric from weather and debris.

6.3.12 - Floating Suction and Suction Trough

A "floating suction" is a jointed pipe connected to the shipping nozzle of the tank that is able to rise and fall with product level inside the tank. This allows product to always be drawn from within a couple of feet of the top level of product in the tank.

Floating suctions offer many benefits, if operating properly, such as:

- More quickly being able to draw product from a tank after a receipt in case of hazy product, particulate contamination, etc.
- Reduces risk of off spec product being shipped if the tank is shipping and receiving product simultaneously
- Enhances the ability to mix tank for RVP blend down, particularly if the tank does not have mixing nozzles, etc.
- Minimizes the risk of water or sludge inadvertently being shipped to the truck rack

However, there are many concerns with floating suctions and many opportunities for them to fail. Failures typically require the tank to be taken out of service to make repairs. Some of the concerns with floating suctions are as follows:

- Floating suction sinking
- Floating suction damaging the floating roof
- Floating suction coming off the rollers
- Improper style elbow ("Y" preferred vs. 90 degree single elbow)
- Swivel/swing joint failure
- Loss of suction head because of additional pipe length potentially reducing the working capacity of the tank
- Need for proper product gravity calculations for flotation of floating suction (buoyancy).
- Need to recalculate buoyancy and reset pontoons with product changes
- Cost and time needed for installation
- Long lead time on ordering swivels
- Possible alterations to tank shell and possible resulting hydrotest requirements
- Overall increased risks of failures

All aviation tanks that ship product to the rack are required to have floating suctions. Refer to Section 9 for more details.



Floating suction piping equipped with external target indicators must be monitored daily. Failure of a floating suction line may mean the suction line is resting on the tank floor, and all withdrawals are from the floor area. The outgoing stream often picks up sludge, sediment or other contaminants when floating suctions fail (sink).

A "suction trough" is a fixed piece of pipe with an opening towards the top of the tank. This orientation prevents water/sludge being drawn from the bottom of the tank. A suction trough offers many benefits, such as:

- More cost effective installation
- Easy to fabricate and install without special materials, tools or skills
- Minimal time required to fabricate and install
- No calculation for buoyancy with product change
- No moving parts
- No maintenance
- No significant loss in suction head (NPSH) or reduction in tank working capacity
- No target to fail
- Does not interfere w/ IFR operation

Some of the concerns associated with suction troughs are:

- No added benefit for reducing settlement time
- Little experience with use, may have unforeseen drawbacks

Due to the many complications of floating suctions, it has become the preference to install a suction trough on any tanks that do not already have a floating suction.



Beginning in late 2006, any tank without a floating suction must have a suction trough or floating suction installed at its next OOS inspection.

In addition, any tanks that already have a floating suction should be evaluated at the time of OOS inspection to verify whether a suction trough would make more sense for the business.

Considerations include quality issues such as the following:

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- Free water history
- Sediment history
- Entrained water history
- RVP blend down operations
- Shipping and receiving product in the same tank simultaneously

These considerations should be reviewed when evaluating the need for floating suctions versus suction troughs. The one exception is for Jet-A and aviation product tanks, where floating suctions will continue to be the requirement, see Section 9, Aviation Products. Refer to your technical representative for appropriate design of the suction trough.

In addition, to the new suction trough or floating suction installations at the tank's next OOS inspection, the following items must be verified and/or corrected at the next OOS inspection:

- It must be verified that water sumps are located at the places of lowest elevation on the tank bottom. As a tank settles many times the shape of the floor bottom may change and the low points may move. When this happens, the water sump is no longer effective because it is not located where the water naturally collects.
- It must be verified that the there is an ability to gauge the water level accurately. Many times gauge hatches are not located over sumps and datum plates are located higher than the lowest point in the tank and thus water cannot be detected until there is already a significant accumulation of water in the bottom. Water level should be gauged through a hatch that is located directly over 1 or more of the sumps and where a datum plate does not prevent the gauging mechanism from reaching a point level with the top of the sump.

In addition to these physical changes to the tank to protect against water, there are many operational procedures that are necessary to make sure that water does not get into trucks. Some of the procedures are as follows:

- Assuring minimal amount of water in tank bottoms at all times. This minimizes the chances of inadvertently shipping water, reduces product quality issues caused by biological growth, and minimizes tank bottom damage caused by varied forms of corrosion.
- Draining water and verifying before allowing product levels to drop below pan height
- Proper oversight at truck rack during all truck loading when tank is below low leg level, or when receiving into and shipping out of a tank at the same time when product level is low

Please Refer to Section 3.2.6 and 3.7.2 for more specific information on these procedures.

6.3.13 - Diffusers

Diffusers are appurtenances installed in the tank to reduce the velocity of product during receipt therefore minimizing static electricity and preventing tank sediment from being put into suspension. They are designed such that at maximum receipt rate the velocity of the product out of the diffusers will be 3 feet/sec or less.

All tanks that receive product by pipeline, marine or railcars are required to have diffusers.

6.3.14 - Vents and Flame Arrestors

The functions of vents are to eliminate excessive pressure or vacuum in a tank and allow tanks to equalize internal pressure with atmospheric pressure during filling or withdrawing product

Pressure vacuum vents have the following additional functions:

- To reduce the free discharge of vapor that results from wind and fluctuations in temperature, and
- to restrict tank breathing that results from filling the tank.
- to protect stored product quality by retaining the light ends that vaporize most rapidly, thereby avoiding serious drops in quality.
- to retard gum formation.

All fixed roof tanks require a form of venting. Venting gasoline or other volatile products with an RVP above 1.5 psi to atmosphere is not acceptable. Typically, tanks with internal pans will have eyebrow vents to allow venting of air above the pan. Cone roof tanks without pans should have open elbow vents or open elbows unless local regulations require pressure/vacuum vents. Vapor lines and vapor holding tanks are required to have pressure/vacuum vents. Some additive tanks (e.g. Conductivity) will also have pressure/vacuum vents installed to protect the product quality. All vents must be installed with mesh to prevent animal intrusion.

Typically, smaller tanks (e.g. Less than 40,000 gallons) and all horizontal tanks should have emergency vents. To meet API and NFPA requirements, these small tanks do not have the weak shell-to-roof seam that will fail in the event of an internal tank explosion or fire. See you technical resource for more info.

Flame arrestors are devices that prevent flame propagation into the tank through the vent. When used they are mounted between the tank and the vent. See Section 6.10.9 for details on flame arrestors at the rack.



Use flame arrestors on storage tank vents only when a regulatory authority with legal jurisdiction requires this equipment. Company facilities shall not use flame arrestors in the absence of such specific requirements.

Consult with region technical support for assistance with all matters concerning vents and flame arrestors (including sizing).

Inspection of Vents and Flame Arrestor Seals

Visually inspect P/V vents on above-ground tank at least quarterly and other required vents (i.e. eyebrow, elbow, emergency) and flame arrestors at least annually. Cold weather may make more frequent inspections necessary. Moisture from high humidity, rain, sleet or fog can freeze on vent screens at temperatures up to 40°F, due to cooling from air flow.



Review the *Health & Safety Manual* for proper safety procedures associated with walking on tank roofs for the purpose of inspecting pressure vacuum vents.

Vents and flame arrestors must meet the following operational criteria:

- Interior of vents thoroughly clean on pressure and vacuum sides
- Properly seated pallets (if required to have installed)
- Protective screening clean
- Vent hood clean
- Honeycomb bank from flame arrestors clean and dry
- Drain valves operating freely
- Nuts and screws securely fastened

Each terminal is to have a form with all tanks with vents and flame arrestors listed where personnel performing inspection can initial and date form after checking the items listed above.



Tanks with eyebrow vents do not require P/V vent inspections. Pallets should be removed from such P/V vents unless locally required. The eyebrow vents that require inspection can be inspected from ground level.

Repair any defective items at once. Refer to the manufacturer's maintenance and operating instructions. A defective vent valve may cause serious trouble. A vent valve stuck in the closed position may cause tank rupture due to excessive pressure when filling or tank collapse due to vacuum when pumping out of the tank. A vent valve stuck in the open position will release hydrocarbon vapors, greatly increasing risk of vapor ignition.

6.3.15 - Legs on Floating Roofs

Most roof legs are adjustable and can be secured in one of the following two positions.

The normal operating setting allows the floating roof to go down to the lowest level. This level is often called "low leg" position or "low roof" position. The purpose of low roof position is to maximize the storage tank's working capacity. In this position, clearance under the roof usually ranges from 3-4 feet. Roof legs should always be set in low roof position during normal operations.



The low legs setting is determined by the interference with tank appurtenances such as the floating suction, diffusers, temperature probes etc.

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The other position is called "high leg" position or "high roof" position. This setting is used during an out-of-service inspection/maintenance procedure. It allows a worker to go under the roof for maintenance without bending at the waist or crawling on the floor. Normally, the high roof position allows about 6 feet of clearance under the roof.



Check with your Environmental Representative prior to creating any vapor space below the pan (i.e. making any leg setting height change).

Terminals must obtain Head Office management approval before setting a roof on its legs. Contact HS&E Representative for current requirements.

6.3.16 - Mixing Nozzles

Mixing nozzles are appurtenances installed inside the tank. Their primary function is to assist in mixing products that stratify. Mixing nozzles are typically used on gasoline tanks during RVP blend down or tanks into which product is blended.

Mixing nozzles can be installed on the receipt line causing mixing during receipt. Nozzles can also be installed so that the tank pump can be used to recirculate through the mixing nozzles causing turbulence and product mixing. A valve must be installed to allow throttling of the flow through the nozzles.

The horizontal angle of the mixing nozzle needs to be 30-45 degrees from the tank shell for swirling effect. The horizontal direction should be pointed away from other tank appurtenances (e.g. thermowells, ladders, suction line, gauges etc).

The vertical angle of the mixing nozzle is determined by the height of the product when nozzle is used, the height and diameter of the tank and the flowrate and pressure through nozzle. Determining the minimum product level when nozzle is used is critical to prevent roof damage. Consult with technical support for design.

Mixing nozzle details (i.e. nozzle orientation; vertical and horizontal angles) are to be documented in tank files. Mixing nozzles must be identified on the tank with its minimum operating height. Mixing nozzles are required to be locked and tagged out if not in use. Run time of mixing nozzles are site specific and can be determined based on experience and testing. Run time is dependent on pump pressure, flowrate, product volume, product type, mixing nozzle orientation and tank size. Typically, the mixing nozzle, if properly installed, should thoroughly mix a tank in 6 hours or less.

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6.3.17 - Tank High Level Alarms

General

All storage tanks receiving by pipeline or marine will have high-level alarms independent of any tank gauging device to warn of an imminent tank overfill in time to take corrective action to prevent the overfill. The only exceptions are tanks containing nonhydrocarbon, nonhazardous liquids (e.g., clean water).

It is encouraged, but does not require, installation of high-level alarms on tanks with 1,000 gallons or less capacity and tanks in process usage.

Alarms are not indicating devices or operating aids, and plant personnel should not use them for such purposes.

Tanks that can be filled only by tank truck or tank car do not require high-level alarms if the receipt is attended and controls are in place to ensure the receipt will not overflow the tank. Examples include additive and own-consumption tanks.

Requirements for Alarms

The following are requirements for alarms.

- High level alarm systems will have both "high" and "high-high" settings.
 Each setting will have its own distinctly recognizable annunciator. (Single high level alarm systems are acceptable on tanks with capacities of 20,000 gallons or less.)
- Alarms must remain functional, if the floating roof or internal pan sinks.
 Only alarms with displacers (i.e. PVC or porcelain), not weights (i.e. lead), will remain functional if a pan sinks.

If a floating roof or internal pan sinks during a product receipt, the high level alarm will not ring at the set level

(because of the changed activation point on the displacer due to buoyancy and the thickness of the pan). This is considered an acceptable risk. Alarms do not need to be set such that they ring at the calculated level in the event a floater/pan sinks. However, in such an event, the high level alarm (not the high-high level alarm also) must ring before the overfill level. In this case the high level alarm will operate later or higher than normal, but at least it will

operate prior to an overfill. The high-high alarm would be above the overfill and consequently not ring. Consult with



your Technical resource for assistance.

 Annunciators will be located at the tank or another central location so that the alarm will be audible by plant personnel.



Some terminals may have multiple alarms.

- Some locations will also have remote annunciators if the Terminal Manager determines they are necessary to make alarms audible to operators on duty (e.g. At pipeline manifold or on docks).
- Any terminal not manned full-time during receipts must have remote alarms at a manned location to ensure personnel will hear the alarm and take action to prevent an overfill.
- Locations must never intentionally disable or disconnect high-level alarms. The system will remain in active operating status at all times. Exceptions require approval from Head Office management. Routine maintenance does not require approval if it occurs when the terminal is not receiving product and is of short duration.
- High level alarm equipment will not have any bypass switch to turn off the system. The circuit breaker at the main electrical panel is required and allowed, but only to deactivate the system for routine maintenance.
 Management will reinforce this requirement through training and normal supervisory oversight.
- High level alarm systems must include devices providing an audible alarm
 if power failure occurs (i.e. must be wired fail-safe). Region tank
 coordinator will recommend equipment to meet this requirement.

Setting High Alarm Levels

- The overflow level is defined as the level of the tank where product overflow first begins to occur. This level can be found on tank strapping charts.
- Set high-high level alarms to activate at the level where the volume of the tank between the overflow level and the high-high alarm level equals the volume of product entering the tank at maximum fill rate, for a time equivalent to the maximum time it would take for the receipt to shutdown after hearing an alarm PLUS 50 percent (consider this 50 percent safety factor a minimum; the Regional Manager has the authority to decrease it if warranted.). Typically, this is the time it takes for the terminal operator and the pipeline control center to communicate with each other and then for pipeline to shut down their pumps and valves (e.g. around 4-10 minutes).
- Set high alarm levels below high-high levels the same distance as the high-high alarms are set below the overflow level.

Designate the safe fill level as the level where the volume of the tank between
the high alarm and the safe fill level equals the volume calculated above, but
without the 50% safety factor (unless the Region Manager decides a safety factor
is necessary for the safe fill level setting). Use the safe fill level to communicate
the nominal tank capacity to Products Supply Department for determining receipt
volumes.

Refer to Appendix 6.19.10 for Level Setting Calculations Sheets.

 Annually review alarm level calculations to be sure settings are at proper levels according to the Setting High Alarms Levels in this section (i.e. ensure there are no changes to flowrates, reactions times, tank strappings, product changes etc.). If there are changes in levels, high level alarms must be adjusted. Document that the review was completed; it requires two signatures one of which needs to be the Terminal/Complex Manager.

Establishing Low Operating Level

Do not set the floating roof down on the roof legs during normal tank operations. Ensure 3-6 inches of clearance between the bottom of the roof legs and the tank floor. Distribution policy prohibits withdrawing product to create a void space between the roof and product level.

Repeatedly withdrawing product from the tank to the point where the floating roof rests on the roof legs results in accelerated tank deterioration in the following two areas.

The weight of the roof causes the legs to grind into the tank floor, resulting in accelerated corrosion-erosion of the striker plate and/or the floor under the leg. In some instances, a roof leg has actually worn through a ½-inch-thick striker plate and then through the ¼-inch tank floor, resulting in perforation and product release.

The second area of deterioration is the deck of the floating roof. If the floating roof is set on roof legs, the deck plate between the legs is no longer buoyed up by the liquid. Thus, the area of deck plate between the roof legs sags down. Repeated up-and-down flexing of the roof deck will cause fatigue cracks in the deck plate - or more likely -cracked welds. Infrequently, deck perforations have occurred and hydrocarbons have flowed up on the floating roof deck.

Establishing Minimum Fill Level

Establish the "minimum fill level" of the floating roof tank 3-6 inches above the low-roof position. Minimum fill level should be established from the tank's most recent strapping chart. The minimum fill level should be set so that the roof never goes below the critical zone during normal operations.

For tanks without floating roofs, set the "minimum fill level" 6-12 inches above the point where the emptying pump begins to cavitate at the operating flow rate or any higher point Terminal management may designate to avoid pumping out tank bottoms.

Working Capacity

Consider the true working capacity ("working space") as the volume between the "minimum fill level" (determined as described in the previous three items) and the operational fill level.

Note the alarm settings and fill levels on the terminal's tank gauge tables and tank files, and stencil them on the tank in a convenient position. (See Appendix 6.19.15 for tank marking requirements.)

Terminal management will verify settings calculated from the above instructions. Review settings once a year to ensure parameters have not changed (e.g., maximum fill rate, internal tank geometry, maximum fill height, etc.).

Alarm Testing and Alarm Failures

Perform an operations check test within 24 hours before every receipt to ensure operability of the high-level alarm system. Test must include checking operability of high level mechanism on tank, audible tank farm annunciators and remote annunciators (e.g. Pipeline control centers). Document the test was performed. Examples of acceptable documentations are notes and initials in a gauge book or on a product receipt form and automatic annunciator panel print out.

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Perform weekly system checks if frequent receipts or other events (i.e. weekend, holiday, scheduling problems) make an alarm system operational check 24-hour before every receipt impractical. This practice required Area manager approval.

Also, perform high level alarm test at least quarterly on tanks equipped with overfill protection systems. Test more often if necessary to comply with local or state ordinances or with Area or pipeline operating procedures. Test must include checking operability of annunciator panel in addition to those components tested before every receipt. Test each component and record the name of the person who performed the test.

See Appendix 6.19.11 for typical tank alarm testing procedures. However, note that the test is complete when the alarm system functions as outlined in the manufacturer's operating instructions. Consult with the original equipment manufacturer or the Technical Department for detailed instructions on conducting the alarm test. Proceed with the receipt if the system checks properly. Take the following actions if an alarm malfunction is indicated.

- Repair as soon as possible if any part of the alarm system is inoperative.
- Proceed with receipt into an alternate tank if repairs cannot be made before receipt and an alternate tank with a functioning alarm system is available.
- Notify terminal management and all personnel involved with the transfer about the system malfunction if an alternate tank is not available and repairs cannot be made prior to the receipt
- Post a notice of the deficiency at the annunciator panel and have sufficient personnel in attendance during the receipt to allow an operator who can instantaneously initiate any required shutdown to constantly monitor the liquid level using the side gauge. Notify the terminal Manager when putting this contingency procedure into effect.



CAUTION! Verify the operability and accuracy of the sight gauge before the receipt begins. Do not use the tank for this contingency procedure if verification cannot be made. Safety practices do not permit physical gauging of a tank during product receipt.

Alarm System Inspection

Perform the following maintenance inspection annually, in addition to an operational test.

• Open the switch mechanism annually and inspect for moisture, corrosion, cleanliness of contact points, etc. The switch mechanism is located outside the tank vapor space, but accessing it may constitute entry into a confined space (e.g., on external floating roof tanks). Follow proper safe work procedures.

- Include a visual inspection of the internal alarm mechanism (i.e., displacers hanging free, cables/chains not kinked, etc.) where possible without actually entering the tank.
- Thoroughly inspect the internal alarm mechanism (i.e., displacer, cable system, spring system, etc.) and the alarm setting levels when taking a tank out of service for internal work.
- Document inspections and tests in the gauge book (a generic bound record or log) or as otherwise directed and retain in terminal files or on the high-level alarm inspection report form in Appendix 6.19.13.
- See Appendix 6.19.12 for a manufacturer's recommended inspections procedure of a typical high level alarm used.
- · Perform maintenance as required.

6.3.18 - Tank Cleaning And Repairs

Authority and Schedules

Prior to taking a tank out of service:

- make appropriate contacts with Product Scheduling/Supply, Region Manager and others as necessary
- discuss with Project Coordinator to predict all repairs and upgrades and review existing tank files. Local Project Coordinator can use Tank Closure Checklist to assist this discussion (Appendix 6.19.2).
- · obtain permits as required by local and state regulations, and
- give the Supplies Department at least 30 days advance written notice of any proposal to clean or repair storage tanks at marine or pipeline supplied plants (except in emergencies). Include the estimated date for work completion and return to service.
- confirm the exact return-to-service date as soon as possible.

Safety Precautions

Entering and working in confined spaces, especially tank cleaning, presents hazards for terminal operating staff and contract employees.

Consider needs to be given to static generation when appurtenances will be disconnected and tank cleaning inspection process. Consideration also needs to be given to operation of cathodic protection systems. Consult your Health and Safety Representative for the latest requirements.

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Cleaning Procedure

Contact your Health and Safety Representative for current procedures on proper tank cleaning procedures.

Replace all old gaskets before reassembling tank manhole covers, vents and other closure openings.



For proper disposal of sludge and hazardous waste, contact the Residual Management Coordinator.

6.3.19 - Tank Record Keeping

Terminal management will set up and maintain a permanent file for each tank in the terminal. The file must contain all available information since the tank's construction, such as original drawings, modifications, inspections, coatings, maintenance and repair records, etc. Records on the cleaning and inspection of each bulk storage tank must be in these files. This file will become the company tank record file, the file required by API 653 and, where applicable, the file required by DOT.

Send copies of inspection/cleaning/repair records to the local technical support person. Include this information in the tank files:

- Tank Number
- Tank construction records, including the Storage Tank Hydrotest Record (Appendix 6.19.3)
- tank inspection records, including repair recommendations
- repair records



If a repair recommendation is made, a note must be made next to the inspector's recommendation indicating whether or not the repair was completed. This note must be dated and initialed. This documentation is especially important for repairs not easily seen (e.g., inside or under a tank).

- Tank Closure Checklist (if used, Appendix 6.19.2)
- paint and coating records, including exterior paint, interior linings and coating on the underside of a tank floor (if any). Minimum data must include:
 - part of the tank that was painted
 - date
 - anchor profile
 - surface cleanliness (according to standards such as NACE 2 or SSPC SP-5)
 - number of coats
 - product names and numbers of primer and paint, and dry film thickness

Stencil the actual cleaning/inspection date in 2" letters onto the tank shell. Refer to Appendix 6.19.15 for all other tank marking requirements.



Tank cleaning and repairs necessitates preparing a new gauge table (recalculation) if the gauge table was developed before 1965. Tanks may also require restrapping. Refer to *Company Distribution Measurement Policy Manual* and local technical support for guidance.

6.3.20 - Switching Tanks

When considering reallocation of tank storage:

- consult with Head Office Management
- consider economics, supply availability and existing or imminent environmental regulations
- consult with Region management and quality assurance representative to determine if cleaning is necessary before switching products
- consult with region technical support to verify structural and mechanical suitability for service
- consult with region environmental support to determine provisions for proper air emission control.
- ensure flushing of all lines and their appurtenances when switching products.



Use care when changing the type of product in a tank. There can be severe implications in changing a product. Ensure contacting Region technical support to provide assistance.

6.3.21 - Calibration Of Storage Tanks

- Accurate gauge tables are essential to correctly determine tank volumes.
 Preparation of gauge tables must follow the methods and procedures in the applicable API/ASTM Standards.
- Only qualified personnel from industry-recognized tank strapping firms, using sound engineering practices, will compile gauge tables.
- Refer to *Company Distribution Measurement Policy Manual*, for detailed guidelines on calibration of storage tanks.
- The technical support person, in cooperation with Head Office Quality Assurance Measurement and Loss Control Department, will provide guidance.

6.4 - Underground Tanks

6.4.1 - General Policy

Consideration should be given to "daylight" terminal underground storage tanks. Install new underground tanks only with Region management's specific approval and when other alternatives are inappropriate.

Never abandon underground tanks in place. Remove previously abandoned tanks as soon as possible. Region environmental support must approve any exceptions to this policy. Added testing requirements apply when a terminal closes and underground tanks remain on the property. Terminal management should request guidance from region environmental support.

Do not reinstall a used fiberglass tank unless it has been tested to confirm tank integrity and approved for reinstallation by the manufacturer. State or local regulations may require the manufacturer to re-certify the used tank.

Never reuse or reinstall a used steel underground tank. New underground tanks are to be fiberglass.

6.4.2 - Requirements for Underground Tanks

Any tank installed underground will be double-wall fiberglass. Double-wall steel tanks require approval from region technical and environmental support. Fiberglass tanks may require an internal lining for specific product service.

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6.5 - Vapor Control Systems

6.5.1 - General

Distribution terminals are required to have a vapor control system to control the vapors from marine and rack loading. There are two primary types of vapor controls systems.

- 1. Vapor recovery units (VRU) process the collected vapors and returns them to a gasoline storage tank. Vapor recovery units are typically more expensive to install and maintain however since they recover up to 2 gallons for every 1000 gallons loaded, there can be significant financial benefit in installing these systems. A rule of thumb is that if a terminal's throughput is greater than 15-20 MBBL per day a vapor recovery unit is beneficial from an economic perspective.
- 2. Vapor combustion units (VCU) destroy the collected vapor by combustion. Sometimes they require an assist gas to maintain a minimum regulated operating temperatures. They are not as expensive to install and maintain as VRUs. Some vapor products, such as neat Ethanol, have to be processed through a VCU (i.e. not a VRU due to product compatibility).

Either of these units can also be installed in conjunction with a vapor holder to limit the impacts of peak loading periods. See Section 6.5.7.

6.5.2 - VRU/VCU Inspections

The Vapor Control System (i.e., vapor recovery unit, vapor combustion unit, vapor bladder, continuous emissions monitor etc.) must be visually inspected each day for key operating parameters (e.g. temperatures and pressures) by the operators based on the manufacturers recommendations. Local management, assisted by region technical support and the equipment manufacturer are to develop the required inspection and documentation.

Local management and region management shall supplement daily vapor combustion unit (VCU), continuous emissions monitor (CEM) and vapor recovery unit (VRU) inspections with other necessary inspections at appropriate intervals to comply with local and state regulatory requirements or specific equipment operating requirements. Verify and inspect the vapor control unit (VRU/VCU) equipment gauges and thermometers at least once a year to assure readings are correct. This is typically done through the VRU/VCU contractor during servicing; records supplied by the contractor, indicating that work was performed, is adequate.

If any readings are outside the allowed parameters, take immediate corrective action to ensure compliance with regulations and to prevent damage to VRU and/or VCU components.

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6.5.3 - Maintenance of VRU/VCU

Detailed VRU/VCU maintenance instructions are beyond the scope of this manual. See VRU and VCU manufacturers supply instructions for trouble shooting problems and maintenance.

The VRU contractor must perform the following preventative maintenance periodically:

- obtain a sample of the vacuum pump seal fluid
- verify specific gravity and pH are within allowed parameters
- · verify there is no biological activity in the seal fluid
- visually inspect the sample for evidence of carbon, and
- take immediate corrective action to prevent damage to the vacuum pump if any parameters are abnormal.
- Keep the lubricators full (when applicable).
- · Others as manufacturer recommends.

The terminal must provide oversight to assure the VRU contractor is performing the above maintenance activities for their specific units.

Though VCU maintenance is minimal (e.g. pilot adjusted, burner tips cleaned, proper insulation etc.), the terminal still has responsibility to assure the proper inspections and repairs are done in accordance with manufacturers recommendations.

Maintain an inventory of critical spare parts to minimize downtime. The VRU and/or VCU manual normally contains spare parts recommendations. Rely on both previous terminal experience and input from the technician who maintains the unit to make the most appropriate additions to the spare parts inventory. Many parts are interchangeable therefore, neighboring terminals can sometime provide spare parts in an emergency. Periodic efficiency testing may be required as a condition of your local permit. If no efficiency testing is required by the permit, the company may choose to perform internal periodic efficiency testing to help ensure proper operating performance. Contact your Environmental Representative to obtain procedure, documentation and frequency of test.



Regulatory agencies will issue permits for vapor recovery units and vapor combustor units. These permits set forth reporting and operating parameters.

Periodically check all emergency shutdowns by actually creating the shutdown situations. Tripping a switch by hand is not a complete test. Records supplied by the contractor indicating that the VRU/VCU shutdown, is adequate. The equipment manufacturer's instructions specifically explain how, and how often, to check emergency shutdowns.



Retain a log of all malfunction shutdowns, along with a record of corrective actions.

Allow only authorized personnel to restart a vapor recovery unit or a vapor combustor unit. Post a VRU/VCU Shutdown Alarm Response Procedure. See Appendix 6.18.14.

6.5.4 - VRU/VCU Maintenance Contractor

Every terminal needs the services of a skilled technician for specialized VRU/VCU work. In addition to correcting failures, the technician provides a valuable service by performing thorough quarterly, semiannual and annual preventive maintenance inspections of the VRU and semiannual preventative maintenance inspections of the VCU. This skilled technician is typically a contractor who represents and is well trained in the specific piece of equipment.

6.5.5 - VRU/VCU Shutdown Alarm Response

Safety/Environmental Precautions

EPA clean air regulations set limits on terminal vapor emissions, depending on local ambient air quality standards.

Terminals must shut down operations that cause vapor release into the atmosphere when the Vapor Control System is not working. Consult with your environmental rep to discuss alternatives to continue operations.

Terminals equipped with TMS (Terminal Management System) can control loading rack volume throughput according to applicable federal, state and local regulations. Locations can set a predefined volume threshold for TMS-controlled meters for a 24-hour period. When the meter reaches the threshold, TMS will deny loading rack access until the next 24-hour period begins. See the applicable TMS Guide for operating details.

Training and Documentation Requirements

Train all terminal personnel who may respond to a VRU/VCU shutdown alarm on the proper procedures.



Fill out a VRU/VCU Shutdown Response Procedure form, in Appendix 6.19.14, with names and phone numbers to call if a VRU/VCU shutdown occurs.

Place the completed form in a clear weatherproof cover and post it in visible location near the VRU/VCU control panel.

Update the posting whenever names and telephone numbers change.

Procedure When Responding to VRU/VCU Shutdown Alarm

The following are steps for responding to a VRU/VCU shutdown alarm.

Push the "alarm reset" button to turn off the alarm.

Log this event for future troubleshooting purposes.

Do not try to restart the unit unless you have authorization. (Assure restarts are done according to manufacturers recommendations.)

Call a supervisor, or terminal operator or other authorized personnel.



VRUs and VCUs with an annunciator display will indicate the cause when shutdown occurs. Be sure to correct the cause of failure before resetting and restarting. Restarting the unit before repair may cause damage to the equipment, such as damage to the vacuum pump if it does not have seal liquid flow.

6.5.6 - Vapor Lines

The following requirements are applicable to vapor lines.

- Ensure all vapor lines have a slight slope to a low point to allow removal of condensate.
- Check vapor line supports periodically for alignment and reset to proper elevations to avoid low places or deflection in the lines. (Condensate can accumulate in low places and corrode the thin wall pipe.)
- Drain the condensate line weekly or as needed to prevent forming a liquid seal in the vapor line or restricting the vapor flow.
- Occasionally insert a non-metallic rod through the condensate drain line all the way into the vapor line to ensure the drain is not obstructed by rust gathering over the outlet in the pipe.
- Vapors lines have installed PV vents to prevent overpressure. These vents are to be included in the Tank Vent and Flame Arrestor inspection or as other local permit conditions require. See Section 6.3.14.

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6.5.7 - Vapor Holder

The vapor holder is a very important component in some recovery systems. It eliminates breathing losses, evens peak loadings and provides a dependable, flexible way to control vapor system loading.

These tanks may not be designed for product storage beyond residual condensate. Do not fill these tanks with product unless you are positive they are suited for product storage. (Consult with your technical resource). However, they are to be inspected using API 653 guidelines and on a similar cycle as your other API 653 tanks. Vapor holders require little maintenance beyond periodic checking for leaks in the diaphragm. Some vapor holders store saturated vapor and may accumulate condensate, which is mostly hydrocarbon. Drain as necessary and salvage the condensate.

The following is a procedure for leak checks.

- Check the vapor space over the diaphragm at least quarterly, using an explosimeter
- Be sure the check is made from the top access vent/hatch when the diaphragm is under pressure, and about one-half to two-thirds inflated. Sampling may also be done at the equator scupper drain holes if additional verification is desired.
- Extend the explosimeter sampling probe to within a few feet above the stabilizer weight (dollar plate) or diaphragm.
- Check the explosimeter scale. A reading below 20% LEL is acceptable.
 However, readings are typically less than 10%. Routine reading above
 10% must be investigated. Consult with your technical and environmental
 representatives. Vapors holders have installed PV vents below the
 bladder to prevent overpressure. These vents are to be included in the
 Tank Vent and Flame Arrestor inspection or other frequency to meet local
 permit conditions. See section 6.3.14.

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6.6 - Corrosion Protection

6.6.1 - Cathodic Protection

Storage tank bottoms and underground piping must receive continuous protection from an impressed current or sacrificial anode cathodic protection system, to guard against external corrosion from soil conditions or stray currents.

The rectifiers can create a potential that can cause arcing when disconnecting equipment. Consult your local health and safety representative for special procedures. Keep rectifiers on at all other times.

Terminal personnel must inspect and record the date, rectifier volts, soil conditions (dry, wet, etc.) and amp reading on impressed current cathodic protection systems monthly. Tide levels must also be recorded at coastal locations since tide level may affect rectifier output. Region technical support and region management must be notified if the rectifier reading varies from an average of the preceding six months readings.

Region technical support will arrange an annual inspection of cathodic protection systems performed by certified corrosion professional technician at distribution terminals. Terminal management will receive notice of the scheduled inspection date.

6.6.2 - Painting and Coating

Appendix 6.18.15 provides guidelines for protection against atmospheric corrosion by painting aboveground piping, tanks and other equipment. Painting of tanks, pipes, etc. is not an aesthetic procedure. It is important to keep the coatings in serviceable condition to prevent more costly complete repaints in the future. All paint and coatings are to be coordinated with your local technical resource to ensure proper procedures, current specs, and material compatibility can be assured.

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6.7 - Dikes and Drains

6.7.1 - General Policy

The following requirements are applicable to dike drains and the release of storm water.

- Each terminal must have a written operating procedure to manage storm water released from an outfall location. (i.e., visually inspecting water for evidence of oil sheen or contamination, testing of water quality if required, closing roof drain valves, conducting surveillance and documenting release, etc.). The plan must include the following.
- Establish a system of quick and easy visual indications of a dike and roof drain valve's status (open or closed) in the field and control center.
- Operators must visually inspect dike drain valves status (open or closed) daily and document on daily walk through checklist.
- Quarterly, operators must physically operate dike drain valves to ensure they work as designed. This must be documented.
- Close external floating roof drain valves before opening dike drains and keep roof drain valves closed during the entire time dike valves are open.
- A log must be maintained to include the time the dike drain was opened, who is responsible and the time it was closed. If person responsible is changed, log must be amended.
- The procedure must include a requirement that an operator be on site while water draining is going on, and that the activity must stop if the operator leaves the premises.
- The operator must visually inspect each outfall location, once every hour if operations allows or at least every 3 hours, during the draining procedure.
- The operating procedure must provide for dike drain valves to remain in the closed and locked position at all times, except when draining water from the diked area.
- Terminals must not drain dikes during product receipt, except during emergency situations such as during periods of heavy rainfall and only with verbal Local Management approval.
- Personnel involved with tank farm drainage activities must receive initial and annual refresher SPCC training. This training must be documented.
- Refer to your National Pollution Discharge Elimination System (NPDES) and/or Storm Water Pollution Prevention Plan (SWPPP) permit to ensure all requirements are being met.

6.7.2 - Spill Prevention, Control and Countermeasure Plan (SPCC)

The SPCC plan is the document that identifies preventative equipment, measures, controls, and countermeasures to address potential releases that may occur at a distribution terminal. The SPCC plan requires daily (when normally staffed) facility inspection to ensure primary containments (i.e. tanks, pipes, pumps, etc.) and secondary containments (i.e. dike walls, OWS systems, strip drains, etc.) are properly maintained and operating as designed and to identify any potential releases. These inspection requirements must be integrated into the daily walk through checklist. Refer to Annex 7 of the Integrated Contingency Plan (ICP) for details.

Secondary containment is required as an integral part of identified SPCC measures. A survey of tank dike capacity is required to be available onsite. Dike capacity can diminish over time due to settlement, wind and rain erosion, and wear from vehicle and pedestrian traffic. Dike containment should be periodically checked. If there is reason to suspect that the dike capacity is insufficient, consult with your Technical Rep. or your SPCC support personnel to determine whether a survey should be conducted to measure dike capacity around the tank(s) affected by the change.

Amendments should be made to the SPCC Plan for your facility in accordance with the general requirements in CFR 40, Part 112, and with any specific section of this part applicable to your facility.

Regular reviews of the SPCC plan must be conducted as follows:

- Annually, Local Management must ensure personnel SPCC plan training is completed.
- A least once every five years Local Management must complete a review and evaluation of the SPCC Plan, including the dike containment capacity; if your facility was in operation on or before August 16, 2002, a review must be conducted five years from the date your last review was required.



Unless there has been a material change to the terminal, a re-certification by a professional engineer is not necessary at the time of the 5 year review/evaluation

• When there is a change in the facility design, construction, operation, or maintenance that materially affects its potential for a discharge, the amendment must be prepared within 6 months by Local Management, and implemented as soon as possible, but not later than 6 months following the preparation of the amendment. Examples of changes that may require amendment of the SPCC Plan include, but are not limited to: commissioning or decommissioning containers; replacement, reconstruction, or movement of containers; reconstruction, replacement, or installation of piping systems; construction or demolition that might alter secondary containment structures; changes of product or service; or revision of standard operation or maintenance procedures at a facility.

Refer to Annex 7 of the Integrated Contingency Plan (ICP) for details.

 Consult with your HS&E representative for any questions related to the SPCC plan.

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6.8 - Product Piping Systems

6.8.1 - General

The following are general requirements for product piping systems.

- Region technical support will provide assistance with design and construction of piping systems, especially relief valves.
- Install new or replacement product piping above ground with proper supports and anchors. Locations may consider underground replacement or installation if there are compelling reasons to do so.
- Consider "day lighting" (bringing above ground) existing underground piping systems whenever maintenance or project work provides an appropriate opportunity. Unless mandated by regulations, base the decision to daylight on cost, condition of line and risk (i.e., will a needed and significantly lowered environmental risk justify the cost?). Work closely with Region management and region technical support to make these decisions.
- When "day lighting" underground piping systems, pay attention to proper disposal of the equipment being replaced (e.g., whether it can be purged and abandoned in place, or must be removed).
- Ensure product pressure-relief systems provide for temperature-induced product expansion around valves and pumps. Relief valve settings normally should be slightly higher than the pump's deadhead pressure on the discharge side of the pump.
- Consult with region technical support to ensure that pressure relief on tanks, lines or any other hardware meet all safety and design requirements.



Extreme care must be taken when installing relief valves in series if at all avoidable. If it must be done, adjustments to relief settings must be made.

6.8.2 - Clearing Product Lines

Clearing lines is the removal of product prior to conducting work. Typically the first option is to drain the product from the lines by gravity and by using a vacuum truck. Other options include pigging the line or blowing the line with nitrogen. Local operations, in conjunction with technical and HS&E representative, will determine which procedure is the best option.

Once the line is cleared the necessary work will dictate additional activities and precautions (i.e. hotwork and coldwork). Consult with your safety representative and technical resource to understand all additional requirements for the necessary work.

Never use compressed air to clear lines.

When reallocating a line (that needs no welding), flush the line with the new product until the line conforms to new product specifications. Prior to undertaking this action, consult with your QA representative, technical resource, Health and Safety, and Environmental representatives.

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6.8.3 - Filters

Follow the instructions on filtration of aviation products in Section 9, Aviation. Filters may be necessary if local conditions do not allow settling time for incoming receipts of motor gasoline. Filters may be necessary to remove abrasive or harmful material (e.g., particles, rust, rouge) that could get into the product during transportation handling. Never ship dirty product.

If installation of non-aviation filters is necessary, develop local operating maintenance and inspection procedures with assistance from environmental and technical representatives.

Refer to Section 6.10.8 for Strainers.

6.8.4 - Product Piping Inspections

All Terminals must periodically ensure the integrity of existing product piping. This section provides minimum requirements to ensure integrity. Local management or region management may take additional measures, with support from region technical support.

Requirements in this section are not intended to contradict regulatory requirements. Regulations will take precedence if any apparent conflict arises. Terminal management must communicate such conflicts to region management

Guidelines for Coastguard Piping

Annually test all piping that meets the U.S. Coast Guard's definition of *oil transfer pipe system*. Locations may consider an API 570 inspection in lieu of annual hydrotest. Consult with your region technical support.



Local agency inspection/testing requirements supercede the guidelines in this document.



The Coast Guard defines *oil transfer pipe system* as one that extends from the last valve inside the EPA-required containment, through the transfer pipe, and to the dock loading arm or vessel manifold.

General Guidelines (Aboveground and Underground Piping)

Terminals must request region technical support to inspect any line in which the integrity is suspect.

Document the inspection and all repairs or modifications to product piping systems or coating on Pipe and Crossing Report, Appendix 6.19.18.

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Guidelines for Underground Piping

For offsite underground lines, that are owned/maintained by the company, visual surveys of surface conditions (i.e. any soil staining, pipe markers present and maintained, area above pipes clear of vegetation and debris, etc.) along and adjacent to offsite pipeline routes servicing the Terminal should be conducted. These visual surveys should be completed twice a year at approximately 6-month intervals. Local Terminal personnel are responsible for completing and documenting the visual inspection on the Underground Pipeline Easement and Surface Inspection Form, Appendix 6.19.27.



Oversight of surface conditions along and adjacent to onsite underground lines is covered during daily walkthrough.

In addition, for all offsite underground lines, that are owned/maintained by the company, perform an API 570 inspection by January 1, 2006 and establish an inspection interval. This inspection will be coordinated by your technical resource. The report must be retained at the Terminal in order to perform any additional inspections (if needed), to identify the next inspection cycle, and to be used as a reference during the next inspection. Terminal Management must work with Technical Rep. to establish the next inspection date.

For onsite underground lines, specific line visual inspections are not required, as this inspection should be covered under the routine ICP/SPCC Plan Inspections. In addition, for all onsite underground lines, perform an API 570 inspection by December 31, 2008 and establish an inspection interval. This inspection will be coordinated by your technical resource. The report must be retained at the Terminal in order to perform any additional inspections (if needed), to identify the next inspection cycle, and to be used as a reference during the next inspection. Terminal Management must work with Technical Rep. to establish the next inspection date.

Inspect pipe and coating for signs of corrosion or coating deterioration when exposing



Annually, local Terminal management is to discuss and strategize onsite and offsite underground pipeline inspections to occur in the next 12 to 18 months with their project coordinator (during this session, dock inspections and API 653 Inspections for tanks should be discussed – Reference Sections 6.3.6 and 6.11.3). Local Terminal management will also coordinate all downtime activities with Supply. Consideration must be taken for peak demand periods.

underground piping for any reason. Document findings on Piping and Crossing Report, Appendix 6.19.18. Contact your technical resource or a qualified contractor if needed. If locations are known, evaluate underground piping segments that could trap water (e.g., dead legs, sags) to determine whether internal corrosion is present. When practical, remove such segments.

Inspect cathodic protection systems monthly and annually according to Section 6.6.1.

The following additional inspection measures may also be considered:

- API 570 inspection
- pressure testing
- acoustic testing
- selective excavation and inspection
- ground penetrating radar
- tracer testing
- internal inspection via instrument (e.g., smart pigs)
- close interval survey
- guided wave

Consult with region technical support for guidance to choose the appropriate option.

Guidelines for Aboveground Piping

Visually inspect aboveground piping during daily walk-though inspections. Conduct a detailed visual inspection annually to investigate pipe integrity. Qualified terminal personnel or qualified contractors are to complete this inspection. The annual inspection must include, but not be limited to, these areas:

- outside of pipe, painting/coating systems and associated hardware (i.e., supports, hangars, valves, pressure-relief valves, etc.)
- signs of misalignment, vibration and leakage
- underside of pipe, especially support contact points
 Extensive corrosion and pitting may develop in this area due to moisture condensation on the pipe surface.



Hand scraping or wire brushing may be necessary to determine the extent of corrosion.

transition zone from aboveground to underground piping (soil/air interface)

The transition zone extends from approximately 12 inches below to 6 inches above the ground surface (API-570). Cathodic protection is often ineffective in the transition zone, and coating damage is common due to grounds-keeping activities, soil movement and thermal expansion/contraction of the pipe. The zone includes piping running parallel and making contact with the soil.

Inspect the aboveground portion of the transition zone coating. Repair or replace coating that is damaged or disbonded (e.g., sagging, blistered). Inspect the pipe for corrosion before repairing or replacing the coating.

If a transition zone coating was not previously installed, excavate the transition zone and inspect pipe for corrosion. Apply a transition zone coating before backfilling.

Consult with region technical support for guidance on selecting and applying an appropriate transition zone coating.

 piping supported by pipe supports of non point-to-point style (pipe saddles)

This support will trap water against the pipe. Inspection may require lifting the pipe clear of the support and then cleaning to determine presence and extent of corrosion. Results may suggest changing the pipe support design.

piping covered by insulation

Corrosion can occur unobserved when water gets under insulation. Remove insulation if the caulking has failed or there are signs of swelling under the insulation. Inspect the pipe and then install new insulation.

dead legs

Extensive corrosion may develop in this kind of piping configuration due to trapped water and sediment. Remove dead legs whenever practical. If removal is impractical, consider draining the trapped water and sediment from a low point drain periodically.



Results must be documented and communicated with technical resource for additional inspection and/or repairs.

Local management or technical resource may also take the additional inspection measures listed below:

- pressure testing (using liquid only)
- ultrasonic wall thickness testing
- magnetic flux exclusion testing, and
- internal inspection via instruments.



Consult with region technical support for guidance to choose the appropriate option.

Drain Piping

Consider pressure testing of gravity drain piping periodically. A stand pipe test is recommended for these low pressure lines.



Review construction standard on drain piping. Some older drain lines might be constructed of clay.

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Relief Valves

Ensure product pressure-relief systems provide for temperature-induced product expansion around valves and pumps. Relief valve settings normally should be slightly higher than the pump's deadhead pressure on the discharge side of the pump.



Extreme care must be taken when installing relief valves in series. If it must be done, adjustments to relief settings must be made.

The following requirements are applicable to relief valves.

- Pipeline relief valves within the terminal must be tested annually.
- Thermal relief valves, at a minimum, must be tested every 2 years.
- Relief valves on the pumps must be reviewed if they are relieving frequently.

Consult with region technical support to ensure that pressure relief on tanks, lines or any other hardware meet all safety and design requirements.

6.9 - Temperature and Gauging Devices

Refer to *Distribution Measurement Policy Manual*, for temperature and gauging device guidelines including calibration requirements.

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6.10 - Loading Racks

6.10.1 - General

Loading rack facilities are best observed while a vehicle is being loaded. The mechanical components of Product Distribution loading racks provide for safe and environmentally sound product transfer when used according to established procedures. The prevention of fire and explosion from electrostatic sparking and the prevention of truck or rail tank overfill must be primary considerations in the loading process.

This section provides details about components common to most loading racks.

6.10.2 - Meters

The following are the types of meters found at loading racks:

- turbine meters
- positive displacement meters

Refer to the *Company Distribution Measurement Policy Manual* for prover calibration frequency and procedures.

6.10.3 - Meter Pre-sets

When a driver gains authorization to load, the preset allows the driver to input the desired amount of product to be loaded into the compartment. The preset communicates with the flow control valve to adjust the flow at established rates. As the preset volume nears completion, the preset signals the flow to decrease and eventually stop the product flow.

There are two primary types of meter pre-sets used:

- Mechanical Mechanical pre-sets are an older version of what is currently being used. They operate through gears and are primarily mechanical in design and operation. Mechanical pre-sets are being removed from service as equipment upgrades are made at the terminals or when reliability and maintenance costs become excessive.
- Electronic Electronic pre-sets perform the same function as mechanical presets, however they are much more reliable, accurate, and have more functionality. As such, electronic pre-sets are used exclusively when upgrades are made. There are several different manufacturers of these units, however the current trend is to upgrade to TopTech Multiload systems. These are 100% compatible with the TopTech systems currently in use.

6.10.4 - Control Valves

General Operating Requirements

Control valves control product flow through the meter and into the truck compartment. Control valves are the primary piece of equipment that controls the flow during start-up, normal loading, and shutdown. Without a properly functioning and adjusted control valve the risk of truck overfill increases and product measurement will not be as accurate.

There are typically two types of valves currently being used throughout the Terminals, the Smith Meter Model 210 control valve and the Brooks Model 788 digital control valve. The Smith valve is a diaphragm operated flow control valve. The Brooks valve operates on a balanced piston principal. Each valve functions to control total flow rate as well as how quickly it reacts to change the desired rate of flow. If a different type of control valve is currently in use, please consult your technical resource for guidance.

Control Valve Adjustment

The following requirements are applicable to control valves.

- Program flow-control valves to initiate product flow at a slow-fill rate (typically 120 gpm) before opening valves to high-flow conditions.
- Never allow high-flow rates to exceed 600 gpm or the meter's rated capacity, which is stamped on the meter's information plate, whichever flow rate is lower.
- Set the flow control valves to gradually reduce flow rate down to the point of shutoff when the compartment is within 50 to 75 gallons of the set amount. This gradual reduction will avoid sudden valve closure and line shock.
- Adjust flow control valves so flow at the high rate will stop in 1 1/2 to 2 seconds. These times correspond to 15 to 20 gallons at a flow rate of 600 gpm. This setting will prevent truck compartment overfills when the valves are properly adjusted and truck compartment freeboard is sufficient.
- Be sure to set the trailer compartment sensor at an elevation that allows enough compartment freeboard to accept 15 to 20 gallons during valve shutdown. (Allow freeboard of 3 percent of compartment size.) The sensor setting is critical because trailer compartment sensors signal the flow control valve to close.

Typically start-up and shutdown parameters which control valves are adjusted for are detailed below. Refer to manufacturer's literature or contact your technical resource for adjustment procedure.

Typical Start-Up Cycle:

<u>Gasoline:</u> First stage start up - slow flow. 120 gpm for 15 seconds (3 fps in a 4" line) <u>Distillate:</u> First stage start up - slow flow. 120 gpm for 360 gallons (3 fps in a 4" line until the fill line outlet and deflector, when provided, is submerged by at least two fill line diameters inside the truck compartment.)



Distillates have a more conservative (longer) start up time due to static generation concerns. Refer to Switch Loading

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Operations Procedure to determine if a less stringent submergence requirement is allowable in your locations.

Maximum loading rate

600 gpm (maximum flow rate)

Typical Shut-Down Cycle:

Maximum full flow

600 gpm

First stage shutdown

60 gpm for last 50 gallons of pre set volume If your Terminal equipment has the ability for a second stage start up or shut down,

consult with your technical resource for intermediate settings.

Control Valve Inspections

Visual inspection of each control valve must be conducted at least guarterly. This inspection must be a sight, sound inspection observing for erratic operations, specified flows, etc.

Full detailed inspection of control valves by full disassembly is based upon usage. This includes inspection of all components, repair as necessary and recalibrate all settings. All control valves must undergo a full inspection every 766,500,000 gallons or 5 years whichever comes first. (The inspection cycle is based upon 10MB/D every day for 5 years or a maximum interval of 5 years. It is doubtful that any riser loads at the 10MBD rate, therefore, the five year cycle is the typical inspection cycle. This equates to 766,000,000 gallons or 18,250,000 barrels). Documentation to track which valves were inspected and when should be locally developed.

6.10.5 - Vapor Hoses

Vapor hoses are used to transfer vapor from a truck to the terminals vapor collection system during truck loading.

The following requirements are applicable to vapor hoses:

- Ensure vapor hoses are equipped with a check valve or that there is a check valve at the rack to prevent backflow of hydrocarbon vapors to the atmosphere. The check valve should be quick-acting, requiring minimal force to open it. A low pressure drop is another important design factor in the overall vapor processing system.
- The hose is to be equipped with a bonding wire to assure electrical continuity between the truck and the loading rack.
- Store the hose when not in use to keep vehicles from running over it and to prevent tripping hazards.

Follow inspection and testing guidelines for product transfer hoses according to Hose Testing Schedule - Terminal Gravity (all products) in Appendix 6.19.9.

6.10.6 - Additive and Dye Injection

Terminals must have procedures in place to effectively monitor additive and dye injection daily. TMS (Terminal Management System) provides data and reports to assist with this function. But these reports should not be relied upon exclusively. In addition to utilizing TMS reports and controls, terminal processes must include other means of independently verifying additive injection compliance including:

- comparing additive meter readings with product meter readings at the close of each folio to verify injection rates
- comparing the additive physical inventory change with product meter readings/throughputs to verify injection rates
- closely monitoring additive inventory loss/gain for significant variations and/or consistent patterns of gains (may indicate under-injection) or losses (may indicate over-injection), and
- performing routine operational checks on the injection equipment such as listening for the clicking of the piston as it moves in the injector and watching the movement of the display on the additive injection meter; and recalibrating meters as required.

At Terminals where TMS uses Hi-level communication to monitor loading rack meter shut down in case of failure (Multi-load, Electronic Presets, Opto-Panel, Smart Injector Titan, Mini-Pak, Blend-Pak), each month the Terminal must review the Meter Profile in TMS for each meter to assure the **Feedback Flag** indicator "P", "O", or "S" is enabled. **Note:** If the **Feedback Flag** indicator is an "N", the Hi-level communication is disabled and/or unavailable. At Terminals where TMS does not control and monitor additive injection, either PLC or multi-load will serve as an acceptable alternative system for shutting down a loading arm in case of injector failure.

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The review must be documented in InControl.

Refer to Section 9.0 of the Company Distribution Measurement Policy Manual for guidance on additive systems calibration.

6.10.7 - Rack Isolation Valves

Each lane must be equipped with quick-closing isolation valves on each riser to shut off flow to the loading arms. These valves shut off product flow if any part of a single loading riser fails. The valves can be manually operated, but must be easily accessible in an emergency. These valves must be fully closed and opened at least annually to assure they will operate properly when needed.

Install shutoff valves on each product line feeding a truck rack. These valves assist with shutdown if a major loading rack failure occurs. Establish a regular maintenance inspection program for operability of isolation valves. This can be performed during rack maintenance.

Make sure all rack isolation valves are clearly identified as to location and product. Truck Operators should be shown the locations and purpose for the valves.

6.10.8 - Strainers

The purpose of the strainer is to remove residual particulate, welding slag, scale, sediment and other debris from reaching the meter, control valve mechanism or control valve orifices, which in turn may prevent the system from operating as designed. Typically, debris may prevent the control valve from operating properly and may prevent closure when required.

Strainer mesh should be 80 mesh wire baskets for gasoline and 40 mesh wire baskets for diesels and jet fuel. No mesh finer than 40 mesh should be used for distillates, due to the restriction of flow and thus increased risk of static generation in the line. Dual basket strainers can also be used; i.e. 10/80 mesh for increased strength and is particularly helpful when used in conjunction with turbine meters.

Inspect the mesh strainer baskets located immediately upstream of the meter for these defects:

- Mesh and basket deterioration or damage
- holes in the mesh, and
- debris clogging the screen.
- Improper seat that would allow debris to bypass the strainer basket.

Perform this inspection annually or more frequently if locally required. Indications of clogged strainers could be a reduced flow. More frequent monitoring is required when maintenance/welding has taken place on a line.

Take precautionary measures to avoid inhaling gasoline vapors or spilling product when opening lines and inspecting strainers.

6.10.9 - Flame and Detonation Arrestors

Flame/Detonation arrestors are devices that prevent flame propagation through the line. Flame/Detonation arrestors are typically located in the vapor line at each lane or on the vapor header. See Section 6.3.14 on flame arrestors on tanks.

Annually check the loading rack flame arrestors by measuring and recording the backpressure at the loading rack or some other point upstream of the flame arrestor. Clean the flame arrestor if backpressure is excessive or has increased significantly since the last backpressure check. If the backpressure is approaching 18 inches of water, consult with region technical support. Locally developed forms are acceptable.

6.10.10 - Drains and Oil Water Separator

Since systems will vary by locations, specific inspection and maintenance requirements for each system and component will need to be identified. Contact your technical support to assist in identifying these specific requirements. Typical requirements are listed below:

- Monthly inspect the separators for general appearances and operations. (Leaks, odors, unusual noises, valves, pumps and alarms properly working).
- If aboveground, annually inspect the exterior for possible rust, corrosion and paint deterioration. When the OWS is emptied (e.g. during cleaning), inspect the interior for possible rust, corrosion and lining deterioration. For technical assistance, contact your Project Coordinator.
- Maintain the operating water level at full in the separator. The level is established by the invert of the outlet pipe.
- Solids will collect in the Interceptor/Distribution chamber. Sludge should be removed every six months or as required by the individual site condition. Periodically clean collection points and strip drains. (Take opportunities such as tank cleaning if being performed)
- Be sure the oil level is checked and removed when it reaches the removal volume recommended by the manufacture. If a skimmer is used, be sure it is operating properly and the drain is free from obstructions.
- Always refill the separator with clean water each time oil or sludge is removed. If
 it is removed automatically the separator should recharge itself and maintain the
 proper operating water level. (Fill from the discharge side).
- If the separator has internal plates or packs, they must be inspected at a minimum once a year for blockage or film and sludge build up. Use a wand inserted between the plates to fully clean, then visually check the plates for cleanliness and damage before putting back into service.

- It is very important to check your separator and all components after a storm
 events that causes flooding conditions and/or wash out the system piping, oil
 spills, and any unusual events that may cause the build up of sludge or debris in
 the system.
- Periodically check the separator to maintain a level elevation of the housing to assure the separator has not settled. This could cause separator failure or improper oil removal.
- Make sure flow control device (Orifice) is working properly. An inlet valves should be used to control flow if an orifice is not used.
- If possible check strip drains before thunderstorms.

Appendix 6.19.5 provides a guide in establishing a schedule and documenting the inspection and maintenance on an Oil Water Separator. An alternative form can be created specific to that location.

6.10.11 - Dry-break Connectors

Liquid and vapor dry-break couplers connected to truck must not show evidence of excessive drips or leaks.

6.10.12 - Terminal Management System (TMS)

TMS is a computer-based system that controls terminal security and loading access and provides product accounting detail.

Refer to the *TMS Manual* and the *TMS Stock Accounting Manual* for operating details about TMS..

6.10.13 - Emergency Shutdown Systems

All emergency shutdown systems must be kept operational. Three types of emergency system shutdowns exist; a single arm shut down, a single lane shut down and full rack shut down, i.e.: ALL loading lanes and positions. Once any of the emergency shutdowns is activated, the corresponding flows should completely stop within 2-3 seconds. Each type of emergency shutdown must be tested at least annually under normal operating conditions. By testing under normal operating conditions, assurance is obtained that the entire system, including components will work as designed. Documentation to track which ESD systems were tested and when should be locally developed.

During shut down events the VRU/VCU should continue to operate as determined by the Terminal Management and technical resource to process residual vapors and prevent excess emissions from entering the atmosphere. Do not make any changes to the process you are currently using concerning VRU/VCU shutdown operation until you have consulted with your technical resource.

Emergency Loading Arm Shutdown

This is a manual shutdown activated by depressing a button on the preset, which controls a specific loading arm. Once activated, flow through the loading arm should completely stop within 2 – 3 seconds. Activation testing should occur for each loading arm on an annual basis.

Emergency Lane Shutdown

The lane emergency shutdown occurs when product activates a overfill probe, if any of the overfill or bonding systems are disconnected or a fault occurs. The overfill protection

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system should signal closure of the control valve within a half second from the time the overfill probe is activated. Once activated, flow for the entire lane should completely stop within 2 – 3 seconds at maximum flow rate. Activation testing should occur for each loading lane on an annual basis. This can be done by disconnecting the high level and or bonding plug.

A 'Lane Stop' (vs. a rack Emergency Shutdown) button may exist (typically with Multiload presets). If this button is depressed, all permissive to allow loading will drop to the presets and the entire lane will stop.

Emergency Rack Shutdown

This shutdown is manually activated by depressing the "Emergency Shutdown" button on any lane in the event that protection of health, safety or environment is necessary or when other shut down systems fail. This shutdown should be installed such that when activated, all control valves should close, all rack pumps should stop immediately, all loading activities should cease until the problem is resolved and loading operations are approved for resumption. Once activated, flow to the all-loading arms should completely stop within 2–3 seconds. Activation testing of an emergency shutdown should occur on a particular lane under full flow conditions. The other lanes can be done without flow and verify that the gates, open, pumps turn off. The full activation testing should be done on a rotating basis to assure all lanes are fully tested (i.e. for a three lane rack, each lane is tested every three year).

6.10.14 - Rack Security

Refer to Section 6.14 for loading rack equipment sealing requirements. Rack sealing requirements are in place to prevent product theft. They must be installed at any location at the rack area where product can be drained or in the metering system where meter pulses/indications could be interrupted. Flange bolts do not require such sealing. Terminal Management System (TMS) controls access to the loading rack by validating equipment and driver/operator. TMS records all system-controlled rack transactions and system function access in an activity log for review.

6.10.15 - Bonding/Grounding

Bonding is the process that allows two pieces of equipment to carry the same electrical charge. Grounding is the process that ensures there is no electrical charge on a piece of equipment (i.e. the same charge as earth).

Trucks and trailers must be electrically bonded to the loading rack before loading to assure that no static electricity is created. The rack structure itself requires proper grounding to avoid stray electricity hazards.

The stand alone bond cables (if present) and those in the loading arms, vapor hoses, and truck overfill systems provide bonding at bottom-loading racks. Note that the bond cable in loading arms supply adequate bonding alone. Use a separate bonding cable at top-loading racks.

Use an ohm meter to check the loading rack bonding system every 6 months. Check by taking a resistance reading between the fixed pipe upstream of the loading arm and a vehicle while loading. Note a clean (i.e. free of oxidation, paint and rust) contact is needed for a good reading. The reading should be 5 ohms or lower. A resistance higher than 5 ohms may indicate a poor bond. A poor bond could be a result of a broken bond wire and/or worn couplers or swivels on loading arms.

6.10.16 - Delivery Vehicles Inspections

All terminals with fleet delivery vehicles, refer to *Company Fleet Operations Policies and Procedures Manual* for current policies. All other policies pertaining to common carrier delivery vehicles are in Section 10 of this Plant Manual. Drivers on each shift must make pre- and post-trip inspections of the vehicle they will operate (Department of Transportation requirement).

Drivers must document the inspection on the "Driver Vehicle Inspection Report." If another form is used for any reason, it must contain all the elements of the "Driver Vehicle Inspection Report," at a minimum. For more information, refer to the *Company Fleet Operations Policies and Procedures Manual*.

Terminal management has oversight responsibility for random inspections of all vehicles loading at the terminal. See Section 10 for more details.

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6.11 - Marine Facilities

6.11.1 - Overview

Refer to the following for operational guidance and inspections at Marine facilities:

- Receipts, Section 3
- STASCO Marine Terminal Operations Manual (November 2003 edition)
- Marine Terminal Guide (Site Specific)
- International Safety guide for Oil tankers and Terminals (ISGOTT), 5th edition.

6.11.2 - Depth Soundings

The following are requirements for depth soundings.

- All coastal and inland terminals with dock facilities will make an annual depth survey of the berth and approaches. Annual soundings of approaches are not required when a federal, state or local government agency has responsibility for surveying the approaches. In such cases, request a copy of annual soundings from that agency.
- Sounding surveys must be retained to create a historical siltation profile.
 Based on this historical data, the frequency of depth sounding surveys
 can be reduced or increased after consultation with the local Marine
 Technical Advisor and STASCO Shipping Operations. It may be
 necessary to make a repeat sounding survey after a hurricane, flooding or
 other meteorological event.
- Terminals suspecting a reduction of the water depth at the berth (e.g., vessel prop wash causing localized shoaling) should request a depth survey to verify the existence and localization of any submerged obstruction or shoaling.
- Local contractors with proper equipment should perform depth soundings to ensure accuracy.
- Contractors will take depth soundings portrayed in a grid pattern. Region management and STASCO Shipping Operations will establish the size of the grid. The local USCG Captain of the Port may also have a specified maximum grid pattern for the port and soundings must comply with this requirement.
- The Terminal Manager will forward a copy of the sounding survey to the local Marine Technical Advisor and the Technical Manager. The terminal should also retain copies of the map.



Contact region technical support and/or Marine Technical Advisor to assist with the above requirements.

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6.11.3 - Marine Dock Inspections

It is vital that the structural integrity of each dock is maintained therefore the following inspections must be performed:

 Visually inspect the dock above the waterline annually. A qualified Motiva employee or contractor shall perform this inspection. Document any deficiencies such as structural corrosion, damaged/worn timber concrete cracking and mooring hook/bollard degradation. Documentation must be retained at the Terminal. Make any repairs that are of immediate concern.



Even, inactive docks must be visually inspected once a year to assure structural integrity.

A qualified engineer must inspect the dock above and below the water. The
inspection will include a detailed visual inspection and ultrasonic testing if
needed. The report with recommendations must be retained at the terminal.
Appropriate repairs must be performed based on the recommendations. The
frequency of this inspection is based on the condition of the dock but cannot
exceed 5 years. The engineer must also recommend the next inspection period
the dock. Coordinate this inspection with your technical resource. Refer to
Marine Terminal Operations Guide, Section 5.1.4, Structural Surveys.

6.11.4 - Marine Dock Insulating Flanges

Marine dock insulating flange are used to electrically isolate the vessel from the dock to eliminate arcing between the two. Bonding cables to the vessel are not to be used on the dock since they defeat the purpose of insulating flanges. The insulating flange should be located at the most outboard permanent flange and it must be on the vessel side of any support or member attached to the dock structure. It is important that no actions be performed that might compromise the insulating properties of the insulating flanges. Activities, such as painting over an insulating flange, can compromise the insulating qualities of an insulating flange, thus rendering it ineffective.

Test the resistance of insulating flanges annually to ensure a measured value of at least 1,000 ohms. A lower resistance value may indicate damaged or deteriorated insulators. Refer to ISGOTT, Fifth Edition, 17.5.5.2 for further information on this requirement. Test insulating flanges more frequently as detailed in the STASCO Marine Terminal Operations Guide, Section 5.5.7.1, Insulating Flanges, if resistance is consistently lower than the requirement.



The line must be void of product on one side of the insulating flange for a valid test.

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6.11.5 - Transfer Hoses

Follow inspection and testing guidelines for product transfer hoses according to Hose Testing Schedule in Appendix 6.19.9 and the *Marine Terminal Operations Manual, Appendix 6*.



Information in the guide is valid, but does not include information on composite constructed hoses.

Replace marine dock hoses after 10 years of service. Mark marine hoses with these elements:

- "Oil Service" or name of product for which hose may be used
- maximum allowable working pressure (MAWP)
- date of manufacture, and
- · date of last hose test.



Marking the date of manufacturer and last test date on the hoses is not necessary if the hose markings indicate this data is available elsewhere in the terminal.

Keep marine hose inspection records at the terminal. Include this data:

- manufacturer's name
- date of purchase and date hose placed in service
- hose brand and serial number
- rated working pressure, and
- test dates and test pressures.

6.12 - Buildings, Yards and Fencing

6.12.1 - Drawings

Terminals should consider maintaining onsite a complete set of engineering quality "asbuilt" drawings accurately depicting property lines, fence lines, buildings, equipment, piping, etc. Technical Department has primary responsibility for preparing and maintaining these drawings for projects. Terminals have responsibility for ensuring that the Head Office knows about equipment and piping changes and that drawings are updated as appropriate.

Terminal should also have on file a copy of general electrical classification drawings (i.e. not site specific). Request this document from your technical resource.

6.12.2 - General Policy

Terminal management should frequently inspect terminal facilities and equipment personally to ensure adequate maintenance and good housekeeping, and to observe for safe working conditions.

Properties and facilities must always present a clean and orderly appearance. Employees must be knowledgeable on their terminal maintenance responsibilities, as well as training on how to do their jobs.

Terminal personnel must immediately clean up product leaks or spills and take corrective action to prevent recurrence. Proper reports and notifications must be filed. Product leaks or spills are unacceptable.

Plant management should consider using contractors to maintain top standards if other duties prevent permanent personnel from accomplishing housekeeping chores. The Motiva Technical Manual contains guidelines for office buildings, warehouses, garages, paving, fencing, parking lots and fire protection. Consult with your technical resource. The Region Manager will provide guidance or engineering support for facility changes.

6.12.3 - Safety and Health Standards

All company facilities are regulated under OSHA requirements. Certain facilities
as well as delivery equipment and truck drivers may have additional
requirements under DOT. Refer to your technical resource and the company
Fleet Operations Policies and Procedures Manual.



Consult with your Safety Representative for any questions on any OSHA, safety or health matters.

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6.12.4 - Painting and Identification

Follow guidelines on terminal paint colors and decal identification in Appendix 6.19.15.

6.12.5 - Nonproduct Pressure Vessels

Vessels operating at gauge pressures of at least 15 pounds per square inch or higher and do not contain hydrocarbon product shall be inspected in accordance with API 510 (e.g. air compressor).

Local management, along with region management, will request the region project coordinator to establish the requirements and provide the inspector and forms for these inspections. There may be state or local certification or license requirements. Local management will assure the documents are current and posted

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6.13 - Property Damage or Loss

A loss and damage record is to be completed whenever damage occurs by way of vehicular accident, personal injury, weather such as hurricanes, hail, wind, rain and flood, theft, security violations, explosions, etc. Also included is damage Motiva causes to others as well as what others cause to Motiva.

It is important that all necessary information and facts be recorded to properly represent the circumstances. Communications must be established with all appropriate internal departments and external contacts, depending upon circumstances. Some examples are financial, marine, procurement, legal, insurance, operations representatives, retail and other customers, technical resource to aid in repairs, supply, H&S and environmental representative, local law enforcement, etc. Careful management of the response and repairs must be undertaken to assure ALL costs related to the incident are tracked to help assure reimbursement form responsible parties, if recoverable.

For vehicular accidents, personnel injury, environmental occurrences, consult with your Health & Safety Representative / Environmental Representative and current guidelines in the Incident Management System.

For theft or other security losses, refer to your Security Manual and contact Corporate Security and your Security Representative.

Other property loss and damage not identified above is be reported to you Head Office Operations Representative for guidance on current administrative procedures.

Note that many loss and damage incidents will cross many areas of responsibility. Your Operations Representative can provide assistance and help clarify the necessary actions and responses.

6.14 - Terminal Security Sealing/Environmental Sealing and Padlocking

6.14.1 - Overview

Terminal management is responsible for checking and verifying all Terminal security/environmental seals. Terminal management also has the responsibility to control all padlocks and keys and ensuring their integrity.

Sealing and padlock locations depend on local conditions and local management requirements. Terminal security sealing or padlocks are required at:

- seal truck load rack equipment, and
- seal all points of access where tampering could affect measurement of product quantity or quality, or where unauthorized withdrawals could be made. (See Appendix 6.19.24, 6.19.25, and 6.19.26)
- padlock all closed tank valves, pipeline manifolds, dock manifolds, water draw valve, air bleed valve and low suction when not in use.
- other locations required by your security plan and local minimum standards

6.14.2 - Seal and Padlock Design

Seal Design: The most common seals found at all locations are E-cup seals. When installing E-cup seals, ensure that the wire twists fit securely in the cup, have no slack and pass through tall pertinent points in the system being sealed. Existing E-cup seals are acceptable until June 1, 2005. Seals installed after this date must be of the Plastic Wire type (Brooks Tooless Roto-Seal or equivalent) or Cable type (Brooks Cable Seal 2000 or equivalent). Some locations may have state weights and measures regulations requiring placement of a state-numbered seal on the meter calibration adjustment.

Padlock Design: Terminals must have a padlock system that allows Terminal management to control access to the locks and keys. This includes a key registry log.

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6.14.3 - Inspection Responsibility, Method and Frequency

Terminal management shall assume responsibility for inspecting and verifying the integrity of seals and recording seal numbers once a quarter at the minimum. Seal security and padlocks must also include random inspections. Any seals that are found to be illegible and/or damaged must be replaced at this time.

Locations with company equipment maintained by terms of a contract (e.g., pipeline, third party or exchange agreement) will designate a representative for random inspections.



Terminal personnel will record Terminal security sealing activities in InControl. Data recorded in InControl should include: Seal Group, Seal Location, Date Inspected, Person Inspected By, Seal Number, Reason for Replacement (if applicable), New Seal Number (if applicable), Date Replaced (if applicable).

6.14.4 - Disposition of Old Seals

Ensure used seals are not reusable before properly disposing of them. Old seals can easily serve illicit purposes.

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6.15 - Hose Inspection and Test

6.15.1 - Overview

This section covers hoses that carry product (i.e. rack, vapor and marine hoses). Hose failure may be a source of spillage and may result in a hazard. Reasons for hose failure include:

- shock pressures beyond the hose's designed working pressure
- mishandling, flattening or crushing
- continual exposure to severe weather
- · excessive end pull
- dropping, and
- sharp bending or kinking of the hose
- non-compatible products.

The visual inspections and test procedures in this section will help to detect weaknesses in hose structure assemblies before the weakness causes the hose to fail.

6.15.2 - Inspection And Testing Schedule

See the Hose Testing Schedule in Appendix 6.19.9 for minimum requirements on test type, testing frequency and inspection records to maintain. Hose testing includes visual inspection and hydrotest. See Appendix 6.19.7-8 for the procedure of these tests, Refer to the Marine Hose Guide for additional instructions and procedures covering dock hoses. 6.15.3 - Visual Inspection

The following are requirements for visual hose inspections.

- Follow the Quarterly Visual Hose Inspection Procedure in Appendix 6.19.7.
- In addition to routine visual inspections, terminal management or other designee must make a more formal visual inspection each quarter and record the results.
- Ensure operators and drivers regularly note the condition of the hose they
 are using. Drivers should note on their vehicle defect report any
 unsatisfactory delivery hose conditions. Operators must be aware of the
 condition of a product transfer hose before placing it in use.
- Immediately withdraw from service any hose that appears damaged or in need of repair.
- Hydrostatically test or replace the hose before returning to service if the repair work might affect the hose's strength or durability. If a hose failure or damage is found during inspection, a hose should be replaced not repaired.



If assistance is needed, contact technical resource when ordering new hoses. Hoses should include an integral bond wire, and, if applicable, hose material should be specific for Gasoline/MTBE/Ethanol compatible service.

6.15.4 - Hydrostatic Test

Follow the hydrostatic inspection procedure in Appendix 6.19.8.

When performing a hydrostatic test, be sure to:

- use the appropriate pressure, and
- test the hose up to, but not over, the designated test pressure.

The test's purpose is to determine the hose's reliability, not to weaken the structure by subjecting the hose to excessive pressure.

Consider replacing hoses in lieu of hydrotesting if more economical and time efficient. If hydrotest must be performed, also consider using contractor to test hoses offsite.

Also, be sure to:

- test hose according to the hose testing schedule or whenever visual inspection reveals questionable defects
- make provisions, before hose pressure tests, to prevent possible property damage and to ensure the safety of personnel performing the tests, and
- ensure only trained personnel using the proper tools and procedures conduct pressure tests.

6.16 - Emergency Planning

It is essential to develop well-defined emergency plans (e.g., to control fire; spills; natural disasters; transportation emergencies; civil disturbances such as vandalism or bomb threats; and mechanical, utility or human failures).

Jurisdictional agencies that will respond to the emergency may review the plans. Secure agreement and develop a protocol for periodic review, updating, training and testing of plans to ensure their reliability.

Some emergency plans are required by regulatory agencies, e.g., SPCC (Spill Prevention Control and Countermeasure) plans, ICP (Integrated Contingency Plan), and Facility Response Plans, by government environmental agencies and dock emergency plans by the U.S. Coast Guard. Region support resources will assist with these plans.

6.16.1 - Planning

Detailed planning is essential to cope with fire or spill emergencies. Consider the safety of people who might be in the terminal when an emergency occurs and also exposures to nearby properties.

Protecting lives and avoiding injuries are the most important elements of an emergency plan. Also consider these issues:

- containing damage
- notification of regulatory agencies
- contamination of water supply
- communication channels (warning and evacuation)
- water supply for fire fighting
- supplies of fire-extinguishing agents
- fire-fighting equipment and manpower
- methods of pollution control, containment and clean-up
- rescue procedures and equipment
- first-aid training and supplies
- traffic control.
- methods to fight fire (put it out) or contain fire (let it burn out) and
- public relations.

Review plans with appropriate emergency services during development, and review at least annually after implementing plans. A plot plan is required, and should include facility details such as:

- types of tanks and contents
- diking or drainage systems
- location of hydrants and other water supplies
- locations of extinguishing agents
- evacuation routes, and
- muster or meeting point outside terminal to take a head count.

6.16.2 - Communications

Prearranged communication channels are of utmost importance in dealing with terminal emergencies. Review the communication plan periodically to keep it up to date. The plan must:

 include a list of emergency telephone numbers of company resources and outside resources such as the fire department, police, hospital, ambulance, etc.



Include numbers of pipeline pump stations, if appropriate.

- identify oil spill cleanup cooperatives or contractors, list their phone numbers and have necessary equipment ready for specific anticipated emergencies, and
- contain a priority call list.



Provide for alternate communication procedures, such as outside phones or radio in case the normal system fails.

Only properly qualified personnel should respond to media inquires.

6.16.3 - Resources

Adequate resources, such as water supply for fires, are essential when responding to an emergency. Plans should outline procedures for obtaining the necessary resources from contractors, the Crisis Management Team, and local municipalities.

6.16.4 - Fire Extinguishers

All fire extinguishers must be visually inspected on a monthly basis to make sure they are ready to operate. The extinguisher tag must be marked (i.e. initial or hole punch) to document the inspection.

Terminal fire extinguishers must be inspected and certified annually by a competent, qualified person.

For more details, refer to Section 2 of this manual and Section 2.6 of the Motiva CM&D HSE Procedural Manual.

6.16.5 - Fire Hydrants

Annually inspect the serviceability of the terminal's fixed fire hydrant system by flushing to check equipment and possible water pressure problems. See Section 2.5.5 of this

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manual and Section 2.6.8 of the Motiva CM&D HSE Procedural Manual for additional information on inspecting fixed fire extinguishing systems.

6.16.6 - Fire Foam Systems

Cooperative groups in areas with several product terminals may find it advantageous to have accessible supplies of foam concentrate. Foam suppliers also maintain quantities of foam concentrate at strategic locations throughout the country. If the terminal does not maintain a supply, the nearest source for this material should be identified ahead of time.



Generally, fire foam is not recommended unless required by local regulations.

Refer to the Company Health & Safety Manual for inspection frequency and procedures.

6.16.7 - Employee Training and Practice Drills

Provide training in emergency recognition and prevention awareness. Plans must include provisions for evacuation drills to safe distances and places of refuge. Practice drills tend to reduce panic in an actual emergency.

Walk-through practice sessions for all procedures will familiarize all employees with the details of emergency procedures and may reveal the need for improvements. Provide for a critique of drills to make appropriate revisions.

All terminals must hold tabletop drills once or twice a year, in which employees answer "what if" questions and demonstrate their knowledge of immediate remedial actions (who to call for help, notification and reports to make, etc.).

One or two terminals in each Region must hold annual realistic "wet drills," in which participants actually go through simulated response activities. The Region Office and involved Head Office departments should authorize and plan wet drills

6.16.8 - Emergency Service Organizations

Coping successfully with a terminal emergency requires good relationships with municipal, county and state emergency service agencies. Invite representatives of emergency service organizations to tour the terminal to become familiar with terminal operations and procedures. Understand capabilities and limitations of agencies and formulate plans accordingly.

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6.16.9 - Police

Coordinate crowd control in cooperation with police. Make provisions for site security and control, evacuation routes and procedures for severe emergencies.

6.16.10 - Media Relations

The company's emergency media relations policy recognizes the news media's legitimate interest in emergency situations. Cooperating with the news media benefits the company. Such cooperation promotes rapid, accurate reporting of the facts, dispelling rumors and exaggerated accounts often occurring in the confusion of an emergency. Refer to Section 1 – Administration for specifics of who to contact. Terminal management should contact appropriate public affairs representative when an emergency involves any of these conditions:

- fatalities or serious injuries
- potential for significant environmental damage
- evacuation of employees (or possibility of evacuation)
- substantial property damage
- involvement of news media, or a situation likely to attract media attention
- public inconvenience due to the emergency
- charges of company negligence, and
- need for Public Affairs support.

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6.17 - Aviation Facilities

Aviation facilities have significant handling procedures and requirements. See Section 9 for details on all requirements.

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6.18 - ETOH Blending Considerations

Ethanol blending at the rack has become a common practice in our terminals for many reasons. It has been mandated in some states, in other locations it has become optimal as a replacement for MTBE in RFG gasoline, and in some states it just makes sense economically. The introduction of ethanol blending has revealed many specialized concerns that must be taken into consideration. Outlined below are the general issues to be addressed.

6.18.1 – Rack Equipment

Rack blending for ETOH requires specialized blend skids to be placed at the rack. Generally, rack blending requires at least one blend skid per lane and each skid can handle up to 4 loading arms. Motiva's preference has been Enraf vertical side stream skids. It has been preferred to have skids controlled by TopTech Multiload and TopTech terminal automation system, however they can also be controlled by rack presets or by dedicated PLCs. Some other considerations for the skids are as follows:

- Use of hydraulic control valves on the skids is preferential to electronic or pneumatic, due to the quickness of operation of the hydraulic control valves.
- Must ensure that V-Ball valves are used to control ETOH flow on skids, since they operate more linearly, i.e. 33% open allows roughly 33% flow.
- Must utilize Tuthill 2" PD gear meters w/ Ryton gears on the skid for proper material compatibility. Tuthill meters allow for better measurement at low flow rates than alternative meters and can be installed in any orientation
- In some cases sulfate or other precipitates have developed on rack turbine meter blades. This will cause the rack turbine meters to read incorrectly and will make them difficult to calibrate. If this kind of problem arises, meters should be changed out to Smith Prime 4's, which are not affected by the precipitate.

In some terminals, spool pieces have been placed immediately after the ETOH injection point. This has been done to make it easier to potentially install static mixers in the future if it is deemed optimal in order to maximize the product growth that occurs before the custody transfer meter. Testing is currently underway to determine the value of he static mixers. Currently, the distance has been set as no less than 15 feet from injection point to custody transfer meter, in order to allow at least 1 second of ETOH/gasoline growth before meter. However, if a greater distance is feasible based on rack set-up, then the injection point will be set as far from the meter as possible. Note, proper temperature measurement, meter maintenance, and stock controls are necessary to be able to identify and track the growth.

6.18.2 - Piping

The main consideration for ETOH piping at the terminal is stress corrosion cracking (SCC) around the welds. In the following cases, ETOH piping must be Post Weld Heat Treated (PWHT):

- Significant lengths of new ETOH piping
- Any new or existing ETOH piping over the water
- Any new or existing ETOH piping underground
- Any new or existing ETOH piping off site
- Any new or existing ETOH piping in other high risk areas

Other options to PWHT are available based on specific conditions. Examples include internal linings, alternates to carbon steel pipe, etc. Please consult w/ a technical representative to discuss alternatives and for further guidance on the procedure for PWHT.

Also, all lines in ETOH service must be well supported to minimize SCC.

6.18.3 - Pumps

When upgrading a terminal for ETOH service, Variable Frequency Drives (VFDs) have been installed on RBOB and ETOH supply pumps to accurately control the pressures. Motiva has been using Goulds PumpSmart systems. It is important that the ETOH stream be at least 10 psi higher than the RBOB stream (typical gasoline product pressure at the loading rack is 45 to 50 psi) to assure proper and consistent blending occurs. Controlled pressure allows for the following benefits:

- Measurement Performance
- Line Shock Elimination
- Reduction of Operating Costs (through use of minimum operating pressures necessary and the resulting decreased electrical costs)
- Decrease of Wear and Tear on Pump and Motor Parts

Care must be taken to ensure electrical frequency (noise in data/communication lines) is controlled in system by utilizing isolated conduit, shielded cable, separators in cable trays, etc.

Since ETOH becomes a vital aspect to loading gasoline, the need for spare equipment should be thoroughly evaluated

Pump Seals must be made of ETOH and denaturant (typically gasoline) compatible materials. The following materials are recommended: Viton F, Chemrez, or CalRez. Viton breaks down over time in pump seals, but it is softer and thus more forgiving to particles than CalRez or Chemrez. It simplifies spare parts if the seal material is compatible with all products in the terminal so that all parts are interchangeable.

6.18.4 - Tanks

There are many tank considerations necessary when upgrading a terminal for ETOH service. The following are some of the main considerations to be aware of:

- All tank bottoms and approx. 6 ft. up shell (above all appurtenances and welding on the first course) to be coated with ETOH and mogas compatible liner.
- Use aluminum pans if possible. However, when using steel pans for denatured ETOH all welds and heat affected zones (including welds on top of pan not in direct contact with ETOH) must be coated to help prevent stress corrosion cracking.
- Utilize ETOH compatible mechanical shoe seal or other systems as required to meet local regulations.

Please consult with your technical representative to ensure these issues are addressed.

6.18.5 – Fire Protection

Fire fighting systems might need to be upgraded to alcohol resistant materials depending on manufacturer recommendations and percentage of ETOH being blended. Foam type and application rate may vary depending on whether neat ETOH vs. final blended ETOH gasoline will be handled at the rack and in tank. Consult your technical representative to verify the following:

- Nozzle sizes
- Pipe sizes
- Foam storage size
- Mixer/diffuser changes
- Pump upgrades
- Need for fire sensor upgrade

6.18.6 - VRU

When terminals are converted to ETOH service, a few changes are necessary to any existing VRU. Generally, adsorber column pressure control and automatic temperature control for the glycol are added to the VRU. It has also been found beneficial to adjust the glycol temperature to run between 110 – 120 degrees F. If this temperature adjustment is not made, the glycol tends to absorb the ETOH causing dilution and inefficient performance. Another option is to install a dry vacuum pump that does not require glycol at all. This is an expensive option and may not become economically viable until terminals blend ETOH at 15% or more. At terminals where neat ETOH is loaded (i.e. hubs, etc.) all neat ETOH vapors may need to be routed to a VCU to allow proper vapor equipment operation.

6.19 - Appendices

6.19.1 -Storage Tank Monthly In-Service Inspection

TANK INFORMATION					
System Name (RAM/SAP Level 1)	gion				
TANK LOCATION (RAM/SAP Level 2)		NK JMBER			DATE
ROOF TYPE	INS	SPECTOR			
SERVICE or PRODUCT	NC	TIFICATION	ONS RE	QUIRED	YES NO
INSPECTIONS				· · · · · · · · · · · · · · · · · · ·	
	Previously Deficient and SAP Notified			If Deficient (Yes) Send Notification to:	Commonto
DIKED AREA AROUND TANK	SAP Notified	Yes	No	Nouncation to:	Comments
Dike wall damaged or lowered			1	Local Manager	
Dike drain valve broken, leaking or inaccessible		 	 	Local Manager	
Hydrocarbon on ground or surface water inside dike				Local Manager	
Materials stored inside dike that significantly reduce storage capacity or creates a fire hazard. Excessive vegetation that hides a spill or is a fire hazard.				Local Manager	
FOUNDATION AND TANK BOTTOM		•	•	<u> </u>	
Tank bottom leaking contents onto the ground				Tank Coordinator	
Check interstitial space of double bottom for leaking: a) open valve and check for liquid (close valves after inspection)				Tank Coordinator	
b) if under pressure/vacuum, make sure vacuum gauges are readable and operating as designed (record reading on back of form)					
Broken concrete foundation or soil loss under tank				Tank Coordinator	
Tank shell has water against it				Local Manager	
Bottom extension has significant corrosion or deterioration				Tank Coordinator	
Bottom extension covered by soil or vegetation				Tank Coordinator	
TANK SHELL					
Major shell deformation either inward or outward		<u> </u>		Tank Coordinator	
Tank shell leaking hydrocarbon onto the ground				Tank Coordinator	
APPURTENANCES	·				
Roof drain or tank valves leaking or broken				Tank Coordinator	
Tank mixer leaking or disconnected				Local Manager	
Stairway or platforms unsafe or need repair				Tank Coordinator	
INSULATION					
 Insulation has damaged areas, corrosion showing or not sealed to prevent water intrusion at the top 				Tank Coordinator	
TANK ROOF					
Fixed Roof or External Floating Roof has significant distortion, buckling or holes				Tank Coordinator	
External Floating Roof has significant hydrocarbons, water, snow or ice				Tank Coordinator	
External Floating Roof sump plugged or needs cleaning				Local Manager	
External Floating Roof significantly out of level				Tank Coordinator	

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*** RESTRICTED ***

TANK INFORMATION				
System Name (RAM/SAP Level 1)	Re	gion		
TANK LOCATION (RAM/SAP Level 2)	1	NK JMBER		DATE
External Floating Roof has significant debris or material on it.			Local Manager	
External Floating Roof seal has significant damage.			Tank Coordinator	
External Floating Roof legs are damaged or pinned in different positions.			Local Manager	

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6.19.2 - Tank Closure Checklist

LOCATION:	
TANK NUMBER:	
PREWORK DATE:	
POSTWORK DATE:	

EXTERNAL		
SHELL	Initial	Comments
Inspection Repairs Complete (if applicable)		
2. Paint in Good Condition		
3. Tank ID Number Visible 2/4 Sides		
4. Hazard Label Visible 2/4 Sides		
5. Tank Label (Capacity, HI & HI-HI Level etc.) Updated (if applicable)		
6. Product Name Per Terminal Operations Manual		
7. Data Plate (if present) Adequately Secured		
8. Grounding Cable Intact (if applicable)		
Isolation and Drain Valves (Positioned & Serviced)		
10. Product Sample Valves and Caps (if present) Removed and Secured		
11. Water Draw Valves Flanged (i.e. not threaded)		
12. Water Draw Valves and Internal Lines in Correct Location (i.e. Low points)		
13. Remove Fire Valves (unless locally required)		
14. Weeping Rivets, Epoxy Applied		
15. Weep Holes (if present) on Nozzle Pad Checked		
16. Over flows / Vents Not Plugged / Covered		
17. Skid Bars in Place, if necessary (prevents vents from being covered by seal)		
18. Foam System Inspected and Repaired		
19. Foam System Connected		
20. Anchor Bolts/Chairs in Place (if applicable)		
21. Stairs in Good Condition Non-skid If Needed		
22. Manways Ready for Closure (B7 Studs and Nuts Used)		
ROOF	Initial	Comments
1. Inspection Repairs Complete (if appl.)		
2. Paint in Good Condition		
3. Change to Free Vents unless PV is Required		
4. PV Vents (if needed) Serviced and Properly Adjusted		
5. Manways Ready for Closure, Both Above and Below (B7 Studs and Nuts used)		
6. Roof Drain not Plugged		
7. Gauge Hatch has Obvious Gauge Point/Notch		

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Tank Closure Checklist contd. (pg 2 of 4)

	Tank Olds	sule Checklist Conta. (pg 2 of 4)
ROOF Contd.	Initial	Comments
8. Inspection Hatches (Closed) → Check quantity		
9. Vent on Cone Roof with Internal Floater		
10. Gauge Hatch Gasket (Screw down lid or equal)		
11. Nonskid (Walk and Gauging Areas) in Good		
Condition		
12. Handrails in Good Condition		
13. Painter's Hub in Good Condition		
14. Remove Painter's Hook, Certify Rating, or Replace		
w/ API Painter's Hub		_
PIPING	Initial	Comments
1. Inspection Repairs Complete (if applicable)		
2. Paint in Good Condition		
Supports are Adequate for Loads Gaskets Installed		
Gaskets installed All Openings Plugged		77.77.77.77
All Openings Flugged Flanges in Good Condition		
(B7 Studs and Nuts Used)	,	
7. Valves are of the Correct Type for Application (eg. Ball vs. Gate)		
8. Valves are in Good Condition		
RELIEF SYSTEM	Initial	Comments
PRV tied into a Closed System		
2. Pipe and Fitting Schedules Correct		
(i.e min sched. 80 for screwed systems)		
3. Valves (Isolation, Thermal, Tank etc.) in Good		
Conditions		
4. PRV discharge located away from suction		
5. Port / tee for testing PRV without removal installed.		
<u> </u>		
DIKE AREA	Initial	Comments
Dike walls reinstalled or returned to preconstruction height to ensure original capacity		
2. Dike Drain Cleaned for Use		
3. Dike Area Clean and Free of Hazardous Waste		
Dike Area regraded to correct project damage		
5. No Tripping Hazards		
6. Construction / project materials removed.		

Tan	k Closur	re Checklist contd. (pg 3 of 4)
INTERNAL		
SECONDICTED LANGE IN 13 JUST RES	duttel	Cambians
1. Inspection Repairs Complete (if appl.)	T	
2. Cleaned; Ready for Product (No Excess Corrosion/Scale)		
3. Nozzles in Good Condition		
4. Nozzles in Correct Location		
5. Validate that Shipping/Receiving Nozzles are the Correct Size		
Adequate Quantity and Type of Nozzles (i.e.mixing nozzle properly installed & marked on tank)		
7. Adequate Design and Size of Diffuser / Suction		
8. Diffuser / Suction Not Plugged		
9. Gauge Float, Cable Guides in Good Conditions		
10. Default Suction Trough installed (if justified, see section 6.3.12)?		
11. Floating Suction (if present) in Good Condition and Chained		
12. Floating Suction Cable - Chain and Target Board in Good Condition		
13. Swing Joint in Good Condition		
14. Gauge Tube is Slotted		
15. Datum Plate for Gauge Tube is Attached to Bottom of Gauge Pole if there is a Separate Water Gauge Pole, Otherwise Attached to Floor (i.e. not to shell)		
16. Validate there is a Gauge Pole Located Over Low		
Point/Water Sump (if not, evaluate need)		
17. Leg Supports in Good Condition		
18. Leg Settings Correct after changes made		
19. All Legs Pinned at Same Height		
20. No Legs Missing (All in place)		
IS/ON FORM CONTRACTOR OF THE PROPERTY OF THE P	lemal	Communis
Inspection Repairs Complete (if appl.)		
2. Cleaned; Ready for Product (No Excess Corrosion/Scale)		
3. Cleaned; No leftover equipment, rags etc.		***************************************
4. Liner Installed for aviation service or chemicals (Floor and 3' up Shell).		
5. Vortex Breaker Installed		
6. Sump(s) Clean	***************************************	, , , , , , , , , , , , , , , , , , , ,
7. Sump(s) in Correct Location(s) (i.e. Low points)		
FAN & COME	/ loutel	Generalis .
Inspection Repairs Complete (if appl.)		
2. Cleaned; Ready for Product (No Excess Corrosion/Scale)		
3. Cleaned; No leftover equipment, rags etc.		
4. Manways Ready for Closure, Both Above and Below (B7		
Studs and Nuts used)		
5. Ladder in Good Condition		
6. Pontoons in Good Condition	2	
7. Pontoons Plugged		
8. Pontoon weights Recalculated (if stored products changed)		
9. Gauge Float Operational		
10. HI Level Alarm Nozzles (ie. Flanged)		
11. Consider Changing to Cable Suspended Roof		
12. Validate HLT Sump is Installed in Floating Roof		
. = . · canada i i = · camp io motanda ii i iodang i too	t	

Tank Closure Checklist contd. (pg 4 of 4)							
	/EXTERNAL						
SEAUS (16)	Untitel	Connens					
Inspection Repairs Complete (if appl,)							
Primary Seals Inspected							
3. Secondary Seals Inspected							
4. Seals in Good Condition							
5. Adequate Seal Type (eg. Upgrade from wiper to mechanical shoe needed?)							
6. Environmental Agency Validation of Acceptable Seal							
7. IFR Leg settings: HI LO							
8. Anti-Rotational Device Not Binding Roof							
9. Roof Ladder and/or Track in Good Condition							
10. Grounding Cable (Shunts)							
MOTRUMENTATION	nantella -	Commens					
Temperature Probe in Correct Location							
2. Thermal Well located near temperature probe							
3. Temperature Probe Installed & Loop Checked							
4. Varec (Auto Gauge System) System Loop Checked (if applicable)							
5. Varec Gauge Mechanical Parts Checked							
6. Electrical Work Complete							
7. Critical levels verified/recalculated. Overflow Height:HLAHHLA, Safe Fill Height							
8. HI and HI-HI Alarm Point Reset (if needed)							
9. LO-LO Alarm Set Point Recalculated (if applicable) and Reset							
10. Tank Strapping/Recalculation Completed							
11. New Strapping Entered into Electronic Gauging System (Varec)							
12. New Strapping Entered into Terminal Management System (TMS)							
13. If Bottom Replaced→Make Sure Under Tank CP Reference Cells and Monitoring Tubes are installed							
14. Cathodic Protection Turned On							
Post WORK	Initial	Comments					
Determine if tank requires hydrostatic test at completion of repairs							
Notify Environmental Rep. of tank return to service date for any required regulator/agency notification							

6.19.3 - Storage Tank Hydrotest

SECTIO	N 1 -	TANK INFORM	ATION							
System N (RAM/SAI Level 1)	ame P			TANK (RAM/ Level 2				Region		•
TANK NU	MBER			TANK DIMENSIO		METER (FEET)		HEIGHT (FE	ET)	
MAXIMUN DESIGN FILL HEIG		FT.	IN.	NOMINAL (CAPACITY (BBL	S OR GALS)	YEAR CONSTRUCTED			
SECTIO	N 2 -	TEST INFORMA	ATION							······································
			REASON FOR	TEST						
iMM		ST ELY AFTER CTION								VA. 10.1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.
☐ RET	EST				·				, 1	
Begin Test	DATE		TIME		☐ AM ☐PM	FILL HEIGHT A HATCH (BEGINNING C		<u> </u>	FT.	IN.
End Test	DATE		TIME		☐ AM ☐ PM	FILL HEIGHT A HATCH (END OF TEST DURATION OF	AT GAUGE		FT.	IN.
TEST FLU	IID					DURATION OF	HYDROTEST			
			IK SHELL TEMP.		,	°F				
Tempera	tures	AMBIENT TEM			MIN		°F	MAX		°F
		TEST FLUID T				°F				
SECTION	13-0	COMMENTS (Si	gnificant of unu	ısual occui	rrences during	g hydrotest)				
WITNESS						COMPANY				
	317477411 - 1447 48 7 4 8 8					Distribution:	Tank Coordinato	r Files OR		

Retention:

Tank Coordinator T Tank Location files Life of the tank

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6.19.4 - Floating Roof Seal Inspections

Visual Inspection From the Manway Procedure

Use a large mirror to reflects sunlight on the seal, and then observe as much of the seal as possible.

Look for any unusual conditions in the seal or floating roof, and for water or product on the roof.

Make sure falling rust from the tank shell, cone roof is minimal.

Note any unusual observations (or normal appearance) in the Remarks section at the bottom of the inspection form.

Observe the roof legs to confirm they are set for low roof position. Notify the plant manager if they are set for high roof position.

Document the inspection on the Visual from Manway Inspection Report below. Contact your technical resource for assistance in procedures and documentation, if needed.

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Visual From Manway Inspection Report

TANK INFORMATION		
SYSTEM NAME	REGION	
(RAM/SAP Level 1) TANK LOCATION	TANK	DATE
(RAM/SAP Level 2)	NUMBER	DATE
INSPECTED BY		
NEAREST CITY/TOWN		STATE
	ANK HEIGHT FT & IN)	TANK DIAMETER (FT & IN)
SEAL INFORMATION		
Check Appropriate Block Primary Seal Inspection O	<u>NLY</u>	Secondary Seal Inspection <u>ONLY</u>
Enter seal data below only for the seal to be inspected. Enter data	a for a primary seal <u>or</u> a seconda	ary seal.
Primary Seal Data	Check Appropriate Blocks	
Seal Manufacturer	☐ Liquid Mounted	☐ Vapor Mounted
Seal Name & Model No.	☐ Foam Filled	☐ Liquid Filled
Date Seal Installed	☐ Metallic Shoe	☐ Wiper
Secondary Seal Data	Check Appropriate Blocks	
Seal Manufacturer	☐ Shoe Mounted	☐ Rim Mounted
Seal Name & Model No.		
Date Seal Installed		
INSTRUCTIONS: Visually inspect the internal floating roof (IF	R) and the roof seal from man	way(s) or hatches in the fixed roof.
LEL reading measured at manway.		
2. Time Period since last withdrawal from this tank	Hours OR 🗆 M	fore than 24-Hours
3. Roof legs are pinned in: Low Roof Position If the legs are in the high roof position, notify location supervise	☐ High Roof Posi	tion
Supervisor:		
Date Notified:		
Date Notified:		
Is there any water on the deck of the floating roof?	☐ Yes	
If "yes", notify location supervisor.		
Supervisor:		
Date Notified:		

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This form meets the record keeping requirements of inspections perfo	rmed subsequent to 40 CFR 60
Subpart Kb–113b(a)(2). 1. Is the floating roof resting on the surface of the liquid?	☐ Yes¹☐ No
2. Is there any product accumulated on the deck?	☐ Yes ¹ ☐ No
3. Is the roof seal detached, i.e. are there obvious gaps where the seal is not pressed against the shell?	☐ Yes¹☐ No
4.Are there holes, tears in the seal fabric?	Yes 1 No
If the answer to any of the above questions is "Yes," give the following	information:
Date repairs were made: ²	
Describe repairs made:	
Repairs made by:	
Print name:	
Signature:	
Note 1: Any deficiencies must be reported to the EPA Administrator w Note 2: Repair within 45 days or remove the tank from service (a 30-c	
Show the seal conditions found on this diagram. The circle represents the tank shell. Roof seal Deficiencies should be inside the tank shell	shown just
Draw in the following items. With reasonable care,	
sketch them to scale as far as possible. > 1. Tank ladder (for Orientation) - L.	
> 2. Manway(s) that were used for this insper	ction -
MW	
 3. Location of any liquid on the roof. Label if water or hydrocarbon. LIQ - W or LIQ - H. 	t as
➤ 4. Holes or tears in the seal fabric. – HOLES	
5. Seal detached away from the tank sh DET.	\
	· T
COMMENTS	
DISTRIBUTION:	ORIGINAL AT TANK LOCATION COPY TO ENVIRONMENTAL REPRESENTATIVE NOTIFICATION
RETENTION:	TO ADMINISTRATOR IF NECESSARY RETAIN LAST TWO SEAL INSPECTION FORMS AT THE LOCATION
Seal Gap Measurement	
Seal dap weasurement	

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Perform a close visual inspection as described above. Then measure the width and length of any gaps found between the shell and the seal. (Gaps allow emission losses)

Before descending onto the roof, and periodically after descent, ensure respiratory and fire safety by checking for acceptable range of oxygen and LEL.

Contact your technical resource for assistance in procedures and documentation, if needed.

Close Visual Inspection Procedure

Make sure the roof is free of liquid (either product or water).

Walk along the roof as close as possible to the seal (within 3 feet). Observe the seal and inside tank shell for signs of wear.

Periodically pull the seal back from the shell and inspect the seal.

Verify that bonding cables on external floating roofs are '00' welding cable from the roof to the rolling ladder, and from the rolling ladder to the tank shell.

Verify that the floating roof is electrically bonded to the tank shell from shunts around the seal or cables to the roof.

Note any unusual observations (or normal appearance) in the Remarks section at the bottom of the inspection form.

Observe the roof legs to confirm they are set for low roof position. Notify the Plant Manager if they are set for high roof position.

Document the inspection on the Visual from Manway Inspection Report below. Contact your technical resource for assistance in procedures and documentation, if needed.

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Close Visual EFR Seal Inspection Report, for Kb – Out of Service Tanks

TANCHICONIATION	MAT AND 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1					****	
TANK INFORMATION SYSTEM NAME			DEC	IONI			
(RAM/SAP Level 1)			REG	ION			•
TANK LOCATION			TAN	K	ATE		
(RAM/SAP Level 2)				BER			
INSPECTED							
BY						T	
NEAREST CITY/TOWN						STATE	
TANK CONTENTS		TANK F (FT & IN	ŧEIGHT √)		TANK DIAME (FT & IN)	TER	
SEAL INFORMATION							
Primary Seal Data		Che	ck Appı	opriate Blocks			
Seal Manufacturer			Liquid N	l ounted	☐ Vapor M	ounted	
Seal Name and Model No.			Foam F	illed	☐ Liquid Fi	lled	
Date Seal Installed	_		Metallic	Shoe	☐ Wiper		
Secondary Seal Data		Che	ck Appr	opriate Blocks			
Seal Manufacturer	ıfacturer				☐ Rim Mou	unted	
Seal Name and Model No.							
Date Seal Installed							
Instructions for this form are in the Tank Inspection ar	nd Main	tenanc	e Manu	al.			
Completing this form meets the Inspection requirements of 40 CFR 60.113B(B)(6) – Kb (TANK MUST BE EMPTY)	Yes	No	N/A	Condition Good/Poor	List of Repairs I	Needed ¹	Date Repaired
Are there any defects in the external floating roof? (Is the roof badly warped? Are there any holes in the roof?)		3			•		
2a. Is the floating roof equipped with a primary seal which is either a mechanical shoe seal or a liquid-mounted seal which completely covers the annular space between the edge of the floating roof and the tank wall.							
2b. Is the floating roof equipped with a secondary seal that completely covers the annular space between the external floating roof and the wall of the storage tank in a continuous fashion.						,	
3. Are there holes, tears or other openings in the primary seal or seal fabric?							
4. Are there holes, tears or other openings in the secondary seal or seal fabric?				,			
5. For a non-contact external floating roof, except for automatic bleeder vents and rim space vents, does each opening provide a projection below the liquid surface?							

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Completing this form meets the Inspection requirements of 40 CFR 60.113B(B)(6) – Kb (TANK MUST BE EMPTY)	Yes	No	N/A	Condition Good/Poor	List of Repairs Needed ¹	Date Repaired
6. Except for automatic bleeder vents, rim space vents, roof drains and leg sleeves, is each opening in the roof equipped with a gasketed cover, seal or lid that is to be maintained in a closed position at all times (i.e. no visible gaps) except when the device is in use?						
7. Are automatic bleeder vents equipped with a gasket and set to open only when the roof is being floated off or is being landed on the roof leg supports (i.e. set to be closed at all times when the roof is floating)?						
8. Are rim space vents equipped with a gasket and set to open only when the internal floating roof is not floating or at the manufacturer's recommended setting?						
9. Is each emergency roof drain provided with a slotted membrane fabric cover that covers at least 90 percent of the area of the opening?						
Show the seal conditions found on this diagram. The circle represents the tank shell. Roof seal Deficiencies shown just inside the tank shell (circle). Draw in the following items. With reasonable care, sketch t scale as far as possible.	hem to	l be				
> 1. Tank ladder (for orientation) — > 2. Manway(s) that were used for						
inspection – MW ➤ 3. Location of any liquid on the ro it as water or hydrocarbon. LIQ – W or LIQ – H	oof. Lab	oel .				
4. Holes or tears in the seal fabriHOLES	c. –					
➤ 5. Seal detached away from the fine DET	tank she	ell.	\			
					ľ	

*** RESTRICTED ***

Is the floating roof electrically bonded to the shell with the she	th 1-inch wide steel sl	hunts at approximately 10 feet spacing?
Is there excessive build-up of paraffin on the shell or Yes	r roof seal?	
Is the bonding cable at the top of the rolling ladder to ☐ Yes ☐ No	o the shell in good rep	pair?
Is the bonding cable from the rolling ladder to the flo ☐ Yes ☐ No	ating roof in good rep	pair?
COMMENTS		
	,	
Notify the Tank Coordinator to schedule any needed	l seal repairs.	
Tank Coordinator:		Date notified:
Notify the company Environmental Representative of	f the seal inspection,	discrepancies, repairs and this report form.
Environmental Representative:	-	Date notified:
	DISTRIBUTION:	ORIGINAL AT TANK LOCATION COPY TO ENVIRONMENTAL REPRESENTATIVE
	RETENTION:	RETAIN LAST TWO SEAL INSPECTION FORMS AT THE TANK LOCATION

Close Visual IFR Seal Inspection Report, for Kb Pre-Initial Fill or Out of Service Tanks

TANK INFORMATION			25010							
SYSTEM NAME (RAM/SAP Level 1)			REGIO	N						
TANK LOCATION					TANK DATE					
(RAM/SAP Level 2)				ER						
INSPECTED BY	,									
NEAREST CITY/TOWN						STATE				
TANK CONTENTS		NK HE	IGHT		TANK DIAMET	ΓER				
SEAL INFORMATION										
Primary Seal Data		Check	Approp	riate Blocks						
Seal Manufacturer	_	☐ Lie	quid Mo	unted	☐ Vapor M	ounted				
Seal Name and Model No.		☐ Fo	am Fille	ed	Liquid Fi	lled				
Date Seal Installed		□М	etallic S	noe	☐ Wiper					
Secondary Seal Data		Check	Approp	riate Blocks						
Seal Manufacturer	_	☐ Sh	noe Mou	nted	☐ Rim Mou	ınted				
Seal Name and Model No.	_									
Date Seal Installed	_									
Instructions for this form are in the Tank Inspection and M	/lainte	nance	Manual	,						
Completing this form meets the inspection requirements of 40 CFR 60.113b(a)(1) and 40 CFR 60 113b(a)(4) – Kb (TANK MUST BE EMPTY)	Yes	No	N/A	Condition Good/Poor	List of Repairs	Needed ¹	Date Repaired			
1. Are there any defects in the external floating roof? (Is the roof badly warped? Are there any holes in the roof?)										
2a. Is the floating roof equipped with a foam or liquid filled seal mounted in contact with the liquid between the wall of the storage vessel and the floating roof, continuously around the circumference of the tank? OR						i				
2b. Is the floating roof equipped with two seals, mounted one above the other so each forms a continuous closure that completely covers the space between the wall of the storage vessel and the edge of the internal floating roof? (The lower seal may be vapor-mounted, but both must be continuous.) OR										
2c. Is the floating roof equipped with a mechanical shoe seal which is a metal sheet held vertically against the wall of the storage vessel by springs or weighted levers and is connected by braces to the floating roof? A flexible coated fabric spans the annular space between the metal sheet and the floating roof?										
3. Are there holes, tears or other openings in the primary seal or seal fabric?										

*** RESTRICTED ***

*** RESTRICTED ***						
Completing this form meets the inspection requirements of 40 CFR 60.113b(a)(1) and 40 CFR 60 113b(a)(4) – Kb (TANK MUST BE EMPTY)	Yes	No	N/A	Condition Good/Poor	List of Repairs Needed ¹	Date Repaired
Are there holes, tears or other openings in the secondary seal or seal fabric?						
5a. Is each opening in the internal floating roof except for leg sleeves, automatic bleeder vents, rim space vents, wells, ladder wells, sample wells and stub drains equipped with a cover or lid which is maintained in a closed position at all times except when the device is in use?						
5b. Is the cover or lid equipped with a gasket?				,		
Are covers on each access hatch and automatic gauge float wells bolted except when they are in use?						
7. Are automatic bleeder vents equipped with a gasket and set to open only when the roof is being floated off or is being landed on the roof leg supports (i.e. set to be closed at all times when the roof is floating)?						
8. Are rim space vents equipped with a gasket and set to open only when the internal floating roof is not floating or at the manufacturer's recommended setting?		1				
9. Each penetration of the internal floating roof for the purpose of sampling is a sample well. Does each sample well have a slit fabric cover that covers at least 90 percent of the opening?						
10. Does each penetration of the internal floating roof that allows for passage of a column supporting the fixed roof have a flexible fabric sleeve or a gasketed sliding cover?						
11.Does each penetration of the internal floating roof that allows for passage of a ladder have a gasketed sliding cover?						
Show the seal conditions found on this diagram. The circle represent the tank shell. Roof seal deficiencies should be shown just inside tank shell (circle).					+	
Draw in the following items. With reasonable care, sketch them to scale as far as possible. NOTE: The height of a course is usually 8 ft and the length of a shell sheet is usually 2			,			
Tank ladder (for orientation) – L						\
2. Manway(s) that were used for this inspection MW						\
3. Location of any liquid on the roof. Label it as water or hydrocarbon. LIQ – W or LIQ – H			+			+1
4. Holes or tears in the seal fabric HOLES			/			/
5. Seal detached away from the tank shell DET			\			

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Terminal Facilities

*** RESTRICTED ***

Is the floating roof electrically bonded to the shell with 1-inch wide stee Yes No Can not determine	shunts at approximately 10 feet spacing?
Is there excessive build-up of paraffin on the shell or roof seal? Yes No	
Is the bonding cable at the top of the rolling ladder to the shell in good o ☐ Yes ☐ No	repair?
Is the bonding cable from the rolling ladder to the floating roof in good r ☐ Yes ☐ No	epair?
COMMENTS	
	· · · · · · · · · · · · · · · · · · ·
Netter the Tests Occupied and a select the second state of the second	
Notify the Tank Coordinator to schedule any needed seal repairs.	
Tank Coordinator:	Date notified:
Notify the company environmental representative of the seal inspection,	
Environmental Representative: DISTRIBUTION:	Date notified: ORIGINAL AT TANK LOCATION
RETENTION:	COPY TO ENVIRONMENTAL REPRESENTATIVE RETAIN LAST TWO CLOSE VISUAL IFR INSPECTION REPORTS AT THE TANK LOCATION

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Terminal Facilities

arator Inspection Forms

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		3]					
Wattage			Heat Trace	2	Wattage					
Voltage					Voltage					
Amnerage					Amperage	-				

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6.19.7 - Quarterly Visual Hose Inspection Procedure

The following are the steps for conducting a visual hose inspection.

Completely extend the hose and examine for cuts, abrasions, tears and gouges.

Look for surface cracking. Covers may show surface cracking due to prolonged exposure to sunlight/ozone, but such deterioration does not justify retirement unless surface cracks extend to the reinforcement.

Carefully investigate any blistering or saturation of the outside cover (indicating leakage through the hose interior layers). Replace the hose.

Inspect linen and cotton utility hose for mildew, mold, breaks and rotting.

Look for kinking, crushing, permanent distortion or bulges that might indicate that the hose carcass has been damaged. Mark all bulges or soft spots with chalk to examine them more closely under test conditions. If bulges become hard under pressure, retire the hose.

Examine the coupling, flanges and nipples for cracks, excessive corrosion, and indication of leaks or nipple slippage. Cracks, excessive corrosion or any evidence of nipple slippage are reasons for retirement if the fittings cannot be reset.



Structural failures are most common near the end of the hose.

Record the visual inspection.

Repair hose and return to service if cuts or gouges in the cover do not extend into the outer reinforcement.



Replace marine hoses after 10 years of service regardless of the results of visual inspections.

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6.19.8 - Hydrostatic Test Pressures and Procedures for Hoses

Hydrostatic Test Pressure

Hose Type	Hose Size	Hydrostatic Test Pressure
Marine	All	150 or 1.5 x MAWP*
All pressure products (truck, transport, tank truck, plant)	1-1/4" to 2"	125#
	2-1/4"	100#
	3"	85#
	4"	85#

^{*}In accordance with local COTP.

Example: if operation allows a maximum of 100 psi operating pressure at the rail, test hoses to 150 psi (100 psi x 1.5).

Test Precautions



Never use air or any other compressible gas as the test medium, because the hose may fail (rupture). Such a failure could result in property damage and serious bodily injury.

The following are test precautions.

- Remove air from the hose by bleeding it through an outlet valve while filling the hose with test medium.
- Restrain the hose before pressure testing by placing steel rods or straps close to each end and at approximate 10-foot (3m) intervals along its length. This procedure keeps the hose from whipping if failure occurs. Anchor steel rods or straps firmly to the test structure, but make sure they do not contact the hose, which must be free to move.
- Secure the outlet end of the hose so that a blown-out fitting will stop.
- Make provisions to protect testing personnel from the forces of the pressure medium if a failure occurs.
- Make sure testing personnel *never* stand in front of or behind the ends of a hose while pressure testing.
- Do not use oil, solvent, gasoline or any other hazardous fluid as a test fluid. Avoiding these fluids protects against fire if a hose fails and the liquid sprays the surrounding area.

Hydrostatic Test Procedure - Hoses

The following are the steps for all hoses requiring hydrostatic testing. Refer to Recommended Testing Procedure in Appendix 6.1.5 on the Marine Terminal Operations Guide.

Connect the hose to a hydrostatic test pump with a pressure rating greater than the hydrostatic pressure.

Fit the opposite end of the hose with a cap or blank flange that has a small air bleeder valve.

Make sure all the connections are tight, and then introduce water (at main pressure) into the hose through the pump end. At the same time elevate the capped end with the vent valve open to bleed off air.

Close the vent valve when the hose is full of water and all the air is out (when a solid stream of water pours from the vent).

Increase the pressure to 60 psi and hold for five minutes. Carefully inspect the hose and couplings or nipples for leaks.

Increase the pressure to the required test pressure and hold for 10 minutes. Check for leaks in the system. (Reference Table in Section 6.19.8 and 6.19.9)

Release the pressure if a coupling leaks. Tighten the couplings if possible, and bring the pressure back to the hose's hydrostatic test maximum. Examine the hose for leaks, especially near the couplings or nipple.



Retire for repair or replacement any length of hose that shows any leakage or defect.

Release pressure from the hose, drain off all liquid and remove test fixtures. Thoroughly eliminate all traces of liquid before returning the hose to service.

Process the test water according to local rules and regulations.

Complete the inspection record, showing test results and disposition of hose.

6.19.9 - Hose Testing Schedule

		Hose Te	sting Sche	dule		
	Visu	al Inspection (H	ydrostatic Te	est	
Hose Type	Frequency	Performed By	Record Required	Frequency	Performed By	Record Required
CARGO* - tanker, barge and refueling hoses supplied by dock (all products including steam)	Before and after each use	Operator	No	Annual	Terminal or outside service	Yes (2)
,	Quarterly	(1)	Yes			
CARGO* - barge and lake tanker supplied by carrier (all Products)	Before and after each use	Operator	No	Annual		Yes (2)
TANK CAR - pressure (e.g. Butane Propane; Loading and Unloading)	Before and after each use	Operator	No	Annual	Terminal or outside service	Yes (2)
	Quarterly	(1)	Yes			
TANK CAR - suction (e.g. Ethanol; Bottom unloading)	Before and after each use	Operator	No	None Required		
	Quarterly	(1)	Yes			
TANK CAR - gravity (all products)	Before and after each use	Operator	No	None Required		
	Quarterly	(1)	Yes			

<u> </u>	·	T = ".	T	T	T	137 (2)
TRUCKS - pressure (e.g. refuel trucks)	Daily	Driver	No	Annual	Terminal or outside service	Yes (2)
	Quarterly	Mechanic	Yes			
TRUCKS - gravity (all products)	Before and After each Use	Driver	No	None Required		
	Quarterly	Mechanic	Yes			
TERMINAL - pressure (e.g. hydraulic hoses, portable pump hoses)	Before and after each use	Operator	No	Annual	Terminal or outside service	Yes (2)
	Quarterly	(1)	Yes			
TERMINAL - bottom loading hoses	Quarterly	(1)	Yes	None Required		
TERMINAL - gravity (all products)	Before and after each use	Operator	No	None Required		
	Quarterly	(1)	Yes			
UTILITY - (e.g. fire)	Before and after each use.	(1)	Yes	Annual	Terminal or outside service	Yes (2)

^{*} Refer to the Marine Terminal Operations Guide for information and test procedures.

- (3) Check marine dock hoses for age stamp and replace after 10 years or sooner if warranted by test or inspection. Replace all product and oily water handling hoses after 10 years of service or sooner, if warranted by test or inspection.
- (4) Replace water hose for fire control after 10 years of service unless the hose passes the annual inspection and test, and an outside/contract inspector certifies/approves the hose free of cuts, abrasions, tears, gouges and cracking that do not extend down to the reinforcement.

⁽¹⁾ Qualified Employee or Contractor

⁽²⁾ Product service, maximum allowable working pressure, date of manufacturer and latest test date to be marked on the hose or documented.

6.19.10 - Tank Alarm and Fill Level Worksheets

Calculating Tank A	larm and Fill Levels		
Refer to Section 6.3	3.17 for details.		
Terminal	TANK NUMBE	R	
* Prior to completing this	form, consider any changes to tank strap	pings, product type, flow rat	e,
reaction time etc			
I. PRELIMINARY DATA			
	fill rate (bbls/minute)		A
	fill time for receipt to shutdown after an		_
	s), typically 4 - 10 min (i.e response time		B
	n bbls) pumped during time "B" (A times		C
	"C" above with 50% safety factor (1.5 ti	mes C)	D
II. ALARM AND FILL L Note: Levels calculated	EVEL SETTINGS below are product levels. When installing	na alarme alao tako into como	ideration
	n activation point. Use Installing Tank A	_	
TOUROS MISTERIOS MICHAELINA	n den vallen penni ete medining ramera	iaini woxaonoot tot assistano	o whom moraning
	OVERFLOW LEVEL	OL =	bbl
	(see strapping chart)	= ft in	002
	(~~ ~~	
	HIGH-HIGH ALARM SETTING	HH =	bbl
	HH = OL MINUS D (see above)	=ftin	
	,		
	HIGH LEVEL ALARM SETTING	H =	bbl
	H = HH MINUS D	= ft in	_
	SAFE FILL LEVEL	S =	_bbl
	S = H MINUS C (see above)	= ft in	
Working Space			
	"HIGH LEGS" LEVEL	HL =	_bbl
		= ft in	
	"LOW LEGS" LEVEL	LL =	_bbl
		= ft in	
T.			
Notes:			
Notes:	Approved by:		Date:
repared by:	Approved by: Verified by:		Date:
repared by:	Verified by:	(Terminal Manager)	Date:
repared by:		(Terminal Manager)	Date:

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Installing and Verifying Tank Alarms Settings - For Tanks with Pans/IFR/EFR

Plant Tank #

Note: This worksheet must be used in conjunction with Calculating Tank Alarm and Fill Level Worksheet.

1) Striking Height

SH = ____ ft ___ in

2) When product is high in tank, measure 'E' with tape.

Top of flange on which alarm will be mounted to top of pan

E = ____ ft ____ in

3) Measure current product level with gauge tape or side gauge.

Datum plate to product level (incl. water, if any)

PL = ____ ft ____ in

4) Height difference between flange that alarm is mounted and gauge hatch

F == ____ ft

(Use best judgment in compensating roof pitch.)

5) Pan height above product level = SH-E-F-PL

PH = ft in

Refer to Calculating Tank Alarm and Fill Level Worksheet for OL, HH and H (in ft-in) referenced below.

If PH<(HH-H), Set alarm displacers on cable at the distances below.

- 6) High-High Level Alarm; Distance from alarm flange to bottom of high-high displacer

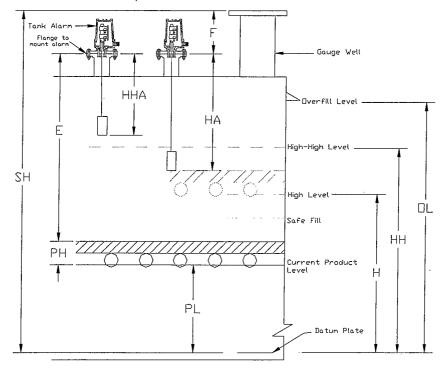
 HHA = SH-HH-PH-F

 HHA = _____ ft _____ in
- 7) High Level Alarm; Distance from alarm flange to bottom of high displacer
 HA = SH-H-PH-F

 HA = ft in

If PH>(HH-H), in the event a pan sinks, an overfill may occur before an alarm rings. Contact your technical resource for further assistance.

Note: On tanks with one unit (i.e. with both hi and hi-hi displacers) may need to modify the HLA equipment or install a second unit if displacers cannot be physically set as detailed above (i.e. the displacers interfere with each other).



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Installing and Verifying Tank Alarms Settings – For Tanks with NO Pans/IFR/EFR

Plant Tank #_____

Note: This worksheet must be used in conjunction with Calculating Tank Alarm and Fill Level Worksheet.

- 1) Normal Tank Height; Distance from datum plate to top of tank shell TH = ___ ft in
- 2) Alarm Flange Height: Top of tank shell to top of flange that alarm will be mounted on (Use best judgment in compensating roof pitch.)

 G = ____ ft ____ in
- 3) Activation Point from bottom of displacer.

 AP = 0 ft _____ in See manufacturer's notes for activation point in that specific product.

 Typically half the displacer (between 2-4 inches, depending on displacer size)

Refer to Calculating Tank Alarm and Fill Level Worksheet for HH and H (in ft-in) referenced below.

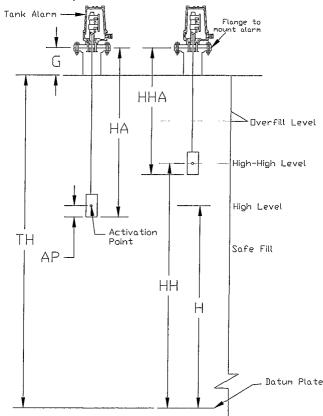
- 4) High-High Level Alarm; Distance from alarm flange to the bottom of the high-high displacer HHA = TH+AP+G-HH

 HHA = ____ ft___ in
- 5) High Level Alarm; Distance from alarm flange to bottom of high displacer

 HA = TH+AP+G-H

 HA = _____ft ____ in

Note: On tanks with one unit (i.e. with both hi and hi-hi displacers) may need to modify the HLA equipment or install a second unit if displacers can not be physically set as described above (i.e. the displacers interfere with each other).



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Terminal Facilities

6.19.11 - Alarm Testing Procedure

Typical Test Procedure Performed Within 24 hours Before Every Receipt

- 1. Notify all remote locations where the alarm will sound (e.g. Pipeline Center, third party security control center) that a high-level alarm system test will soon start.
- 2. If needed, locate annunciator panel and place in test mode (i.e. to prevent automatic shutdown to occur during testing).
- 3. Go to the designated receiving tank(s) and activate the high-level by manually pulling cord.
- 4. Ensure the high level alarm sounds. If applicable, ensure tank MOV is closing.
- 5. Activate the high-high level by pulling the cord further or pulling the second cord.
- 6. Ensure the high-high level alarm sounds and that the sound is distinct from the high level alarm. If applicable, ensure tank MOV is closing. Audible alarms should stop when cords are released.
- 7. If annunciator panel audible alarm is still ringing after cords are released, acknowledge alarm on annunciator panel.
- 8. Contact all remote locations and confirm they received the alarms.
- 9. If applicable, take annunciator panel out of test mode before receipt.
- 10. Document the test was performed. Examples of acceptable documentations are notes and initials in gauge book or product receipt form and automatic annunciator panel print out.

Quarterly High Level Alarm Test Procedure

This test typically needs two operators to perform. Perform all steps listed below in additions to those listed above, quarterly.

After notifying remote locations of testing, if applicable, turn test key on annunciator panel to see if all lights on panel work. (Note: Some locations are wired such that the tank farm audible annunciators and the remote annunciators also sound on this test.)

When high and high-high level cords are pulled, one person should verify the alarm for the appropriate tank was heard and seen on the annunciator panel.

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Terminal Facilities

6.19.12 - Alarm Manufacturer's Inspection Procedures

HIGH-LEVEL ALARM SYSTEM INSPECTION OF A TRANSDATA CORP SERIES 6761 LEVEL SWITCH AND SERIES 6699 ANNUNCIATOR SYSTEM.

Maintenance of the 6761 Level Switch

- Inspect the level switch to assure proper operations.
- Inside surfaces of the switch housing and switch mechanisms be clean and free of moisture and dirt to
 prevent from interfering with the operation of the switch mechanism.
- Cover of the switch assembly should be in place at all times to prevent dirt and foreign matter from entering the housing.
- Check the operation of the switches by pushing the Alnico magnets in towards the stainless steel tube to
 confirm operation of the magnets and switch assembles. (In moving these magnets there should be
 virtually no interference and the magnets should return to their original position upon release.
- It is not recommended that any oil or lubricants be used on the pivot points of the switch mechanism since lower temperature conditions can cause the oil to become thick and prevent operation of the switch mechanism. (The switch assembly is provided with a corrosion inhibitor attached to the upper switch frame.)
- It is recommended that the inhibitor be changed every twelve months,
- It is not recommended that re-adjustments be made to the steel armatures which are installed on the stainless steel connecting rod since these have been set by the factory and tampering will cause failure of the control while in service even though manual operation activates the switches. These armatures have been set and call- brated for the specific gravity of the material being stored.

NOTE: Installation of the Transdata 6693 Level Switch Operation Checker is designed for mounting between the level switch and the tank nozzle in order to manually operate the level switch without having to remove it from the veasel. This affords operating personnel the opportunity of confirming that the level switches are operating property and can be depended upon to function when the liquid level rises to the level actuating points of the switch.

 It is recommended that at six month and twelve month intervals the inside switch mechanisms of the Series 6761 Limit Switch be sprayed with a dry film Tellon coating which is available from Transdata, which will drive out any moisture that is present in the switch assembly and provide a coating which will help prevent condensate build up on the surfaces of the moving parts.

Maintenance of the 6699 Annunciator System

The annunciator system is of normally energized design which affords constant monitoring of the control relays, field wiring and electrical contacts of the Series 6761 Limit Switches. As a result, in the event of mechanical damage to any of these components an alarm would be initiated indicating a trouble condition, which would alert an operator to any problem.

The annunciator also incorporates a full function test push-button which is designed not only to test all lamp circuits, but will also operate all solid state and electromechanical devices, including local and remote homs.

The annunciator is also provided with a power failure indicating circuit (Model 1554) which is provided with a test button which will simulate a power failure condition in both the annunciator and the field mounted horns.

The field mounted homs are provided with a field wire monitoring circuit (Model 1543) which is designed to constantly monitor the condition of the field hom wiring.

It is recommended that the annunciator system and the power fallure indicator test button be actuated on a weekly basis to confirm operation of all circuits.

DECR90318027

Maintenance Instructions Series 6761 Level Switch and Series 6699 Annunciator System

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High Level Alarm Inspection Form

Inspe	ection			Maintenance						
	If Visible, Are	and Chains	Dry Interior	Clean Corrosion	Change Desiccant Pack/Spray with Anti-Corrosion	Grease Cover Threads and Checker Pivot	Completed By			
					·					

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Terminal Facilities

6.19.14 - Vapor Recovery/Combustion Unit Shutdown Alarm Response Procedure

If you are responding to the vapor recovery unit shutdown alarm, take the following steps:

Push the "Alarm Reset" to silence the alarm.

Do not attempt to restart the unit unless you are authorized to do so.

Contact a supervisor or terminal operator if available at the terminal.

If unavailable, call in the order listed below:

Name	Office	Home
Supervisor		
Supervisor		
Operator		
Contractor		
Area Technician		
Central Dispatch		Call if contact not made
		above

Clean air regulations apply to the operation of this unit. Do not perform loading operations while this unit is out of service unless authorized to do so by terminal management.

Maintenance or service on this unit is not to be performed unless the lockout/tagout procedures in effect at this facility are in place.

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Terminal Facilities

6.19.15 - Terminal Paint/Identification Guide

Terminal Facilities - Markings

Fire Protection Equipment

Appropriate identification for extinguishers, foam system, water wheels, etc. is required.

Product Piping

At appropriate locations, the following markings are recommended as needs dictate:

- W/3-inch bands, and
- directional flow arrows.

Storage Tanks

The following markings are required for storage tanks:

- appropriate information on product hazards if locally required
- tank number—12-inch-high numbers
- product stored—6-inch-high letters (unless product changes often)
- near manway cover in 2-inch-high letters: (optional, if kept in tank file)

tank diameter, height and nominal capacity in barrels

date of last internal inspection and cleaning.

• on tank shell—exterior *paint system* (optional if kept in tank file):

date painted type of surface preparation paint specification (primer and overcoat), and contractor.

• on tank shell—interior coating (optional if kept in tank file)

date coated surface preparation area coated type of coating and thickness, and contractor.

> near gauge hatch on roof—"reference gauge height" in feet, inches, and fractions

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- on tank shell near side gauge readout and near gauge hatch on roof—"safe fill height" in feet, inches, and fractions
- tanks with floating pans (near sight gauge readout)—"floating pan operational low-level gauge" in feet, inches, fractions, and
- on cone-roof and external floating-roof tanks near manhole—"Entrance into this tank/onto this roof may be done only when observing approved confined space entry procedures."

Terminal Facilities - Color Scheme

Truck Rack

The color schemes for the truck is are (change only when repainting for protection is required):

- Ground level up to canopy underside "cut line": medium gray
- Canopy underside and piping above "cut line": white
- Canopy exterior: medium gray

Product Storage Tanks

The color schemes for product storage tanks are:

- · light oil/lubricants—white, and
- residual/asphalt—black.

Piping and Equipment

The color schemes for piping and equipment are:

- light oil/lubricants/additive—medium gray or white or match existing color
- residual/asphalt—black
- vapor recovery—white
- fire protection (foam/water) —red
- utilities—medium gray.

Structural and Stair Walkways

The color scheme for walkways is white or medium gray to match existing. Galvanized or aluminum does not need to be repainted. See OSHA Regulations for additional color scheme requirements.

Loading Rack Meters, Manifold, Strategic Block, and Emergency Shut-Down Valves

 Loading rack meters, manifold, strategic block, and emergency shutdown valves must be painted the appropriate product colors.

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Terminal Facilities

Plant Facilities - Color Specifications

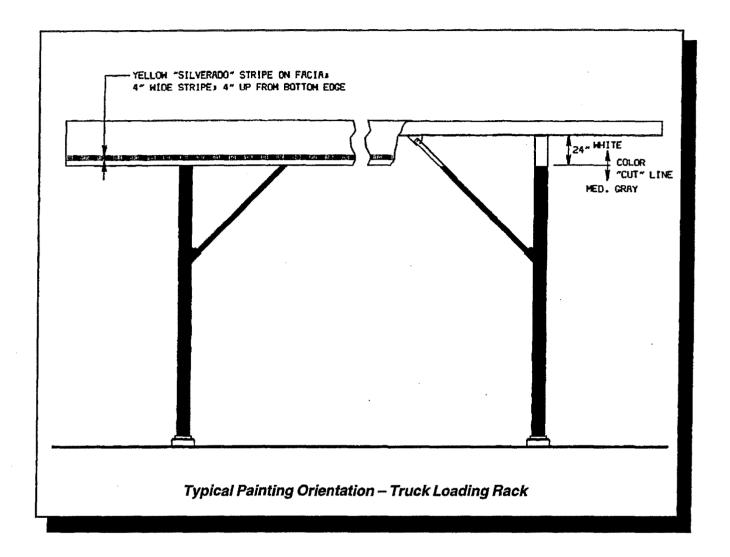
Medium Gray	ANSI #61	
White	Tank white	
Black	Black	
Blue	OSHA blue	
Red	OSHA red	
Green	OSHA green	
Orange	OSHA orange	
Yellow	OSHA yellow	
Brown	Medium brown	

Product Color

Product	API Color Code
Regular	White
Regular - MTBE	
Regular - Ethanol	
Plus	Blue
Plus - MTBE	
Plus - Ethanol	
Premium	Red
Premium - MTBE	
Premium - Ethanol	
Jet A	Black
Avgas 100LL	Red, White, and Blue
Kerosine	Brown
Diesel	Yellow
#2 Fuel Oil	Green
Vapor Recovery	Orange
Interface Mix (Transmix)	Gray
Additives	
Ethanol	Bronze

Contact Region management if required.

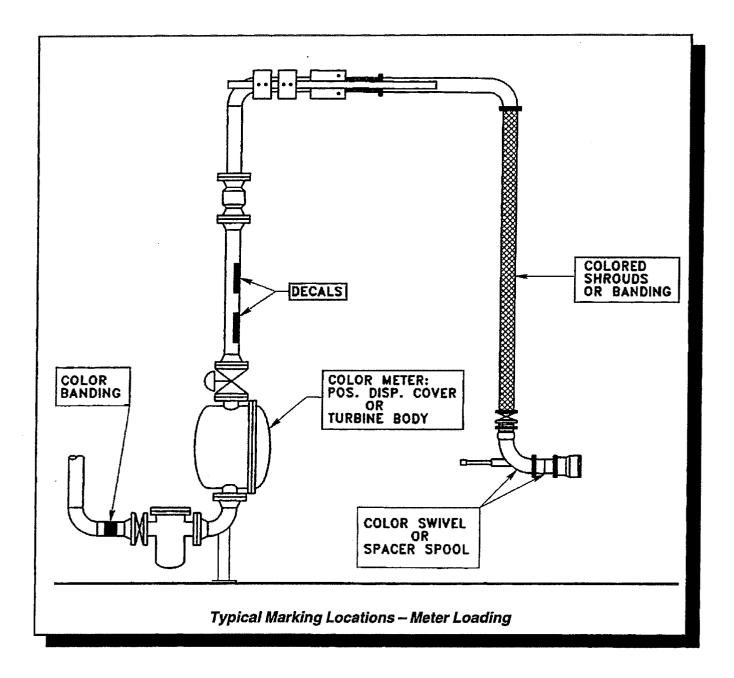
6.19.16 - Typical Painting Orientation



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6.19.17 - Typical Marking Location



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Terminal Facilities

DAMAGE DAMAGE

TO SIGNATURE TIVES TNO

WHITE/YELLOW COPIES - HEAD OFFICE

6.19.18 - Pipe and Crossing Inspection Form

Use the form that follows to document terminal pipe inspections.

Pipe And Crossing Report Shell Pipe Line Corporation West Coast Area LOCATION FOREMAN NO LOCATION CODE DATE OF OCCURRENCE FOREIGN CROSSING PIPING CHANGE MTC COUNTY STATE PIPE EXPOSURE, ONLY SYSTEM CHECK ONE CHUDE OIL REFINED PRODUCTS SYSTEM NAME FACILITY NAME/DESCRIPTION NATURAL GAS GATHERING SYSTEM MAP/ORAWING NO SURVEY STATION RMILE MARKER NOMINAL DIA. WALL THICKNESS OF LIT CORROSION & COATING INFORMATION - (INFO ON EXISTING PIPE) DISBONDED COLD FLOW/SAGGING MECHANICAL DAMAGE COATING COATING CONDITION TERITTLE/CRACKS VISUAL HOLIDAYS NO OBVIOUS PROBLEMS OTHER YES NO EXTERNAL INTERNAL IF CORROSION PRESENT LENGTH OF CORRODED AREA GENERAL LOCALIZED PITTING CORROSION YES NO YES NO ACTION NOTE SEE INSTRUCTIONS ON THE RACK SIDE OF THIS FO FOREIGN STRUCTURE DETERMINE IF FURTHER ACTION IS REQUIRED CLEARANCE OVER SHELL'S LINE UNDER SHELL'S LINE STRUCTURE MATERIAL POWER SEWER ADDRESS TELEPHONE WATER CONTRACTOR TELEPHONE PIPING CHANGE - (INFO ON NEW PIPE) ADDED/REPLACED LINE YES OR COMPONENTS NO REPAIRED DOCUMENTS ATTACHED (SEE BACK INSTRUCTIONS) LOWERED LINE]NO BELOW GROUND DEPTH OF COVER (INCHES) NOMINAL DIA WALL THICK GRADE SKETCH/DESCRIPTION

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Terminal Facilities

YES NO

YES NO

RETENTION - LIFE OF FACILITY

DATE FORM COMPLETED

YES NO

PINK COPY - ORIGINATOR

INSTRUCTIONS

LOCATION

This section should be completed for foreign oversings, piping charges or my other time the pipe is required. The Facility Name/Description is the location of the work, is, mainthe, narry of puma station-terminal, etc. If resided, Aréa Office will assign thin Area No. The form should be mailed to Proid Office within 10 calendar

CCRROSION & COATING INFORMATION (EXISTING PIPE)

This section should be completed engine the pipe is exposed, for any readed. If no external correction is precipit, the correction action. Length of corrected area, and may pit depth boxes should not be completed.

Whenever excreasions are premied, in it alwaye good practice is inform the Companion Technicism to that he can be present. A Companion Technicism may want to complete a Coating & Sipe Evaluation Form,

Cooling & Pipe Evaluation Form (PUOP), 1071) Completion of a Coating & Pipe Evaluation Form will not always be necessary especially if there is enough decembers that these this site executional foundation of the cooling and the pipeline. Cooling and Pipe Evaluation forms should be used for the following.

- 1. When his lopemen sees a mod.

- When the lear man sees in mad.
 When there is an interest to gettin all overtable information on certain lines.
 When something new can be learned about the dealing or pide.
 When there is not sufficient history on the condition of the line or cooling.
 At locations that are very difficult in excavable, such as city streats; pipe with excessive cover, awaring/matsh areas, etc.
 Where the soil condition may have changed due to chemical or of spits.
 On all rice advisor extend consequents.

- 8. On all pipa where external corresponds prenent.

General Corresion and Localized Pitting. To determine Pipeline Insp & Mice Manual, Sects 3 N(C) for liquids & 3.9(C) for gas To determine if replacement or repair is required due to general corrosion or localized pitting, reference the

COREIGN STRUCTURE

All bores in the section should be completed whenever a public road, railroad, buried utility, or loreign utility crosses the fine.

PIPINO CHAPIGE/MAINTENANCE

This section should be complained when the pipe is lowered, replaced, relocand, reperied, or when proe/components are added to the system. This form our also be used to document replacement of system components, as valvus, refere, etc.

The following are required when prise is replaced, research, research, or when pipe/components are added. (Helerence the Pipelina, Corrozion, and Coating Inspection & Maintenance and Sulety Manuals to more information)

Jurisdictional	Fareitalital nub-note	Form Required
Yes Added Pipa;	Area Determines	PL-218 Hydrostatic Test Centificate with the following documentation: Form PL 318-A.
Relocations, A]	Pressore and Temperature Recording Chans, Deadweight Tester.
Replacements	Ì	Fressure Recorder, and Temperature Device Calibration Certificates;
		Explanation of Presauce Committees, and it recessory in Profile of the
No Repairs	i	Pipeline when test section procedure differences exceed 100 leet.
Y#s	Area Determines	Pt. 779 Wold Non Destructive Trigling reputs (X-Rey tilm retained for 1 year),
		Location to storage of X-Hay film shall be Head Orince, or NDT Contractor Office.
Yes	Area Detrymines	PL 779 Results: of Inspection Completion Report or Inspection Company's Report
Yes	Area Dotoroanes	Visual Inspector Qualification records and NOT Inspector Qualification Records
Yes	Yos.	PL 782 Welder Cualification Records
Y ₁₂	Агов Поизонось	Pl. 568 Internal Improtion of Pine Removal
i		

SYETCH DESCRIPTION. This section should give enough defail, is, starch numbers, applies enough, distances, not, so that revisions to existing drawings can be completed. Remarks, comments, and descriptions of any damage should also be written in this exition.

BAMAGE

This section should be completed for loreign crassings, pipping changes, or any other time the pipe is a cossest.

ALL FORMS SHOULD BE SIGNED WITH TITLE, TELEPHONE NUMBER, AND DATE FORM COMPLETED.

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Terminal Facilities

6.19.19 - Tank Vent Chart

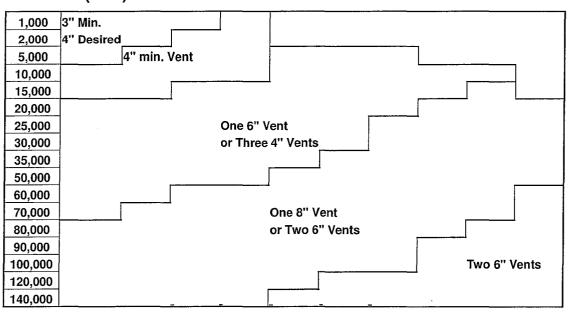
Vent Sizes For Normal Venting of Storage Tanks

Pumping Rate

Bbl. Per Hr.	500	1000	1500	2000	3000	4000	5000	6000	7000	8000
Gal. Per Mins.	350	700	1050	1400	2100	2800	3500	4200	4900	5600

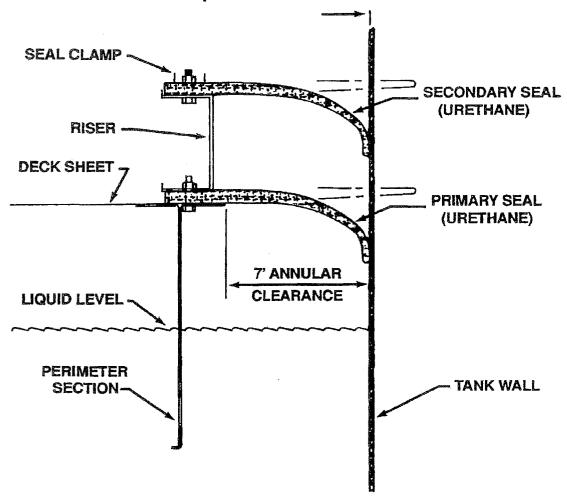
Minimum Size Open Vents For Non-Volatile Products (Flash over 100°)

Tank Size (BBL)

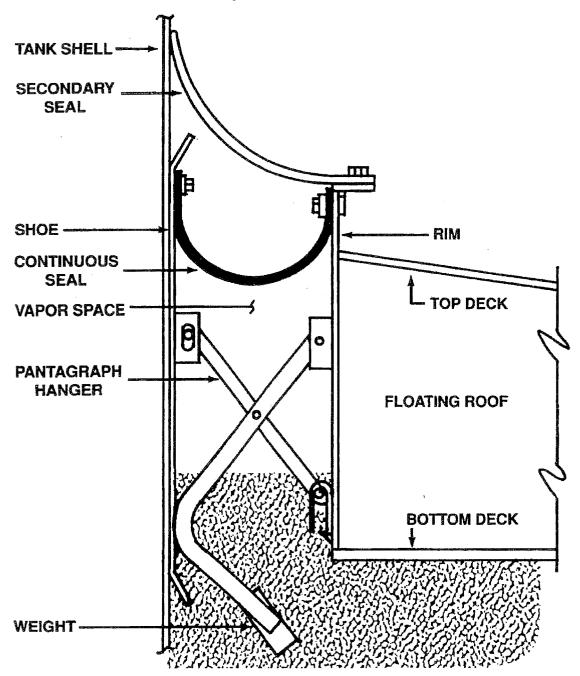


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Terminal Facilities

6.19.20 - Double Wiper Seal

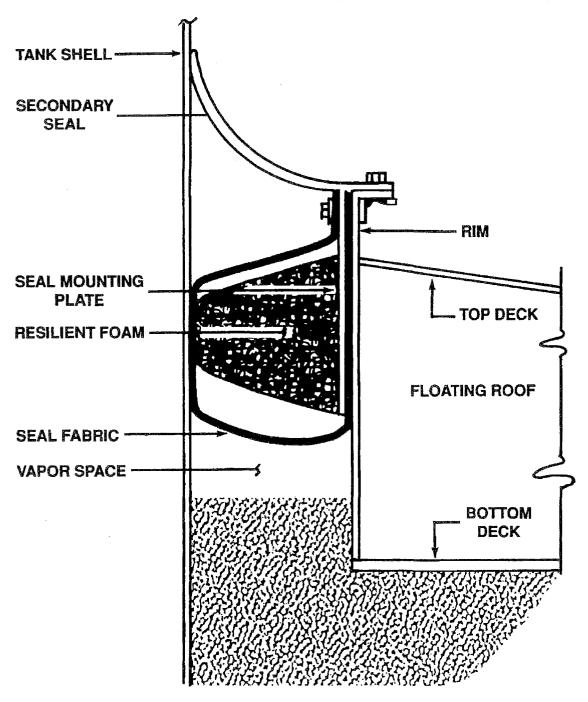


6.19.21 - Typical Metallic Shoe Primary Seal With Rim-Mounted Secondary Seal



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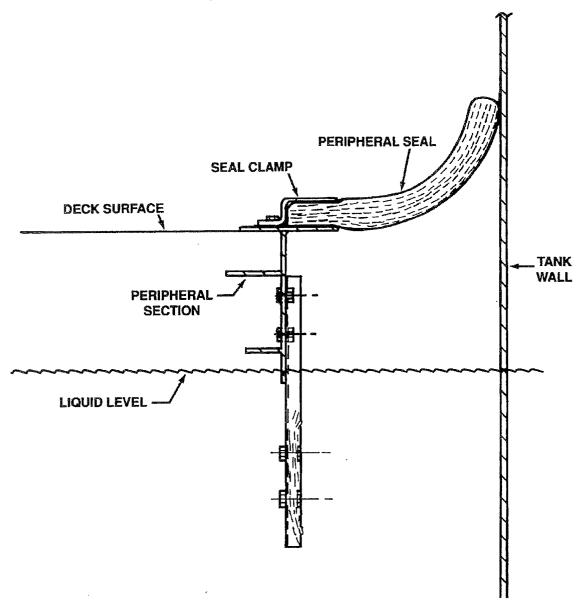
6.19.22 - Typical Nonmetallic Vapor-Mounted Primary Seal With Rim-Mounted Secondary Seal



November 2008

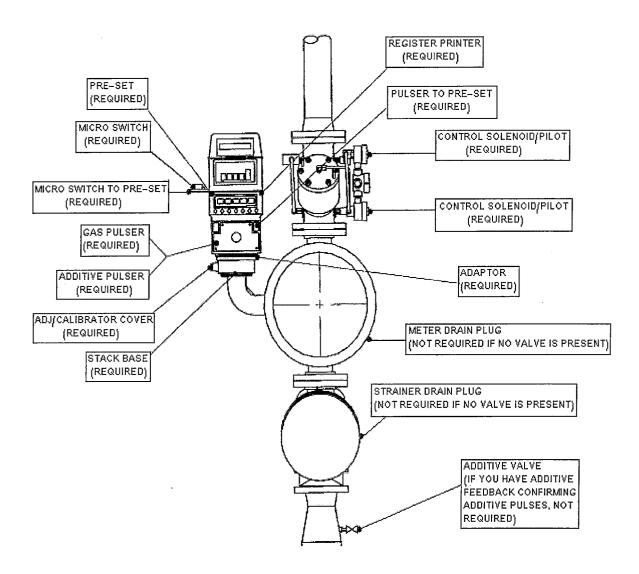
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6.19.23 - Flexible-Wiper Primary Seal



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Terminal Facilities

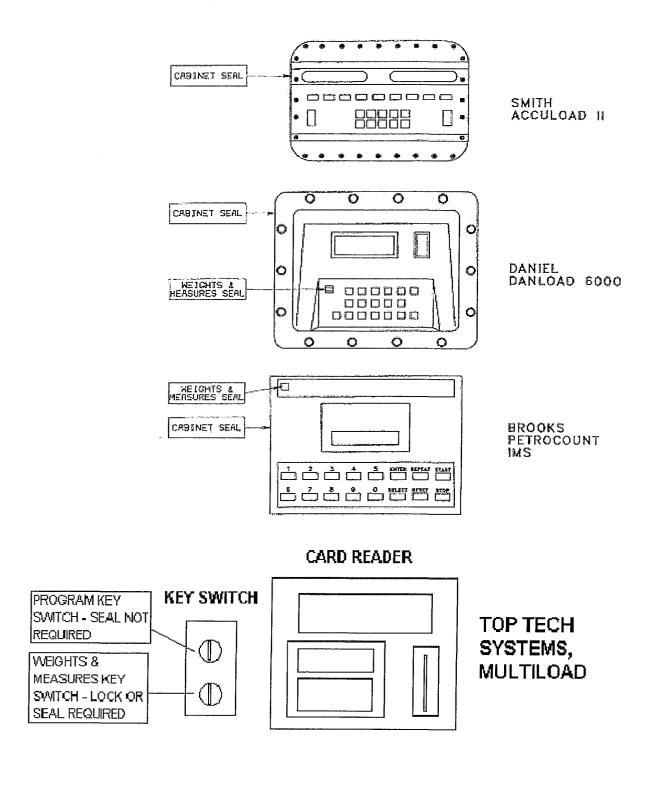
6.19.24 - Minimum Sealing Requirements For a Typical Meter Assembly



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Terminal Facilities

6.19.25 - Minimum Sealing Requirements For Electronic Presets

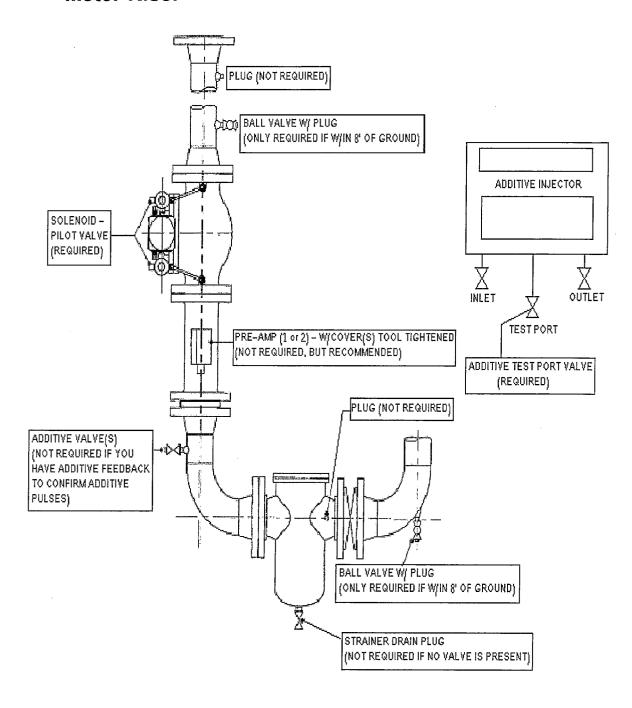


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Terminal Facilities

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6.19.26 - Minimum Sealing Requirements For Typical Turbine Meter Riser



6.19.27 – Underground Pipeline Easement & Surface Inspection Form

Person Inspecting:	Date Inspected:
Facility Name:	Pipeline Product Service & Diameter:
Description of Pipeline Location:	
Is there a clear access path along the ground about etc.)? If not, please describe obstacles and their make path clear, please indicate intended date of	location along line. Action must be taken to
Is the location of the underground line marked? A markers present? If not, markers must be replace intended date of completion.	
Is there anything that would indicate a pipeline lea etc.) on the ground above the pipeline path? If so, staining/dead grass, etc. Cause of symptom(s) m Technical and HSSE Reps.	please describe coloring, size, location of
•	

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TANK Description

PRODUCT STORAGE TANK LIST

TANK NO.	PRODUCT IDENTIFICATION	CONST,	NOMINAL CAPACITY (GAL.)	ACTUAL CAPACITY (GAL.)
41	ETHANOL	A/G	90,700	80,500
42	ETHANOL	A/G	90,700	80,500
43	GASOLINE (REGULAR)	A/G	90,700	80,500
44	GASOLINE (REGULAR)	A/G	90,700	80,700
45	ETHANOL	A/G	90,700	80,700
46	ETHANOL	A/G	88,875	78,373
47	GASOLINE (REGULAR)	A/G	425,000	373,755
48	GASOLINE (REGULAR)	A/G	425,000	373,609
49	GASOLINE (SUPER)	A/G	450,000	419,926
50	GASOLINE (SUPER)	A/G	450,000	422,926
51	ADDITIVE (SHELL)	A/G	5,000	4,500
52	ADDITIVE (EXXON)	U/G	5,000	3,600
53	WATER/GASOLINE	A/G	6,000	5,400
54	ADDITIVE (MOBIL)	A/G	5,000	4,500
55	DIESEL	A/G	10,000	9,300
7	OUT OF SERVICE	A/G	12,000	10,200
8	OUT OF SERVICE	A/G	12,000	10,200
9	ADDITIVE (GENERIC)	A/G	12,000	10,200
10	ADDITIVE (SHELL)	A/G	12,000	10,200
16	OIL/WATER SEP.	U/G	6,000	5,400

A/G: ABOVE GROUND A/U: UNDER GROUND 58603 -2010-06-30-mon-01 (annual sampling report-sci). Pdf



MOTIVA ENTERPRISES LLC TERMINAL 25 PAIDGE AVENUE BROOKLYN, NEW YORK NYSDEC SPILL NO. 87-09990

2010 ANNUAL SAMPLING REPORT

(July 2009 - June 2010)

June 30, 2010

PREPARED FOR:

SHELL OIL PRODUCTS US

Doug Weimer Senior Project Manager 4094 Majestic Lane PMB 224 Fairfax, VA 22033

PREPARED BY:

SOVEREIGN CONSULTING INC

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John McCollums Engineering Technician

Gregory Bosiljcic Project Manager

MOTIVA ENTERPRISES LLC TERMINAL 25 PAIDGE AVENUE BROOKLYN, NEW YORK NYSDEC SPILL NO. 87-09990 INCIDENT NO. 97094981

2010 ANNUAL SAMPLING REPORT (July 2009 – June 2010)

SITE STATUS

The site is an active Terminal and is under a NYSDEC Stipulation Agreement. During the reporting period, the site continues to be in the remediation phase using hand bailing to recover free product on a monthly basis. Groundwater monitoring will continue on an annual basis as will the recovery of free product.

SITE ACTIVITIES

- All monitoring wells not exhibiting separate phase product were sampled on April 15, 2010 consistent with the request made in a NYSDEC letter dated February 13, 2008 and the existing Stipulation Agreement. Each sample was analyzed utilizing EPA Method 8260 for VOCs with the addition of MTBE. Laboratory analysis reports are included in Appendix A.
- Gauging of all wells and hand bailing of product was performed on a monthly basis.
- Three additional monitoring wells, MW-42, MW-43 and MW-44 were installed along the buckeye pipeline in the southwest area of the site. Monitoring wells MW-7, MW-21 and MW-22 were abandoned during bulkhead wall installation. They were replaced with new monitoring wells MW-7R, MW-21R and MW-22R. Well construction logs for the newly installed monitoring wells are included in *Appendix B*.
- One 500-gallon AST from the deactivated skimming system was removed from the site in February 2010. Waste disposal documentation is included in *Appendix C*.

GROUNDWATER MONITORING

Number of Wells:

33

Gauging Frequency:

Monthly

Sampling Frequency: Recent Sample Dates:

Annually April 15, 2010

BTEX Range:

Below detection limit – 9,266 ug/l (MW-15)

MTBE Range:

Below detection limit – 145 ug/l (MW-20)

PRODUCT RECOVERY

Total Product Recovered:

1,201 gallons (as of May 2010)

Recent Gauging Date:

May 3, 2010

Wells Exhibiting Product since July 2009:

MW-2, MW-4, MW-26, MW-31, MW-34, MW-36, MW-37, MW-40, and MW-41

MW-36, MW-37, MW-40, and MW-41.

Maximum Product Thickness since July

1.96 ft (MW-40) (May 3, 2010)

2009:

HYDROGEOLOGY

Geology:

Geology consists of 12 ft. fine to coarse sand and gravel (fill material),

underlain by naturally occurring organic clay and silt (peat)

Depth to Water:

0.6 to 10.5 ft.

Flow Direction:

North - Northeast towards Newtown Creek under a gradient of 0.01 ft/ft

CONCLUSIONS AND RECOMMENDATIONS

- Review of historical BTEX and MTBE concentrations in the groundwater beneath the site indicates concentrations have generally decreased over time. Annual sampling of all wells will continue with the next sampling in April-May 2011.
- Based on the product thicknesses and the results of the product bail-down testing results completed in May 2005 (Documented in the 2005 Annual Report), product gauging and hand bailing recovery will continue.

ATTACHMENTS

- Table 1. Current Groundwater Analytical Results Summary.
- Table 2. Historical Groundwater Analytical Results Summary.
- Table 3. Groundwater Elevation Summary (2006-2010).
- Figure 1. Groundwater Contour Map April 15, 2010.
- Figure 2. Total BTEX/MTBE Concentrations in Groundwater April 15, 2010.
- Figure 3. LNAPL Thickness Contour Map April 15, 2010.
- Figure 4. Cumulative Product Recovery Graph.
- Appendix A. April 15, 2010 Groundwater Analysis Laboratory Reports.
- Appendix B. Well Construction Logs.
- Appendix C. Waste Disposal Documentation.

TABLES

Table 1 Current Groundwater Analytical Summary

Motiva Enterprises LLC Terminal # 58603

25 Paidge Avenue Brooklyn, New York NYSDEC SPILL NO. 87-09990

< GW Standard > MW-01 4/15/2010 MW-02 4/15/2010 NOT MW-03 4/15/2010 NOT MW-04 4/15/2010 NOT MW-05 4/15/2010 NOT MW-06 4/15/2010 A MW-07R 4/15/2010 A MW-08 4/15/2010 A MW-09 4/15/2010 A MW-13 4/15/2010 A MW-14 4/15/2010 A MW-15 4/15/2010 A MW-16 4/15/2010 A MW-17 4/15/2010 A MW-18 4/15/2010 A MW-21R 4/15/2010 A MW-22R 4/15/2010 A MW-23 4/15/2010 A MW-24 4/15/2010 A MW-25 4/15/2010 A MW-26 4/15/2010 A MW-27 4/15/2010 A MW-28 </th <th>nzene 0.7 ></th> <th>Toluene</th> <th>(ug/L</th> <th></th> <th></th> <th></th> <th>(ppm)</th> <th>(°C)</th>	nzene 0.7 >	Toluene	(ug/L				(ppm)	(°C)
Location Date Be		Taluana		Xylenes,	Total		ſ '	
< GW Standard > MWV-01 4/15/2010 NOT MWV-02 4/15/2010 NOT MWV-03 4/15/2010 NOT MWV-04 4/15/2010 NOT MWV-05 4/15/2010 NOT MWV-06 4/15/2010 A MWV-07R 4/15/2010 A MWV-08 4/15/2010 A MWV-09 4/15/2010 A MWV-13 4/15/2010 A MWV-14 4/15/2010 A MWV-15 4/15/2010 A MWV-16 4/15/2010 A MWV-17 4/15/2010 A MWV-18 4/15/2010 A MWV-20 4/15/2010 A MWV-21R 4/15/2010 A MWV-22R 4/15/2010 A MWV-23 4/15/2010 A MWV-24 4/15/2010 A MWV-25 4/15/2010 A MWV-29 4/15/2010 A			Ethylbenzene	Total	BTEX	MTBE	D.O.	Temp.
MW-01 4/15/2010 MW-02 4/15/2010 NOT MW-03 4/15/2010 NOT MW-04 4/15/2010 NOT MW-05 4/15/2010 NOT MW-06 4/15/2010 MW-07R 4/15/2010 MW-08 4/15/2010 MW-09 4/15/2010 MW-13 4/15/2010 MW-14 4/15/2010 MW-15 4/15/2010 MW-16 4/15/2010 MW-17 4/15/2010 MW-18 4/15/2010 MW-19 4/15/2010 MW-20 4/15/2010 MW-21R 4/15/2010 MW-22R 4/15/2010 MW-23 4/15/2010 MW-24 4/15/2010 MW-25 4/15/2010 MW-26 4/15/2010 MW-27 </th <th></th> <th>< 5 ></th> <th>< 5 ></th> <th><5></th> <th></th> <th>< 10 ></th> <th></th> <th></th>		< 5 >	< 5 >	<5>		< 10 >		
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MW-04 4/15/2010 NOT MW-05 4/15/2010 S 4/15	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	3.10	13.75
MW-05 4/15/2010 < MW-06 4/15/2010 < MW-06 4/15/2010 < MW-07R 4/15/2010 < MW-07R 4/15/2010 < MW-09 4/15/2010 < MW-09 4/15/2010 < MW-13 4/15/2010 < MW-14 4/15/2010 < MW-15 4/15/2010 < MW-15 4/15/2010 < MW-16 4/15/2010 < MW-17 4/15/2010 < MW-18 4/15/2010 < MW-18 4/15/2010 < MW-19 4/15/2010 < MW-20 4/15/2010 < MW-21R 4/15/2010 < MW-22R 4/15/2010 < MW-22R 4/15/2010 < MW-22R 4/15/2010 < MW-22 4/15/2010 < MW-24 4/15/2010 < MW-25 4/15/2010 < MW-25 4/15/2010 < MW-26 4/15/2010 < MW-27 4/15/2010 < MW-28 4/15/2010 < MW-29 4/15/2010 < MW-30 4/15/2010 < MW-31 4/15/2010 < MW-31 4/15/2010 < MW-31 4/15/2010 < MW-33 4/15/2010 < MW-34 4/15/2010 < MW-35 4/15/2010 < MW-36 4/15/2010 < MW-37 4/15/2010 < MW-38 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39		LED (PROD					ļ	
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MW-07R 4/15/2010 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	6.20	12.66
MVV-08 4/15/2010 4/15/2010 MVV-09 4/15/2010 4/15/2010 MVV-13 4/15/2010 4/15/2010 MVV-14 4/15/2010 4/15/2010 MVV-15 4/15/2010 4/15/2010 MVV-16 4/15/2010 4/15/2010 MVV-17 4/15/2010 4/15/2010 MVV-18 4/15/2010 4/15/2010 MVV-19 4/15/2010 4/15/2010 MVV-21R 4/15/2010 4/15/2010 MVV-22R 4/15/2010 MVV-23 4/15/2010 MVV-24 4/15/2010 MVV-25 4/15/2010 MV-26 4/15/2010 MV-28 4/15/2010 MV-30 4/15/2010 MV-31 4/15/2010 MV-32 4/15/2010 MV-33 4/15/2010 MV-34 4/15/2010 MV-36 4/15/2010 MV-	6.9	<5.00	<5.00	<5.00	16.9	31.5	2.65	10.31
MW-09 4/15/2010 MW-13 4/15/2010 MW-14 4/15/2010 MW-15 4/15/2010 MW-16 4/15/2010 MW-17 4/15/2010 MW-18 4/15/2010 MW-18 4/15/2010 MW-20 4/15/2010 MW-21R 4/15/2010 MW-21R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-23 4/15/2010 MW-24 4/15/2010 MW-25 4/15/2010 MW-26 4/15/2010 MW-27 4/15/2010 MW-28 4/15/2010 MW-29 4/15/2010 MW-30 4/15/2010 MW-31 4/15/2010 MW-31 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-35 4/15/2010 MW-36 4/15/2010 MW-37 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MM-39 4/15	4.9	<5.00	<5.00	<5.00	44.9	37.6	2.42	10.85
MVV-13 4/15/2010 MVV-14 4/15/2010 MVV-15 4/15/2010 MVV-16 4/15/2010 MVV-17 4/15/2010 MVV-18 4/15/2010 MVV-19 4/15/2010 MWV-21R 4/15/2010 MWV-22R 4/15/2010 MWV-22R 4/15/2010 MWV-23 4/15/2010 MWV-24 4/15/2010 MWV-25 4/15/2010 MWV-26 4/15/2010 MWV-28 4/15/2010 MWV-30 4/15/2010 MW-31 4/15/2010 MW-32 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-36 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MW-	2.5	<5.00	<5.00	<5.00	12.5	15.2	2.89	11.80
MW-14 4/15/2010 S WW-15	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	2.31	11.79
MW-15 4/15/2010 MW-16 4/15/2010 MW-17 4/15/2010 MW-18 4/15/2010 MW-19 4/15/2010 MW-20 4/15/2010 MW-21R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-24 4/15/2010 MW-25 4/15/2010 MW-26 4/15/2010 MW-26 4/15/2010 MW-27 4/15/2010 MW-28 4/15/2010 MW-29 4/15/2010 MW-30 4/15/2010 MW-31 4/15/2010 MW-31 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-35 4/15/2010 MW-36 4/15/2010 MW-37 4/15/2010 MW-37 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MM-39 4/15	5.00	<5.00	<5.00	< 5.00	<5.00	<5.00	2.93	12.72
MW-16 4/15/2010 3 MW-17 4/15/2010 3 MW-18 4/15/2010 3 MW-19 4/15/2010 4 MW-20 4/15/2010 4 MW-21R 4/15/2010 3 MW-21R 4/15/2010 3 MW-22R 4/15/2010 3 MW-22R 4/15/2010 3 MW-23 4/15/2010 3 MW-24 4/15/2010 3 MW-25 4/15/2010 3 MW-26 4/15/2010 3 MW-27 4/15/2010 3 MW-28 4/15/2010 3 MW-29 4/15/2010 3 MW-30 4/15/2010 3 MW-31 4/15/2010 3 MW-31 4/15/2010 3 MW-32 4/15/2010 3 MW-33 4/15/2010 3 MW-34 4/15/2010 3 MW-35 4/15/2010 3 MW-36 4/15/2010 3 MW-37 4/15/2010 3 MW-38 4/15/2010 3 MW-39 4/15/2010 3 MW-39 4/15/2010 3 MW-39 4/15/2010 3 MW-39 4/15/2010 3 MW-39 4/15/2010 3	339	4,350	556	3,521	9,266	38.8	1.40	15.56
MW-17 4/15/2010 S MW-18 4/15/2010 S MW-19 4/15/2010 S MW-20 4/15/2010 S MW-21R 4/15/2010 S MW-22R 4/15/2010 S MW-22R 4/15/2010 S MW-23 4/15/2010 S MW-24 4/15/2010 S MW-25 4/15/2010 S MW-26 4/15/2010 S MW-27 4/15/2010 S MW-28 4/15/2010 S MW-29 4/15/2010 S MW-30 4/15/2010 S MW-31 4/15/2010 S MW-31 4/15/2010 S MW-33 4/15/2010 S MW-34 4/15/2010 S MW-35 4/15/2010 S MW-36 4/15/2010 S MW-37 4/15/2010 S MW-38 4/15/2010 S MW-39 4/15/2010 S MW-39 4/15/2010 S MW-39 4/15/2010 S MW-39 4/15/2010 S MW-40 4/15/2010 S	7.6	<5.00	<5.00	5.22	42.82	14.6	1.23	16.68
MW-18 4/15/2010 3 3 4/15/2010 MW-21R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-22 4/15/2010 MW-25 4/15/2010 MW-26 4/15/2010 MW-26 4/15/2010 MW-27 4/15/2010 MW-28 4/15/2010 MW-29 4/15/2010 MW-30 4/15/2010 MW-31 4/15/2010 MW-31 4/15/2010 MW-32 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-35 4/15/2010 MW-36 4/15/2010 MW-37 4/15/2010 MW-38 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MM-39 4/15/2010 MW-39 4/15/2010 MW-39 4/15/2010 MW-39 4/15/2010 MM-39 4/15/2	5.00	< 5.00	<5.00	<5.00	<5.00	5.1	1.66	15.47
MW-19 4/15/2010 MW-20 4/15/2010 MW-21R 4/15/2010 MW-21R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-25 4/15/2010 MW-26 4/15/2010 MW-27 4/15/2010 MW-28 4/15/2010 MW-29 4/15/2010 MW-30 4/15/2010 MW-31 4/15/2010 MW-31 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-35 4/15/2010 MW-36 4/15/2010 MW-37 4/15/2010 MW-37 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MM-39 4/15	6.6	5.08	13.3	16.9	71.88	<5.00	1.88	16.38
MW-20 4/15/2010 MW-21R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-22 4/15/2010 MW-25 4/15/2010 MW-26 4/15/2010 MW-27 4/15/2010 MW-28 4/15/2010 MW-29 4/15/2010 MW-30 4/15/2010 MW-31 4/15/2010 MW-32 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-35 4/15/2010 MW-36 4/15/2010 MW-37 4/15/2010 MW-38 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MM-39 4/15	1.2	6.34	<5.00	44.9	62.44	5.59	1.50	15,55
MW-21R 4/15/2010 MW-22R 4/15/2010 MW-22R 4/15/2010 MW-23 4/15/2010 MW-24 4/15/2010 MW-25 4/15/2010 MW-26 4/15/2010 MW-27 4/15/2010 MW-28 4/15/2010 MW-29 4/15/2010 MW-30 4/15/2010 MW-31 4/15/2010 MW-32 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-35 4/15/2010 MW-36 4/15/2010 MW-37 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MW-39 4/15/2010 MW-39 4/15/2010 MW-40 4/15/2010 MW-40 4/15/2010 MW-40 4/15/2010 MW-40 MM-40	197	43.2	20.4	84.9	645.5	145	1.39	15.49
MW-22R 4/15/2010	139	12.2	41.5	54.6	247.3	<5.00	2.41	11.74
MW-23 4/15/2010 < MW-24 4/15/2010 < MW-25 4/15/2010 < MW-26 4/15/2010 < MW-26 4/15/2010 < MW-27 4/15/2010 < MW-28 4/15/2010 < MW-29 4/15/2010 < MW-30 4/15/2010 < MW-31 4/15/2010 < MW-31 4/15/2010 < MW-32 4/15/2010 < MW-33 4/15/2010 < MW-34 4/15/2010 < MW-35 4/15/2010 < MW-36 4/15/2010 < MW-36 4/15/2010 < MW-37 4/15/2010 < MW-38 4/15/2010 < MW-38 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-39 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2010 < MW-40 4/15/2	386	68.4	2140	111.2	2705.6	42.8	2.42	11.78
MW-24 4/15/2010 < MW-25 4/15/2010 < MW-26 4/15/2010 NOT MW-27 4/15/2010 < MW-28 4/15/2010 < MW-29 4/15/2010 MW-30 4/15/2010 NOT MW-31 4/15/2010 MW-32 4/15/2010 MW-33 4/15/2010 MW-34 4/15/2010 MW-35 4/15/2010 MW-36 4/15/2010 MW-37 4/15/2010 MW-38 4/15/2010 MW-38 4/15/2010 MW-39 4/15/2010 MW-39 4/15/2010 MW-40 4/15/2010 NOT MW	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	2.07	13.99
MW-25 4/15/2010	5.00	<5.00	<5.00	<5.00	<5.00	6,63	2.05	13.75
MW-26 4/15/2010 NOT MW-27 4/15/2010 <	5,00	<5.00	<5.00	<5.00	<5.00	<5.00	1.30	14.77
MVV-27 4/15/2010 < MVV-28 4/15/2010 < MVV-29 4/15/2010 < MVV-30 4/15/2010 < MVV-31 4/15/2010 < MVV-32 4/15/2010 < MVV-33 4/15/2010 < MVV-33 4/15/2010 < MVV-34 4/15/2010 < MVV-35 4/15/2010 < MVV-36 4/15/2010 < MVV-37 4/15/2010 < MVV-38 4/15/2010 < MVV-38 4/15/2010 < MVV-39 4/15/2010 < MVV-39 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2010 < MVV-40 4/15/2		LED (PROI					İ	
MVV-28 4/15/2010 < MVV-29 4/15/2010 < MVV-30 4/15/2010 < MVV-31 4/15/2010 < MVV-32 4/15/2010 < MVV-33 4/15/2010 < MVV-34 4/15/2010 MVV-35 4/15/2010 MVV-36 4/15/2010 MVV-37 4/15/2010 MVV-38 4/15/2010 MVV-39 4/15/2010 MVV-39 4/15/2010 MVV-40 4/15/2010 NOT	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.91	16.16
MW-29 4/15/2010	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.58	15.60
MW-30 4/15/2010 < MW-31 4/15/2010 NOT MW-32 4/15/2010 NOT MW-33 4/15/2010 NOT MW-34 4/15/2010 NOT MW-35 4/15/2010 NOT MW-37 4/15/2010 NOT MW-38 4/15/2010 MW-39 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 MW-40 NOT MW-31 MW-40 MW-40 MW-40 NOT MW-31 MW-40	122	<5.00	<5.00	<5.00	122	<5.00	2.44	15.08
MW-31 4/15/2010 NOT MW-32 4/15/2010 < MW-33 4/15/2010 NOT MW-34 4/15/2010 NOT MW-35 4/15/2010 NOT MW-36 4/15/2010 NOT MW-38 4/15/2010 MW-39 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 MW-40 MOT MW-31 NOT MW-40 MW-40 MOT MW-40 MOT MW-40 MOT MW-40 MOT MW-40 MOT MW-40 MOT MOT MOT MOT MW-40 MOT MOT MOT MOT MOT MOT MOT MOT MOT MOT	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.94	16,17
MW-32 4/15/2010 < MW-33 4/15/2010 NOT MW-34 4/15/2010 NOT MW-35 4/15/2010 NOT MW-36 4/15/2010 NOT MW-37 4/15/2010 NOT MW-38 4/15/2010 < MW-39 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 MW-40 MOT MATCH MA		LED (PRO					,	
MW-33 4/15/2010 NOT MW-35 4/15/2010 NOT MW-36 4/15/2010 NOT MW-37 4/15/2010 NOT MW-38 4/15/2010 NOT MW-39 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 4/15/2010 NOT	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.70	16.47
MW-34 4/15/2010 NOT MW-35 4/15/2010 NOT MW-36 4/15/2010 NOT MW-37 4/15/2010 NOT MW-38 4/15/2010 CMW-39 4/15/2010 NOT MW-40 4/15/2010 NOT MW-40 4/15/2010 NOT	223	<5.00	<5.00	<5.00	223	61.9	1.78	14.87
MW-35 4/15/2010 NOT MW-36 4/15/2010 NOT MW-37 4/15/2010 NOT MW-38 4/15/2010 MW-39 4/15/2010 NOT MW-40 4/15/2010 NOT		LED (PROI]	
MW-36 4/15/2010 NOT MW-37 4/15/2010 NOT MW-38 4/15/2010 < MW-39 4/15/2010 6 MW-40 4/15/2010 NOT	765	9.78	<5.00	<5.00	774.78	97.4	1.21	15,42
MW-37 4/15/2010 NOT MW-38 4/15/2010 < MW-39 4/15/2010 6 MW-40 4/15/2010 NOT		LED (PROE						
MW-38 4/15/2010 < MW-39 4/15/2010 6 MW-40 4/15/2010 NOT		LED (PRO	•				}	
MW-39 4/15/2010 6 MW-40 4/15/2010 NOT	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.68	17.57
MW-40 4/15/2010 NOT	5.9	<5.00	<5.00	<5.00	65.9	36.7	1.42	15.09
1 .		LED (PRO)	
		LED (PROE	•					
*****	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.84	13,92
	5.00	<5.00	<5,00	<5.00	<5.00	17.5	1.97	14.91
	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.39	14.63
*****		SSIBLE (FL				-		
	5.00	<5.00	<5.00	<5.00	<5.00	<5.00	1.44	13,62
		SSIBLE (FL						
		SSIBLE (FL						
		SSIBLE (FL					}	
		LED (PROD						

Notes:

GW Standard ≈ Values in **bold and italic** exceed the Groundwater Standard.

 μ g/L = micrograms per liter, or parts per billion (ppb)

<X = Parameter detected below the method limit of quantitation (X).

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)							
Sample					Xylenes,	Total	MTDC		
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE		
< GW Sta		< 0.7 >	<5>	< 5 >	< 5 >	N.5	< 10 >		
MW-01	8/14/1989	ND	ND	ND	ND	ND	NA		
MW-01	11/14/1989	ND	ND	ND	ND	ND	NA		
MW-01	2/13/1990	ND	ND	ND	ND	ND	NA		
MW-01	5/4/1990	ND	ND	ND	ND	ND	NA		
MW-01	5/8/1991	ND	ND	ND	ND	ND	NA		
MW-01	5/13/1992	ND	ND	ND	ND	ND	NA		
MW-01	5/12/1993	ND	ND	ND	ND	ND	NA		
MW-01	5/10/1994	ND	ND	ND	ND	ND	NA		
MW-01	5/22/1995	ND	ND	ND	ND	ND	NA		
MW-01	5/23/1996	ND	ND	ND	ND	ND	NA		
MW-01	6/18/1997	ND	ND	ND	ND	ND	NA		
MW-01	5/29/1998	ND	ND	ND	ND	ND	NA		
MW-01	5/11/1999	ND	ND	ND	ND	ND	NA		
MW-01	10/27/1999	ND	ND	ND	ND	ND	2		
MW-01	6/7/2000	ND	ND	ND	ND	ND	ND		
MW-01	5/29/2001	ND	ND	ND	ND	ND	ИD		
MW-01	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	< 1.0		
MW-01	6/30/2003	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-01	6/15/2004	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-01	6/7/2005	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-01	6/28/2006	<1.00	<1.00	<1.00	<1.00	<6.00	<1.00		
MW-01	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-01	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-01	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-01	4/15/2010_	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00		
MW-02	6/8/2005	172	5.5	3.2	16.4	197.1	6.3		
MW-02	5/12/2008	NOT SAMPI	ED (PRODU	JCT)					
MW-02	4/29/2009	NOT SAMPI	ED (PRODU	JCT)					
MW-02	4/15/2010_	NOT SAMP	ED (PRODU	JCT)					
MW-03	8/14/1989	ND	ND	ND	ND	ND	NA		
MW-03	11/14/1989	ND	ND	ND	ND	ND	NA		
MW-03	2/13/1990	ND	ND	ND	ND	ND	NA		
MW-03	5/4/1990	ND	ND	ND	ND	ND	NA		
MW-03	5/8/1991	ND	ND	ND	ND	ND	NA		
MW-03	5/13/1992	ND	ND	ND	ND	ND	NA		
MW-03	5/12/1993	ND	ND	ND	ND	ND	NA		
MW-03	5/10/1994	ND	ND	ND	ND	ND	NA		
MW-03	5/22/1995	ND	ND	ND	ND	ND	NA		
MW-03	5/23/1996	ND	ND	ND	ND	ND	NA		
WW-03	6/18/1997	ND	ND	ND	ND	ND	NA		
MW-03	5/29/1998	ND	ND	ND	ND	ND	NA		
WW-03	5/11/1999	ND	ND	ND	ND	ND	NA		
MW-03	10/27/1999	ND	ND	ND	ND	ND	1.2		
MW-03	6/7/2000	ND	ND	ND	ND	ND	ND		
MW-03	5/29/2001	ND	ND	ND	ND	ND	2.1		
MW-03	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	< 1.0		
MW-03	6/30/2003	0.97	0.70	<1.0	<1.0	1.67	<1.0		
MW-03	6/15/2004	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	<1.0		
MW-03	6/7/2005	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	<1.0		
MW-03	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-03	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-03	5/12/2008	<1.00	<1.00	<1.00	<1.0	<4.0	<1.0		
MW-03	5/12/2008 4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
	4/23/2009	→1. 0	~1.0	-1,U	- 1.4	,			

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)							
Sample					Xylenes,	Total			
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE		
< GW Sta		< 0.7 >	<5>	< 5 >	< 5 >		< 10 >		
MW-04	5/12/1993	1.8	ND	2	12	15.8	NA		
MW-04	5/10/1994	ND	ND	ND	ND	ND	NA		
MW-04	6/18/1997	ND	ND	0.49	ND	0.49	NA		
MVV-04	6/30/2003	<2.5	<2.5	<2.5	<2.5	<10	38.8		
MW-04	6/15/2004	<1.0	<1.0	<1.0	<1.0	<4.0	24.8		
MW-04	6/7/2005	<1.0	<1.0	<1.0	<1.0	<4.0	11.6		
MW-04	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-04	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	3.1		
MW-04	4/15/2010	NOT SAMPL	ED (PRODL	CT)					
MW-05	8/14/1989	ND	ND	ND	ND	ND	NA		
MVV-05	11/14/1989	ND	ND	ND	ND .	ND	NA		
MW-05	2/13/1990	4.6	ND	ND	2	6.6	NA		
MW-05	5/4/1990	2.9	ND	ND	ND	2.9	NA		
MW-05	5/8/1991	ND	ND	ND	ND	ND	NA		
MW-05	5/13/1992	ND	ND	ND	ND	ND	NA		
MW-05	5/12/1993	ND	ND	ND	ND	ND	NA		
MVV-05	5/10/1994	ND	ND	ND	ND	ND	NA		
MW-05	5/22/1995	ND	ND	ND	ND	ND	NA		
MW-05	5/23/1996	ND	ND	ND	ND	ND	NA ·		
MW-05	6/18/1997	ND	ND	0.29	ND	0.29	NA		
MW-05	5/29/1998	ND	ND	ND	ND	ND	NA		
MW-05	5/11/1999	ND	ND	ND	ND	ND	NA		
MW-05	10/27/1999	ND	ND	ND	ND	ND	228		
MW-05	6/7/2000	ND	ND	ND	ND	ND	19.7		
MW-05	5/29/2001	ND	ND	ND	ND	ND	18.5		
MW-05	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	17		
MW-05	6/30/2003	<1.0	<1.0	<1.0	<1.0	<4.0	17.1		
MVV-05	6/15/2004	88.9	10	7.8	32.4	139	38.9		
MW-05	6/7/2005	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-05	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-05	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-05	5/12/2008	Not Accessib	le (Underwat	er/Flooded)					
MW-05	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MVV-05	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00		

Table 2 Historical Groundwater Analytical Results Summary (Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)							
Sample					Xylenes,	Total	*****		
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE		
< GW Sta		< 0.7 >	<5>	< 5 >	< 5 >		< 10 >		
MW-06	8/14/1989	ND	ND	ND	ND	ND	NA		
MVV-06	11/14/1989	ND	ND	ND	ND	ND	NA		
MW-06	2/13/1990	ND	ND	ND	ND	ND	NA		
MW-06	5/4/1990	ND	ND	ND	ND	ND	NA		
MW-06	5/8/1991	ND	ND	ND	ND	ND	NA		
MW-06	5/13/1992	ND	ND	ND	ND	ND	NA		
MW-06	5/12/1993	ND	ND	ND	ND	ND	NA		
MW-06	5/10/1994	ND	ND	ND	ND	ND	NA		
MW-06	5/23/1996	ND	ND	ND	ND	ND	NA		
MW-06	5/29/1998	ND	ND	ND	ND	ND	NA		
MW-06	5/11/1999	ND	ND	ND	ND	ND	NA		
MW-06	10/27/1999	ND	ND	ND	ND	ND	28.7		
MW-06	6/7/2000	ND	ND	ND	ND	ND	10.5		
MW-06	5/29/2001	ND	ND	ND	ND	ND	ND		
MW-06	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	< 1.0		
MW-06	6/30/2003	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	13.4		
MW-06	6/15/2004	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	<1.0		
MW-06	6/7/2005	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	<1.0		
MW-06	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-06	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-06	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-06	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-06	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00		
MW-07	8/14/1989	ND	ND	ND	ND	ND	NA		
MW-07	11/14/1989	ND	ND	ND	ND	ND	NA		
MW-07	2/13/1990	ND	ND	ND	ND	ND	NA		
MW-07	5/4/1990	ND	ND	ND	ND	ND	NA		
MW-07	5/8/1991	ND	ND	ND	ND	ND	NA		
MW-07	5/13/1992	ND	ND	ND	ND	ND	NA		
MW-07	5/12/1993	ND	ND	ND	ND.	ND	NA		
MW-07	5/10/1994	ND	ND	ND	ND	ND	NA		
MW-07	5/22/1995	ND	ND	ND	ND	ND	NA		
MW-07	5/23/1996	ND	ND	ND	ND	ND	NA		
MW-07	6/18/1997	ND	ND	ND	ND	ND	NA		
MW-07	5/29/1998	ND	ND	ND	ND	ND	NA		
MW-07	5/11/1999	ND	ND	ND	ND	ND	NA		
MW-07	10/27/1999	ND	ND	ND	ND	ND	1.3		
MW-07	6/7/2000	ND	ND	ND	ND	ND	ND		
MW-07	5/29/2001	ND	ND	ND	ND	ND	4.0		
MW-07									
MW-07	5/30/2002 6/30/2003	< 1.0 < 1.0	< 1.0 < 1.0	< 1.0 < 1.0	< 5.0 < 1.0	< 8.0 <4.0	1.4 13.4		
MW-07	1	< 1.0							
	6/15/2004		< 1.0	< 1.0	< 1.0	<4.0	1.8		
MW-07	6/7/2005	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	<1.0		
MW-07	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-07	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-07	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-07R	4/15/2010	16.9	<5.00	<5.00	<5.00	16,9	31.5		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)						
Sample					Xylenes,	Total		
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE	
< GW Sta		< 0.7 >	< 5 >	< 5>	< 5 >		< 10 >	
MW-08	8/14/1989	ND	ND	ND	ND	ND	NA	
MW-08	11/14/1989	ND	ND	ND	ND	ND	NA	
MW-08	2/13/1990	ND	ND	ND	ND	ND	NA	
MW-08	5/4/1990	ND	ND	ND	ND	ND	NA	
MW-08	5/8/1991	ND	ND	ND	ND	ND	NA	
MW-08	5/13/1992	ND	ND	ND	ND	ND	NA	
MW-08	5/12/1993	9.5	ND	ND	ND	9.5	NA	
MW-08	5/10/1994	1.7	ND	ND	ND	1.7	NA	
MW-08	5/22/1995	ND	ND	ND	ND	ND	NA	
MW-08	5/23/1996	ND	ND	ND	ND	ND	NA	
MW-08	6/18/1997	ND	ND	ND	ND	ND	NA	
MW-08	5/29/1998	ND	ND	ND	ND	ND	NA	
WW-08	5/11/1999	ND	ND	ND	ND	ND	NA	
MW-08	10/27/1999	ND	ND	ND	ND	ND	3.20	
MW-08	6/7/2000	ND	ND	ND	ND	ND	21.0	
MVV-08	5/29/2001	0.43	ND	ND	ND	0.43	39.0	
MW-08	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	1.9	
MVV-08	6/30/2003	18.3	<1.0	<1.0	<1.0	18.3	58.2	
MW-08	6/15/2004	1.5	<1.0	<1.0	<1.0	1.5	8.50	
MW-08	6/7/2005	<1.0	<1.0	<1.0	<1.0	<4.0	5,80	
MW-08	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	5.00	
MW-08	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	6,20	
MW-08	5/15/2009	2.4	<1.0	<1.0	<1.0	2.4	6.6	
MW-08	4/15/2010	44.9	<5.00	<5.00	<5.00	44.9	37.6	
MW-09	5/12/1993	ND	ND	ND	ND	ND	NA	
MW-09	5/10/1994	ND	ND	ND	ND	ND	NA	
MW-09	5/22/1995	ND	ND	ND	ND	ND	NA	
MW-09	5/23/1996	ND	ND	ND	ND	ND	NA	
MW-09	6/18/1997	ND	ND	ND	ND	ND	NA	
MW-09	5/29/1998	ND	ND	ND	ND	ND	NA	
MW-09	5/11/1999	ND	ND	ND	ND	ND	NA	
MW-09	10/27/1999	ND	ND	ND	ND	ND	6.5	
MW-09	6/7/2000	ND	ND	ND	ND	ND	ND	
MW-09	5/29/2001	ND	ND	ND	ND	ND	3.3	
MW-09	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8,0	< 1.0	
MW-09	6/30/2003	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	9.2	
MW-09	6/15/2004	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	0.79	
MW-09	6/7/2005	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	5.0	
MW-09	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00	
MW-09	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00	
MW-09	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.00	
MW-09	5/15/2009	<1.0	<1.0	<1.0	<1.0	<4.0	4.7	
MW-09	4/15/2010	12.5	<5.00	<5.00	<5.00	12.5	15.2	

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)						
Sample					Xylenes,	Total		
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE	
< GW Standard >		< 0.7 >	<5>	< 5 >	< 5 >		< 10 >	
MW-13	8/14/1989	ND	ND	ND	ND	ND	NA	
MW-13	11/14/1989	ND	ND	ND	ND	ND	NA	
MW-13	2/13/1990	ND	ND	ND	ND	ND	NA	
MW-13	5/4/1990	ND	ND	ND	ND	ND	NA	
MW-13	5/8/1991	ND	ND	ND	ND	ND	NA NA	
MW-13	5/13/1992	ND	ND	ND	ND	ND	NA	
MW-13	5/12/1993	8.6	ND	ND	ND	8.6	NA	
MW-13	5/10/1994	ND	ND	ND	ND	ND	NA	
MVV-13	5/22/1995	ND	ND	ND	ND	ND	NA	
MW-13	6/18/1997	1.4	ND	ND	1.4	2.8	NA	
MW-13	5/29/1998	1.2	ND	ND	ND	1.2	NA	
MW-13	5/11/1999	ND	ND	ND	ND	ND	NA	
MW-13	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	7.4	
MW-13	6/30/2003	< 1.0	< 1.0	< 1.0	< 1.0	<4.0	<1.0	
MW-13	6/15/2004	0.37 ^J	<1.0	<1.0	<1.0	0.37 ^J	1.1	
MW-13	6/8/2005	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0	
MW-13	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00	
MVV-13	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00	
MW-13	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0	
MW-13	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0	
MW-13	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00	
MW-14	8/14/1989	2.5	1.7	4.4	4.9	13.5	NA	
MW-14	11/14/1989	6.7	ND	1	ND	7.7	NA	
MW-14	2/13/1990	60	5.4	ND	18	83.4	NA	
MW-14	5/4/1990	68	2.3	8.1	7.1	85.5	NA	
MW-14	5/8/1991	43	2.6	6.5	7.2	59.3	NA	
MW-14	5/13/1992	97	4.8	8.5	12	122.3	NA	
MW-14	5/12/1993	45	2.1	4.9	7.8	59.8	NA	
MW-14	5/10/1994	57	2.1	2.7	8.3	70.1	NA	
MW-14	5/22/1995	33	1.8	1.1	5.9	41.8	NA	
MW-14	5/23/1996	25.7	1.6	1.3	6.6	35.2	NA	
MW-14	6/18/1997	13.1	1.1	0.98	5.3	20.48	NA	
MW-14	5/29/1998	24.6	2	2.2	9.6	38.4	NA	
MW-14	5/11/1999	19	ND	0.83	2.2	22.03	NA	
MW-14	10/27/1999	24.4	1.3	ND	4.8	30.5	ND	
MW-14	6/7/2000	1.5	ND	ND	ND	1.5	ND	
MW-14	5/29/2001	16.1	0,67	ND	3.2	19.97	ND	
MW-14	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	< 1.0	
MW-14	6/30/2003	1.9	< 1.0	< 1.0	< 1.0	1.9	<1.0	
MW-14	6/15/2004	5.8	<1.0	<1.0	1.3	7	<1.0	
MW-14	6/8/2005	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0	
MW-14	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00	
MW-14	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00	
MW-14	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0	
MW-14	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0	
MW-14	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00	

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

				(ug/	L)		
Sample					Xylenes,	Total	
Location	Date	Benzene < 0.7 >	Toluene	Ethylbenzene	Total	BTEX	MTBE
< GW Sta	< GW Standard >		< 5 >	< 5 >	< 5 >		< 10 >
MW-15	5/10/1994	1,200	48	130	130	1,508	NA
MVV-15	6/18/1997	1,600	624	686	3,300	6,210	NA
MW-15	5/11/1999	162.0	ND	122	408.0	692	NA
MW-15	10/27/1999	1,360	176	740	2,350	4,626	8,080
MW-15	6/7/2000	1,050	143	58 <i>4</i>	1,330	3,107	2,120
MW-15	5/29/2001	507	81.3	386	500	1,474	1,430
MW-15	6/30/2003	281	21	158	250	710	52.7
MW-15	6/7/2005	280	18.7	30.6	53.3	383	45.2
MW-15	6/28/2006	361	28.0	22.7	44.9	457	47.3
MW-15	6/26/2007	234	15.6	21.2	48.6	319	<i>54.7</i>
MW-15	5/12/2008	264	19.4	26.2	71.2	381	40.9
MW-15	4/29/2009	165	20.4	13.7	121	320	45.9
MW-15	4/15/2010	839	4,350	<i>5</i> 56	3,521	9,266	38.8
MW-16	8/14/1989	300	310	43	240	893	NA
MW-16	11/14/1989	ND	ND	ND	ND	ND	NA
MW-16	5/12/1993	73	ND	10	17	100	NA
MW-16	5/10/1994	46	ND	1,6	4.1	51.7	NA
MW-16	6/18/1997	2,470	17,800	3,760	19,900	43,930	NA
MW-16	5/11/1999	1,040	350	469	3,900	5,759	NA
MW-16	6/30/2003	331	47.7	76. 4	118	573	335
MW-16	6/15/2004	218	12.1	107	118	455	197
MW-16	6/7/2005	225	7.6	29.2	26.0	288	32.6
MW-16	6/28/2006	52.6	2.88	6.59	8.90	71.0	5.88
MW-16	6/26/2007	99.8	6.20	4.93	17.1	128	34.2
MW-16	5/12/2008	83.8	4.10	2.00	20.7	111	13.4
MW-16	4/29/2009	56.2	5.3	2.2	15.2	78.9	26.7
MW-16	4/15/2010	37.6	<5.00	<5,00	5.22	42.82	14.6
MW-17	8/14/1989	900	2,600	600	3,300	7,400	NA
MW-17	11/14/1989	400	1,200	590	2,700	4,890	NA
MW-17	2/13/1990	410	960	ND	3,100	4,470	NA
MW-17	5/12/1993	290	24	70	130	514	NA
MW-17	5/10/1994	82	10	30	48	170	NA
MW-17	5/29/1998	347	435	797	5,220	6,799	NA
MW-17	5/11/1999	133	42	162	370	707	NA
MW-17	10/27/1999	213	161	615	2,150	3,139	96.4
MW-17	6/7/2000	136	30.7	77.8	229	474	254
MW-17	5/29/2001	70.9	16.5	78.7	170	336	ND
MW-17	5/30/2002	53	7.1	12.9	14	87	13.4
MW-17	6/30/2003	13.9	5.3	3.9	17.2	40	12.5
MW-17	6/15/2004	13	3.1	1.4	8.7	26	6.8
MW-17	6/7/2005	54.3	4.0	1.9	24.7	85	16.1
MW-17	6/28/2006	3.37	<1.00	<1.00	<3.00	3.37	3.59
MW-17	6/26/2007	67.7	4.44	1,54	25.2	98.9	11.8
MW-17	5/12/2008	44.2	3.70	<1.0	27.9	75.8	8.00
MW-17 MW-17	4/29/2009 4/15/2010	30.1 <5.00	2.8 <5.00	<1.0 <5.00	17.2 <5.00	50.1 <5.00	4.6 5.1

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603 25 Paidge Avenue

		(ug/L)							
Sample					Xylenes,	Total	·		
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE		
< GW Sta	ndard >	< 0.7 >	< 5 >	< 5 >	< 5 >		< 10 >		
MW-18	8/14/1989	1,100	2,500	580	2,900	7,080	NA		
MW-18	11/14/1989	680	770	590	2,900	4,940	NA		
MW-18	2/13/1990	630	570	ND	3,100	4,300	NA		
MW-18	5/4/1990	420	540	420	2,800	4,180	NA		
MW-18	5/13/1992	480	78	380	580	1,518	NA		
MW-18	5/12/1993	59 0	400	61	420	1,471	NA		
MW-18	5/10/1994	210	20	70	130	430	NA		
MW-18	5/22/1995	5,900	19,000	1,600	12,000	38,500	NA		
MW-18	5/23/1996	1,520	12,600	2,750	15,200	32,070	NA		
MW-18	6/18/1997	794	1,140	2,280	11,200	15,414	NA		
MW-18	5/29/1998	1,010	294	2,300	8,140	11,744	NA		
MW-18	5/11/1999	501	127	1,690	3,030	5,348	NA		
MW-18	10/27/1999	432	95.6	1,190	779	2,497	178		
MW-18	6/7/2000	378	85.2	1,240	1,080	2,783	704		
MW-18	5/29/2001	184	47	601	279	1,111	79		
MW-18	5/30/2002	104	19	424	48.5	595.9	22.8		
MW-18	6/30/2003	42.2	11	154	37.5	245	12.8		
MW-18	6/15/2004	71.7	10.4	39	19,9	141	14.9		
MW-18	6/7/2005	97	7.9	13.2	35.0	153	18.4		
MW-18	6/28/2006	31.8	4.84	29.3	15.4	81.3	8.77		
MW-18	6/26/2007	83.1	8.33	12.1	25.6	129	12.2		
MW-18	5/12/2008	49.8	4.00	7.50	21.9	83.2	3.70		
MW-18	4/29/2009	76.9	4.8	7.7	33.4	123	6.6		
MW-18	4/15/2010	36.6	5.08	13,3	16.9	71.88	<5.00		
MW-19	5/30/2002	165	4,8	3,6	10.3	184	56.9		
MW-19	6/30/2003	76.7	9.9	6.5	45.5	139	19.8		
MW-19	6/15/2004	179	15.8	6.1	37	238	20.4		
MW-19	6/7/2005	194	12,4	8.8	41.3	257	16.8		
MW-19	6/28/2006	49.5	2.74	<1.00	9.16	61,4	11.9		
MW-19	6/26/2007	114	4.91	2.27	17.7	139	12.0		
MW-19	5/12/2008	11.4	<1.0	<1.0	1.60	13.0	4.20		
MW-19	4/29/2009	7.5	1.5	<1.0	2.9	11.9	7.7		
MW-19	4/15/2010	11.2	6.34	<5.00	44.9	62.44	5.59		
MW-20	5/12/1993	410	ND	180	62	652	NA NA		
MW-20	6/30/2003	525	103	34.9	178	841	3,440		
MW-20	6/15/2004	443	95.5	48.1	353	940	220		
MW-20	6/7/2005	861	25.1	38.9	90.1	1,015	230		
MW-20	6/28/2006	1,420	2,260	36.9 342	3,730	7,752	230 341		
MW-20	6/26/2007	1,320	263	98.7	1,420	3,102	341 188		
MW-20	5/12/2008	636	203 19.7	96.7 45.4	1,420	820	100		
MW-20	4/29/2009	59.7	2.5	7.3	719 5.9	75.4			
MW-20	4/29/2009	99.7 497	43.2	20.4	5.9 84.9	75.4 645.5	56.6 145		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)						
Sample					Xylenes,	Total		
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE	
< GW Sta	ndard >	< 0.7 >	<5>	<5>	< 5 >		< 10 >	
MW-21	5/8/1991	140	6.5	12.0	41	199.5	NA	
MW-21	5/13/1992	20	5.6	15.0	54	94.6	NA	
MW-21	5/12/1993	66	17	40	160	283	NA	
MW-21	5/10/1994	41	12	46	170	269	NA	
MW-21	5/22/1995	14	9.1	31	130	184.1	NA	
MW-21	6/18/1997	18.4	ND	32.7	122	173.1	NA	
MW-21	5/29/1998	3.4	0.68	4.5	15.1	23.68	NA	
MW-21	5/11/1999	56.9	10.8	61.5	201	330.2	NA	
MW-21	10/27/1999	13.4	ND	11.1	41.6	66.1	275	
MW-21	6/7/2000	6.6	1.6	6.6	24.4	39.2	214	
MW-21	5/29/2001	5.2	1,4	8.6	25.2	40.4	110	
MW-21	5/30/2002	1.6	< 1.0	1.5	5.1	8.2	28.9	
MW-21	6/30/2003	10.5	0.66 ^J	3.2	11.4	25	156	
MW-21	6/15/2004	1.4	0.36	0.79 ^J	2,8	5.4	48.4	
MW-21	6/8/2005	<1.0	<1.0	<1,0	<1.0	<4.0	65.3	
MW-21	6/28/2006	<.1.00	<1.00	<1.00	<3.00	<6.00	50.0	
MW-21	6/26/2007	7.07	<1.00	5.57	14.6	27.2	10.7	
MW-21	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	93.2	
MW-21R	4/15/2010	139	12.2	41.5	54.6	247.3	<5.00	
MW-22	5/12/1993	2,300	24	620	210	3,154	NA	
MW-22	5/10/1994	2,500	49	720	390	3,659	NA	
MW-22	6/18/1997	819	ND	375	76.1	1,270	NA	
MW-22	5/29/1998	677	19.9	232	41.9	971	NA NA	
MW-22	10/27/1999	650	31.6	323	21.8	1,026	478	
MW-22	6/30/2003	646	91.2		86.4	2,064	19.3	
MW-22	6/15/2004	285	23.2	1,240 185	00.4 16.4	510	19.3 34.4	
MW-22	,					817		
	6/8/2005	346	24.8	434	12.1	692	29.5	
MW-22 MW-22	6/28/2006	251 . 444	38.9	370	31.6	850	22.0	
MW-22	6/26/2007		38.0	344	23.7	486	13.8	
MW-22R	5/12/2008	270	20.5	177	18.4		19.6	
MW-23	4/15/2010	386	68.4 3	2140	111.2	2705.6 16.5	42.8	
	5/8/1991	3.9		1.4	8.2	51	NA	
MW-23	5/12/1993	42 36	4.1	ND	4.9	30.9	NA NA	
MW-23	5/10/1994	26 4.6	1.6	ND	3.3	30,9 10.6	NA	
MW-23 MW-23	5/22/1995	4.6	1.5	ND	4.5	10.6	NA NA	
	5/23/1996	9.2	1.7	ND	3.4		NA	
MW-23 MW-23	6/18/1997	7.8	1.4	0.55	5.1	14.85	NA	
	5/29/1998	11.6	1.8	ND	6.1	19.5	NA NA	
MW-23	5/11/1999	6	0.9	ND	3.7	10.6	NA	
MW-23	10/27/1999	9.1	2.1	0.53	6.3	18.03	20.3	
MW-23	6/7/2000	8.5	1.9	ND	5.5	15.9	19.3	
MW-23	5/29/2001	4.7	0.98	ND	3,3	8.98	38.1	
MW-23	5/30/2002	1.7	1.3	< 1.0	2	5.0	21.7	
MW-23	6/30/2003	1.4	1.3	<1.0	3.7	6.4	12.9	
MW-23	6/15/2004	1.1	1.6	<1.0	3.5	6.2	17.9	
MW-23	6/8/2005	<1.0	<1,0	<1.0	1.6	1.6	11.9	
MW-23	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	7.05	
MW-23	6/26/2007	<1.00	1.27	<1.00	3.10	4.37	5.64	
MVV-23	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	2.70	
MW-23	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	2.8	
MW-23	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00	

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)							
Sample					Xylenes,	Total			
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE		
< GW Sta		< 0.7 >	< 5 >	<5>	< 5 >		< 10 >		
MW-24	5/8/1991	230	180	83	270	763	NA		
MW-24	5/13/1992	240	64	200	300	804	NA		
MW-24	5/12/1993	31	ND	ND	ND	31	NA		
MW-24	5/10/1994	460	16	130	230	836	NA		
MW-24	5/22/1995	100	ND	86	7	193	NA		
MW-24	5/23/1996	168	3.5	50.3	42.2	264	NA ·		
MW-24	6/18/1997	126	5.7	17.7	169	318.4	NA		
MW-24	5/29/1998	54.6	3.6	10.2	61.8	130.2	NA		
MW-24	5/11/1999	78.2	2	3.8	10.5	94.5	NA		
MW-24	10/27/1999	1.3	ND	ND	1.3	2.6	<i>26.4</i>		
MW-24	6/7/2000	24	1.9	3.9	7.3	37.1	234		
MW-24	5/29/2001	75.6	12	5.6	37.2	130.4	1,380		
MW-24	5/30/2002	< 1,0	< 1.0	< 1.0	4.1	4.1	295		
MW-24	6/30/2003	99.9	4.2	11.6	85.9	202	543		
MW-24	6/15/2004	7.6	0.67 ^J	<1.0	2.2	9.8	16.2		
MW-24	6/8/2005	15.3	1.2	<1.0	2.0	18.5	78.3		
MW-24	6/28/2006	27.6	<1.00	<1.00	<3.00	27.6	164		
MW-24	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	5.13		
MW-24	5/12/2008	144	22.1	28.8	70.3	265	621		
MW-24	4/29/2009	11.3	<1.0	<1.0	6.0	17.3	37.1		
MW-24	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	6.63		
MW-25	5/8/1991	210	4.4	1.9	ND	216.3	NA		
MW-25	5/13/1992	28	ND	ND	1.5	29.5	NA		
MW-25	5/12/1993	30	ND	ND	3.2	33.2	NA		
MW-25	5/10/1994	4.6	ND	ND	1.5	6.1	NA		
MW-25	5/22/1995	ND	ND	ND	ND	ND	NA		
MW-25	5/23/1996	0.78	ND	ND	ND	0.78	NA		
MW-25	6/18/1997	ND	ND	ND	ND	ND	NA		
MW-25	5/29/1998	ND	ИD	ND	2.9	2.9	NA		
MW-25	5/11/1999	ND	ND	ND	ND	ND	NA		
MW-25	10/27/1999	ND	ND	ND	1.7	1.7	28.2		
MW-25	6/7/2000	ND	ND	ND	ND	ND	74.4		
MW-25	5/29/2001	ND	ND	ND	ND	ND	25.8		
MW-25	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	18		
MW-25	6/30/2003	<1.0	<1.0	<1.0	<1.0	<4.0	12.6		
MW-25	6/15/2004	<1.0	<1.0	<1.0	<1.0	<4.0	42.9		
MW-25	6/7/2005	<1.0	<1.0	<1.0	<1.0	<4.0	13.6		
MW-25	6/28/2006	<1,00	<1.00	<1.00	<3.00	<6.00	7.18		
MW-25	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	12.5		
MW-25	5/12/2008	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-25	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	3,8		
MW-25	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00		
MW-26	6/15/2004	53.5	8.3	29.2	37.2	128	18.2		
MW-26	6/8/2005	6.6	1.3	1.3	8.6	17.8	3.3		
MW-26	5/12/2008	NOT SAMPLI							
MW-26	4/29/2009	NOT SAMPLE		•					
MW-26	4/15/2010	NOT SAMPLE		•					

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)							
Sample]	Xylenes,	Total			
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE		
< GW Sta	ndard >	< 0.7 >	< 5 >	< 5 >	< 5 >		< 10 >		
MW-27	5/29/1998	0.92	ND	ND	1.8	2.72	NA		
MW-27	5/11/1999	ND	ND	ND	1	1	NA		
MW-27	10/27/1999	ND	ND	ND	1.9	1.9	50.1		
MW-27	6/7/2000	ND	ND	ND	ND	ND	1.7		
MW-27	5/29/2001	ND	ND	ND	ND	ND	23.8		
MW-27	5/30/2002	< 1.0	< 1.0	< 1.0	< 5.0	< 8.0	28.3		
MW-27	6/30/2003	<1.0	<1.0	<1,0	<1.0	<4.0	13.1		
MW-27	6/15/2004	<1.0	<1.0	<1.0	<1.0	<4.0	18.6		
MW-27	6/7/2005	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-27	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-27	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	8.86		
MW-27		<1.00	<1.00	<1.00	<1.0	<4.0	<1.0		
MW-27	5/12/2008	l .							
	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-27	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00_		
MW-28	5/29/1998	ND	ND	ND	1.9	1.9	NA		
MW-28	5/11/1999	ND	ND	ND	0.97	0.97	NA		
MW-28	10/27/1999	ND	ND	ND	1.4	1.4	13.2		
MW-28	6/7/2000	ND	ND	ND	ND	ND	9,5		
MW-28	5/29/2001	ND	ND	ND	1.5	1.5	8		
MW-28	5/30/2002	< 1.0	< 1.0	< 1.0	1.5	1.5	12.6		
MW-28	6/30/2003	1.3	<1.0	<1.0	2.4	3.7	20.4		
MW-28	6/15/2004	1.3	0.61	<1.0	3.8	5.7	23.4		
MW-28	6/7/2005	<1.0	<1.0	<1.0	1.7	1.7	10.1		
MW-28	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	3,96		
MW-28	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	5.75		
MW-28	5/12/2008	<1.0	<1.0	<1.0	2.40	2.4	6.40		
MW-28	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	3.9		
MW-28	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00		
MW-29	5/29/1998	1,250	17.2	62.9	79.2	1409	NA		
MW-29	5/11/1999	651	10.5	33.3	50.1	745	NA		
MW-29	10/27/1999	1,060	18.1	40.6	53.6	1172	ND		
MW-29	6/7/2000	173	2.8	4.4	5.7	186	ND		
MW-29	5/29/2001	267	4.4	6.3	9.2	287	11.7		
MW-29	6/30/2003	390	14	45	33	482	7,5		
MW-29	6/15/2004	250	10	23.6	30.1	314	3.6		
MW-29	1					44.9			
MW-29	6/7/2005	35.6	1.3	4.2	3.8	216	<1.0		
	6/28/2006	184	4.36	12.6	15.0		<1.00		
MW-29	6/26/2007	303	5.46	10.0	26.8	345	<1.00		
MVV-29	5/12/2008	335	4.60	12.5	22.9	375	1,00		
MW-29	4/29/2009	105	1.9	3.9	7.6	118	<1.0		
MW-29	4/15/2010	122	<5.00_	<5.00	<5.00	122	<5.00		
MW-30	6/30/2003	<1.0	<1.0	<1.0	<1.0	<4.0	3.5		
MW-30	6/15/2004	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-30	6/7/2005	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MVV-30	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-30	6/26/2007	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00		
MW-30	5/12/2008	NOT ACCES	SIBLE (FLOC	DDED)					
MVV-30	4/29/2009	<1.0	<1.0	<1.0	<1.0	<4.0	<1.0		
MW-30	4/15/2010	<5.00	<5.00_	<5.00	<5.00	<5.00	<5.00		
MW-31	5/12/2008	NOT SAMPLE		CT)					
	1	NOT SAMPLED (PRODUCT) NOT SAMPLED (PRODUCT)							
MW-31	4/29/2009	INO) SHIVIELS	LD (F NODO)	01)					

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

		(ug/L)						
Sample					Xylenes,	Total		
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE	
< GW Sta	ndard >	< 0.7 >	< 5 >	<5>	< 5 >		< 10 >	
MW-32	10/27/1999	21.7	5.4	3.2	19.2	49.5	37	
MW-32	5/30/2002	7.2	2.8	1.1	10.9	22	28.6	
MW-32	6/30/2003	5.2	2.3	1.8	10.8	20	13.5	
MW-32	6/15/2004	3.5	1.4	0.78 ^J	5.6	11.3	18.1	
MW-32	6/7/2005	<1.0	<1.0	<1.0	3.0	4.8	4.7	
MW-32	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	3.81	
MW-32	6/26/2007	1.18	1.02	<1.00	4.16	4.16	4.50	
MW-32	5/12/2008	<1.0	<1.0	<1.0	1.00	1.0	2.80	
MW-32	4/29/2009	<1.0	<1.0	<1.0	1.6	1.6	3.2	
MW-32	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00	
MW-33	6/15/2004	284	5.7	4.1	16	310	298	
MW-33	6/8/2005	212	4.6	9.2	13.2	239	138	
MW-33	6/28/2006	148	1.70	4.74	9.17	164	142	
MW-33	6/26/2007	240	2.67	<1.00	5.93	249	89.9	
MW-33	5/12/2008	72.4	4.30	2.20	10.5	89.4	27.1	
MW-33	4/29/2009	13.7	<1.0	<1.0	5.6	19.3	7.8	
MW-33	4/15/2010	223	<5.00	<5.00	<5.00	223	61.9	
MW-34	6/8/2005	115	3.8	4.4	16.4	140	22.6	
MW-34	6/28/2006	83.7	3.14	2.31	7.42	96.6	22.2	
MW-34	6/26/2007	73.2	3.41	1.41	10.80	88.8	19.4	
MW-34	5/12/2008	NOT SAMPL	.ED (PRODU					
MW-34	4/29/2009	77.5	<1.0	<1.0	4.0	81.5	61.6	
MW-34	4/15/2010	NOT SAMPL						
MW-35	6/15/2004	1,180	22.2	18.6	33.3	1,254	472	
MW-35	6/8/2005	1,220	22.8	30.4	44.9	1,318	284	
MW-35	6/28/2006	693	7.43	3.49	17.3	721	189	
MW-35	6/26/2007	742	6.87	2.68	17.8	769	142	
MW-35	5/12/2008	518	10.4	6.50	28.6	564	79.9	
MW-35	4/29/2009	173	4,3	2.0	14.1	193	42.4	
MW-35	4/15/2010	765	9.78	<5.00	<5.00	774.78	97.4	
MW-36	5/12/2008	NOT SAMPL			0.00	77 0		
MW-36	4/29/2009	NOT SAMPL	•	•				
MW-36	4/15/2010	NOT SAMPL	-	-				
MW-37	6/15/2004	259	8.7	1.4	18	287	64.3	
MW-37	6/8/2005	209	4.2	<1.0	7.4°	221	55.5	
MW-37	6/28/2006	133	2.39	<1.00	3.81	139	49.4	
MW-37	5/12/2008	NOT SAMPL						
MW-37	4/29/2009	162	1,9	<1.0	3.0	167	36.4	
MW-37		NOT SAMPLE						
MW-38	5/29/2001	9.9	ND ND	0.76	ND	10.7	18.9	
MVV-38	5/30/2002	5.4	0.72	< 1.0	1.4	7.52	6.9	
MW-38	6/30/2003	17.2	4.2	0.84 ^J	2.1	23.5	29.5	
MW-38	6/15/2004	9.6	1.8	0,55 ^J	2.1	13.5	12.7	
MVV-38	6/8/2005	5.5	<1.0	<1.0	<1.0	5,5	1.8	
MW-38	6/28/2006	5.71	<1.00	<1.00	<3.00	5.71	22.9	
MVV-38	6/26/2007	2.33	<1.00	<1.00	<3.00	2.33	2.24	
MW-38	5/12/2008	10.1	<1.00	3.80	1,60	15.5	3.80	
MW-38	4/29/2009					2.9		
	ı	2.9	<1.0 <5.00	<1.0	<1.0		3,4	
MW-38	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00	

Table 2 **Historical Groundwater Analytical Results Summary**

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

25 Paidge Avenue Brooklyn, New York NYSDEC SPILL NO. 87-09990

				(ug/	'L)		
Sample				, ,	Xylenes,	Total	
Location	Date	Benzene	Toluene	Ethylbenzene	Total	BTEX	MTBE
< GW Sta	ndard >	< 0.7 >	< 5 >	<5>	<5>		< 10 >
MW-39	6/15/2004	296	21	19.2	42.4	379	125
MW-39	6/8/2005	246	14.8	12.5	27.6	301	74.8
MVV-39	6/28/2006	119	7.29	3.45	14.1	144	60.9
MVV-39	6/26/2007	136	7.04	3.21	17.0	163	57.3
MW-39	5/12/2008	225	13.8	4.50	19.3	263	69.9
MW-39	4/29/2009	183	7.3	4.9	20.6	216	65.5
MW-39	4/15/2010	65.9	<5.00	<5.00	<5.00	65.9	36.7
MW-40	5/12/2008	NOT SAMPL	.ED (PRODU	ICT)			
MW-40	4/29/2009	NOT SAMPL	.ED (PRODU	ICT)			
MW-40	4/15/2010	NOT SAMPL	.ED (PRODU	ICT)			
MW-41	6/8/2005	347	10.7	2.7	22.1	383	68.2
MW-41	5/12/2008	NOT SAMPL	.ED (PRODU	CT)			
MW-41	4/29/2009	NOT SAMPL	.ED (PRODU	CT)			
MW-41	4/15/2010	NOT SAMPL	.ED (PRODU	CT)			
MW-42	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00
MW-43	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	17.5
MW-44	4/15/2010	<5.00	<5.00	<5,00	<5.00	<5.00	<5.00
TW-01	5/12/2008	NOT ACCES	SIBLE (FLO	ODED)			
TW-01	4/29/2009	NOT SAMPL	ED (PRODU	CT)			
TW-01	4/15/2010	NOT ACCES	SIBLE (FLO	ODED)			
TW-02	6/28/2006	41.9	2.63	1.84	4.22	50.6	2.97
TW-02	5/12/2008	17.3	1.0	<1.0	<1.0	18.3	<1.0
TW-02	4/29/2009	3.4	<1.0	<1.0	<1.0	3.4	<1.0
TW-02	4/15/2010	<5.00	<5.00	<5.00	<5.00	<5.00	<5.00
TW-03	6/28/2006	<1.00	<1.00	<1.00	<3.00	<6.00	<1.00
TW-03	5/12/2008	NOT ACCES	•	,			
TW-03	4/29/2009	NOT ACCES	SIBLE (FLO	ODED)			
TW-03	4/15/2010	NOT ACCES	SIBLE (FLO	ODED)			
TW-04	5/12/2008	NOT ACCES	SIBLE (FLO	ODED)			
TW-04	4/29/2009	NOT ACCES	SIBLE (FLO	ODED)			
TW-04	4/15/2010	NOT ACCES	SIBLE (FLOC	ODED)			
TW-05	5/12/2008	NOT ACCES	SIBLE (FLO	DDED)			
TW-05	4/29/2009	NOT SAMPLI	ED (PRODU	CT)			
TW-05	4/15/2010	NOT ACCES	SIBLE (FLOC	DDED)			
TW-06	5/12/2008	NOT ACCES	SIBLE (FLOC	DDED)			
TW-06	4/29/2009	NOT ACCES	SIBLE (FLOC	DDED)			
TW-06	4/15/2010	NOT SAMPLI	ED (PRODU	CT)			

Notes:
GW Standard = Values in bold and italic exceed the Groundwater Standard.

μg/L = micrograms per liter, or parts per billion (ppb)

NA = Sample not analyzed for target parameter.

NS = No sample collected from well.

ND(X) = Parameter not-detected at the reporting limit (or method detection limit if shown)(X).

<X = Parameter detected below the method limit of quantitation (X).

J = The target analyte was positively identified below the MQL and above the SQL.

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.) 102.41	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-01						102.18	102.18		
2/21/2006	MW-01	104.99	~	2.81			102.10	102.10		
3/7/2006	MW-01	104.99		3.09						
5/18/2006	MW-01	104.99		2.84			102.15	102.15		
6/28/2006	MW-01	104.99		2.63			102.36	102.36		
8/16/2006	MW-01	104.99		2.78			102.21	102.21		
9/29/2006	MW-01	104.99		2.66			102.33	102.33		
10/20/2006	MW-01	104.99		2.65			102.34	102.34	4	
11/22/2006	MW-01	104.99		2.76			102.23	102.23		
12/15/2006	MW-01	104.99		3.06			101.93	101.93		
1/23/2007	MW-01	104.99		3.16			101.83	101.83		
2/2/2007	MW-01	104.99		3.27			101.72	101.72		
3/5/2007	MW-01	104,99		2.98			102.01	102.01	***	
5/1/2007	MW-01	104.99		2.77			102.22	102.22		
6/22/2007	MW-01	104.99		3,15			101.84	101.84		
6/26/2007	MW-01	104.99		2.87			102.12	102.12		
7/6/2007	MW-01	104.99		2.83			102.16	102.16		
8/1/2007	MW-01	104.99		2.75			102.24	102.24		
8/7/2007	MW-01	104.99	*****	2.81			102.18	102.18		
9/14/2007	MW-01	104.99		3,19			101.80	101.80		
	MW-01	104.99		3.39			101.60	101.60		
10/8/2007		104.99		3.06			101.93	101.93		
11/20/2007	MW-01			3.25			101.74	101.74		
12/26/2007	MW-01	104.99		3.26			101.93	101,93		
1/2/2008	MW-01	104.99					101.97	101.97		
3/5/2008	MW-01	104.99		3.02			101.94	101.94		
4/23/2008	MW-01	104.99		3.05						
5/12/2008	MW-01	104.99		3.10			101.89	101.89		
6/27/2008	MW-01	104.99		3.15			101.84	101.84		
8/5/2008	MW-01	104.99		3.29			101.70	101.70		
9/10/2008	MW-01	104.99		3.16			101.83	101.83		
10/27/2008	MW-01	104.99		3.41			101.58	101.58		
11/4/2008	MW-01	104.99		3.49			101.50	101.50		
1/5/2009	MW-01	104.99		3.30			101.69	101.69		
2/27/2009	MW-01	104.99		3.79			101.20	101.20		
3/9/2009	MW-01	104.99		3.74			101.25	101.25		
4/20/2009	MW-01	104.99		3.56			101.43	101.43		
4/29/2009	MW-01	104.99		3.33			101.66	101.66		
5/6/2009	MW-01	104.99		3.05			101.94	101.94		
6/2/2009	MW-01	104.99		3.48			101.51	101.51		
7/6/2009	MW-01	104.99		3.02			101.97	101.97		
8/14/2009	MW-01	104.99		3.19			101.80	101,80		
9/28/2009	MW-01	104.99		3.45			101.54	101.54		
10/13/2009	MW-01	104.99		3.59			101.40	101.40		
11/23/2009	MW-01	104.99		3.48			101.51	101.51		
	MW-01	104.99		3.58			101.41	101.41		
12/2/2009	MW-01	104.99		3.49			101.50	101,50		
1/12/2010		104.99		3.62			101.37	101.37		
2/2/2010	MW-01			2.46			101.57	101.57		
3/2/2010	MW-01	104.99					102.53			
3/15/2010	MW-01	104.99		2.29				102.70		
4/15/2010	MW-01	104.99		2.90			102.09	102.09		
4/22/2010	MW-01	104.99		2.92			102.07	102.07		
5/3/2010	MW-01	104.99_		2.21			102.78	102.78		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-02	103.94		3.14			100.80	100,80		
2/21/2006	MW-02	103.94		3.90		***	100.04	100.04		****
3/7/2006	MW-02	103.94	4.04	4.11	0.07	99.90	99.83	99.88	0.10	Hand Bailing
5/18/2006	MW-02	103.94	3.59	3.69	0.10	100.35	100.25	100.32	0.25	
6/28/2006	MW-02	103.94	3.45	3.61	0.16	100.49	100.33	100.45		
8/16/2006	MW-02	103.94	3.75	4.29	0.54	100.19	99,65	100.05		
9/29/2006	MW-02	103.94	3,52	3.84	0.32	100.42	100.10	100.34		
10/20/2006	MW-02	103.94	3.19	3.49	0.30	100.75	100,45	100.67		
11/22/2006	MW-02	103.94	3.34	3.52	0,18	100.60	100.42	100.55		
12/15/2006	MW-02	103.94	3.98	4.16	0,18	99.96	99.78	99.91		
1/23/2007	MW-02	103.94	4.36	4.52	0.16	99.58	99.42	99.54	0.25	
2/2/2007	MW-02	103.94	4.21	4.39	0.18	99.73	99.55	99.68	0.25	****
3/5/2007	MW-02	103.94	4.00	4.18	0.18	99.94	99.76	99.89	0.25	
5/1/2007	MW-02	103.94	3.36	3.53	0.17	100.58	100.41	100.54	0.25	
6/22/2007	MW-02	103.94	3.80	4.15	0.35	100.38	99.79	100.05	0.25	
6/26/2007	MW-02	103.94	4.02	4.42	0.40	99.92	99.52	99.82		
7/6/2007	MW-02	103.94	3.92	4.32	0.40	100.02	99.62	99.92	0.25	
8/1/2007	MW-02	103.94	3.59	3.94	0.40	100.02	100.00	100.26	0.25	***
8/7/2007	MW-02	103.94		NG			100.00			
	MW-02	103.94		NG						
9/14/2007	MW-02	103.94		4.59						
10/9/2007			4.05		0.54	99.89	99.35	99.75	0.50	
11/20/2007	MW-02	103.94	4.00	4.39	0.39	99.94	99.55	99.84	0.50	
12/26/2007	MW-02	103.94		3.95		400.04	99.99	99.99		
1/2/2008	MW-02	103.94	3.73	4.09	0.36	100.21	99.85	100.12	0,50	
3/5/2008	MW-02	103.94		NG						****
4/23/2008	MW-02	103.94	4.06	4.45	0.39	99.88	99.49	99.78	0.50	
5/12/2008	MW-02	103.94	3.15	3.35	0.20	100.79	100.59	100.74		
6/27/2008	MW-02	103.94	3.68	4.10	0.42	100.26	99.84	100.15	0.50	
8/5/2008	MW-02	103.94	3.91	4.46	0.55	100.03	99.48	99.89	0.50	
9/10/2008	MW-02	103.94	3.71	4.29	0.58	100.23	99.65	100.08	0.75	
10/27/2008	MW-02	103.94	***	NG				****	,	
11/4/2008	MW-02	103.94	4.61	4.62	0.01	99.33	99.32	99.33		
1/5/2009	MW-02	103.94	4.15	4.50	0.35	99.79	99.44	99.70	0.50	
2/27/2009	MW-02	103.94	4.58	4.89	0.31	99.36	99.05	99.28	0.50	
3/9/2009	MW-02	103.94	4.00	4.53	0.53	99.94	99.41	99.80	1.00	
4/20/2009	MW-02	103.94	3.84	4.30	0.46	100.10	99.64	99.98	1.00	****
4/29/2009	MW-02	103.94	4.42	5.41	0.99	99.52	98.53	99.26	0.75	and the last
5/6/2009	MW-02	103.94	3.49	3.97	0.48	100.45	99.97	100.33	0.75	
6/2/2009	MW-02	103.94	3.93	4.44	0.51	100.01	99.50	99.88	0.75	
7/6/2009	MW-02	103.94	3.42	3.70	0.28	100.52	100.24	100.45	0.50	
8/14/2009	MW-02	103.94	3.70	4.07	0.37	100.24	99.87	100.14	0.50	
9/28/2009	MW-02	103.94	3.78	4.04	0.26	100.16	99.90	100.09	0.50	
10/13/2009	MW-02	103.94	4.01	4.32	0.31	99.93	99.62	99.85	0.50	
11/23/2009	MW-02	103.94	3.77	3.79	0.02	100.17	100.15	100.16	0.50	
12/2/2009	MW-02	103.94	4.07	4.12	0.05	99.87	99.82	99,86	0.50	
1/12/2010	MW-02	103.94	4.05	4.09	0.04	99.89	99.85	99.88		
2/2/2010	MW-02	103,94	4.24	4.35	0.11	99.70	99.59	99.67	0.25	
3/2/2010	MW-02	103.94	2.56	2.81	0.25	101.38	101.13	101.32	0.25	
3/15/2010	MW-02	103.94	1,81	1.81	0.00	102.13	102.13	102.13		Trace LNAPL
4/15/2010	MW-02	103.94	3,77	3.79	0.02	100.17	100.15	100.16		
4/22/2010	MW-02	103.94		3,53			100.41	100.41		
5/3/2010	MW-02	103.94	3.28	3.31	0.03	100.66	100.63	100.65		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-03	103.94		2.15			101.79	101.79	****	
2/21/2006	MW-03	103.94		2.40			101.54	101.54		***
3/7/2006	MW-03	103.94		2.72			101.22	101.22		
5/18/2006	MW-03	103.94		2.39			101.55	101.55		-
6/28/2006	MW-03	103.94	~~~	2.12			101.82	101.82		
8/16/2006	MW-03	103.94		2.31			101.63	101.63		****
9/29/2006	MW-03	103.94	~	2.35			101.59	101.59		
10/20/2006	MW-03	103.94	~	2.04			101.90	101.90		
11/22/2006	MW-03	103.94		2.31			101.63	101.63		
12/15/2006	MW-03	103.94	****	2.63			101.31	101.31		
1/23/2007	MW-03	103.94		2.81			101.13	101.13		
2/2/2007	MW-03	103.94	~	3.51			100.43	100.43		
3/5/2007	MW-03	103.94	~~~	2.49			101.45	101.45		
5/1/2007	MW-03	103.94		2.14			101.80	101.80		
6/22/2007	MW-03	103.94		2.65			101.29	101.29		
6/26/2007	MW-03	103.94		2.74			101.20	101.20		
7/6/2007	MW-03	103.94		2.52			101.42	101.42		
8/1/2007	MW-03	103.94		2.29			101.65	101.65		
8/7/2007	MW-03	103.94		2.43			101.51	101.51		
9/14/2007	MW-03	103.94		2.63			101.31	101.31		
10/8/2007	MW-03	103.94		3.04			100.90	100.90		
11/20/2007	MW-03	103.94		2.99			100.95	100.95		
12/26/2007	MW-03	103.94		2.65			101.29	101.29		
1/2/2008	MW-03	103.94		2.48			101.46	101.46		
3/5/2008	MW-03	103.94		2.56			101.38	101.38		
4/23/2008	MW-03	103.94		3.04			100.90	100.90		
5/12/2008	MW-03	103.94		2.70			101,24	101.24		
6/27/2008	MW-03	103.94		2.68			101.26	101.26		
8/5/2008	MW-03	103.94		2.94			101.00	101.00		
9/10/2008	MW-03	103.94		2.71			101.23	101.23		
10/27/2008	MW-03	103.94		2.79			101.15	101.15		
11/4/2008	MW-03	103.94		2.95			100.99	100.99		
1/5/2009	MW-03	103.94		2.67			101.27	101.27		
2/27/2009	MW-03	103.94		3.29			100.65	100.65		
3/9/2009	MW-03	103.94		2.93			101.01	101.01		
4/20/2009	MW-03	103.94		3.02			100.92	100.92		
4/29/2009	MW-03	103.94		2.87			101.07	101.07		
5/6/2009	MW-03	103.94	-	2.59			101.35	101.35		
6/2/2009	MW-03	103.94		2.94			101.00	101.00		
7/6/2009	MW-03	103.94		2.35			101.59	101.59		
8/14/2009	MW-03	103.94		2.58			101.36	101.36		
9/28/2009	MW-03	103.94		2.76			101.18	101,18		
10/13/2009	MW-03	103.94		3.07			100.87	100.87		
11/23/2009	MW-03	103.94		2.81			100.07	101.13		
12/2/2009	MW-03	103.94		2.94			101.10	101.00		
1/12/2010	MW-03	103.94		2.87			101.07	101.07		
2/2/2010	MW-03	103.94		3.05			100.89	100.89		
3/2/2010	MW-03	103.94		1.28			100.69	100.69		
3/15/2010	MW-03	103.94		1.43			102.50	102.55		
	MW-03	103.94		2.53			102.51			
4/15/2010								101.41		
4/22/2010	MW-03	103.94 103.94		2.61 2.42			101.33 101.52	101.33 101.52		

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-04	103.24	1.90	1.92	0.02	101.34	101.32	101.33	0.10	
2/21/2006	MW-04	103.24	2.20	2.21	0.01	101.04	101.03	101.04	0.10	
3/7/2006	MW-04	103.24	2.40	2.42	0.02	100.84	100.82	100.83	0.10	Hand Bailing
5/18/2006	MW-04	103.24		2.08			101.16	101.16		
6/28/2006	MW-04	103.24	1.91	1.93	0.02	101.33	101.31	101.32		
8/16/2006	MW-04	103.24	2.20	2.21	0.01	101.04	101.03	101.04		
9/29/2006	MW-04	103.24		2.15			101.09	101.09		
10/20/2006	MW-04	103.24	1.86	1.97	0,11	101.38	101.27	101.35		
11/22/2006	MW-04	103.24	2.06	2.16	0.10	101.18	101.08	101.15		
12/15/2006	MW-04	103.24	2.30	2.39	0.09	100.94	100.85	100.92	****	
1/23/2007	MW-04	103.24	2.53	2.57	0.04	100.71	100.67	100.70		
2/2/2007	MW-04	103.24	2.63	2.72	0.09	100.61	100.52	100.59	0.25	
3/5/2007	MW-04	103.24	2.38	2.39	0.01	100.86	100.85	100.86	0.25	******
5/1/2007	MW-04	103.24	1.78	1.82	0.04	101.46	101.42	101.45	0.25	
6/22/2007	MW-04	103.24	2.17	2.26	0.09	101.07	100.98	101.05		
6/26/2007	MW-04	103.24	2.30	2.42	0.12	100.94	100.82	100.91	*	
7/6/2007	MW-04	103.24	2.28	2.40	0.12	100.96	100.84	100.93	0.25	
8/1/2007	MW-04	103.24	2.00	2.11	0.11	101.24	101.13	101.21		
8/7/2007	MW-04	103.24	2.11	2.21	0.10	101.13	101.03	101.10	No.	
9/14/2007	MW-04	103.24	2.34	2.48	0.10	100.90	100.76	100.86		
	MW-04	103.24	2.63	2.72	0.14	100.90	100.76	100.59		
10/8/2007										
11/20/2007	MW-04	103.24	2.65	2.67	0.02	100.59	100.57	100.58		
12/26/2007	MW-04	103.24		2.42			100.82	100.82		
1/2/2008	MW-04	103.24		2.29			100.95	100.95		
3/5/2008	MW-04	103.24		2.32			100.92	100.92		
4/23/2008	MW-04	103.24		2.64			100.60	100.60		
5/6/2008	MW-04	103.24	2.35	2.36	0.01	100.89	100.88	100.89	~	
5/12/2008	MW-04	103.24		2.26			100,98	100.98		
6/27/2008	MW-04	103.24	2.26	2.28	0.02	100.98	100.96	100.97		
8/5/2008	MW-04	103.24		2.49			100.75	100.75		
9/10/2008	MW-04	103.24	2.48	2.52	0.04	100.76	100.72	100.75		
10/27/2008	MW-04	103.24		2.46			100.78	100.78		
11/4/2008	MW-04	103.24	2.61	2.63	0.02	100.63	100.61	100.62		
1/5/2009	MW-04	103.24	2.40	2.44	0.04	100.84	100,80	100.83		
2/27/2009	MW-04	103.24	2.88	2.95	0.07	100.36	100.29	100.34		
3/9/2009	MW-04	103.24	2.81	2.84	0.03	100.43	100,40	100.42		
4/20/2009	MW-04	103.24		2.67			100.57	100.57		
4/29/2009	MW-04	103.24		2.56	~		100.68	100.68		
6/2/2009	MW-04	103.24	2.48	2.50	0.02	100.76	100.74	100.75		
7/6/2009	MW-04	103.24	1.97	1.98	0.01	101.27	101,26	101.27		
8/14/2009	MW-04	103.24	2.25	2.42	0,17	100.99	100.82	100.95	0.25	
9/28/2009	MW-04	103.24	2.37	2.39	0.02	100.87	100.85	100.86		
10/13/2009	MW-04	103.24	2.59	2.68	0.09	100.65	100.56	100.63	0.25	
11/23/2009	MW-04	103.24	2.40	2.46	0.06	100.84	100.38	100.82	0.25	
12/2/2009	MW-04	103.24	2.54	2.58	0.04	100.70	100.76	100.62	0.25	
1/12/2010	MW-04	103.24	2.49	2.54	0.04	100.75	100.66	100.59		
2/2/2010	MW-04	103.24	2.64	2.69	0.05	100.60	100,55	100.59		
3/2/2010	MW-04	103.24	0.00	1.59	0.00	400.00	101.65	101.65		
3/15/2010	MW-04	103.24	0.98	0.98	0.00	102.26	102.26	102.26		Trace LNAPL
4/15/2010	MW-04	103.24	2.11	2.16	0.05	101.13	101.08	101.12		
4/22/2010	MW-04	103.24	2.13	2.15	0.02	101.11	101.09	101.10		

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-05	102.64		1.78			100.86	100.86		
2/21/2006	MW-05	102.64		1.60			101.04	101.04		
3/7/2006	MW-05	102.64		1.85			100.79	100.79		
5/18/2006	MW-05	102.64		1.52			101.12	101.12		~~~
6/28/2006	MW-05	102.64		1.01			101.63	101.63		
8/16/2006	MW-05	102.64		1.61			101.03	101.03		
9/29/2006	MW-05	102,64		1.61			101.03	101.03		
10/20/2006	MW-05	102.64		0.79			101.85	101.85		
11/22/2006	MW-05	102.64		1.54			101.10	101.10		
12/15/2006	MW-05	102.64		1.74			100.90	100,90		
1/23/2007	MW-05	102.64		NG				****		
2/2/2007	MW-05	102.64		2.12			100.52	100.52		
	MVV-05	102.64		1.88			100.76	100.76		
3/5/2007	MW-05	102.64		1.26			101.38	101.38		
5/1/2007	MW-05	102.64		1.65			100.99	100.99		
6/22/2007		102.64		1.80			100.84	100.84		
6/26/2007	MW-05			1.70			100.94	100.94		
7/6/2007	MW-05	102.64					100.34	101.22		
8/1/2007	MW-05	102.64		1.42			101.22	101.22		
8/7/2007	MW-05	102.64		1.55	~			100,80		
9/14/2007	MW-05	102.64		1.84			100.80			
10/8/2007	MW-05	102.64		2.12			100.52	100.52		
11/20/2007	MW-05	102.64		2.00	~		100.64	100.64		
12/26/2007	MW-05	102.64		1.80			100.84	100,84		
1/2/2008	MW-05	102.64		1.74	*		100.90	100.90		
3/5/2008	MW-05	102.64		2.10	~		100.54	100.54		
4/23/2008	MW-05	102.64		NG						
5/6/2008	MW-05	102.64		1.78	*****		100.86	100.86		
5/12/2008	MW-05	102.64		NG						
6/27/2008	MW-05	102.64		1.78	~~~		100.86	100.86		
8/5/2008	MW-05	102.64		1.95			100.69	100.69		
9/10/2008	MW-05	102.64		1.95	~~~	***	100.69	100.69		
10/27/2008	MW-05	102.64		NG						
11/4/2008	MW-05	102.64		2.09	~~~		100.55	100.55		
1/5/2009	MW-05	102.64		1.88			100.76	100.76		
2/27/2009	MW-05	102.64		2.32	-	,,,,,	100.32	100.32		
3/9/2009	MW-05	102.64		2.29	P		100.35	100.35		
	MW-05	102.64		2.13			100.51	100.51		History
4/20/2009		102.64		2.13			100.40	100.40		
4/29/2009	MW-05			1.99			100.40	100.65		
6/2/2009	MW-05	102.64 102.64		1.48			101.16	101.16		
7/6/2009	MW-05			1.48			101.16	100.89		
8/14/2009	MW-05	102.64					100.89	100.39		
9/28/2009	MW-05	102.64		1.85			100.79	100.79		
10/13/2009	MW-05	102.64		2.09						
11/23/2009	MW-05	102.64		1.89			100.75	100.75		
12/2/2009	MVV-05	102.64		1.99			100.65	100.65		
1/12/2010	MW-05	102.64		1.95			100.69	100.69		
2/2/2010	MW-05	102.64		2.07	'		100.57	100.57		
3/2/2010	MW-05	102.64		1.06			101.58	101.58		
3/15/2010	MW-05	102.64		NG						Flooded
4/15/2010	MW-05	102.64		1.37			101.27	101.27		
4/22/2010	MW-05	102.64		1.59			101.05	101.05		
5/3/2010	MW-05	102.64		NG						

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-06	103.42		3.23			100.19	100.19		
2/21/2006	MW-06	103.42		4.59			98.83	98.83	4	~
3/7/2006	MW-06	103.42		4.37			99.05	99.05		
5/18/2006	MW-06	103.42		3.46			99.96	99.96		
6/28/2006	MW-06	103.42		2.28			101.14	101.14		~
8/16/2006	MW-06	103.42		4.69			98.73	98.73		
9/29/2006	MW-06	103.42		3.65			99.77	99.77		
10/20/2006	MW-06	103.42		2.57	~		100.85	100.85		
11/22/2006	MW-06	103.42		2.84			100.58	100.58		
12/15/2006	MW-06	103.42		4.21			99.21	99.21		
1/23/2007	MW-06	103.42		4.65			98.77	98.77	~	
2/2/2007	MW-06	103.42		2.45			100.97	100.97	~	
3/5/2007	MW-06	103.42		3.67			99.75	99.75		
5/1/2007	MW-06	103.42		3.41			100.01	100.01		
6/22/2007	MW-06	103.42		4.29			99.13	99.13		
6/26/2007	MW-06	103.42		4.10			99.32	99.32		
7/6/2007	MW-06	103.42		4.73			98.69	98.69	~	
8/1/2007	MW-06	103.42		3.69			99.73	99.73		
8/7/2007	MW-06	103.42		3.91			99.51	99.51		
9/14/2007	MW-06	103.42		4.12			99.30	99.30		
	MW-06	103.42		2.81			100.61	100.61		
10/8/2007	MW-06	103.42		3.49			99.93	99.93		
11/20/2007		103.42		3.76			99.66	99.66		
12/26/2007	MW-06	103.42		4.05			99.37	99.37		
1/2/2008	MW-06			3.00			100.42	100.42		
3/5/2008	MW-06	103.42					99.12	99.12		
4/23/2008	MW-06	103.42		4.30			100.62	100.62		
5/12/2008	MW-06	103.42		2.80				99.49		
6/27/2008	MW-06	103.42		3.93			99.49			
8/5/2008	MVV-06	103.42		4.19			99.23	99.23		
9/10/2008	MW-06	103.42		3.89			99.53	99.53		
10/27/2008	MW-06	103.42		2.00			101.42	101.42		
11/4/2008	MW-06	103.42		4.79			98.63	98.63		
1/5/2009	MW-06	103.42		4.39			99.03	99.03		
2/27/2009	MW-06	103.42		4.18			99.24	99.24		
3/9/2009	MW-06	103.42		2.36			101.06	101.06		
4/20/2009	MW-06	103.42		3,54			99.88	99.88		
4/29/2009	MW-06	103.42		6.20			97.22	97.22		
5/6/2009	MW-06	103.42		3.06			100.36	100.36		
6/2/2009	MW-06	103.42		4.63			98.79	98.79		
7/6/2009	MW-06	103.42		3.68			99.74	99.74		
8/14/2009	MW-06	103.42		4.96			98.46	98.46		
9/28/2009	MW-06	103.42		4.34			99.08	99.08		
10/13/2009	MW-06	103.42		4.49			98.93	98.93		
11/23/2009	MW-06	103.42		4.24			99.18	99.18		
12/2/2009	MW-06	103.42		2.55			100.87	100.87		
1/12/2010	MW-06	103.42		3.87	***	<u></u>	99.55	99.55		
2/2/2010	MW-06	103.42		4.45			98.97	98.97		
3/2/2010	MW-06	103.42		2.34			101.08	101.08		
3/15/2010	MW-06	103.42		1.86			101.56	101.56		
4/15/2010	MW-06	103.42		5.08			98.34	98.34	***	
	MW-06	103.42		5.08		***	98.34	98.34		
4/22/2010	MW-06	103.42		3.06 4.59			98.83	98.83		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-07	102.86		4.81			98.05	98.05		
2/21/2006	MW-07	102.86		4.94			97.92	97.92	****	
3/7/2006	MW-07	102.86		4.84			98.02	98.02		
5/18/2006	MW-07	102.86		4.91			97.95	97.95		
6/28/2006	MW-07	102.86		4.11			98.75	98.75		
8/16/2006	MW-07	102.86		4.85			98.01	98.01		
9/29/2006	MW-07	102.86		4.63	***		98.23	98.23		
10/20/2006	MW-07	102.86		3.50			99.36	99.36		
11/22/2006	MW-07	102.86		4.43			98.43	98.43		
12/15/2006	MW-07	102.86		4.57			98.29	98.29		
1/23/2007	MW-07	102.86		4.11			98.75	98.75		
2/2/2007	MW-07	102.86		2.95			99.91	99.91		
3/5/2007	MW-07	102.86		4.55			98.31	98.31		
5/1/2007	MW-07	102.86		3.97			98.89	98.89		
6/22/2007	MW-07	102.86		4.55			98.31	98.31		
6/26/2007	MW-07	102.86		4.53		****	98.33	98.33		
7/6/2007	MW-07	102.86		4.61			98.25	98.25		
8/1/2007	MW-07	102.86		4.61			98.25	98.25		
8/7/2007	MW-07	102.86		4.53			98.33	98.33	****	
9/14/2007	MW-07	102.86		4.55			98.31	98,31		
10/8/2007	MW-07	102.86		3.03			99.83	99,83		
11/20/2007	MW-07	102.86		4.48			98.38	98.38		
12/26/2007	MW-07	102.86		4.22			98.64	98,64		
1/2/2008	MW-07	102.86		4.55			98.31	98.31		
3/5/2008	MW-07	102.86		4.59			98.27	98,27		
4/23/2008	MW-07	102.86		4.36			98.50	98.50		
5/12/2008	MW-07	102.86	****	4.20	****		98.66	98.66		
6/27/2008	MW-07	102.86		4.50			98.36	98.36		
8/5/2008	MW-07	102.86		4.59			98.27	98.27		
9/10/2008	MW-07	102.86		4.49			98.37	98.37		
10/27/2008	MW-07	102.86		NG						
1/5/2009	MW-07	102.86		NG						Abandoned
3/2/2010	MW-07R			2.52						
3/15/2010	MW-07R			3.78					wo.m	
4/15/2010	MW-07R			5.80		***		****		
4/22/2010	MW-07R			5.67			****			
5/3/2010	MW-07R		***	5.45	****		****			****

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/23/2006	MW-08	104.05		4.67	~		99.38	99.38		
3/7/2006	MW-08	104.05		NG						
5/18/2006	MW-08	104.05		NG						
6/28/2006	MW-08	104.05		NG						~
9/29/2006	MW-08	104.05		NG						
10/20/2006	MW-08	104.05		3.84			100.21	100.21		
11/22/2006	MW-08	104.05		5.06			98.99	98.99		
12/15/2006	MW-08	104.05		5.91			98.14	98.14		
2/2/2007	MW-08	104.05		3.40			100.65	100.65	~	
3/5/2007	MW-08	104.05		5.13	~		98.92	98.92		
5/1/2007	MW-08	104.05		4.44			99.61	99.61		
6/22/2007	MW-08	104.05		5.81			98.24	98.24	~	
6/26/2007	MW-08	104.05		5.58			98.47	98.47		
7/6/2007	MW-08	104.05		6.07			97.98	97.98	~	
8/1/2007	MW-08	104.05		5.36			98.69	98.69	~	
8/7/2007	MW-08	104.05		5.85			98.20	98.20		
9/14/2007	MW-08	104.05		5.05			99.00	99.00		
10/8/2007	MW-08	104.05		3.53			100,52	100.52	*****	
11/20/2007	MW-08	104.05		5.79			98.26	98.26		
12/26/2007	MVV-08	104.05		4.87			99.18	99.18	~	
1/2/2008	MW-08	104.05		5.88			98.17	98.17		
3/5/2008	MW-08	104.05		5.15			98.90	98.90		
4/23/2008	MVV-08	104.05		5.88			98.17	98.17		
5/12/2008	MVV-08	104.05		4.63			99.42	99.42		
6/27/2008	MW-08	104.05		5.78			98.27	98.27		
	MW-08	104.05		6.00			98.05	98.05		
8/5/2008	MW-08	104.05		5.47			98.58	98.58		
9/10/2008	MW-08	104.05		NG						
10/27/2008				NG						
1/5/2009	MVV-08	104.05					00.40			
5/15/2009	MW-08	104.05		5.62			98.43	98.43		-4-
6/2/2009	MW-08	104.05		5.49			98.56	98.56		
7/6/2009	MW-08	104.05		5.48			98.57	98.57		
8/14/2009	MW-08	104.05		5.97			98.08	98.08		
9/28/2009	MW-08	104.05		5.92			98.13	98.13		
10/13/2009	MW-08	104.05		6.15			97.90	97.90		
11/23/2009	MW-08	104.05		5.24			98.81	98.81		
12/2/2009	MW-08	104.05		3.65			100.40	100.40		
1/12/2010	MW-08	104.05		5.54			98.51	98.51		
2/2/2010	MW-08	104.05		5.34			98.71	98.71		
3/2/2010	MW-08	104.05		3.04			101.01	101.01		
3/15/2010	MW-08	104.05		4.41			99.64	99.64		
4/15/2010	MW-08	104.05		6.48			97.57	97.57		
4/22/2010	MW-08	104.05		6.18			97.87	97.87		
5/3/2010	MW-08	104.05		6.10			97.95	97.95		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-09	103.83		5.12			98.71	98.71		
2/21/2006	MW-09	103.83	****	5.90			97.93	97.93		
3/7/2006	MW-09	103.83		NG						
5/18/2006	MW-09	103.83		5.69			98.14	98.14		***
6/28/2006	MW-09	103.83		4.36			99.47	99.47		
8/16/2006	MW-09	103.83		5.92			97.91	97.91		*****
9/29/2006	MW-09	103.83		5.75			98.08	98.08		
10/20/2006	MW-09	103.83	****	3.97			99.86	99.86		
11/22/2006	MW-09	103.83		4.88	****		98.95	98,95		
12/15/2006	MW-09	103.83		5.75			98.08	98.08	*****	
1/23/2007	MW-09	103.83		4.40			99.43	99.43		
2/2/2007	MW-09	103.83		3.21			100.62	100.62		
3/5/2007	MW-09	103.83		NG						
5/1/2007	MW-09	103.83		4.18			99.65	99,65		
6/22/2007	MW-09	103,83		5.79		****	98.04	98.04		
6/26/2007	MW-09	103,83		5.41			98.42	98.42	****	
7/6/2007	MVV-09	103.83		5.91			97.92	97.92		
8/1/2007	MW-09	103.83		5.14			98.69	98.69		
8/7/2007	MW-09	103.83		6.77			97.06	97.06		
9/14/2007	MW-09	103.83		4.71			99.12	99.12		
10/8/2007	MW-09	103.83		3.29			100.54	100.54		
11/20/2007	MW-09	103.83		5.72			98.11	98,11		
12/26/2007	MW-09	103.83		4.40			99.43	99.43	***	
1/2/2008	MW-09	103.83		4.40 5.77			99.43 98.06	99.43 98.06		
3/5/2008	MW-09	103.83		5.00			98.83	98.83		*****
4/23/2008	MW-09	103.83		5.81			98.02	98.02		
5/12/2008	MW-09	103.83		4.40			99.43	99.43		
6/27/2008	MW-09	103.83		5.75			98.08	98.08		
8/5/2008	MW-09	103.83		5.91			97.92	97.92		****
9/10/2008	MW-09	103.83		5.41			98.42	98.42	****	
10/27/2008	MW-09	103.83		NG						
1/5/2009	MW-09	103.83		NG			*****			
5/15/2009	MW-09	103.83		5.63			98.20	98.20		
6/2/2009	MW-09	103.83		5.45			98.38	98.38		
7/6/2009	MW-09	103.83		5.34			98.49	98,49		
8/14/2009	MW-09	103.83		5.91			97.92	97.92		****
9/28/2009	MW-09	103.83		5.82			98.01	98.01		
10/13/2009	MW-09	103.83		6.08			97.75	97.75		
11/23/2009	MW-09	103.83		5.25			98.58	98.58		
12/2/2009	MW-09	103.83		3.63			100.20	100.20		
1/12/2010	MW-09	103.83		5.67			98.16	98.16		
2/2/2010	MW-09	103.83		5.33			98.50	98.50		
3/2/2010	MW-09	103.83		2.97			100.86	100.86	*	
3/15/2010	MW-09	103.83		4.26			99.57	99.57		
4/15/2010	MW-09	103.83	===	6.46			97.37	97.37		
4/22/2010	MW-09	103.83		6.12			97.71	97.71		
5/3/2010	MW-09	103.83		6.05	****		97.78	97.78		*****

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-13	107.78		6.79			100.99	100.99		
2/21/2006	MW-13	107.78		7.99			99.79	99.79		
3/7/2006	MW-13	107.78		7.39			100.39	100.39		
5/18/2006	MW-13	107.78		6.82			100.96	100.96		
6/28/2006	MW-13	107.78		6.90			100.88	100.88		
8/16/2006	MW-13	107.78		7.16			100.62	100.62		
9/29/2006	MW-13	107.78		7.21			100.57	100.57		
10/20/2006	MW-13	107.78		6.69			101.09	101.09		
11/22/2006	MW-13	107.78		6.91			100.87	100.87		
12/15/2006	MW-13	107.78		7.41			100.37	100.37		
1/23/2007	MW-13	107.78		7.31			100.47	100.47		
2/2/2007	MW-13	107.78		7.51			100.27	100.27		
3/5/2007	MW-13	107.78		6.57			101.21	101.21		
5/1/2007	MW-13	107.78		7.05			100.73	100.73		
6/22/2007	MW-13	107.78		7.45		**-	100.33	100.33		
6/26/2007	MW-13	107.78		7.62			100.16	100.16		
7/6/2007	MW-13	107.78		6.99			100.79	100.79		
8/1/2007	MW-13	107.78		7.15			100.63	100.63		
8/7/2007	MW-13	107.78		7.25			100.53	100.53		
9/14/2007	MW-13	107.78		7.38			100.40	100.40		
10/8/2007	MW-13	107.78		7.55			100.40	100.40		
	MW-13	107.78		7.33			100.23	100.23		
11/20/2007										
12/26/2007	MW-13	107.78		7.09			100.69	100.69		
1/2/2008	MW-13	107.78		7.00			100.78	100.78		
3/5/2008	MW-13	107.78		7.00			100.78	100.78		
4/23/2008	MW-13	107.78		7.44			100.34	100.34		
5/12/2008	MW-13	107.78		6.75			101.03	101.03		
6/27/2008	MW-13	107.78	*	7.35			100.43	100.43		
8/5/2008	MW-13	107.78		7.24			100.54	100.54		
9/10/2008	MW-13	107.78		6.94			100.84	100.84		
10/27/2008	MW-13	107.78		6.66			101.12	101.12		
11/4/2008	MW-13	107.78		7.21			100.57	100.57		
1/5/2009	MW-13	107.78		7.31			100.47	100.47		
2/27/2009	MW-13	107.78		7.78			100.00	100.00		
3/9/2009	MW-13	107.78		7.64			100.14	100.14		
4/20/2009	MW-13	107.78		7.18			100.60	100.60		
4/29/2009	MW-13	107.78		7.20			100.58	100.58		
5/6/2009	MW-13	107.78		6.59			101.19	101.19		
6/2/2009	MW-13	107.78		7.49			100.29	100.29		
7/6/2009	MW-13	107.78		7.10			100.68	100.68		
8/14/2009	MW-13	107.78		7.25			100.53	100.53		
9/28/2009	MW-13	107.78		7.08			100.70	100.70		
10/13/2009	MW-13	107.78		7.41			100.37	100.37		
11/23/2009	MW-13	107.78		7.18			100.60	100.60	~	
12/2/2009	MW-13	107.78	~	7.35			100.43	100.43		
1/12/2010	MW-13	107.78		7.43		~~~	100.35	100.35	~	
2/2/2010	MW-13	107.78	~	7.28			100.50	100.50		
3/2/2010	MW-13	107.78		6.49			101.29	101.29		
3/15/2010	MW-13	107.78	~~-	5.99			101.79	101.79		
4/15/2010	MW-13	107.78		2.37			105.41	105.41		
4/22/2010	MW-13	107.78		7.32			100.46	100.46		
5/3/2010	MW-13	107.78		6.52			100.40	101.26		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-14	107.74		5.72			102.02	102.02		
2/21/2006	MW-14	107.74		6.97			100.77	100.77		
3/7/2006	MW-14	107.74		6.58			101.16	101.16		
5/18/2006	MW-14	107.74		5.99	*****		101.75	101.75		
6/28/2006	MW-14	107.74		5.95			101.79	101.79		
8/16/2006	MW-14	107.74		6.22			101.52	101.52		
9/29/2006	MW-14	107.74		6,38			101.36	101.36		
10/20/2006	MW-14	107.74		5,85			101.89	101.89		
11/22/2006	MW-14	107.74		6.23			101.51	101.51		
12/15/2006	MW-14	107.74		6.67			101.07	101.07		
1/23/2007	MW-14	107.74		6.63			101.11	101.11		
2/2/2007	MW-14	107.74		6.94			100.80	100.80		
3/5/2007	MW-14	107.74		5,79			101.95	101.95		
5/1/2007	MW-14	107.74		5.68	*****		102.06	102.06		
6/22/2007	MW-14	107.74		6.54			101.20	101.20		
6/26/2007	MW-14	107.74		6.68			101.06	101.06		***
7/6/2007	MW-14	107.74		5.93			101.81	101.81		
8/1/2007	MW-14	107.74		6.05			101.69	101.69	****	
8/7/2007	MW-14	107.74		6,25			101.49	101.49		
9/14/2007	MW-14	107.74		6.54			101.20	101.20		
10/8/2007	MW-14	107.74	***	6.95			100.79	100.79		
11/20/2007	MW-14	107.74		6.45	****		101.29	101.29		
12/26/2007	MW-14	107.74	-	6.01			101.73	101.73		
1/2/2008	MW-14	107.74		5.85			101.89	101.89		
3/5/2008	MW-14	107.74	-	6.19			101.55	101.55		
4/23/2008	MW-14	107.74		6.80			100.94	100.94		
5/6/2008	MW-14	107.74		5.57			102.17	102.17		
	MW-14	107.74		6.00		a	101.74	101.74		
5/12/2008		107.74		6.53			101.74	101.21		
6/27/2008	MW-14	107.74		6.33			101.41	101.41		
8/5/2008	MW-14			5.68			102.06	102.06		
9/10/2008	MW-14	107.74		6.00			101.74	101.74		
10/27/2008	MW-14	107.74	****	6.25			101.74	101.74		
11/4/2008	MW-14	107.74		6.25		444	101.43	101.49		
1/5/2009	MW-14	107.74					100.80	100.80		
2/27/2009	MW-14	107.74		6.94	****		100.79	100.79		
3/9/2009	MW-14	107.74		6.95			100.79	100.79		
4/20/2009	MW-14	107.74		6.39			101.33	101.33		
4/29/2009	MW-14	107.74		6.30				100.99		
6/2/2009	MW-14	107.74		6.75			100.99	98.81		
7/6/2009	MW-14	107.74		8.93			98.81			
8/14/2009	MW-14	107.74		6.33			101.41	101.41		
9/28/2009	MW-14	107.74		6.12			101.62	101.62		
10/13/2009	MW-14	107.74		6.53			101.21	101.21		
11/23/2009	MW-14	107.74		6.27			101.47	101.47		
12/2/2009	MW-14	107.74		6.68			101.06	101.06		
1/12/2010	MW-14	107.74		6.64			101.10	101.10		
2/2/2010	MW-14	107.74		6.43			101.31	101.31		
3/2/2010	MW-14	107.74		5.44			102.30	102.30		
3/15/2010	MW-14	107.74		5.09			102.65	102.65		
4/15/2010	MW-14	107.74		6.55	~~~		101.19	101.19		
4/22/2010	MW-14	107.74		6.94			100.80	100.80		
5/3/2010	MW-14	107.74	~~~	5.61			102.13	102,13		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-15	103.99		2.87			101.12	101.12		
2/21/2006	MW-15	. 103.99		2.94			101.05	101.05		
3/7/2006	MW-15	103.99		3.31			100.68	100.68		
5/18/2006	MW-15	103.99		3.10			100.89	100.89		
6/28/2006	MW-15	103.99		2.85		***	101.14	101.14		
8/16/2006	MW-15	103.99		3.02			100.97	100.97		
9/29/2006	MW-15	103.99		3.00			100.99	100.99		
10/20/2006	MW-15	103.99		2.93			101.06	101.06		
11/22/2006	MW-15	103.99		2.93			101.06	101.06		
12/15/2006	MW-15	103.99		3.29			100.70	100.70		
2/2/2007	MW-15	103.99		3.58			100.41	100.41		
3/5/2007	MW-15	103.99		3.34			100.65	100.65		
5/1/2007	MW-15	103.99		2.70			101.29	101.29		
6/22/2007	MW-15	103.99		3,25			100.74	100.74		
6/26/2007	MW-15	103.99		3.37			100.62	100.62		
7/6/2007	MW-15	103.99		3.38			100.61	100.61		
8/1/2007	MW-15	103.99		2.99			101.00	101.00		
8/7/2007	MW-15	103.99		3.09			100.90	100.90		
9/14/2007	MW-15	103.99		3.48			100.51	100.51		
10/8/2007	MW-15	103.99		3.79			100.20	100.20		
11/20/2007	MW-15	103.99		3,66			100.33	100.33		
12/26/2007	MW-15	103.99		3.27			100.72	100.72		
1/2/2008	MW-15	103.99		3,15			100.84	100.84		
3/5/2008	MW-15	103.99		3.16			100,83	100.83		
4/23/2008	MW-15	103.99		3.50			100.49	100.49		
5/12/2008	MW-15	103.99		3.22			100.77	100.77		
6/27/2008	MW-15	103.99		3.13			100.86	100.86		
8/5/2008	MW-15	103.99		3,49			100.50	100.50		
9/10/2008	MW-15	103.99		3,46			100.53	100.53		
10/27/2008	MW-15	103.99		3.39			100.60	100.60		
11/4/2008	MW-15	103.99		NG						
1/5/2009	MW-15	103.99		3,33			100.66	100.66		
2/27/2009	MW-15	103.99		3.95	****		100.04	100.04		
3/9/2009	MW-15	103.99		3.89			100.04	100.04		
4/20/2009	MW-15	103.99		3.57			100.10	100.10		
4/29/2009	MVV-15	103.99		3.48			100.42	100.42		
5/6/2009	MVV-15	103.99		3.48			100.71	100.31		
	MW-15	103.99		3.49			100.71	100.77		
6/2/2009 7/6/2009	MVV-15	103.99		2.90			100.00	101.09		
	MW-15			3.22			107.09	100.77		
8/14/2009		103.99								
9/28/2009 10/13/2009	MW-15 MW-15	103.99 103.99		3.54 3.67			100.45 100.32	100.45 100.32		
11/23/2009	MW-15	103.99		3,39			100.52	100.52		
12/2/2009	MW-15	103.99		3,62			100.80	100.60		
	MW-15	103.99		3,39			100.57	100.57		
1/12/2010 2/2/2010	MW-15	103.99		3,48			100.50	100.60		
				3,46 2,45			100.51			
3/2/2010	MW-15	103.99						101.54		
3/15/2010	MW-15	103.99		1.89			102.10	102.10		
4/15/2010	MW-15	103.99		2.94			101.05	101.05		
4/22/2010	MW-15	103.99		2.94			101.05	101.05		
5/3/2010	MW-15	103.99		2,48			101.51	101.51		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well #	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-16	104.03		2.94			101.09	101.09		
2/21/2006	MW-16	104.03		3.09			100.94	100.94		
3/7/2006	MW-16	104.03		3.18			100.85	100.85		
5/18/2006	MW-16	104.03		2.89			101.14	101.14		
6/28/2006	MW-16	104.03		2.89			101.14	101.14		
8/16/2006	MW-16	104.03		2.91			101.12	101.12		
9/29/2006	MW-16	104.03		2.98			101.05	101.05		
10/20/2006	MW-16	104.03		2.95			101.08	101.08		
11/22/2006	MW-16	104.03		2.91			101.12	101.12		
12/15/2006	MW-16	104.03		3.21			100.82	100.82		
1/23/2007	MW-16	104.03		3.36			100.67	100.67		
2/2/2007	MW-16	104.03		3.49			100.54	100.54		
3/5/2007	MW-16	104.03		3.13			100.90	100.90		
5/1/2007	MW-16	104.03		2.64		****	101.39	101.39		
6/22/2007	MW-16	104.03		3.13			100.90	100.90		
6/26/2007	MW-16	104.03		2.17			101.86	101.86		
7/6/2007	MW-16	104.03		3.15			100.88	100.88		****
8/1/2007	MW-16	104.03		NG						~
8/7/2007	MW-16	104.03		NG						
9/14/2007	MW-16	104.03		NG						
10/8/2007	MW-16	104.03		3.58			100.45	100.45		
11/20/2007	MW-16	104.03		3.51			100.43	100.43		
12/26/2007	MW-16	104.03		3.16			100.87	100.87		
1/2/2008	MW-16	104.03		3.05		===	100.98	100.98		~~~
3/5/2008	MW-16	104.03		3.09			100.94	100.98		
	MW-16			3.42						
4/23/2008		104.03	***				100.61	100.61		
5/12/2008	MW-16	104.03		3.00			101.03	101.03	*****	
6/27/2008	MW-16	104.03		3.03			101.00	101.00		
8/5/2008	MW-16	104.03		3.29	~~~		100.74	100.74		
9/10/2008	MW-16	104.03		3.18		***	100.85	100.85		~~~
10/27/2008	MW-16	104.03		3.19			100.84	100.84		
11/4/2008	MW-16	104.03		4.00			100.03	100.03		
1/5/2009	MW-16	104.03		3.18			100.85	100.85		
2/27/2009	MW-16	104.03		3.79			100.24	100.24		
3/9/2009	MW-16	104.03		3.81			100.22	100.22		
4/20/2009	MW-16	104.03		3.44			100.59	100.59		
4/29/2009	MW-16	104.03		3.31		-	100.72	100.72		
5/6/2009	MW-16	104.03		3.12			100.91	100.91		*****
6/2/2009	MW-16	104.03		3.39			100.64	100.64		
7/6/2009	MW-16	104.03		NG					***	
8/14/2009	MW-16	104.03		NG						
9/28/2009	MW-16	104.03		2.98			101,05	101.05		
0/13/2009	MW-16	104.03		3.49			100.54	100.54		
1/23/2009	MW-16	104.03		NG						****
12/2/2009	MW-16	104.03		3.46			100.57	100.57		
1/12/2010	MW-16	104.03		3.32			100.71	100.71		
2/2/2010	MW-16	104.03		3.28			100.75	100,75		
3/2/2010	MW-16	104.03		2.12			101.91	101.91		
3/15/2010	MW-16	104.03		NG						Obstruction
4/15/2010	MW-16	104.03		2.24			101.79	101.79		
1/22/2010	MW-16	104.03		2.86			101.17	101.17		
5/3/2010	MW-16	104.03		1.86			102.17	102.17		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-17	104.06		2.25			101.81	101.81		***
2/21/2006	MW-17	104.06		3.11			100.95	100.95		
3/7/2006	MW-17	104,06		3.44			100.62	100.62		
5/18/2006	MW-17	104.06		3.14			100.92	100.92		
6/28/2006	MW-17	104.06		2.96			101.10	101.10		
8/16/2006	MW-17	104.06		3.12			100.94	100.94		
9/29/2006	MW-17	104.06		3,15			100.91	100.91		
10/20/2006	MW-17	104.06		3.04			101.02	101.02		
11/22/2006	MW-17	104.06		3.04			101.02	101.02		
12/15/2006	MW-17	104.06		3.60			100.46	100.46		
1/23/2007	MW-17	104.06		3,68			100.38	100.38		
2/2/2007	MW-17	104.06		3.90			100.16	100.16		
3/5/2007	MW-17	104.06		3.28			100.78	100.78		
5/1/2007	MW-17	104.06		2.73			101.33	101.33		
6/22/2007	MW-17	104.06		3.38			100.68	100.68	***	
6/26/2007	MW-17	104.06		3.54			100.52	100.52		
7/6/2007	MW-17	104.06		3.48			100.58	100.58		
8/1/2007	MW-17	104.06		2.99			101.07	101.07		
8/7/2007	MW-17	104.06		3,15			100.91	100.91		
9/14/2007	MW-17	104.06		3.65			100.41	100.41		
10/8/2007	MW-17	104.06		3,97			100.09	100.09		
	MW-17	104.06		3.72			100.34	100.34		
11/20/2007	MW-17	104.06		3,27	***		100.79	100.79		
12/26/2007	MW-17	104.06		3.11			100.95	100.95		
1/2/2008		104.06		3.19			100.87	100.87		
3/5/2008	MW-17			3.70			100.36	100.36		
4/23/2008	MW-17	104.06		3.70			100.86	100.86		
5/12/2008	MW-17	104.06					100.83	100.83		
6/27/2008	MW-17	104.06		3.23			100.65	100.65		***
8/5/2008	MW-17	104.06		3.41						
9/10/2008	. MW-17	104.06		3.00			101.06	101.06		
10/27/2008	MW-17	104.06		3,66			100.40	100.40		
11/4/2008	MW-17	104.06		3.53			100.53	100.53		
1/5/2009	MW-17	104.06		3.31			100.75	100.75		
2/27/2009	MW-17	104.06		4.21			99.85	99.85		
3/9/2009	MW-17	104.06		4.16			99.90	99.90		
4/20/2009	MW-17	104.06		3.63			100.43	100.43		
4/29/2009	MW-17	104.06		3,35			100.71	100.71		
5/6/2009	MW-17	104.06		3.23			100.83	100.83		
6/2/2009	MW-17	104.06		3.65			100.41	100.41		
7/6/2009	MW-17	104,06		2.90			101.16	101.16		
8/14/2009	MW-17	104.06		3.12			100.94	100.94		
9/28/2009	MW-17	104.06		3,64			100.42	100.42		
10/13/2009	MW-17	104.06		3.68			100.38	100.38		
11/23/2009	MW-17	104.06		4.38			99.68	99.68		
12/2/2009	MW-17	104.06		3.65			100.41	100.41		
1/12/2010	MW-17	104.06		3.59			100.47	100.47		
2/2/2010	MW-17	104.06		3.46			100.60	100.60	~	
3/2/2010	MW-17	104,06		2.27			101.79	101.79		
3/15/2010	MW-17	104.06		1.66			102.40	102.40		
4/15/2010	MW-17	104.06		3.17			100.89	100.89		
4/22/2010	MW-17	104.06		2.58			101.48	101.48		
5/3/2010	MW-17	104.06		NG						

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-18	104.05	~	2.56			101.49	101.49		
2/21/2006	MW-18	104.05		3.12			100.93	100.93		
3/7/2006	MW-18	104.05	~~~	3.41			100.64	100.64		
5/18/2006	MW-18	104.05		3.12			100.93	100.93		
6/28/2006	MW-18	104.05		2.96			101.09	101.09		
8/16/2006	MW-18	104.05		3.11			100.94	100.94		
9/29/2006	MW-18	104.05		3.15			100.90	100.90		
10/20/2006	MW-18	104.05		3.04			101.01	101.01		
11/22/2006	MW-18	104.05		3.04			101.01	101.01		
12/15/2006	MW-18	104.05		3.57			100.48	100.48		
1/23/2007	MW-18	104.05		3.64			100.41	100.41		
2/2/2007	MW-18	104.05		4.04			100.01	100.01		
3/5/2007	MW-18	104.05		3.24			100.81	100.81		
5/1/2007	MW-18	104.05		2.73			101.32	101.32		
6/22/2007	MW-18	104.05		3.32			100.73	100.73		
6/26/2007	MW-18	104.05		3.47			100.58	100.58		
7/6/2007	MW-18	104.05		3.43			100.62	100.62		
8/1/2007	MW-18	104.05		2.98			101.07	101.07		
8/7/2007	MW-18	104.05		3.13			100.92	100.92		
9/14/2007	MW-18	104.05		NG				100.02		
10/8/2007	MW-18	104.05		4.11			99.94	99.94		
11/20/2007	MW-18	104.05		3.69			100,36	100,36		
	MW-18	104.05		3.21			100.84	100.84		
12/26/2007				3.10			100.04			
1/2/2008	MW-18	104.05						100.95		
3/5/2008	MW-18	104.05		3.17			100.88	100.88		
4/23/2008	MW-18	104.05		3.63			100.42	100.42		
5/12/2008	MW-18	104.05		3.17			100.88	100.88		
6/27/2008	MW-18	104.05		3.17			100.88	100.88		***-
8/5/2008	MW-18	104.05	***	3.35			100.70	100.70		
9/10/2008	MW-18	104.05		3.06			100.99	100.99		
10/27/2008	MW-18	104.05		3.54			100.51	100.51		
11/4/2008	MW-18	104.05		3.45			100.60	100.60		
1/5/2009	MW-18	104.05		3.30			100.75	100.75		
2/27/2009	MW-18	104.05		4.28			99.77	99.77		
3/9/2009	MW-18	104.05		4.21			99.84	99.84		
4/20/2009	MW-18	104.05		3,58			100.47	100.47		
4/29/2009	MW-18	104.05		3.31			100.74	100.74		
5/6/2009	MW-18	104.05		3.24			100.81	100.81		
6/2/2009	MW-18	104.05		3.64			100.41	100.41		
7/6/2009	MW-18	104.05		2.87			101.18	101.18		
8/14/2009	MW-18	104.05		3.14			100.91	100.91		
9/28/2009	MW-18	104.05		3.62			100.43	100.43		
10/13/2009	MW-18	104.05		3.69			100.36	100.36		
11/23/2009	MW-18	104.05		3.34			100.71	100.71		
12/2/2009	MW-18	104.05		3.63			100.42	100.42		
1/12/2010	MW-18	104.05		3.56			100.42	100.42		
2/2/2010	MW-18	104.05		3.43			100.43	100.43		
	MW-18	104.05		2.26			100.02	100.02		
3/2/2010										
3/15/2010	MW-18	104.05		1.61			102.44	102.44		
4/15/2010	MW-18	104.05		3.01			101.04	101.04		
4/22/2010	MW-18	104.05		3.06			100.99	100.99		
5/3/2010	MW-18	104.05		2.12			101.93	101.93		

Date	Well #	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-19	104.20		3.10			101.10	101.10		
2/21/2006	MW-19	104.20		3.61		~	100.59	100.59		
3/7/2006	MW-19	104.20		4.29			99.91	99.91		
5/18/2006	MW-19	104.20		3.69			100.51	100.51		
6/28/2006	MW-19	104.20		3.53			100.67	100.67		
8/16/2006	MW-19	104.20	3,80	3.81	0.01	100.40	100.39	100.40		
9/29/2006	MW-19	104.20		3.70			100.50	100.50		
10/20/2006	MW-19	104.20		3.53			100.67	100.67		
11/22/2006	MW-19	104.20		3.58			100.62	100.62		
12/15/2006	MW-19	104.20		4.36			99.84	99.84		
1/23/2007	MW-19	104.20		4.64			99.56	99.56		
2/2/2007	MW-19	104.20		4.73		~	99.47	99.47		
3/5/2007	MW-19	104.20		4.27			99.93	99.93		
5/1/2007	MW-19	104.20		3.29			100.91	100.91		
6/22/2007	MW-19	104.20		3.99			100.21	100.21		
6/26/2007	MW-19	104.20		4.29			99,91	99.91		
7/6/2007	MW-19	104.20		4.24			99,96	99.96		
8/1/2007	MW-19	104.20	****	3.55			100.65	100.65		
8/7/2007	MW-19	104.20		3.71			100.49	100.49		
9/14/2007	MW-19	104.20		NG			~			
10/8/2007	MW-19	104.20	4.56	4.61	0.05	99.64	99.59	99.63		
11/20/2007	MW-19	104.20		4.42			99.78	99.78		
12/26/2007	MW-19	104.20		3.85			100.35	100.35		
12/26/2007	MW-19	104.20		NG						
3/5/2008	MW-19	104.20		3.59			100.61	100.61		
4/23/2008	MW-19	104.20		4.30			99.90	99.90		
5/12/2008	MW-19	104.20		3,57			100.63	100.63		
6/27/2008	MW-19	104.20		3.63			100.57	100.57		
8/5/2008	MW-19	104.20		3.39			100.81	100.81	*****	~
9/10/2008	MW-19	104.20		3.59			100,61	100.61		
10/27/2008	MW-19	104.20		3.98			100.22	100.22		~~~
11/4/2008	MW-19	104.20		4.38			99.82	99.82		~
1/5/2009	MW-19	104.20		3.80			100.40	100.40		
2/27/2009	MW-19	104.20		4.91			99.29	99.29		
3/9/2009	MW-19	104.20		4.69			99.51	99.51		
4/20/2009	MW-19	104.20		4.29			99.91	99.91		
4/29/2009	MW-19	104.20		3.98			100.22	100.22		
5/6/2009	MW-19	104.20		3.69			100.51	100.51		
6/2/2009	MW-19	104.20		4.25			99.95	99.95	***	
7/6/2009	MW-19	104.20		3.28			100.92	100.92		
8/14/2009	MW-19	104.20		3.49			100.32	100.71		
9/28/2009	MW-19	104.20		4.09			100.77	100.11		
10/13/2009	MW-19	104.20		4.33		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	99.87	99.87		
11/23/2009	MW-19	104.20	****	3.76			100,44	100,44		
12/2/2009	MW-19	104.20		4.36			99.84	99.84		
1/12/2010	MW-19	104.20		4.29			99.91	99.91		
2/2/2010	MW-19	104.20		4.34			99,86	99.86		
3/2/2010	MW-19	104.20		2.72			101.48	101.48		
3/15/2010	MW-19	104.20		1.92			101.46	101.48		
4/15/2010	MW-19	104.20		3.57			102.28	102.26		
4/22/2010	MW-19	104.20		3.58						
							100.62	100.62		
5/3/2010	MW-19	104.20		2.98			101.22	101.22		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-20	103.90		2.54			101.36	101.36		=#-4
2/21/2006	MW-20	103.90		2.80			101.10	101.10		
3/7/2006	MW-20	103.90		3.14			100.76	100.76		
5/18/2006	MW-20	103.90		2.93			100.97	100.97		
6/28/2006	MW-20	103.90		2.69			101.21	101.21		
8/16/2006	MW-20	103.90		NG						
9/29/2006	MW-20	103.90		2.87			101.03	101.03		
10/20/2006	MW-20	103.90		2.55			101.35	101.35		
11/22/2006	MW-20	103.90		2.79			101.11	101.11		
12/15/2006	MW-20	103.90		3.10			100.80	100.80		
2/2/2007	MW-20	103.90		3.46			100.44	100.44		
3/5/2007	MW-20	103.90		3.24			100.66	100.66		
5/1/2007	MW-20	103.90	2.55	2.56	0.01	101.35	101.34	101.35		
6/22/2007	MW-20	103.90		3.08		***	100.82	100.82		
6/26/2007	MW-20	103.90		3.22			100.68	100.68		
7/6/2007	MW-20	103.90		3.38			100.52	100.52		
8/1/2007	MW-20	103.90		2.89		****	101.01	101.01		
8/7/2007	MW-20	103.90		2.99			100.91	100.91		
9/14/2007	MW-20	103.90		2.36			101.54	101.54		
10/8/2007	MW-20	103.90		3.65			100.25	100.25		
11/20/2007	MW-20	103.90		3.59			100,31	100.31		
	MW-20	103.90		3.20			100.70	100.70		****
12/26/2007	MW-20	103.90		3.05			100.85	100.85	erena.	
1/2/2008	MW-20	103.90	~~~	NG						
3/5/2008			244	3.34			100.56	100.56		
4/23/2008	MW-20	103.90		3.10			100.80	100.80		***
5/12/2008	MW-20	103.90		3.10			100.80	100.80		
6/27/2008	MW-20	103.90					100.57	100.57		-
8/5/2008	MW-20	103.90		3.33			100.57	100.57		
9/10/2008	MW-20	103.90		3,39				100.51		
10/27/2008	MW-20	103.90		3.25		****	100.65			
11/4/2008	MW-20	103.90		3.35			100.55	100.55		
1/5/2009	MW-20	103.90		3.15			100.75	100.75		
2/27/2009	MW-20	103.90		3.76			100.14	100.14		
3/9/2009	MW-20	103.90		3.71			100.19	100.19		
4/20/2009	MW-20	103.90		3.42		*	100.48	100.48		
4/29/2009	MW-20	103.90		3.36			100.54	100.54		
5/6/2009	MW-20	103.90		3.09			100.81	100.81		
6/2/2009	MW-20	103.90		3.29			100.61	100.61		
7/6/2009	MW-20	103.90		2.73			101.17	101.17		
8/14/2009	MW-20	103.90		3.03			100.87	100.87		
9/28/2009	MW-20	103.90		3.38			100.52	100.52		
10/13/2009	MW-20	103.90		3.49			100.41	100.41		
11/23/2009	MW-20	103.90		3.24			100.66	100.66		
12/2/2009	MW-20	103.90		3.44		****	100.46	100.46		
1/12/2010	MW-20	103.90		3.24			100.66	100.66		
2/2/2010	MW-20	103.90		3.35			100.55	100.55		
3/2/2010	MW-20	103.90		2,18			101.72	101.72		
3/15/2010	MW-20	103.90		1.68			102,22	102.22		
4/15/2010	MW-20	103.90		2.75			101.15	101.15		
4/22/2010	MW-20	103.90		2.76			101.14	101.14		
5/3/2010	MW-20	103.90		2.61			101.29	101.29		

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-21	104.63		4.93			99.70	99.70		
2/21/2006	MW-21	104.63		5.28			99.35	99.35		
3/7/2006	MW-21	104.63		5.17			99.46	99.46		
5/18/2006	MW-21	104.63		4.94			99.69	99.69		
6/28/2006	MW-21	104.63		4.92			99.71	99.71		
8/16/2006	MW-21	104.63		5.11			99.52	99.52		
9/29/2006	MW-21	104.63		4.99			99.64	99.64		
10/20/2006	MW-21	104.63		3.71			100.92	100.92		
11/22/2006	MW-21	104.63		4.80			99.83	99.83		
12/15/2006	MW-21	104.63		5.20			99.43	99.43		
1/23/2007	MW-21	104.63		5.03			99.60	99.60		
2/2/2007	MW-21	104.63		3.25			101.38	101.38		
3/5/2007	MW-21	104.63		4.84			99.79	99.79		
5/1/2007	MW-21	104.63		4.91			99.72	99.72		
6/22/2007	MW-21	104.63		5.15			99.48	99.48		
6/26/2007	MW-21	104.63		5.31			99.32	99.32		
7/6/2007	MW-21	104.63		5.09			99.54	99.54		
8/1/2007	MW-21	104.63		4.89			99.74	99.74		
8/7/2007	MW-21	104.63		5.05			99.58	99.58		
9/14/2007	MW-21	104.63		5.04			99.59	99.59		
10/8/2007	MW-21	104.63		4.15			100.48	100.48		
11/20/2007	MW-21	104.63		5.02			99.61	99.61		
12/26/2007	MW-21	104.63		4.71			99.92	99.92		
1/2/2008	MW-21	104.63		5.05			99.58	99.58		
3/5/2008	MW-21	104.63		4.99			99.64	99.64		
4/23/2008	MW-21	104.63		5.09			99.54	99.54		
5/12/2008	MW-21	104.63		4.88			99.75	99.75		
6/27/2008	MW-21	104.63		5.08			99.55	99.55		
8/5/2008	MW-21	104.63		4.98			99.65	99.65		
9/10/2008	MW-21	104.63		4.97			99.66	99.66		
10/21/2008	MW-21	104.63		_ NG						Abandoned
3/2/2010	MW-21R			2.96						
3/15/2010	MW-21R			2.49						
4/15/2010	MW-21R			3.95						
4/22/2010	MW-21R			3.89						
5/3/2010	MW-21R			3.29						

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-22	104.57		4.54			100.03	100.03		
2/21/2006	MW-22	104.57		5.01			99.56	99.56		
3/7/2006	MW-22	104.57	4	5.18			99.39	99.39		
5/18/2006	MW-22	104.57		4.67			99.90	99,90		
6/28/2006	MW-22	104.57	~~~	4.66			99.91	99.91		
8/16/2006	MW-22	104.57	***	4.91			99.66	99.66		
9/29/2006	MW-22	104.57		4.82			99.75	99.75		~~~
10/20/2006	MW-22	104.57		3.97			100.60	100.60		
11/22/2006	MW-22	104.57	~~~	4.24			100.33	100.33		
12/15/2006	MW-22	104.57		5.17			99.40	99.40		
1/23/2007	MW-22	104.57		4.91			99.66	99.66		
2/2/2007	MW-22	104.57	~	4.41			100.16	100.16		
3/5/2007	MW-22	104.57		4.02			100.55	100.55		~
5/1/2007	MW-22	104.57	~~~	4.70			99.87	99.87		
6/22/2007	MW-22	104.57		4.99			99.58	99:58		
6/26/2007	MW-22	104.57		5.14			99.43	99.43		***
7/6/2007	MW-22	104.57	R	4.71			99.86	99.86		
8/1/2007	MW-22	104.57		4,59			99.98	99.98		
8/7/2007	MW-22	104.57		4,72			99.85	99,85		
9/14/2007	MW-22	104.57		4.79			99.78	99,78		***
10/8/2007	MW-22	104.57		4.54			100.03	100.03		
11/20/2007	MW-22	104.57		4.81			99.76	99.76		
12/26/2007	MW-22	104.57		4.71			99.86	99.86		
1/2/2008	MW-22	104.57		4,85			99.72	99,72		
3/5/2008	MW-22	104.57		4.75	~		99.82	99.82		
4/23/2008	MW-22	104.57		5.03			99.54	99,54		
5/12/2008	MW-22	104.57		4.05	*****		100.52	100.52		
6/27/2008	MW-22	104.57		5.02			99.55	99.55		
8/5/2008	MW-22	104.57		4.75			99.82	99.82		
9/10/2008	MW-22	104,57		4.65			99.92	99.92		
10/27/2008	MW-22	104.57		NG	~					Abandoned
3/2/2010	MW-22R			2.81						
3/15/2010	MW-22R			2.53						
4/15/2010	MW-22R			4.06						
4/22/2010	MW-22R			3.92						
5/3/2010	MW-22R			3.10						

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-23	105,33		3.74			101.59	101.59		
2/21/2006	MW-23	105.33		3.74	~~~		101.59	101.59		
3/7/2006	MW-23	105.33		4.10			101.23	101.23		
5/18/2006	MW-23	105.33		3.49	***		101.84	101.84		
6/28/2006	MW-23	105.33		3.60			101.73	101.73		
8/16/2006	MW-23	105.33		3.82	~		101.51	101.51		
9/29/2006	MW-23	105.33		3.95	~		101.38	101.38		
10/20/2006	MW-23	105.33		3.53	*		101.80	101.80		
11/22/2006	MW-23	105.33		3.82			101.51	101.51		
12/15/2006	MW-23	105.33		4.18			101.15	101.15		
1/23/2007	MW-23	105.33		4.18	~		101.15	101.15		
2/2/2007	MW-23	105,33		4.44			100.89	100.89		
3/5/2007	MW-23	105,33		NG						
5/1/2007	MW-23	105.33		3.54			101.79	101.79		
6/22/2007	MW-23	105.33		4.11			101.22	101.22		
6/26/2007	MW-23	105.33		4.19	-		101.14	101.14		
	MW-23	105.33		3.72			101.61	101.61		
7/6/2007	MW-23	105.33		3.71			101.62	101.62		
8/1/2007		105.33		3.89			101.44	101.44		
8/7/2007	MW-23			4.19			101.14	101.14		
9/14/2007	MW-23	105,33					100.81	100.81		
10/8/2007	MW-23	105,33		4.52			100.87	100.81		
11/20/2007	MW-23	105.33		4.12				101.21		
12/26/2007	MW-23	105.33		3.69			101.64			
1/2/2008	MW-23	105.33		3.57			101.76	101.76		
3/5/2008	MW-23	105.33		3.82			101.51	101.51		
4/23/2008	MW-23	105.33		4.30			101.03	101.03		
5/12/2008	MW-23	105.33		3.73			101.60	101.60		
6/27/2008	MW-23	105.33	3.99	4.00	0.01	101.34	101.33	101.34		
8/5/2008	MW-23	105.33		3.99			101.34	101.34		
9/10/2008	MW-23	105.33		3.39		****	101.94	101.94		
10/27/2008	MW-23	105.33		3.92			101.41	101.41		
11/4/2008	MW-23	105,33		3.89			101.44	101.44		
1/5/2009	MW-23	105.33		3.98			101.35	101.35		
2/27/2009	MW-23	105.33		4.45		~	100.88	100.88		
3/9/2009	MW-23	105,33		4.49		~~~	100.84	100.84		
4/29/2009	MW-23	105.33		3.23		~	102.10	102.10		
	MW-23	105.33		3.50			101.83	101.83		
5/6/2009	MW-23	105.33		4.34		~	100.99	100.99	~	
6/2/2009	MW-23	105.33		3.64		~	101.69	101.69	~	
7/6/2009	MW-23	105.33		3.97		****	101.36	101.36		
8/14/2009		105.33		3.93			101.40	101.40		
9/28/2009	MW-23			3.93 4.18			101.40	101.15		
10/13/2009	MW-23	105.33		3.94			101.13	101.13	~	
11/23/2009	MW-23	105.33					101.39	101.39		
12/2/2009	MW-23	105.33	***	4.22				101.11	~~~	
1/12/2010	MW-23	105,33		4.16			101.17			
2/2/2010	MW-23	105.33		4.04			101.29	101.29		
3/2/2010	MW-23	105.33		2.18			103.15	103,15		
3/15/2010	MW-23	105.33		1.89			103.44	103.44		
4/15/2010	MW-23	105.33		3.98			101.35	101.35		
4/22/2010	MW-23	105.33		4.10			101.23	101.23		
5/3/2010	MW-23	105,33		3.65			101.68	101.68		

				NISOLOS	PILL NO. 87-0				<u></u>	
Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-24	105.09		3.30			101.79	101.79		
2/21/2006	MW-24	105.09		3.69			101.40	101.40		
3/7/2006	MW-24	105.09		3.99			101.10	101.10		
5/18/2006	MW-24	105,09		3.65			101.44	101.44		
6/28/2006	MW-24	105.09		3.64			101.45	101.45		
8/16/2006	MW-24	105.09		3.79			101.30	101.30		
9/29/2006	MW-24	105.09		3.91			101.18	101.18		
10/20/2006	MW-24	105.09		3.66			101.43	101.43		
11/22/2006	MW-24	105.09		3.76			101.33	101.33		
12/15/2006	MW-24	105.09		4.10			100.99	100.99		
1/23/2007	MW-24	105.09		4.11			100.98	100.98		
2/2/2007	MW-24	105.09		4.31			100.78	100.78		
3/5/2007	MW-24	105.09		3.46			101.63	101.63		
5/1/2007	MW-24	105.09		3.50			101.59	101.59		
6/22/2007	MW-24	105.09		4.05			101.04	101.04		
6/26/2007	MW-24	105.09		4.13	=n=		100.96	100.96		
7/6/2007	MW-24	105.09		3.92			101.17	101.17		
8/1/2007	MW-24	105.09		3.72			101.37	101.37		
	MW-24	105.09		3.86			101.23	101.23		
8/7/2007		105.09		4,16			100,93	100.93	*	
9/14/2007	MW-24	105.09		4.45			100.64	100.64		
10/8/2007	MW-24			4.45			100.98	100.98		
11/20/2007	MW-24	105.09					100.35	100.35		
12/26/2007	MW-24	105.09		3.74				101.33		
1/2/2008	MW-24	105.09		3.62			101.47			
3/5/2008	MW-24	105.09		3.79			101.30	101.30		
4/23/2008	MW-24	105.09		4.21			100.88	100.88		
5/12/2008	MW-24	105.09		3.80			101.29	101.29		
6/27/2008	MW-24	105.09		3.93			101.16	101.16		
8/5/2008	MW-24	105.09		4.00			101.09	101.09		
9/10/2008	MW-24	105.09		3.42			101.67	101.67		
10/27/2008	MW-24	105.09		4.00			101.09	101.09		
11/4/2008	MW-24	105.09		3.96			101.13	101.13		
1/5/2009	MW-24	105.09		3.90			101.19	101.19		
2/27/2009	MW-24	105.09		4.35			100.74	100.74		
3/9/2009	MW-24	105.09		4.43			100.66	100.66		
4/20/2009	MW-24	105.09		3.99			101.10	101.10		
4/29/2009	MW-24	105.09		3.84			101,25	101.25		
5/6/2009	MW-24	105.09		3.61			101.48	101.48		
6/2/2009	MW-24	105.09		4.18			100.91	100.91		
7/6/2009	MW-24	105.09		3.60			101.49	101.49		
8/14/2009	MW-24	105.09		3.87			101.22	101.22		
9/28/2009	MW-24	105.09		3.92			101.17	101.17		~
10/13/2009	MW-24	105.09		4.14			100.95	100.95		
11/23/2009	MW-24	105.09		3.88			101.21	101.21		
12/2/2009	MW-24	105.09		4.11			100.98	100.98		
1/12/2010	MW-24	105.09		4.02			101.07	101.07	~	~
2/2/2010	MW-24	105.09		3.95			101.14	101.14		~
3/2/2010	MW-24	105.09		3.14			101.95	101,95		
	MW-24	105.09		2.69			102.40	102.40		
3/15/2010	MW-24	105.09		3.82			101.27	101,27	~	
4/15/2010		105.09		3.91			101.18	101.18		
4/22/2010	MW-24						101.18	101,43		
5/3/2010	MW-24	105.09		3.66			101,43	101,40		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-25	104.10	~	2.44			101.66	101.66		
2/21/2006	MW-25	104.10		2.84			101.26	101.26		
3/7/2006	MW-25	104.10		3.14			100.96	100.96		
5/18/2006	MW-25	104.10		2.81			101.29	101.29		
6/28/2006	MW-25	104.10		2.76			101.34	101.34		~
8/16/2006	MW-25	104.10		2.91			101.19	101.19		
9/29/2006	MW-25	104.10		3.00			101.10	101.10		
10/20/2006	MW-25	104.10	~	2.68			101.42	101.42		
11/22/2006	MW-25	104.10		2.87			101.23	101.23		
12/15/2006	MW-25	104.10	~~~	3.23			100.87	100.87		
1/23/2007	MW-25	104.10		3.26			100.84	100.84		
2/2/2007	MW-25	104.10		3,47			100.63	100.63		
3/5/2007	MW-25	104.10		2.68			101.42	101.42		
5/1/2007	MW-25	104.10		2.58			101.52	101.52		
6/22/2007	MW-25	104.10		3.11			100.99	100.99		
6/26/2007	MW-25	104.10		3.19			100.91	100.91		
7/6/2007	MW-25	104.10		3.01			101.09	101.09		
8/1/2007	MW-25	104.10		2.79			101.31	101.31		
8/7/2007	MW-25	104.10		2,96			101.14	101.14		
9/14/2007	MW-25	104.10		3,25			100.85	100.85		
	MW-25	104.10		3,55			100.55	100.55		
10/8/2007	MW-25	104.10		3.23			100.87	100.87		
11/20/2007		104.10		2.88			101.22	101.22		
12/26/2007	MVV-25			2,76			101.34	101.34		
1/2/2008	MW-25	104.10					101.34	101.31		
3/5/2008	MW-25	104.10		2.79			100.80	100.80		
4/23/2008	MW-25	104.10		3,30			100.80	100.80		~
5/12/2008	MW-25	104.10		2.80						
6/27/2008	MW-25	104.10		3.00			101.10	101.10		
8/5/2008	MW-25	104.10		3.10			101.00	101.00		~=-
9/10/2008	MW-25	104.10		2.59	-~-		101.51	101.51		
10/27/2008	MW-25	104.10		2.74			101.36	101.36		~
11/4/2008	MW-25	104.10		3.06			101.04	101.04		
1/5/2009	MW-25	104.10		3,00			101.10	101.10		~
2/27/2009	MW-25	104.10		3.54			100.56	100.56		
3/9/2009	MW-25	104.10		3.62			100.48	100.48		
4/20/2009	MW-25	104.10		3.12			100.98	100,98		
4/29/2009	MW-25	104.10		3.01			101.09	101.09		
5/6/2009	MW-25	104.10		2.73			101.37	101.37		
6/2/2009	MW-25	104.10		3.29			100.81	100.81		
7/6/2009	MW-25	104.10		2.75	~		101.35	101.35		
8/14/2009	MW-25	104.10		2.96			101.14	101.14		
9/28/2009	MW-25	104.10		3.02			101.08	101.08		
10/13/2009	MW-25	104.10		3.26			100.84	100.84		
11/23/2009	MW-25	104.10		2.97			101.13	101.13		
12/2/2009	MW-25	104.10		3.21	N==		100.89	100.89		
1/12/2010	MW-25	104.10		3.12			100.98	100.98		
	MW-25	104.10		3.06			101.04	101.04		
2/2/2010		104.10		2.21			101.89	101.89		
3/2/2010	MW-25	104.10		1.62			102.48	102.48		
3/15/2010	MW-25			2.89			101.21	101.21		
4/15/2010	MW-25	104.10					101.21	101.21		
4/22/2010	MW-25	104.10		2.93			101.17	101.17		
5/3/2010	MW-25	104.10		NG_						

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-26			3.22	****					
2/21/2006	MW-26			3.95						
3/7/2006	MW-26			4.17						
5/18/2006	MW-26			3.61						
6/28/2006	MW-26		3.55	3.58	0.03					
8/16/2006	MW-26		3.78	3.79	0.01					
9/29/2006	MW-26		3.63	3.65	0.02	****				
10/20/2006	MW-26		3.53	3,55	0.02					
11/21/2006	MW-26		3.70	3.72	0.02					
12/15/2006	MW-26		4.21	4.23	0.02					
1/23/2007	MW-26			4.41						-
2/2/2007	MW-26			4.58						
3/5/2007	MW-26			4.09		****				
5/1/2007	MW-26		2.56	2.57	0.01					
6/22/2007	MW-26		3.89	3.90	0.01		~			
6/26/2007	MW-26		4.16	4.22	0.06					
7/6/2007	MW-26		4.03	4.06	0.03					
8/1/2007	MW-26		3.56	3.59	0.03					
8/7/2007	MW-26			NG						
9/14/2007	MW-26			NG		****				
10/8/2007	MW-26		4.41	4.45	0.04					
11/20/2007	MW-26		4.29	4.31	0.02					
12/26/2007	MW-26		4.06	4.09	0.03					
1/2/2008	MW-26		3.79	3.81	0.02					
3/5/2008	MW-26		3.79	3.82	0.03					
4/23/2008	MW-26		4.10	4.28	0.18				0.25	
5/12/2008	MW-26		3.38	3.43	0.05				***	
6/27/2008	MW-26		3.84	3.86	0.02					
8/5/2008	MW-26		3.95	4.01	0.06					
9/10/2008	MW-26		3.85	3.86	0.01					
10/27/2008	MW-26		3.88	3.89	0.01					
11/4/2008	MW-26		4.29	4.31 4.28	0.02 0.08					
1/5/2009	MW-26		4.20	4.28 4.78						
2/27/2009	MW-26		4.50		0.00					
3/9/2009	MW-26 MW-26		4.53 4.01	4.55 4.09	0.02 0.08					
4/20/2009 4/29/2009	MW-26		4.01	4.09 4.48	0.08				0.25	~~~
5/6/2009	MW-26		4.29 3.80	4.46 3.81	0.19					***
6/2/2009	MW-26		3.60 4.11	3.61 4.15	0.01					
7/6/2009	MW-26		4.11	3.30	0.04					
8/14/2009	MW-26		3.72	3.30 3.76	0.04					
9/28/2009	MW-26		3.72	3.89	0.04					
10/13/2009	MW-26		4.24	4.26	0.02					
11/23/2009	MW-26		2.86	2.87	0.02					
12/2/2009	MW-26		4.35	4.37	0.02					
1/12/2010	MW-26		4.25	4.27	0.02					
2/2/2010	MW-26		4.26	4.27	0.02					
3/2/2010	MW-26		2.85	2.86	0.01					
3/15/2010	MW-26		2.00	NG	0.01					Flooded
4/15/2010	MW-26		3.68	3.70	0.02					, 100000
4/22/2010	MW-26		3.71	3.72	0.02					
5/3/2010	MW-26			NG						

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-27	102.89		1.79			101.10	101.10		
2/21/2006	MW-27	102.89		2.21			100.68	100.68		
3/7/2006	MW-27	102.89		2.44			100.45	100.45		
5/18/2006	MW-27	102.89		1.95			100.94	100.94		
6/28/2006	MW-27	102.89		1.65			101.24	101.24		
8/16/2006	MW-27	102.89		2.10			100.79	100.79		
9/29/2006	MW-27	102.89		2.09			100.80	100.80		
10/20/2006	MW-27	102.89		1.44			101.45	101.45		
11/22/2006	MW-27	102,89		2.01			100.88	100.88		
12/15/2006	MW-27	102.89		2.28			100.61	100.61		
1/23/2007	MW-27	102.89		NG						
2/2/2007	MW-27	102.89		2.61			100.28	100.28		
3/5/2007	MW-27	102.89		2.27			100.62	100.62		
5/1/2007	MW-27	102.89		1.81			101.08	101.08		
6/22/2007	MW-27	102.89		2.15			100.74	100.74		~
6/26/2007	MW-27	102,89		2.31			100.58	100.58		~
7/6/2007	MW-27	102.89		1.84			101.05	101.05		~
8/1/2007	MW-27	102.89		1.92			100.97	100.97		
8/7/2007	MW-27	102.89		2.11			100.78	100.78		
9/14/2007	MW-27	102.89		2.32			100.57	100.57		
10/8/2007	MW-27	102.89		2.54			100.35	100.35		
	MW-27	102.89		2.48			100.41	100.41		
11/20/2007		102.89		2.40			100.49	100.49		
12/26/2007	MW-27	102.89		2.02			100.87	100.87		***
1/2/2008	MW-27	102.89		1,96			100.93	100.93		
3/5/2008	MW-27		n	2.57			100.32	100.32		
4/23/2008	MW-27	102.89		1.64			100.32	101.25		
5/6/2008	MW-27	102.89		1.74			101.25	101.15		
5/12/2008	MW-27	102.89					101.13	100.62		
6/27/2008	MW-27	102.89		2.27	~		100.52	100.52		
8/5/2008	MW-27	102.89		2.37			100.52	100.52		
9/10/2008	MW-27	102.89		2.38	~		100.51	100.51		
10/27/2008	MW-27	102.89		NG				100.35		
11/4/2008	MW-27	102,89		2.54	~		100.35			
1/5/2009	MW-27	102.89		2.45	~~=		100.44	100.44		
2/27/2009	MW-27	102.89		2.89	~		100.00	100.00		
3/9/2009	MW-27	102.89		2.82	~		100.07	100.07		
4/20/2009	. MW-27	102.89		2.64	~		100.25	100.25		4
4/29/2009	MW-27	102.89		2.60	~~~		100.29	100.29		
6/2/2009	MW-27	102.89		2.45	~~~		100.44	100.44		
7/6/2009	MW-27	102.89		1.97	~~~		100.92	100.92		
8/14/2009	MW-27	102.89		2.26			100.63	100.63		
9/28/2009	MW-27	102,89		1.53	~		101.36	101.36		
10/13/2009	MW-27	102.89		2.57			100.32	100.32		
11/23/2009	MW-27	102.89		2.34			100.55	100.55		
12/2/2009	MW-27	102.89	-~-	2.52			100.37	100.37		
1/12/2010	MW-27	102.89		2.59			100.30	100.30		
2/2/2010	MW-27	102.89		2.66		~~~	100.23	100.23		
3/2/2010	MW-27	102.89		1.54			101.35	101.35		
3/15/2010	MW-27	102.89		NG						Flooded
4/15/2010	MW-27	102.89		2.23			100.66	100.66		
4/22/2010	MW-27	102,89		2.13			100.76	100.76		
5/3/2010	MW-27	102.89		0.80			102.09	102.09		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-28	102.57		1.17			101.40	101.40		
2/21/2006	MW-28	102.57		1.41			101.16	101.16		***
3/7/2006	MW-28	102.57		1.69			100.88	100.88		~
5/18/2006	MW-28	102.57		1.34			101.23	101.23		~
6/22/2006	MW-28	102.57		1.51			101.06	101.06		
6/28/2006	MW-28	102.57		1.18			101.39	101.39		~
8/16/2006	MW-28	102.57		1.41			101.16	101.16	***	
9/29/2006	MW-28	102.57		1.42			101.15	101.15	~	
10/20/2006	MW-28	102.57		1.69			100.88	100.88	~	
11/22/2006	MW-28	102.57		1.34			101.23	101.23	~	
12/15/2006	MW-28	102.57		1.55			101.02	101.02		
1/23/2007	MW-28	102.57		1.79			100.78	100.78	~~~	
2/2/2007	MW-28	102.57		1.93			100.64	100.64	~	
3/5/2007	MW-28	102.57		1.65			100.92	100.92	~~~	
5/1/2007	MW-28	102.57		1.10			101,47	101.47		
	MW-28	102.57		1.62			100.95	100.95	~~~	
6/26/2007		102.57		1.47			101.10	101.10	-	w
7/6/2007	MW-28	102.57		1.23			101.34	101.34		
8/1/2007	MW-28			1.25			101,22	101.22		
8/7/2007	MW-28	102.57		1.62			100.95	100.95		Nu=
9/14/2007	MW-28	102.57					100,63	100.63		
10/8/2007	MW-28	102.57		1.94	****		100,63	100.55		
11/20/2007	MW-28	102.57		2.01			100.56	100.30		
12/26/2007	MW-28	102.57		1.78	***					
1/2/2008	MW-28	102.57		1.64			100.93	100.93		
3/5/2008	MW-28	102.57		1.61			100.96	100.96		
4/23/2008	MW-28	102.57		1.98			100.59	100.59		
5/6/2008	MW-28	102.57		1.66			100.91	100.91		
5/12/2008	MW-28	102.57		1.65			100.92	100.92		
6/27/2008	MW-28	102.57	1.10	1.11	0.01	101.47	101.46	101.47		
8/5/2008	MW-28	102.57		1.85			100.72	100.72		
9/10/2008	MW-28	102.57		1.89			100.68	100.68		
10/27/2008	MW-28	102.57		1.85			100.72	100.72		
11/4/2008	MW-28	102.57		1.92			100.65	100.65		
1/5/2009	MW-28	102.57		1.68			100.89	100.89		
2/27/2009	MW-28	102.57		2.19			100.38	100.38		
3/9/2009	MW-28	102.57		2.11			100.46	100.46		
4/20/2009	MW-28	102.57		3.01			99.56	99.56		
4/29/2009	MW-28	102.57		1.95			100.62	100.62		
6/2/2009	MW-28	102.57		1.84			100.73	100.73		
7/6/2009	MW-28	102.57		1.28			101.29	101.29		
	MW-28	102.57		1.54			101.03	101.03		
8/14/2009		102.57		1.69	====		100.88	100.88		
9/28/2009	MW-28			1.89			100.68	100.68		
10/13/2009	MW-28	102.57		1.73			100.84	100.84		
11/23/2009	MW-28	102.57					100.84	100.34		
12/2/2009	MW-28	102.57		1.83			100.74	100.74		
1/12/2010	MW-28	102.57		1.64						
2/2/2010	MW-28	102.57		1.92			100.65	100.65		
3/2/2010	MW-28	102.57		0.91			101.66	101.66		
3/15/2010	MW-28	102.57		0.53			102.04	102.04		
4/15/2010	MW-28	102.57		1.43			101.14	101.14		
4/22/2010	MW-28	102.57		1.43			101.14	101.14		
5/3/2010	MW-28	102.57		1.26			101.31	101.31		

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-29	102.71		1.36	****		101.35	101.35		
2/21/2006	MW-29	102.71		1.58			101.13	101.13		
3/7/2006	MW-29	102.71		1.86			100.85	100.85		
5/18/2006	MW-29	102.71		1.56			101.15	101.15		
6/28/2006	MW-29	102.71		1.31			101.40	101.40		
8/16/2006	MW-29	102.71		1.60			101.11	101.11		
9/29/2006	MW-29	102.71		1.50			101.21	101.21		
10/20/2006	MW-29	102.71		1.02			101.69	101.69		
11/22/2006	MW-29	102.71		1.50			101.21	101.21		
12/15/2006	MW-29	102.71		1.80			100.91	100.91		
1/23/2007	MW-29	102.71		1.99			100.72	100.72		
2/2/2007	MW-29	102.71		2.12			100.59	100.59		
3/5/2007	MW-29	102.71		1.92			100.79	100.79		
5/1/2007	MW-29	102.71		1.28			101.43	101.43		
6/22/2007	MW-29	102.71		1.71			101.00	101.00		
6/26/2007	MW-29	102.71		1.78			100,93	100.93		
7/6/2007	MW-29	102.71		1.60			101.11	101.11		
8/1/2007	MW-29	102.71	****	1.46			101.25	101.25		
8/7/2007	MW-29	102.71		1.59			101.12	101.12		
9/14/2007	MW-29	102.71		1.83			100.88	100.88		
10/8/2007	MW-29	102.71		2.12			100.59	100.59		
11/20/2007	MW-29	102.71		NG						
12/26/2007	MW-29	102.71		1.94			100.77	100.77		
1/2/2008	MW-29	102.71		NG						
3/5/2008	MW-29	102.71		NG						
4/23/2008	MW-29	102.71		2.14			100.57	100.57		
5/12/2008	MW-29	102.71		1.84			100.87	100.87		
6/27/2008	MW-29	102.71		NG						
8/5/2008	MW-29	102.71		1.99			100.72	100.72		
9/10/2008	MW-29	102.71		2.09			100.62	100.62		
10/27/2008	MW-29	102.71		NG					a	
11/4/2008	MW-29	102.71		2.19			100.52	100.52		
1/5/2009	MW-29	102.71		1.81			100.90	100.90		
2/27/2009	MW-29	102.71		2.48			100.23	100.23		
3/9/2009	MW-29	102.71		2.38			100.33	100.33		
4/20/2009	MW-29	102.71		2.19		-	100.52	100.52		
4/29/2009	MW-29	102.71		1,98			100.73	100.73		
5/6/2009	MW-29	102.71		1.86			100.85	100.85		
6/2/2009	MW-29	102.71		1.96			100.75	100.75		
7/6/2009	MW-29	102.71		1.43			101.28	101.28		
8/14/2009	MW-29	102.71		1.72			100.99	100.99		
9/28/2009	MW-29	102.71		2.04			100.67	100.67		
10/13/2009	MW-29	102.71		2.14			100.57	100.57		
11/23/2009	MW-29	102.71		1.96			100.75	100.75		
12/2/2009	MW-29	102.71		2.12		***	100.59	100.59		
1/12/2010	MW-29	102.71		1.96			100.75	100.75		
2/2/2010	MW-29	102.71		2.12			100.59	100.59	***	
3/2/2010	MW-29	102.71		1.04 0.59			101.67	101.67		
3/15/2010	MW-29	102.71					102.12	102.12		
4/15/2010	MW-29	102.71		1.53 NC	700		101.18	101.18		
4/22/2010	MW-29	102.71		NG 1.00			101.71	101.71		
5/3/2010	MW-29	102.71		1.00			101.71	101.71		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-30			1.64						
2/21/2006	MW-30			2.10						
3/7/2006	MW-30			2.34						
5/18/2006	MW-30			2.01						
6/28/2006	MW-30			0.47						
8/16/2006	MW-30			1.98						
9/29/2006	MW-30			1.22						
10/20/2006	MW-30			0.58		w				
11/22/2006	MW-30			1.76						
12/15/2006	MW-30			1.00						
1/23/2007	MW-30			2.41	*****					
2/2/2007	MW-30			2.54						
3/5/2007	MW-30			2.38						***
5/1/2007	MW-30			1.84						
6/22/2007	MW-30			NG					*****	*****
6/26/2007	MW-30			2.22			***			
7/6/2007	MW-30			1.60			****			
8/1/2007	MW-30			1.75						
8/7/2007	MW-30			1.89						
9/14/2007	MW-30			2.18						
10/8/2007	MW-30			2.42						
11/20/2007	MVV-30			NG	***				****	
12/26/2007	MW-30			2.28						
1/2/2008	MW-30	***		1.69						
3/5/2008	MW-30			NG						
4/23/2008	MW-30	-		2.50						
5/6/2008	MW-30			1.81						
5/12/2008	MW-30			NG						
6/27/2008	MW-30			6.65						
8/5/2008	MW-30			2.24						
9/10/2008	MW-30			1.91						
i e	MW-30			NG						
10/27/2008	MW-30			2.35						
11/4/2008 1/5/2009	MW-30			2.33						
2/27/2009	MW-30			2.38 3.11						
				2.92						Here
3/9/2009	MW-30 MW-30			2.92 2.61						
4/20/2009 4/29/2009	MW-30			2.72						
6/2/2009	MW-30			2.72						
7/6/2009	MW-30			2.54 1.88						
1				2.14						
8/14/2009 9/28/2009	MW-30 MW-30			1.23						
1										
10/13/2009	MW-30			2.43						
11/23/2009	MW-30			2.18						
12/2/2009	MW-30	***		1.72						
1/12/2010	MW-30			2.56						
2/2/2010	MW-30			2.68		pr== 64				
3/2/2010	MW-30			NG		****		****		Under Water
3/15/2010	MW-30			NG				***		Flooded
4/15/2010	MW-30			2.14	***					
4/22/2010	MW-30			2.03						
5/3/2010	MW-30			0.60						

Date	. Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-31	103.36	2.95	2.99	0.04	100.41	100.37	100.40	0.10	
2/21/2006	MW-31	103.36	3.60	4.15	0.55	99.76	99.21	99.62	1.00	
3/7/2006	MW-31	103,36	3.84	4.86	1.02	99,52	98,50	99.25	0.66	Hand Bailing
5/18/2006	MW-31	103.36	3.09	3.36	0.27	100.27	100,00	100.20	0.50	
6/28/2006	MW-31	103.36	3.26	3.59	0.33	100.10	99.77	100.01	0.50	
8/16/2006	MW-31	103.36	3.65	4.01	0.36	99.71	99.35	99.62		
9/29/2006	MW-31	103.36	3.38	3.65	0.27	99,98	99,71	99.91		
10/20/2006	MW-31	103.36		NG	=	202				
11/22/2006	MW-31	103.36	3.24	3.56	0.32	100.12	99.80	100.04		
12/15/2006	MW-31	103.36	3.69	4.64	0.95	99.67	98.72	99.42	0.75	
1/23/2007	MW-31	103.36	4.09	4.84	0.75	99,27	98.52	99.08	1.50	
2/2/2007	MW-31	103.36	3.99	4.72	0.73	99,37	98.64	99.18	0.25	
3/5/2007	MW-31	103.36	3.79	4.68	0.89	99.57	98.68	99.34	1.25	,,
5/1/2007	MW-31	103.36	3.05	3.58	0.53	100.31	99.78	100.17	0.25	
6/22/2007	MW-31	103.36	3.55	4.15	0.60	99.81	99.21	99.65	0.25	
6/26/2007	MW-31	103.36	3.81	4.62	0.81	99.55	98.74	99.34		
7/6/2007	MW-31	103.36	3.58	4.73	1.15	99.78	98.63	99.48	0.50	
8/1/2007	MW-31	103.36	3.44	3.78	0.34	99.92	99.58	99.83	0.25	
8/7/2007	MW-31	103.36	3.51	3.61	0.10	99.85	99.75	99.82		
9/14/2007	MW-31	103.36	3.99	4.73	0.74	99.37	98,63	99.18	1.00	
10/8/2007	MW-31	103.36	3.85	4.75	0.90	99.51	98.61	99.28	1.00	
11/20/2007	MW-31	103.36	3.75	4.85	1.10	99.61	98.51	99.32	1.00	
12/26/2007	MW-31	103.36	3.90	4.69	0.79	99.46	98.67	99.25		
1/2/2008	MW-31	103.36		NG		-				
3/5/2008	MW-31	103.36		NG						
4/23/2008	MW-31	103.36		NG						
5/12/2008	MW-31	103.36	2.92	3.34	0.42	100.44	100.02	100.33	***	
6/27/2008	MW-31	103.36	3.52	4.17	0.65	99.84	99.19	99.67	1.00	
8/5/2008	MW-31	103.36	3.75	4.66	0.91	99.61	98.70	99.37	1.00	
9/10/2008	MW-31	103.36	3.63	4.67	1.04	99.73	98.69	99.46	1.00	
10/27/2008	MW-31	103.36	3.19	4.05	0.86	100.17	99.31	99.95	1.00	
11/4/2008	MW-31	103.36	4.09	5.25	1.16	99.27	98.11	98.97	1.25	
1/5/2009	MW-31	103.36	4.02	4.80	0.78	99.34	98.56	99.14	1.25	
2/27/2009	MW-31	103.36	4.42	4.85	0.43	98.94	98.51	98.83	0.75	
3/9/2009	MW-31	103.36	3.81	4.34	0.53	99.55	99.02	99.41	1.00	
4/20/2009	MW-31	103.36	3.68	4.47	0.79	99.68	98.89	99.47	1.50	
4/29/2009	MW-31	103.36	4.20	4.60	0.40	99.16	98.76	99.06	1.00	
5/6/2009	MW-31	103.36	3.39	3.91	0.52	99.97	99.45	99.83	1.00	
6/2/2009	MW-31	103.36	3.71	4.81	1.10	99.65	98.55	99.36	1.00	
7/6/2009	MW-31	103.36	3.29	3.75	0.46	100.07	99.61	99.95	0.50	
8/14/2009	MW-31	103.36	3.59	4.05	0.46	99.77	99.31	99.65	0.75	
9/28/2009	MW-31	103.36	3.42	4.13	0.46	99.77	99.31	99.65	0.75	
10/13/2009	MW-31	103.36	3.81	4.80	0.71	99.55	98,56	99.76	1,00	
11/23/2009	MW-31	103.36	3.66	4. <i>00</i> 3.91	0.99	99.55	99,45	99.29		
12/2/2009	MW-31	103.36	3.00	3.91 4.84	0.25	99.70	99.45 98.52	99.64	2.00	
1/12/2010	MW-31	103.36	3.85	4.56	0.71	99.51	98.52 98.80			n=n
2/2/2010	MW-31	103.36	4.23	4.56 4.79	0.74	99.51	98.80 98.57	99.33 98.98	0.75	
									0.75	
3/2/2010	MW-31	103.36	2.39	2.93	0.54	100.97	100.43	100.83	0.75	
3/15/2010	MW-31	103.36	1.69	1.75	0.06	101.67	101.61	101.65		
4/15/2010	MW-31	103.36	3.68	3.78	0.10	99.68	99.58	99.65		
4/22/2010	MW-31	103.36	3.26	3.43	0.17	100.10	99.93	100.06	0.25	
5/3/2010	MW-31	103.36	3.09	3.15	0.06	100,27	100.21	100.25		

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-32	104.44		3.04			101.40	101.40		
2/21/2006	MW-32	104.44		3.79			100.65	100.65		
3/7/2006	MW-32	104.44		4.50			99.94	99.94		
5/18/2006	MW-32	104.44		3.73			100.71	100.71		
6/28/2006	MW-32	104.44		3.59		***	100.85	100.85		
8/16/2006	MW-32	104.44		3.71			100.73	100.73		
9/29/2006	MW-32	104.44		3.72			100.72	100.72		
10/20/2006	MW-32	104.44		3.55			100.89	100.89		
11/21/2006	MW-32	104.44		3.57			100.87	100.87		
12/15/2006	MW-32	104.44		4.55			99.89	99.89		
1/23/2007	MW-32	104.44		4.72	~~-		99.72	99.72		
2/2/2007	MW-32	104.44		5.01			99.43	99.43		
3/5/2007	MW-32	104.44		3.79			100.65	100.65		
5/1/2007	MW-32	104.44		3.25			101,19	101.19	-	
6/22/2007	MW-32	104.44		4.11			100.33	100.33		
6/26/2007	MW-32	104.44		4.42			100.02	100.02		
7/6/2007	MW-32	104.44		4.34			100.10	100.10		
8/1/2007	MW-32	104.44		3.71	*****		100.73	100.73		
8/7/2007	MW-32	104.44		3.85			100.59	100.59		
9/14/2007	MW-32	104.44		4.66			99.78	99.78		
10/8/2007	MW-32	104.44	***	4.84			99.60	99.60		
11/20/2007	MW-32	104.44		4.63			99.81	99.81		
12/26/2007	MW-32	104.44		4.12			100.32	100.32		
1/2/2008	MW-32	104.44		3.71			100.73	100.73		
3/5/2008	MW-32	104.44		3.85			100.59	100.59		
4/23/2008	MW-32	104.44		4.61			99.83	99.83		
5/12/2008	MW-32	104.44		3.54			100.90	100.90		
6/27/2008	MW-32	104.44	-	4.06			100.38	100.38		
8/5/2008	MW-32	104.44		4.25			100.19	100.19		
9/10/2008	MW-32	104.44		3.60			100.84	100.84		
10/27/2008	MW-32	104.44		4.11			100,33	100.33		
11/4/2008	MW-32	104.44		4.45		~	99,99	99.99		
1/5/2009	MW-32	104.44		4.30			100.14	100.14		
2/27/2009	MW-32	104.44		5.26			99.18	99.18		
3/9/2009	MW-32	104.44		4.94			99.50	99.50		
4/20/2009	MW-32	104.44		4.45			99.99	99.99		
4/29/2009	MW-32	104.44		4.39			100.05	100.05		
5/6/2009	MW-32	104.44		3.92	~~-		100.52	100.52		
6/2/2009	MW-32	104.44		4.59			99.85	99.85		
7/6/2009	MW-32	104.44		3.54			100.90	100.90		~
8/14/2009	MW-32	104.44		3.94			100.50	100.50		~
9/28/2009	MW-32	104.44	•	4.24			100,20	100.20		
10/13/2009	MW-32	104.44		4.63			99.81	99.81		
11/23/2009	MW-32	104.44		4.06			100.38	100.38		
12/2/2009	MW-32	104.44		4.77			99,67	99.67		
1/12/2010	MW-32	104.44		4.45			99.99	99.99		
2/2/2010	MW-32	104.44		4.59			99.85	99.85		***
3/2/2010	MW-32	104.44		2.77			101.67	101.67		
3/15/2010	MW-32	104.44		1.59			102.85	102.85		
4/15/2010	MW-32	104.44		3.62			100.82	100.82		
4/15/2010	MW-32	104.44		3.66		~~=	100.78	100.78		
5/3/2010	MW-32	104.44		2.95	==~		101.49	101.49		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-33	103.15	****	5.00			98.15	98.15		
2/21/2006	MW-33	103.15		5.71			97.44	97.44		
3/7/2006	MW-33	103.15		5.76			97.39	97.39		
5/18/2006	MW-33	103.15		5.61			97.54	97.54		
6/28/2006	MW-33	103.15		5.62			97.53	97.53		
8/16/2006	MW-33	103.15		5.61			97.54	97.54		
9/29/2006	MW-33	103.15		5.67			97.48	97.48		
10/20/2006	MW-33	103.15		5.43			97.72	97.72		
11/22/2006	MW-33	103.15		5.68			97.47	97.47		
12/15/2006	MW-33	103.15		5.76			97.39	97.39		
1/23/2007	MW-33	103.15		5.85			97.30	97.30		
2/2/2007	MW-33	103.15		6.41			96.74	96.74		
3/5/2007	MW-33	103.15		5.63			97.52	97.52		
5/1/2007	MW-33	103.15		5.38			97.77	97.77		
6/22/2007	MW-33	103.15		5.66			97.49	97.49		
6/26/2007	MW-33	103.15		5.69			97.46	97.46		
7/6/2007	MW-33	103.15		5.65			97.50	97.50		
8/1/2007	MW-33	103.15		5.61			97.54	97.54		
8/7/2007	MW-33	103.15		5.65			97.50	97.50		
9/14/2007	MW-33	103.15		7.29			95.86	95.86		
10/8/2007	MW-33	103.15		5.81			97.34	97.34		
11/20/2007	MW-33	103.15		5.79			97.36	97.36		
12/26/2007	MW-33	103.15		5.66			97.49	97.49		
1/2/2008	MW-33	103.15		5.67			97.48	97.48		
3/5/2008	MW-33	103.15		5.69	••••		97.46	97.46		
4/23/2008	MW-33	103.15		5.74		****	97.41	97.41		
5/12/2008	MW-33	103.15		5.39			97.76	97.76		
6/27/2008	MW-33	103.15		5.65			97.50	97.50		
8/5/2008	MW-33	103.15		5.68			97.47	97.47		
9/10/2008	MW-33	103.15		7.21			95.94	95.94		
10/27/2008	MW-33	103.15		5.59			97.56	97.56		
11/4/2008	MW-33	103.15		5.71			97.44	97.44		
1/5/2009	MW-33	103.15		5.74			97.41	97.41		
2/27/2009	MW-33	103.15		6.57			96.58	96.58		
3/9/2009	MW-33	103.15		5.96			97.19	97.19		
4/20/2009	MW-33	103.15		5.72		~	97.43	97.43		
4/29/2009	MW-33	103.15	****	5.70			97.45	97.45		
5/6/2009	MW-33	103.15		5.51			97.64	97.64		
6/2/2009	MW-33	103.15		5.72			97.43	97.43		
7/6/2009	MW-33	103.15		5.60			97.55	97.55		
8/14/2009	MW-33	103.15		5.64			97.51	97.51		
9/28/2009	MW-33	103.15		5.59			97.56	97.56		
10/13/2009	MW-33	103.15		5.71			97.44	97.44		
11/23/2009	MW-33	103.15		5.25			97.90	97.90		
12/2/2009	MW-33	103.15		5.70			97.45	97.45		
1/12/2010	MW-33	103.15		5.71			97.44	97.44		
2/2/2010	MW-33	103.15		5.72			97.43	97.43		
3/2/2010	MW-33	103.15	****	4.85			98.30	98.30		
3/15/2010	MW-33	103.15	5.69	5.69	0.00	97.46	97.46	97.46		Trace LNAPL
4/15/2010	MW-33	103.15		5.62			97.53	97.53		
4/22/2010	MW-33	103.15		5.59			97.56	97.56		
5/3/2010	MW-33	103.15		5.35			97.80	97.80		

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-34 / RW-34			6.56						
2/21/2006	MW-34 / RW-34			7.31						
3/7/2006	MW-34 / RW-34			7.47				***		
5/18/2006	MW-34 / RW-34			7.13						
6/28/2006	MW-34 / RW-34			7.12						
8/16/2006	MW-34 / RW-34	·		7.05						
9/29/2006	MW-34 / RW-34			7.18						
10/20/2006	MW-34 / RW-34			6.42						
11/22/2006	MW-34 / RW-34			5.48						
12/15/2006	MW-34 / RW-34			7.81						
1/23/2007	MW-34 / RW-34			7.96						
2/2/2007	MW-34 / RW-34			8.11						
3/5/2007	MW-34 / RW-34			7.11				have the		
5/1/2007	MW-34 / RW-34			6.86					***	
6/22/2007	MW-34 / RW-34			7.15						
6/26/2007	MW-34 / RW-34			7.13						
7/6/2007	MW-34 / RW-34			7.18						
8/1/2007	MW-34 / RW-34		~	7.10						
				7.14						
8/7/2007	MW-34 / RW-34									
9/14/2007	MW-34 / RW-34			5.71				****		
10/8/2007	MW-34 / RW-34			7.79						
11/20/2007	MW-34 / RW-34		*****	7.43						
12/26/2007	MW-34 / RW-34			7.19						
1/2/2008	MW-34 / RW-34			7.14				*****		
3/5/2008	MW-34 / RW-34			7.14					•••	
4/23/2008	MW-34 / RW-34			7.39						
5/12/2008	MW-34 / RW-34		6.70	6.85	0.15					
6/27/2008	MW-34 / RW-34			7.15				****		
8/5/2008	MW-34 / RW-34		7.11	7.21	0.10			****	0.25	
9/10/2008	MW-34 / RW-34			5.70						
10/27/2008	MW-34 / RW-34		***	7.02		****		~		
11/4/2008	MW-34 / RW-34			7.19						
1/5/2009	MW-34 / RW-34			7.39			-			
2/27/2009	MW-34 / RW-34			8.30						
3/9/2009	MW-34 / RW-34			8.09				******		
4/20/2009	MW-34 / RW-34			7.41			****			
4/29/2009	MW-34 / RW-34			7.24						
5/6/2009	MW-34 / RW-34			7.02						
6/2/2009	MW-34 / RW-34			7.29			****			
7/6/2009	MW-34 / RW-34		7.10	7.11	0.01	*****			0.50	
8/14/2009	MW-34 / RW-34		7.09	7.13	0.04					
9/28/2009	MW-34 / RW-34		7.07	7.13	0.06					
10/13/2009	MW-34 / RW-34		7.38	7.45	0.07			***		
11/23/2009	MW-34 / RW-34		7.18	7.22	0.04					
12/2/2009	MW-34 / RW-34		7.18	7.32	0.04					
1/12/2010	MW-34 / RW-34		7.20	7.32	0.04					
2/2/2010	MW-34 / RW-34		7.31	7.35 7.35	0.02					
3/2/2010	MW-34 / RW-34			6.33						
3/15/2010	MW-34 / RW-34		744	4.04			P. 4.4			
4/15/2010	MW-34 /RW-34		7.11	7.16	0.05					
4/22/2010	MW-34 /RW-34		7.09	7.14	0.05					
5/3/2010	MW-34 /RW-34		6.81	6.85	0.04					

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-35	103.89		5.74			98.15	98.15		
2/21/2006	MW-35	103.89		6.42			97.47	97.47		
3/7/2006	MW-35	103.89		6.53			97.36	97.36		
5/18/2006	MW-35	103.89		6.42			97.47	97.47		
6/28/2006	MW-35	103.89		6.44			97.45	97.45		
8/16/2006	MW-35	103.89		6.40			97.49	97.49		
9/29/2006	MW-35	103.89		6.49			97.40	97.40		
10/20/2006	MW-35	103.89		6.27			97.62	97.62		
11/22/2006	MW-35	103.89		6.46			97.43	97.43		
12/15/2006	MW-35	103.89		6.56			97.33	97.33		
1/23/2007	MW-35	103.89		6.69			97.20	97.20		
2/2/2007	MW-35	103.89		6,88			97.01	97.01		
3/5/2007	MW-35	103.89		6.38			97.51	97.51		
5/1/2007	MW-35	103.89		6.13			97.76	97.76		
6/22/2007	MW-35	103.89		6.49			97.40	97.40		
6/26/2007	MW-35	103.89		6.49			97.40	97.40		
7/6/2007	MW-35	103.89		6.48			97.41	97.41		
8/1/2007	MW-35	103.89		6.42			97.47	97.47		
8/7/2007	MW-35	103.89		6.48			97.41	97.41		
	MW-35	103.89		6.49			97.40	97.40		
9/14/2007		103.89		6.61			97.28	97.28		
10/8/2007	MW-35			6.52			97.37	97.37		
11/20/2007	MW-35	103.89					97.44	97.44		
12/26/2007	MW-35	103.89		6.45				97.43		
1/2/2008	MW-35	103.89		6.46			97.43			
3/5/2008	MW-35	103.89		6.49			97.40	97.40		
4/23/2008	MW-35	103.89		6.58			97.31	97.31		
5/12/2008	MW-35	103.89		6.14			97.75	97.75		*****
6/27/2008	MW-35	103.89		6.49			97.40	97.40		
8/5/2008	MW-35	103.89		6.48			97.41	97.41		
9/10/2008	MW-35	103.89		6.47			97.42	97.42		
10/27/2008	MW-35	103.89		6.39			97.50	97.50		
11/4/2008	MW-35	103.89		6.51			97,38	97.38		
1/5/2009	MW-35	103.89		6.55			97.34	97.34		
2/27/2009	MW-35	103.89		6.83			97.06	97.06	*****	
3/9/2009	MW-35	103.89		6.81			97.08	97.08		
4/20/2009	MW-35	103.89		6.56			97.33	97.33		
4/29/2009	MW-35	103.89		6.51			97.38	97.38		
5/6/2009	MW-35	103.89		6.45			97.44	97.44		
6/2/2009	MW-35	103.89		6.51			97.38	97.38		
7/6/2009	MW-35	103.89		6.46			97.43	97.43		
8/14/2009	MW-35	103.89		6.49			97.40	97.40		
9/28/2009	MW-35	103.89		6.47			97.42	97.42		
10/13/2009	MW-35	103.89		6.50			97,39	97.39		
	MW-35	103.89		6.48			97.41	97.41		****
11/23/2009		103.89		6.49			97,40	97.40		
12/2/2009	MW-35			6.49			97.40	97.40		
1/12/2010	MW-35	103.89		6.53			97.36	97.36		
2/2/2010	MW-35	103.89					98.28	98.28		
3/2/2010	MW-35	103.89		5.61						
3/15/2010	MW-35	103.89		5.02			98,87	98.87		
4/15/2010	MW-35	103.89		6.47			97.42	97.42		
4/22/2010	MW-35	103.89		6.46			97.43	97.43		
5/3/2010	MW-35	103.89		6.47			97.42	97.42_		

(Sorted by Well)

										
Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-36 / RW-36	103.87	7.99	8.21	0.22	95.88	95.66	95.82	0.50	
2/21/2006	MW-36 / RW-36	103.87	9.10	9.22	0.12	94.77	94.65	94.74	0.10	
3/7/2006	MW-36 / RW-36	103.87	9.51	10.02	0.51	94.36	93.85	94.23	1.00	
5/18/2006	MW-36 / RW-36	103.87	8,59	8.82	0.23	95.28	95.05	95.22	0.25	
6/28/2006	MW-36 / RW-36	103.87	8.37	8.69	0.32	95,50	95.18	95.42		
8/16/2006	MW-36 / RW-36	103.87	8.75	8.76	0.01	95.12	95.11	95.12		
9/29/2006	MW-36 / RW-36	103.87	8.62	8.89	0.27	95.25	94.98	95.18		
10/20/2006	MW-36 / RW-36	103.87	7.80	7.98	0.18	96.07	95.89	96.02		
11/22/2006	MW-36 / RW-36	103.87	8.05	8.33	0.28	95.82	95.54	95.75		
12/15/2006	MW-36 / RW-36	103.87	8.86	8.95	0.09	95.01	94.92	94.99		
1/23/2007	MW-36 / RW-36	103.87	9.48	9.53	0.05	94.39	94.34	94.38	****	
2/2/2007	MW-36 / RW-36	103.87	8.58	8.60	0.02	95.29	95.27	95.28		
3/5/2007	MW-36 / RW-36	103.87	9.04	9.11	0.07	94.83	94.76	94.81		
5/1/2007	MW-36 / RW-36	103.87	8.15	8.52	0.37	95.72	95.35	95.62	1.25	
6/22/2007	MW-36 / RW-36	103.87	8,95	9.25	0.30	94.92	94.62	94.84	0.25	
6/26/2007	MW-36 / RW-36	103.87	9.29	9.63	0.34	94.58	94.24	94.49		
7/6/2007	MW-36 / RW-36	103.87	9.41	9.92	0.51	94,46	93.95	94.33	0.50	
8/1/2007	MW-36 / RW-36	103.87	8.77	9.05	0.28	95.10	94.82	95.03	0.25	
8/7/2007	MW-36 / RW-36	103.87	8.64	8.88	0.24	95.23	94.99	95.17	0.25	
9/14/2007	MW-36 / RW-36	103.87	8.91	9.51	0.60	94.96	94.36	94.80	0.75	
10/8/2007	MW-36 / RW-36	103.87	8.51	8.85	0.34	95.36	95.02	95.27	0.25	
11/20/2007	MW-36 / RW-36	103.87	8.91	9,22	0.31	94.96	94.65	94.88	0.50	
	MW-36 / RW-36	103.87	8.85	9.05	0.20	95.02	94.82	94.97		
12/26/2007	MW-36 / RW-36	103.87	8.95	9.45	0.50	94.92	94.42	94.79	0.75	
1/2/2008	MW-36 / RW-36	103.87	8,38	8.53	0.15	95.49	95.34	95,45	0.25	
3/5/2008	•	103.87	9.50	9.56	0.06	94.37	94.31	94.35		
4/23/2008	MW-36 / RW-36		7.89	8.03	0.00	95.98	95.84	95.94		
5/12/2008	MW-36 / RW-36	103.87	7.09	8.95	U. 14		94.92	94.92		
6/27/2008	MW-36 / RW-36	103.87			0.85	94.74	93.89	94.52	1.00	
8/5/2008	MW-36 / RW-36	103.87	9.13	9.98	0.83	95.10	94.18	94.86	1.00	
9/10/2008	MW-36 / RW-36	103.87	8.77	9.69			95.96	96.06	0.25	
10/27/2008	MW-36 / RW-36	103.87	7.78	7.91	0.13	96.09				
11/4/2008	MW-36 / RW-36	103.87	9.55	9.64	0.09	94.32	94.23	94.30		
1/5/2009	MW-36 / RW-36	103.87	10.50	10.51	0.01	93.37	93.36	93.37		
2/27/2009	MW-36 / RW-36	103.87	9.19	9.21	0.02	94.68	94.66	94.67		
3/9/2009	MW-36 / RW-36	103.87	7.99	8.00	0.01	95.88	95.87	95.88	0.25	
4/20/2009	MW-36 / RW-36	103.87	8.60	8.68	0.08	95.27	95,19	95.25	0.25	
4/29/2009	MW-36 / RW-36	103.87		10.52			93.35	93.35	0.50	
5/6/2009	MW-36 / RW-36	103.87	8.22	8.47	0.25	95.65	95.40	95,59	0.50	
6/2/2009	MW-36 / RW-36	103.87	9.09	9.45	0.36	94.78	94.42	94.69	0.50	
7/6/2009	MW-36 / RW-36	103.87	8.41	8.59	0.18	95.46	95.28	95.41	0.50	
8/14/2009	MW-36 / RW-36	103.87	8.98	9.34	0.36	94.89	94.53	94.80	0.50	
9/28/2009	MW-36 / RW-36	103.87	9.03	9.31	0.28	94.84	94.56	94.77	0.50	
10/13/2009	MW-36 / RW-36	103.87	9.69	9.86	0.17	94.18	94.01	94.14	0.25	
11/23/2009	MW-36 / RW-36	103.87		8.78			95.09	95.09		
12/2/2009	MW-36 / RW-36	103.87	8.08	8.13	0.05	95.79	95.74	95.78		
1/12/2010	MW-36 / RW-36	103.87	8.88	8.95	0.07	94.99	94.92	94.97		
2/2/2010	MW-36 / RW-36	103.87	9.35	9.39	0.04	94.52	94.48	94.51		
3/2/2010	MW-36 / RW-36	103.87		NG						
3/15/2010	MW-36 / RW-36	103.87	6.73	6.82	0.09	97.14	97.05	97.12		
4/15/2010	MW-36 / RW-36	103.87	8.68	8.76	0.08	95.19	95.11	95.17		
4/22/2010	MW-36 / RW-36	103.87	8.62	8.65	0.03	95.25	95.22	95.24		
5/3/2010	MW-36 / RW-36	103,87	8.64	8.78	0.14	95.23	95.09	95.19	0.25	

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-37 / RW-37	103.49		6.98			96.51	96.51		
2/21/2006	MW-37 / RW-37	103.49		8.15			95.34	95.34		
3/7/2006	MW-37 / RW-37	103.49		7.86			95.63	95.63		
5/18/2006	MW-37 / RW-37	103.49		NG						
6/28/2006	MW-37 / RW-37	103.49		7.59			95.90	95.90		
8/16/2006	MW-37 / RW-37	103.49		7.56			95.93	95.93		
9/29/2006	MW-37 / RW-37	103.49		7.58			95.91	95.91		
10/20/2006	MW-37 / RW-37	103.49		7.54			95.95	95.95		
11/22/2006	MW-37 / RW-37	103.49		7.59			95.90	95.90		
12/15/2006	MW-37 / RW-37	103.49		7.92			95.57	95.57		
1/23/2007	MW-37 / RW-37	103.49		8.18			95.31	95,31		
2/2/2007	MW-37 / RW-37	103.49		8.53			94,96	94.96		
3/5/2007	MW-37 / RW-37	103.49		7.47			96.02	96.02		
5/1/2007	MW-37 / RW-37	103.49	7.19	7.20	0.01	96.30	96.29	96.30		
6/22/2007	MW-37 / RW-37	103.49	7.61	7.64	0.03	95.88	95.85	95.87		
6/26/2007	MW-37 / RW-37	103.49	8.04	8.11	0.07	95.45	95.38	95.43		
	MW-37 / RW-37	103.49	7.78	7.79	0.01	95.71	95.70	95.71		
7/6/2007	MW-37 / RW-37	103.49	7.59	7.61	0.02	95,90	95.88	95.89		
8/1/2007		103.49	7.61	7.75	0.14	95.88	95.74	95.84	0.25	
8/7/2007	MW-37 / RW-37	103.49	7.83	7.73	0.04	95.66	95,62	95.65		
9/14/2007	MW-37 / RW-37			8.00	0.04	95.50	95.49	95.50		
10/8/2007	MW-37 / RW-37	103.49	7.99	7.89			95.60	95.60		
11/20/2007	MW-37 / RW-37	103.49					95.89	95.89		
12/26/2007	MW-37 / RW-37	103.49		7.60			95.84	95.84		
1/2/2008	MW-37 / RW-37	103.49		7.65						
3/5/2008	MW-37 / RW-37	103.49		7.61			95.88	95.88		
4/23/2008	MW-37 / RW-37	103.49		7.80			95.69	95.69		
5/12/2008	MW-37 / RW-37	103.49	7.39	7.41	0.02	96.10	96.08	96.09		
6/27/2008	MW-37 / RW-37	103.49	7.66	7.69	0.03	95.83	95.80	95.82		
8/5/2008	MW-37 / RW-37	103.49	7.86	7.88	0.02	95.63	95.61	95.62		
9/10/2008	MW-37 / RW-37	103.49		7.69			95.80	95.80		
10/27/2008	MW-37 / RW-37	103.49		7.13			96,36	96.36		
11/4/2008	MW-37 / RW-37	103.49		7.98			95.51	95.51		
1/5/2009	MW-37 / RW-37	103.49		7.90			95.59	95.59		
2/27/2009	MW-37 / RW-37	103.49	8.35	8.37	0.02	95.14	95.12	95.13		
3/9/2009	MW-37 / RW-37	103.49		8.25			95.24	95.24		
4/20/2009	MW-37 / RW-37	103.49		7.89			95,60	95.60		
4/29/2009	MW-37 / RW-37	103.49		7.91			95.58	95.58		
5/6/2009	MW-37 / RW-37	103.49		6.75			96.74	96.74		
6/2/2009	MW-37 / RW-37	103.49		7.89			95,60	95.60		
7/6/2009	MW-37 / RW-37	103.49		7.56		_~~	95.93	95.93		
8/14/2009	MW-37 / RW-37	103.49	7.64	7.69	0.05	95.85	95.80	95.84		
9/28/2009	MW-37 / RW-37	103.49	,.o-,	7.71			95.78	95.78		
10/13/2009	MW-37 / RW-37	103.49	7.84	7.87	0.03	95.65	95.62	95.64		
	MW-37 / RW-37	103,49		7.59			95,90	95.90		
11/23/2009	MW-37 / RW-37	103.49		7.75			95.74	95.74		
12/2/2009			7.74	7.75	0.01	95,75	95.74	95.75		
1/12/2010	MW-37 / RW-37	103.49	7.7 4 7.86	7.73	0.03	95,63	95.60	95.62		
2/2/2010	MW-37 / RW-37	103.49			0.03		55.00			
3/2/2010	MW-37 / RW-37	103.49	C 00	NG e oo		07 44		97.41		
3/15/2010	MW-37 / RW-37	103.49	6.08	6.09	0.01	97.41	97.40			
4/15/2010	MW-37 / RW-37	103.49	7.58	7.62	0.04	95.91	95.87	95.90		
4/22/2010	MW-37 / RW-37	103.49	7.56	7.58	0.02	95.93	95.91	95.92		
5/3/2010	MW-37 / RW-37	103.49	7.48	7.50	0.02	96.01	95.99	96.00		

					FILL NO. 07-0			,	, <u></u>	
Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-38			6.49						
2/21/2006	MW-38			7.01						
3/7/2006	MW-38			7.26						
5/18/2006	MW-38			6.95						
6/28/2006	MW-38			6.83						
8/16/2006	MW-38			6.90						
10/20/2006	MW-38			6.65						
11/22/2006	MW-38			6.76						
12/15/2006	MW-38			7.25						
1/23/2007	MW-38			7.48						
2/2/2007	MW-38			7.62						
3/5/2007	MW-38			7.27						
5/1/2007	MW-38			6.60						
6/22/2007	MW-38			6.65						
6/26/2007	MW-38			7.12						
7/6/2007	MW-38			7.16						
8/1/2007	MW-38	***		6.81						
8/7/2007	MW-38			6.86						
9/14/2007	MW-38			7.19						
10/8/2007	MW-38		****	7.49						
11/20/2007	MW-38			7.35						
12/26/2007	MW-38			7.07						
1/2/2008	MW-38			6.94						
3/5/2008	MW-38			7.05						
4/23/2008	MW-38			7.35						
5/12/2008	MW-38			6.85						
6/27/2008	MW-38			7.07				A		
8/5/2008	MW-38			7.17						
9/10/2008	MW-38			7.16						
10/27/2008	MW-38	***		5.82						
11/4/2008	MW-38	~		7.29						
1/5/2009	MW-38	~		7.38						
2/27/2009	MW-38	~		7.92	,,,,,					
3/9/2009	MW-38		~~-	7.94						
4/20/2009	MW-38	~		7.45			~			
4/29/2009	MW-38			7.38						***
5/6/2009	MW-38			7.22			~			
6/2/2009	MW-38			7.39						
7/6/2009	MW-38			6.70						
8/14/2009	MW-38			6.93						
9/28/2009	MW-38			7.05						
10/13/2009	MW-38			7.24						
11/23/2009	MW-38			6.93						
12/2/2009	MW-38			7.23						
1/12/2010	MW-38			7.28						
2/2/2010	MW-38			7.38						
3/2/2010	MW-38			NG			***			
3/15/2010	MW-38			5.71						
4/15/2010	MW-38			6.83						
4/22/2010	MW-38			6.84		n				
5/3/2010	MW-38			6.63						

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

25 Paidge Avenue Brooklyn, New York NYSDEC SPILL NO. 87-09990

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-39			6.50						
2/21/2006	MW-39			7.06						
3/7/2006	MW-39			7.01						*****
5/18/2006	MW-39			6.86						
6/28/2006	MW-39			6,45						
8/16/2006	MW-39			6.79						
9/29/2006	MW-39			6.52						
10/20/2006	MW-39			5.42						
11/22/2006	MW-39			5.60						
12/15/2006	MW-39			6.49						***
1/23/2007	MW-39			7.14						
2/2/2007	MW-39			6.47						
3/5/2007	MW-39			6.84	Marel .					
	MW-39			6.26						
5/1/2007 6/22/2007	MW-39			6.26 6,95						
6/26/2007	MW-39			6.97	****				***	
7/6/2007	MW-39	***		7.18						
8/1/2007	MW-39			6.88						
8/7/2007	MW-39			6.61						arrival.
9/14/2007	MW-39			6.95						
10/8/2007	MW-39			6.24						
11/20/2007	MW-39			6.55			*****			
12/26/2007	MW-39			6.84				P		
1/2/2008	MW-39			6.85						Nu-
3/5/2008	MW-39			6.14						
4/23/2008	MW-39			7.12			*****			
5/12/2008	MW-39			5.64						
6/27/2008	MW-39			NM						
8/5/2008	MW-39			7.16						
9/10/2008	MW-39			6.73						~~~
10/27/2008	MW-39			5,33						
11/4/2008	MW-39			7.34				****		
1/5/2009	MW-39	****		7.53	~~~	****				
2/27/2009	MW-39			7.52						
3/9/2009	MW-39			5.23						
4/20/2009	MW-39			6.12						
4/29/2009	MW-39			7.76						
5/6/2009	MW-39			5.89						
6/2/2009	MW-39			6.63						
7/6/2009	MW-39			6.70						
8/14/2009	MW-39			6.64						
9/28/2009	MW-39			6.63						
10/13/2009	MW-39			6.77						
11/23/2009	MW-39			6.67						
12/2/2009	MW-39			5.49						
1/12/2010	MW-39			6.65						
2/2/2010	MW-39		~	7.49						
3/2/2010	MW-39		****	4.68						
3/15/2010	MW-39			5.43						
4/15/2010	MW-39			7.07						
4/22/2010	MW-39			6.60						
5/3/2010	MW-39		MW4	6.71						

Table 3 Groundwater Elevation Summary (Sorted by Well)

Date	Well #	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-40 / RW-40		7.64	8.25	0.61					
2/21/2006	MW-40 / RW-40		8.20	8.47	0.27					
3/7/2006	MW-40 / RW-40		9.29	10.14	0.85	*****				
5/18/2006	MW-40 / RW-40		7.87	8.69	0.82					
6/28/2006	MW-40 / RW-40		8.14	8.86	0.72					
8/16/2006	MW-40 / RW-40	'	8.40	8.95	0.55					
9/29/2006	MW-40 / RW-40		7.98	8.40	0.42					
10/20/2006	MW-40 / RW-40		8,04	8.98	0.94					
11/22/2006	MW-40 / RW-40		7.50	8.39	0.89					
12/15/2006	MW-40 / RW-40		8,50	8.65	0.15				0.50	
1/23/2007	MW-40 / RW-40		8.90	8.92	0.02					
2/2/2007	MW-40 / RW-40		8.56	8.90	0.34					
3/5/2007	MW-40 / RW-40		7.49	8.29	0.80				0.50	
5/1/2007	MW-40 / RW-40		7.35	8.21	0.86				1.50	
	MW-40 / RW-40		8.09	9.21	1.12				2.00	
6/22/2007	MW-40 / RW-40		8.43	9.53	1.10	****				
6/26/2007			8.67	8.89	0.22				0.25	
7/6/2007	MW-40 / RW-40 MW-40 / RW-40		7.87	8.79	0.92				2.00	
8/1/2007			7.07 8.06	8.35	0.32				0.25	
8/7/2007	MW-40 / RW-40			8.83	0.23					
9/14/2007	MW-40 / RW-40		8.81							
10/8/2007	MW-40 / RW-40		8.29	8,31	0.02				0.25	
11/20/2007	MW-40 / RW-40		8.41	8.51	0.10					
12/26/2007	MW-40 / RW-40		7.55	9.30	1.75					
1/2/2008	MW-40 / RW-40		7.59	9.41	1.82				2.00	
3/5/2008	MW-40 / RW-40		7.75	8.39	0.64				0.50	
4/23/2008	MW-40 / RW-40		8.66	9.10	0.44				0.75	
5/12/2008	MW-40 / RW-40		7.21	7.81	0.60					
6/27/2008	MW-40 / RW-40			8.60						
8/5/2008	MW-40 / RW-40		8.85	9.10	0.25				0.25	
9/10/2008	MW-40 / RW-40		7.70	8.68	0.98				1.00	
10/27/2008	MW-40 / RW-40		7.32	9.06	1.74				2.00	
11/4/2008	MW-40 / RW-40		9.35	10.25	0.90				1.25	
1/5/2009	MW-40 / RW-40		9.90	9.93	0.03					
2/27/2009	MW-40 / RW-40		8.99	9.00	0.01					
3/9/2009	MW-40 / RW-40		7.49	7.51	0.02					
4/20/2009	MW-40 / RW-40		8.10	8,33	0.23				0.50	
4/29/2009	MW-40 / RW-40		10.40	10.46	0.06				0.25	
	MW-40 / RW-40		7.79	7.89	0.10				0,25	
5/6/2009	MW-40 / RW-40		8.88	9.07	0.19				0.25	
6/2/2009			8.23	9.50	1.27		****		1.50	
7/6/2009	MW-40 / RW-40		6.∠3 8.98	9.08	0.10				0.25	
8/14/2009	MW-40 / RW-40			9.00	0.10				0.50	
9/28/2009	MW-40 / RW-40		8.87	9.14	0.27				0.25	
10/13/2009	MW-40 / RW-40		8.97		0.26				0.23	
11/23/2009	MW-40 / RW-40		7.00	8.65						
12/2/2009	MW-40 / RW-40	***	7.32	7.35	0.03					
1/12/2010	MW-40 / RW-40		8.76	8.87	0.11					
2/2/2010	MW-40 / RW-40		9.31	9.42	0.11				0.25	
3/2/2010	MW-40 / RW-40		6.92	7.04	0.12				0.25	
3/15/2010	MW-40 / RW-40		6.16	7.41	1.25					
4/15/2010	MW-40 / RW-40		9.09	9.11	0.02					
4/22/2010	MW-40 / RW-40		8.56	8.79	0.23				0.25	
5/3/2010	MW-40 / RW-40		8.59	10.55	1.96				2.00	

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

25 Paidge Avenue Brooklyn, New York NYSDEC SPILL NO. 87-09990

				NTSDEC S	PILL NO. 87-0	3990		<u> </u>		
Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	MW-41		7.59	7.63	0.04	,			0.10	
2/21/2006	MW-41		8.20	8.21	0.01	*****			0.10	
3/7/2006	MW-41			8.14						
5/18/2006	MW-41			8.19						
6/28/2006	MW-41		7.32	7.39	0.07					
8/16/2006	MW-41		7.95	8.01	0.06				***	******
9/29/2006	MW-41		7.78	7.94	0.16					
10/20/2006	MW-41			6.34						
11/22/2006	MW-41		6.68	6.71	0.03					
12/15/2006	MW-41 MW-41		7.60	7,62 8.16	0.02					
1/23/2007 2/2/2007	MW-41			6.85						
3/5/2007	MW-41			7.99						
5/1/2007	MW-41		7.05	7.16	0.11					
6/22/2007	MW-41		8.12	8.18	0.06	_~~				
6/26/2007	MW-41		7.69	7.72	0.03					
7/6/2007	MW-41		8.16	8.21	0.05					
8/1/2007	MW-41		7.79	7.91	0.12					
8/7/2007	MW-41		7.69	7.79	0.10					
9/14/2007	MW-41		7.84	7.96	0.12				0.25	
10/8/2007	MW-41		7.12	7.15	0.03				0.25	
11/20/2007	MW-41		7.61	7.63	0.02					
12/26/2007	MW-41			8.05						
1/2/2008	MW-41		8.00	8.09	0.09				0.25	
3/5/2008	MW-41		7.09	7.18	0.09				0.25	
4/23/2008	MW-41		8.11	8.16	0.05					
5/12/2008	MW-41		6.48	6.49	0.01					
6/27/2008	MW-41		7.67	7.82	0.15				0.25	
8/5/2008	MW-41		8.12	8.18	0.06					
9/10/2008	MW-41		7.68	7.75	0.07					
10/27/2008	MW-41			7.60	~					
11/4/2008	MW-41		8.21	8.22	0.01					
1/5/2009	MW-41		9.96	9.98	0.02					
2/27/2009	MW-41			8.11						
3/9/2009	MW-41 MW-41			5.94 7.31						
4/20/2009 4/29/2009	MW-41		9.13	9.14	0.01				***	***
5/6/2009	MW-41		6.61	6.62	0.01					-
6/2/2009	MW-41		8.09	8.15	0.06		****			
7/6/2009	MW-41			7.35						
8/14/2009	MW-41		8.15	8,25	0.10				0.25	
9/28/2009	MW-41		8.15	8.24	0.09					
10/13/2009	MW-41		8.24	8.33	0.09				0.25	
11/23/2009	MW-41		7.51	7.55	0.04					*
12/2/2009	MW-41			6.13		****	***			
1/12/2010	MW-41		8.01	8.04	0.03					
2/2/2010	MW-41		8.05	8.07	0.02					
3/2/2010	MW-41			NG						
3/15/2010	MW-41		5.94	5.95	0.01					
4/15/2010	MW-41		8.01	8.21	0.20					
4/22/2010	MW-41		8.24	8.41	0.17				0.25	
5/3/2010	MW-41		8.11	8.28	0.17				0.25	
3/2/2010	MW-42			2.90						
3/15/2010	MW-42			2.50						
4/15/2010	MW-42			3.54						
4/22/2010	MW-42			3.78						
5/3/2010	MW-42			3.45						
3/2/2010	MW-43			2.91						
3/15/2010	MW-43			2.64						
4/15/2010	MW-43			3.47						
4/22/2010	MW-43			3.64						
5/3/2010	MW-43			3.41						

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603 25 Paidge Avenue

Brooklyn, New York NYSDEC SPILL NO. 87-09990

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
3/2/2010	MW-44			2.87						
3/15/2010	MW-44		****	2.47						
4/15/2010	MW-44			3.58						
4/22/2010	MW-44			3.59						
5/3/2010	MW-44			3.37						
1/6/2006	TW-01			3.36						
2/21/2006	TW-01			NG					***	
3/7/2006	TW-01		4.28	4.34	0.06				0.10	
5/18/2006	TW-01		3.78	3.81	0.03				0.25	
6/28/2006	TW-01		3.79	3.84	0.05		*****			
8/16/2006	TW-01			NG		~~~				
9/29/2006	TW-01			NG		-				
10/20/2006	TW-01	and Principal	4.17	4.21	0.04					
12/15/2006	TW-01		4.28	4.32	0.04				in the rid	
1/23/2007	TW-01			NG						
2/2/2007	TW-01			4.21			-			
3/5/2007	TW-01		4.21	4.22	0.01	***				
5/1/2007	TW-01	***		NG						
6/22/2007	TW-01			NG						
6/26/2007	TW-01			NG						
7/6/2007	TW-01			NG						
8/1/2007	TW-01			NG			~~~			
8/7/2007	TW-01			NG						
9/14/2007	TW-01			NG						
10/8/2007	TW-01			NG						
11/20/2007	TW-01			NG						***
12/26/2007	TW-01			NG						
1/2/2008	TW-01			NG			****			
3/5/2008	TW-01			NG				******		****
4/23/2008	TW-01			NG					***	
5/12/2008	TW-01			NG						
6/27/2008	TW-01			NG						
8/5/2008	TW-01			NG						
9/10/2008	TW-01			NG						
10/27/2008	TW-01			NG						
11/4/2008	TW-01			NG		Here				
1/5/2009	TW-01	~~~		NG						
2/27/2009	TW-01			NG						
3/9/2009	TW-01			NG						
4/20/2009	TW-01		4.21	4.28	0.07					
4/29/2009	TW-01		4.35	4.40	0.05					Under water
5/6/2009	TW-01			NG						Under water
6/2/2009	TW-01			NG						Under Water
7/6/2009	TW-01			NG						Under Water
8/14/2009	TW-01			NG						
9/28/2009	TW-01			NG						
10/13/2009	TW-01			NG						
11/23/2009	TW-01			NG						
12/2/2009	TW-01			NG						
1/12/2010	TW-01		4.30	4.33	0.03					
2/2/2010	TW-01		4.42	4.44	0.02		*****			500
3/2/2010	TW-01			NG						Under Water
3/15/2010	TW-01			NG		****				Flooded
4/15/2010	TW-01			NG						
4/22/2010	TW-01			NG						
5/3/2010	TW-01			NG						

(Sorted by Well)

Motiva Enterprises LLC Terminal # 58603

25 Paidge Avenue Brooklyn, New York NYSDEC SPILL NO. 87-09990

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
1/6/2006	TW-02			3.17						
2/21/2006	TW-02			3.98						
3/7/2006	TW-02			4.21					***	
5/18/2006	TW-02			3.59						
6/28/2006	TW-02			3.58					~	
8/16/2006	TW-02			3.89						
9/29/2006	TW-02			3.65						
10/20/2006	TW-02			3.98						
12/15/2006	TW-02			4.16						
1/23/2007	TW-02			4.49					****	
2/2/2007	TW-02			4.37						
3/5/2007	TW-02		4.15	4.16	0.01					
5/1/2007	TW-02		3.52	3.54	0.02					
6/22/2007	TW-02			NG						
6/26/2007	TW-02		4.16	4.18	0.02					
7/6/2007	TW-02		4.02	4.05	0.03					
8/1/2007	TW-02		3.64	4.02	0.38			*****		
8/7/2007	TW-02			NG						
9/14/2007	TW-02			NG						
10/8/2007	TW-02			NG						
11/20/2007	TW-02			NG						
12/26/2007	TW-02			4.07						
1/2/2008	TW-02			NG						
3/5/2008	TW-02			NG						
4/23/2008	TW-02			NG						
5/12/2008	TW-02			3.34						
6/27/2008	TW-02		3,68	4.10	0.42					
8/5/2008	TW-02			NG						
9/10/2008	TW-02			NG						
10/27/2008	TW-02			NG						
11/4/2008	TW-02			4.29						
1/5/2009	TW-02			4.25						
2/27/2009	TW-02			4.79						
3/9/2009	TW-02			4.45						
4/20/2009	TW-02			4.20						
4/29/2009	TW-02			4.30						
5/6/2009	TW-02			3.79						
6/2/2009	TW-02			4.11						
7/6/2009	TW-02		****	NG						
8/14/2009	TW-02			NG						
9/28/2009	TW-02			3.93						
10/13/2009	TW-02			4.18					~	
11/23/2009	TW-02			3.89					****	
12/2/2009	TW-02		~	4.30						
1/12/2010	TW-02			4.17					~~~	
2/2/2010	TW-02			4.31						
3/2/2010	TW-02			2.79						
3/15/2010	TW-02			2.04						
4/15/2010	TW-02			3.76						
4/22/2010	TW-02			3.61			****			
5/3/2010	TW-02			3.35						

Table 3 Groundwater Elevation Summary (Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
2/21/2006	TW-03			NG						
3/7/2006	TW-03		3.74	3.76	0.02				0.10	
5/18/2006	TW-03			3,19						
6/28/2006	TW-03			3.02						
8/16/2006	TW-03			NG						
9/29/2006	TW-03			NG						
10/20/2006	TW-03		3.94	3.96	0.02					
12/15/2006	TW-03		3.62	3.71	0.09					
1/23/2007	TW-03		4.01	4.09	0.08					
2/2/2007	TW-03		4.06	4.11	0.05					
3/5/2007	TW-03			NG						
5/1/2007	TW-03			NG						
6/22/2007	TW-03			NG						
7/6/2007	TW-03			NG						
8/1/2007	TW-03			NG						
8/7/2007	TW-03			NG						
9/14/2007	TW-03			NG						
10/8/2007	TW-03			NG						
11/20/2007	TW-03			NG						
12/26/2007	TW-03			NG						
1/2/2008	TW-03			NG						
3/5/2008	TW-03			NG						
4/23/2008	TW-03			NG						
	TW-03			NG						
5/12/2008				NG						
6/27/2008	TW-03									
8/5/2008	TW-03			NG						
9/10/2008	TW-03			NG						
10/27/2008	TW-03			NG						
11/4/2008	TW-03			NG						
1/5/2009	TW-03			NG						
2/27/2009	TW-03		~~~	NG						
3/9/2009	TW-03			NG						
4/20/2009	TW-03	****		NG						
4/29/2009	TW-03			NG						Under water
5/6/2009	TW-03	~		NG						Under water
6/2/2009	TW-03			NG						Under Water
7/6/2009	TW-03	~		NG						Under Water
8/14/2009	TW-03			NG						
9/28/2009	TW-03			NG						
10/13/2009	TW-03	~		NG						
11/23/2009	TW-03	~		NG						
12/2/2009	TW-03	•		NG			~~~	an 10.00		
1/12/2010	TW-03			NG						
2/2/2010	TW-03			NG						Under Water
3/2/2010	TW-03			NG						Under Water
3/15/2010	TW-03			NG			*			Flooded
4/15/2010	TW-03			NG			***			
4/22/2010	TW-03			NG						
5/3/2010	TW-03			NG						

(Sorted by Well)

Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
2/21/2006	TW-04			NG						
3/7/2006	TW-04			. NG						
5/18/2006	TW-04			2.66						
6/28/2006	TW-04			NG						
8/16/2006	TW-04			NG						
9/29/2006	TW-04			NG						
10/20/2006	TW-04			NG						
12/15/2006	TW-04			3.05						
1/23/2007	TW-04			3.15			5			
2/2/2007	TW-04			3.36						
3/5/2007	TW-04			NG						
5/1/2007	TW-04			NG						
6/22/2007	TW-04			NG						
6/26/2007	TW-04			NG						
7/6/2007	TW-04			NG						
8/1/2007	TW-04			NG						
8/7/2007	TW-04			NG						
	TW-04			NG						
9/14/2007				NG						
10/8/2007	TW-04									
11/20/2007	TW-04			NG						
12/26/2007	TW-04			NG		***				
1/2/2008	TW-04			NG						~
3/5/2008	TW-04			NG						~
4/23/2008	TW-04			NG						~
5/12/2008	TW-04			NG						
6/27/2008	TW-04			NG						
8/5/2008	TW-04			NG						
9/10/2008	TW-04			NG						
10/27/2008	TW-04			NG						~
11/4/2008	TW-04			NG					~	
1/5/2009	TW-04			NG						
2/27/2009	TW-04			NG					~	
3/9/2009	TW-04			NG						
4/20/2009	TW-04			NG						
4/29/2009	TW-04			NG						Under water
5/6/2009	TW-04			NG					~	Under water
6/2/2009	TW-04			NG						Under Water
7/6/2009	TW-04			NG						Under Water
8/14/2009	TW-04			NG		***				
9/28/2009	TW-04			NG						
10/13/2009	TW-04			NG						
11/23/2009	TW-04			NG						
12/2/2009	TW-04			NG						
1/12/2010	TW-04	·		NG						
2/2/2010	TW-04			NG						Under Water
3/2/2010	TW-04			NG						
3/15/2010	TW-04			NG						Under Water
										Flooded
4/15/2010	TW-04			NG						
4/22/2010	TW-04			NG						
5/3/2010	TW-04			NG						

Table 3 Groundwater Elevation Summary (Sorted by Well)

·					· ·					
Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
2/21/2006	TW-05			NG						
3/7/2006	TW-05		3,54	3.75	0.21				0.50	
5/18/2006	TW-05		2.75	2.90	0.15				0.25	
6/28/2006	TW-05		2.72	2.91	0.19		*****			
9/29/2006	TW-05		3.05	3.20	0.15					
10/20/2006	TW-05			NG						
12/15/2006	TW-05		3.42	3.71	0.29				0.25	
1/23/2007	TW-05		3.80	4.17	0.37				0.25	
2/2/2007	TW-05		3.75	4.14	0,39				0.25	
3/5/2007	TW-05		3.56	3.67	0.11				0.25	
5/1/2007	TW-05		2.56	2.65	0.09				0.25	
6/22/2007	TW-05			NG	****					
6/26/2007	TW-05		4.33	4.54	0.21					
7/6/2007	TW-05		3.25	3.33	0.08					
8/1/2007	TW-05			NG						
8/7/2007	TW-05			NG						
9/14/2007	TW-05			NG						
10/8/2007	TW-05			NG						,,==
11/20/2007	TW-05			NG						
12/26/2007	TW-05			NG						
1/2/2008	TW-05			NG						
3/5/2008	TW-05			NG					*****	
4/23/2008	TW-05			NG		-				
5/12/2008	TW-05			NG						
6/27/2008	TW-05			NG			****			
8/5/2008	TW-05			NG						
9/10/2008	TW-05			NG						
10/27/2008	TW-05			NG						
11/4/2008	TW-05			NG						
1/5/2009	TW-05			NG						
			3.44	3.62	0.18					
4/20/2009	TW-05			4.00						
4/29/2009	TW-05 TW-05		3.79 	4.00 NG	0.21					Under water
5/6/2009	TW-05			NG						Under Water
6/2/2009 7/6/2009	TW-05			NG NG						Under Water Under Water
	TW-05			NG						Onder water
8/14/2009	TW-05		3,19	3,26	0.07				0.25	
9/28/2009				3.26 3.68	0.07					
10/13/2009	TW-05 TW-05		3,35	NG	0,33				0.50	
11/23/2009	TW-05			NG						
12/2/2009				NG						
1/12/2010	TW-05			NG NG						Under Water
2/2/2010	TW-05					*****				
3/2/2010	TW-05			NG						Under Water
3/15/2010	TW-05			NG						Flooded
4/15/2010	TW-05			NG						
4/22/2010	TW-05			NG			***			
5/3/2010	TW-05			NG						

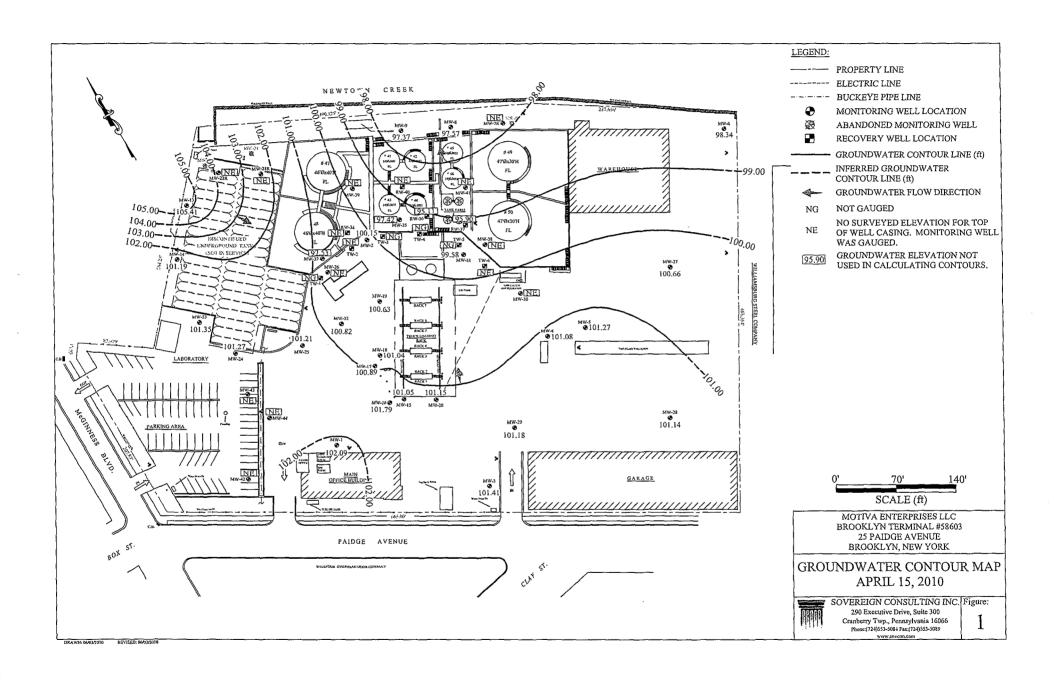
(Sorted by Well)

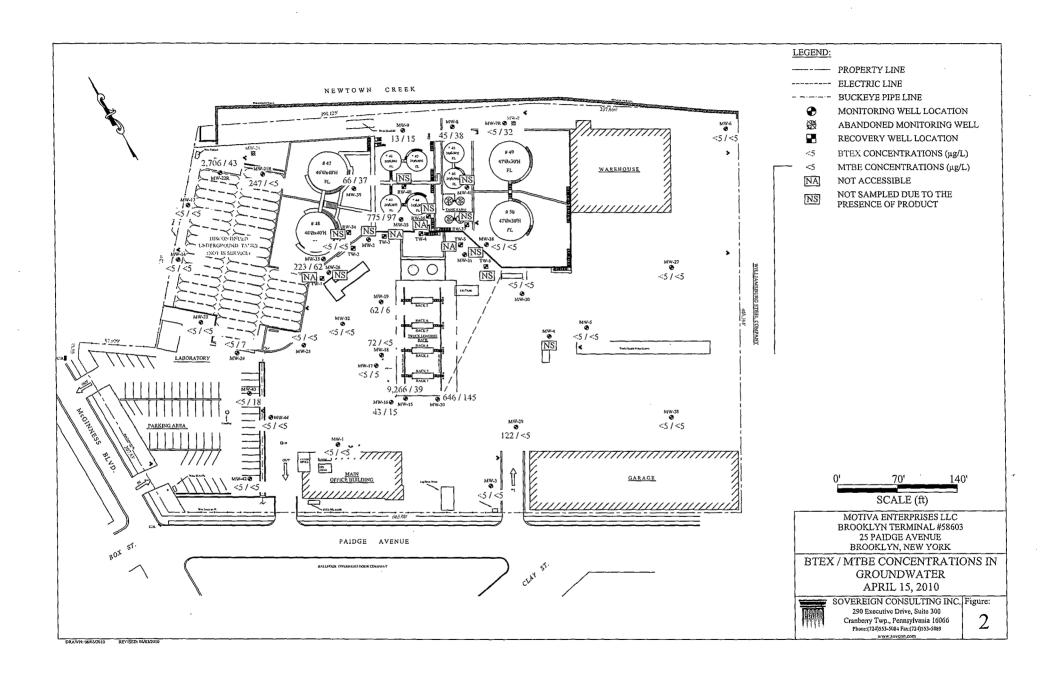
Motiva Enterprises LLC Terminal # 58603 25 Paidge Avenue Brooklyn, New York NYSDEC SPILL NO. 87-09990

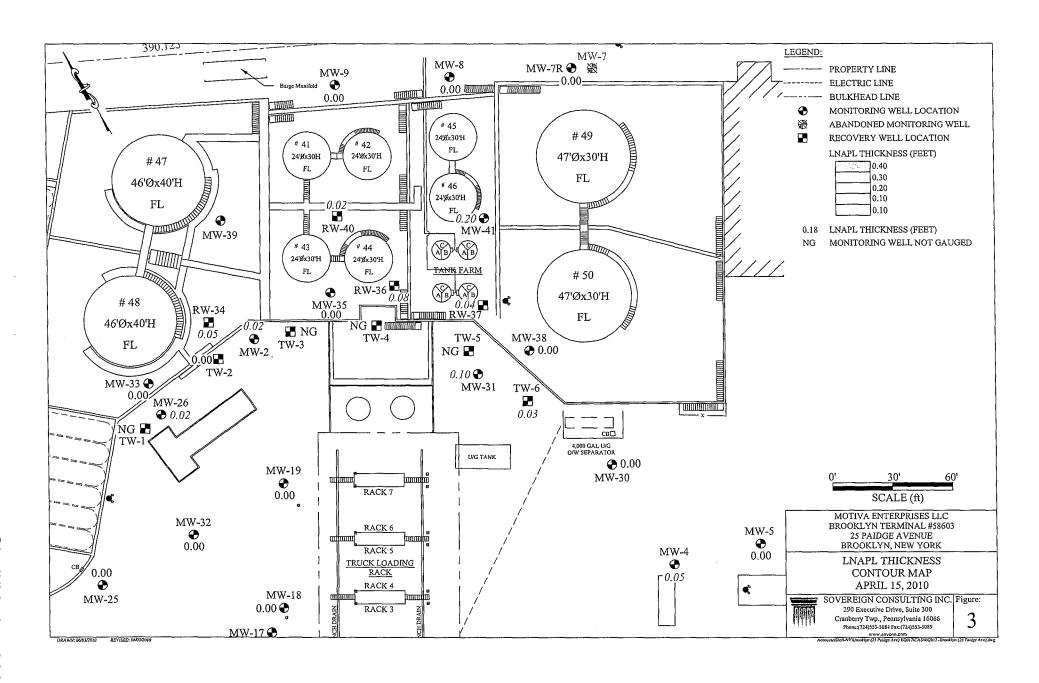
Date	Well#	Top of Casing Elevation (ft)	Depth to Product (ft.)	Depth to Water (ft.)	Product Thickness (ft.)	Product Elevation (ft.)	Water- Table Elevation (ft.)	Corrected Water-Table Elevation (ft.)	Product Rec. (gal.)	Notes
2/21/2006	TW-06			NG						
3/7/2006	TW-06		3.05	3.19	0.14				0.10	
5/18/2006	TW-06			NG						
6/28/2006	TW-06		2.52	2.68	0.16					
9/29/2006	TW-06	*****		NG						
10/20/2006	TW-06			NG						
12/15/2006	TW-06		2.98	3.24	0.26					
1/23/2007	TW-06		3.35	3.59	0.24			****		
2/2/2007	TW-06		3.28	3.48	0.20				0.25	
3/5/2007	TW-06		3.10	3.14	0.04					
5/1/2007	TW-06		2.32	2.34	0.02					
6/22/2007	TW-06			NG						
6/26/2007	TW-06		3.08	3.13	0.05		****			
7/6/2007	TW-06			NG						
8/1/2007	TW-06			NG						
8/7/2007	TW-06			NG			****		***	
9/14/2007	TW-06			NG						
10/8/2007	TW-06			NG						
11/20/2007	TW-06			NG						
12/26/2007	TW-06			NG		n-4				
1/2/2008	TW-06			NG		-				
3/5/2008	TW-06			NG		M-17-4				
4/23/2008	TW-06			NG						
5/12/2008	TW-06			NG						
6/27/2008	TW-06			NG						
8/5/2008	TW-06			NG						
9/10/2008	TW-06			NG						
10/27/2008	TW-06			NG						~
11/4/2008	TW-06			NG						P#4
1/5/2009	TW-06			NG					****	
2/27/2009	TW-06			NG						
3/9/2009	TW-06			NG						
4/20/2009	TW-06			NG						•
4/29/2009	TW-06	*****		NG						Under water
5/6/2009	TW-06			NG						Under water
6/2/2009	TW-06			NG			******			Under Water
7/6/2009	TW-06			NG						Under Water
8/14/2009	TW-06			NG						
9/28/2009	TW-06			NG						
10/13/2009	TW-06			NG						
11/23/2009	TW-06			NG			bearing.			
12/2/2009	TW-06			NG						1
1/12/2010	TW-06		****	NG						
2/2/2010	TW-06			NG						Under Water
3/2/2010	TW-06			NG						
3/15/2010	TW-06			NG						Flooded
4/15/2010	TW-06		2.82	2.85	0.03					
4/22/2010	TW-06		2.82	2.85	0.03					
5/3/2010	TW-06			NG						

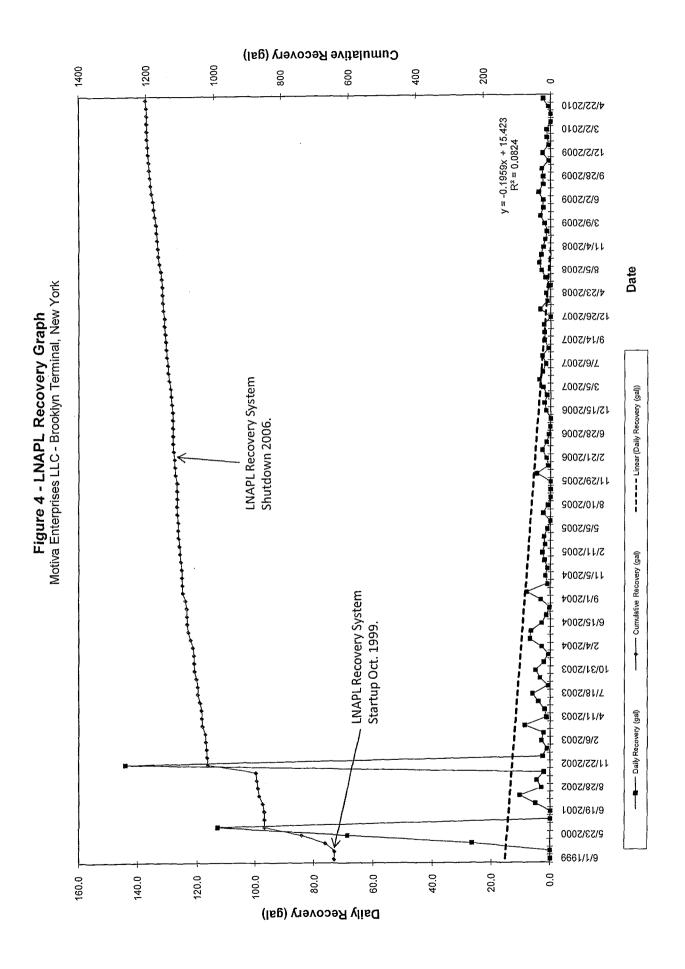
Note: NG = Not Gauged

FIGURES









APPENDIX A

April 2010 Groundwater Analysis Laboratory Report

Analytical Report 369409

for

Sovereign Consulting, Inc. (NY)

Project Manager: Gregory Bosiljcic

25 Paidge Avenue EQ24

30-APR-10





4143 Greenbriar Dr., Stafford, TX 77477 Ph:(281) 240-4200 Fax:(281) 240-4280

Xenco-Houston (EPA Lab code: TX00122):

Texas (T104704215-TX), Arizona (AZ0738), Arkansas (08-039-0), Connecticut (PH-0102), Florida (E871002) Illinois (002082), Indiana (C-TX-02), Iowa (392), Kansas (E-10380), Kentucky (45), Louisiana (03054) New Hampshire (297408), New Jersey (TX007), New York (11763), Oklahoma (9218), Pennsylvania (68-03610) Rhode Island (LAO00312), USDA (S-44102)

Xenco-Atlanta (EPA Lab Code: GA00046): Florida (E87429), North Carolina (483), South Carolina (98015), Utah (AALI1), West Virginia (362), Kentucky (85) Louisiana (04176), USDA (P330-07-00105)

Xenco-Miami (EPA Lab code: FL01152): Florida (E86678), Maryland (330)
Xenco-Tampa Mobile (EPA Lab code: FL01212): Florida (E84900)
Xenco-Odessa (EPA Lab code: TX00158): Texas (T104704400-TX)
Xenco-Dallas (EPA Lab code: TX01468): Texas (T104704295-TX)
Xenco-Corpus Christi (EPA Lab code: TX02613): Texas (T104704370)
Xenco-Boca Raton (EPA Lab Code: FL00449):
Florida(E86240),South Carolina(96031001), Louisiana(04154), Georgia(917)
North Carolina(444), Texas(T104704468-TX), Illinois(002295)





30-APR-10

Project Manager: Gregory Bosiljcic Sovereign Consulting, Inc. (NY) 3104 Unionville Road, Suite 150 Cranberry Twp, PA 16066

Reference: XENCO Report No: 369409

25 Paidge Avenue

Project Address: Brooklyn, NY

Gregory Bosiljcic:

We are reporting to you the results of the analyses performed on the samples received under the project name referenced above and identified with the XENCO Report Number 369409. All results being reported under this Report Number apply to the samples analyzed and properly identified with a Laboratory ID number. Subcontracted analyses are identified in this report with either the NELAC certification number of the subcontract lab in the analyst ID field, or the complete subcontracted report attached to this report.

Unless otherwise noted in a Case Narrative, all data reported in this Analytical Report are in compliance with NELAC standards. Estimation of data uncertainty for this report is found in the quality control section of this report unless otherwise noted. Should insufficient sample be provided to the laboratory to meet the method and NELAC Matrix Duplicate and Matrix Spike requirements, then the data will be analyzed, evaluated and reported using all other available quality control measures.

The validity and integrity of this report will remain intact as long as it is accompanied by this letter and reproduced in full, unless written approval is granted by XENCO Laboratories. This report will be filed for at least 5 years in our archives after which time it will be destroyed without further notice, unless otherwise arranged with you. The samples received, and described as recorded in Report No. 369409 will be filed for 60 days, and after that time they will be properly disposed without further notice, unless otherwise arranged with you. We reserve the right to return to you any unused samples, extracts or solutions related to them if we consider so necessary (e.g., samples identified as hazardous waste, sample sizes exceeding analytical standard practices, controlled substances under regulated protocols, etc).

We thank you for selecting XENCO Laboratories to serve your analytical needs. If you have any questions concerning this report, please feel free to contact us at any time.

Respectfully,

Carlos Castro

Managing Director, Texas

Recipient of the Prestigious Small Business Administration Award of Excellence in 1994.

Certified and approved by numerous States and Agencies.

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Houston - Dallas - San Antonio - Austin - Tampa - Miami - Atlanta - Corpus Christi - Latin America



Sample Cross Reference 369409



Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id	Matrix	Date Collected	Sample Depth	Lab Sample Id
MW-1	W	Apr-15-10 07:00		369409-001
MW-3	W	Apr-15-10 07:15		369409-002
MW-29	W	Apr-15-10 07:30	•	369409-003
MW-5	W	Apr-15-10 07:45		369409-004
MW-28	W	Apr-15-10 07:55		369409-005
MW-27	W	Apr-15-10 08:00		369409-006
MW-6	W	Apr-15-10 08:10		369409-007
MW-7R	W	Apr-15-10 08:20		369409-008
MW-8	W	Apr-15-10 08:30		369409-009
MW-9	W	Apr-15-10 08:40		369409-010
MW-21R	W	Apr-15-10 08:50		369409-011
MW-22R	W	Apr-15-10 09:00		369409-012
MW-13	W	Apr-15-10 09:10		369409-013
MW-14	W	Apr-15-10 09:20		369409-014
MW-23	W	Apr-15-10 09:30		369409-015
MW-24	W	Apr-15-10 09:40		369409-016
MW-43	W	Apr-15-10 09:50		369409-017
MW-42	W	Apr-15-10 10:00		369409-018
MW-44	W	Apr-15-10 10:10		369409-019
MW-30	W	Apr-15-10 10:20		369409-020
MW-25	W	Apr-15-10 10:30		369409-021
TRW-2	W	Apr-15-10 10:40		369409-022
MW-20	W	Apr-15-10 10:50		369409-023
MW-15	W	Apr-15-10 11:00		369409-024
MW-16	W	Apr-15-10 11:10		369409-025
MW-17	W	Apr-15-10 11:20		369409-026
MW-19	W	Apr-15-10 11:30		369409-027
MW-32	W	Apr-15-10 11:40		369409-028
MW-33	W	Apr-15-10 11:50		369409-029
MW-39	W	Apr-15-10 12:00		369409-030
MW-35	W	Apr-15-10 12:10		369409-031
MW-38	W	Apr-15-10 12:20		369409-032
MW-18	W	Apr-15-10 12:30		369409-033
Trip Blank	W	Apr-15-10 00:00		369409-034
Field Blank	W	Apr-15-10 07:00		369409-035
:: = <u>-</u> = <u>-</u>		•		





Client Name: Sovereign Consulting, Inc. (NY)

Project Name: 25 Paidge Avenue



Proiect ID:

EO24

Work Order Number: 369409

Report Date: 30-APR-10

Date Received: 04/16/2010

Sample receipt non conformances and Comments:

None

Sample receipt Non Conformances and Comments per Sample:

None

Analytical Non Conformances and Comments:

Batch: LBA-803446 VOAs by SW-846 8260B

SW8260B

Batch 803446, Trichlorofluoromethane recovered above QC limits in the laboratory control sample. Any hits would be considered as biased high; however, there are no hits reporting for this compound for the affected sample. Samples affected are: 369409-002, -001.

Batch: LBA-803645 VOAs by SW-846 8260B

SW8260B

Batch 803645, n-Propylbenzene recovered below QC limits in the Matrix Spike Duplicate. Samples affected are: 369409-003.

The Laboratory Control Sample for n-Propylbenzene is within laboratory Control Limits

SW8260B

Batch 803645, Methylene Chloride recovered below QC limits in the laboratory control sample. Any hits would be considered as biased low; however, there are no hits reporting for this compound for the affected sample. The Laboratory Control Sample passes due to Nelac Quality Systems, Appendix D, Marginal Exceedences. Samples affected are: 369409-003.

Batch: LBA-803828 VOAs by SW-846 8260B

SW8260B

Batch 803828, Toluene-D8 recovered above QC limits . Matrix interferences is suspected; data confirmed by re-analysis

Samples affected are: 369409-012.





Client Name: Sovereign Consulting, Inc. (NY)

Project Name: 25 Paidge Avenue



Project ID:

EQ24 Work Order Number: 369409

Report Date: 30-APR-10

Date Received: 04/16/2010

Batch: LBA-804058 VOAs by SW-846 8260B

SW8260B

Batch 804058, Vinyl Chloride recovered below QC limits in the Matrix Spike.

Samples affected are: 369409-025.

The Laboratory Control Sample for Vinyl Chloride is within laboratory Control Limits

Batch: LBA-804067 VOAs by SW-846 8260B

None

Batch: LBA-804536 VOAs by SW-846 8260B

None

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-1

Matrix: Water

% Moisture:

Lab Sample Id: 369409-001

Date Collected: Apr-15-10 07:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

	Analyst: CY Seq Number: 803		Date Prep:	Apr-20-10 19	9:12	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL U	Jnits	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00	ug	g/L	04/20/10 20:50		1
Bromobenzene	108-86-1	BRL	5.00	uş	g/L	04/20/10 20:50		1
Bromochloromethane	74-97-5	BRL	5.00	ug	g/L	04/20/10 20:50		1
Bromodichloromethane	75-27-4	BRL	5.00	ug	g/L	04/20/10 20:50		1
Bromoform	75-25-2	BRL	5.00	ug	g/L	04/20/10 20:50		I
Bromomethane	74-83-9	BRL	5.00		g/L	04/20/10 20:50		1
MTBE	1634-04-4	BRL	5.00	ug	<u>z</u> /L	04/20/10 20:50		1
n-Butylbenzene	104-51-8	BRL	5.00	ug	<u>z</u> /L	04/20/10 20:50		1
Sec-Butylbenzene	135-98-8	BRL	5.00	ug	z/L	04/20/10 20:50		1
tert-Butylbenzene	98-06-6	BRL	5.00	ug	g/L	04/20/10 20:50		1
Carbon Tetrachloride	56-23-5	BRL	5.00	ug	z/L	04/20/10 20:50		1
Chlorobenzene	108-90-7	BRL	5.00	ug	g/L	04/20/10 20:50		1
Chloroethane	75-00-3	BRL	10.0	ug	z/L	04/20/10 20:50		1
Chloroform	67-66-3	7.96	5.00	ug	z/L	04/20/10 20:50		1
Chloromethane	74-87-3	BRL	10.0		g/L	04/20/10 20:50		1
2-Chlorotoluene	95-49-8	BRL	5.00			04/20/10 20:50		1
4-Chlorotoluene	106-43-4	BRL	5.00	ug		04/20/10 20:50		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00	นย	z/L	04/20/10 20:50		1
Dibromochloromethane	124-48-1	BRL	5.00			04/20/10 20:50		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00	นย		04/20/10 20:50		1
Dibromomethane	74-95 - 3	BRL	5.00	ug	ý/L	04/20/10 20:50		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00			04/20/10 20:50		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00			04/20/10 20:50		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		/L	04/20/10 20:50		1
Dichlorodifluoromethane	75-71-8	BRL	5.00			04/20/10 20:50		1
1,1-Dichloroethane	75-34-3	BRL	5.00			04/20/10 20:50		1
1,2-Dichloroethane	107-06-2	BRL	5.00	ug		04/20/10 20:50		1
1,1-Dichloroethene	75-35-4	BRL	5.00	ug		04/20/10 20:50		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00	ug		04/20/10 20:50		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ug		04/20/10 20:50		1
1,2-Dichloropropane	78-87-5	BRL	5.00	ug		04/20/10 20:50		1
1,3-Dichloropropane	142 - 28-9	BRL	5.00	ug		04/20/10 20:50		1
2,2-Dichloropropane	594 - 20-7	BRL	5.00	ug	/L	04/20/10 20:50		1
1,1-Dichloropropene	563-58-6	BRL	5.00	ug		04/20/10 20:50		I
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00	ug.	/L	04/20/10 20:50		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00	ug	/L	04/20/10 20:50		1
Ethylbenzene	100-41-4	BRL	5.00	ug		04/20/10 20:50		1
Hexachlorobutadiene	87-68-3	BRL	5.00	ug		04/20/10 20:50		1
isopropylbenzene	98-82-8	BRL	5.00	ug,	/L	04/20/10 20:50		1

Project: Standard List of Methods

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-1

Matrix: Water

% Moisture:

Lab Sample Id: 369409-001

Date Collected: Apr-15-10 07:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-20-10 19:12

Tech: CYE

	Seq Number: 803	446	•	•				
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/20/10 20:50		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/20/10 20:50		I
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/20/10 20:50		1
Styrene	100-42-5	BRL	5.00		ug/L	04/20/10 20:50		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/20/10 20:50		1
1,1,2,2-Tetrachloroethane	79-34-5	\mathtt{BRL}	5.00		ug/L	04/20/10 20:50		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/20/10 20:50		1
Toluene	108-88-3	BRL	5.00		ug/L	04/20/10 20:50		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/20/10 20:50		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/20/10 20:50		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/20/10 20:50		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/20/10 20:50		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/20/10 20:50		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/20/10 20:50		1
1,2,3-Trichloropropane	96-18-4	\mathtt{BRL}	5.00		ug/L	04/20/10 20:50		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/20/10 20:50		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/20/10 20:50		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/20/10 20:50		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/20/10 20:50		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/20/10 20:50		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/20/10 20:50		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-3

Matrix: Water

% Moisture:

Lab Sample Id: 369409-002

Date Collected: Apr-15-10 07:15

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-20-10 20:30

Tech: CYE

	Analyst: CY		Date Prep:	Apr-20-10 20:3	0 Tech: C	CYE
	Seq Number: 803	446				
Parameter	Cas Number	Result	PQL	MDL Uni	ts Analysis Date F	lag Dil
Benzene	71-43-2	BRL	5.00	ug/L	04/21/10 05:05	1
Bromobenzene	108-86-1	BRL	5.00	ug/L	04/21/10 05:05	1
Bromochloromethane	74-97-5	BRL	5.00	ug/L	04/21/10 05:05	1
Bromodichloromethane	75-27-4	BRL	5.00	ug/L		1
Bromoform	75-25-2	BRL	5.00	ug/L	04/21/10 05:05	I
Bromomethane	74-83-9	BRL	5.00	ug/L	04/21/10 05:05	1
MTBE	1634-04-4	BRL	5.00	ug/L	04/21/10 05:05	1
n-Butylbenzene	104-51-8	BRL	5.00	ug/L	04/21/10 05:05	1
Sec-Butylbenzene	135-98-8	BRL	5.00	ug/L		1
tert-Butylbenzene	98-06-6	BRL	5.00	ug/L		1
Carbon Tetrachloride	56-23-5	BRL	5.00	ug/L	04/21/10 05:05	1
Chlorobenzene	108-90-7	BRL	5.00	ug/L	04/21/10 05:05	1
Chloroethane	75-00-3	BRL	10.0	ug/L		1
Chloroform	67-66-3	BRL	5.00	ug/L	04/21/10 05:05	1
Chloromethane	74-87-3	BRL	10.0	ug/L	04/21/10 05:05	1
2-Chlorotoluene	95-49-8	BRL	5.00	ug/L	04/21/10 05:05	1
4-Chlorotoluene	106-43-4	BRL	5.00	ug/L		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00	ug/L	04/21/10 05:05	1
Dibromochloromethane	124-48-1	BRL	5.00	ug/L	04/21/10 05:05	1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00	ug/L	04/21/10 05:05	1
Dibromomethane	74-95-3	BRL	5.00	ug/L	04/21/10 05:05	1
1,2-Dichlorobenzene	95-50-1	BRL	5.00	ug/L	04/21/10 05:05	1
1,3-Dichlorobenzene	541-73-1	BRL	5.00	ug/L	04/21/10 05:05	1
1,4-Dichlorobenzene	106-46-7	BRL	5.00	ug/L	04/21/10 05:05	1
Dichlorodifluoromethane	75-71-8	BRL	5.00	ug/L	04/21/10 05:05	1
1,1-Dichloroethane	75-34-3	BRL	5.00	ug/L	04/21/10 05:05	1
1,2-Dichloroethane	107-06-2	BRL	5.00	ug/L	04/21/10 05:05	1
1,1-Dichloroethene	75-35-4	BRL	5.00	ug/L	04/21/10 05:05	1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00	ug/L	04/21/10 05:05	1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ug/L	04/21/10 05:05	1
1,2-Dichloropropane	78-87-5	BRL	5.00	ug/L	04/21/10 05:05	1
1,3-Dichloropropane	142-28-9	BRL	5.00	ug/L	04/21/10 05:05	1
2,2-Dichloropropane	594-20-7	BRL	5.00	ug/L	04/21/10 05:05	1
1,1-Dichloropropene	563-58 - 6	BRL	5.00	ug/L	04/21/10 05:05	1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00	ug/L	04/21/10 05:05	1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00	ug/L	04/21/10 05:05	1
Ethylbenzene	100-41-4	BRL	5.00	ug/L	04/21/10 05:05	1
Hexachlorobutadiene	87-68-3	BRL	5.00	ug/L	04/21/10 05:05	1
isopropylbenzene	98-82-8	BRL	5.00	ug/L	04/21/10 05:05	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-3

Matrix: Water

% Moisture:

Lab Sample Id: 369409-002

Date Collected: Apr-15-10 07:15

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-20-10 20:30

Tech: CYE

	Seq Number: 803		Date Frep.	Apr-20-1	0 20.30	lecn:	CIE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/21/10 05:05		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/21/10 05:05		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/21/10 05:05		1
Styrene	100-42-5	BRL	5.00		ug/L	04/21/10 05:05		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/21/10 05:05		1
1,1,2,2-Tetrachloroethane	79-34- 5	BRL	5.00		ug/L	04/21/10 05:05		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/21/10 05:05		1
Toluene	108-88-3	BRL	5.00		ug/L	04/21/10 05:05		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/21/10 05:05		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/21/10 05:05		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/21/10 05:05		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/21/10 05:05		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/21/10 05:05		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/21/10 05:05		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/21/10 05:05		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/21/10 05:05		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/21/10 05:05		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/21/10 05:05		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/21/10 05:05		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/21/10 05:05		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/21/10 05:05		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-29

Matrix: Water

% Moisture:

Lab Sample Id: 369409-003

Date Collected: Apr-15-10 07:30

Date Received: Apr-16-10 09:00

Prep Method: SW5030B

Analytical Method: VOAs	by SW-846 8260					Prep Method: SV	W5030B	
	Analyst: CYl Seq Number: 803		Date Prep:	Apr-21-10	13:30	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	122	5.00		ug/L	04/21/10 13:58		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/21/10 13:58		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/21/10 13:58		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/21/10 13:58		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/21/10 13:58		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/21/10 13:58		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/21/10 13:58		1
n-Butylbenzene	104-51-8	10.9	5.00		ug/L	04/21/10 13:58		1
Sec-Butylbenzene	135-98-8	7.19	5.00		ug/L	04/21/10 13:58		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/21/10 13:58		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/21/10 13:58		1
Chlorobenzene	108-90 - 7	BRL	5.00		ug/L	04/21/10 13:58		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/21/10 13:58		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/21/10 13:58		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/21/10 13:58		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/21/10 13:58		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/21/10 13:58		1
p-Cymene (p-Isopropyltoluene)	99-87 - 6	BRL	5.00		ug/L	04/21/10 13:58		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/21/10 13:58		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/21/10 13:58		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/21/10 13:58		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/21/10 13:58		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/21/10 13:58		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/21/10 13:58		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/21/10 13:58		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/21/10 13:58		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/21/10 13:58		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/21/10 13:58		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/21/10 13:58		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00			04/21/10 13:58		1
1,2-Dichloropropane	78-87-5	BRL	5.00			04/21/10 13:58		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/21/10 13:58		1
2,2-Dichloropropane	594-20-7	BRL	5.00			04/21/10 13:58		1
1,1-Dichloropropene	563-58-6	BRL	5.00		_	04/21/10 13:58		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00			04/21/10 13:58		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00			04/21/10 13:58		1
Ethylbenzene	100-41-4	BRL	5.00		_	04/21/10 13:58		1
Hexachlorobutadiene	87-68-3	BRL	5.00			04/21/10 13:58		1
isopropylbenzene	98-82-8	63.1	5.00			04/21/10 13:58		1

Project: Standard List of Methods

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Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-29

Matrix: Water

% Moisture:

Lab Sample Id: 369409-003

Date Collected: Apr-15-10 07:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-21-10 13:30

Tech: CYE

Seq	Num	ber:	803645
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	Seq Number: 803	645					
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/21/10 13:58	1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/21/10 13:58	1
n-Propylbenzene	103-65-1	107	5.00		ug/L	04/21/10 13:58	1
Styrene	100-42-5	BRL	5.00		ug/L	04/21/10 13:58	1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/21/10 13:58	1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/21/10 13:58	1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/21/10 13:58	1
Toluene	108-88-3	BRL	5.00		ug/L	04/21/10 13:58	1
1,2,3-Trichlorobenzene	87-61 - 6	BRL	5.00		ug/L	04/21/10 13:58	1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/21/10 13:58	1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/21/10 13:58	1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/21/10 13:58	1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/21/10 13:58	1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/21/10 13:58	1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/21/10 13:58	1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/21/10 13:58	1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/21/10 13:58	1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/21/10 13:58	1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/21/10 13:58	1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/21/10 13:58	1
Total Xylenes	1330-20-7	\mathtt{BRL}	5.00		ug/L	04/21/10 13:58	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-5

Matrix: Water

% Moisture:

Lab Sample Id: 369409-004

Date Collected: Apr-15-10 07:45

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 15:06

Tech: CYE

	Seq Number: 803	828	•	•				
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 16:14		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 16:14		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 16:14		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 16:14		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 16:14		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 16:14		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 16:14		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 16:14		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 16:14		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 16:14		1
Carbon Tetrachloride	56-23 - 5	BRL	5.00		ug/L	04/22/10 16:14		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 16:14		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 16:14		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 16:14		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/22/10 16:14		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 16:14		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 16:14		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 16:14		1
Dibromochloromethane	124-48-1	\mathtt{BRL}	5.00		ug/L	04/22/10 16:14		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 16:14		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 16:14		1
1,2-Dichlorobenzene	95 - 50-1	BRL	5.00		ug/L	04/22/10 16:14		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 16:14		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 16:14		1
Dichlorodifluoromethane	75-71-8	\mathtt{BRL}	5.00		ug/L	04/22/10 16:14		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 16:14		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 16:14		1
1,1-Dichloroethene	75 - 35-4	BRL	5.00		ug/L	04/22/10 16:14		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 16:14		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 16:14		1
1,2-Dichloropropane	78-87 - 5	BRL	5.00		ug/L	04/22/10 16:14		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 16:14		1
2,2-Dichloropropane	594-20-7	BRL	5.00			04/22/10 16:14		1
1,1-Dichloropropene	563-58-6	BRL	5.00			04/22/10 16:14		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00			04/22/10 16:14		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00			04/22/10 16:14		1
Ethylbenzene	100-41-4	BRL	5.00			04/22/10 16:14		1
Hexachlorobutadiene	87-68-3	BRL	5.00			04/22/10 16:14		1
isopropylbenzene	98-82-8	BRL	5.00			04/22/10 16:14		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-5

Matrix: Water

% Moisture:

Lab Sample Id: 369409-004

Date Collected: Apr-15-10 07:45

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 15:06

Tech: CYE

	Seq Number: 803		Date Prep.	Apr-22-1	0 13:00	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 16:14		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 16:14		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 16:14		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 16:14		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 16:14		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 16:14		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 16:14		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 16:14		1
1,2,3-Trichlorobenzene	87-61 - 6	BRL	5.00		ug/L	04/22/10 16:14		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 16:14		1
1,1,1-Trichloroethane	71 - 55-6	BRL	5.00		ug/L	04/22/10 16:14		1
1,1,2-Trichloroethane	79-00 - 5	BRL	5.00		ug/L	04/22/10 16:14		1
Trichloroethene	79-01 - 6	BRL	5.00		ug/L	04/22/10 16:14		1.
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 16:14		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 16:14		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 16:14		i
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 16:14		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 16:14		1
m,p-Xylenes	179601-23-1	BRL	10.0			04/22/10 16:14		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 16:14		1
Total Xylenes	1330-20-7	BRL	5.00			04/22/10 16:14		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-28 Matrix: Water

% Moisture:

Lab Sample Id: 369409-005

Date Collected: Apr-15-10 07:55

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

-	-					-		
	Analyst: CYI		Date Prep:	Apr-22-10	18:56	Tech:	CYE	
	Seq Number: 803	828 						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 19:33		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 19:33		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 19:33		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 19:33		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 19:33		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 19:33		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 19:33		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 19:33		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 19:33		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 19:33		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 19:33		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 19:33		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 19:33		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 19:33		1
Chloromethane	74-87 - 3	BRL	10.0		ug/L	04/22/10 19:33		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 19:33		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 19:33		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 19:33		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 19:33		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 19:33		Ī
Dibromomethane	74-95 - 3	BRL	5.00		ug/L	04/22/10 19:33		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 19:33		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 19:33		ī
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 19:33		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 19:33		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 19:33		ì
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 19:33		î
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 19:33		î
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 19:33		î
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 19:33		î
1,2-Dichloropropane	78-87 - 5	BRL	5.00		ug/L	04/22/10 19:33		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 19:33		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 19:33		1
1,1-Dichloropropene	563-58-6	BRL	5.00			04/22/10 19:33		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		. 9 -	04/22/10 19:33		î
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		_	04/22/10 19:33		ì
Ethylbenzene	100-41-4	BRL	5.00			04/22/10 19:33		1
Hexachlorobutadiene	87-68-3	BRL	5.00		_	04/22/10 19:33		1
					n≪\ı ⊓K\T`			_
isopropylbenzene	98-82-8	BRL	5.00	·	ug/L	04/22/10 19:33		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-28

Matrix: Water

% Moisture:

Lab Sample Id: 369409-005

Date Collected: Apr-15-10 07:55

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 18:56

Tech: CYE

	Seq Number: 803		Date Frep.	. Apr-22-1	0 16.50	recn:	CIL	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 19:33		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 19:33		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 19:33		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 19:33		I
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 19:33		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 19:33		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 19:33		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 19:33		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 19:33		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 19:33		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/22/10 19:33		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 19:33		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 19:33		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 19:33		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 19:33		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 19:33		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 19:33		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 19:33		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 19:33		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 19:33		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/22/10 19:33		1

Project: Standard List of Methods

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-27

Matrix: Water

Lab Sample Id: 369409-006

Date Collected: Apr-15-10 08:00 Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

% Moisture:

	Analyst: CY Seq Number: 803		Date Prep:	Apr-22-10	18:58	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 19:55		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 19:55		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 19:55		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 19:55		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 19:55		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 19:55		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 19:55		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 19:55		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 19:55		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 19:55		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 19:55		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 19:55		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 19:55		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 19:55		1
Chloromethane	74-87 - 3	BRL	10.0		ug/L	04/22/10 19:55		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 19:55		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 19:55		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 19:55		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 19:55		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 19:55		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 19:55		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 19:55		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 19:55		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 19:55		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 19:55		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 19:55		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 19:55		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 19:55		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 19:55		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00			04/22/10 19:55		1
1,2-Dichloropropane	78-87-5	BRL	5.00			04/22/10 19:55		1
1,3-Dichloropropane	142-28 - 9	BRL	5.00			04/22/10 19:55		ĺ
2,2-Dichloropropane	594-20-7	BRL	5.00			04/22/10 19:55		1
1,1-Dichloropropene	563-58-6	BRL	5.00			04/22/10 19:55		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		U	04/22/10 19:55		1
trans-1,3-dichloropropene	10061-01-5	BRL	5.00		U	04/22/10 19:55		1
Ethylbenzene	10001-02-0	BRL	5.00		_	04/22/10 19:55		1
Hexachlorobutadiene	87-68-3	BRL	5.00		_	04/22/10 19:55		1
isopropylbenzene	98-82-8	BRL	5.00			04/22/10 19:55		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-27 Matrix: Water % Moisture:

Lab Sample Id: 369409-006

Date Collected: Apr-15-10 08:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 18:58

Tech: CYE

	Seq Number: 803	828	*	•				
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date 1	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 19:55		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 19:55		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 19:55		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 19:55		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 19:55		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 19:55		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 19:55		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 19:55		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 19:55		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 19:55		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/22/10 19:55		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 19:55		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 19:55		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 19:55		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 19:55		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 19:55		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 19:55		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 19:55		ļ
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 19:55		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 19:55		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/22/10 19:55		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-6

Matrix: Water

% Moisture:

Lab Sample Id: 369409-007

Date Collected: Apr-15-10 08:10

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

	Analyst: CYI Seq Number: 803		Date Prep:	Apr-22-1	0 19:00	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 20:17		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 20:17		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 20:17		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 20:17		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 20:17		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 20:17		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 20:17		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 20:17		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 20:17		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 20:17		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 20:17		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 20:17		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 20:17		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 20:17		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/22/10 20:17		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 20:17		ī
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 20:17		ī
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 20:17		î
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 20:17		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 20:17		ī
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 20:17		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L ug/L	04/22/10 20:17		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L ug/L	04/22/10 20:17		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L ug/L	04/22/10 20:17		ì
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 20:17		î
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L ug/L	04/22/10 20:17		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 20:17		î
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 20:17		î
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L ug/L	04/22/10 20:17		î
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L ug/L	04/22/10 20:17		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L ug/L	04/22/10 20:17		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L ug/L	04/22/10 20:17		1
2,2-Dichloropropane	594-20-7	BRL	5.00			04/22/10 20:17		1
1,1-Dichloropropene	563-58-6	BRL	5.00			04/22/10 20:17		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00			04/22/10 20:17		1
trans-1,3-dichloropropene		BRL				04/22/10 20:17		1
	10061-02-6 100-41-4	BRL	5.00 5.00					
Ethylbenzene						04/22/10 20:17]
Hexachlorobutadiene	87-68-3	BRL	5.00			04/22/10 20:17		1
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/22/10 20:17		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-6

% Moisture:

Lab Sample Id: 369409-007

Matrix: Water
Date Collected: Apr-15-10 08:10

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

	Analyst: CYE Seq Number: 803828		Date Prep: Apr-22-10		0 Tech: C	YE
Parameter	Cas Number	Result	PQL	MDL Uni	ts Analysis Date Fl	ag Dil
Methylene Chloride	75-09-2	BRL	5.00	ug/L	04/22/10 20:17	1
Naphthalene	91-20-3	BRL	10.0	ug/L		1
n-Propylbenzene	103-65-1	BRL	5.00	ug/L		1
Styrene	100-42-5	BRL	5.00	ug/L		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00	ug/L		1
1,1,2,2-Tetrachloroethane	79-34 - 5	BRL	5.00	ug/L		1
Tetrachloroethylene	127-18-4	BRL	5.00	ug/L		1
Toluene	108-88-3	BRL	5.00	ug/L		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00	ug/L		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00	ug/L		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00	ug/L		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00	ug/L		1
Trichloroethene	79-01 - 6	BRL	5.00	ug/L		1
Trichlorofluoromethane	75-69-4	BRL	5.00	ug/L		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00	ug/L		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00	ug/L		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00	ug/L		1
o-Xylene	95-47-6	BRL	5.00	ug/L		1
m,p-Xylenes	179601-23-1	BRL	10.0	ug/L		1
Vinyl Chloride	75-01-4	BRL	2.00	ug/L	04/22/10 20:17	1
Total Xylenes	1330-20-7	BRL	5.00	ug/L	04/22/10 20:17	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-7R

Matrix: Water

% Moisture:

Lab Sample Id: 369409-008

Date Collected: Apr-15-10 08:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analytical Method: VOAs	UY 377-040 840U				Prep Method: Sw	DUDUD
	Analyst: CYE Seq Number: 803828		Date Prep:	Apr-22-10 19:0	Tech:	CYE
Parameter	Cas Number	Result	PQL	MDL Un	its Analysis Date	Flag Di
Benzene	71-43-2	16.9	5.00	ug/I	04/22/10 20:39	1
Bromobenzene	108-86-1	BRL	5.00	ug/I	. 04/22/10 20:39	1
Bromochloromethane	74-97 - 5	BRL	5.00	ug/I	. 04/22/10 20:39	1
Bromodichloromethane	75-27-4	BRL	5.00	ug/L	, 04/22/10 20:39	1
Bromoform	75-25-2	BRL	5.00	ug/L	, 04/22/10 20:39	1
Bromomethane	74-83-9	BRL	5.00	ug/L		1
MTBE	1634-04-4	31.5	5.00	ug/L		1
n-Butylbenzene	104-51-8	BRL	5.00	ug/L		1
Sec-Butylbenzene	135-98-8	BRL	5.00	ug/L		1
tert-Butylbenzene	98-06-6	BRL	5.00	ug/L		1
Carbon Tetrachloride	56-23-5	BRL	5.00	ug/L		1
Chlorobenzene	108-90-7	BRL	5.00	ug/L		1
Chloroethane	75-00-3	BRL	10.0	ug/L		1
Chloroform	67-66-3	BRL	5.00	ug/L		1
Chloromethane	74-87-3	BRL	10.0	ug/L		1
2-Chlorotoluene	95-49-8	BRL	5.00	ug/L		î
4-Chlorotoluene	106-43-4	BRL	5.00	ug/L		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00	ug/L	04/22/10 20:39	î
Dibromochloromethane	124-48-1	BRL	5.00	ug/L		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00	ug/L		î
Dibromomethane	74-95 - 3	BRL	5.00	ug/L	04/22/10 20:39	1
1,2-Dichlorobenzene	95-50-1	BRL	5.00	ug/L		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00	ug/L ug/L		1
1,4-Dichlorobenzene	106-46 - 7	BRL	5.00			1
Dichlorodifluoromethane	75-71-8	BRL	5.00	ug/L		1
				ug/L		1
1,1-Dichloroethane	75-34-3	BRL	5.00	ug/L		1
1,2-Dichloroethane	107-06-2	BRL	5.00	ug/L		
1,1-Dichloroethene	75-35-4	BRL	5.00	ug/L		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00	ug/L		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ug/L		1
1,2-Dichloropropane	78-87-5	BRL	5.00	ug/L		1
1,3-Dichloropropane	142-28-9	BRL	5.00	ug/L		1
2,2-Dichloropropane	594-20-7	BRL	5.00	ug/L		1
1,1-Dichloropropene	563-58-6	BRL	5.00	ug/L		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00	ug/L	04/22/10 20:39	1
rans-1,3-dichloropropene	10061-02-6	BRL	5.00	ug/L	04/22/10 20:39	1
Ethylbenzene	100-41-4	BRL	5.00	ug/L		1
Hexachlorobutadiene	87-68-3	BRL	5.00	ug/L	04/22/10 20:39	1
isopropylbenzene	98-82-8	BRL	5.00	ug/L	04/22/10 20:39	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-7R

Matrix: Water

% Moisture:

Lab Sample Id: 369409-008

Date Collected: Apr-15-10 08:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:02

Tech: CYE

	Seq Number: 803828		Date Flep: Apr-22-10		0 19.02	lecn:	CIE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 20:39		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 20:39		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 20:39		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 20:39		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 20:39		1
1,1,2,2-Tetrachloroethane	79 - 34-5	BRL	5.00		ug/L	04/22/10 20:39		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 20:39		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 20:39		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 20:39		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 20:39		1
1,1,1-Trichloroethane	71-55 - 6	BRL	5.00		ug/L	04/22/10 20:39		1
1,1,2-Trichloroethane	79-00 - 5	BRL	5.00		ug/L	04/22/10 20:39		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 20:39		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 20:39		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 20:39		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 20:39		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 20:39		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 20:39		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 20:39		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 20:39		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/22/10 20:39		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-8 Matrix: Water

% Moisture:

Lab Sample Id: 369409-009

Date Collected: Apr-15-10 08:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Date Prep: Apr-22-10 19:04

Tech: CYE

	Analyst: CY. Seq Number: 803		Date Prep:	Apr-22-1	0 19:04	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	44.9	5.00		ug/L	04/22/10 21:01		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 21:01		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 21:01		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 21:01		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 21:01		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 21:01		1
MTBE	1634-04-4	37.6	5.00		ug/L	04/22/10 21:01		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 21:01		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 21:01		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 21:01		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 21:01		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 21:01		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 21:01		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 21:01		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/22/10 21:01		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 21:01		ì
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 21:01		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 21:01		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 21:01		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 21:01		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 21:01		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 21:01		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 21:01		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 21:01		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 21:01		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 21:01		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 21:01		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 21:01		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 21:01		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 21:01		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/22/10 21:01		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 21:01		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 21:01		1
1,1-Dichloropropene	563-58-6	BRL	5.00			04/22/10 21:01		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		U	04/22/10 21:01		î
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		0	04/22/10 21:01		î
Ethylbenzene	100-41-4	BRL	5.00		0	04/22/10 21:01		i
Hexachlorobutadiene	87-68-3	BRL	5.00			04/22/10 21:01		1
isopropylbenzene	98-82-8	BRL	5.00			04/22/10 21:01		î





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-8

Matrix: Water

% Moisture:

Lab Sample Id: 369409-009

Date Collected: Apr-15-10 08:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

Analyst: CYE
Seq Number: 803828

Prep Method: SW5030B

Tech: CYE

	Seq Number: 803	828						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09 - 2	BRL	5.00		ug/L	04/22/10 21:01		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 21:01		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 21:01		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 21:01		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 21:01		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 21:01		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 21:01		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 21:01		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 21:01		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 21:01		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/22/10 21:01		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 21:01		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 21:01		1
Trichlorofluoromethane	75-69 - 4	BRL	5.00		ug/L	04/22/10 21:01		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 21:01		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 21:01		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 21:01		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 21:01		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 21:01		1
Vinyl Chloride	75 - 01-4	BRL	2.00		ug/L	04/22/10 21:01		1
Total Xylenes	_ 1330-20-7 _	BRL	5.00		ug/L	04/22/10 21:01		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-9

Matrix: Water

% Moisture:

Lab Sample Id: 369409-010

Date Collected: Apr-15-10 08:40

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:06

Tech: CYE

	Seq Number: 803	828	Date Frep.	Apr-22-10 1.	2.00	recii.	CIE	
Parameter	Cas Number	Result	PQL	MDL U	Jnits	Analysis Date	Flag	Dil
Benzene	71-43-2	12.5	5.00		g/L	04/22/10 21:23		1
Bromobenzene	108-86-1	BRL	5.00	119	g/L	04/22/10 21:23		î
Bromochloromethane	74-97-5	BRL	5.00		g/L	04/22/10 21:23		1
Bromodichloromethane	75-27-4	BRL	5.00		g/L	04/22/10 21:23		1
Bromoform	75-25-2	BRL	5.00		g/L	04/22/10 21:23		1
Bromomethane	74-83-9	BRL	5.00		g/L	04/22/10 21:23		1
MTBE	1634-04-4	15.2	5.00		g/L	04/22/10 21:23		1
n-Butylbenzene	104-51-8	BRL	5.00		g/L	04/22/10 21:23		1
Sec-Butylbenzene	135-98-8	BRL	5.00		g/L	04/22/10 21:23		1
tert-Butylbenzene	98-06-6	BRL	5.00		g/L	04/22/10 21:23		1
Carbon Tetrachloride	56-23-5	BRL	5.00		g/L	04/22/10 21:23		1
Chlorobenzene	108-90-7	BRL	5.00		g/L	04/22/10 21:23		1
Chloroethane	75-00-3	BRL	10.0		g/L	04/22/10 21:23		1
Chloroform	67-66-3	BRL	5.00		g/L	04/22/10 21:23		1
Chloromethane	74-87-3	BRL	10.0		g/L	04/22/10 21:23		1
2-Chlorotoluene	95-49-8	BRL	5.00		g/L	04/22/10 21:23		1
4-Chlorotoluene	106-43-4	BRL	5.00		g/L	04/22/10 21:23		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		g/L	04/22/10 21:23		1
Dibromochloromethane	124-48-1	BRL	5.00		g/L	04/22/10 21:23		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		g/L	04/22/10 21:23		1
Dibromomethane	74-95-3	BRL	5.00		g/L	04/22/10 21:23		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		g/L	04/22/10 21:23		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		g/L	04/22/10 21:23		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		g/L	04/22/10 21:23		1
Dichlorodifluoromethane	75-71-8	BRL	5.00	uş	z/L	04/22/10 21:23		1
1,1-Dichloroethane	75-34-3	BRL	5.00		2/L	04/22/10 21:23		1
1,2-Dichloroethane	107-06-2	BRL	5.00	ug	z/L	04/22/10 21:23		1
1,1-Dichloroethene	75-35 - 4	BRL	5.00	ug	g/L	04/22/10 21:23		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		g/L	04/22/10 21:23		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ug	z/L	04/22/10 21:23		1
1,2-Dichloropropane	78-87 <i>-</i> 5	BRL	5.00	ug	g/L	04/22/10 21:23		1
1,3-Dichloropropane	142-28-9	BRL	5.00		g/L	04/22/10 21:23		1
2,2-Dichloropropane	594-20-7	BRL	5.00		z/L	04/22/10 21:23		1
1,1-Dichloropropene	563-58-6	BRL	5.00		₂ /L	04/22/10 21:23		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		g/L	04/22/10 21:23		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		<u>z</u> /L	04/22/10 21:23		1
Ethylbenzene	100-41-4	BRL	5.00	ug	z/L	04/22/10 21:23		1
Hexachlorobutadiene	87-68-3	BRL	5.00	ug	z/L	04/22/10 21:23	•	1
isopropylbenzene	98-82-8	BRL	5.00	ug	z/L	04/22/10 21:23		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-9

Matrix: Water

% Moisture:

Lab Sample Id: 369409-010

Date Collected: Apr-15-10 08:40

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:06

Tech: CYE

	Seq Number: 803	828						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 21:23		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 21:23		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 21:23		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 21:23		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 21:23		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 21:23		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 21:23		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 21:23		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 21:23		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 21:23		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00	•	ug/L	04/22/10 21:23		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 21:23		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 21:23		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 21:23		1
1,2,3-Trichloropropane	96-18-4	\mathtt{BRL}	5.00		ug/L	04/22/10 21:23		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 21:23		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 21:23		1
o-Xylene	95-47-6	\mathtt{BRL}	5.00		ug/L	04/22/10 21:23		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 21:23		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 21:23		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/22/10 21:23		1



Lab Sample Id: 369409-011

Certificate of Analytical Results 369409



Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-21R Matrix: Water % Moisture:

Date Collected: Apr-15-10 08:50 Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:08 Tech: CYE

	Seq Number: 803		Date Frep.	Apr-22-10	7 17.00	recn: C	, I E	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date F	lag	Dil
Benzene	71-43-2	139	5.00		ug/L	04/22/10 21:45		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 21:45		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 21:45		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 21:45		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 21:45		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 21:45		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 21:45		1
n-Butylbenzene	104-51-8	11.0	5.00		ug/L	04/22/10 21:45		1
Sec-Butylbenzene	135-98-8	29.9	5.00		ug/L	04/22/10 21:45		î
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 21:45		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 21:45		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 21:45		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 21:45		î
Chloroform	67-66-3	BRL	5.00		ug/L ug/L	04/22/10 21:45		1
Chloromethane	74-87-3	BRL	10.0		ug/L ug/L	04/22/10 21:45		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L ug/L	04/22/10 21:45		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 21:45		1
p-Cymene (p-Isopropyltoluene)	99-87-6	5.29	5.00		ug/L	04/22/10 21:45		î
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 21:45		ì
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 21:45		î
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 21:45		î
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 21:45		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 21:45		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 21:45		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 21:45		i
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 21:45		î
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 21:45		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 21:45		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 21:45		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 21:45		i
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/22/10 21:45		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 21:45		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 21:45		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/22/10 21:45		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/22/10 21:45		î
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/22/10 21:45		1
Ethylbenzene	100-41-4	41.5	5.00		ug/L	04/22/10 21:45		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/22/10 21:45		1
isopropylbenzene	98-82-8	145	5.00		ug/L	04/22/10 21:45		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-21R

Matrix: Water

% Moisture:

Lab Sample Id: 369409-011

Date Collected: Apr-15-10 08:50

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:08

Tech: CYE

	Seq Number: 803	828						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 21:45		1
Naphthalene	91-20-3	20.0	10.0		ug/L	04/22/10 21:45		1
n-Propylbenzene	103-65-1	34.0	5.00		ug/L	04/22/10 21:45		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 21:45		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 21:45		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 21:45		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 21:45		1
Toluene	108-88-3	12.2	5.00		ug/L	04/22/10 21:45		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 21:45		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 21:45		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/22/10 21:45		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 21:45		1
Trichloroethene	79-01 - 6	BRL	5.00		ug/L	04/22/10 21:45		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 21:45		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 21:45		1
1,2,4-Trimethylbenzene	95-63-6	133	5.00		ug/L	04/22/10 21:45		1
1,3,5-Trimethylbenzene	108-67-8	139	5.00		ug/L	04/22/10 21:45		1
o-Xylene	95-47-6	16.9	5.00		ug/L	04/22/10 21:45		1
m,p-Xylenes	179601-23-1	37.7	10.0		ug/L	04/22/10 21:45		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 21:45		1
Total Xylenes	1330-20-7	54.6	5.00		ug/L	04/22/10 21:45		1



Lab Sample Id: 369409-012

Certificate of Analytical Results 369409



Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-22R Matrix: Water

Date Collected: Apr-15-10 09:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

% Moisture:

	Analyst: CYI Seq Number: 803		Date Prep:	Apr-22-1	0 19:10	Tech:	СҮЕ	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	386	25.0		ug/L	04/23/10 19:36	D	5
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 22:07		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 22:07		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 22:07		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 22:07		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 22:07		1
MTBE	1634-04-4	42.8	5.00		ug/L	04/22/10 22:07		1
n-Butylbenzene	104-51-8	29.9	5.00		ug/L	04/22/10 22:07		1
Sec-Butylbenzene	135-98-8	19.2	5.00		ug/L	04/22/10 22:07		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 22:07		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 22:07		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 22:07		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 22:07		1
Chloroform	67 - 66-3	BRL	5.00		ug/L	04/22/10 22:07		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/22/10 22:07		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 22:07		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 22:07		1
p-Cymene (p-Isopropyltoluene)	99-87-6	6.61	5.00		ug/L	04/22/10 22:07		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 22:07		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 22:07		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 22:07		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 22:07		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 22:07		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 22:07		. 1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 22:07		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 22:07		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 22:07		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 22:07		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 22:07		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 22:07		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/22/10 22:07		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 22:07		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 22:07		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/22/10 22:07		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/22/10 22:07		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/22/10 22:07		1
Ethylbenzene	100-41-4	2140	100		ug/L	04/23/10 19:58	D	20
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/22/10 22:07		1
isopropylbenzene	98-82-8	217	25.0		ug/L	04/23/10 19:36	D	5





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-22R

Matrix: Water

% Moisture:

Lab Sample Id: 369409-012

Date Collected: Apr-15-10 09:00

Date Received: Apr-16-10 09:00

Date Prep: Apr-22-10 19:10

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Tech: CYE

	Seq Number: 803	828						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 22:07		1
Naphthalene	91-20-3	412	50.0		ug/L	04/23/10 19:36	D	5
n-Propylbenzene	103-65-1	426	25.0		ug/L	04/23/10 19:36	D	5
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 22:07		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 22:07		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L:	04/22/10 22:07		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 22:07		1
Toluene	108-88-3	68.4	5.00		ug/L	04/22/10 22:07		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 22:07		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 22:07		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/22/10 22:07		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 22:07		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 22:07		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 22:07		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 22:07		1
1,2,4-Trimethylbenzene	95-63-6	14.6	5.00		ug/L	04/22/10 22:07		1
1,3,5-Trimethylbenzene	108-67-8	217	25.0		ug/L	04/23/10 19:36	D	5
o-Xylene	95-47-6	22.9	5.00		ug/L	04/22/10 22:07		1
m,p-Xylenes	179601-23-1	88.3	10.0		ug/L	04/22/10 22:07		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 22:07		1
Total Xylenes	1330-20-7	111.2	5.00		ug/L	04/22/10 22:07		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-13

Matrix: Water

% Moisture:

Lab Sample Id: 369409-013

Date Collected: Apr-15-10 09:10

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:14

Tech: CYE

Seq Number: 803828

Seq Number: 803828									
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date F	lag	Dil	
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 22:51		1	
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 22:51		1	
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 22:51		1	
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 22:51		1	
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 22:51		1	
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 22:51		1	
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 22:51		1	
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 22:51		1	
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 22:51		1	
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 22:51		1	
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 22:51	•	1	
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 22:51		1	
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 22:51		1	
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 22:51		1	
Chloromethane	74-87-3	BRL	10.0		ug/L	04/22/10 22:51		1	
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 22:51		1	
4-Chlorotoluene	106-43-4	\mathtt{BRL}	5.00		ug/L	04/22/10 22:51		1	
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 22:51		1	
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 22:51		1	
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 22:51		1	
Dibromomethane	74-95 - 3	BRL	5.00		ug/L	04/22/10 22:51		1	
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 22:51		1	
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 22:51		1	
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 22:51		1	
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 22:51		1	
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 22:51		1	
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 22:51		1	
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 22:51		1	
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 22:51		1	
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 22:51		1	
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/22/10 22:51		1	
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 22:51		1	
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 22:51		1	
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/22/10 22:51		1	
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/22/10 22:51		1	
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/22/10 22:51		1	
Ethylbenzene	100-41-4	BRL	5.00			04/22/10 22:51		1	
Hexachlorobutadiene	87-68-3	BRL	5.00			04/22/10 22:51		1	
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/22/10 22:51		1	

Project: Standard List of Methods

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-13

Matrix: Water

% Moisture:

Lab Sample Id: 369409-013

Date Collected: Apr-15-10 09:10

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:14 Tech: CYE

	Seq Number: 803	828						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 22:51		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 22:51		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 22:51		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 22:51		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 22:51		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 22:51		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 22:51		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 22:51		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 22:51		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 22:51		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/22/10 22:51		1
1,1,2-Trichloroethane	79-00-5	\mathtt{BRL}	5.00		ug/L	04/22/10 22:51		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 22:51		1
Trichlorofluoromethane	75-69-4	\mathtt{BRL}	5.00		ug/L	04/22/10 22:51		1
1,2,3-Trichloropropane	96-18-4	\mathtt{BRL}	5.00		ug/L	04/22/10 22:51		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 22:51		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 22:51		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 22:51		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 22:51		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 22:51		1
Total Xylenes	1330-20-7	\mathtt{BRL}	5.00		ug/L	04/22/10 22:51		1

Project: Standard List of Methods

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-14 Matrix: Water % Moisture:

Lab Sample Id: 369409-014 Date Collected: Apr-15-10 09:20
Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

	Analyst: CY	E	Date Prep:	Apr-22-1	0 19:16	Tech:	CYE	
	Seq Number: 803	828						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 23:13		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 23:13		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 23:13		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 23:13		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 23:13		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 23:13		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 23:13		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 23:13		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 23:13		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 23:13		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 23:13		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 23:13		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 23:13		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 23:13		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/22/10 23:13		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 23:13		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 23:13		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 23:13		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 23:13		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 23:13		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 23:13		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 23:13		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 23:13		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 23:13		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 23:13		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 23:13		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 23:13		1
1,1-Dichloroethene	75-35 - 4	BRL	5.00		ug/L	04/22/10 23:13		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 23:13		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 23:13		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/22/10 23:13		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 23:13		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 23:13		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/22/10 23:13		ī
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/22/10 23:13		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/22/10 23:13		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/22/10 23:13		î
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/22/10 23:13		î
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/22/10 23:13		î





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-14

Matrix: Water

% Moisture:

Lab Sample Id: 369409-014

Date Collected: Apr-15-10 09:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:16

Tech: CYE

	Seq Number: 803	828		1		Toon.	. 012	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 23:13		1
Naphthalene	91-20 - 3	BRL	10.0		ug/L	04/22/10 23:13		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 23:13		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 23:13		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 23:13		1
1,1,2,2-Tetrachloroethane	79-34 - 5	BRL	5.00		ug/L	04/22/10 23:13		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 23:13		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 23:13		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 23:13		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 23:13		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/22/10 23:13		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 23:13		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 23:13		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 23:13		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 23:13		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 23:13		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 23:13		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 23:13		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 23:13		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 23:13		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/22/10 23:13		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-23 Matrix: Water % Moisture:

Lab Sample Id: 369409-015 Date Collected: Apr-15-10 09:30
Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

Analyst: CYE Sea Number: 803828

Date Prep:	Apr-22-10 19:18	Tech:	CYE

Seq Number: 803828										
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil		
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 23:35		1		
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 23:35		1		
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 23:35		1		
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 23:35		1		
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 23:35		1		
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 23:35		1		
MTBE	1634-04-4	BRL	5.00		ug/L	04/22/10 23:35		1		
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 23:35		1		
Sec-Butylbenzene	135-98-8	\mathtt{BRL}	5.00		ug/L	04/22/10 23:35		1		
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 23:35		1		
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 23:35		1		
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 23:35		1		
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 23:35		1		
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 23:35		1		
Chloromethane	74-87-3	BRL	10.0		ug/L	04/22/10 23:35		1		
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/22/10 23:35		1		
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 23:35		1		
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 23:35		1		
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 23:35		1		
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/22/10 23:35		1		
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 23:35		1		
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 23:35		1		
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 23:35		1		
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 23:35		1		
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/22/10 23:35		1		
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 23:35		1		
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/22/10 23:35		1		
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/22/10 23:35		1		
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 23:35		1		
rans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 23:35		1		
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/22/10 23:35		1		
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 23:35		1		
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 23:35		1		
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/22/10 23:35		1		
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/22/10 23:35		1		
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/22/10 23:35		1		
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/22/10 23:35		1		
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/22/10 23:35		1		
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/22/10 23:35		1		





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-23

Matrix: Water

% Moisture:

Lab Sample Id: 369409-015

Date Collected: Apr-15-10 09:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:18

Tech: CYE

	Seq Number: 803	828						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 23:35		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 23:35		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 23:35		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 23:35		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 23:35		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 23:35		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 23:35		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 23:35		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 23:35		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 23:35		1
1,1,1-Trichloroethane	71-55-6	\mathtt{BRL}	5.00		ug/L	04/22/10 23:35		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 23:35		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 23:35		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 23:35		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 23:35		1
1,2,4-Trimethylbenzene	95-63-6	\mathtt{BRL}	5.00		ug/L	04/22/10 23:35		1
1,3,5-Trimethylbenzene	108 - 67-8	BRL	5.00		ug/L	04/22/10 23:35		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 23:35		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 23:35		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 23:35		1
Total Xylenes	1330-20-7	BRL	5.00	~	ug/L	04/22/10 23:35		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-24

Matrix: Water

% Moisture:

Lab Sample Id: 369409-016

Date Collected: Apr-15-10 09:40

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-22-10 19:20

Tech: CYE

Seq Number: 803828										
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date Flag	Dil			
Benzene	71-43-2	BRL	5.00		ug/L	04/22/10 23:57	1			
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/22/10 23:57	1			
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/22/10 23:57	1			
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/22/10 23:57	1			
Bromoform	75-25-2	BRL	5.00		ug/L	04/22/10 23:57	1			
Bromomethane	74-83-9	BRL	5.00		ug/L	04/22/10 23:57	1			
MTBE	1634-04-4	6.63	5.00		ug/L	04/22/10 23:57	1			
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/22/10 23:57	1			
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/22/10 23:57	1			
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/22/10 23:57	1			
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/22/10 23:57	1			
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/22/10 23:57	1			
Chloroethane	75-00-3	BRL	10.0		ug/L	04/22/10 23:57	1			
Chloroform	67-66-3	BRL	5.00		ug/L	04/22/10 23:57	1			
Chloromethane	74-87 - 3	BRL	10.0		ug/L	04/22/10 23:57	1			
2-Chlorotoluene	95-49 - 8	BRL	5.00		ug/L	04/22/10 23:57	1			
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/22/10 23:57	1			
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/22/10 23:57	1			
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/22/10 23:57	1			
1,2-Dibromo-3-Chloropropane	96-12 - 8	BRL	5.00		ug/L	04/22/10 23:57	1			
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/22/10 23:57	1			
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/22/10 23:57	1			
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/22/10 23:57	1			
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/22/10 23:57	1			
Dichlorodifluoromethane	75-71 - 8	BRL	5.00		ug/L	04/22/10 23:57	1			
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/22/10 23:57	1			
1,2-Dichloroethane	107-06-2	BRL	5.00		· ug/L	04/22/10 23:57	1			
1,1-Dichloroethene	75-35 - 4	BRL	5.00		ug/L	04/22/10 23:57	1			
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/22/10 23:57	1			
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/22/10 23:57	1			
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/22/10 23:57	1			
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/22/10 23:57	1			
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/22/10 23:57	1			
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/22/10 23:57	1			
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/22/10 23:57	1			
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/22/10 23:57	1			
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/22/10 23:57	1			
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/22/10 23:57	1			
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/22/10 23:57	1			





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-24 Matrix: Water

Lab Sample Id: 369409-016 Date Collected: Apr-15-10 09:40 Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

> Analyst: CYE Date Prep: Apr-22-10 19:20 Tech: CYF

% Moisture:

	Seq Number: 803	Date Prep:	Apr-22-1	0 19:20	Tech: CYE			
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date F	lag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/22/10 23:57		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/22/10 23:57		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/22/10 23:57		1
Styrene	100-42-5	BRL	5.00		ug/L	04/22/10 23:57		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/22/10 23:57		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/22/10 23:57		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/22/10 23:57		1
Toluene	108-88-3	BRL	5.00		ug/L	04/22/10 23:57		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/22/10 23:57		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/22/10 23:57		1
1,1,1-Trichloroethane	71-55 - 6	BRL	5.00		ug/L	04/22/10 23:57		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/22/10 23:57		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/22/10 23:57		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/22/10 23:57		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/22/10 23:57		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/22/10 23:57		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/22/10 23:57		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/22/10 23:57		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/22/10 23:57		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/22/10 23:57		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/22/10 23:57		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-43 Matrix: Water % Moisture:

Lab Sample Id: 369409-017 Date Collected: Apr-15-10 09:50 Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

	Analyst: CY	E	Date Prep:	Apr-23-1	0 15:48	Tech:	CYE	
	Seq Number: 8040		•	•				
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/23/10 17:23		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/23/10 17:23		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/23/10 17:23		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/23/10 17:23		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/23/10 17:23		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/23/10 17:23		1
MTBE	1634-04-4	17.5	5.00		ug/L	04/23/10 17:23		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/23/10 17:23		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/23/10 17:23		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/23/10 17:23		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/23/10 17:23		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/23/10 17:23		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/23/10 17:23		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/23/10 17:23		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/23/10 17:23		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/23/10 17:23		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/23/10 17:23		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/23/10 17:23		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/23/10 17:23		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/23/10 17:23		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/23/10 17:23		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/23/10 17:23		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/23/10 17:23		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/23/10 17:23		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/23/10 17:23		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/23/10 17:23		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/23/10 17:23		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/23/10 17:23		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/23/10 17:23		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/23/10 17:23		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/23/10 17:23		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/23/10 17:23		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/23/10 17:23		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/23/10 17:23		î
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/23/10 17:23		î
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L ug/L	04/23/10 17:23		î
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/23/10 17:23		î
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/23/10 17:23		î
isopropylbenzene	98-82-8	BRL	5.00		ug/L ug/L	04/23/10 17:23		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-43

Matrix: Water

% Moisture:

Lab Sample Id: 369409-017

Date Collected: Apr-15-10 09:50

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

04/23/10 17:23

ug/L

	Analyst: CY Seq Number: 804		Date Prep:	Apr-23-1	0 15:48	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 17:23		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/23/10 17:23		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/23/10 17:23		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 17:23		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 17:23		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/23/10 17:23		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 17:23		1
Toluene	108-88-3	BRL	5.00		ug/L	04/23/10 17:23		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/23/10 17:23		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 17:23		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 17:23		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 17:23		1
Trichloroethene	79-01 - 6	BRL	5.00		ug/L	04/23/10 17:23		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/23/10 17:23	•	1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/23/10 17:23		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/23/10 17:23		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/23/10 17:23		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/23/10 17:23		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/23/10 17:23		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/23/10 17:23		1

BRL

5.00

1330-20-7

Project: Standard List of Methods

Total Xylenes





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-42

Matrix: Water

% Moisture:

Lab Sample Id: 369409-018

Date Collected: Apr-15-10 10:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:46

Tech: CYE

	Seq Number: 804	067		1.12. 20 10 10110	reem. C	, D
Parameter	Cas Number	Result	PQL	MDL Units	Analysis Date Fla	ıg Dil
Benzene	71-43-2	BRL	5.00	ug/L	04/23/10 20:20	1
Bromobenzene	108-86-1	BRL	5.00	ug/L	04/23/10 20:20	1
Bromochloromethane	74-97 - 5	BRL	5.00	ug/L	04/23/10 20:20	1
Bromodichloromethane	75-27-4	BRL	5.00	ug/L	04/23/10 20:20	1
Bromoform	75-25-2	BRL	5.00	ug/L	04/23/10 20:20	1
Bromomethane	74-83-9	BRL	5.00	ug/L	04/23/10 20:20	1
MTBE	1634-04-4	BRL	5.00	ug/L	04/23/10 20:20	1
n-Butylbenzene	104-51-8	BRL	5.00	ug/L	04/23/10 20:20	1
Sec-Butylbenzene	135-98 - 8	BRL	5.00	ug/L	04/23/10 20:20	1
tert-Butylbenzene	98-06-6	BRL	5.00	ug/L	04/23/10 20:20	1
Carbon Tetrachloride	56-23-5	BRL	5.00	ug/L	04/23/10 20:20	1
Chlorobenzene	108-90-7	BRL	5.00	ug/L	04/23/10 20:20	1
Chloroethane	75-00 - 3	BRL	10.0	ug/L	04/23/10 20:20	1
Chloroform	67-66-3	BRL	5.00	ug/L	04/23/10 20:20	1
Chloromethane	74-87-3	BRL	10.0	ug/L	04/23/10 20:20	1
2-Chlorotoluene	95-49-8	BRL	5.00	ug/L	04/23/10 20:20	1
4-Chlorotoluene	106-43-4	BRL	5.00	ug/L	04/23/10 20:20	1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00	· ug/L	04/23/10 20:20	1
Dibromochloromethane	124-48-1	BRL	5.00	ug/L	04/23/10 20:20	1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00	ug/L	04/23/10 20:20	1
Dibromomethane	74-95-3	BRL	5.00	ug/L	04/23/10 20:20	1
1,2-Dichlorobenzene	95 - 50-1	BRL	5.00	ug/L	04/23/10 20:20	1
1,3-Dichlorobenzene	541 - 73-1	BRL	5.00	ug/L	04/23/10 20:20	1
1,4-Dichlorobenzene	106-46-7	BRL	5.00	ug/L	04/23/10 20:20	1
Dichlorodifluoromethane	75-71-8	BRL	5.00	ug/L	04/23/10 20:20	1
1,1-Dichloroethane	75-34-3	BRL	5.00	ug/L	04/23/10 20:20	1
1,2-Dichloroethane	107-06-2	BRL	5.00	ug/L	04/23/10 20:20	1
1,1-Dichloroethene	75-35-4	BRL	5.00	ug/L	04/23/10 20:20	1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00	ug/L	04/23/10 20:20	1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ug/L	04/23/10 20:20	1
1,2-Dichloropropane	78-87 - 5	BRL	5.00	ug/L	04/23/10 20:20	1
1,3-Dichloropropane	142-28-9	BRL	5.00	ug/L	04/23/10 20:20	1
2,2-Dichloropropane	594-20-7	BRL	5.00	ug/L	04/23/10 20:20	1
1,1-Dichloropropene	563-58-6	BRL	5.00	ug/L	04/23/10 20:20	1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00	ug/L	04/23/10 20:20	1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00	ug/L	04/23/10 20:20	1
Ethylbenzene	100-41-4	BRL	5.00	ug/L	04/23/10 20:20	1
Hexachlorobutadiene	87-68-3	BRL	5.00	ug/L	04/23/10 20:20	1
isopropylbenzene	98-82-8	BRL	5.00	ug/L	04/23/10 20:20	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-42

Matrix: Water

% Moisture:

Lab Sample Id: 369409-018

Date Collected: Apr-15-10 10:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:46

Tech: CYE

	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 20:20		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/23/10 20:20		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/23/10 20:20		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 20:20		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 20:20		1
1,1,2,2-Tetrachloroethane	79-34 - 5	BRL	5.00		ug/L	04/23/10 20:20		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 20:20		1
Toluene	108-88-3	BRL	5.00		ug/L	04/23/10 20:20		1
1,2,3-Trichlorobenzene	87-61 - 6	BRL	5.00		ug/L	04/23/10 20:20		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 20:20		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 20:20		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 20:20		1
Trichloroethene	79-01 - 6	BRL	5.00		ug/L	04/23/10 20:20		1
Trichlorofluoromethane '	75-69-4	BRL	5.00		ug/L	04/23/10 20:20		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/23/10 20:20		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/23/10 20:20		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/23/10 20:20		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/23/10 20:20		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/23/10 20:20		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/23/10 20:20		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/23/10 20:20		1



Lab Sample Id: 369409-019

Certificate of Analytical Results 369409



Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Matrix: Water Sample Id: MW-44

Date Collected: Apr-15-10 10:10

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

Analyst: CYF

% Moisture:

	Analyst: CY	E	Date Prep:	Apr-23-1	0 18:48	Tech:	CYE	
	Seq Number: 804067							
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/23/10 20:42		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/23/10 20:42		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/23/10 20:42		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/23/10 20:42		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/23/10 20:42		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/23/10 20:42		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/23/10 20:42		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/23/10 20:42		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/23/10 20:42		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/23/10 20:42		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/23/10 20:42		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/23/10 20:42		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/23/10 20:42		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/23/10 20:42		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/23/10 20:42		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/23/10 20:42		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/23/10 20:42		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/23/10 20:42		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/23/10 20:42		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/23/10 20:42		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/23/10 20:42		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/23/10 20:42		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/23/10 20:42		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/23/10 20:42		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/23/10 20:42	•	1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/23/10 20:42		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/23/10 20:42		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/23/10 20:42		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/23/10 20:42		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/23/10 20:42		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/23/10 20:42		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/23/10 20:42		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/23/10 20:42		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/23/10 20:42		î
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/23/10 20:42		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/23/10 20:42		î
Ethylbenzene	100-41-4	BRL	5.00		ug/L ug/L	04/23/10 20:42		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L ug/L	04/23/10 20:42		1
isopropylbenzene	98-82-8	BRL	5.00		ug/L ug/L	04/23/10 20:42		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-44

Matrix: Water

% Moisture:

Lab Sample Id: 369409-019

Date Collected: Apr-15-10 10:10

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:48

Tech: CYE

	Seq Number: 804	067	•	*				
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date F	lag I)il
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 20:42		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/23/10 20:42		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/23/10 20:42		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 20:42		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 20:42		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/23/10 20:42		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 20:42		1
Toluene	108-88-3	BRL	5.00		ug/L	04/23/10 20:42		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/23/10 20:42		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 20:42		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 20:42		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 20:42		1
Trichloroethene	79-01 - 6	BRL	5.00		ug/L	04/23/10 20:42		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/23/10 20:42		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/23/10 20:42		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/23/10 20:42		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/23/10 20:42		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/23/10 20:42		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/23/10 20:42		1
Vinyl Chloride	75-01 - 4	BRL	2.00		ug/L	04/23/10 20:42		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/23/10 20:42		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-30

Matrix: Water

% Moisture:

Lab Sample Id: 369409-020

Date Collected: Apr-15-10 10:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:50

Tech: CYE

Parameter						
r at afficter	Cas Number	Result	PQL	MDL Units	Analysis Date Fla	g Dil
Benzene	71-43-2	BRL	5.00	ug/L	04/23/10 21:04	1
Bromobenzene	108-86-1	BRL	5.00	ug/L	04/23/10 21:04	1
Bromochloromethane	74 - 97-5	BRL	5.00	ug/L	04/23/10 21:04	1
Bromodichloromethane	75-27-4	BRL	5.00	ug/L	04/23/10 21:04	1
Bromoform	75-25-2	BRL	5.00	ug/L	04/23/10 21:04	1
Bromomethane	74-83-9	BRL	5.00	ug/L	04/23/10 21:04	1
MTBE	1634-04-4	BRL	5.00	ug/L	04/23/10 21:04	1
n-Butylbenzene	104-51-8	BRL	5.00	ug/L	04/23/10 21:04	1
Sec-Butylbenzene	135-98-8	BRL	5.00	ug/L	04/23/10 21:04	1
tert-Butylbenzene	98-06-6	BRL	5.00	ug/L	04/23/10 21:04	1
Carbon Tetrachloride	56-23-5	BRL	5.00	ug/L	04/23/10 21:04	1
Chlorobenzene	108-90-7	BRL	5.00	ug/L	04/23/10 21:04	1
Chloroethane	75-00-3	BRL	10.0	ug/L	04/23/10 21:04	1
Chloroform	67-66-3	BRL	5.00	ug/L	04/23/10 21:04	1
Chloromethane	74-87-3	BRL	10.0	ug/L	04/23/10 21:04	1
2-Chlorotoluene	95-49-8	BRL	5.00	ug/L	04/23/10 21:04	1
4-Chlorotoluene	106-43-4	BRL	5.00	ug/L	04/23/10 21:04	1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00	ug/L	04/23/10 21:04	1
Dibromochloromethane	124-48-1	BRL	5.00	ug/L	04/23/10 21:04	1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00	ug/L	04/23/10 21:04	1
Dibromomethane	74-95-3	BRL	5.00	ug/L	04/23/10 21:04	1
1,2-Dichlorobenzene	95-50-1	BRL	5.00	ug/L	04/23/10 21:04	1
1,3-Dichlorobenzene	541-73-1	BRL	5.00	ug/L	04/23/10 21:04	1
1,4-Dichlorobenzene	106-46-7	BRL	5.00	ug/L	04/23/10 21:04	1
Dichlorodifluoromethane	75-71-8	BRL	5.00	ug/L	04/23/10 21:04	1
1,1-Dichloroethane	75-34-3	BRL	5.00	ug/L	04/23/10 21:04	î
1,2-Dichloroethane	107-06-2	BRL	5.00	ug/L	04/23/10 21:04	1
1,1-Dichloroethene	75-35-4	BRL	5.00	ug/L	04/23/10 21:04	1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00	ug/L	04/23/10 21:04	1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ug/L	04/23/10 21:04	1
1,2-Dichloropropane	78-87-5	BRL	5.00	ug/L	04/23/10 21:04	1
1,3-Dichloropropane	142-28-9	BRL	5.00	ug/L	04/23/10 21:04	1
2,2-Dichloropropane	594-20-7	BRL	5.00	ug/L	04/23/10 21:04	1
1,1-Dichloropropene	563-58-6	BRL	5.00	ug/L	04/23/10 21:04	1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00	ug/L ug/L	04/23/10 21:04	1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00	ug/L ug/L	04/23/10 21:04	1
Ethylbenzene	100-41-4	BRL	5.00	ug/L ug/L	04/23/10 21:04	1
Hexachlorobutadiene	87-68-3	BRL	5.00	ug/L	04/23/10 21:04	1
isopropylbenzene	98-82-8	BRL	5.00	ug/L ug/L	04/23/10 21:04	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-30

Matrix: Water

% Moisture:

Lab Sample Id: 369409-020

Date Collected: Apr-15-10 10:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

	Analyst: CYI Seq Number: 804		Date Prep:	Apr-23-1	0 18:50	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 21:04		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/23/10 21:04		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/23/10 21:04		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 21:04		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 21:04		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/23/10 21:04		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 21:04		1
Toluene	108-88-3	BRL	5.00		ug/L	04/23/10 21:04		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/23/10 21:04		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 21:04		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 21:04		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 21:04		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/23/10 21:04		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/23/10 21:04		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/23/10 21:04		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/23/10 21:04		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/23/10 21:04		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/23/10 21:04		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/23/10 21:04		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/23/10 21:04		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/23/10 21:04		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-25

Matrix: Water

% Moisture:

Lab Sample Id: 369409-021

Date Collected: Apr-15-10 10:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

	Analyst: CY	E	Date Prep:	Apr-23-1	0 18:52	Tech:	CYE	
	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/23/10 21:26		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/23/10 21:26		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/23/10 21:26		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/23/10 21:26		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/23/10 21:26		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/23/10 21:26		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/23/10 21:26		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/23/10 21:26		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/23/10 21:26		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/23/10 21:26		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/23/10 21:26		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/23/10 21:26		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/23/10 21:26		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/23/10 21:26		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/23/10 21:26		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/23/10 21:26		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/23/10 21:26		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/23/10 21:26		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/23/10 21:26		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/23/10 21:26		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/23/10 21:26		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/23/10 21:26		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/23/10 21:26		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/23/10 21:26		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/23/10 21:26		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/23/10 21:26		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/23/10 21:26		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/23/10 21:26		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/23/10 21:26		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/23/10 21:26		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/23/10 21:26		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/23/10 21:26		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/23/10 21:26		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/23/10 21:26		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/23/10 21:26		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/23/10 21:26		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/23/10 21:26		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/23/10 21:26		1
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/23/10 21:26		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-25

Matrix: Water

% Moisture:

Lab Sample Id: 369409-021

Date Collected: Apr-15-10 10:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:52

Tech: CYE

,	Seq Number: 804	067				2 2 2 2 2 2	012	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 21:26		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/23/10 21:26		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/23/10 21:26		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 21:26		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 21:26		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/23/10 21:26		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 21:26		1
Toluene	108-88-3	BRL	5.00		ug/L	04/23/10 21:26		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/23/10 21:26		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 21:26		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 21:26		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 21:26		1
Trichloroethene	79-01 - 6	BRL	5.00		ug/L	04/23/10 21:26		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/23/10 21:26		1
1,2,3-Trichloropropane	96-18-4	\mathtt{BRL}	5.00		ug/L	04/23/10 21:26		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/23/10 21:26		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/23/10 21:26		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/23/10 21:26		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/23/10 21:26		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/23/10 21:26		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/23/10 21:26		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: TRW-2

Matrix: Water

% Moisture:

Lab Sample Id: 369409-022

Date Collected: Apr-15-10 10:40
Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:54

	Analyst: CY		Date Prep:	Apr-23-1	0 18:54	Tech:	CYE	
	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/23/10 21:48		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/23/10 21:48		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/23/10 21:48		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/23/10 21:48		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/23/10 21:48		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/23/10 21:48		1
MTBE	1634 - 04-4	BRL	5.00		ug/L	04/23/10 21:48		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/23/10 21:48		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/23/10 21:48		1
tert-Butylbenzene	98-06 - 6	BRL	5.00		ug/L	04/23/10 21:48		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/23/10 21:48		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/23/10 21:48		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/23/10 21:48		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/23/10 21:48		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/23/10 21:48		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/23/10 21:48		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/23/10 21:48		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/23/10 21:48		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/23/10 21:48		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/23/10 21:48		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/23/10 21:48		1
1,2-Dichlorobenzene	95 - 50-1	BRL	5.00		ug/L	04/23/10 21:48		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/23/10 21:48		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/23/10 21:48		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/23/10 21:48		1
1,1-Dichloroethane	75 - 34-3	BRL	5.00		ug/L	04/23/10 21:48		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/23/10 21:48		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/23/10 21:48		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/23/10 21:48		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/23/10 21:48		1
1,2-Dichloropropane	78 - 87-5	BRL	5.00		ug/L	04/23/10 21:48		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/23/10 21:48		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/23/10 21:48		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/23/10 21:48		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/23/10 21:48		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/23/10 21:48		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/23/10 21:48		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/23/10 21:48		1
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/23/10 21:48		î





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: TRW-2

Matrix: Water

% Moisture:

Lab Sample Id: 369409-022

Date Collected: Apr-15-10 10:40

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:54

Tech: CYE

	Analyst: CY. Seq Number: 804		Date Prep:	Apr-23-1	0 18:54	Tech: (CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date I	lag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 21:48		1
Naphthalene	91-20-3	BRL	10,0		ug/L	04/23/10 21:48		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/23/10 21:48		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 21:48		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 21:48		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/23/10 21:48		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 21:48		1
Toluene	108-88-3	BRL	5.00		ug/L	04/23/10 21:48		1
1,2,3-Trichlorobenzene	87-61 - 6	BRL	5.00		ug/L	04/23/10 21:48		I
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 21:48		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 21:48		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 21:48		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/23/10 21:48		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/23/10 21:48		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/23/10 21:48		1
1,2,4-Trimethylbenzene	95-63 - 6	BRL	5.00		ug/L	04/23/10 21:48		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/23/10 21:48		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/23/10 21:48		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/23/10 21:48		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/23/10 21:48		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/23/10 21:48		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-20

Matrix: Water

% Moisture:

Lab Sample Id: 369409-023

Date Collected: Apr-15-10 10:50

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 18:56

Tech: CYE

	Seq Number: 804		Date Prep:	Apr-23-1	0 18:56	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	497	25.0		ug/L	04/23/10 22:32	D	5
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/23/10 22:09		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/23/10 22:09		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/23/10 22:09		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/23/10 22:09		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/23/10 22:09		1
MTBE	1634-04-4	145	5.00		ug/L	04/23/10 22:09		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/23/10 22:09		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/23/10 22:09		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/23/10 22:09		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/23/10 22:09		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/23/10 22:09		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/23/10 22:09		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/23/10 22:09		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/23/10 22:09		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/23/10 22:09		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/23/10 22:09		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/23/10 22:09		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/23/10 22:09		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/23/10 22:09		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/23/10 22:09		1
1,2-Dichlorobenzene	95 - 50-1	BRL	5.00		ug/L	04/23/10 22:09		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/23/10 22:09		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/23/10 22:09		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/23/10 22:09		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/23/10 22:09		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/23/10 22:09		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/23/10 22:09		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/23/10 22:09		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/23/10 22:09		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/23/10 22:09		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/23/10 22:09		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/23/10 22:09		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/23/10 22:09		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/23/10 22:09		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/23/10 22:09		1
Ethylbenzene	100-41-4	20.4	5.00		ug/L	04/23/10 22:09		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/23/10 22:09		1
isopropylbenzene	98-82-8	12.7	5.00		ug/L ug/L	04/23/10 22:09		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-20

Matrix: Water

% Moisture:

Lab Sample Id: 369409-023

Date Collected: Apr-15-10 10:50

Date Received: Apr-16-10 09:00

Date Prep: Apr-23-10 18:56

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Tech: CYE

	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 22:09		1
Naphthalene	91-20-3	31.5	10.0		ug/L	04/23/10 22:09		1
n-Propylbenzene	103-65-1	14.4	5.00		ug/L	04/23/10 22:09		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 22:09		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 22:09		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/23/10 22:09		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 22:09		1
Toluene	108-88-3	43.2	5.00		ug/L	04/23/10 22:09		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/23/10 22:09		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 22:09		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 22:09		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 22:09		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/23/10 22:09		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/23/10 22:09		1
1,2,3-Trichloropropane	96-18-4	\mathtt{BRL}	5.00		ug/L	04/23/10 22:09		1
1,2,4-Trimethylbenzene	95-63-6	18.0	5.00		ug/L	04/23/10 22:09		1
1,3,5-Trimethylbenzene	108-67-8	11.4	5.00		ug/L	04/23/10 22:09		1
o-Xylene	95-47-6	28.4	5.00		ug/L	04/23/10 22:09		1
m,p-Xylenes	179601-23-1	56.5	10.0		ug/L	04/23/10 22:09		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/23/10 22:09		1
Total Xylenes	1330-20-7	84.9	5.00		ug/L	04/23/10 22:09		. 1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-15

Matrix: Water

% Moisture:

Lab Sample Id: 369409-024

Date Collected: Apr-15-10 11:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:00

Tech: CYE

	Seq Number: 804		Date Frep.	Apr-23-10	12.00	lecn:	CIE	
	Seq Number, 804							
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	839	100		ug/L	04/28/10 15:08	D	20
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/23/10 22:54		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/23/10 22:54		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/23/10 22:54		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/23/10 22:54		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/23/10 22:54		1
MTBE	1634-04-4	38.8	5.00		ug/L	04/23/10 22:54		1
n-Butylbenzene	104-51-8	36.3	5.00		ug/L	04/23/10 22:54		1
Sec-Butylbenzene	135-98-8	23.4	5.00		ug/L	04/23/10 22:54		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/23/10 22:54		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/23/10 22:54		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/23/10 22:54		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/23/10 22:54		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/23/10 22:54		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/23/10 22:54		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/23/10 22:54		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/23/10 22:54		1
p-Cymene (p-Isopropyltoluene)	99-87-6	6.37	5.00		ug/L	04/23/10 22:54		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/23/10 22:54		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/23/10 22:54		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/23/10 22:54		I
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/23/10 22:54		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/23/10 22:54		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/23/10 22:54		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/23/10 22:54		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/23/10 22:54		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/23/10 22:54		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/23/10 22:54		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/23/10 22:54		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/23/10 22:54		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/23/10 22:54		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/23/10 22:54		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/23/10 22:54		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/23/10 22:54		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/23/10 22:54		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/23/10 22:54		1
Ethylbenzene	100-41-4	556	25.0		ug/L	04/26/10 16:56	D	5
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/23/10 22:54		1
isopropylbenzene	98-82-8	120	5.00		ug/L	04/23/10 22:54		1



Lab Sample Id: 369409-024

Certificate of Analytical Results 369409



% Moisture:

Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-15 Matrix: Water

1330-20-7

Date Collected: Apr-15-10 11:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B Analyst: CYE Date Prep: Apr-23-10 19:00 Tech: CYE Seq Number: 804067 **Parameter** Units Analysis Date Flag Dil Cas Number Result **PQL** MDL Methylene Chloride 75-09-2 BRL 5.00 ug/L 04/23/10 22:54 1 91-20-3 04/23/10 22:54 Naphthalene 101 10.0 ug/L 1 n-Propylbenzene 103-65-1 173 25.0 04/26/10 16:56 5 ug/L Styrene 100-42-5 BRL 5.00 ug/L 04/23/10 22:54 1 1,1,1,2-Tetrachloroethane 630-20-6 BRL 5.00 ug/L 04/23/10 22:54 1 1,1,2,2-Tetrachloroethane 04/23/10 22:54 79-34-5 BRL 5.00 ug/L 1 Tetrachloroethylene 127-18-4 BRL 5.00 ug/L 04/23/10 22:54 1 Toluene 108-88-3 4350 250 ug/L 04/28/10 15:30 50 1,2,3-Trichlorobenzene 87-61-6 **BRL** 5.00 ug/L 04/23/10 22:54 1 1,2,4-Trichlorobenzene 120-82-1 BRL 5.00 ug/L 04/23/10 22:54 1 1,1,1-Trichloroethane 04/23/10 22:54 1 71-55-6 BRL 5.00 ug/L 1,1,2-Trichloroethane 04/23/10 22:54 1 79-00-5 BRL 5.00 ug/L Trichloroethene 79-01-6 BRL 5.00 04/23/10 22:54 1 ug/L Trichlorofluoromethane 04/23/10 22:54 1 75-69-4 BRL 5.00 ug/L 1,2,3-Trichloropropane 96-18-4 BRL 5.00 04/23/10 22:54 1 ug/L 1,2,4-Trimethylbenzene 95-63-6 532 100 ug/L 04/28/10 15:08 D 20 1,3,5-Trimethylbenzene 5.00 108-67-8 111 ug/L 04/23/10 22:54 1 o-Xylene 95-47-6 705 100 D 20 04/28/10 15:08 ug/L m,p-Xylenes 179601-23-1 1730 200 04/28/10 15:08 20 D ug/L Vinyl Chloride 75-01-4 BRL 2.00 04/23/10 22:54 1 ug/L

3521

250

ug/L

04/28/10 15:08

Project: Standard List of Methods

Total Xylenes

20





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-16

Matrix: Water

% Moisture:

Lab Sample Id: 369409-025

Date Collected: Apr-15-10 11:10

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 12:02

Tech: CYE

	Seq Number: 804		Date Trep.	Apr-20-10	7 12.02	recn. (CIL	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date I	Flag	Dil
Benzene	71-43-2	37.6	5.00		ug/L	04/26/10 13:11		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/26/10 13:11		. 1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/26/10 13:11		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/26/10 13:11		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/26/10 13:11		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/26/10 13:11		1
MTBE	1634-04-4	14.6	5.00		ug/L	04/26/10 13:11		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/26/10 13:11		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/26/10 13:11		1
tert-Butylbenzene	98 - 06-6	BRL	5.00		ug/L	04/26/10 13:11		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/26/10 13:11		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/26/10 13:11		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/26/10 13:11		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/26/10 13:11		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/26/10 13:11		1
2-Chlorotoluene	95-49 - 8	BRL	5.00		ug/L	04/26/10 13:11		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/26/10 13:11		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/26/10 13:11		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/26/10 13:11		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/26/10 13:11		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/26/10 13:11		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/26/10 13:11		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/26/10 13:11		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/26/10 13:11		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/26/10 13:11		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/26/10 13:11		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/26/10 13:11		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/26/10 13:11		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/26/10 13:11		1
trans-1,2-dichloroethene	156-60 - 5	BRL	5.00		ug/L	04/26/10 13:11		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/26/10 13:11		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/26/10 13:11		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/26/10 13:11		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/26/10 13:11		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/26/10 13:11		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/26/10 13:11	*	1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/26/10 13:11		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/26/10 13:11		1
isopropylbenzene	98-82-8	53.4	5.00		ug/L	04/26/10 13:11		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-16

Matrix: Water

% Moisture:

Lab Sample Id: 369409-025

Date Collected: Apr-15-10 11:10

Date Received: Apr-16-10 09:00

Date Prep: Apr-26-10 12:02

Analytical Method: VOAs by SW-846 8260 Prep

Prep Method: SW5030B

Tech: CYE

Analyst: CYE Seq Number: 804058

	Seq Number: 804	058					
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date Fla	ıg Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/26/10 13:11	1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/26/10 13:11	I
n-Propylbenzene	103-65-1	51.3	5.00		ug/L	04/26/10 13:11	1
Styrene	100-42-5	BRL	5.00		ug/L	04/26/10 13:11	1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/26/10 13:11	1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/26/10 13:11	1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/26/10 13:11	1
Toluene	108-88-3	BRL	5.00		ug/L	04/26/10 13:11	1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/26/10 13:11	1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/26/10 13:11	1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/26/10 13:11	1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/26/10 13:11	1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/26/10 13:11	1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/26/10 13:11	1
1,2,3-Trichloropropane	96-18-4	\mathtt{BRL}	5.00		ug/L	04/26/10 13:11	1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/26/10 13:11	1
1,3,5-Trimethylbenzene	108-67-8	51.6	5.00		ug/L	04/26/10 13:11	1
o-Xylene	95-47-6	5.22	5.00		ug/L	04/26/10 13:11	1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/26/10 13:11	1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/26/10 13:11	1
Total Xylenes	1330-20-7	5.22	5.00		ug/L	04/26/10 13:11	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-17

Matrix: Water

% Moisture:

Lab Sample Id: 369409-026

Date Collected: **Apr-15-10 11:20**

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

	Analyst: CYl Seq Number: 804		Date Prep:	Apr-23-1	0 19:04	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00	1,1213	ug/L	04/23/10 23:38	_	1
Bromobenzene	108-86-1	BRL	5.00		ug/L ug/L	04/23/10 23:38		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L ug/L	04/23/10 23:38		î
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/23/10 23:38		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/23/10 23:38		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/23/10 23:38		1
MTBE	1634-04-4	5.10	5.00		ug/L	04/23/10 23:38		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/23/10 23:38		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/23/10 23:38		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/23/10 23:38		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/23/10 23:38		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/23/10 23:38		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/23/10 23:38		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/23/10 23:38		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/23/10 23:38		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/23/10 23:38		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/23/10 23:38		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/23/10 23:38		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/23/10 23:38		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/23/10 23:38		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/23/10 23:38		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/23/10 23:38		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/23/10 23:38		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/23/10 23:38		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/23/10 23:38		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/23/10 23:38		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/23/10 23:38		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/23/10 23:38		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/23/10 23:38		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/23/10 23:38		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/23/10 23:38		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/23/10 23:38		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/23/10 23:38		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/23/10 23:38		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/23/10 23:38		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/23/10 23:38		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/23/10 23:38		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/23/10 23:38		1
isopropylbenzene	98-82-8	18.0	5.00		ug/L	04/23/10 23:38		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-17

Matrix: Water

% Moisture:

Lab Sample Id: 369409-026

Date Collected: Apr-15-10 11:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:04

Tech: CYE

	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/23/10 23:38		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/23/10 23:38		1
n-Propylbenzene	103-65-1	12.9	5.00		ug/L	04/23/10 23:38		1
Styrene	100-42-5	BRL	5.00		ug/L	04/23/10 23:38		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/23/10 23:38		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/23/10 23:38		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/23/10 23:38		1
Toluene	108-88-3	BRL	5.00		ug/L	04/23/10 23:38		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/23/10 23:38		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/23/10 23:38		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/23/10 23:38		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/23/10 23:38		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/23/10 23:38		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/23/10 23:38		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/23/10 23:38		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/23/10 23:38		1
1,3,5-Trimethylbenzene	108-67-8	17.3	5.00		ug/L	04/23/10 23:38		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/23/10 23:38		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/23/10 23:38		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/23/10 23:38		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/23/10 23:38		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-19

Matrix: Water

% Moisture:

Lab Sample Id: 369409-027

Date Collected: Apr-15-10 11:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

	Analyst: CY		Date Prep:	Apr-23-1	0 19:06	Tech:	CYE	
	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	11.2	5.00		ug/L	04/24/10 00:00		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/24/10 00:00		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/24/10 00:00		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/24/10 00:00		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/24/10 00:00		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/24/10 00:00		1
MTBE	1634-04-4	5.59	5.00		ug/L	04/24/10 00:00		1
n-Butylbenzene	104-51-8	5.17	5.00		ug/L	04/24/10 00:00		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/24/10 00:00		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/24/10 00:00		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/24/10 00:00		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/24/10 00:00		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/24/10 00:00		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/24/10 00:00		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/24/10 00:00		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/24/10 00:00		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/24/10 00:00		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/24/10 00:00		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/24/10 00:00		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/24/10 00:00		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/24/10 00:00		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/24/10 00:00		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/24/10 00:00		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/24/10 00:00		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/24/10 00:00		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/24/10 00:00		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/24/10 00:00		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/24/10 00:00		1
cis-1,2-Dichloroethene	156 - 59-2	BRL	5.00		ug/L	04/24/10 00:00		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/24/10 00:00		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/24/10 00:00		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/24/10 00:00		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/24/10 00:00		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/24/10 00:00		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/24/10 00:00		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/24/10 00:00		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/24/10 00:00		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/24/10 00:00		î
isopropylbenzene	98-82-8	51.8	5.00		ug/L ug/L	04/24/10 00:00		1

Project: Standard List of Methods

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-19

Matrix: Water

% Moisture:

Lab Sample Id: 369409-027

Date Collected: Apr-15-10 11:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:06

Tech: CYE

	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/24/10 00:00		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/24/10 00:00		1
n-Propylbenzene	103-65-1	51.6	5.00		ug/L	04/24/10 00:00		1
Styrene	100-42-5	BRL	5.00		ug/L	04/24/10 00:00		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/24/10 00:00		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/24/10 00:00		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/24/10 00:00		1
Toluene	108-88-3	6.34	5.00		ug/L	04/24/10 00:00		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/24/10 00:00		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/24/10 00:00		1
1,1,1-Trichloroethane	71-55-6	BRL	*5.00		ug/L	04/24/10 00:00		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/24/10 00:00		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/24/10 00:00		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/24/10 00:00		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/24/10 00:00		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/24/10 00:00		1
1,3,5-Trimethylbenzene	108-67-8	50.9	5.00		ug/L	04/24/10 00:00		1
o-Xylene	95-47-6	23.9	5.00		ug/L	04/24/10 00:00		1
m,p-Xylenes	179601-23-1	21.0	10.0		ug/L	04/24/10 00:00		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/24/10 00:00		1
Total Xylenes	1330-20-7	44.9	5.00		ug/L	04/24/10 00:00		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Matrix: Water % Moisture: Sample Id: MW-32

Lab Sample Id: 369409-028 Date Collected: Apr-15-10 11:40 Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

> Analyst: CVF Date Pren: Apr-23-10 10:08

	Analyst: CY	E	Date Prep:	Apr-23-1	0 19:08	Tech:	CYE	
	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/24/10 00:22		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/24/10 00:22		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/24/10 00:22		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/24/10 00:22		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/24/10 00:22		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/24/10 00:22		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/24/10 00:22		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/24/10 00:22		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/24/10 00:22		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/24/10 00:22		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/24/10 00:22		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/24/10 00:22		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/24/10 00:22		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/24/10 00:22		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/24/10 00:22		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/24/10 00:22		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/24/10 00:22		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/24/10 00:22		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/24/10 00:22		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/24/10 00:22		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/24/10 00:22		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/24/10 00:22		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/24/10 00:22		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/24/10 00:22		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/24/10 00:22		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/24/10 00:22		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/24/10 00:22		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/24/10 00:22		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/24/10 00:22		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/24/10 00:22		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/24/10 00:22		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/24/10 00:22		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/24/10 00:22		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/24/10 00:22		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/24/10 00:22		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/24/10 00:22		î
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/24/10 00:22		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/24/10 00:22		1
isopropylbenzene	98-82-8	6.79	5.00		ug/L ug/L	04/24/10 00:22		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-32

Matrix: Water

% Moisture:

Lab Sample Id: 369409-028

Date Collected: Apr-15-10 11:40

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:08

Tech: CYE

	Seq Number: 804	067	•	•				
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/24/10 00:22		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/24/10 00:22		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/24/10 00:22		1
Styrene	100-42-5	BRL	5.00		ug/L	04/24/10 00:22		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/24/10 00:22		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/24/10 00:22		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/24/10 00:22		1
Toluene	108-88-3	BRL	5.00		ug/L	04/24/10 00:22		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/24/10 00:22		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/24/10 00:22		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/24/10 00:22		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/24/10 00:22		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/24/10 00:22		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/24/10 00:22		1
1,2,3-Trichloropropane	96-18-4	\mathtt{BRL}	5.00		ug/L	04/24/10 00:22		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/24/10 00:22		1
1,3,5-Trimethylbenzene	108-67-8	6.55	5.00		ug/L	04/24/10 00:22		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/24/10 00:22		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/24/10 00:22		1
Vinyl Chloride	75-01-4	\mathtt{BRL}	2.00		ug/L	04/24/10 00:22		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/24/10 00:22		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-33

Matrix: Water

% Moisture:

Lab Sample Id: 369409-029

Date Collected: Apr-15-10 11:50

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:10

Tech: CYE

	Seq Number: 804		Date Trep.	. Apr-23-10	0 19.10	i ech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	223	25.0		ug/L	04/24/10 01:06	D	5
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/24/10 00:44		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/24/10 00:44		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/24/10 00:44		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/24/10 00:44		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/24/10 00:44		1
MTBE	1634-04-4	61.9	5.00		ug/L	04/24/10 00:44		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/24/10 00:44		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/24/10 00:44		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/24/10 00:44		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/24/10 00:44		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/24/10 00:44		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/24/10 00:44		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/24/10 00:44		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/24/10 00:44		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/24/10 00:44		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/24/10 00:44		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/24/10 00:44		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/24/10 00:44		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/24/10 00:44		1
Dibromomethane.	74-95-3	BRL	5.00		ug/L	04/24/10 00:44		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/24/10 00:44		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/24/10 00:44		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/24/10 00:44		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/24/10 00:44		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/24/10 00:44		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/24/10 00:44		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/24/10 00:44		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/24/10 00:44		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/24/10 00:44		1
1,2-Dichloropropane	78-87 - 5	BRL	5.00		ug/L	04/24/10 00:44		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/24/10 00:44		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/24/10 00:44		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/24/10 00:44		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/24/10 00:44		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/24/10 00:44		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/24/10 00:44		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/24/10 00:44		1
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/24/10 00:44		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-33

Matrix: Water

% Moisture:

Lab Sample Id: 369409-029

Date Collected: Apr-15-10 11:50

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:10

Tech: CYE

	Seq Number: 804	067	•	1			~	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/24/10 00:44		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/24/10 00:44		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/24/10 00:44		1
Styrene	100-42-5	BRL	5.00		ug/L	04/24/10 00:44		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/24/10 00:44		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/24/10 00:44		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/24/10 00:44		1
Toluene	108-88-3	BRL	5.00		ug/L	04/24/10 00:44		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/24/10 00:44		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/24/10 00:44		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/24/10 00:44		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/24/10 00:44		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/24/10 00:44		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/24/10 00:44		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/24/10 00:44		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/24/10 00:44		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/24/10 00:44		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/24/10 00:44		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/24/10 00:44		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/24/10 00:44		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/24/10 00:44		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-39

Matrix: Water

% Moisture:

Lab Sample Id: 369409-030

Date Collected: Apr-15-10 12:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:14

Tech: CYE

	Seq Number: 804067
'arameter	

	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	65.9	5.00		ug/L	04/24/10 01:28		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/24/10 01:28		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/24/10 01:28		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/24/10 01:28		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/24/10 01:28		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/24/10 01:28		1
MTBE	1634-04-4	36.7	5.00		ug/L	04/24/10 01:28		1
n-Butylbenzene	104-51-8	8.38	5.00		ug/L	04/24/10 01:28		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/24/10 01:28		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/24/10 01:28		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/24/10 01:28		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/24/10 01:28		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/24/10 01:28		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/24/10 01:28		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/24/10 01:28		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/24/10 01:28		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/24/10 01:28		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/24/10 01:28		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/24/10 01:28		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/24/10 01:28		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/24/10 01:28		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/24/10 01:28		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/24/10 01:28		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/24/10 01:28		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/24/10 01:28		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/24/10 01:28		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/24/10 01:28		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/24/10 01:28		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/24/10 01:28		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/24/10 01:28		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/24/10 01:28		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/24/10 01:28		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/24/10 01:28		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L ug/L	04/24/10 01:28		î
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/24/10 01:28		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L ug/L	04/24/10 01:28		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/24/10 01:28		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/24/10 01:28		1
isopropylbenzene	98-82-8	13.3	5.00		ug/L ug/L	04/24/10 01:28		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-39

Matrix: Water

% Moisture:

Lab Sample Id: 369409-030

Date Collected: Apr-15-10 12:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-23-10 19:14

Tech: CYE

	Seq Number: 804	067						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date F	lag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/24/10 01:28		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/24/10 01:28		1
n-Propylbenzene	103-65-1	21.1	5.00		ug/L	04/24/10 01:28		1
Styrene	100-42-5	BRL	5.00		ug/L	04/24/10 01:28		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/24/10 01:28		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/24/10 01:28		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/24/10 01:28		1
Toluene	108-88-3	BRL	5.00		ug/L	04/24/10 01:28		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/24/10 01:28		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/24/10 01:28		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/24/10 01:28		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/24/10 01:28		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/24/10 01:28		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/24/10 01:28		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/24/10 01:28		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/24/10 01:28		1
1,3,5-Trimethylbenzene	108-67-8	12.7	5.00		ug/L	04/24/10 01:28		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/24/10 01:28		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/24/10 01:28		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/24/10 01:28		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/24/10 01:28		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-35

Matrix: Water

% Moisture:

Lab Sample Id: 369409-031

Date Collected: **Apr-15-10 12:10**

Date Received: Apr-16-10 09:00

Date Prep: Apr-26-10 13:56

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Tech: CYE

	Seq Number: 804		Date Trep.	. Apr-20-1	0 13.30	recn:	CIE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	765	50.0		ug/L	04/26/10 16:30	D	10
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/26/10 16:08		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/26/10 16:08		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/26/10 16:08		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/26/10 16:08		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/26/10 16:08		1
MTBE	1634-04-4	97.4	5.00		ug/L	04/26/10 16:08		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/26/10 16:08		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/26/10 16:08		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/26/10 16:08		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/26/10 16:08		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/26/10 16:08		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/26/10 16:08		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/26/10 16:08		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/26/10 16:08		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/26/10 16:08		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/26/10 16:08		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/26/10 16:08		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/26/10 16:08		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/26/10 16:08		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/26/10 16:08		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/26/10 16:08		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/26/10 16:08		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/26/10 16:08		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/26/10 16:08		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/26/10 16:08		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/26/10 16:08		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/26/10 16:08		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/26/10 16:08		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/26/10 16:08		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/26/10 16:08		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/26/10 16:08		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/26/10 16:08		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/26/10 16:08		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/26/10 16:08		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/26/10 16:08		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/26/10 16:08		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/26/10 16:08		1
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/26/10 16:08		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-35

Matrix: Water

% Moisture:

Lab Sample Id: 369409-031

Date Collected: Apr-15-10 12:10

Date Received: Apr-16-10 09:00

Date Prep: Apr-26-10 13:56

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Tech: CYE

	Seq Number: 804	058						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/26/10 16:08		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/26/10 16:08		1
n-Propylbenzene	103-65-1	5.87	5.00		ug/L	04/26/10 16:08		1
Styrene	100-42-5	BRL	5.00		ug/L	04/26/10 16:08		I
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/26/10 16:08		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/26/10 16:08		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/26/10 16:08		1
Toluene	108-88-3	9.78	5.00		ug/L	04/26/10 16:08		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/26/10 16:08		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/26/10 16:08		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/26/10 16:08		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/26/10 16:08		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/26/10 16:08		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/26/10 16:08		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/26/10 16:08		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/26/10 16:08		1
1,3,5-Trimethylbenzene	108-67-8	\mathtt{BRL}	5.00		ug/L	04/26/10 16:08		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/26/10 16:08		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/26/10 16:08		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/26/10 16:08		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/26/10 16:08		1

Project: Standard List of Methods

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-38

Matrix: Water

% Moisture:

Lab Sample Id: 369409-032

Date Collected: Apr-15-10 12:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 13:48

Tech: CYE

	Seq Number: 804		Date Frep.	. Apr-20-11	J 13.46	lecn:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	BRL	5.00		ug/L	04/26/10 14:39		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/26/10 14:39		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/26/10 14:39		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/26/10 14:39		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/26/10 14:39		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/26/10 14:39		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/26/10 14:39		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/26/10 14:39		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/26/10 14:39		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/26/10 14:39		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/26/10 14:39		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/26/10 14:39		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/26/10 14:39		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/26/10 14:39		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/26/10 14:39		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/26/10 14:39		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/26/10 14:39		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/26/10 14:39		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/26/10 14:39		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/26/10 14:39		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/26/10 14:39		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/26/10 14:39		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/26/10 14:39		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/26/10 14:39		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/26/10 14:39		1
1,1-Dichloroethane	75-34-3	BRL	5.00	•	ug/L	04/26/10 14:39		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/26/10 14:39		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/26/10 14:39		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/26/10 14:39		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/26/10 14:39		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/26/10 14:39		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/26/10 14:39		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/26/10 14:39		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/26/10 14:39		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/26/10 14:39		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/26/10 14:39		1
Ethylbenzene	100-41-4	BRL	5.00		ug/L	04/26/10 14:39		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/26/10 14:39		1
isopropylbenzene	98-82-8	BRL	5.00		ug/L	04/26/10 14:39		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-38

Matrix: Water

% Moisture:

Lab Sample Id: 369409-032

Date Collected: Apr-15-10 12:20

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 13:48

Tech: CYE

	Seq Number: 804	058						
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/26/10 14:39		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/26/10 14:39		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/26/10 14:39		1
Styrene	100-42-5	BRL	5.00		ug/L	04/26/10 14:39		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/26/10 14:39		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/26/10 14:39		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/26/10 14:39		1
Toluene	108-88-3	BRL	5.00		ug/L	04/26/10 14:39		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/26/10 14:39		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/26/10 14:39		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/26/10 14:39		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/26/10 14:39		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/26/10 14:39		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/26/10 14:39		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/26/10 14:39		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/26/10 14:39		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/26/10 14:39		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/26/10 14:39		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/26/10 14:39		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/26/10 14:39		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/26/10 14:39		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-18 Matrix: Water % Moisture:

Lab Sample Id: 369409-033 Date Collected: Apr-15-10 12:30
Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260 Prep Method: SW5030B

	Analyst: CY Seq Number: 804		Date Prep:	Apr-26-10	13:50	Tech:	CYE	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Benzene	71-43-2	36.6	5.00		ug/L	04/26/10 15:02		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/26/10 15:02		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/26/10 15:02		1
Bromodichloromethane	75-27-4	BRL	5.00		ug/L	04/26/10 15:02		1
Bromoform	75-25-2	BRL	5.00		ug/L	04/26/10 15:02		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/26/10 15:02		1
MTBE	1634-04-4	BRL	5.00		ug/L	04/26/10 15:02		1
n-Butylbenzene	104-51-8	BRL	5.00		ug/L	04/26/10 15:02		1
Sec-Butylbenzene	135-98-8	BRL	5.00		ug/L	04/26/10 15:02		1
tert-Butylbenzene	98-06-6	BRL	5.00		ug/L	04/26/10 15:02		1
Carbon Tetrachloride	56-23-5	BRL	5.00		ug/L	04/26/10 15:02		1
Chlorobenzene	108-90-7	BRL	5.00		ug/L	04/26/10 15:02		1
Chloroethane	75-00-3	BRL	10.0		ug/L	04/26/10 15:02		1
Chloroform	67-66-3	BRL	5.00		ug/L	04/26/10 15:02		1
Chloromethane	74-87-3	BRL	10.0		ug/L	04/26/10 15:02		1
2-Chlorotoluene	95-49-8	BRL	5.00		ug/L	04/26/10 15:02		1
4-Chlorotoluene	106-43-4	BRL	5.00		ug/L	04/26/10 15:02		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00		ug/L	04/26/10 15:02		1
Dibromochloromethane	124-48-1	BRL	5.00		ug/L	04/26/10 15:02		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00		ug/L	04/26/10 15:02		1
Dibromomethane	74-95-3	BRL	5.00		ug/L	04/26/10 15:02		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00		ug/L	04/26/10 15:02		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00		ug/L	04/26/10 15:02		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00		ug/L	04/26/10 15:02		1
Dichlorodifluoromethane	75-71-8	BRL	5.00		ug/L	04/26/10 15:02		1
1,1-Dichloroethane	75-34-3	BRL	5.00		ug/L	04/26/10 15:02		1
1,2-Dichloroethane	107-06-2	BRL	5.00		ug/L	04/26/10 15:02		1
1,1-Dichloroethene	75-35-4	BRL	5.00		ug/L	04/26/10 15:02		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00		ug/L	04/26/10 15:02		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00		ug/L	04/26/10 15:02		1
1,2-Dichloropropane	78-87-5	BRL	5.00		ug/L	04/26/10 15:02		1
1,3-Dichloropropane	142-28-9	BRL	5.00		ug/L	04/26/10 15:02		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ug/L	04/26/10 15:02		1
1,1-Dichloropropene	563-58-6	BRL	5.00		ug/L	04/26/10 15:02		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ug/L	04/26/10 15:02		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00		ug/L	04/26/10 15:02		1
Ethylbenzene	100-41-4	13.3	5.00		ug/L	04/26/10 15:02		1
Hexachlorobutadiene	87-68-3	BRL	5.00		ug/L	04/26/10 15:02		1
isopropylbenzene	98-82-8	51.7	5.00		ug/L	04/26/10 15:02		1

Project: Standard List of Methods

Final Ver. 1.000





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: MW-18

Matrix: Water

% Moisture:

Lab Sample Id: 369409-033

Date Collected: Apr-15-10 12:30

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 13:50

Tech: CYE

	Seq Number: 804	058				•		
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/26/10 15:02		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/26/10 15:02		1
n-Propylbenzene	103-65-1	35.9	5.00		ug/L	04/26/10 15:02		1
Styrene	100-42-5	BRL	5.00		ug/L	04/26/10 15:02		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/26/10 15:02		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/26/10 15:02		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/26/10 15:02		1
Toluene	108-88-3	5.08	5.00		ug/L	04/26/10 15:02		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/26/10 15:02		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/26/10 15:02		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/26/10 15:02		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/26/10 15:02		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/26/10 15:02		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/26/10 15:02		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/26/10 15:02		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/26/10 15:02		1
1,3,5-Trimethylbenzene	108-67-8	50.2	5.00		ug/L	04/26/10 15:02		1
o-Xylene	95-47-6	5.10	5.00		ug/L	04/26/10 15:02		1
m,p-Xylenes	179601-23-1	11.8	10.0		ug/L	04/26/10 15:02		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/26/10 15:02		1
Total Xylenes	1330-20-7	16.9	5.00		ug/L	04/26/10 15:02		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: Trip Blank

Matrix: Water

% Moisture:

Lab Sample Id: 369409-034

Date Collected: Apr-15-10 00:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 13:52

Tech: CYE

	Seq Number: 804	058	Date Trep.	Apr-20-10 13.32	rech: Cr	E
Parameter	Cas Number	Result	PQL	MDL Unit	ts Analysis Date Fla	g Dil
Benzene	71-43-2	BRL	5.00	ug/L	04/26/10 15:24	1
Bromobenzene	108-86-1	BRL	5.00	ug/L		1
Bromochloromethane	74 - 97-5	BRL	5.00	ug/L		1
Bromodichloromethane	. 75-27-4	BRL	5.00	ug/L		1
Bromoform	75-25-2	BRL	5.00	ug/L		1
Bromomethane	74-83-9	BRL	5.00	ug/L		1
MTBE	1634-04-4	BRL	5.00	ug/L		1
n-Butylbenzene	104-51-8	BRL	5.00	ug/L		1
Sec-Butylbenzene	135-98-8	BRL	5.00	ug/L		1
tert-Butylbenzene	98-06-6	BRL	5.00	ug/L	04/26/10 15:24	1
Carbon Tetrachloride	56-23-5	BRL	5.00	ug/L	04/26/10 15:24	· 1
Chlorobenzene	108-90-7	BRL	5.00	ug/L	04/26/10 15:24	1
Chloroethane	75-00-3	BRL	10.0	ug/L	04/26/10 15:24	1
Chloroform	67-66-3	BRL	5.00	ug/L	04/26/10 15:24	1
Chloromethane	74-87-3	BRL	10.0	ug/L		1
2-Chlorotoluene	95-49-8	BRL	5.00	ug/L	04/26/10 15:24	1
4-Chlorotoluene	106-43-4	BRL	5.00	ug/L	04/26/10 15:24	1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00	ug/L	04/26/10 15:24	1
Dibromochloromethane	124-48-1	BRL	5.00	ug/L	04/26/10 15:24	1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00	ug/L	04/26/10 15:24	1
Dibromomethane	74-95-3	BRL	5.00	ug/L	04/26/10 15:24	1
1,2-Dichlorobenzene	95-50-1	BRL	5.00	ug/L	04/26/10 15:24	1
1,3-Dichlorobenzene	541-73-1	BRL	5.00	ug/L	04/26/10 15:24	1
1,4-Dichlorobenzene	106-46-7	BRL	5.00	ug/L	04/26/10 15:24	1
Dichlorodifluoromethane	75-71-8	BRL	5.00	ug/L	04/26/10 15:24	1
1,1-Dichloroethane	75-34-3	BRL	5.00	ug/L	04/26/10 15:24	1
1,2-Dichloroethane	107-06-2	BRL	5.00	ug/L	04/26/10 15:24	1
1,1-Dichloroethene	75-35-4	BRL	5.00	ug/L	04/26/10 15:24	1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00	ug/L	04/26/10 15:24	1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ug/L	04/26/10 15:24	1
1,2-Dichloropropane	78-87-5	BRL	5.00	ug/L	04/26/10 15:24	1
1,3-Dichloropropane	142-28-9	BRL	5.00	ug/L	04/26/10 15:24	1
2,2-Dichloropropane	594-20-7	BRL	5.00	ug/L	04/26/10 15:24	1
1,1-Dichloropropene	563-58-6	BRL	5.00	· ug/L	04/26/10 15:24	1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00	ug/L	04/26/10 15:24	1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00	ug/L	04/26/10 15:24	1
Ethylbenzene	100-41-4	BRL	5.00	ug/L	04/26/10 15:24	1
Hexachlorobutadiene	87-68-3	BRL	5.00	ug/L	04/26/10 15:24	1
isopropylbenzene	98-82-8	BRL	5.00	ug/L	04/26/10 15:24	1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: Trip Blank

Matrix: Water

% Moisture:

Lab Sample Id: 369409-034

Date Collected: Apr-15-10 00:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 13:52

Tech: CYE

	Seq Number: 804	058		1			012	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date]	Flag	Dil
Methylene Chloride	75-09 - 2	BRL	5.00		ug/L	04/26/10 15:24		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/26/10 15:24		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/26/10 15:24		1
Styrene	100-42-5	BRL	5.00		ug/L	04/26/10 15:24		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/26/10 15:24		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/26/10 15:24		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/26/10 15:24		1
Toluene	108-88-3	BRL	5.00		ug/L	04/26/10 15:24		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/26/10 15:24		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/26/10 15:24		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/26/10 15:24		1
1,1,2-Trichloroethane	79-00-5	BRL	5.00		ug/L	04/26/10 15:24		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/26/10 15:24		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/26/10 15:24		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/26/10 15:24		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/26/10 15:24		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/26/10 15:24		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/26/10 15:24		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/26/10 15:24		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/26/10 15:24		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/26/10 15:24		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: Field Blank

Matrix: Water

% Moisture:

Lab Sample Id: 369409-035

Date Collected: Apr-15-10 07:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 13:54

Tech: CYE

	Seq Number: 804	058	*	•		200,000		
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date F	lag	Dil
Benzene	71-43-2	BRL	5.00	. 1	ug/L	04/26/10 15:46		1
Bromobenzene	108-86-1	BRL	5.00		ug/L	04/26/10 15:46		1
Bromochloromethane	74-97-5	BRL	5.00		ug/L	04/26/10 15:46		1
Bromodichloromethane	75-27-4	BRL	5.00		ıg/L	04/26/10 15:46		1
Bromoform	75-25-2	BRL	5.00		ıg/L	04/26/10 15:46		1
Bromomethane	74-83-9	BRL	5.00		ug/L	04/26/10 15:46		1
MTBE	1634-04-4	BRL	5.00	1	ıg/L	04/26/10 15:46		1
n-Butylbenzene	104-51-8	BRL	5.00		ıg/L	04/26/10 15:46		1
Sec-Butylbenzene	135-98-8	BRL	5.00	1	ıg/L	04/26/10 15:46		1
tert-Butylbenzene	98-06 - 6	BRL	5,00	ī	ıg/L	04/26/10 15:46		1
Carbon Tetrachloride	56-23-5	BRL	5.00	ì	ıg/L	04/26/10 15:46		1
Chlorobenzene	108-90-7	BRL	5.00		ıg/L	04/26/10 15:46		1
Chloroethane	75-00-3	BRL	10.0	ı	ıg/L	04/26/10 15:46		1
Chloroform	67-66-3	BRL	5.00	ì	ıg/L	04/26/10 15:46		1
Chloromethane	74-87-3	BRL	10.0	ı	ıg/L	04/26/10 15:46		1
2-Chlorotoluene	95-49-8	BRL	5.00	1	ıg/L	04/26/10 15:46		1
4-Chlorotoluene	106-43-4	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
p-Cymene (p-Isopropyltoluene)	99-87-6	BRL	5.00	ı	ıg/L	04/26/10 15:46		1
Dibromochloromethane	124-48-1	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
1,2-Dibromo-3-Chloropropane	96-12-8	BRL	5.00	ı	ıg/L	04/26/10 15:46		1
Dibromomethane	74-95-3	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
1,2-Dichlorobenzene	95-50-1	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
1,3-Dichlorobenzene	541-73-1	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
1,4-Dichlorobenzene	106-46-7	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
Dichlorodifluoromethane	75-71-8	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
1,1-Dichloroethane	75-34-3	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
1,2-Dichloroethane	107-06-2	BRL	5.00	ι	ıg/L	04/26/10 15:46		1
1,1-Dichloroethene	75-35-4	BRL	5.00	ı	ıg/L	04/26/10 15:46		1
cis-1,2-Dichloroethene	156-59-2	BRL	5.00	ı	ıg/L	04/26/10 15:46		1
trans-1,2-dichloroethene	156-60-5	BRL	5.00	ι	ıg/L	04/26/10 15:46	•	1
1,2-Dichloropropane	78-87 <i>-</i> 5	BRL	5.00	ì	ıg/L	04/26/10 15:46		1
1,3-Dichloropropane	142-28-9	BRL	5.00	t	ıg/L	04/26/10 15:46		1
2,2-Dichloropropane	594-20-7	BRL	5.00		ıg/L	04/26/10 15:46		1
1,1-Dichloropropene	563-58-6	BRL	5.00	υ	ıg/L	04/26/10 15:46		1
cis-1,3-Dichloropropene	10061-01-5	BRL	5.00		ıg/L	04/26/10 15:46		1
trans-1,3-dichloropropene	10061-02-6	BRL	5.00	t	ıg/L	04/26/10 15:46		1
Ethylbenzene	100-41-4	BRL	5.00	υ		04/26/10 15:46		1 .
Hexachlorobutadiene	87-68-3	BRL	5.00	υ	ıg/L	04/26/10 15:46		1
isopropylbenzene	98-82-8	BRL	5.00	υ	ıg/L	04/26/10 15:46		1





Sovereign Consulting, Inc. (NY), Cranberry Twp, PA

25 Paidge Avenue

Sample Id: Field Blank

Matrix: Water

% Moisture:

Lab Sample Id: 369409-035

Date Collected: Apr-15-10 07:00

Date Received: Apr-16-10 09:00

Analytical Method: VOAs by SW-846 8260

Prep Method: SW5030B

Analyst: CYE

Date Prep: Apr-26-10 13:54

Tech: CYE

	Seq Number: 804	058				10011.	CIL	
Parameter	Cas Number	Result	PQL	MDL	Units	Analysis Date	Flag	Dil
Methylene Chloride	75-09-2	BRL	5.00		ug/L	04/26/10 15:46		1
Naphthalene	91-20-3	BRL	10.0		ug/L	04/26/10 15:46		1
n-Propylbenzene	103-65-1	BRL	5.00		ug/L	04/26/10 15:46		1
Styrene	100-42-5	BRL	5.00		ug/L	04/26/10 15:46		1
1,1,1,2-Tetrachloroethane	630-20-6	BRL	5.00		ug/L	04/26/10 15:46		1
1,1,2,2-Tetrachloroethane	79-34-5	BRL	5.00		ug/L	04/26/10 15:46		1
Tetrachloroethylene	127-18-4	BRL	5.00		ug/L	04/26/10 15:46		1
Toluene	108-88-3	BRL	5.00		ug/L	04/26/10 15:46		1
1,2,3-Trichlorobenzene	87-61-6	BRL	5.00		ug/L	04/26/10 15:46		1
1,2,4-Trichlorobenzene	120-82-1	BRL	5.00		ug/L	04/26/10 15:46		1
1,1,1-Trichloroethane	71-55-6	BRL	5.00		ug/L	04/26/10 15:46		1
1,1,2-Trichloroethane	79-00-5	\mathtt{BRL}	5.00		ug/L	04/26/10 15:46		1
Trichloroethene	79-01-6	BRL	5.00		ug/L	04/26/10 15:46		1
Trichlorofluoromethane	75-69-4	BRL	5.00		ug/L	04/26/10 15:46		1
1,2,3-Trichloropropane	96-18-4	BRL	5.00		ug/L	04/26/10 15:46		1
1,2,4-Trimethylbenzene	95-63-6	BRL	5.00		ug/L	04/26/10 15:46		1
1,3,5-Trimethylbenzene	108-67-8	BRL	5.00		ug/L	04/26/10 15:46		1
o-Xylene	95-47-6	BRL	5.00		ug/L	04/26/10 15:46		1
m,p-Xylenes	179601-23-1	BRL	10.0		ug/L	04/26/10 15:46		1
Vinyl Chloride	75-01-4	BRL	2.00		ug/L	04/26/10 15:46		1
Total Xylenes	1330-20-7	BRL	5.00		ug/L	04/26/10 15:46		1



XENCO CHRONOLOGY OF HOLDING TIMES

Analytical Method: VOAs by SW-846 8260	Client:	Sovereign Consulting, Inc. (N
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Work Order #: 369409 Project ID: <u>EQ24</u>

Field Sample ID	Date Collected	Date Received	Date Extracted	Max Holding Time Extracted (Days)	Time Held Extracte d (Days)	Date Analyzed	Max Holding Time Analyzed (Days)	Time Held Analyzed (Days)	Q
MW-8	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P
Field Blank	Apr. 15, 2010	Apr. 16, 2010				Apr.26, 2010	14	11	P
MW-43	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
TRW-2	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
MW-21R	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P
MW-28	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P
MW-7R	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P
MW-9	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	Р
MW-42	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
MW-20	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	Р
MW-15	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
MW-16	Apr. 15, 2010	Apr. 16, 2010				Apr.26, 2010	14	11	P
MW-18	Apr. 15, 2010	Apr. 16, 2010				Apr.26, 2010	14	11	P
MW-29	Apr. 15, 2010	Apr. 16, 2010			_	Apr.21, 2010	14	6	P
MW-27	Apr. 15, 2010	Apr. 16, 2010		İ		Apr.22, 2010	14	7	P
MW-6	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P
MW-30	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
MW-35	Apr. 15, 2010	Apr. 16, 2010				Apr.26, 2010	14	11	P
MW-1	Apr. 15, 2010	Apr. 16, 2010				Apr.20, 2010	14	5	P
MW-44	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
MW-3	Apr. 15, 2010	Apr. 16, 2010		ĺ		Apr.21, 2010	14	6	Р
MW-13	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P
MW-23	Apr. 15, 2010	Apr. 16, 2010		i		Apr.22, 2010	14	7	P
MW-17	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
MW-19	Apr. 15, 2010	Apr. 16, 2010				Apr.24, 2010	14	9	P
MW-32	Apr. 15, 2010	Apr. 16, 2010				Apr.24, 2010	14	9	Р
MW-33		Apr. 16, 2010				Apr.24, 2010	14	9	P
MW-39		Apr. 16, 2010				Apr.24, 2010		9	P
MW-5		Apr. 16, 2010				Apr.22, 2010		7	P
MW-24		Apr. 16, 2010				Apr.22, 2010		7	P



XENCO CHRONOLOGY OF HOLDING TIMES

Analytical Method: VOAs by SW-846 8260		Sovereign Consulting, Inc. (N
Work Order #: <u>369409</u>	Project ID:	EQ24

Field Sample ID	Date Collected	Date Received	Date Extracted	Max Holding Time Extracted (Days)	Extracte	· · · · · · ·	Max Holding Time Analyzed (Days)		Q
Trip Blank	Apr. 15, 2010	Apr. 16, 2010				Apr.26, 2010	14	11	P
MW-22R	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P
MW-25	Apr. 15, 2010	Apr. 16, 2010				Apr.23, 2010	14	8	P
MW-38	Apr. 15, 2010	Apr. 16, 2010				Apr.26, 2010	14	11	P
MW-14	Apr. 15, 2010	Apr. 16, 2010				Apr.22, 2010	14	7	P

 $F = \mbox{These samples were analyzed outside the recommended holding time.} \\ P = \mbox{Samples analyzed within the recommended holding time.} \\$



Flagging Criteria



- X In our quality control review of the data a QC deficiency was observed and flagged as noted. MS/MSD recoveries were found to be outside of the laboratory control limits due to possible matrix /chemical interference, or a concentration of target analyte high enough to effect the recovery of the spike concentration. This condition could also effect the relative percent difference in the MS/MSD.
- **B** A target analyte or common laboratory contaminant was identified in the method blank. Its presence indicates possible field or laboratory contamination.
- **D** The sample(s) were diluted due to targets detected over the highest point of the calibration curve, or due to matrix interference. Dilution factors are included in the final results. The result is from a diluted sample.
- E The data exceeds the upper calibration limit; therefore, the concentration is reported as estimated.
- F RPD exceeded lab control limits.
- J The target analyte was positively identified below the MQL and above the SQL.
- U Analyte was not detected.
- L The LCS data for this analytical batch was reported below the laboratory control limits for this analyte.

 The department supervisor and QA Director reviewed data. The samples were either reanalyzed or flagged as estimated concentrations.
- **H** The LCS data for this analytical batch was reported above the laboratory control limits. Supporting QC Data were reviewed by the Department Supervisor and QA Director. Data were determined to be valid for reporting.
- K Sample analyzed outside of recommended hold time.
- JN A combination of the "N" and the "J" qualifier. The analysis indicates that the analyte is "tentatively identified" and the associated numerical value may not be consistent with the amount actually present in the environmental sample.
- **BRL** Below Reporting Limit.
- **RL** Reporting Limit
- * Outside XENCO's scope of NELAC Accreditation.

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9701 Harry Hines Blvd, Dallas, TX 75220	(214) 902 0300	(214) 351-9139
5332 Blackberry Drive, San Antonio TX 78238	(210) 509-3334	(210) 509-3335
2505 North Falkenburg Rd, Tampa, FL 33619	(813) 620-2000	(813) 620-2033
5757 NW 158th St, Miami Lakes, FL 33014	(305) 823-8500	(305) 823-8555
12600 West I-20 East, Odessa, TX 79765	(432) 563-1800	(432) 563-1713
842 Cantwell Lane, Corpus Christi, TX 78408	(361) 884-0371	(361) 884-9116

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Final Ver. 1.000



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Sample: 561312-1-BKS / BKS

Project ID: EQ24

Lab Batch #: 803446

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/20/10 19:44	SU	RROGATE R	E RECOVERY STUDY			
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene	0.0511	0,0500	102	74-124		
Dibromofluoromethane	0.0497	0.0500	99	75-131		
1,2-Dichloroethane-D4	0.0469	0.0500	94	63-144		
Toluene-D8	0.0507	0.0500	101	80-117		

Lab Batch #: 803446

Sample: 561312-1-BLK / BLK

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/20/10 20:28	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0513	0.0500	103	74-124		
Dibromofluoromethane		0.0498	0,0500	100	75-131		
1,2-Dichloroethane-D4		0.0472	0.0500	94	63-144		
Toluene-D8		0.0478	0.0500	96	80-117		

Lab Batch #: 803446

Sample: 369409-001 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/	/20/10 20:50	0/10 20:50 SURROGATE RECOVERY				
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0501	0.0500	100	74-124	
Dibromofluoromethane		0.0492	0.0500	98	75-131	
1,2-Dichloroethane-D4		0.0497	0.0500	99	63-144	
Toluene-D8		0.0491	0.0500	98	80-117	

Lab Batch #: 803446

Sample: 369409-001 S/MS

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed:	04/20/10 21:11	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0510	0.0500		74.104		
4-Biomonuoropenzene		0.0519	0.0500	104	74-124		
Dibromofluoromethane		0.0523	0.0500	105	75-131		
1,2-Dichloroethane-D4		0.0496	0.0500	99	63-144		
Toluene-D8		0.0491	0.0500	98	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 803446

Project ID: EQ24

Sample: 369409-001 SD / MSD

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/20/10 21:32	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene	0.0504	0.0500	101	74-124		
Dibromofluoromethane	0.0535	0.0500	107	75-131		
1,2-Dichloroethane-D4	0.0491	0.0500	98	63-144		
Toluene-D8	0.0490	0.0500	98	80-117		

Lab Batch #: 803446

Sample: 369409-002 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/21/10 05:05 SURROGATE RECOVERY STUDY						
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0512	0.0500	102	74-124	
Dibromofluoromethane		0.0512	0.0500	102	75-131	
1,2-Dichloroethane-D4		0.0490	0.0500	98	63-144	
Toluene-D8		0.0483	0.0500	97	80-117	

Lab Batch #: 803645

Sample: 561445-1-BKS / BKS

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/21/10 10:43	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0514	0.0500	103	74-124		
Dibromofluoromethane		0.0482	0.0500	96	75-131		
1,2-Dichloroethane-D4		0.0458	0.0500	92	63-144		
Toluene-D8		0.0522	0.0500	104	80-117		

Lab Batch #: 803645

Sample: 561445-1-BLK / BLK

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/21/10 11:27	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0517	0.0500	103	74-124		
Dibromofluoromethane		0.0495	0.0500	99	75-131		
1,2-Dichloroethane-D4		0.0492	0.0500	98	63-144		
Toluene-D8		0.0483	0.0500	97	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 803645 Sample: 369409-003 / SMP Project ID: EQ24

Batch: 1 Matrix: Water

SURROGATE RECOVERY STUDY Units: mg/L Date Analyzed: 04/21/10 13:58 True Control VOAs by SW-846 8260 Found Amount Recovery Limits Flags [A] [B] %R %R Analytes [D] 4-Bromofluorobenzene 0.0533 0.0500 107 74-124 Dibromofluoromethane 0.0487 0.0500 97 75-131 1,2-Dichloroethane-D4 0.0457 0.0500 63-144 91

0.0494

Lab Batch #: 803645

Toluene-D8

Sample: 369409-003 S / MS

Batch:

Matrix: Water

80-117

0.0500

Units: mg/L	Date Analyzed: 04/21/10 14:20	SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0522	0.0500	104	74-124		
Dibromofluoromethane		0.0526	0.0500	105	75-131		
1,2-Dichloroethane-D4		0.0489	0.0500	98	63-144		
Toluene-D8		0.0502	0.0500	100	80-117		

Lab Batch #: 803645

Sample: 369409-003 SD / MSD

Batch:

Matrix: Water

Units: mg/L	Date Analyzed: 04/21/10 14:42	SU	RROGATE R	ECOVERY S	STUDY	
VOAs	s by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
· · ·	Analytes			[~]		_
4-Bromofluorobenzene		0.0515	0.0500	103	74-124	
Dibromofluoromethane		0.0529	0,0500	106	75-131	
1,2-Dichloroethane-D4		0.0481	0.0500	96	63-144	
Toluene-D8		0.0496	0.0500	99	80-117	

Lab Batch #: 803828

Sample: 561560-1-BKS / BKS

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 15:08	SURROGATE RECOVERY STUDY					
	SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
	alytes						
4-Bromofluorobenzene	·	0.0494	0.0500	99	74-124		
Dibromofluoromethane		0.0516	0.0500	103	75-131		
1,2-Dichloroethane-D4		0.0482	0.0500	96	63-144		
Toluene-D8		0.0503	0.0500	101	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Sample: 561560-1-BLK/BLK

Project ID: EQ24

Lab Batch #: 803828

Batch: Matrix: Water

Units: mg/L Date Analyzed: 04/22/10 15:52	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene	0.0545	0.0500	109	74-124		
Dibromofluoromethane	0.0503	0.0500	101	75-131		
1,2-Dichloroethane-D4	0.0510	0.0500	102	63-144		
Toluene-D8	0.0495	0.0500	99	80-117		

Lab Batch #: 803828

Sample: 369409-004 / SMP

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed:	04/22/10 16:14	SU	RROGATE R	ECOVERY S	STUDY	
VOAs by SW-846 8260		Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags
Analytes				[D]		
4-Bromofluorobenzene		0.0513	0.0500	103	74-124	-
Dibromofluoromethane		0.0494	0.0500	99	75-131	_
1,2-Dichloroethane-D4		0.0485	0.0500	97	63-144	
Toluene-D8		0.0504	0.0500	101	80-117	

Lab Batch #: 803828

Sample: 369409-004 S / MS

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 16:36	SURROGATE RECOVERY STUI			STUDY				
VOAs	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags			
4-Bromofluorobenzene	1xiiaiy tes	0.0495	0.0500	99	74-124				
Dibromofluoromethane		0.0523	0.0500	105	75-131	_			
1,2-Dichloroethane-D4		0.0533	0.0500	107	63-144	~_ ·~			
Toluene-D8		0.0512	0.0500	102	80-117	_			

Lab Batch #: 803828

Sample: 369409-004 SD / MSD

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 16:58	SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
	Analytes			(2)		<u></u>	
4-Bromofluorobenzene		0.0510	0.0500	102	74-124		
Dibromofluoromethane		0.0519	0.0500	104	75-131		
1,2-Dichloroethane-D4		0,0537	0.0500	107	63-144		
Toluene-D8		0.0492	0.0500	98	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 803828

Sample: 369409-005 / SMP

Project ID: EQ24

Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 19:33	SU	RROGATE R	ECOVERY	STUDY	
•	SW-846 8260 alytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0501	0.0500	100	74-124	
Dibromofluoromethane		0.0513	0.0500	103	75-131	
1,2-Dichloroethane-D4		0.0519	0.0500	104	63-144	
Toluene-D8		0.0507	0.0500	101	80-117	

Lab Batch #: 803828

Sample: 369409-006 / SMP

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 19:55	SURROGATE RECOVERY STUDY				
VOAs	by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0513	0.0500	103	74-124	
Dibromofluoromethane		0.0512	0.0500	102	75-131	
1,2-Dichloroethane-D4		0.0534	0.0500	107	63-144	
Toluene-D8		0.0495	0.0500	99	80-117	-

Lab Batch #: 803828

Sample: 369409-007 / SMP

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 20:17	SURROGATE RECOVERY STUI			STUDY	
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0510	0.0500	102	74-124	-
Dibromofluoromethane		0.0474	0.0500	95	75-131	
1,2-Dichloroethane-D4		0.0539	0.0500	108	63-144	
Toluene-D8		0.0486	0.0500	97	80-117	

Lab Batch #: 803828

Sample: 369409-008 / SMP

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 20:39	SURROGATE RECOVERY STUDY					
	by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0519	0.0500	104	74-124	··	
Dibromofluoromethane		0.0490	0.0500	98	75-131		
1,2-Dichloroethane-D4		0.0541	0.0500	108	63-144		
Toluene-D8		0.0528	0.0500	106	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409, Lab Batch #: 803828

Sample: 369409-009 / SMP

Project ID: EQ24

Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 21:01	SU	ECOVERY	STUDY		
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0512	0.0500	102	74-124	
Dibromofluoromethane		0.0528	0.0500	106	75-131	
1,2-Dichloroethane-D4		0.0492	0.0500	98	63-144	
Toluene-D8		0.0509	0.0500	102	80-117	

Lab Batch #: 803828

Sample: 369409-010 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/22/10 21:23	SURROGATE RECOVERY STUDY				
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene	0.0513	0.0500	103	74-124	
Dibromofluoromethane	0,0482	0.0500	96	75-131	
1,2-Dichloroethane-D4	0.0499	0.0500	100	63-144	
Toluene-D8	0.0502	0.0500	100	80-117	

Lab Batch #: 803828

Sample: 369409-011 / SMP

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 21:45	SU	RROGATE R	TE RECOVERY STUDY				
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags		
4-Bromofluorobenzene		0.0547	0.0500	109	74-124			
Dibromofluoromethane	·	0.0504	0.0500	101	75-131			
1,2-Dichloroethane-D4		0.0485	0.0500	97	63-144			
Toluene-D8		0.0527	0.0500	105	80-117			

Lab Batch #: 803828

Sample: 369409-012 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/22/10 22:07	SURROGATE RECOVERY STUDY			STUDY	
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene	0.0536	0.0500	107	74-124	
Dibromofluoromethane	0.0488	0.0500	98	75-131	
1,2-Dichloroethane-D4	0.0491	0.0500	98	63-144	
Toluene-D8	0.0524	0.0500	105	80-117	

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 803828

Sample: 369409-013 / SMP

Project ID: EQ24

Matrix: Water Batch: 1

SURROGATE RECOVERY STUDY Date Analyzed: 04/22/10 22:51 Units: mg/L Amount True Control VOAs by SW-846 8260 Found Amount Recovery Limits Flags [A] %R %R [B] [D] Analytes 4-Bromofluorobenzene 0.0537 0.0500 107 74-124 Dibromofluoromethane 0.0504 0.0500 101 75-131 1,2-Dichloroethane-D4 0.0491 0.0500 98 63-144 Toluene-D8 0.0505 0.0500 101 80-117

Lab Batch #: 803828

Sample: 369409-014 / SMP

Batch:

Matrix: Water

Units: mg/L	Date Analyzed: 04/22/10 23:13	SURROGATE RECOVERY STUDY			STUDY	_
VOAs by SW-846 8260 Analytes		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0528	0.0500	106	74-124	
Dibromofluoromethane		0.0503	0.0500	101	75-131	
1,2-Dichloroethane-D4		0.0485	0.0500	97	63-144	
Toluene-D8		0.0508	0.0500	102	80-117	

Lab Batch #: 803828

Sample: 369409-015 / SMP

Batch:

Matrix: Water

Units: mg/L Date Analyzed: 04/22/10 23:35 SURROGATE RECOVERY STUDY						
VOAs by SW-8-		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
Analytes 4-Bromofluorobenzene		0.0530	0.0500	106	74-124	
		0.0530	0.0300	106	74-124	
Dibromofluoromethane		0.0507	0.0500	101	75-131	
1,2-Dichloroethane-D4		0.0498	0.0500	100	63-144	
Toluene-D8		0.0494	0.0500	99	80-117	

Lab Batch #: 803828

Sample: 369409-016 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/22/10 23:57	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene	0.0525	0.0500	105	74-124	_	
Dibromofluoromethane	0.0492	0.0500	98	75-131		
1,2-Dichloroethane-D4	0.0502	0.0500	100	63-144		
Toluene-D8	0.0512	0.0500	102	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Sample: 561728-1-BKS / BKS

Project ID: EQ24

Lab Batch #: 804058

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/26/10 11:40	SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0514	0.0500	103	74-124		
Dibromofluoromethane		0.0497	0.0500	99	75-131		
1,2-Dichloroethane-D4		0.0495	0.0500	99	63-144		
Toluene-D8		0.0481	0.0500	96	80-117		

Lab Batch #: 804058

Sample: 561728-1-BLK / BLK

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/26/10 12:23	SURROGATE RECOVERY STUDY						
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags		
4-Bromofluorobenzene	0.0494	0.0500	99	74-124			
Dibromofluoromethane	0.0505	0.0500	101	75-131			
1,2-Dichloroethane-D4	0.0501	0.0500	100	63-144	 		
Toluene-D8	0.0477	0.0500	95	80-117			

Lab Batch #: 804058

Sample: 369409-025 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date	te Analyzed: 04/26/10 13:11	SURROGATE RECOVERY STUDY					
VOAs by SW Analy		Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0498	0.0500	100	74-124		
Dibromofluoromethane		0.0485	0.0500	97	75-131		
1,2-Dichloroethane-D4		0.0479	0.0500	96	63-144		
Toluene-D8		0.0485	0.0500	97	80-117		

Lab Batch #: 804058

Sample: 369409-025 S / MS

Batch:

Matrix: Water

Units: mg/L Date Analyzed: 04/26/10 13:33 SURROGATE RECOVERY STUDY						
VOA	s by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags
	Analytes			[D]		
4-Bromofluorobenzene		0.0496	0.0500	99	74-124	
Dibromofluoromethane		0.0492	0.0500	98	75-131	
1,2-Dichloroethane-D4		0.0505	0.0500	101	63-144	
Toluene-D8		0.0479	0.0500	96	80-117	

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Project ID: EQ24

Lab Batch #: 804058

Sample: 369409-025 SD / MSD

Matrix: Water Batch: 1

Units: mg/L	Date Analyzed: 04/26/10 13:55	SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
	Analytes						
4-Bromofluorobenzene		0.0500	0.0500	100	74-124		
Dibromofluoromethane		0.0513	0.0500	103	75-131		
1,2-Dichloroethane-D4		0.0497	0.0500	99	63-144	,	
Toluene-D8		0.0485	0.0500	97	80-117		

Lab Batch #: 804058

Sample: 369409-032 / SMP

Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/26/10 14:39	ate Analyzed: 04/26/10 14:39 SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0490	0,0500	98	74-124		
Dibromofluoromethane		0.0509	0.0500	102	75-131		
1,2-Dichloroethane-D4		0.0507	0.0500	101	63-144		
Toluene-D8		0.0483	0.0500	97	80-117		

Lab Batch #: 804058

Sample: 369409-033 / SMP

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/26/10 15:02	SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags	
	Analytes			[D]	ļ		
4-Bromofluorobenzene		0.0516	0.0500	103	74-124		
Dibromofluoromethane		0.0501	0.0500	100	75-131		
1,2-Dichloroethane-D4		0.0503	0.0500	101	63-144		
Toluene-D8		0.0503	0.0500	101	80-117		

Lab Batch #: 804058

Sample: 369409-034 / SMP

Batch:

Matrix: Water

Units: mg/L Date Analyzed: 04/26/10 15:24	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene	0.0509	0.0500	102	74-124		
Dibromofluoromethane	0.0513	0.0500	103	75-131		
1,2-Dichloroethane-D4	0.0496	0.0500	99	63-144		
Toluene-D8	0.0404	0.0500	. 81	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409, Lab Batch #: 804058

Sample: 369409-035 / SMP

Project ID: EQ24

Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/26/10 15:46
VOAs	by SW-846 8260

Units: mg/L	Date Analyzed: 04/26/10 15:46	SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0489	0.0500	98	74-124	-	
Dibromofluoromethane		0.0499	0.0500	100	75-131		
1,2-Dichloroethane-D4		0.0501	0.0500	100	63-144		
Toluene-D8		0.0442	0.0500	88	80-117		

Lab Batch #: 804058

Sample: 369409-031 / SMP Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/26/10 16:08	SU	RROGATE R	ECOVERY	STUDY		
VOA	s by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags	
	Analytes			[D]	Control Limits		
4-Bromofluorobenzene		0.0470	0.0500	94	74-124		
Dibromofluoromethane		0.0497	0.0500	99	75-131		
1,2-Dichloroethane-D4		0.0512	0.0500	102	63-144		
Toluene-D8		0.0502	0.0500	100	80-117		

Lab Batch #: 804058

Sample: 369409-031/DL Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/26/10 16:30	SU	RROGATE R	ECOVERY	STUDY	
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0496	0.0500	99	74-124	
Dibromofluoromethane		0.0531	0.0500	106	75-131	
1,2-Dichloroethane-D4		0.0499	0.0500	100	63-144	
Toluene-D8		0.0485	0.0500	97	80-117	

Lab Batch #: 804058

Sample: 369409-024 / DL Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/26/10 16:56	SU	RROGATE R	ECOVERY	STUDY	
VOA	s by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags
	Analytes	ı		[D]		
4-Bromofluorobenzene		0.0497	0.0500	99	74-124	
Dibromofluoromethane		0.0505	0.0500	101	75-131	_
1,2-Dichloroethane-D4		0.0511	0.0500	102	63-144	
Toluene-D8	·	0.0501	0.0500	100	80-117	

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

All results are based on MDL and validated for QC purposes.

Final Ver. 1.000

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Project ID: EQ24

Lab Batch #: 804067

Sample: 561731-1-BKS / BKS

Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/23/10 16:17	SU	RROGATE R	ECOVERY S	STUDY	
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene	Analytes	0.0504	0.0500	101	74-124	
Dibromofluoromethane		0.0504	0.0500	101	75-131	
1,2-Dichloroethane-D4		0.0491	0.0500	98	63-144	
Toluene-D8		0.0509	0.0500	102	80-117	

Lab Batch #: 804067

Sample: 561731-1-BLK / BLK

Batch:

Matrix: Water

Units: mg/L	Date Analyzed: 04/23/10 17:01	SURROGATE RECOVERY STUDY				
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0503	0.0500	101	74-124	
Dibromofluoromethane		0.0490	0.0500	98	75-131	
1,2-Dichloroethane-D4		0.0527	0.0500	105	63-144	<u> </u>
Toluene-D8		0.0495	0.0500	99	80-117	

Lab Batch #: 804067

Sample: 369409-017 / SMP

Batch:

Matrix: Water

Units: mg/L	Date Analyzed: 04/23/10 17:23	SU	RROGATE R	ECOVERY	STUDY	
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0489	0.0500	98	74-124	
Dibromofluoromethane		0.0496	0.0500	99	75-131	
1,2-Dichloroethane-D4		0.0504	0.0500	101	63-144	
Toluene-D8		0.0503	0.0500	101	80-117	

Lab Batch #: 804067

Sample: 369409-017 S / MS

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 17:45	SU	RROGATE R	ECOVERY S	STUDY	
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
Analytes			[D]		
4-Bromofluorobenzene	0.0490	0.0500	98	74-124	
Dibromofluoromethane	0.0505	0.0500	101	75-131	
1,2-Dichloroethane-D4	0.0474	0.0500	95	63-144	
Toluene-D8	0.0490	0.0500	98	80-117	

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 804067

Project ID: EQ24

Sample: 369409-017 SD / MSD

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 18:07	7 SU	RROGATE R	ECOVERY	STUDY	-
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene	0.0483	0.0500	97	74-124	
Dibromofluoromethane	0.0505	0.0500	101	75-131	
1,2-Dichloroethane-D4	0.0512	0.0500	102	63-144	
Toluene-D8	0.0502	0.0500	100	80-117	

Lab Batch #: 804067

Sample: 369409-012 / DL

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/23/10 19:36	SU	RROGATE R	ECOVERY	STUDY	
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True · Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0504	0.0500	101	74-124	
Dibromofluoromethane		0.0501	0.0500	100	75-131	
1,2-Dichloroethane-D4		0.0488	0.0500	98	63-144	
Toluene-D8		0.0491	0.0500	98	80-117	

Lab Batch #: 804067

Sample: 369409-012/DL

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/23/10 19:58	SU	RROGATE R	ECOVERY S	STUDY	***************************************
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene		0.0510	0.0500	102	74-124	
Dibromofluoromethane		0.0503	0.0500	101	75-131	
1,2-Dichloroethane-D4		0.0496	0.0500	99	63-144	
Toluene-D8		0.0497	0.0500	99	80-117	

Lab Batch #: 804067

Sample: 369409-018 / SMP

Batch:

Matrix: Water

Units: mg/L	Date Analyzed: 04/23/10 20:20	SURROGATE RECOVERY STUDY				
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
	Alialytes			1~1		
4-Bromofluorobenzene		0.0496	0.0500	99	74-124	
Dibromofluoromethane		0.0481	0.0500	96	75-131	
1,2-Dichloroethane-D4		0.0503	0.0500	101	63-144	
Toluene-D8		0.0498	0.0500	100	80-117	

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 804067

Project ID: EQ24

Sample: 369409-019 / SMP

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 20:42	SU	RROGATE R	ECOVERY	STUDY	
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene	0.0500	0,0500	100	74-124	
Dibromofluoromethane	0.0480	0.0500	96	75-131	
1,2-Dichloroethane-D4	0.0495	0.0500	99	63-144	
Toluene-D8	0.0491	0.0500	98	80-117	

Lab Batch #: 804067

Sample: 369409-020 / SMP

Batch:

Matrix: Water

Units: mg/L D	SURROGATE RECOVERY STUDY						
·	W-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
Ana	lytes			[D]			
4-Bromofluorobenzene		0.0490	0.0500	98	74-124		
Dibromofluoromethane		0.0484	0.0500	97	75-131		
1,2-Dichloroethane-D4		0.0509	0.0500	102	63-144		
Toluene-D8		0.0503	0.0500	101	80-117		

Lab Batch #: 804067

Sample: 369409-021 / SMP

Batch:

Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 21:26	SURROGATE RECOVERY STUDY						
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags		
Analytes			[D]				
4-Bromofluorobenzene	0.0497	0.0500	99	74-124			
Dibromofluoromethane	0.0504	0.0500	101	75-131			
1,2-Dichloroethane-D4	0.0514	0.0500	103	63-144			
Toluene-D8	0.0498	0.0500	100	80-117			

Lab Batch #: 804067

Sample: 369409-022 / SMP

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/23/10 21:48	8 SURROGATE RECOVERY STUDY						
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags		
4-Bromofluorobenzene		0.0497	0.0500	99	74-124			
Dibromofluoromethane		0.0490	0.0500	98	75-131			
1,2-Dichloroethane-D4		0.0510	0.0500	102	63-144			
Toluene-D8		0.0502	0.0500	100	80-117	-		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409, Lab Batch #: 804067

Sample: 369409-023 / SMP

Project ID: EQ24

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 22:	09 SU	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags		
Analytes							
4-Bromofluorobenzene	0.0466	0.0500	93	74-124			
Dibromofluoromethane	0.0503	0.0500	101	75-131			
1,2-Dichloroethane-D4	0.0497	0.0500	99	63-144			
Toluene-D8	0.0513	0.0500	103	80-117			

Lab Batch #: 804067

Sample: 369409-023 / DL

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 22:32	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags	
Analytes			[D]	Limits	1	
4-Bromofluorobenzene	0.0490	0.0500	98	74-124		
Dibromofluoromethane	0.0516	0.0500	103	75-131		
1,2-Dichloroethane-D4	0.0545	0.0500	109	63-144		
Toluene-D8	0.0496	0.0500	99	80-117		

Lab Batch #: 804067

Sample: 369409-024 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 22:	54 SU	SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags		
Analytes			[D]				
4-Bromofluorobenzene	0.0551	0.0500	110	74-124			
Dibromofluoromethane	0.0452	0.0500	90	75-131			
1,2-Dichloroethane-D4	0.0473	0.0500	95	63-144			
Toluene-D8	0.0564	0.0500	113	80-117			

Lab Batch #: 804067

Sample: 369409-026 / SMP

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/23/10 23:38	8 SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene	0.0500	0.0500	100	74-124		
Dibromofluoromethane	0.0497	0.0500	99	75-131		
1,2-Dichloroethane-D4	0.0490	0.0500	98	63-144		
Toluene-D8	0.0505	0.0500	101	80-117		

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 804067

Project ID: EQ24

Sample: 369409-027 / SMP

Matrix: Water Batch:

Units: mg/L Date Analyzed: 04/24/10 00:00	SURROGATE RECOVERY STUDY						
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags		
Analytes			[D]	%R 74-124			
4-Bromofluorobenzene	0.0492	0.0500	98	74-124			
Dibromofluoromethane	0.0491	0.0500	98	75-131			
1,2-Dichloroethane-D4	0.0500	0.0500	100	63-144			
Toluene-D8	0.0495	0.0500	99	80-117			

Lab Batch #: 804067

Sample: 369409-028 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/24/10 00:22	SU	SURROGATE RECOVERY STUDY						
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags			
Analytes			[D]	74-124 75-131 63-144				
4-Bromofluorobenzene	0.0498	0.0500	100	74-124				
Dibromofluoromethane	0.0494	0.0500	99	75-131	~			
1,2-Dichloroethane-D4	0.0508	0.0500	102	63-144	· · · · · · · · · · · · · · · · · · ·			
Toluene-D8	0.0501	0.0500	100	80-117				

Lab Batch #: 804067

Sample: 369409-029 / SMP

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/24/10 00:44	SURROGATE RECOVERY STUDY						
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags		
Analytes			[D]	Control Limits %R 74-124 75-131 63-144			
4-Bromofluorobenzene	0.0505	0.0500	101	74-124			
Dibromofluoromethane	0.0482	0.0500	96	75-131			
1,2-Dichloroethane-D4	0.0488	0.0500	98	63-144			
Toluene-D8	0.0504	0.0500	101	80-117			

Lab Batch #: 804067

Sample: 369409-029 / DL

Batch: 1

Matrix: Water

Units: mg/L Date Analy	SURROGATE RECOVERY STUDY						
VOAs by SW-846 8 Analytes	3260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0492	0.0500	98	74-124		
Dibromofluoromethane		0.0502	0.0500	100	75-131		
1,2-Dichloroethane-D4		0.0531	0.0500	106	63-144		
Toluene-D8		0.0489	0.0500	98	80-117	·	

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Form 2 - Surrogate Recoveries

Project Name: 25 Paidge Avenue

Work Orders: 369409, Lab Batch #: 804067

Sample: 369409-030 / SMP

Project ID: EQ24

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/24/10 01:28	SURROGATE RECOVERY STUDY						
VOAs by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags		
Analytes	ļ		(2)				
4-Bromofluorobenzene	0.0505	0.0500	101	74-124			
Dibromofluoromethane	0.0498	0.0500	100	75-131			
1,2-Dichloroethane-D4	0.0506	0.0500	101	63-144			
Toluene-D8	0.0528	0.0500	106	80-117			

Lab Batch #: 804536

Sample: 561998-1-BKS / BKS

Batch: 1 Matrix: Water

Units: mg/L Date Analyzed: 04/28/10 11:02 SURROGATE RECOVERY STUDY					
Amount Found [A]	True Amount [B]	Recovery %R	Control Limits %R	Flags	
		[D]			
0.0506	0.0500	101	74-124		
0.0522	0.0500	104	75-131		
0.0514	0.0500	103	63-144		
0.0498	0.0500	100	80-117		
	Amount Found [A] 0.0506 0.0522 0.0514	Amount Found Amount [A] [B] 0.0506 0.0500 0.0522 0.0500 0.0514 0.0500	Amount True Recovery %R [D]	Amount Found [A] True Amount [B] Recovery %R [D] Control Limits %R 0.0506 0.0500 101 74-124 0.0522 0.0500 104 75-131 0.0514 0.0500 103 63-144	

Lab Batch #: 804536

Sample: 561998-1-BLK / BLK

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/28/10 13:13	ECOVERY	STUDY			
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene	0.0500	0.0500	100	74-124	
Dibromofluoromethane	0.0468	0.0500	94	75-131	<u> </u>
1,2-Dichloroethane-D4	0.0492	0.0500	98	63-144	
Toluene-D8	0.0507	0.0500	101	80-117	

Lab Batch #: 804536

Sample: 370094-006 S / MS

Batch: 1

Matrix: Water

Units: mg/L Date Analyzed: 04/28/10 14:24 SURROGATE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
· · · · · · · · · · · · · · · · · · ·					
4-Bromofluorobenzene	0.0495	0.0500	99	74-124	
Dibromofluoromethane	0.0506	0.0500	101	75-131	
1,2-Dichloroethane-D4	0.0525	0.0500	105	63-144	
Toluene-D8	0.0497	0.0500	99	80-117	

^{*} Surrogate outside of Laboratory QC limits

Surrogate Recovery [D] = 100 * A / B

All results are based on MDL and validated for QC purposes.

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Form 2 - Surrogate Recoveries

Project Name: 25 Paidge Avenue

Work Orders: 369409,

Lab Batch #: 804536

Sample: 370094-006 SD / MSD

Project ID: EQ24

Batch: 1 Matrix: Water

Units: mg/L	Date Analyzed: 04/28/10 14:46	SURROGATE RECOVERY STUDY					
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags	
4-Bromofluorobenzene		0.0513	0.0500	103	74-124		
Dibromofluoromethane		0.0501	0.0500	100	75-131		
1,2-Dichloroethane-D4	·	0.0485	0.0500	97	63-144		
Toluene-D8		0.0510	0.0500	102	80-117		

Lab Batch #: 804536

Sample: 369409-024 / DL

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/28/10 15:08	SU	RROGATE R	RECOVERY S	STUDY	
VOA	s by SW-846 8260	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags
4-Bromofluorobenzene	Analytes	0.0495	0.0500	99	74-124	
Dibromofluoromethane		0.0519	0.0500	104	75-131	
1,2-Dichloroethane-D4		0.0525	0.0500	105	63-144	
Toluene-D8		0.0503	0.0500	101	80-117	

Lab Batch #: 804536

Sample: 369409-024 / DL

Batch: 1

Matrix: Water

Units: mg/L	Date Analyzed: 04/28/10 15:30	SURROGATE RECOVERY STUDY							
VOA	s by SW-846 8260 Analytes	Amount Found [A]	True Amount [B]	Recovery %R [D]	Control Limits %R	Flags			
4-Bromofluorobenzene		0.0484	0.0500	97	74-124				
Dibromofluoromethane		0.0508	0.0500	102	75-131				
1,2-Dichloroethane-D4		0.0515	0.0500	103	63-144				
Toluene-D8		0.0509	0.0500	102	80-117				

Surrogate Recovery [D] = 100 * A / B

All results are based on MDL and validated for QC purposes.

^{*} Surrogate outside of Laboratory QC limits

^{**} Surrogates outside limits; data and surrogates confirmed by reanalysis

^{***} Poor recoveries due to dilution



Blank Spike Recovery



Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 803446

Sample: 561312-1-BKS

Matrix: Water

Date Analyzed: 04/20/2010

Date Prepared: 04/20/2010

Analyst: CYE

Reporting	Units:	ug/L	

Reporting Units: ug/L	BLANK/I	BLANK/BLANK SPIKE RECOVERY STUDY					
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags	
Benzene	<5.00	50.0	43.3	87	66-142		
Bromobenzene	<5.00	50.0	46.7	93	75-125		
Bromochloromethane	<5.00	50.0	42.9	86	73-125		
Bromodichloromethane	<5.00	50.0	50.3	101	75-125		
Bromoform	<5.00	50.0	44.7	89	75-125		
Bromomethane	<5.00	50.0	64.1	128	70-130		
MTBE	<5.00	50.0	48.3	97	65-135		
n-Butylbenzene	<5.00	50.0	49.8	100	75-125		
Sec-Butylbenzene	<5.00	50.0	50.3	101	75-125		
tert-Butylbenzene	<5.00	50.0	50.6	101	75-125		
Carbon Tetrachloride	<5.00	50.0	54.0	108	62-125		
Chlorobenzene	<5.00	50.0	47.1	94	60-133		
Chloroethane	<10.0	50.0	51.2	102	70-130		
Chloroform	<5.00	50.0	49.7	99	74-125		
Chloromethane	<10.0	50.0	46.0	92	70-130		
2-Chlorotoluene	<5.00	50.0	46.9	94	73-125		
4-Chlorotoluene	<5.00	50.0	50.3	101	74-125		
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	51.3	103	75-125		
Dibromochloromethane	<5.00	50.0	47.7	95	73-125		
1,2-Dibromo-3-Chloropropane	<5.00	50.0	46.4	93	59-125		
Dibromomethane	<5.00	50.0	44.6	89	69-127		
1,2-Dichlorobenzene	<5.00	50.0	46.1	92	75-125		
1,3-Dichlorobenzene	<5.00	50.0	48.1	96	75-125		
1,4-Dichlorobenzene	<5.00	50.0	46.4	93	75-125		
Dichlorodifluoromethane	<5.00	50.0	56.7	113	70-130		
1,1-Dichloroethane	<5.00	50.0	49.9	100	72-125		
1,2-Dichloroethane	<5.00	50.0	53.2	106	68-127		
1,1-Dichloroethene	<5.00	50.0	43.4	87	59-172		
cis-1,2-Dichloroethene	<5.00	50.0	42.6	85	75-125		
trans-1,2-dichloroethene	<5.00	50.0	44.1	88	75-125		
1,2-Dichloropropane	<5.00	50.0	44.9	90	74-125		
1,3-Dichloropropane	<5.00	50.0	44.4	89	75-125		
		:		· · · · · · · · · · · · · · · · · · ·	···		

Blank Spike Recovery [D] = 100*[C]/[B] . All results are based on MDL and validated for QC purposes.

BRL - Below Reporting Limit

2,2-Dichloropropane

Final Ver. 1.000

110

75-125

<5.00

50.0

54.8





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 803446

Sample: 561312-1-BKS

Matrix: Water

Date Analyzed: 04/20/2010

Date Prepared: 04/20/2010

Analyst: CYE

Date Analyzed: 04/20/2010	Date Prepared: 04/20/2010 Analyst: CYE					
Reporting Units: ug/L	Batch #: 1	BLANK/BLANK SPIKE RECOVERY ST				
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags
1,1-Dichloropropene	<5.00	50.0	44.4	89	75-125	
cis-1,3-Dichloropropene	<5.00	50.0	48.8	98	74-125	
trans-1,3-dichloropropene	<5.00	50.0	51.5	103	66-125	ĺ
Ethylbenzene	<5.00	50.0	47.6	95	75-125	
Hexachlorobutadiene	<5.00	50.0	48.7	97	75-125	
isopropylbenzene	<5.00	50.0	47.5	95	75-125	
Methylene Chloride	<5.00	50.0	40.7	81	75-125	
Naphthalene	<10.0	50.0	45.2	90	75-125	
n-Propylbenzene	<5.00	50.0	49.7	99	75-125	
Styrene	<5.00	50.0	46.1	92	75-125	
1,1,1,2-Tetrachloroethane	<5.00	50.0	49.8	100	72-125	
1,1,2,2-Tetrachloroethane	<5.00	50.0	44.2	88	74-125	
Tetrachloroethylene	<5.00	50.0	46.6	93	71-125	
Toluene	<5.00	50.0	44.4	89	59-139	
1,2,3-Trichlorobenzene	<5.00	50.0	44.4	89	75-137	
1,2,4-Trichlorobenzene	<5.00	50.0	45.7	91	75-135	
1,1,1-Trichloroethane	<5.00	50.0	52.5	105	75-125	
1,1,2-Trichloroethane	<5.00	50.0	44.9	90	75-127	
Trichloroethene	<5.00	50.0	47.7	95	62-137	
Trichlorofluoromethane	<5.00	50.0	62.9	126	67-125	Н
1,2,3-Trichloropropane	<5.00	50.0	48.2	96	75-125	
1,2,4-Trimethylbenzene	<5.00	50.0	51.0	102	75-125	
1,3,5-Trimethylbenzene	<5.00	50.0	51.3	103	70-125	
o-Xylene	<5.00	50.0	45.8	92	75-125	
m,p-Xylenes	<10.0	100	92.2	92	75-125	
Vinyl Chloride	<2.00	50.0	53,3	107	75-125	

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes.
BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 803645

Sample: 561445-1-BKS

Matrix: Water

Date Analyzed: 04/21/2010

Date Prepared: 04/21/2010

Analyst: CYE

Date Analyzed: 04/21/2010 Date Prepared: 04/21/2010 Analyst: CYE						
Reporting Units: ug/L	Batch #: 1 BLANK /BLANK SPIKE RECOVERY					
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags
Benzene	<5.00	50.0	43.5	87	66-142	
Bromobenzene	<5.00	50.0	45.7	91	75-125	
Bromochloromethane	<5,00	50.0	39.8	80	73-125	
Bromodichloromethane	<5.00	50.0	48.3	97	75-125	
Bromoform	<5,00	50.0	44.5	89	75-125	
Bromomethane	<5.00	50.0	57.2	114	70-130	
MTBE	<5.00	50.0	42.6	85	65-135	
n-Butylbenzene	<5.00	50.0	50.9	102	75-125	
Sec-Butylbenzene	<5.00	50.0	50.7	101	75-125	
tert-Butylbenzene	<5.00	50.0	51.6	103	75-125	
Carbon Tetrachloride	<5.00	50.0	53.6	107	62-125	İ
Chlorobenzene	<5.00	50.0	44.8	90	60-133	
Chloroethane	<10.0	50.0	44.6	89	70-130	
Chloroform	<5.00	50.0	47.5	95	74-125	
Chloromethane	<10.0	50.0	41.0	82	70-130	
2-Chlorotoluene	<5.00	50.0	46.5	93	73-125	
4-Chlorotoluene	<5.00	50.0	51.2	102	74-125	
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	52.5	105	75-125	
Dibromochloromethane	<5.00	50.0	47.4	95	73-125	
1,2-Dibromo-3-Chloropropane	<5.00	50.0	54.0	108	59-125	
Dibromomethane	<5.00	50.0	44.1	88	69-127	
1,2-Dichlorobenzene	<5.00	50.0	44.8	90	75-125	7
1,3-Dichlorobenzene	<5.00	50.0	46.7	93	75-125	
1,4-Dichlorobenzene	<5.00	50.0	45.8	92	75-125	
Dichlorodifluoromethane	<5.00	50.0	50.3	101	70-130	
1,1-Dichloroethane	<5.00	50.0	45.9	92	72-125	
1,2-Dichloroethane	<5.00	50.0	55.7	111	68-127	
1,1-Dichloroethene	<5.00	50.0	40.1	80	59-172	
cis-1,2-Dichloroethene	<5.00	50.0	39.4	79	75-125	
trans-1,2-dichloroethene	<5.00	50.0	40.0	80	75-125	
1,2-Dichloropropane	<5.00	50.0	42.9	86	74-125	
1,3-Dichloropropane	<5.00	50.0	44.4	89	75-125	
2,2-Dichloropropane	<5.00	50.0	54.2	108	75-125	

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes.

BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 803645

Sample: 561445-1-BKS

Matrix: Water

Date Analyzed: 04/21/2010

Date Prepared: 04/21/2010

Analyst: CYE

Reporting Units: ug/L Batch #: 1 BLANK/BLAN					ANK SPIKE RECOVERY STUDY				
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags			
1,1-Dichloropropene	<5.00	50.0	44.7	89	75-125				
cis-1,3-Dichloropropene	<5.00	50.0	45.4	91	74-125				
trans-1,3-dichloropropene	<5.00	50.0	52.4	105	66-125				
Ethylbenzene	<5.00	50,0	46.9	94	75-125				
Hexachlorobutadiene	<5.00	50.0	50.7	101	75-125				
isopropylbenzene	<5.00	50.0	47.2	94	75-125				
Methylene Chloride	<5.00	50.0	35.6	71	75-125	L			
Naphthalene	<10.0	50.0	45.0	90	75-125				
n-Propylbenzene	<5.00	50.0	47.7	95	75-125				
Styrene	<5.00	50.0	43.8	88	75-125				
1,1,1,2-Tetrachloroethane	<5.00	50.0	47.8	96	72-125				
1,1,2,2-Tetrachloroethane	<5.00	50.0	43.5	87	74-125				
Tetrachloroethylene	<5.00	50.0	47.1	94	71-125				
Toluene	<5.00	50.0	44.5	89	59-139				
1,2,3-Trichlorobenzene	<5.00	50.0	42.8	86	75-137				
1,2,4-Trichlorobenzene	<5.00	50.0	43.6	87	75-135				
1,1,1-Trichloroethane	<5.00	50.0	52.4	105	75-125				
1,1,2-Trichloroethane	<5.00	50.0	43.7	87	75-127				
Trichloroethene	<5.00	50.0	46.5	93	62-137				
Trichlorofluoromethane	<5.00	50.0	54.8	110	67-125				
1,2,3-Trichloropropane	<5.00	50.0	50,3	101	75-125				
1,2,4-Trimethylbenzene	<5.00	50.0	50.9	102	75-125				
1,3,5-Trimethylbenzene	<5.00	50.0	51.4	103	70-125				
o-Xylene	<5.00	50.0	44.0	88	75-125				
m,p-Xylenes	<10.0	100	87.8	88	75-125				
Vinyl Chloride	<2.00	50.0	43.8	88	75-125				

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes.
BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 803828

Sample: 561560-1-BKS

Matrix: Water

Date Analyzed: 04/22/2010

Date Prepared: 04/22/2010

Analyst: CYE

Reporting Units: ug/L	Batch #: 1	BLANK /BLANK SPIKE RECOVERY ST				
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags
Benzene	<5.00	50.0	51.9	104	66-142	
Bromobenzene	<5.00	50.0	47.8	96	75-125	
Bromochloromethane	<5.00	50.0	52.2	104	73-125	
Bromodichloromethane	<5.00	50.0	49.8	100	75-125	
Bromoform	<5.00	50.0	50.7	101	75-125	
Bromomethane	<5.00	50.0	53.3	107	70-130	
MTBE	<5.00	50.0	58.8	118	65-135	
n-Butylbenzene	<5.00	50.0	52.8	106	75-125	
Sec-Butylbenzene	<5.00	50.0	53.6	107	75-125	
tert-Butylbenzene	<5.00	50.0	52.8	106	75-125	
Carbon Tetrachloride	<5.00	50.0	54.1	108	62-125	
Chlorobenzene	<5.00	50.0	50.9	102	60-133	
Chloroethane	<10.0	50.0	54.0	108	70-130	
Chloroform	<5.00	50.0	51.3	103	74-125	
Chloromethane	<10.0	50.0	61.0	122	70-130	
2-Chlorotoluene	<5.00	50.0	51.0	102	73-125	
4-Chlorotoluene	<5.00	50.0	51.3	103	74-125	
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	53.7	107	75-125	
Dibromochloromethane	<5.00	50.0	51.3	103	73-125	
1,2-Dibromo-3-Chloropropane	<5.00	50.0	57.0	114	59-125	
Dibromomethane	<5.00	50.0	49.4	99	69-127	
1,2-Dichlorobenzene	<5.00	50.0	50.0	100	75-125	
1,3-Dichlorobenzene	<5.00	50.0	50.2	100	75-125	
1,4-Dichlorobenzene	<5.00	50.0	49.9	100	75-125	
Dichlorodifluoromethane	<5.00	50.0	59.4	119	70-130	
1,1-Dichloroethane	<5.00	50.0	53.3	107	72-125	
1,2-Dichloroethane	<5.00	50.0	51.4	103	68-127	
1,1-Dichloroethene	<5.00	50.0	52.3	105	59-172	
cis-1,2-Dichloroethene	<5.00	50.0	52.9	106	75-125	
trans-1,2-dichloroethene	<5.00	50.0	54.8	110	75-125	
1,2-Dichloropropane	<5.00	50.0	50.6	101	74-125	
1,3-Dichloropropane	<5.00	50.0	48.2	96	75-125	
2,2-Dichloropropane	<5.00	50.0	58.2	116	75-125	

Blank Spike Recovery [D] = 100*[C]/[B]All results are based on MDL and validated for QC purposes.

BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 803828

Sample: 561560-1-BKS

Matrix: Water

Date Analyzed: 04/22/2010

Date Prepared: 04/22/2010

Analyst: CYE

Reporting Units: ug/L	Batch #: 1	BLANK/BLANK SPIKE RECOVERY STUDY						
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags		
1,1-Dichloropropene	<5.00	50.0	49.7	99	75-125			
cis-1,3-Dichloropropene	<5.00	50.0	50.7	101	74-125	-		
Ethylbenzene	<5.00	50.0	52.1	104	75-125			
Hexachlorobutadiene	<5.00	50.0	50.3	101	75-125			
isopropylbenzene	<5.00	50.0	53.8	108	75-125			
Methylene Chloride	<5.00	50.0	52.0	104	75-125			
Naphthalene	<10.0	50.0	56.2	112	75-125			
n-Propylbenzene	<5.00	50.0	52.4	105	75-125			
Styrene	<5.00	50.0	51.8	104	75-125			
1,1,1,2-Tetrachloroethane	<5.00	50.0	52.0	104	72-125			
Tetrachloroethylene	<5.00	50.0	49.5	99	71-125			
Toluene	<5.00	50.0	50.1	100	59-139			
1,2,3-Trichlorobenzene	<5.00	50.0	56.0	112	75-137			
1,2,4-Trichlorobenzene	<5.00	50.0	52.6	105	75-135			
1,1,1-Trichloroethane	<5.00	50.0	53.0	106	75-125			
1,1,2-Trichloroethane	<5.00	50.0	50.7	101	75-127			
Trichloroethene	<5.00	50.0	50,9	102	62-137			
Trichlorofluoromethane	<5,00	50.0	59.5	119	67-125			
1,2,3-Trichloropropane	<5.00	50.0	54.2	108	75-125			
1,2,4-Trimethylbenzene	<5.00	50.0	52.6	105	75-125			
1,3,5-Trimethylbenzene	<5.00	50.0	52.3	105	70-125			
o-Xylene	<5.00	50.0	53.4	107	75-125			
m,p-Xylenes	<10.0	100	104	104	75-125			
Vinyl Chloride	<2.00	50.0	52.7	105	75-125			

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes.
BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 804058

Sample: 561728-1-BKS

Matrix: Water

Date Analyzed: 04/26/2010

Date Prepared: 04/26/2010

Analyst: CYE

Reporting Units: ug/L	Batch #: 1	BLANK/I	STUDY			
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags
Benzene	<5.00	50.0	46.2	92	66-142	
Bromobenzene	<5.00	50.0	51.6	103	75-125	
Bromochloromethane	<5.00	50.0	48.3	97	73-125	
Bromodichloromethane	<5.00	50.0	56.6	113	75-125	
Bromoform	<5.00	50.0	58.7	117	75-125	
Bromomethane	<5.00	50.0	38.5	77	70-130	
MTBE	<5.00	50.0	49.1	98	65-135	
n-Butylbenzene	<5.00	50,0	50.0	100	75-125	
Sec-Butylbenzene	<5.00	50.0	53.9	108	75-125	
tert-Butylbenzene	<5.00	50.0	54.7	109	75-125	
Carbon Tetrachloride	<5.00	50.0	48.9	98	62-125	
Chlorobenzene	<5.00	50.0	52.6	105	60-133	
Chloroethane	<10.0	50.0	40.4	81	70-130	
Chloroform	<5.00	50.0	49.4	99	74-125	
Chloromethane	<10.0	50.0	38.9	78	70-130	
2-Chlorotoluene	<5.00	50.0	51.5	103	73-125	
4-Chlorotoluene	<5.00	50.0	50.7	101	74-125	
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	52.6	105	75-125	
Dibromochloromethane	<5.00	50.0	60.6	121	73-125	
1,2-Dibromo-3-Chloropropane	<5.00	50.0	51.4	103	59-125	
Dibromomethane	<5.00	50.0	48.5	97	69-127	
1,2-Dichlorobenzene	<5.00	50.0	52.1	104	75-125	
1,3-Dichlorobenzene	<5.00	50.0	52.4	105	75-125	
1,4-Dichlorobenzene	<5.00	50.0	51.2	102	75-125	
Dichlorodifluoromethane	<5.00	50.0	46.2	92	70-130	
1,1-Dichloroethane	<5.00	50.0	49.9	100	72-125	
1,2-Dichloroethane	<5.00	50.0	48.5	97	68-127	
1,1-Dichloroethene	<5.00	50.0	42.7	85	59-172	
cis-1,2-Dichloroethene	<5.00	50.0	46.0	92	75-125	
trans-1,2-dichloroethene	<5.00	50.0	42.2	84	75-125	
1,2-Dichloropropane	<5.00	50.0	51.4	103	74-125	
1,3-Dichloropropane	<5,00	50.0	50.2	100	75-125	
2,2-Dichloropropane	<5.00	50.0	49.5	99	75-125	

Blank Spike Recovery [D] = 100*[C]/[B]All results are based on MDL and validated for QC purposes.

BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 804058

Sample: 561728-1-BKS

Matrix: Water

Date Analyzed: 04/26/2010

Date Prepared: 04/26/2010

Analyst: CYE

Date Analyzed: 04/26/2010	Date Prepared: 04/26/2010 Analyst: CYE								
Reporting Units: ug/L	Batch #: 1	BLANK /	BLANK/BLANK SPIKE RECOVERY STUDY						
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags			
1,1-Dichloropropene	<5.00	50.0	40.8	82	75-125				
cis-1,3-Dichloropropene	<5.00	50.0	57.1	114	74-125				
trans-1,3-dichloropropene	<5.00	50.0	55.9	112	66-125				
Ethylbenzene	<5.00	50.0	49.1	98	75-125				
Hexachlorobutadiene	<5.00	50.0	51.6	103	75-125				
isopropylbenzene	<5.00	50.0	49.7	99	75-125				
Methylene Chloride	<5.00	50.0	44.8	90	75-125				
Naphthalene	<10.0	50.0	50.3	101	75-125				
n-Propylbenzene	<5.00	50.0	51.5	103	75-125				
Styrene	<5.00	50.0	51.0	102	75-125				
1,1,1,2-Tetrachloroethane	<5.00	50.0	52.3	105	72-125				
1,1,2,2-Tetrachloroethane	<5.00	50.0	55.1	110	74-125				
Tetrachloroethylene	<5.00	50.0	47.5	95	71-125				
Toluene	<5.00	50.0	48.9	98	59-139				
1,2,3-Trichlorobenzene	<5.00	50.0	52.1	104	75-137				
1,2,4-Trichlorobenzene	<5.00	50.0	50.9	102	75-135				
1,1,1-Trichloroethane	<5.00	50.0	45.2	90	75-125				
1,1,2-Trichloroethane	<5.00	50.0	53.4	107	75-127				
Trichloroethene	<5.00	50.0	47.0	94	62-137	•			
Trichlorofluoromethane	<5.00	50.0	50.4	101	67-125				
1,2,3-Trichloropropane	<5.00	50.0	54.9	110	75-125				
1,2,4-Trimethylbenzene	<5.00	50.0	51.6	103	75-125				
1,3,5-Trimethylbenzene	<5.00	50.0	51.3	103	70-125				
o-Xylene	<5.00	50.0	50.4	101	75-125				
m,p-Xylenes	<10.0	100	99.9	100	75-125				
Vinyl Chloride	<2.00	50.0	39.1	78	75-125				

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes.
BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 804067

Sample: 561731-1-BKS

Matrix: Water

Date Analyzed: 04/23/2010

Date Prepared: 04/23/2010

Analyst: CYE

Reporting Units: ug/L	Batch #: 1	BLANK/BLANK SPIKE RECOVERY STUDY

VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags
Benzene	<5.00	50.0	48.7	97	66-142	
Bromobenzene	<5.00	50.0	53.1	106	75-125	
Bromochloromethane	<5.00	50.0	51.3	103	73-125	
Bromodichloromethane	<5.00	50.0	55.1	110	75-125	
Bromoform	<5.00	50.0	55.9	112	75-125	
Bromomethane	<5.00	50.0	46.6	93	70-130	
MTBE	<5.00	50.0	54.5	109	65-135	
n-Butylbenzene	<5.00	50.0	52.1	104	75-125	
Sec-Butylbenzene	<5.00	50.0	54.4	109	75-125	
tert-Butylbenzene	<5.00	50.0	55.0	110	75-125	
Carbon Tetrachloride	<5.00	50.0	50.9	102	62-125	
Chlorobenzene	<5.00	50.0	53.7	107	60-133	
Chloroethane	<10.0	50.0	46.8	94	70-130	
Chloroform	<5.00	50.0	50.6	101	74-125	
Chloromethane	<10.0	50.0	44.3	89	70-130	
2-Chlorotoluene	<5.00	50.0	51.8	104	73-125	
4-Chlorotoluene	<5.00	50.0	52.9	106	74-125	
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	53.6	107	75-125	
Dibromochloromethane	<5.00	50.0	56.6	113	73-125	
1,2-Dibromo-3-Chloropropane	<5.00	50.0	52.3	105	59-125	
Dibromomethane	<5.00	50.0	50.0	100	69-127	
1,2-Dichlorobenzene	<5.00	50.0	52.3	105	75-125	
1,3-Dichlorobenzene	<5.00	50.0	53.5	107	75-125	
1,4-Dichlorobenzene	<5.00	50.0	52.1	104	75-125	
Dichlorodifluoromethane	<5.00	50.0	50.1	100	70-130	
1,1-Dichloroethane	<5.00	50.0	53.3	107	72-125	
1,2-Dichloroethane	<5.00	50.0	48.6	97	68-127	
1,1-Dichloroethene	<5.00	50.0	49.3	99	59-172	
cis-1,2-Dichloroethene	<5.00	50.0	48.9	98	75-125	
trans-1,2-dichloroethene	<5.00	50.0	49.3	99	75-125	
1,2-Dichloropropane	<5.00	50.0	51.5	103	74-125	
1,3-Dichloropropane	<5.00	50.0	51.7	103	75-125	
2,2-Dichloropropane	<5.00	50.0	54.3	109	75-125	

Blank Spike Recovery [D] = 100*[C]/[B]All results are based on MDL and validated for QC purposes.

BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 804067

Sample: 561731-1-BKS

Matrix: Water

Date Analyzed: 04/23/2010

Date Prepared: 04/23/2010

Analyst: CYE

Date Analyzed: 04/23/2010	Date Prepared: 04/23/2010 Analyst: CYE								
Reporting Units: ug/L	Batch #: 1	BLANK/BLANK SPIKE RECOVERY STUDY							
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags			
1,1-Dichloropropene	<5.00	50.0	43.8	88	75-125				
cis-1,3-Dichloropropene	<5.00	50.0	53.9	108	74-125				
trans-1,3-dichloropropene	<5.00	50.0	54.6	109	66-125				
Ethylbenzene	<5.00	50.0	50.8	102	75-125				
Hexachlorobutadiene	<5.00	50.0	54.9	110	75-125				
isopropylbenzene	<5.00	50.0	52.0	104	75-125				
Methylene Chloride	<5.00	50.0	49.9	100	75-125	· · · · · · · · · · · · · · · · · · ·			
Naphthalene	<10.0	50.0	55.8	112	75-125				
n-Propylbenzene	<5.00	. 50.0	52.8	106	75-125				
Styrene	<5.00	50.0	52.1	104	75-125				
1,1,1,2-Tetrachloroethane	<5.00	50.0	52.1	104	72-125				
1,1,2,2-Tetrachloroethane	<5.00	50.0	54.7	109	74-125				
Tetrachloroethylene	<5.00	50.0	51.6	103	71-125				
Toluene	<5.00	50.0	49.5	99	59-139				
1,2,3-Trichlorobenzene	<5.00	50.0	56.4	113	75-137				
1,2,4-Trichlorobenzene	<5.00	50.0	55.4	111	75-135				
1,1,1-Trichloroethane	<5.00	50.0	47,9	96	75-125				
1,1,2-Trichloroethane	<5.00	50.0	53.3	107	75-127				
Trichloroethene	<5.00	50.0	49.4	99	62-137				
Trichlorofluoromethane	<5.00	50.0	56.0	112	67-125				
1,2,3-Trichloropropane	<5.00	50.0	55.6	111	75-125				
1,2,4-Trimethylbenzene	<5.00	50.0	52.3	105	75-125				
1,3,5-Trimethylbenzene	<5.00	50.0	52.0	104	70-125				
o-Xylene	<5.00	50.0	52.7	105	75-125				
m,p-Xylenes	<10.0	100	104	104	75-125	-			
Vinyl Chloride	<2.00	50.0	44.6	89	75-125				

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes. BRL - Below Reporting Limit

Final Ver. 1.000





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 804536

Sample: 561998-1-BKS

Matrix: Water

Date Analyzed: 04/28/2010

Date Prepared: 04/28/2010

Analyst: CYE

Reporting U	nits: ug/L
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o z repartu.		
Batch #:	1	BLANK/BLANK SPIKE RECOVERY STUDY

Reporting Onto: ug/L	Daten #. 1	BEATTR/BEATTRE RECOVERT 510					
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags	
Benzene	<5.00	50.0	52.0	104	66-142		
Bromobenzene	<5.00	50.0	51.6	103	75-125		
Bromochloromethane	<5.00	50.0	53.9	108	73-125		
Bromodichloromethane	<5.00	50.0	58.3	117	75-125		
Bromoform	<5.00	50.0	60.6	121	75-125		
Bromomethane	<5.00	50.0	45.3	91	70-130		
MTBE	<5.00	50.0	56.4	113	65-135		
n-Butylbenzene	<5.00	50.0	52.8	106	75-125		
Sec-Butylbenzene	<5.00	50.0	55.1	110	75-125		
tert-Butylbenzene	<5.00	50.0	55,6	111	75-125		
Carbon Tetrachloride	<5.00	50.0	53.8	108	62-125		
Chlorobenzene	<5.00	50.0	54.1	108	60-133	1	
Chloroethane	<10.0	50.0	47.5	95	70-130		
Chloroform	<5.00	50.0	53.1	106	74-125		
Chloromethane	<10.0	50.0	48.8	98	70-130		
2-Chlorotoluene	<5.00	50.0	52.5	105	73-125		
4-Chlorotoluene	<5.00	50.0	51.9	104	74-125		
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	54.7	109	75-125		
Dibromochloromethane	<5.00	50.0	59.9	120	73-125		
1,2-Dibromo-3-Chloropropane	<5.00	50.0	61.3	123	59-125		
Dibromomethane	<5.00	50.0	52.2	104	69-127		
1,2-Dichlorobenzene	<5.00	50.0	52.4	105	75-125		
1,3-Dichlorobenzene	<5.00	50.0	53.3	107	75-125		
1,4-Dichlorobenzene	<5.00	50.0	51.5	103	75-125		
Dichlorodifluoromethane	<5.00	50.0	52.5	105	70-130	,	
1,1-Dichloroethane	<5.00	50.0	55.0	110	72-125		
1,2-Dichloroethane	<5.00	50.0	51.7	103	68-127		
1,1-Dichloroethene	<5.00	50.0	49.8	100	59-172		
cis-1,2-Dichloroethene	<5.00	50.0	50.6	101	75-125		
trans-1,2-dichloroethene	<5.00	50.0	50.3	101	75-125		
1,2-Dichloropropane	<5.00	50,0	53.0	106	74-125		
1,3-Dichloropropane	<5.00	50.0	52.5	105	75-125		
2,2-Dichloropropane	<5.00	50.0	58.6	117	75-125		

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes.

BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue

Work Order #: 369409

Project ID:

EQ24

Lab Batch #: 804536

Sample: 561998-1-BKS

Matrix: Water

Date Analyzed: 04/28/2010

Date Prepared: 04/28/2010

Analyst: CYE

Reporting Units: ug/L Batch #: 1 BLANK/BLANK SPIKE RECOVER						STUDY
VOAs by SW-846 8260 Analytes	Blank Result [A]	Spike Added [B]	Blank Spike Result [C]	Blank Spike %R [D]	Control Limits %R	Flags
1,1-Dichloropropene	<5.00	50.0	45.6	91	75-125	
cis-1,3-Dichloropropene	<5,00	50.0	58.4	117	74-125	
trans-1,3-dichloropropene	<5.00	50.0	57,4	115	66-125	
Ethylbenzene	<5.00	50.0	51.3	103	75-125	
Hexachlorobutadiene	<5.00	50.0	57.1	114	75-125	
isopropylbenzene	<5.00	50.0	52.9	106	75-125	
Methylene Chloride	<5.00	50.0	61.9	124	75-125	
Naphthalene	<10.0	50.0	57.1	114	75-125	
n-Propylbenzene	<5.00	50.0	52.5	105	75-125	
Styrene	<5.00	50.0	52.0	104	75-125	
1,1,1,2-Tetrachloroethane	<5.00	50.0	54.0	108	72-125	
1,1,2,2-Tetrachloroethane	<5.00	50.0	55.7	111	74-125	
Tetrachloroethylene	<5,00	50.0	52.1	104	71-125	
Toluene	<5.00	50.0	51.1	102	59-139	
1,2,3-Trichlorobenzene	<5.00	50.0	55.9	112	75-137	
1,2,4-Trichlorobenzene	<5.00	50.0	56.2	112	75-135	
1,1,1-Trichloroethane	<5.00	50.0	50.2	100	75-125	
1,1,2-Trichloroethane	<5.00	50.0	53.3	107	75-127	
Trichloroethene	<5.00	50.0	49.2	98	62-137	
Trichlorofluoromethane	<5.00	50.0	59.0	118	67-125	
1,2,3-Trichloropropane	<5.00	50.0	57.4	115	75-125	
1,2,4-Trimethylbenzene	<5.00	50.0	53.1	106	75-125	
1,3,5-Trimethylbenzene	<5.00	50.0	53.4	107	70-125	
o-Xylene	<5.00	50.0	53.6	107	75-125	
m,p-Xylenes	<10,0	100	104	104	75-125	
Vinyl Chloride	<2.00	50.0	45.9	92	75-125	

Blank Spike Recovery [D] = 100*[C]/[B]
All results are based on MDL and validated for QC purposes.
BRL - Below Reporting Limit





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 803446 Date Analyzed: 04/20/2010 QC- Sample ID: 369409-001 S **Date Prepared:** 04/20/2010

Batch #:

Matrix: Water

Analyst: CYE

Reporting Units: ug/L MATRIX SPIKE / MATRIX SPIKE DUPLICATE RECOVERY STUDY											
VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Fla
Benzene	<5.00	50.0	43.1	86	50.0	44.3	89	3	66-142	21	
Bromobenzene	<5.00	50.0	46.0	92	50.0	44.9	90	2	75-125	20	
Bromochloromethane	<5.00	50.0	45.0	90	50.0	48.0	96	6	73-125	20	
Bromodichloromethane	<5.00	50.0	51.8	104	50.0	52.3	105	1	75-125	20	
Bromoform	<5.00	50.0	45.9	92	50.0	47.0	94	2	75-125	20	
Bromomethane	<5.00	50.0	59.4	119	50.0	63.4	127	7	70-130	20	
MTBE	<5.00	50.0	50.5	101	50.0	55.5	111	9	65-135	20	<u> </u>
n-Butylbenzene	<5.00	50.0	47.2	94	50.0	48.8	98	3	75-125	20	
Sec-Butylbenzene	<5.00	50.0	48.6	97	50.0	48.5	97	0	75-125	20	İ
tert-Butylbenzene	<5.00	50.0	49.6	99	50.0	48.1	96	3	75-125	20	
Carbon Tetrachloride	<5.00	50.0	55.1	110	50.0	55.7	111	1	62-125	20	
Chlorobenzene	<5.00	50.0	46.3	93	50.0	46.4	93	0	60-133	21	
Chloroethane	<10.0	50.0	42.9	86	50.0	48.8	98	13	70-130	20	
Chloroform	7.96	50.0	59.9	104	50.0	63.4	111	6	74-125	20	
Chloromethane	<10.0	50.0	42.0	84	50.0	44.8	90	6	70-130	20	
2-Chlorotoluene	<5.00	50.0	44.7	89	50.0	44.6	89	0	73-125	20	
4-Chlorotoluene	<5.00	50.0	49.7	99	50.0	49.5	99	0	74-125	20	
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	50.1	100	50.0	50.2	100	0	75-125	20	
Dibromochloromethane	<5.00	50.0	48.8	98	50.0	48.5	97	1	73-125	20	
1,2-Dibromo-3-Chloropropane	<5.00	50.0	45.8	92	50.0	48.8	98	6	59-125	28	Г
Dibromomethane	<5.00	50.0	47.0	94	50.0	45.8	92	3	69-127	23	
1,2-Dichlorobenzene	<5.00	50.0	45.8	92	50.0	47.6	95	4	75-125	20	
1,3-Dichlorobenzene	<5.00	50.0	47.6	95	50.0	47.5	95	0	75-125	20	\top

Matrix Spike Percent Recovery [D] = 100*(C-A)/BRelative Percent Difference RPD = 200*[(C-F)/(C+F)]

Matrix Spike Duplicate Percent Recovery [G] = 100*(F-A)/E

ND = Not Detected, J = Present Below Reporting Limit, B = Present in Blank, NR = Not Requested, I = Interference, NA = Not ApplicableN = See Narrative, EQL = Estimated Quantitation Limit





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 803446

QC- Sample ID: 369409-001 S

Batch #: 1 Matrix: Water

Date Analyzed: 04/20/2010

Date Prepared: 04/20/2010

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
1,4-Dichlorobenzene	<5.00	50.0	45.8	92	50.0	45.6	91	0	75-125	20	·
Dichlorodifluoromethane	<5.00	50.0	50.2	100	50.0	53.8	108	7	70-130	23	
1,1-Dichloroethane	<5.00	50.0	50.1	100	50.0	53.7	107	7	72-125	20	
1,2-Dichloroethane	<5.00	50.0	55.1	110	50.0	57.3	115	4	68-127	20	
1,1-Dichloroethene	<5.00	50.0	40.9	82	50.0	45.4	91	10	59-172	22	
cis-1,2-Dichloroethene	<5.00	50.0	42.1	84	50.0	44.0	88	4	75-125	20	
trans-1,2-dichloroethene	<5.00	50.0	42.0	84	50.0	45.6	91	8	75-125	20	
1,2-Dichloropropane	<5.00	50.0	45.8	92	50.0	46.5	93	2	74-125	20	
1,3-Dichloropropane	<5.00	50.0	43.8	88	50.0	43.3	87	1	75-125	20	
2,2-Dichloropropane	<5.00	50.0	54.1	108	50.0	58.9	118	8	75-125	20	
1,1-Dichloropropene	<5.00	50.0	41.6	83	50.0	43.6	87	5	75-125	20	
cis-1,3-Dichloropropene	<5.00	50.0	48.9	98	50,0	47.6	95	3	74-125	20	
trans-1,3-dichloropropene	<5.00	50.0	49.9	100	50.0	47.8	96	4	66-125	20	
Ethylbenzene	<5.00	50.0	46.6	93	50.0	47.2	94	1	75-125	20	
Hexachlorobutadiene	<5.00	50.0	46.1	92	50.0	48.8	98	6	75-125	20	
isopropylbenzene	<5.00	50.0	47.0	94	50.0	49.4	99	5	75-125	20	
Methylene Chloride	<5.00	50.0	40.4	81	50.0	43.9	88	8	75-125	35	
Naphthalene	<10.0	50.0	45.5	91	50.0	46.4	93	2	75-125	20	
n-Propylbenzene	<5.00	50.0	47.5	95	50.0	47.1	94	1	75-125	20	
Styrene	<5.00	50.0	46.3	93	50,0	47.5	95	3	75-125	51	
1,1,1,2-Tetrachloroethane	<5.00	50.0	48.7	97	50.0	50.5	101	4	72-125	20	
1,1,2,2-Tetrachloroethane	<5.00	50.0	43,1	86	50.0	43.2	86	0	74-125	31	
Tetrachloroethylene	<5.00	50.0	42.6	85	50.0	44.3	89	4	71-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 803446

QC- Sample ID: 369409-001 S

Batch #: Matrix: Water

Date Analyzed: 04/20/2010

Date Prepared: 04/20/2010

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260	Parent Sample Result	Spike Added	Spiked Sample Result [C]	Spiked Sample %R	Spike Added	Duplicate Spiked Sample Result [F]	Spiked Dup. %R	RPD %	Control Limits %R	Control Limits %RPD	Flag
Analytes	[A]	[B]		[D]	[E]		[G]				
Toluene	<5.00	50.0	42.3	85	50.0	42.7	85	1	59-139	21	
1,2,3-Trichlorobenzene	<5.00	50.0	44.6	89	50.0	44.2	88	1	75-137	20	
1,2,4-Trichlorobenzene	<5.00	50.0	44.5	89	50.0	46.4	93	4	75-135	20	
1,1,1-Trichloroethane	<5.00	50.0	51.3	103	50.0	56.3	113	9	75-125	20	
1,1,2-Trichloroethane	<5.00	50.0	44.1	88	50.0	43.5	87	1	75-127	20	
Trichloroethene	<5.00	50.0	46.3	93	50.0	47.1	94	2	62-137	24	
Trichlorofluoromethane	<5.00	50.0	56.8	114	50.0	62.1	124	9	67-125	20	
1,2,3-Trichloropropane	<5.00	50.0	49.4	99	50.0	48.7	97	1	75-125	20	
1,2,4-Trimethylbenzene	<5.00	50.0	50.2	100	50.0	50.6	101	1	75-125	20	
1,3,5-Trimethylbenzene	<5.00	50.0	50.0	100	50.0	50.1	100	0	70-125	20	
o-Xylene	<5.00	50.0	45.9	92	50.0	47.1	94	3	75-125	20	
m,p-Xylenes	<10.0	100	89.8	90	100	92.2	92	3	75-125	20	
Vinyl Chloride	<2.00	50.0	46.2	92	50.0	49.8	100	8	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 803645

QC- Sample ID: 369409-003 S

Batch #: Matrix: Water

Date Analyzed: 04/21/2010

Date Prepared: 04/21/2010

Analyst: CYE

Reporting Units: ug/L	<u> </u>	MATRIX SPIKE / MATRIX SPIKE DUPLICATE RECOVERY STUDY										
VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag	
Benzene	122	50.0	156	68	50.0	157	70	1	66-142	21		
Bromobenzene	<5.00	50.0	46.1	92	50.0	45.5	91	1	75-125	20		
Bromochloromethane	<5.00	50.0	43.9	88	50.0	43.9	88	0	73-125	20		
Bromodichloromethane	<5.00	50.0	52.5	105	50.0	51.7	103	2	75-125	20		
Bromoform	<5.00	50.0	46.2	92	50.0	47.1	94	2	75-125	20		
Bromomethane	<5.00	50.0	50.7	101	50.0	51.8	104	2	70-130	20		
MTBE	<5,00	50.0	52.4	105	50.0	52.7	105	1	65-135	20		
n-Butylbenzene	10.9	50.0	59.7	98	50.0	57.8	94	3	75-125	20		
Sec-Butylbenzene	7.19	50.0	56.1	98	50.0	54.2	94	3	75-125	20		
tert-Butylbenzene	<5.00	50.0	50.7	101	50.0	50.1	100	1	75-125	20		
Carbon Tetrachloride	<5.00	50.0	55.1	110	50.0	55.8	112	1	62-125	20		
Chlorobenzene	<5.00	50.0	44.9	90	50.0	45.6	91	2	60-133	21		
Chloroethane	<10.0	50.0	42.1	84	50.0	44.6	89	6	70-130	20		
Chloroform	<5.00	50.0	52.6	105	50.0	52.0	104	1	74-125	20		
Chloromethane	<10.0	50.0	35.9	72	50.0	36.5	73	2	70-130	20	<u> </u>	
2-Chlorotoluene	<5.00	50.0	45.1	90	50.0	45.0	90	0	73-125	20	<u> </u>	
4-Chlorotoluene	<5.00	50.0	50.4	101	50:0	49.8	100	1	74-125	20		
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	51.4	103	50.0	49.4	99	4	75-125	20	i	
Dibromochloromethane	<5.00	50.0	49.1	98	50.0	50.0	100	2	73-125	20		
1,2-Dibromo-3-Chloropropane	<5.00	50.0	51.4	103	50.0	53.4	107	4	59-125	28	<u> </u>	
Dibromomethane	<5,00	50.0	45.0	90	50.0	45.9	92	2	69-127	. 23		
1,2-Dichlorobenzene	<5.00	50.0	46.4	93	50.0	45.8	92	1	75-125	20		
1,3-Dichlorobenzene	<5.00	50.0	47.0	94	50.0	46.6	93	1	75-125	20	 	

Matrix Spike Percent Recovery [D] = 100*(C-A)/BRelative Percent Difference RPD = 200*[(C-F)/(C+F)]

Matrix Spike Duplicate Percent Recovery [G] = 100*(F-A)/E

ND = Not Detected, J = Present Below Reporting Limit, B = Present in Blank, NR = Not Requested, I = Interference, NA = Not Applicable N = See Narrative, EQL = Estimated Quantitation Limit





Project Name: 25 Paidge Avenue



Work Order #: 369409

Lab Batch ID: 803645

QC-Sample ID: 369409-003 S

Project ID: EQ24 Matrix: Water

Date Analyzed: 04/21/2010

Date Prepared: 04/21/2010

Batch #:

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
1,4-Dichlorobenzene	<5.00	50.0	45.9	92	50.0	45.3	91	1	75-125	20	
Dichlorodifluoromethane	<5.00	50.0	48,3	97	50.0	47.6	95	1	70-130	23	
1,1-Dichloroethane	<5.00	50.0	50.0	100	50.0	50.1	100	0	72-125	20	
1,2-Dichloroethane	<5.00	50.0	61.1	122	50.0	61.5	123	1	68-127	20	
1,1-Dichloroethene	<5,00	50.0	41.1	82	50.0	41.4	83	1	59-172	22	
cis-1,2-Dichloroethene	<5.00	50.0	42.3	85	50.0	41.0	82	3	75-125	20	
trans-1,2-dichloroethene	<5.00	50.0	40,6	81	50.0	42.5	85	5	75-125	20	
1,2-Dichloropropane	<5.00	50.0	46.1	92	50.0	46.1	92	0	74-125	20	
1,3-Dichloropropane	<5.00	50.0	43.2	86	50.0	44.1	88	2	75-125	20	
2,2-Dichloropropane	<5.00	50.0	54.6	109	50.0	55.8	112	2	75-125	20	
1,1-Dichloropropene	<5.00	50.0	42.0	84	50.0	40.2	80	4	75-125	20	
cis-1,3-Dichloropropene	<5.00	50.0	48.6	97	50.0	47.5	95	2	74-125	20	
trans-1,3-dichloropropene	<5.00	50.0	49.2	98	50.0	48.9	98	1	66-125	20	
Ethylbenzene	<5.00	50.0	50,2	100	50.0	49.8	100	1	75-125	20	
Hexachlorobutadiene	<5.00	50.0	51.2	102	50.0	47.9	96	7	75-125	20	
isopropylbenzene	63.1	50.0	106	86	50.0	106	86	0	75-125	20	
Methylene Chloride	<5.00	50.0	40.3	81	50.0	41.6	83	3	75-125	35	
Naphthalene	<10.0	50.0	50.6	101	50.0	50.0	100	1	75-125	20	
n-Propylbenzene	107	50.0	148	82	50.0	143	72	3	75-125	20	Х
Styrene	<5.00	50.0	45.1	90	50.0	45.4	91	1	75-125	51	
1,1,1,2-Tetrachloroethane	<5.00	50.0	49.7	99	50.0	50.4	101	1	72-125	20	
1,1,2,2-Tetrachloroethane	<5.00	50.0	45.5	91	50.0	44.5	89	2	74-125	31	
Tetrachloroethylene	<5.00	50.0	43.0	86	50.0	43.6	87	1	71-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)| Matrix Spike Duplicate Percent Recovery [G] = 100*(F-A)/E

ND = Not Detected, J = Present Below Reporting Limit, B = Present in Blank, NR = Not Requested, I = Interference, NA = Not ApplicableN = See Narrative, EQL = Estimated Quantitation Limit





Project Name: 25 Paidge Avenue



Work Order #: 369409 Lab Batch ID: 803645

OC-Sample ID: 369409-003 S

Project ID: EQ24

Matrix: Water

Date Analyzed: 04/21/2010

Batch #:

Date Prepared: 04/21/2010

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Toluene	<5.00	50.0	43.7	87	50.0	44.0	88	1	59-139	21	
1,2,3-Trichlorobenzene	<5.00	50.0	45.8	92	50.0	46.3	93	1	75-137	20	
1,2,4-Trichlorobenzene	<5.00	50.0	47.0	94	50.0	45.7	91	3	75-135	20	
1,1,1-Trichloroethane	<5.00	50.0	52.7	105	50.0	52.5	105	0	75-125	20	
1,1,2-Trichloroethane	<5.00	50.0	45.0	90	50.0	45.5	91	1	75-127	20	
Trichloroethene	<5.00	50.0	46.8	94	50.0	47.8	96	2	62-137	24	
Trichlorofluoromethane	<5.00	50.0	55.6	111	50.0	56.0	112	1	67-125	20	
1,2,3-Trichloropropane	<5.00	50.0	49.9	100	50.0	49.1	98	2	75-125	20	
1,2,4-Trimethylbenzene	<5.00	50.0	51.7	103	50.0	50.2	100	3	75-125	20	
1,3,5-Trimethylbenzene	<5.00	50.0	50.6	101	50.0	49.3	99	3	70-125	20	
o-Xylene	<5.00	50.0	46.2	92	50,0	47.5	95	3	75-125	20	
m,p-Xylenes	<10.0	100	93.5	94	100	94.5	95	1	75-125	20	
Vinyl Chloride	<2.00	50.0	40.7	81	50.0	40.9	82	0	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 803828

QC-Sample ID: 369409-004 S

Batch #:

Matrix: Water

Date Analyzed: 04/22/2010

Date Prepared: 04/22/2010

Analyst: CYE

Reporting Units: ug/L		M	ATRIX SPIK	E / MAT	RIX SPI	KE DUPLICA	TE REC	OVERY S	STUDY		
VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Benzene	<5.00	50.0	52.1	104	50.0	49.7	99	5	66-142	21	
Bromobenzene	<5.00	50.0	50.1	100	50.0	51.2	102	2	75-125	20	
Bromochloromethane	<5.00	50.0	53.3	107	50.0	53.1	106	0	73-125	20	
Bromodichloromethane	<5.00	50.0	53.4	107	50.0	53.1	106	1	75-125	20	
Bromoform	<5.00	50.0	52.4	105	50.0	55.7	111	6	75-125	20	
Bromomethane	<5,00	50.0	55.3	111	50.0	46.4	93	18	70-130	20	
MTBE	<5.00	50.0	61.9	124	50.0	60.1	120	3	65-135	20	
n-Butylbenzene	<5.00	50.0	52.0	104	50.0	50.1	100	4	75-125	20	
Sec-Butylbenzene	<5.00	50.0	53,0	106	50.0	51.4	103	3	75-125	20	
tert-Butylbenzene	<5.00	50.0	53.0	106	50.0	53.6	107	1	75-125	20	
Carbon Tetrachloride	<5.00	50.0	50.4	101	50.0	48.9	98	3	62-125	20	
Chlorobenzene	<5.00	50.0	53.1	106	50.0	52.4	105	1	60-133	21	
Chloroethane	<10.0	50.0	54.8	110	50.0	48.2	96	13	70-130	20	
Chloroform	<5.00	50.0	53.3	107	50.0	51.9	104	3	74-125	20	
Chloromethane	<10.0	50.0	59.7	119	50.0	53.1	106	12	70-130	20	
2-Chlorotoluene	<5.00	50.0	51.0	102	50.0	50.7	101	1	73-125	20	
4-Chlorotoluene	<5.00	50.0	53.4	107	50.0	51.7	103	3	74-125	20	
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	54.3	109	50.0	52.3	105	4	75-125	20	
Dibromochloromethane	<5.00	50.0	52.5	105	50.0	55.0	110	5	73-125	20	
1,2-Dibromo-3-Chloropropane	<5.00	50.0	48.3	97	50.0	53.9	108	11	59-125	28	
Dibromomethane	<5.00	50.0	51.0	102	50.0	51.5	103	1	69-127	23	
1,2-Dichlorobenzene	<5.00	50.0	52.7	105	50.0	51.6	103	2	75-125	20	
1,3-Dichlorobenzene	<5.00	50.0	51.4	103	50.0	51.1	102	1	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 803828

QC- Sample ID: 369409-004 S

Matrix: Water

Date Analyzed: 04/22/2010

Batch #:

Date Prepared: 04/22/2010 Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
1,4-Dichlorobenzene	<5.00	50.0	51.1	102	50.0	51.6	103	1	75-125	20	
Dichlorodifluoromethane	<5.00	50.0	58.2	116	50.0	52.8	106	10	70-130	23	
1,1-Dichloroethane	<5.00	50.0	57.7	115	50.0	55.0	110	5	72-125	20	
1,2-Dichloroethane	<5.00	50.0	53.7	107	50.0	53.1	106	1	68-127	20	
1,1-Dichloroethene	<5.00	50.0	50.1	100	50.0	50.0	100	0	59-172	22	
cis-1,2-Dichloroethene	<5.00	50.0	53.0	106	50.0	52.3	105	1	75-125	20	
trans-1,2-dichloroethene	<5.00	50.0	54.2	108	50.0	51.2	102	6	75-125	20	
1,2-Dichloropropane	<5.00	50.0	53.5	107	50.0	54.9	110	3	74-125	20	
1,3-Dichloropropane	<5.00	50.0	49.6	99	50.0	53.8	108	8	75-125	20	
2,2-Dichloropropane	<5.00	50.0	57.3	115	50.0	50.6	101	12	75-125	20	
1,1-Dichloropropene	<5.00	50.0	47.4	95	50.0	45.6	91	4	75-125	20	
cis-1,3-Dichloropropene	<5.00	50.0	53.1	106	50,0	55.5	111	4	74-125	20	
trans-1,3-dichloropropene	<5.00	50.0	53.3	107	50.0	56.2	112	5	66-125	20	
Ethylbenzene	<5.00	50.0	52.1	104	50.0	50.0	100	4	75-125	20	
Hexachlorobutadiene	<5.00	50.0	49.9	100	50.0	48.0	96	4	75-125	20	
isopropylbenzene	<5.00	50.0	53.6	107	50.0	50.7	101	6	75-125	20	
Methylene Chloride	<5.00	50.0	52.2	104	50.0	51.5	103	1	75-125	35	
Naphthalene	<10.0	50.0	55.8	112	50.0	57.0	114	2	75-125	20	
n-Propylbenzene	<5.00	50.0	51.6	103	50.0	53.3	107	3	75-125	20	
Styrene	<5.00	50.0	53.8	108	50.0	53.2	106	1	75-125	51	
1,1,1,2-Tetrachloroethane	<5.00	50.0	53.4	107	50.0	52.4	105	2	72-125	20	
1,1,2,2-Tetrachloroethane	<5.00	50.0	50.2	100	50,0	54.9	110	9	74-125	31	
Tetrachloroethylene	<5.00	50.0	53.7	107	50.0	52.2	104	3	71-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*[(C-F)/(C+F)]





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EO24

Lab Batch ID: 803828

OC- Sample ID: 369409-004 S

Batch #:

.

Matrix: Water

Date Analyzed: 04/22/2010

Date Prepared: 04/22/2010

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Toluene	<5.00	50.0	49.6	99	50.0	48.9	98	1	59-139	21	
1,2,3-Trichlorobenzene	<5.00	50.0	55.3	111	50.0	52.2	104	6	75-137	20	
1,2,4-Trichlorobenzene	<5.00	50.0	55.4	111	50.0	51.1	102	8	75-135	20	
1,1,1-Trichloroethane	`<5.00	50.0	49.9	100	50.0	46.9	94	6	75-125	20	
1,1,2-Trichloroethane	<5.00	50.0	51.2	102	50.0	54.0	108	5	75-127	20	
Trichloroethene	<5.00	50.0	50.1	100	50.0	50.2	100	0	62-137	24	
Trichlorofluoromethane	<5.00	50.0	61.4	123	50.0	52.7	105	15	67-125	20	
1,2,3-Trichloropropane	<5.00	50.0	51.8	104	50.0	59.6	119	14	75-125	20	
1,2,4-Trimethylbenzene	<5.00	50.0	54.2	108	50.0	51.7	103	5	75-125	20	
1,3,5-Trimethylbenzene	<5.00	50.0	50.8	102	50,0	50.7	101	0	70-125	20	
o-Xylene	<5.00	50.0	54.4	109	50.0	51.9	104	5	75-125	20	
m,p-Xylenes	<10.0	100	106	106	100	104	104	2	75-125	20	
Vinyl Chloride	<2.00	50.0	49.3	99	50.0	44.2	88	11	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804058

QC- Sample ID: 369409-025 S

Batch #:

1 Matrix: Water

Date Analyzed: 04/26/2010

Date Prepared: 04/26/2010 Analyst: CYE

Reporting Units: ug/L		M	IATRIX SPIK	E / MAT	RIX SPI	KE DUPLICA	TE REC	OVERY	STUDY		
VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Benzene	37.6	50.0	85.5	96	50.0	90.4	106	6	66-142	21	
Bromobenzene	<5.00	50.0	50,0	100	50.0	52.7	105	5	75-125	20	
Bromochloromethane	<5.00	50.0	47.5	95	50.0	51.3	103	8	73-125	20	
Bromodichloromethane	<5.00	50.0	55.0	110	50.0	57.9	116	5	75-125	20	
Bromoform	<5.00	50.0	59.1	118	50.0	59.8	120	1	75-125	20	
Bromomethane	<5.00	50.0	35.6	71	50.0	36.6	73	3	70-130	20	
MTBE	14.6	50.0	70,3	111	50.0	72.3	115	3	65-135	20	
n-Butylbenzene	<5.00	50.0	53.0	106	50.0	56.0	112	6	75-125	20	
Sec-Butylbenzene	<5.00	50.0	55,9	112	50.0	58.9	118	5	75-125	20	
tert-Butylbenzene	<5.00	50.0	54.3	109	50.0	58.1	116	7	75-125	20	
Carbon Tetrachloride	<5.00	50.0	47.0	94	50.0	50.9	102	8	62-125	20	
Chlorobenzene	<5.00	50.0	51.9	104	50.0	54.4	109	5	60-133	21	
Chloroethane	<10.0	50.0	40.2	80	50.0	40.4	81	0	70-130	20	
Chloroform	<5.00	50.0	49.6	99	50.0	53.0	106	7	74-125	20	
Chloromethane	<10.0	50.0	37.3	75	50.0	38.3	77	3	70-130	20	
2-Chlorotoluene	<5.00	50.0	49.0	98	50.0	52.6	105	7	73-125	20	
4-Chlorotoluene	<5.00	50.0	49.1	98	50.0	51.6	103	5	74-125	20	
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	49.6	99	50.0	52.1	104	5	75-125	20	
Dibromochloromethane	<5.00	50.0	58.1	116	50.0	60.2	120	4	73-125	20	
1,2-Dibromo-3-Chloropropane	<5.00	50.0	58.5	117	50.0	57.1	114	2	59-125	28	
Dibromomethane	<5.00	50.0	49.5	99	50.0	52.3	105	6	69-127	23	
1,2-Dichlorobenzene	<5.00	50.0	51.7	103	50.0	54.4	109	5	75-125	20	
1,3-Dichlorobenzene	<5.00	50.0	53.0	106	50.0	55.1	110	4	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804058

QC- Sample ID: 369409-025 S **Date Prepared:** 04/26/2010

Batch #: 1 Matrix: Water

Date Analyzed: 04/26/2010

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
1,4-Dichlorobenzene	<5.00	50.0	50.1	100	50.0	52.8	106	5	75-125	20	
Dichlorodifluoromethane	<5.00	50.0	44.1	88	50.0	45.8	92	4	70-130	23	
1,1-Dichloroethane	<5.00	50.0	50,2	100	50.0	52.7	105	5	72-125	20	
1,2-Dichloroethane	<5.00	50.0	49.4	99	50.0	51.9	104	5	68-127	20	
1,1-Dichloroethene	<5.00	50.0	42.1	84	50.0	44.6	89	6	59-172	22	
cis-1,2-Dichloroethene	<5.00	50.0	46.0	92	50.0	48.8	98	6	75-125	20	
trans-1,2-dichloroethene	<5.00	50.0	41.4	83	50.0	44.6	89	7	75-125	20	
1,2-Dichloropropane	<5.00	50.0	53.0	106	50.0	54.6	109	3	74-125	20	
1,3-Dichloropropane	<5.00	50.0	50.8	102	50.0	52.4	105	3	75-125	20	
2,2-Dichloropropane	<5.00	50.0	51.5	103	50.0	52.5	105	2	75-125	20	İ
1,1-Dichloropropene	<5.00	50.0	38.2	76	50.0	41.8	84	9	75-125	20	
cis-1,3-Dichloropropene	<5.00	50.0	52.7	105	50.0	56.9	114	8	74-125	20	
trans-1,3-dichloropropene	<5.00	50.0	52.9	106	50.0	55.7	111	5	66-125	20	
Ethylbenzene	<5.00	50.0	49.9	100	50.0	52.6	105	5	75-125	20	
Hexachlorobutadiene	<5.00	50.0	52,7	105	50.0	54.6	109	4	75-125	20	
isopropylbenzene	53.4	50.0	105	103	50.0	108	109	3	75-125	20	
Methylene Chloride	<5.00	50.0	44.8	90	50.0	47.4	95	6	75-125	35	
Naphthalene	<10.0	50.0	54.9	110	50.0	55.6	111	1	75-125	20	
n-Propylbenzene	51.3	50.0	101	99	50.0	104	105	3	75-125	20	
Styrene	<5.00	50.0	44.2	88	50.0	43.1	86	3	75-125	51	
1,1,1,2-Tetrachloroethane	<5.00	50.0	53.8	108	50.0	55.2	110	3	72-125	20	
1,1,2,2-Tetrachloroethane	<5.00	50.0	57.7	115	50.0	59.6	119	3	74-125	31	
Tetrachloroethylene	<5.00	50.0	47.3	95	50.0	49.6	99	5	71-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804058

Date Analyzed: 04/26/2010

QC- Sample ID: 369409-025 S

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Date Prepared: 04/26/2010

Matrix: Water

Analyst: CYE

Batch #:

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Toluene	<5.00	50.0	48.2	96	50.0	50.9	102	5	59-139	21	
1,2,3-Trichlorobenzene	<5.00	50.0	52.8	106	50.0	54.8	110	4	75-137	20	
1,2,4-Trichlorobenzene	<5.00	50.0	52.0	104	50.0	54.3	109	4	75-135	20	
1,1,1-Trichloroethane	<5.00	50.0	44.3	89	50.0	47.2	94	6	75-125	20	
1,1,2-Trichloroethane	<5.00	50.0	56.3	113	50.0	56.6	113	1	75-127	20	
Trichloroethene	<5.00	50.0	46.6	93	50.0	50.4	101	8	62-137	24	
Trichlorofluoromethane	<5.00	50.0	47.4	95	50.0	48.9	98	3	67-125	20	
1,2,3-Trichloropropane	<5.00	50.0	56.4	113	50.0	58.6	117	4	75-125	20	
1,2,4-Trimethylbenzene	<5.00	50.0	47.3	95	50.0	47.5	95	0	75-125	20	
1,3,5-Trimethylbenzene	51.6	50.0	102	101	50.0	106	109	4	70-125	20	
o-Xylene	5.22	50.0	55.7	101	50.0	57.5	105	3	75-125	20	
m,p-Xylenes	<10.0	100	104	104	100	108	108	4	75-125	20	
Vinyl Chloride	<2.00	50.0	37.0	74	50.0	38.3	77	3	75-125	20	X

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*(C-F)/(C+F)





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804067

QC- Sample ID: 369409-017 S

Batch #: 1 Matrix: Water

Date Analyzed: 04/23/2010

Date Prepared: 04/23/2010

Analyst: CYE

Paparting Units: ug/l

Analyst: CYI

Reporting Units: ug/L	MATRIX SPIKE / MATRIX SPIKE DUPLICATE RECOVERY STUDY Parent Spiked Sample Spiked Duplicate Spiked Control Control Sample Spiked													
VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]		RPD %	Control Limits %R	Control Limits %RPD	Flag			
Benzene	<5.00	50.0	46.9	94	50.0	48.2	96	3	66-142	21				
Bromobenzene	<5.00	50.0	49.5	99	50.0	49.9	100	1	75-125	20	<u> </u>			
Bromochloromethane	<5.00	50.0	48.5	97	50.0	49.2	98	1	73-125	20				
Bromodichloromethane	<5.00	50.0	51.1	102	50.0	52.4	105	3	75-125	20				
Bromoform	<5.00	50.0	49.1	98	50.0	49.3	99	0	75-125	20				
Bromomethane	<5.00	50.0	41.9	84	50.0	44.7	89	6	70-130	20				
MTBE	17.5	50.0	65.1	95	50.0	69.5	104	7	65-135	20				
n-Butylbenzene	<5.00	50.0	49.8	100	50.0	50.0	100	0	75-125	20				
Sec-Butylbenzene	<5.00	50.0	52.4	105	50.0	51.7	103	1	75-125	20				
tert-Butylbenzene	<5.00	50.0	51.9	104	50.0	52.1	104	0	75-125	20				
Carbon Tetrachloride	<5.00	50.0	48.0	96	50.0	49.9	100	4	62-125	20	Ī			
Chlorobenzene	<5.00	50.0	50.0	100	50.0	51.3	103	3	60-133	21				
Chloroethane	<10.0	50.0	42.7	85	50.0	44.9	90	5	70-130	20				
Chloroform	<5.00	50.0	48.6	97	50.0	49.4	99	2	74-125	20				
Chloromethane	<10.0	50.0	43.1	86	50.0	42.6	85	1	70-130	20				
2-Chlorotoluene	<5.00	50.0	49.2	98	50.0	50,3	101	2	73-125	20				
4-Chlorotoluene	<5.00	50.0	49.6	99	50.0	50.2	100	1	74-125	20				
p-Cymene (p-Isopropyltoluene)	<5.00	50.0	51.1	102	50.0	51.5	103	1	75-125	20				
Dibromochloromethane	<5.00	50.0	52.3	105	50.0	53.4	107	2	73-125	20				
1,2-Dibromo-3-Chloropropane	<5.00	50.0	44.7	89	50.0	46.3	93	4	59-125	28				
Dibromomethane	<5.00	50.0	46.4	93	50.0	47.9	96	3	69-127	23				
1,2-Dichlorobenzene	<5.00	50.0	49.8	100	50.0	50.1	100	1	75-125	20				
1,3-Dichlorobenzene	<5.00	50.0	51.1	102	50.0	51.0	102	0	75-125	20				

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*(C-F)/(C+F)| Matrix Spike Duplicate Percent Recovery [G] = 100*(F-A)/E

ND = Not Detected, J = Present Below Reporting Limit, B = Present in Blank, NR = Not Requested, I = Interference, NA = Not Applicable N = See Narrative, EQL = Estimated Quantitation Limit





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804067

QC- Sample ID: 369409-017 S

1 Matrix: Water

Date Analyzed: 04/23/2010

Date Prepared: 04/23/2010

Analyst: CYE

Batch #:

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
1,4-Dichlorobenzene	<5.00	50.0	49.4	99	50.0	50.0	100	1	75-125	20	
Dichlorodifluoromethane	<5.00	50.0	49.3	99	50.0	48.3	97	2	70-130	23	
1,1-Dichloroethane	<5.00	50.0	50.3	101	50.0	51.7	103	3	72-125	20	
1,2-Dichloroethane	<5.00	50.0	47.2	94	50.0	47.3	95	0	68-127	20	
1,1-Dichloroethene	<5.00	50.0	47.2	94	50.0	47.6	95	1	59-172	22	
cis-1,2-Dichloroethene	<5.00	50.0	46.1	92	50.0	47.6	95	3	75-125	20	
trans-1,2-dichloroethene	<5.00	50.0	47.0	94	50.0	47.0	94	0	75-125	20	
1,2-Dichloropropane	<5.00	50.0	50.1	100	50.0	51.0	.102	2	74-125	20	
1,3-Dichloropropane	<5.00	50.0	46.7	93	50.0	48.4	97	4	75-125	20	
2,2-Dichloropropane	<5.00	50.0	49.2	98	50.0	51.9	104	5	75-125	20	
1,1-Dichloropropene	<5.00	50.0	41.7	83	50.0	42.9	86	3	75-125	20	
cis-1,3-Dichloropropene	<5.00	50.0	50.7	101	50.0	51.7	103	2	74-125	20	
trans-1,3-dichloropropene	<5.00	50.0	48.5	97	50.0	49.5	99	2	66-125	20	
Ethylbenzene	<5.00	50.0	47.1	94	50.0	48.8	98	4	75-125	20	
Hexachlorobutadiene	<5.00	50.0	52.0	104	50.0	53.4	107	3	75-125	20	
isopropylbenzene	<5,00	50.0	48.2	96	50.0	50.3	101	4	75-125	20	
Methylene Chloride	<5.00	50.0	47.8	96	50.0	49.7	99	4	75-125	35	
Naphthalene	<10.0	50.0	50.2	100	50.0	52.7	105	5	75-125	20	
n-Propylbenzene	<5.00	50.0	51.1	102	50.0	50.2	100	2	75-125	20	
Styrene	<5.00	50.0	47.7	95	50.0	49.2	98	3	75-125	51	
1,1,1,2-Tetrachloroethane	<5.00	50.0	47.8	96	50.0	51.2	102	7	72-125	20	
1,1,2,2-Tetrachloroethane	<5.00	50.0	49.7	99	50.0	50.3	101	1	74-125	31	
Tetrachloroethylene	<5.00	50.0	49.1	98	50.0	49.6	99	1	71-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*(C-F)/(C+F) Matrix Spike Duplicate Percent Recovery [G] = 100*(F-A)/E

ND = Not Detected, J = Present Below Reporting Limit, B = Present in Blank, NR = Not Requested, I = Interference, NA = Not ApplicableN = See Narrative, EQL = Estimated Quantitation Limit





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804067

QC- Sample ID: 369409-017 S

Batch #: Matrix: Water

Date Analyzed: 04/23/2010

Date Prepared: 04/23/2010

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Toluene	<5.00	50.0	46.8	94	50.0	47.2	94	1	59-139	21	
1,2,3-Trichlorobenzene	<5.00	50.0	52,9	106	50.0	55.0	110	4	75-137	20	
1,2,4-Trichlorobenzene	<5.00	50.0	52.5	105	50.0	53.6	107	2	75-135	20	
1,1,1-Trichloroethane	<5.00	50.0	44.8	90	50.0	46.0	92	3	75-125	20	
1,1,2-Trichloroethane	<5.00	50.0	46.9	94	50.0	49.0	98	4	75-127	20	
Trichloroethene	<5.00	50.0	47.5	95	50.0	48.6	97	2	62-137	24	
Trichlorofluoromethane	<5.00	50.0	50.6	101	50.0	53.2	106	5	67-125	20	
1,2,3-Trichloropropane	<5.00	50.0	48.3	97	50.0	49.7	99	3	75-125	20	
1,2,4-Trimethylbenzene	<5.00	50.0	49.6	99	50.0	50.0	100	1	75-125	20	
1,3,5-Trimethylbenzene	<5.00	50.0	49.6	99	50.0	49.5	99	0	70-125	20	
o-Xylene	<5.00	50.0	48.9	98	50.0	50.2	100	3	75-125	20	
m,p-Xylenes	<10.0	100	97.4	97	100	100	100	3	75-125	20	
Vinyl Chloride	<2.00	50.0	42.5	85	50.0	41.9	84	1	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Date Analyzed: 04/28/2010

Lab Batch ID: 804536

QC-Sample ID: 370094-006 S

Batch #:

Matrix: Water

Project ID: EQ24

Date Prepared: 04/28/2010 Analyst: CYE

Reporting Units: ug/L		M	IATRIX SPIK	E / MAT	RIX SPI	KE DUPLICA	TE REC	OVERY	STUDY		
VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Benzene	<5.00	50.0	50.3	101	50.0	48.8	98	3	66-142	21	
Bromobenzene	<0.000	50.0	48.8	98	50.0	50.6	101	4	75-125	20	
Bromochloromethane	<0.000	50.0	50.1	100	50.0	50.0	100	0	73-125	20	
Bromodichloromethane	<0.000	50.0	54.0	108	50.0	52.7	105	2	75-125	20	
Bromoform	<0.000	50.0	48.9	98	50.0	52.7	105	7	75-125	20	
Bromomethane	<0.000	50.0	42.6	85	50.0	42.3	85	1	70-130	20	
MTBE	<0.000	50.0	51.6	103	50.0	49.9	100	3	65-135	20	
n-Butylbenzene	<0.000	50.0	50.0	100	50.0	50.3	101	1	75-125	20	
Sec-Butylbenzene	<0.000	50.0	53.2	106	50.0	53.4	107	0	75-125	20	
tert-Butylbenzene	<0.000	50.0	53.7	107	50.0	53.1	106	1	75-125	20	
Carbon Tetrachloride	<0.000	50.0	50.5	101	50.0	49.3	99	2	62-125	20	
Chlorobenzene	<5.00	50.0	51.6	103	50.0	52.0	104	1	60-133	21	
Chloroethane	<0.000	50.0	42.1	84	50,0	41.8	84	1	70-130	20	
Chloroform	<0.000	50.0	49.5	99	50.0	48.7	97	2	74-125	20	
Chloromethane	0.970	50.0	44.0	86	50.0	43.5	85	1	70-130	20	
2-Chlorotoluene	<0.000	50.0	50.5	101	50.0	50.5	101	0	73-125	20	<u> </u>
4-Chlorotoluene	<0.000	50.0	50.2	100	50.0	50.5	101	1	74-125	20	
p-Cymene (p-Isopropyltoluene)	<0.000	50.0	52.7	105	50.0	51.7	103	2	75-125	20	
Dibromochloromethane	<0.000	50.0	53.8	108	50.0	54.2	108	1	73-125	20	
1,2-Dibromo-3-Chloropropane	<0.000	50,0	46.8	94	50.0	47.3	95	1	59-125	28	
Dibromomethane	<0.000	50.0	49.0	98	50.0	48.1	96	2	69-127	23	
1,2-Dichlorobenzene	<0.000	50.0	50.6	101	50.0	50.6	101	0	75-125	20	İ
1,3-Dichlorobenzene	<0.000	50.0	51.3	103	50.0	51.8	104	1	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)|





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804536

QC- Sample ID: 370094-006 S

Batch #:

Matrix: Water

Date Analyzed: 04/28/2010

Date Prepared: 04/28/2010

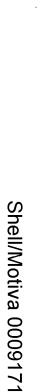
Analyst:

CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
1,4-Dichlorobenzene	<0.000	50.0	50.0	100	50.0	50.4	101	1	75-125	20	
Dichlorodifluoromethane	<0.000	50.0	47.3	95	50.0	46.7	93	1	70-130	23	
1,1-Dichloroethane	<0.000	50.0	52.1	104	50.0	52.2	104	0	72-125	20	
1,2-Dichloroethane	<5.00	50.0	48.3	97	50.0	47.0	94	3	68-127	20	
1,1-Dichloroethene	<0.000	50.0	49.3	99	50.0	48.1	96	2	59-172	22	
cis-1,2-Dichloroethene	<5.00	50.0	49.1	98	50.0	47.9	96	2	75-125	20	
trans-1,2-dichloroethene	<0,000	50.0	48.5	97	50.0	48.0	96	1	75-125	20	
1,2-Dichloropropane	<0.000	50.0	50.7	101	50.0	50.7	101	0	74-125	20	
1,3-Dichloropropane	<0.000	50.0	47.4	95	50.0	49.1	98	4	75-125	20	
2,2-Dichloropropane	<0.000	50.0	53.1	106	50.0	52.0	104	2	75-125	20	
1,1-Dichloropropene	<0.000	50.0	43.3	87	50.0	43.7	87	1	75-125	20	
cis-1,3-Dichloropropene	<0.000	50.0	53.1	106	50.0	54.5	109	3	74-125	20	
trans-1,3-dichloropropene	<0.000	50.0	50.6	101	50.0	51.5	103	2	66-125	20	
Ethylbenzene	<5.00	50.0	49.5	99	50.0	49.6	99	0	75-125	20	
Hexachlorobutadiene	<0.000	50.0	54.3	109	50.0	53.3	107	2	75-125	20	
isopropylbenzene	<5.00	50.0	50.2	100	50.0	50.6	101	1	75-125	20	
Methylene Chloride	1.89	50.0	51.1	98	50.0	49.9	96	2	75-125	35	
Naphthalene	<0.000	50.0	50,1	100	50.0	49.4	99	1	75-125	20	
n-Propylbenzene	<0.000	50.0	50.6	101	50.0	50.9	102	1	75-125	20	
Styrene	<0.000	50.0	49.8	100	50.0	50.2	100	1	75-125	51	
1,1,1,2-Tetrachloroethane	<0.000	50.0	51.4	103	50.0	51.2	102	0	72-125	20	
1,1,2,2-Tetrachloroethane	<0.000	50.0	50.6	101	50.0	50.7	101	0	74-125	31	<u> </u>
Tetrachloroethylene	<5.00	50.0	50.1	100	50.0	50.6	101	1	71-125	20	<u> </u>

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*[(C-F)/(C+F)]





Project Name: 25 Paidge Avenue



Work Order #: 369409

Project ID: EQ24

Lab Batch ID: 804536

QC- Sample ID: 370094-006 S

Matrix: Water

Date Analyzed: 04/28/2010

Date Prepared: 04/28/2010

Batch #:

Analyst: CYE

Reporting Units: ug/L

VOAs by SW-846 8260 Analytes	Parent Sample Result [A]	Spike Added [B]	Spiked Sample Result [C]	Spiked Sample %R [D]	Spike Added [E]	Duplicate Spiked Sample Result [F]	Spiked Dup. %R [G]	RPD %	Control Limits %R	Control Limits %RPD	Flag
Toluene	2.75	50.0	51.5	98	50.0	51.3	97	0	59-139	21	
1,2,3-Trichlorobenzene	<0,000	50.0	53,4	107	50.0	51.4	103	4	75-137	20	
1,2,4-Trichlorobenzene	<0.000	50.0	53.3	107	50.0	53.1	106	0	75-135	20	
1,1,1-Trichloroethane	<0,000	50.0	46.5	93	50.0	45.7	91	2	75-125	20	
1,1,2-Trichloroethane	<0.000	50.0	48.0	96	50.0	50.4	101	5	75-127	20	
Trichloroethene	<5.00	50.0	49.4	99	50.0	48.3	97	2	62-137	24	
Trichlorofluoromethane	<0.000	50.0	51.9	104	50.0	51.2	102	1	67-125	20	
1,2,3-Trichloropropane	<0.000	50.0	49.7	99	50.0	50.2	100	1	75-125	20	
1,2,4-Trimethylbenzene	<0.000	50.0	50.6	101	50.0	50.8	102	0	75-125	20	
1,3,5-Trimethylbenzene	<0,000	50.0	50.7	101	50.0	50.9	102	0	70-125	20	
o-Xylene	<5.00	50.0	51.6	103	50.0	51.4	103	0	75-125	20	
m,p-Xylenes	<10.0	100	99.2	99	100	101	101	2	75-125	20	
Vinyl Chloride	<2.00	50.0	41.9	84	50.0	42.1	84	0	75-125	20	

Matrix Spike Percent Recovery [D] = 100*(C-A)/B Relative Percent Difference RPD = 200*|(C-F)/(C+F)|

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ADDRESS: 3104 Unio	nville Ro	ad, Sui	te 150	:					CONS	ULTANT	TPROJE	CT CONT	ACT (Rep	out to):										ULTANT	PROJE	CT NO:				
Cranbe	erry Twp	. PA 160	380									R NA											EQ	24			- EA	a use	ONLY	
TELEPHONE: FAX 724-553-5084		E-MAIL:		silicic@	sovco	n.com			7	,		ne <u>- 1</u>					nenta	1 63·	1-472	-173	12						30	59	1409-	\mathcal{H}
TURNAROUND TIME (CALENDAR DAYS);		2 DAYS	☐ 24 HO	JPS:	4.7	RESULT ON W	S NEEDI	ED	T	٠.											STED	AN	ALYS	SIS						,
DELIVERABLES: LEVEL 1 LEVEL 2 LEVEL 3			OTHER (SPEC	A 223					T	Ţ.	Τ	1						T				_			Γ	Π	T			٠.
TEMPERATURE ON RECEIPT Cº Cooler #1 2-0	Cooler#2			Cooler #		<u> </u>	70 V V		1								.			ļ										
SPECIAL INSTRUCTIONS OR NOTES :		•	☑ SHELL	CONTRAC	***	E APPLIES	×4		E				}				- 1		-											
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	SAME	LING		e'.	PRE	BRVATIVE		1	8260	1								- {				ľ		ľ		1				
Field Sample Identification	DATE	TIME	MATRIX	HCL H	NO3 H	SO4 NON	OTHE	NO. OF CONT.	EPA 8	MTBE											i		-						Container PID Re- or Laboratory N	
MW-1	4/15/10	7:00	GW	X	130	304 110/4	Ice	3	x	-	_	+					_	7						-						
MW-3	4/15/10	_7:15	GW	x			Ice	3	X	х	Т	T																	-	
MW-29	4/15/10	7:30	GW	x			Ice	*3	х	x	T							\neg			;									
MW-5	4/15/10	7:45	GW	x			ice	3	x	X	T									-										
MW-28	4/15/10	7:55	GW	x		i.	lce	3	х	x										•										
. MW-27	4/15/10	8:00	GW	х		.1.3	lce	3	X	X													L							
MW-6	4/15/10	8:10	GW	x			lce	3	X	X															Ĺ					
MW-7R	4/15/10	8:20	.GW	x			lce	3	х	X			<u> </u>						·					_						
MW-8	4/15/10	8:30	GW	x			Ice	3	X	X	\perp	1_												_	_	_	_			
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Greg Bosiljcic - 724-553-5084 EC	Q24	•
Cranberry Twp, PA 16066 SAMPLER NAME(S) (Print):		369 409-H
724-553-5084 gbosilicic@sovcon.com Nick Zarcone - Longshore Environmental 631-472-1732		367 4º M
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Client: Support Client: Land Client:	Jereign	C	onsult	Mis		()	1/	
	409		7				7) /	
Initials: (CM						$\overline{}$	
		Sam	ple Receip	t Check	list			
1. Samples on ice?					Blue	Water	No _	
2. Shipping container	in good condition?	?			Yea	No	None	
3. Custody seals intac			(cooler) and I	ottles?	(es)	No	N/A	
4. Chain of Custody p	resent?				Yes	No		
5. Sample instructions	s complete on chai	n of cu	ustody?		¥68	No.		
6. Any missing / extra	samples?				Yes	MG)		
7. Chain of custody si	gned when relinqu	ished	/ received?		Yes	No		
8. Chain of custody aç	rees with sample	label(s)?		/Yes	No		
9. Container labels leç	jible and intact?				Yes	No		
10. Sample matrix / pr		n chair	of custody?)	Xes	No		
11. Samples in proper					Xes)	No		
12. Samples properly					YES	No	N/A	
13. Sample container			•		Yes	No		
14. Sufficient sample		ed test	(s)?		Yes	No		
15. All samples receiv					Yes)	No		
16. Subcontract of sar					Yes	No	N/A	·
17. VOC sample have					Yes	No	N/A	
18. Cooler 1 No. 258	, T		Cooler 3 No		Cooler 4 No),	Cooler 5 No.	
)°C lbs	°C		°C	lbs	°C	lbs	°C
	Nor	nconf	ormance D	ocume:	ntation			
Contact:	Con	tacted	by:		[Date/Time:		
Regarding:			<u>.</u>					
Corrective Action Take	en:							
Check all that apply:	□ Cooling proces condition □Initial and Back □ Client understa	accep	otable by NEL mperature co	.AC 5.5.8. Infirm out	3.1.a.1. of temperat	ure condi	-	

Final Ver. 1.000

APPENDIX B

Well Construction Logs



Log of Borehole: MW-21R

Project No.: EQ017

Project: Motiva Enterprise LLC - Brooklyn Terminal

Client: Shell Oil Products US

Location: 25 Paidge Ave, Brooklyn, NY

	SUE	SSURFACE PROFILE		SAMPL				
Depth	Symbol	Description	Lab Sample Interval	Sample Type	Recovery (ft/ft)	PID (ppm)	Well Construction Details	
0-		Ground Surface						
2-		(0.0'-0.5') Gravel (GP) Coarse Gravel (2" Road Base) (0.5'-5.0') Fill Material Fine to medium sand with fill material (wood and bricks), little silt, reddish brown to dark gray, moist to wet at 4.0'	NA	Soft Dig	NA	0.0	Concrete Concrete Bentonite	
8		(5.0'-13.0') No Recovery <u>Drill Cuttings:</u> Clay with little gravel, dark gray, wet	NA	DT	0.0/5.0	NA	10" #2 Silca Sand #2 Silca Sand #3 Silca Sand #4 #4 #5 #5 #5 #5 #5 #5	
10			NA	DT	0.0/3.0	110	0 - 0.020" Slot 8	
14-	,	End of Boring					4" PV	
18-	A Company						HSA (6.25"ID) to 13.0' DT= Dual Tube (3.25"OD)	
Di	rilled By: L	ongshore Environmental Inc				Holo	Size: ~10"	
Di	Drill Method: Direct Push/ HSA - 6.25" ID							
Ĭ	rill Date: 2/		Static Groundwater:					
G	eologist: P	aul R Yesconis	Sheet: 1 of 1					



Log of Borehole: MW-22R

Project No.: EQ017

Project: Motiva Enterprise LLC - Brooklyn Terminal

Client: Shell Oil Products US

Location: 25 Paidge Ave, Brooklyn, NY

SUBSURFACE PROFILE				SAMPL			
Depth	Symbol	Description	Lab Sample Interval	Sample Type	Recovery (ft/ft)	PID (ppm)	Well Construction Details
0-		Ground Surface					
2-		(0.0'-0.5') Gravel (GP) Coarse Gravel (2" Road Base) (0.5'-5.0') Gravelly Sand (SP) Fine to medium sand with fine to coarse gravel (sub-angular), little silt, dark grayish brown, wet at 4.5'	NA	Soft Dig	NA	0.0	10" Flush-Mount Manhole Concrete Concrete Bentonite
8		(5.0'-9.0') Sandy Gravel (GP) Medium gravel (sub-rounded) with fine to coarse sand, dark grayish brown, wet DT and HSA Refusal at 9.0'	NA	рτ	1.0/4.0	600	#2 Silca Sand
10		End of Boring					PVC - 0.020"
12							**************************************
14							DT= Dual Tube (3.25"OD)
16							HSA to 9.0'
J	-	ongshore Environmental Inc				Hole -	Size: ~10"
ļ.		: Direct Push/ HSA - 6.25" ID					Groundwater:
1	rill Date: 2/						: 1 of 1
	eologist: P	aul R Yesconis				5,,000	



Log of Borehole: MW-42

Project No.: EQ017

Project: Motiva Enterprise LLC - Brooklyn Terminal

Client: Shell Oil Products US

Location: 25 Paidge Ave, Brooklyn, NY

Debth O Ground Surface (0.0'-0.5') Asphalt (0.5'-5.0') Fill Material Debth Well Construction O Ground Surface (0.5'-5.0') Fill Material	
(0.01.0.51) Acabalt	-
1 7 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	7
(0.5'-5.0') Fill Material 음 및 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계 기계	-11
(0.5'-5.0') Fill Material Brick, reddish orange, no odors NA Soft Dig NA 0.0 W-W-W-W-W-W-W-W-W-W-W-W-W-W-W-W-W-W-W	Bentonite
0.0 5 0.5 5') Sand (SW)	
Fine to coarse sand with medium gravel and brick fragments, dark grayish brown, wet (5.5'-10.0') Silty Sand (SM) Fine sand and silt, light grayish brown, very moist to wet	4" PVC - 0.020" Slot Screen (3.0'-13.0')
(10.0'-12.4') Organic Clay (OH) Marine Clay, high plasticity, light gray, wet NA DT 3.0/3.0 0.0 0.0	0.020" Slot S
Marine Clay with root material, high plasticity, light gray, wet	4" PVC -
End of Boring	
HSA to 1	3.0'
DT= Dual Tube	(3.25"OD)
Drilled By: Longshore Environmental Inc	
Drill Method: Direct Push/ HSA - 6.25" ID	
Drill Date: 2/24/10 Static Groundwater:	
Geologist: Paul R Yesconis Sheet: 1 of 1	



Log of Borehole: MW-43

Project No.: EQ017

Project: Motiva Enterprise LLC - Brooklyn Terminal

Client: Shell Oil Products US

Location: 25 Paidge Ave, Brooklyn, NY

	SUE	SSURFACE PROFILE		SAMPL	E		
Depth	Symbol	Description	Lab Sample Interval	Sample Type	Recovery (ft/ft)	PID (ppm)	Well Construction Details
0-		Ground Surface					
"	ショ <i>シ</i> ョ	(0.0'-0.5') Asphalt	i				υ
1		(0.5'-1.0') Gravel (GP) Coarse Gravel (2" Road Base)					Concrete Concrete Control
4-1		(1.0'-5.0') Fill Material Fine to medium brown sand with reddish orange brick, some fine to coarse gravel, moist to wet at 4'	NA	Soft Dig	NA	0.0	Concrete Concrete Concrete Building Building Butonite Bentonite
6		(5.0'-10.0') Silt (ML) Silt, light gray, stiff, non plastic,				0.0	10" F
8		moist	NA	DT	0.8/5.0	0.0	1 (#2 Silca Sand
10		(10.0'-10.8') Silty Clay (ML-CL)	<u></u>			0.0	#
10		Clay with silt, brownish gray, low plasticity saturated	NA	DT	3.0/3.0		0.02
12		(10.8'-13.0') Organic Clay (OH) Marine Clay with organic material (roots) and mussel shells, high				0.0	4" PVC
14-]	\plasticity, light gray, wet/					
		End of Boring					
16							
18-							HSA to 13.0'
20							DT= Dual Tube (3.25"OD)
Dr	illed By: L	ongshore Environmental Inc	L		<u>+</u>	Wa!-	Sizo. ~10"
Di	ill Method	: Direct Push/ HSA - 6.25" ID					Size: ~10"
Di	rill Date: 2/	24/10		Static Groundwater:			
G	eologist: P	aul R Yesconis			· · · · · · · · · · · · · · · · · · ·	Sheet	t: 1 of 1



Log of Borehole: MW-44

Project No.: EQ017

Project: Motiva Enterprise LLC - Brooklyn Terminal

Client: Shell Oil Products US

Location: 25 Paidge Ave, Brooklyn, NY

	SUE	SURFACE PROFILE		SAMPL	E		
Depth	Symbol	Description	Lab Sample Interval	Sample Type	Recovery (ft/ft)	PID (ppm)	Well Construction Details
0-		Ground Surface					
		(0.0'-0.8') Asphalt				İ	<u>u</u>
2-		(0.8'-5.0') Fill Material Reddish-orange brick with concrete at 4.5'-5.0'	NA	Soft Dig	NA	0.0	Concrete Concrete Concrete Bentonite Bentonite
						0.0	L
8		(5.0'-6.2') Silty Clay (ML-CL) Clay with silt, dark gray, stiff, slightly plastic, wet (6.2'-10.0') Sandy Silt (ML) Silt with fine sand, dark gray, non plastic, medium to stiff, wet	NA	DT	3.2/5.0	0.0	10" Flush-Mr.
10		(10.0'-13.0') Organic Clay (OH) Marine Clay with organic material (roots) and mussel shells, high plasticity, light gray, wet	NA	DT	3.0/3.0	0.0	
14-		End of Boring					4
16							
18							1104 4 40 61
] =							HSA to 13.0'
20-							DT= Dual Tube (3.25"OD)
<u> </u>	rilled Rv. l	ongshore Environmental Inc	L				
l	•	: Direct Push/ HSA - 6.25" ID				Hole .	Size: ~10"
1	rılı wetnod rili Date: 2/					Static	: Groundwater:
						Sheet	: 1 of 1
G	eologist: P	aul R Yesconis					



Log of Borehole: MW-7R

Project No.: EQ017

Project: Motiva Enterprise LLC - Brooklyn Terminal

Client: Shell Oil Products US

Location: 25 Paidge Ave, Brooklyn, NY

	SUE	SSURFACE PROFILE		SAMPL	E		
Depth	Symbol	Description	Lab Sample Interval	Sample Type	Recovery (ft/ft)	PID (ppm)	Well Construction Details
0-	V 5 V 5	Ground Surface					
	%	(0.0'-0.5') Gravel (GP) Coarse Gravel (2" Road Base) (0.5'-1.5') Sand (SP)					rete
2-		Fine to medium sand, brown, moist (1.5'-5.0') Sand (SP)	NA	Soft Dig	NA	0.0	Concrete Con
4	o PYXXV o PYXX	Fine to medium sand with fill material, dark gray, wet at 4.5'				450	10" Flush-M
6		(5.0'-7.7') Clayey Gravel (GC) Fine to medium gravel with clay, dark grayish brown, wet, hydrocarbon odor	NA	DT	1.5/5.0	500	
10		(7.7'-10.0') Silty Gravel (GM) Fine to medium gravel (subangular) with silt, little fine to coarse sand, dark gray to black staining, hydrocarbon odor, wet				500	#2 Silca Sand
12		(10.0'-13.0') No Recovery Drill Cuttings: Clay, very soft, high plasticity, dark gray to black, wet, hydrocarbon odors	NA	DT	0.0/3.0	NA	#2 Silca Sand
14-		End of Boring					4" PVC
16	·						
18							HSA to 13.0'
20=							DT= Dual Tube (3.25"OD)
Dr	rilled By: L	ongshore Environmental Inc			L		0(40)
Dr	rill Method	: Direct Push/ HSA - 6.25" ID					Size: ~10"
	rill Date: 2/		Static Groundwater:				
Ge	eologist: P	aul R Yesconis				Sheet	: 1 of 1

APPENDIX C

Waste Disposal Documentation

Lorco Petroleum Services 450 South Front St. Elizabeth, NJ 07202 (908) 820-8800 (800) 734-0910 FAX: (908) 820-8412



STANDARD COLLECTION ORDER FORM

748118

www.torcopetroleum.com

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INVOICE

0748118-IN

SALESPERSON | DATE OF INVOICE |
ARD | 02/04/10 |
JOB SITE |

SOVEREIGN CONSULTANTS -6-TERRI LANE

SUITE 500

FEB 18 2010

SHELL 58603 25 PAIDGE AVE BROOKLYN

NY

	lington NJ 0801cr	BROOKLYN	NY		
ACCOUNTING.	DATE SHIPPED	TERMS	YOUR ORDER NUMBER		
0032396	MANIF #27445		. 58603		
QUANTITY	DESCRIPTION		UNIT PRICE	AMOUNT .	
60.00	GASOLINE & WATER - VAC TR NY	LOG#PO		19.20	
	FUEL SURCHARGE	AMOUNTS 405.54 PRI-APP-TH EQUIT	-sc 50660	15.00	
4.00	TRANSPORTATION - VAC TR NY	PMAPP: DSG I	NA CONTRINEDAT	340.00	
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<u>.</u>			TOTAL	405.54	
. A	A SERVICE CHARGE OF 15% WILL BE ADDED TO ALL PAST UDE BRIANCES.	nk You!	↑ RETURN YELLOW WITH PAYME	COPY	

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www.lorcopetroleum.com

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Shell Pipeline Company LP Residual Information Pick-Up Request (RIPR)

Engineer: WEIMER, DOUG Phone / Fax: 703/259-2019 / 7032592068 RIPR# 82042

RDC: ROBERT BILLECK

Facility / SAP Cost Center: 58603

Region/Dist/Area: MOTIVA - DIST. - NEW ENGLAND....

RIPR Date 01/20/2010

Address: 25 PAIDGE AVENUE BROOKLYN, NY-11222-

Remediation: YES SAP Cost Element: 276501

Connty: KINGS

Incident #: 97094981

Send Copies: Reimb. Invoice NO

Direct Pay: NO

Other Info:

Company: Contact:

Consultant / Contractor Information

Company: SOVEREIGN CONSULTING, INC.

Contact: MEHLER, LINDA

Address: 6 TERRI LANE

Type of Facility: OTHER MOTIVA TERMINAL

Phone / Fax: 6093261500 / 6093261501

BURLINGTON, NJ 08016

Material Description

Free Liquids: YES

GASOLINE & WATER

Process Generating this Residual

CLEANING OF ONSITE AST TO BE REMOVED FROM THE SITE.

Accumulation Date:

02/01/2010

Sampling Date (if applicable):

Container Information:

Drums: Quantity / Type:

Id#:

Bins: Quantity / Size:

Supplied by:

Bulk Pile: Indicator / Size: NO

Other Container:

Volume:

Container Description: AST

Contents/Prev. Contents:

Requirements or conditions associated with pick-up:

Comments or suggestions for local vendor:

Form Filled Out by:

Name: MEHLER, LINDA

01/20/2010 Date

Email: LMEHLER@SOVCON.COM

Phone/Fax: 6093261500/6093261501

http://rpmp.shellpipeline.com/epoch/ripr/Temp/RIPRFORM_82042_LMEHLER.htm .

1/20/2010



Proof of Delivery

Dear Customer,

This notice serves as proof of delivery for the shipment listed below.

Tracking Number:

1Z97A7X70193169772

Reference Number(s):

EQ017-711-16, ANNUAL SAMPLING REPORT

Service:

NEXT DAY AIR

Weight:

4.00 Lbs

Shipped/Billed On:

06/30/2010

Delivered On:

07/01/2010 10:30 A.M.

Delivered To:

4740 21ST ST

LONG ISLAND CITY, NY, US 11101

Signed By:

BISSESSAR

Location:

RECEIVER

Thank you for giving us this opportunity to serve you.

Sincerely,

UPS

Tracking results provided by UPS: 07/01/2010 10:59 A.M. ET

DOCUMENT INFO

DocID:

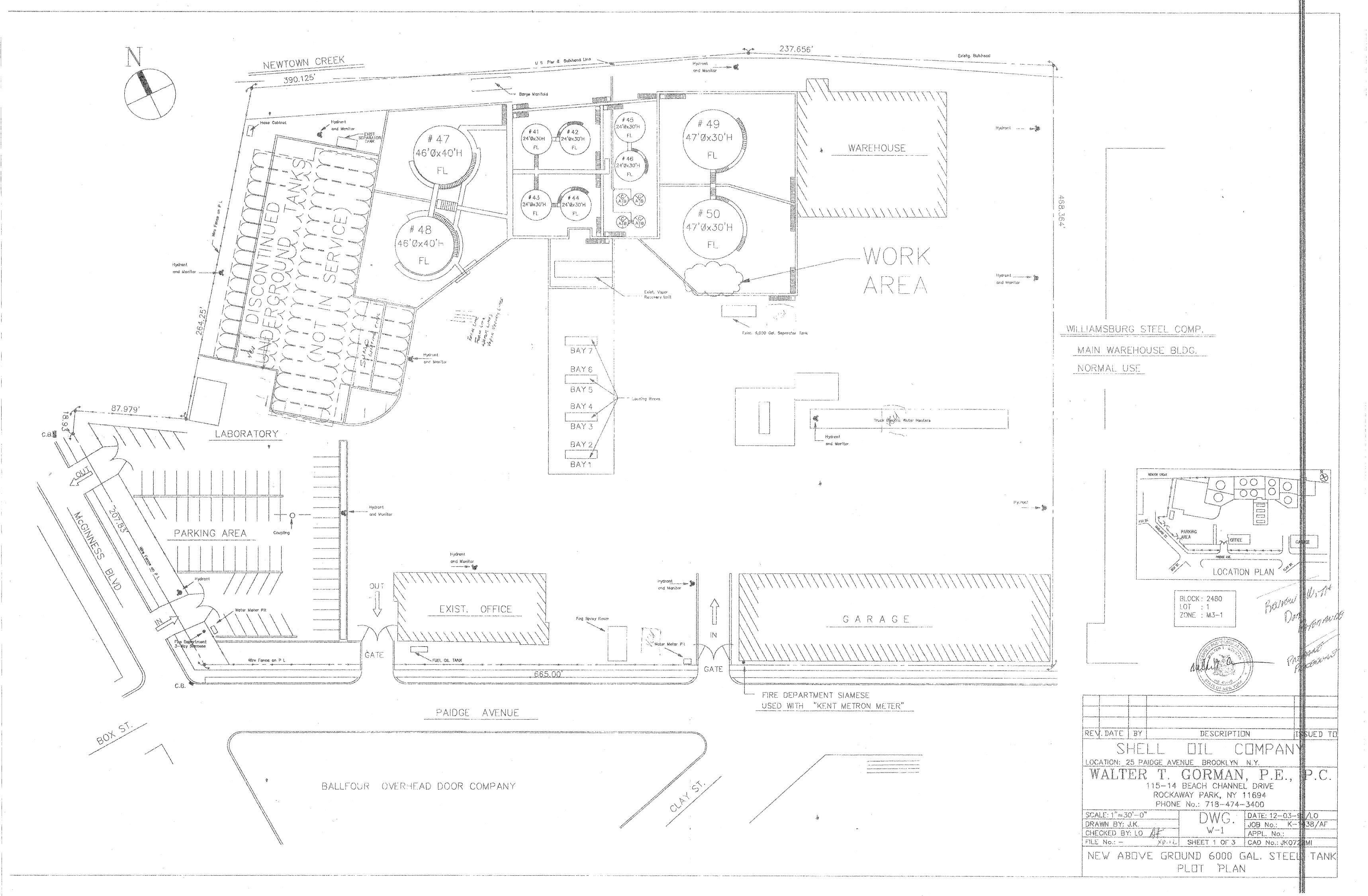
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Filename:

58603-1991-12-03-FIG-01 (New Above

Ground 6000 Gal Steel Tank Plot Plan -

Gorman).pdf



DOCUMENT INFO

DocID:

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Filename:

58603-1999-11-03-PER-01 (Faxed MOSF

License 02154011 - NYSDEC).pdf

(SHELL)

facsimile TRANSMITTAL

John P. Cahill Commissioner

To: Doug Lessing

Fax: (732)536-4659

Pages: 21 Pages, Plus this cover page.

Date: November 3, 1999

RE: Motiva's Greenpoint MOSF License

Doug,

Sorry for the delay in sending the MOSF license. Thanks for the reminder. I think the problem was that the Post Office did not recognize Motiva as Shell Oil. Please find your copy of the MOSF. If you have any question, please call me at (718)482-4933 ext. 7110.

Sincerely,

Anthony Sigona, P.E.

From the desk of...

Anthony J. Sigona, P.E. Environmental Engineer II NYSDEC 30-20 Thomson Avenue 3rd Floor Long Island City, New York 11101 (718) 482-4933 ed. 7110

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New York State Department of Environmental Conservation

Division of Environmental Remediation, Region 2 47-40 21st Street, Long Island City, NY 11101-5407 Phone: (718) 482-4933 ext. 7100 FAX: (718) 482-4954



March 31, 1999

Certified Mail - Return Receipt Requested

Motiva Enterprises 25 Paidge Avenue Brooklyn, N.Y. 11222

ATT: Mr. M.A. D'Antonio, Facility Manager

Dear Mr. D'Antonio:

Enclosed herewith is your Major Petroleum Facility License #02-1540, which expires March 31, 2004. You must apply for renewal 90 days before that date. You must comply with any new or modified conditions imposed by this license. You must comply with all guidelines to prevent, contain, cleanup and remove discharges of petroleum to surface and groundwater. Scheduled facility inspections will be made by Department representatives annually, as well as at random times during the term of the license. Information regarding license fees will be sent by the Division of Fiscal Management, Oil Spill Revenue Unit.

The Department bases the issuance of this license on: (1) an evaluation of the information contained in your application, (2) on-site facility inspections and (3):

	evaluation of submitted State and Federal plans to prevent, α and remove discharges \underline{OR}	control,	conf	tain
**********	a schedule for when such plans are to be submitted.			

March 31, 1999

-2-

Motiva Enterprises

The Department hereby certifies that this major facility currently:

X

has implemented or _____ is in the process of implementing State and Federal plans and regulations for the prevention, control, containment and removal of discharges.

X

of 6 NYCRR Sections 613,2 through 613.9 and 614.2 through 614.14

is in the process of implementing the requirements

Included in your license are general, standard and special Conditions as deemed necessary to protect the waters of the State based upon evaluation of State and Federal plans, compliance with 6 NYCRR Parts 613 and 614, environmental setting and/or facility inspections.

Future license renewals will be based on, among other factors, the history of spills and discharges at the major enshere facility, the history of compliance with the applicable provisions of 6 NYCRR Parts 613 and 614, a review of submitted plans and inspections of the major enshere facility, compliance with license conditions and additional guidelines as subsequently issued.

Please post this license conspicuously at the facility for which it is issued.

has implemented or

Sincerely yours, at

Randall W. Austin Regional Spill Engineer

Spill Prevention & Response Programs

cc: Anthony J. Sigona, P.E. MOSF File



New York State Department of Environmental Conservation

MAJOR PETROLEUM FACILITY LICENSE



FACILITY:

OWNER:

MOTIVA ENTERPRISES, LLC 25 PAIDGE AVENUE BROOKLYN, NY 11222 MOTIVA ENTERPRISES, LLC 1100 LOUISIANA STREET HOUSTON, TX 77002

The facility named above has been duly licensed, pursuant to Article 12 of the Navigation Law. Any conditions placed on this license are marked on the attached Special Conditions Check List.

MAILING CORRESPONDENCE:

LICENSE NUMBER: 2-1540

DATE ISSUED: APRIL 1, 1999

EXPIRATION DATE: MARCH 31, 2004

ATTN: M.A. D'ANTONIO/DAVID BIER MOTIVA ENTERPRISES, LLC 25 PAIDGE AVENUE BROOKLYN, NY 11222

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THIS LICENSE IS NON-TRANSFERABLE

NEW YORK STATE DEPARTMENT OF ENVIRONMENTAL CONSERVATION

MAJOR PETROLEUM FACILITY LICENSE

Tank Listing For License Number: 2-1540

Page ____ of ____

TANK NUMBER.	DATE INSTALLED (Month/Year)	TANK LOCATION	TANK TYPE	CAPACITY (Gallons)	PRODUCT STORED
41	01/48	Aboveground	Steel/Carbon Steel	88,200	Unleaded Gasoline
42	01/48	Aboveground	Steel/Carbon Steel	88,200	Unleaded Gasoline
43	01/50	Aboveground	Steel/Carbon Steel	88,200	Unleaded Gasoline
44	01/50	Aboveground	Steel/Carbon Steel	88,200	Unicaded Gasoline
45 46	01/50	Aboveground	Steel/Carbon Steel	88,200	Unleaded Gasoline
46	01/50	Aboveground	Steel/Carbon Steel	88,200	Unleaded Gasoline
47	01/48	Aboveground	Steel/Carbon Steel	407,400	Unleaded Gasoline
48	01/48	Aboveground	Steel/Carbon Steel	407,400	Unleaded Gasoline
49	01/48	Aboveground	Steel/Carbon Steel	445,200	Unleaded Gasoline
50		Aboveground	Steel/Carbon Steel	445 200	Unleaded Gasoline
55	02/99	Aboveground on rack	Steel/Carbon Steel	10,000	Diesel

GENERAL CONDITIONS FOR MAJOR PETROLEUM FACILITY LICENSE

- 1. No chemical dispersants may be employed in the clean-up of a spill or discharge without approval. If a Spill Prevention and Containment Plan or spill clean-up plan contains a list of chemical or biological agents that are to be used in clean-up operations, the use of such chemicals is subject to prior approval from the Department.
- 2. The use of sorbents shall be limited to the cleanup of small spills and the final cleanup of large spills.
- 3. Disposal of all recovered petroleum products and oil-soaked debris shall be in accordance with 6 NYCRR Section 611.6.
- 4. The owner or operator shall maintain all equipment, including spill clean-up equipment, in good repair.
- 5. Major additions, changes or rehabilitation in the structures or equipment of the onshore major facility, which would materially affect the potential for a petroleum discharge must be approved in advance by the Department. Any amendments or changes to any plans submitted with or referred to in the license application shall be promptly furnished to the Regional Offices.
- 6. The Department shall be notified of all leaks or spills immediately, but in no case later than 2 hours after the spill. Notification must be made by calling the DEC Spill Hotline at (800) or (518) 457-7362.
- 7. Any person transporting and/or disposing of recovered oil and/or oily debris must be registered by the Department, as a "REGISTERED WASTE HAULER" pursuant to 6 NYCRR Part 364 and must transport the material to a disposal facility shown on the Part 364 registration.
- 8. License fees must be paid by the licensee as required by 17 NYCRR Section 30.9, "Oil Spill Prevention and Control, Licensing of Major Facilities".
- 9. The owner or operator of the facility shall provide access to the facility to representatives of the Department during normal business hours for the purpose of determining compliance with State and federal regulations and all general, standard and special conditions of this license.

10. Department Initiated Modifications, Suspensions or Revocations and Licensee Initiated Modifications:

Department Initiated Modifications, Suspensions or Revocations

- (a) The Department may modify, suspend or revoke this license at any time based on the grounds including, but not limited to, the following:
 - (1) materially false or inaccurate statements in the license application or supporting documentation;
 - (2) failure by the license to comply with any terms or conditions of the license;
 - (3) exceeding the scope of the project as described in the license application;
 - (4) failure to pay monthly license fees and/or submit monthly license reports;
 - (5) newly discovered material information or a material change in environmental conditions, relevant technology or applicable law or regulations since the issuance of the existing license: or
 - (6) noncompliance with previously issued license conditions, orders of the Commissioner, any provision of the Navigation Law or Environmental Conservation Law or the regulations adopted pursuant to such laws related to the licensed activity.
- (b) The Department shall send a notice of intent to modify, suspend or revoke a license too the licensee by mail or personal service. The notice shall state the alleged facts or conduct which appear to warrant the intended action.
- (c) Within 15 days of the date of such notice of intent, the licensee may submit a written statement to the Department, giving reasons why the permit should not be denied, suspended or revoked, or requesting a hearing, or both. Failure by the licensee to submit a timely statement shall result in the Department's action becoming effective on the date specified in the notice of intent.
- (d) Within 30 days of receipt of the licensee's statement, the Department shall either:
 - (1) if a statement without a request for a hearing is submitted, rescind or confirm the notice of intent based on a review of the information provided by the license; or
 - (2) if a statement with a request for a hearing has been submitted, notify the license of a date and place for a hearing, to be commenced not later than 60 days from this notification.

- (e) In the event such a hearing is held, the Commissioner shall, within 30 days of receipt of the complete record, issue a decision which:
 - continues the license in effect as originally issued;
 - (2) modifies the license, or suspends it for a stated period of time or upon stated conditions; or
 - (3) revokes the license, including where order by the Commissioner, removal or modification of all or any portion of a project, whether completed or not.

Notice of the decisions, stating the findings and reasons therefore, shall be mailed to the licensee.

- (f) Where the Department proposed to modify a license and the licensee requests a hearing on the proposed modification, the original license conditions remain in effect until there has been a decision issued by the Commissioner as provided herein. At such time the modified license conditions will take effect.
- (g) Nothing in these license conditions shall preclude or affect the Commissioner's authority to issue summary abatement orders under ECLI 71-0301 or take emergency action summarily suspending a license under section 401(3) of the State Administrative Procedure Act.

License Initiated Modification

Applications for modification of a license must include a statement of necessity or reasons for the modification, as well as a description of the requested modification. The Department shall notify the licensee of its decision, by mail, within fifteen days of receipt of such application. An application for modification may be denied for failure to meet any of the standards or criteria applicable under the Navigation Law and regulations adopted thereunder, Article 8 of the Environmental Conservation Law or for any of the reasons set forth in paragraphs (a) (1) - (6) above.

The Department may determine that an application for modification shall be treated as a new application for a license if:

- (1) the application represents a material change in existing license conditions or in the scope of permitted activities; or
- (2) there is newly discovered material information or there has been a material change in environmental conditions, relevant technology or applicable law or regulations since the issuance of the existing license;

Until the Department grants a request for modification requested by a licensee, the original license conditions remain in effect.

MAJOR OIL STORAGE FACILITY LICENSE SPECIAL CONDITIONS CHECK-LIST

Instructions: If an "X" appears in the column labeled "Condition", the specified condition applies to the license issued to the facility. The details of each condition and compliance dates are included in the section fitted, "Special Conditions for Major Oil Storage Facilities".

•	Section Cor	opliance	
Condition	Number	_Date_	Section Title
			Installing Monitoring Wells
	I(a)	· ·	Initial Installation of Monitoring Wells
	1(b)		Additional Monitoring Wells
			Sampling and Testing of Monitoring Wells
***************************************	2(a)		Initial Testing of Monitoring Wells
	2(ь)		Six Month Testing of Monitoring Wells
X	2(c)	June 30	Yearly Testing of Monitoring Wells
<u> </u>	2(d)	Monthly	Monthly Monitoring of Wells
			Spill Prevention and Containment Plan
	3(a)		P.E. Certification/Management Review of Plan
\	3(6)		Description of Secondary Containment System
· · · · · · · · · · · · · · · · · · ·	3(¢)	•	Testing of Secondary Containment System
	3(g)		Engineering Plan for Upgrading Secondary Containment System
	3(e)		Implementation of Engineering Plan
	3 (f)	*******************************	Site Map
	3(g)		Description of Previous Spills
3	3(h)		Compliance Report
	3(1)	***************************************	Updated SPCC Plan and Facility Response Plan
X	3()	8-31-01	Inspection Certification of Secondary Containment Systems

^{*} This is not a requirement for underground storage systems and NYC mounded tanks. It is only applicable to aboveground, free standing, tanks with a capacity in excess of 10,000 gallons or where otherwise required due to proximity to surface water.

MAJOR OIL STORAGE FACILITY LICENSE SPECIAL CONDITIONS CHECK-LIST (Continued)

•	×.		MTBE Monitoring		
· 	4(a)		Initial Testing of Monitoring Wells		
New York Control of the Control of t	4(b)	<u> </u>	Six Month Testing of Monitoring Wells		
X	4(c)	. <u>June 30</u>	Yearly Testing of Monitoring Wells		

SPECIAL LICENSE CONDITIONS (Instructions and Deadlines)

The Department of Environmental Conservation is required by Article 12 of the Navigation Law to protect and preserve the lands and waters of New York State from all discharges of petroleum from Major Oil Storage Facilities. To protect and preserve the waters of the State, owners/operators are required to show how they guard against contamination of surface and groundwater. Surface and groundwater protection at MOSF's is accomplished through the following:

- 1. installing groundwater monitoring wells;
- 2. monitoring groundwater quality;
- 3. developing and implementing the Spill Prevention and Containment Plan, Section 610.4(a)(4).

The following sections detail how to meet each of the conditions marked on the Special Conditions Check-list. Sections 1-3 correspond to the three elements of protecting the waters of the State. The section numbers on the check-list correspond to the following section numbers.

1. Installation of Monitoring Wells

Monitoring wells are needed to determine ambient groundwater quality and to detect possible groundwater contamination that could come from any portion of the facility. The number and location of wells must be approved by the Department. Plans of existing and/or proposed wells must be submitted to the issuing DEC Regional Office by the indicated date. Subject to DEC approval, these monitoring wells must be installed by the date set by the Department.

a. Initial Installation of Monitoring Wells

Install at least one (1) hydraulically up gradient of the facility and install at least three (3) wells hydraulically down gradient of the facility.

When adjacent facilities exist, monitoring wells should be placed on the property lines to determine the source of contamination. In this case, common monitoring wells will exist between facilities so the schedules for testing should be consistent.

Submit plan b	у			
		•	•	
Date to be Ins	talled			

b. Additional Monitoring Wells

Installation of additional wells are necessary based on site conditions, information obtained from existing wells and evidence of past spills or evidence of a potential spill source. The number and location of all additional monitoring wells must be submitted on a site plan for approval by the Regional Office prior to installation.

Number of Wells to b	e Installed	 <u> </u>	· · · · · · · · · · · · · · · · · · ·		
Submit plan by		— ···			
Date to be Installed _				·	·

2. Sampling and Testing of Monitoring Wells

Owners/operators shall conduct a groundwater sampling and testing program to ensure protection of groundwater at the major oil storage facility. All sampling and testing must be conducted by a private or "out-of house" laboratory that is certified by the NYS Department of Health. The laboratory must send the test results to both the facility and the DEC Regional Office. The facility operator may monitor free product without the aid of an outside contractor.

TABLE 1 Recommended Testing Methods for Detecting Petroleum in Groundwater

TYPE OF PETROLEUM	TESTING METHODS		
Gasoline	EPA 602, 624, 503.1		
Aviation Gasoline	EPA 602, 624, 503.1		
Kerosene	EPA 625		
Diesel	EPA 625		
#2 Fuel Oil	EPA 625		
#4, #5, #6 Fuel Oil	EPA 625		

EPA 602 (EPA 8020) tests for seven compounds, including benzene, ethylbenzene, toluene and xylene (BETX) using a GC-PID (gas chromatograph - photo ionization detector) by P/T, purge and trap. This test is most effective in testing for volatile organic compounds in gasoline and aviation gasoline.

EPA 624 (EPA 8040) tests series covers a broader number of substances using GC-MS (gas chromatograph - mass spectrometer) by extraction. This is most effective in testing for volatile organic compounds found in gasoline.

EPA 625 (EPA 8270) series covers a broader number of substances using a gas chromatographic/mass spectrometry (GC/MC) by extraction. This is useful for detecting semi-volatile organics found in kerosene, fuel oil, jet and diesel fuels. If gasoline and fuel oil are stored in the same area, both EPA 602 and EPA 625 may be used to determine if there is petroleum product present in the groundwater.

EPA 503.1 series was adapted by the New York State Department of Health to test drinking water. This series is applicable in the determination of 33 aromatic hydrocarbons using a chromatographic/photoionization detector. This is effective for detecting volatile organics found in light grade products, such as gasoline.

Additional analytical methods may be found in Chart 7-1, Section 7.0 of "Sampling Guidelines and Protocols", NYSDEC - Division of Water.

Prior to collecting a groundwater sample for analysis, a monitoring well must be purged. Purging of wells must consist of bailing 3 to 5 volumes of water present in the well prior to taking samples. If free product is found in any monitoring wells, the incident must be reported to the DEC Spill Hotline within two (2) hours. The owner/operator must perform the following testing and monitoring of wells, providing results and reports as scheduled.

a. Initial Testing of Monitoring Wells

All monitoring v	vells must have an	initial testing	to determine a	baseline assessment
of water quality,	using appropriate	methods discu	issed above.	

Test	Results to	be	Submitted	bу	
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b. Six Month Testing of Monitoring Wells

All monitoring wells must be retested six months after initial testing. This requires analytical testing as described above, refer to Section #2-a. Based on the results of the initial and six-month testing, the DEC Regional Office will establish a schedule for further sampling and testing.

Test Resul	lts to be	Submitted by	7		

c. Yearly Testing of Monitoring Wells.

Annual testing of monitoring wells must be done between April 15 and May 15 of each year using the analytical tests that are described in Section 2, Table 1.

Test Results to be Submitted Annually by June 30 each year

d. Monthly Monitoring of Wells

Routine monitoring for free product is to be done at least monthly using manual methods, such as a bailer, product paste, electronic hydrocarbon probe, or other equivalent method. Results from the manual test are to be recorded and kept on file at the facility as part of the facility's monthly inspection. If free product is found, the Department must be notified on the DEC Spill Hotline within two (2) hours. The Department may request that these monthly reports be submitted to the Regional Office.

·	Submit Monitoring Well Monthly Reports to Regional Office
x	Keep Monitoring Well Monthly Reports on file at facility.

3. State Spill Prevention and Containment Plan

A State Spill Prevention and Containment Plan prepared in accordance with 6NYCRR Section 610.4(a)(4) must be submitted to the Department prior to the issuance of a license. The following are considered elements of a State Spill Prevention and Containment Plan:

- 1. Spill Prevention Control and Countermeasure Plan (SPCC Plan) written according to 40 CFR 112;
- 2. Operations Manual written according to 33 CFR 151, 154, 155 and 156;
- Facility Response Plan written according to Oil Pollution Act (OPA) of 1990;
- 4. Groundwater Contingency Plan written according to Special License Condition and Part 610.4(a)(4)(iv);
- 5. Site Plan written according to Special License Condition and Part 610.4(a)(iii);
- 6. Description of Previous Spills written according to Special License Condition and Part 610.4(a)(4)(ii);
- 7. Compliance Report written according to Special License Condition and Part 610.5(a)(4);
- 8. Inspection records for secondary containment pursuant to Section 613.6(c).

a. PE Certification/Management Review

A licensed professional engineer, preferably a New York State licensed P.E., must certify that the Plan has been prepared in accordance with good engineering practices. The Plan must be updated and recertified whenever any major additions, changes or rehabilitation occurs, as defined in 6NYCRR Section 610.5(c)(2). If no major changes occur, then the owner or operator must complete a review and evaluation of the Plan at least every three years. The owner/operator must submit all recertification or management reviews to the Regional Office.

PE Certification/Management Review to be Submitted by	У
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b. Description of Secondary Containment System

Owners or operators of onshore Major Oil Storage Facilities shall submit a description of the existing secondary containment system in detail, and explain how this system prevents a spill of petroleum from reaching the lands or waters outside the containment area before cleanup occurs.

Secondary Containment Description to be Submitted t	by	
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c. Testing of Secondary Containment System

The secondary containment system shall be tested according to the guidance provided in the Department's technical guidance memo, SPOTS 10. The Plan must contain a description of the procedures and methods used to inspect and test the effectiveness of the system along with the results of permeability tests and geological studies showing the groundwater flow direction, minimum time for the lightest product stored within the secondary containment area to contact the groundwater and a subsoil profile.

Test Results to be Submitted by	
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d. Engineering Plan For Upgrading Secondary Containment System

If the secondary containment system does not meet the standards set forth in 6NYCRR Section 613.3(6), then an engineering plan certified by a professional engineer, preferably a New York State Licensed Engineer, must be submitted to the DEC Regional Office describing how the existing system will be improved. This plan should include the composition and permeability of the existing soil, the methodology that will be used to upgrade the secondary containment system, such as a synthetic liner, the specifications of the material to be used, installation procedures and the proposed permeability of the resulting containment system.

	This plan must be submitted to and approved by the DEC Regional Office before construction is started.
	Engineering Plan to be submitted by
e,	Implementation of Engineering Plan
	After the engineering plan to improve the secondary containment system has been reviewed and is acceptable to the Department, the owner or operator will begin implementation of the proposed secondary containment system.
	Construction to be completed by
f.	Site Map
	The Plan must contain a site map showing the location of all surface water, observation, monitoring, and recovery wells, location of tanks and their respective secondary containment areas, product transfer areas, and spill clean-up equipment storage. This site plan must be drawn to scale.
	Site Map to be submitted by
g.	Description of Previous Spills
	The Plan must contain a description of all spills, discharges and clean-up activities during the previous year. This description must include the cause, type and amount of product spilled and recovered, corrective action taken, clean-up effectiveness, long-term clean-up plans and plans for preventing the recurrence of such a spill or discharge.
	Description of Previous Spills to be Submitted by
h.	Compliance Report
	The Plan must contain an assessment of compliance with the 6 NYCRR Parts 610, 611, 613, 614; 17 NYCRR Parts 30 and 32; and 40 CFR 112 and special conditions required under this license. This must include a status report and schedule for compliance. Guidance and reporting format is available from the Regional Office.
	Compliance Report to be submitted by

I. Updated SPCC Plan and Facility Response Plan which may be required by 40 CFR 112 and Oil Pollution Act of 1990.

Facility Response Plans are required under the Oil Pollution Act (OPA) of 1990 for any on-shore facility that could reasonably be expected to discharge oil to navigable waters, adjoining shoreline or to the exclusive economic zone. These must contain plans for responding, to the maximum extent practical, to a worse-case discharge.

Any facility which must have a Facility Response Plan pursuant to OPA must file the plan and any subsequent amendments with the Department. Such plan must be filed concurrent with the filing with the President.

U.S. Environmental Protection Agency has proposed amendments to the rules for preparing SPCC Plans (40 CFR 112). Any amendments to the SPCC Plan required by future revisions to 40 CFR 112 or any other update or change whatsoever must be filed with the Department.

Match	SPCC	Plan and	Facility	Regnance	Plan to	he sul	mitted by	
opeaco	DI CC	T TITLE CONT.	a ricorred	76000011110	Y TOTAL FO	00 240	Janatica O y	

j. Inspection Certification of Secondary Containment Systems.

Secondary containment systems must be inspected and certified monthly that the secondary systems still meet the standards set forth in 6 NYCRR Section 613.3(c)6. Certification must identify any deficiency found during the inspection and any subsequent repairs rendered. See Section 613.6(a) and (c).

The Department will accept documented monthly inspections that are "visually performed", if these are performed in conjunction with in-depth integrity inspections performed on a frequency not to exceed five years, with such in-depth inspections conducted and certified by a licensed Professional Engineer. The Regional Office must be notified prior to any modifications and repairs to the secondary containment systems. The Regional Office will decide if additional information or plans are required.

This requirement applies only to aboveground (free standing) tanks with a capacity in excess of ten thousand gallons, or to other tanks specifically designated due to their proximity to water. This requirement does not apply to underground tanks and NYC mounded tanks.

In-depth Integrity Inspection and Certification to be submitted by 8-31-01 and every five years thereafter.

4. MTBE Monitoring

Owners/operators shall conduct a groundwater sampling and testing program to ensure protection of groundwater at the major oil storage facility. All sampling and testing must be conducted by a private or "out-of house" laboratory that is certified by the NYS Department of Health. The laboratory must send the test results to both the facility and the DEC Regional Office. The facility operator may monitor free product without the aid of an outside contractor. MTBE Monitoring can be performed concurrently with Sampling and Testing of Monitoring Wells. See Special Condition 2.

TABLE 2

Recommended Testing Methods for Detecting MTBE in Groundwater

TYPE OF PETROLEUM

TESTING METHODS

Volatile Organic Compounds*

502.2, 524.2, 602, 624, 8020, 8021, 8260

*Measurements of MTBE are not standard outputs of these test methods. To obtain such measurements, the lab must be instructed to add these as target analytes.

EPA 602 (EPA 8020) test for seven compounds, including benzene, ethylbenzene, toluene and xylene (BTEX) using a GC-PID (gas chromatograph -photo ionization detector) by purge and trap. This test is effective in testing for volatile organic compounds found in gasoline. Method 602 does not include the isomers of xylene as target analytes. To obtain measurements of these isomers, the lab must be instructed to add these as target analytes.

EPA 624 (EPA 8260) test series covers a broader number of substances using GC-MS (gas chromatograph -mass spectrometer) by extraction. This is effective in testing for volatile organic compounds in gasoline and aviation gasoline.

EPA 625 (EPA 8270) test series covers a broader number of substances using a gas chromatographic/mass spectrometry (GC/MC) by extraction. This is useful for detecting semi-volatile organics found in kerosene, fuel oil, jet and diesel fuels. If gasoline and fuel oil are stored in the same area, both EPA 602 and EPA 625 may be used to determine if there is petroleum product present in the groundwater.

The EPA 500 test series was adopted by the New York State Department of Health to test drinking water. The 502.2 test is applicable in the determination of 33 aromatic hydrocarbons using a chromatographic/photo ionization detector. This is effective for detecting volatile organics found in light grade products, such as gasoline.

b.

c.

EPA 524.2 is a capillary column GC/MS purgeable organics test for volatile organics which have a vapor pressure equal to or greater than 0.1 mm of Hg. The method which is suited for the detection of MTBE is described in EPA's reference "Methods For The Determination of Organics Compounds In Drinking Water."

a.	Initial	Testing	of	Mon	itoring	Wells
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Test Results to be Submitted Annually by

·
All monitoring wells must have an initial test to determine a baseline assessment of water quality, using appropriate methods discussed above.
Test Results to be Submitted by
Six Month Testing of Monitoring Wells
All monitoring wells must be retested six months after initial testing. This requires analytical testing as described in Section #4-a. Based on the results of the initial and sixmonth testing, the DEC Regional Office will establish a schedule for further sampling and testing.
Test Results to be Submitted by
Yearly Testing of Monitoring Wells
Annual testing of monitoring wells must be done between April 15 and May 15 of each year using the analytical tests that are described in Section 4, Table 2.

June 30

GUIDELINES ON INSTALLATION OF MONITORING WELLS

The following is the Department's guidance on installation of monitoring wells at on-shore Major Oil Storage Facilities.

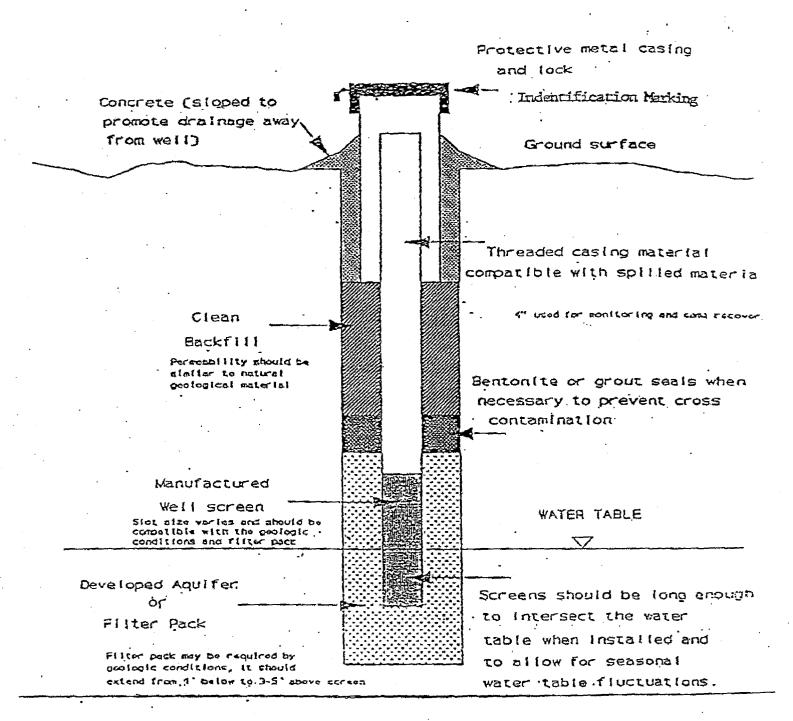
- 1. All wells must be four (4) inches in diameter.
- A log must be kept for each boring that is made. Soil samples must be taken when the composition of the soil layer changes or at five (5) foot intervals, whichever comes first, and a general description of the composition of the soil, as well as the depth that groundwater was first encountered.
- 3. Monitoring wells must be installed plum and straight.
- 4. Flush threaded joints, instead of glued joints, must be used to avoid contamination of the groundwater.
- S. Well screens are to be machine slotted, and must be of adequate length and placement to accommodate seasonal variations in the water table.
- 6. Filter pack must be compatible with soil around the screened portion of the well and with the screen opening. The filter pack must extend approximately one foot below the screen and three to five feet above the screen.
- 7. The well must be sealed between the easing and the bore hole with an impermeable material, such a bentonite, to prevent contamination of the aquifer due to surface run off.
- 8. The well must be sufficiently developed to ensure that the well is free flowing and accurately represents the conditions of the groundwater table.
- 9. The tops of all wells must be enclosed by a protective metal casing that has a locking cap. All wells must be capped and locked at all times. In addition, the monitoring well should be assigned an arbitrary number, such as MW #1. This number should be marked on the monitoring well, as well as any site plans, to facilitate the coordination of the groundwater sampling program.
- All well caps must be clearly marked "Monitoring Well".

All monitoring wells must conform to the well specifications given in this section. The number and location of monitoring wells will be determined by the DEC regional office based on topography and geological studies of the facility. A drawing of an acceptable monitoring well is given on the next page.

All monitoring wells shall be installed outside a secondary containment area. If it is impractical to install the monitoring wells outside of a containment area, a variance must be obtained from the Department. Monitoring wells that are installed inside the secondary containment area must have water tight well caps or placing the top of the well above the height of the dike wall. In addition, the well easing must be properly sealed to prevent infiltration of petroleum in the event of a spill.

MOSF-LP-17

TYPICAL MONITORING WELL CONSTRUCTION



REFERENCES

1. Analytical Handbook

New York State Department of Health (NYSDOH) Division of Laboratories and Research Toxicity Center Albany, New York 12201

2. Analytical Services Protocol

New York State Department of Environmental Conservation Bureau of Technical Services and Research, Room 301 50 Wolf Road Albany, New York 12233-3502

- 3. SPOTS 9, Inspection of Major Oil Storage Facilities.
- 4. SPOTS 10, Spill Prevention and Containment Plan-State Plan.

MOSF-LP-19

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New York State Department of Environmental Conservation Division of Environmental Remediation, Region 2

47-40 21ST Street, Long Island City, NY 11101-5407 Phone: (718) 482-6455 • FAX: (718) 482-6390

Website: www.dec.ny.gov

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CERTIFIED MAIL-RETURN RECEIPT REQUESTED

NOTICE OF VIOLATION



09/16/2008

JAMES LINTZ MOTIVA ENTERPRISES LLC 25 PAIDGE AVENUE BROOKLYN, NY 11222

> Re: Chemical Bulk Storage (CBS) Program Site Inspection -6NYCRR Parts 595-599 CBS# 2-000209, Inspection# 14739 MOTIVA ENTERPRISES LLC 25 PAIDGE AVENUE BROOKLYN, NY 11222

Dear James Lintz:

On September 11, 2008, Department's staff inspected the MOTIVA ENTERPRISES LLC facility to determine compliance with New York State's CBS regulations. The following violations were identified during that inspection and need your immediate attention to bring your facility into compliance. Citations to the applicable regulations are noted in brackets and pertain to the tanks listed. Enclosed to this letter is a CBS application.

The law requires that you comply fully with the CBS regulations. You must correct all of the violations noted below within the stated time frames and submit required documentation.

CBS Registration Certificate - Accuracy of Information - [§596.2(f)]

The registration information is not current. Enclosed is a CBS application form that you may use to correctly inform the Department of the status of your site and/or the status of any particular tank. Return the completed form within 7 calendar days from the date of receipt of this letter. In particular, Tank # 52 is underground—not underground, vaulted, with access as it is in the facility's information report; Tank # 52 does not have vapor wells for internal monitoring; the name of the emergency contact is incorrect.

Spill Prevention Report (SPR) - A. Preparation of SPR [§598.1(k)(1)]

By August 11, 1996, the owner or operator of any site must prepare and maintain an SPR at the site. The SPR should have been developed at the time of installation and updated every year. This report does not comply with the requirements listed below.

Has not been updated annually or whenever a significant release occurred or a substantial modification was made [§598.1(k)(1)].

Within 30 calendar days from the date of receipt of this letter, the owner shall update and submit to this office a site-specific SPR.

A copy of the current registration application is not included in the SPR [§598.1(k)(2)(i)]. The owner shall include a copy of the current application in the SPR.

The SPR lacks an up-to-date site map that is sufficiently detailed to locate and identify tanks, transfer stations and connecting pipes [§ 598.1(k)(2)(iii)]. Within 30 calendar days from the date of receipt of this letter, the owner/operator shall submit to this office an up-to-date sufficiently detailed site map.

There is no listing and/or description of the magnitude and impact of reportable spills over the past five years or the information is not current [§598.1(k)(2)(v)]. Within 30 calendar days from the date of receipt of this letter, the owner/operator shall submit to this office a current listing and description of all reportable spills over the past five years. If there have been no reportable spills, a certified statement to that effect is acceptable.

A spill response plan must be prepared and include: a prediction of the direction of flow/dispersion of a spill; a map showing areas impacted by a spill including sewers, drainage ditches, water supplies, wells, streams and populated areas; a list of equipment and materials to contain a spill; name and phone number for emergency contacts, coordinators, and clean-up contractors; spill reporting procedures; plans for annual drills; and other information consistent with generally accepted spill prevention control and countermeasure practices.

A spill response plan has not been prepared or has not been incorporated into the SPR [§598.1(k)(2)(x)]. Within 30 days from the date of receipt of this letter, the owner/operator shall submit to this office a detailed spill response plan.

B. SPR - Inspections

AST Systems - Annual Inspections

The owner/operator must conduct a comprehensive annual inspection of aboveground storage tank systems to include visually inspecting for cracks, corrosion, poor maintenance and operating practices, excessive settlement of structures, separation or swelling of tank insulation, malfuntioning equipment, safety interlocks safety trips, automatic shutoffs, leak detection and monitoring, warning or gauging equipment which may not be operating properly; and including reviewing compliance with Parts 598 and 599. The inspection shall also include an inspection of the cathodic protection system for aboveground tanks and piping subject to corrosion [§598.7(c)(1)]. Further, the qualified technician must sign and date a statement certifying that the test or inspection has been performed in a manner consistent with the requirements of Part 198 and records must be kept for five (5) years [§598.8].

TANK # 9, 10, 51, 52, 54

The annual inspection for these tanks has not been performed in a manner consistent with the requirements [§598.7(c)(2)]; for example, secondary containment and piping systems were not listed as inspected. Within 30 calendar days from the date of receipt of this letter, the owner/operator shall have the required annual test performed and submit report to this office. Items of non-compliance are listed below.

AST Systems - 5 Year Inspections

The owner/operator must conduct a five-year inspection of all aboveground tank and piping systems. The inspection must be consistent with a consensus code, standard, or practice that is developed by a nationally recognized association or independent testing laboratory. Based upon the inspection, an assessment and evaluation must be made of system tightness, structural soundness, corrosion, wear, foundation weakness and operability, etc. Further, the engineer or qualified technician must sign and date a statement certifying that the test or inspection has been performed in a manner consistent with the requirements of Part 598 and records must be kept for 10 years.

a. Aboveground Tanks -

TANK # 9, 10, 51, 54

The 5-year inspection for these tanks has not been conducted in accordance with a consensus code, standard, or practice developed by a nationally recognized association or independent testing laboratory [§598.7(d)]; for example, secondary containments were not listed in the inspection report; inspections for Tanks # 9 and 10 must be signed by a PE registered in New York State. Within 30 calendar days from the date of receipt of this letter, the owner/operator shall have the required 5-years inspection performed or deficiencies corrected and submit report to this office.

b. Aboveground Piping -

TANK # 9, 10, 51, 54

The 5-year inspection for this piping has not been conducted in accordance with a consensus code, standard, or practice developed by a nationally recognized association or independent testing laboratory. Within 30 calendar days from the date of receipt of this letter, the owner/operator shall have the required 5-years inspection performed or deficiencies corrected and submit report to this office.

Status report on compliance with Parts 596,598 and 599 must be developed [§598.7(c)(v)] and [§598.1(k)(2)(vii)]

TANK # 9, 10, 51, 52, 54

A compliance review has not been prepared and incorporated into the SPR [§598.1(k)(2)(vii)]. Within 30 days from the date of receipt of this letter, the owner/operator shall submit to this office a detailed compliance review.

Secondary Containment for Transfer Stations: [§598.5(d) & §599.17(c)]

TANK # 9, 10, 51, 52, 54

The transfer station for these tanks does not have a secondary containment system.

Within 30 days from the date of receipt of this letter, the owner/operator shall submit to this office a design that meets the requirement of 599.17 (c)(2). Within 60 days of department approval of the design, construction of the secondary containment system for the transfer station shall be completed. All transfers of hazardous substances must occur at a transfer station equipped with a permanently installed secondary containment system. The containment system must have an acceptable spill containment volume; satisfy permeability to the substance stored; must be constructed, coated, or lined with materials that are compatible with the substance stored; and be equipped with a sump & manually-controlled drainage system which must be locked closed [§599.17(c)(2)].

The owner/operator may also apply for a variance from provisions of 6NYCRR 598.5(d) and 599.17(c) to:

New York State Department of Environmental Conservation Division of Environmental Remediation Bureau of Technical Support, 11th Floor 625 Broadway, 11th FloorAlbany, NY 12233-7020 attn: Andrew J. English, PE, Director

Fill port labels

TANK # 9, 10, 51, 54

All fill and dispensing ports for aboveground tanks which are remote to the tank must be labeled with the chemical name or common name, the design capacity and working capacity of the tank, the tank identification number as shown on the registration certificate, and must display legible and clearly visible hazard warnings as required by 9 NYCRR Section 1174.1(h) of the New York State Uniform Fire Prevention and Building Code. The remote fill ports for these tanks are not labeled as required under §596.2(h), §598.4(b)(8), and §599.17(b)(1)(ii). Within 30 days from the date of receipt of this letter, the owner/operator shall submit to this office photographic evidence that the remote fill ports have been properly labeled.

Hazardous Substance Level Gauge - [§599.17(b)(1)(iii)]

a. Where filling or emptying is remotely operated, all gauges must be located at the remote operating station. In addition, remote flow controls shall be provided.

TANK # 9, 10, 51, 54

The remote fill port for these tanks system does not have the required level gauge and flow control. Within 30 days from the date of receipt of this letter, the owner/operator shall submit to this office certification, sign document and photographic evidence that the required level gauge for the remote fill ports for these tanks system is

installed and operational.

TANK# 9, 10, 51, 54

Where safety, pressure relief or vacuum relief valves are used, each must be permanently labeled with the required information of this Section [§599.18(d)]. The labeling must be provided on the valve itself, or on a plate or plates securely fastened to the valve. Labels may be stamped, etched, impressed or cast in the valve or nameplate. All or portions of the required label information have not been provided for the valves associated with these tanks [§599.18(d)]. Within 30 days from the date of receipt of this letter, the owner/operator shall submit to this office photographic evidence that the remote fill ports have been properly labeled.

Valves & Couplings - [§599.17(b)(2)]

All valves and couplings used in making a transfer must meet the following standards.

- 1. Any coupling or open-ended valve used for making a transfer must be located within the secondary containment system of the transfer station;
- 2. Where a product transfer line or fill line is not drained of liquid upon completion of a transfer operation, it must be equipped with a valve such as a dry disconnect shutoff valve which prevents discharges from the line;
- 3. Where siphoning or backflow is possible, fill pipes must be equipped with a properly functioning check valve, siphon break, or equivalent device or system which provides automatic protection against backflow; and
- 4. Each tank connection through which a hazardous substance can normally flow must be equipped with an operating valve or other appropriate means to control such flow.

These valves and couplings do not comply with the following requirement(s).

TANK # 9, 10, 51, 54

For these tanks, the product transfer line or fill line remains full of liquid upon completion of a transfer operation and is ot equipped with the required valve such as a dry disconnect shutoff valve, which prevents discharges from the line. Within 30 days from the date of receipt of this letter, the owner/operator shall submit to this office certification and documents that valves and couplings for these tanks system comply with these requirements.

Corrective Action and Penalties

As a result of these violations, you are subject to penalties. Pursuant to Environmental Conservation Law Section 71-4303, you may be liable for a civil penalty of up to \$25,000 per day for each of the above noted violations. The violations identified in this letter require your immediate attention. Delays in correcting the violations noted above will affect the amount of penalties for which you will be liable. In addition, under Environmental Conservation Law Section 71-1933, a person may be held criminally liable if any of the foregoing violations was the result of intentional, knowing or criminally negligent conduct.

Note that the inspection may not have disclosed all violations that exist at your site. You are responsible for ensuring that the entire facility is in compliance with applicable requirements.

If you have any questions, please call me at (718) 482-6455.

neh Tielindin

Sincerely,

Leszek Zielinski

Environmental Engineer

Emediation Section C

cc: Jacob Krimgold, NYSDEC

(cbsrenew march05)

New York State Department of Environmental Conservation Division of Environmental Remediation

Hazardous Substance Bulk Storage Application

Pursuant to the Hazardous Substance Bulk Storage Law, Article 40 of ECL and 6 NYCRR 595-599



Please Type or Print Clearly



Return Completed Form & Fees To:

NYSDEC Spill Prevention & Bulk Storage Section 625 Broadway, 11th Floor Albany, NY 12233-7020



(See enclosed instructions and please be sure to complete Sections A & B) and Complete All Items **Expiration Date:** 11/30/2008 Facility Name: **CBS Number** TYPE OF CHEMICAL FACILITY (Check only one) MOTIVA ENTERPRISES LLC 2-000209 01=Storage Terminal 03=Other Wholesale/Retail F Location (Not P.O. Boxes) Sales DEC PBS Number 25 PAIDGE AVENUE 02=Retail Gasoline Sales 05=Utility (Other Than (If applicable) Location (cont.): 04=Manufacturing(Other Than Municipal) Chemical)/Processing 07=Apartment Building DEC MOSE Number: State: Zip Code: 06=Trucking/Transportation (If applicable) BROOKLYN NY 11222 /Fleet Operation 09=Farm L County: Township or City: DEC SPDES Number: 08=School 11=Airline/Air Taxi τ Kings New York City (If applicable) 10=Private Residence 13=Municipality (Incl. Waste Name of Operator at Facility: Facility Telephone Number: Т Water Treatment Plants. 12=Chemical Distributor (718) 383-4066 MOTIVA ENTERPRISES LLC **Transaction Type** Utilities, Swimming Pools, etc.) 15=Railroad Emergency Telephone Number: Emergency Contact Name: (Check all that apply) 21=Swimming Pools (Other NOTE: Transaction Types MARIO D'ANTONIO (718) 383-4066 20=Chemical Manufacturing than Municipal) I, 2 and 5 require a fee Owner Name: 99=Other (Specify) 1)Initial/ MOTIVA ENTERPRISES, LLC hereby certify that the information on this form is true and correct. False New Facility Address (Street and/or P.O.): statements made herein may be punishable as a criminal offense in accordance 2)Change of with applicable State and federal law. The facility has maintained its 1100 LOUISIANA STREET, SUITE 2200 o requirements relating to daily, monthly, annual and five year inspections as Ownership City: State: Zin Code: required by Part 598.7 and has had its SPR annually undated as required by 77002 HOUSTON w TX 3)Substantial Part 598.1(k). Tank Owner Telephone Number: Federal Tax ID Number: Name of Owner or Authorized Representative: Amount Enclosed: N Modification 76-0262490 (718) 383-4066 MARIO A. D'ANTONO X 4)Information Title: Type of Owner: 2 State Government 4 Federal Government Correction COMPLEX MANAGER *** *** 1 Private Resident 3 Local Government 5 X Corporate/Commercial Signature: 5) Renewal (Please keep up to date - this information is used for mailing and contact purposes) Spill Prevention Report OFFICIAL USE ONLY In addition, a copy of the R Spill Prevention Report Attention: R (SPR)'s cover page, table MARIO D'ANTONIO Page of contents and signature Name of Company: MOTIVA ENTERPRISES LLC page is submitted.*** Date Received / / P SPR: YES Address: 25 PAIDGE AVENUE O NO Date Processed N *** Application Address: Amount Received \$ will be returned City/State/Zip Code: BROOKLYN NY 11222 if these items Reviewed by E-Mass. Address: Telephone Number: are blank (718) 383-4066

Shell/Motiva 000922

CBS Number:

2-000209

Section B - Tank Information

(See enclosed instructions and use the key located on the bottom of this sheet to complete each item/column)

Registration Expiration Date: 11/30/2008

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		ottor ottorio Signifi Signification	irina 11-90 N 13-11-51 11-11-51 Piping	AND STANDARD AND S	Tank Location	Status	Installation or Permanent Closure Date (Month/ Day/Year)	Capacity (Gallons	Tenning Transc	Tank Internal Protection	This of the second	Socontain Contains on Santains	Tank Leak Defection	Tank	Overfill Prevention	Spill Prevention	Piping Location	ear mudig	Tunnanti Alla III.	Opinic Sec. Containing	Piping Leak Detection	Hazardous Substance Name (List <u>all</u> Part 597 Substances, if more than 3 please list on separate sheet)	CAS Number	% of Haz Sub	Tank Fee \$	
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Action (1)

- 1. Initial Listing
- 2.Add Tank
- 3. Close/Remove Tank
- 4. Information

Correction

5. Recondition/Repair/ Reline Tank

Tank Location (3)

- I. Aboveground-contact w/soil
- 2. Aboveground-contact w/ impervious barrier
- 3. Aboveground on saddles, legs, stilts, rack, or cradle
- 4. Aboveground with 10% or more below ground
- 5. Underground
- Underground, vaulted, with access

Status (4)

- 1. In-service
- 2. Temporarily out-of-service
- 3 Closed-Removed
- 4. Closed- In Place
- 05. Steel Tank in Concrete 5. Tank converted to 06. Fiberglass Reinforced Non-Regulated use
 - Plastic (FRP)
 - 07 Plastic
 - 08. Equivalent Technology 09. Concrete
 - 10. Urethane Clad Steel

Tank Type (8)

01. Steel/Carbon Steel/Iron

02. Galvanized Steel Alloy

04. Fiberglass Coated Steel

03. Stainless Steel Alloy

99. Other-please list:*

Internal Protection (9)

- 00. None
- 01, Epoxy Liner 02. Rubber Liner
- 03. Fiberglass Liner (FRP)
- 04. Glass Liner
- 99. Other-please list:*

External Protection (10/18)

- 00. None
- 01. Painted/Asphalt Coating
- 02. Original Sacrificial Anode
- 03. Original Impressed Current
- 04. Fiberglass
- 05. Jacketed
- 06. Wrapped (Piping)
- 07. Retrofitted Sacrificial Anode
- 08. Retrofitted Impressed Current
- 09. Urethane
- 99. Other-please list:*

Tank Leak Detection (12)

- 00 None
- 01.Interstitial Electronic Monitoring
- 02. Interstitial Manual Monitoring
- 03. Vapor Well
- 04. Groundwater Well
- 05. In-Tank System (ATG)
- 06. Impervious Barrier/Concrete Pad (A/G)
- 99. Other-please list:* * If other, please list on a senarate sheet inclu

Tank Number

Piping Type (17)

- 00. None
- 01. Steel/Carbon Steel/Iron
- 02. Galvanized Steel
- 03. Stainless Steel Allov
- 04. Fiberglass Coated Steel
- 05. Steel Encased in Concrete
- 06. Fiberglass Reinforced
- Plastic (FRP)
- 07. Plastic
- 08. Equivalent Technology
- 09. Concrete 10. Copper
- 11. Flexible Piping
- 99. Other-please list:*

Overfill Prevention(13) 11. Double Bottom (A/G) 00. None

- 01. Float Vent Valve
- 02. High Level Alarm
- 03. Automatic Shut-off
- 04. Product Level Gauge(A/G) 01. Catch Basin
- 05. Vent Whistle

- 00. None

99. Other-please list:*

Spill Prevention (14)

Secondary Containment (11/19)

01. Diking (A/G)

02. Vault (w/access)

05. Synthetic Liner

System

(Bladder)

(A/G)

03. Vault (w/o access)

04. Double-Walled (U/G)

06, Remote Impounding Area

07. Excavation/Trench Liner

09. Modified Double-Walled

10. Impervious Underlayment

08. Flexible Internal Liner

- 02. Transfer Station Containment OO Othor Bloom lines
- 99. Other-please list:*

Detector

Piping Location (16) 00. No Piping

02. Underground/On-ground

Pine Leak Detection (20)

02. Interstitial Manual Monitoring

03. Aboveground/Underground

01. Aboveground

01. Interstitial Electronic

04. Groundwater Well

07. Pressurized Piping Leak

08. Tank Top Sump (Piping)

09. Exempt Suction Piping

Combination

00. None

Monitoring

03. Vapor Well

DOCUMENT INFO

28 3 →

DocID:

00000424

Filename:

58603-2010-10-06-PER-01 (CBS Renewal

Application - Motiva).pdf



October 06, 2010

New York State Department of Environmental Conservation Spill Prevention & Bulk Storage Section 625 Broadway, 11th Floor Albany, NY 12233-7020

SUBJECT: HAZARDOUS SUBSTANCE BULK STORAGE

MOTIVA ENTERPRISES LLC -

BROOKLYN TERMINAL CBS NO. 2-000209

CBS RENEWAL APPLICATION

Dear Madam or Sir:

Enclosed is the Hazardous Substance Bulk Storage Application for renewal of the Chemical Bulk Storage License for the Motiva Enterprises LLC Brooklyn Terminal located at 25 Paidge Avenue, Brooklyn, New York 11222. Also is enclosed is a check for the applicable fee.

Please contact me at 718-383-4066 if you have any questions about the information provided.

Very truly yours,

MOTIVA ENTERPRISES LLC

James W. Lintz Complex Manager

Enclosure

cc: J. Bothwell, Motiva

. File: 750-04 ENV.01.03

25 Paidge Avenue

Brooklyn, NY 11222

Phone: 718-383-4066

Fax: 718-383-4066

New York State Department of Environmental Conservation Division of Environmental Remediation

Hazardous Substance Bulk Storage Application Pursuant to the Hazardous Substance Bulk Storage Law, Article 40 of ECL and 6 NYCRR 595-599



NYSDEC Spill Prevention &Bulk Storage Section 625 Broadway, 11th Floor Albany, NY 12233-7020



Please Type or Print Clearly

Section A

and Complete All Items			ions and pier	ase be su	ire to complete Section	S A & B) Expira	tion Date: 1	1/30/2010
CBS Number 2-000209	F	Facility Name: MOTIVA ENTERPRISES LL(Location (Not P.O. Boxes)	<u> </u>			TYPE OF CHEMICAL FACILITY © 01=Storage Terminal	•	only one) r Wholesale/Retail
DEC PBS Number: (If applicable)	A C	25 PAIDGE AVENUE Location (cont.):			-	02=Retail Gasoline Sales 04=Manufacturing(Other Than	Sales 05=Utility Municipa	y (Other Than al)
DEC MOSF Number: (If applicable) 2-1540 DEC SPDES Number:	l L	City: BROOKLYN County:	State: NY Township or C	city:	Zip Code: 11222	Chemical)/Processing 06=Trucking/Transportation /Fleet Operation 08=School	09=Farm	
(If applicable) N7-000 6131 Transaction Type	I T	Kings Name of Operator at Facility: MOTIVA ENTERPRISES LLC	New York	Facility	Telephone Number:	10=Private Residence 12=Chemical Distributor	13=Muni Water Tro	ne/Air Taxi icipality (Incl. Waste eatment Plants,
(Check all that apply) NOTE: Transaction Types 1, 2 and 5 require a fee	Y	Emergency Contact Name: JAMES W. LINTZ		1 -	ncy Telephone Number: 383-4066	15=Railroad 20=Chemical Manufacturing		Swimming Pools,etc.) naming Pools (Other nicipal)
1)Initial/ New Facility		Owner Name: MOTIVA ENTERPRISES, LL Address (Street and/or P.O.):	С			99=Other (Specify) I hereby certify that the information on t statements made herein may be punishab		
2)Change of Ownership	0	1100 LOUISIANA STREET, S City:	Stat	1	Zip Code: 77002	with applicable State and federal law. The requirements relating to daily, monthly, a required by Part 598.7 and has had its Sl	he facility has r annual and five	maintained its e year inspections as
3)Substantial Tank Modification	W N	HOUSTON Federal Tax ID Number: 76-0262490	į.		hone Number:	Part 598.1(k). Name of Owner or Authorized Representative JAMES W. LINTZ	· · · · · · · · · · · · · · · · · · ·	Amount Enclosed:
4)Information Correction	E R		e Government		Federal Government	Title: COMPLEX MANAGER Signature:	***	***
X 5) Renewal	С		al Government		Corporate/Commercial	Ames Whitz		Date: *** 0-6-2010
Spill Prevention Report In addition, a copy of the Spill Prevention Report (SPR)'s cover page, table	O R R	Attention:	up to date - this JAMES W		on is used for mailing and co	ontact purposes)	OFFICI Page of	IAL USE ONLY
of contents and signature page is submitted. ***	E S P	Name of Company: Address:	MOTIVA 25 PAIDO		PRISES LLC	,	Date Received	
SPR: YES NO	O N	Address:	2011110	, 2 , 1 , 1				d//
*** Application will be returned if these items	D E N	City/State/Zip Code:	BROOKL		NY 11:			ived \$
are blank	c	Telephone Number: (718) 383-4066	5	E-Mai	I Address: JAMES. LI	NTZ @MOTIVAENT, COM		

Shell/Motiva 0009225

CBS Number:

2-000209

Section B - Tank Information

(See enclosed instructions and use the key located on the bottom of this sheet to complete each item/column)

Registration Expiration Date: 11/30/2010

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Action	coli sui mov ins Tar	inis DA iplied alizate	ilsheer provided ing Tank	놀	Status		Capacity (Gallons	Tankati ya	Tank Internal Protection	- X(ema) Woledton	Secondare Comment	Tank	Leak Detection	Tank Overfill Prevention	Spill Prevention	Piping Location	audi, audi,	្សារព្ធភភិបាលក្នុងរូបវិទាស់ មួយប្រែក្រុមប្រជាពលក្នុងរូបវិទាស់	Pipme Sca.Conalantar	Piping Leak Detection	Hazardous Substance Name (List <u>all</u> Part 597 Substances, if more than 3 please list on separate sheet)	CAS Number	% of Haz Sub	Tank Fee \$
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Action (1)

- 1. Initial Listing
- 2.Add Tank
- 3. Close/Remove Tank
- 4. Information
- Correction
- 5. Recondition/Repair/ Reline Tank

Tank Location (3)

- 1. Aboveground-contact
- 2. Aboveground-contact w/
- 3. Aboveground on saddles,
- 4. Aboveground with 10%
- or more below ground
- with access

Status (4)

- I. In-service
- 2. Temporarily out-of-service
- 3. Closed-Removed
- 4. Closed- In Place
- 5. Tank converted to
- Non-Regulated use

- w/soil
- impervious barrier
- legs, stilts, rack, or cradle
- 5. Underground
- 6. Underground, vaulted,

- 01. Steel/Carbon Steel/Iron
- 02. Galvanized Steel Allov
- 03. Stainless Steel Alloy
- - 06. Fiberglass Reinforced
- Plastic (FRP)
 - 07. Plastic

 - 10. Urethane Clad Steel

- 00, None
- 01. Epoxy Liner
- 03. Fiberglass Liner (FRP)
- 99. Other-please list:*

Tank Type (8)

- 04. Fiberglass Coated Steel
- 05, Steel Tank in Concrete
- 08. Equivalent Technology
- 09. Concrete
- 99. Other-please list:*

Internal Protection (9)

- 02. Rubber Liner
- 04. Glass Liner

- 00. None 01. Painted/Asphalt Coating
- 02. Original Sacrificial Anode
- 03. Original Impressed Current
- 04. Fiberglass
- 05. Jacketed
- 06. Wrapped (Piping)
- 07. Retrofitted Sacrificial Anode Plastic (FRP)
- 08. Retrofitted Impressed Current 07. Plastic
- 09. Urethane
- 99. Other-please list:*

Tank Leak Detection (12)

- 00 None 01.Interstitial Electronic Monitoring
- 02. Interstitial Manual Monitoring
- 03. Vapor Well
- 04. Groundwater Well
- 05. In-Tank System (AutoTankGauge)
- 06. Impervious Barrier/Concrete Pad (Aboveground Only)
- 99. Other-please list:*

- Piping Type (17) 00. None
- 01. Steel/Carbon Steel/Iron
- 02. Galvanized Steel
- 03. Stainless Steel Alloy
- 04. Fiberglass Coated Steel
- 05. Steel Encased in Concrete
- 06. Fiberglass Reinforced
- 08. Equivalent Technology
- 09. Concrete 10, Copper
- 11. Flexible Piping
- 99. Other-please list:*

Overfill Prevention(13)

- 00. None
- 01. Float Vent Valve 02. High Level Alarm
- 03. Automatic Shut-off
- 04. Product Level Gauge(Aboveground Only)
- 05. Vent Whistle
- * If other, please list on a separate sheet including Tank Number 99. Other-please list:*

Secondary Containment (11/19)

- 00, None
- 01, Diking (Aboveground Only)
- 02. Vault (w/access)
- 03. Vault (w/o access) 04. Double-Walled (Underground Only)
- 05, Synthetic Liner 06. Remote Impounding Area
- 07. Excavation/Trench Liner System
- 08. Flexible Internal Liner (Bladder)
- 09. Modified Double-Walled (Aboveground Only)
- 10. Impervious Underlayment 11. Double Bottom (Aboveground Only)
- 99. Other-please list:*

- 00. None
 - 01. Catch Basin
 - 02. Transfer Station Containment

01. Aboveground

01. Interstitial Electronic

04. Groundwater Well

99. Other-please list:*

07. Pressurized Piping Leak

08. Tank Top Sump (Piping)

09. Exempt Suction Piping

Combination

00. None

Monitoring

Detector

03. Vapor Well

02. Underground/On-ground

Pipe Leak Detection (20)

02. Interstitial Manual Monitoring

03. Aboveground/Underground

99. Other - Please list*

Spill Prevention (14)

MOTIVA ENTERPRISES LLC P.O. BOX 4913 HOUSTON, TX 77210

> SHL01-000042-10130414-C9090-M000047 NEW YORK STATE DEPT OF ENVIRONMENTAL CONSERVATION 625 BROADWAY 14TH FL ALBANY, NY 12233-5500

CHECK NO.: 5000012507

COMPANY CODE: 0001

CHECK DATE: 10/13/2010

CLIENT NO.: 0005438016

Page 1 of 1

INVOICE NO.	INV. DATE	REFERENCE	DESCRIPTION	DISC. AMOUNT	NET AMOUNT
50386	10/11/2010	3019080997	FRANK SIGNORIELLO, BROOKLYN BULK S	. \$0.00	\$500.00
			;		
		•			
	į				
				. 4	
				TOTAL:	\$500.00

Direct all Inquiries to: APHOTLINE@SHELL.COM; 1-877-395-8031

We invite you to convert to electronic payments in the form of ACH. Please contact us at the above address/phone number for further details.

DETACH AND RETAIN THIS STUB FOR YOUR RECORDS.

MOTIVA ENTERPRISES LLC P.O. BOX 4913 HOUSTON, TX 77210

82-20 311 Check No.:5000012507

10/13/2010

PAY TO THE ORDER OF

NEW YORK STATE DEPT OF ENVIRONMENTAL CONSERVATION

625 BROADWAY 14TH FL ALBANY, NY 12233-5500 *********\$500.00

NOT VALID AFTER 180 DAYS

Five hundred and 00/100 Dollars

CITIBANK N.A. ONE PENNS WAY, NEW CASTLE, DE 19720 AUTHORIZED SIGNATURE

AUTHORIZED SIGNATURE

50000 1 250 7#

10311002091

38 70 20 16#

MOTIVA ENTERPRISES LLC – BROOKLYN TERMINAL

SPILL PREVENTION REPORT

SECTION 1: GENERAL INFORMATION

This Spill Prevention Report (SPR) has been prepared to meet the requirements of 6NYCRR 598.1(k)(1). Motiva Enterprise LLC (Motiva) has prepared and continually updates as needed an Integrated Contingency Plan/Facility Response Plan (ICP) which includes the required elements of the Spill Prevention Plan. The ICP is designed to meet the requirements of the many, often overlapping plans, that the terminal maintains in accordance with applicable Federal, State and Local regulations. The ICP has been submitted to the EPA, Coast Guard and NYSDEC for review and approval and periodic updates are provided to these agencies. This SPR is incorporated by reference into the ICP, therefore select sections of the ICP are provided here to meet the requirements of the SPR. The entire ICP is on file at the NYSDEC and available for review in support of this Chemical Bulk Storage Permit Renewal Application

Facility Name:

Motiva Enterprises LLC - Brooklyn Terminal

25 Paidge Avenue

Brooklyn, New York 11222-1281

Phone: 718-383-4066 Fax: 718-383-7970

CBS No. 2-000209

Major Onshore Facility License No. 2-1540

DEC SPDES No. NY-0006131

Description of Operations

- The facility stores gasoline, fuel grade ethanol and gasoline additives.
- The facility has a total storage capacity of 55,971 Bbls with an average storage volume of 38,000 to 42,000 Bbls. Daily throughput is approximately 17,000 Bbls across a six bay truck loading rack.
- All products are received through three methods: via pipeline, barge, and truck.
- Gasoline additives are received by truck.

Products Handled

- Gasoline
- Fuel Grade Ethanol
- Gasoline Additives

Required Response and Operating Plans

The plans listed below are maintained by the Brooklyn Terminal and are available on-site at all times for reference and use by terminal personnel:

- Spill Prevention Control and Countermeasure (SPCC) Plan (40 CFR 112)
- US Coast Guard Dock Operations Manual (33 CFR 151, 154, 155 and 156)
- Site Plan Information (included in the ICP)
- Description of Spills (list is included in the ICP along with the Oil Spill Contingency Plan)
 All spills are document on Motiva HSSE Forms and kept on file at the terminal.
 NOTE: There have been no spills at the terminal in the past 5 years.
- Environmental Compliance Report (a copy of the most recent report is attached)
- Secondary Containment Inspection Report (reports kept on file at the terminal)
- Inspection Records for Aboveground Storage Tanks (reports are kept on file at the terminal)

Facility Changes/New Equipment/Engineering Plans

In 2010 the truck loading rack canopy was replaced with a larger canopy to provide greater control of storm water in the truck loading area. New curbing, drains, and piping were installed to convey the flow of water under the rack to an underground tank for temporary storage. The new arrangement also increased the storage capacity of the drainage system. As part of this project, the SPCC Plan for the facility was updated and certified by a New York State Licensed Professional Engineer. A copy of the SPCC plan, containment calculations and PE Certification are included in this report. Engineering plans are available for review at the terminal.

SECTION 2: SUMMARY OF RELEASES

Description of Spills, Discharges and Response Actions

There have been no spills at the terminal in the last five years. If a spill occurs, a description of the incident is documented in the facilities ICP. Additionally, all spill incidents are documented on a Motiva HSE Report form as required by Motiva's procedures.

SECTION 3: STATUS REPORT ON COMPLIANCE & SPILL PREVENTION PREPAREDNESS

New York State Chemical Bulk Storage Inspection Report

A CBS self-inspection was performed by Motiva personnel and the form is attached to this report.

SECTION 4: PERIODIC EQUIPMENT INSPECTION RECORDS

Annual and five year tank inspection reports prepared by outside contractors are kept on file at the terminal and are available for review. Monthly and daily inspections are performed by terminal operators and the inspection forms are kept on file and are available for review at the terminal.

SECTION 5: FINANCIAL RESPONSIBILITY

Motiva will provide evidence of financial responsibility upon request.

SECTION 6: SPILL RESPONSE PLAN

Motiva maintains an Integrated Contingency Plan/Facility Response plan at the terminal. The ICP contain the following:

- Spill reporting procedures
- Material safety data sheets for all products stored on site
- Identification and evaluation of potential spill hazards
- Initial response and containment procedures
- A prediction of the flow of a release and a site drainage map
- Maps of nearby environmental sensitive areas
- A list of spill response contractors contracted by Motiva
- Name and contact numbers for the qualified individual and two alternate qualified individuals
- Training requirements for employees
- Records of annual drills
- Security measures (A facility Security Plan is also available at the terminal)

Excerpts of the ICP are attached.

SECTION 7: DISCUSSION AND ASSESSMENT OF EQUIVALENT EQUIPMENT, METHOD OR PRACTICE

This section is not applicable to the Motiva Brooklyn Terminal.

SECTION 8: SITE ASSESSMENT AND FINDINGS

In response to historic impact to soil and groundwater at the terminal, Motiva entered into a Stipulation Agreement with the NYSDEC and completed an assessment of soil and groundwater conditions across the site. A groundwater remediation system was installed and operated in the 1990s and removed in 2007. Monthly gauging and annual groundwater sampling is performed at the site.

SECTION 9: WRITTEN PROCEDURES TO PREVENT THE MIXING OF INCOMPATIBLE SUBSTANCES

Written procedures for handling of product are included in the Terminal Operation Manual which is available for review at the terminal.

SECTION 10: CONSENSUS CODES

Motiva uses industry standards for maintenance and installation of tanks and piping at the Brooklyn Terminal.

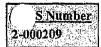
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ATTACHMENT 1

REGISTRATION APPLICATION AND RECERTIFICATION







New York State Department of "vironmental Conservation CHEMICAL BULK STO., AGE CERTIFICATE

625 Broadway, 11th Floor, Albany, NY 12233-7020 Phone: 518-402-9553

Region 2 One Hunters Point Plaza, 18 oor 47-40 21st Street, L.I. City, NY 11101-6454 (718) 482-6454

					•	
TANK NUMBER	DATE INSTALLED	TANK LOCATION AND TYPE	CAPACITY (GALLONS)	HAZARDOUS SUBSTANCE	% HAZ SUBST	CHEMICAL ABSTRACT#
10	01/01/1945	AST - Steel/Carbon Steel/Iron	10,000			
	•	<u>.</u>		XYLENE (MIXED)	3.00	1330-20-7
51	10/01/1990	AST - Steel/Carbon Steel/Iron	5,000		•	•
				XYLENE (MIXED)	17.00	1330-20-7
52	12/01/1990	AST - Steel/Carbon Steel/Iron	4,000	·		
				XYLENE (MIXED)	17.00	1330-20-7
54	10/01/1993	AST - Steel/Carbon Steel/Iron	5,014	**************************************		4444 44 =
	04/04/1042	A CORD CALLED A L. CALLER	10.000	XYLENE (MIXED)	17.00	1330-20-7
9	04/01/1945	AST - Steel/Carbon Steel/Iron	10,000	VVI ENE (MIVED)	27.00	1330-20-7
			•	XYLENE (MIXED)	27.00	1330-20-/

OWNER:

MOTIVA ENTERPRISES, LLC 1100 LOUISIANA STREET, SUITE 2200 HOUSTON, TX 77002

OPERATOR: MOTIVA ENTERPRISES LLC

(718) 383-4066

EMERGENCY JAMES W. LINTZ CONTACT: (718) 383-4066

ISSUED BY:

Commissioner

Alexander B. Grannis

CBS NUMBER:

2-000209

DATE ISSUED:

11/03/2008

EXPIRATION DATE:

11/30/2010

FEE PAID:

\$ 625.00

SITE:

MOTIVA ENTERPRISES LLC **25 PAIDGE AVENUE**

BROOKLYN, NY 11222

MAILING CORRESPONDENCE:

JAMES W. LINTZ

MOTIVA ENTERPRISES LLC

25 PAIDGE AVENUE

BROOKLYN, NY 11222

As an authorized representative of the above named facility. I hereby certify that the information on this form is true and correct. Additionally, I recognize that I am responsible for assuring that this facility is in compliance with all sections of ECL Article 40 and 6 NYCRR Parts 595, 596, 597, 598, and 599, not just those cited

- The facility must be re-registered if there is a transfer of ownership.

- The facility has maintained it's requirements relating to daily, monthly, annual and five year inspections as required by Part 598.7 and has has it's SPR annually updated as required by Part 598.1(k).

- The Department must be notified within 3 business days prior to adding, replacing, reconditioning, or permanently closing a stationary tank.

- This certificate must be signed and posted on the premises at all times. Posting must be at the tank, at the entrance of the facility, or the main office where the storage tanks are located.

-- Any person with knowledge of a spill, leak or discharge must report the incident to DEC within two hours (1-800-457-7362).

Name and Title of Authorized Representative/Owner (Please Print)

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ATTACHMENT 2

SPILL PREVENTION REPORT (SPR) CERTIFICATION

I certify that I have acquired, through education and/or related practical experience, knowledge of the physical sciences, technology and principles of storing and handling hazardous substances as it relates to this facility.

I have examined the facility, and being familiar with the provisions of 6 NYCRR Parts 595, 596, 597, 598, and 599, attest that this spill prevention report has been prepared in accordance with requirements therein.

Name of Qualified Person

Date: 10-20-2010

Signature of Qualified Person

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ATTACHMENT 3

SAMPLE COMPLIANCE STATUS CHECKLIST

NEW YORK STATE CHEMICAL BULK STORAGE INSPECTION REPORT

Rev. 8/28/06 Checklet 2005

•					.DSCKISE ZU
CBS# 2 -000 209	or Unregistered In	spection numb	er	Date 10/20/2010	
Site Name Motiva Enterprises I	LC - Brooklyn Terminal	Owner Nan	ne Motiva Enterprises LLC		
Site Address 25 Paidge Ave, B	rooklyn, NY 11222-1281	. Owner Add	ress 1100 Louisiana St, S	Ste 2200	
		_	Houston, TX 77002	<u> </u>	
Site Contact Frank Signoriello		Owner Con	tact		
Phone Number	5, ext 12	_ Phone Num			
Fax Number718-383-7970)	_ Fax Numbe			
Email Address Frank Signon	ello@Motivaent.com	Email Addı	ressJames.Lintz@Motiva	ent.com	
OFFE PEDITOSCHOULD	N] z, Frank Signoriello f-assessment	Location 3. At	1.' AST 4. At UST 5.Main	Visitor parking 2. C	
i. GENERAL			YES	NO	X
1. All regulated tanks at this site a	re registered [§596.2(a)]?		Y	· · · · · · · · · · · · · · · · · · ·	
2. Is the registration certificate po-	sted at the facility [§596.2(g)]?		Y		
3. Is registration information of	urrent & correct [§596.2(f)]?	-	Tænk 52 should be removed		
II, SPILL PREVENTION REPORT			YES	NO	X
4. Does facility have an SPR [§5	598.1(k)(1)]? Y/N Date:		Incorporated in ICP, last update 10/2010		
5. Has SPR been updated annua When a substantial modification	lly or Whenever a significant release on was made. Y/N/X	occurred or	Υ		
6. Does the SPR contains a copy of [§598.1(k)(2)(i)]? Y/N	of current registration application & o	certificate.	Y		
7. Current approval of manageme	nt [\$598.1(k)(2)(ii)]? Y/N		Y		10.12.5
8. Current site map [§598.1(k)(2) connecting piping Y/N	(iii)]? Locate/identify tanks, transfer	r stations,	Y		
9. Preparer's name and signature	[§598.1(k)(2)(iv)]? Y/N		Y		
10. Listing and description of spi	lls for past 5 years [§598.1(k)(2)(v)]?	Y/N	Y		
11. An assessment of causes of sp §598.1(k)(2)(vi)]? Y/N	ills, leaks, and releases for past 5 yea	urs	NA NO SPILLS IN 5 YRS		
12. SPR contain a spill response p	olan [§598.1(k)(2)(x)]? Y/N/1 (incon	nplete)	Y in ICP		
B. Periodic Inspections of Tank §598.6 &§598.8]	/Piping and Record keeping §598.1	(k)(2)(viii) ,			
13. Is weekly monitoring perform containment system for: a. UST 1: 8598.6(b)(2)12 Y/N/2	ed between the tank/pipe and the secon	ondary	NA no USTS		

 b. Underground piping [§599.15(b); §598.6(c)(1); §598.5(a)]? Can be in combination with: inventory with annual tightness test; vapor wells; gw wells; auto tank gauging; equiv. Y/N/X 	NA no underground pipinf		
14. UST Systems - Monthly inspections Monthly visual is performed [§598.6(a)(1)]? Y/N/X/1 (records not retained for 10 yrs §598.8(a))/2 (report signed, dated, certified §598.8(b))/3 (records not in SPR)/4(operability)	NA no USTS	·	
15. AST Monthly (≥10% volume beneath ground) [§598.7(b)] a. Aboveground tank - Monthly leak detection is performed [§598.7(b)]? Y/N/X/1 (records not retained for 10 yrs §598.8(a))/ 2 (report signed, dated, certified §598.8(b)/ 3 (records not in SPR)	Y records on file at terminal		
b. Underground piping - Monthly leak detection is performed [§598.6(c);§598.7(b);§599.15(b)]? Y/N/ 1 (records not retained for 10 yrs §598.8(a))/ 2 (report signed, dated, certified §598.8(b)/ 3 (records not in SPR)	NA no underground piping		
16. UST Systems - Annual Inspections [§598.6(a)(2)] Date: a. Automatic Line Leak Detector? Y/N(not performed)/1(no records in SPR)/2(records not retained 5 yrs)/3(no cert.)/4(not operational)	NA no USTS	,	
 b. Cathodic Protection System for Tanks? Y/N/X(not performed)/I(no records in SPR)/2(records not retained 5 yrs)/3(no cert.)/4(not maintained to achieve protection) 	NA no USTS	·	
 c. Cathodic Protection System for Piping? Y/N(not performed)/1(no records in SPR)/2(records not retained 5 yrs)/3(no cert.)/4(not maintained to achieve protection) 	NA no underground piping		
17. AST Systems - Annual Inspections [§598.7] Date Completed: 10/20/2010 a. Aboveground Tank- (1) Visual inspections performed [§598.7(c)(2)]? Y/N/ 1 (records not in SPR)	Υ		
(2) For tank subject to corrosion, cathodic protection system is inspected by qualified technician and is maintained to achieve protection [§598.7(c)(1); §598.8(a); §598.8(b) & §598.9]?Y/N (not performed)/X(not in contact with soil)/I(no records in SPR)/ 2 (records not retained 5 yrs)/3 (no cert.)/4 (not maintained to achieve protection)	Not in contact with soil		
b. Aboveground Piping - (1) Visual inspections performed [§598.7(c)(2)]? Y/N/1 (records not in SPR)	Υ		
(2) For piping subject to corrosion, cathodic protection system is inspected by qualified technician and is maintained to achieve protection [§598.7(c)(1); §598.8(a); §598.8(b) & §598.9]? Y/N(not performed)/X(not in contact with soil)/1 (no records in SPR)/2 (records not retained 5 yrs)/3 (no cert.)/4 (not maintained to achieve protection)	Not in contact with soil; entire terminal system is inspected annually		
18. AST Systems - 5-year Inspections [§598.7(d)] Date: 10/1/08 Aboveground tanks and piping must undergo a 5-year inspection in accordance with a consensus code, standard, or practice. An assessment & evaluation must be made of structural soundness, system tightness, corrosion, wear, foundation weakness & operability. Reports are dated, signed, & certified [§598.8(b)] & records are maintained for 10-year period [§598.8(a)]. For tanks > 10,000 gal, the inspection is certified by a NYS-licensed professional engineer. The remaining life expectancy must be determined. a. Aboveground tanks? Y/N/X/1 (not in accordance with code)/2 (no assessment)/3 (no cert)/4 (records not retained 10 yrs)/5 (no cert. for tank>10,000 g)/6 (records not in SPR)	5 yr Tank inspection reports on file at terminal		
b. Aboveground piping? Y/N/X/ 1(not in accordance with code)/ 2(no assessment)/3(no cert)/4(records not retained 10 yrs)/5 (records not in SPR)	Y		
	 		

19. UST Inspection - Reconditioned Tanks With Liners [\$598.6(d)]? Y/N (not inspected internally)/X/ 1 (not performing to design specs)/ 2 (no assessment)/ 3 (no cert.)/ 4 (records not retained)/ 5 (records not in SPR)	NA no USTs		
20. Facility report on status of compliance [§598.1(k)(2)(vii)]?	Inspection reports		
C. Tank & Piping Certifications (Apply to tanks installed on or after 2/11/95) 21. Does the SPR contain a certification statement for design and installation of tank and piping systems - a. USTs [§599.6(g)(4)& (5)]? Y/N/ X (no USTs)/1 (record not available)/2 (no records for 5 yrs)/3 (records not in SPR)	NA tanks installed prior to 1995 X, no USTs		
b. ASTs [§599.11(f)(4) & (5)]? Y/N/ X (no ASTs)/1 (record not available)/2 (no records for 5 yrs)/3 (records not in SPR)	NA tanks installed prior to 1995		
c. Piping [§599.16(e)(3)&(4)]? Y/N/I (record not available)/2 (no records for 5 yrs)/3 (records not in SPR)	NA tanks installed prior to 1995		
D. Life Expectancy/Warranty 22. UST secondary containment liner - liner life expectancy is specified in the SPR [§599.4(d)]? Y/N/X	NA		
23. Useful life for UST tank design, if < 30 years, is specified in the SPR [§599.3(c)(1)]? Y/N/X	NA	·	
24. Useful life for AST tank design, if < 30 years, is specified in the SPR [§599.8(b)(1)]? Y/N/X	NA		
25. Piping life expectancy is specified in the SPR? [§599.13(a)(1)]? Y/N	NA		
E. Additional Requirements			
26.Are rupture disks replaced			
a. Every 3 years, Y/N (no option selected)/X	4		
b. According to manufacturer's guidelines, Y/N (no option selected)/X			
c. On the basis of operating experience [§598.9(f)]?Y/N (no option selected)/X	Υ		
27. Does SPR contain a site assessment for UST, or AST with ≥10% volume beneath ground, for{ closure[§598.10(e)]}; {change-in-service [§598.10(a)(2)} or {when directed by the department[§598.1(g)(3)]} Y/N/X (not applicable)/1 (inadequate)/2 (not in SPR §598.1(k)(4) &§598.10(e)(4))	NA, no USTs		
28. If facility have written procedures to prevent deliveries to the wrong tank, are they referenced in SPR [§598.4(b)(7)]? Y/N/X (single tank with no other fill ports, or facility has mated connections)	X, in Terminal Operation Manual		
		•	
III. TRANSFER STATIONS & HAZARDOUS SUBSTANCE TRANSFERS	YES NO	<u> </u>	
29. Transfer station [§599.17(c)(2)]: Transfer stations must have a permanently installed secondary containment system. Containment system must have an acceptable spill containment volume; satisfy permeability to substance stored; constructed, coated, or lined with materials that are compatible with substance stored; and equipped with a sump and manually-controlled drainage system (must be locked closed). Y/X/N (no containment)/1 (not perm. installed)/2 (unacceptable cont. vol.)/ 3 (permeable)/4(not maintained)/5 (incompatible)/6 (no sump or lockable drainage valve)	Y		
To prevent mixing of incompatible substances: [§598.4(b)(7)] 30. Does the facility have written site procedures in SPR to prevent delivery to the wrong tank, fill ports with mated connections? Y/N/X (have written	X, Terminal Operation Manual		

31. Are remote fill/dispensing ports properly labeled at point of delivery. [§ 598.4(b)(8), 599.17(b)(1)(ii), 596.2(h)]? Tank ID#, chemical or common name, hazard warning, (for USTs - design & working capacities are required in addition) Y/N	X	
32. Valves for filling/emptying a tank are properly labeled for closed/open positions [§598.4(b)(8)]? Y/N	X	<u>.</u>
Storage of Solids and Non-Stationary Tanks:		
33. Are water soluble solids stored in non-stationary tanks and protected from stormwater [§598.5(f)]? Y/N/X/1 (floor is permeable)/ 2 (no enclosure or container does not prevent entry of stormwater)	NA	
34. Do non-stationary tanks satisfy performance standards [§598.5(g)]: Y/N/X/1 (proximity)/2 (enclosure for water reactive)/3 (impervious floor, curb, 110%, permeability)/4 (NSTs satisfy consensus code)/5 (stored in stable position)/6 (labeling & inventory records)	NA	

IV. ABOVEGROUND STORAGE TANKS/PIPING

	91	0 4	51	54		
Aboveground Storage Tanks * For tanks installed prior to 02/11/95, items marked with an asterisk are recommended but are NOT required until the tank system undergoes substantial modification						
Tank Volume if different than registered	10,000	10,000	5,000	5,000		
Date Installed	1960	1960	1970	1970		
35. Are daily visual inspections performed on AST systems [§598.7(a)]? Y/N	Υ	Υ	Υ	Υ		
36. Are temporarily out-of-service tanks (>30 days) properly closed [§598.10(b)]? Y/N/X	Х	Х	Х	Х		
37. Are permanently out-of-service tanks properly closed [§598.10(c)]? Y/N/X	Х	Х	X	Х	•	
38. Protected against scouring [§599.8(a)]? Y/N/X	Υ	Υ	Υ	Υ		
39. Tanks subject to melting are protected against fire [§599.8(c)]? Y/N/X	X	Х	Χ	Х		
40. Tank bottoms resting on soil are cathodically protected [§599.8(d)]? Y/N/X/1 (improper design)/2 (not insulated from piping)/3 (not isolated from stray current)	х	х	X	x		
41. Tank ≥ 5,000 gallons has a manway [§599.8(e)]? Y/N/X	Υ	Υ	Y	Y.		
42. Exterior surfaces are corrosion protected (painted) [§598.9(e) & §599.8(f)]? Y/N/X	Υ	Υ	Y	Υ		
43.*For tank bottoms resting on ground, tank is equipped with double bottom or impervious barrier[§599.8(g)]? Y/N/X("old tanks")	X	Х	Χ	Х		
44. Tanks are protected from explosion [§599.8(h)]? Y/N	Υ	Υ	Υ	Υ		
45.*Does tank have leak monitoring between bottom and secondary containment [§599.10(a)]? Y/N/X("old tanks")	x	x	x	X		
46. High level alarm, high-level trip, or automatic bypass to overflow tank is installed [§598.5(b); §599.17(b)(1)(i)]? Y/N/1 (not visible/audible at remote fill port)/2 (not operational)	Υ	Υ	Υ	Υ		

		<i>\</i>		<i>'</i> ''		\ '	/)	
	9\1	0	<u>51\</u>	54\	· ·	300000	\	<u> </u>
47. Level gauge [§599.17(b)(1)(iii)]								7.7
a. If a remote fill is present, is there a level gauge & flow control at remote fill port? Y (has both) / N (neither)/ X/1 (no gauge)/2 (gauge not operational)/3 (no flow control)/4 (flow control not operational)	Y	Y	Υ	Y				
b. If no remote fill port, is there a level gauge at the AST? Y(has gauge or tank is translucent)/ N/ 1(not operational)								
48. Vacuum and over pressurization [§599.18]?								
a. Vacuum and over pressurization equipment installed? Y/N	Y	Υ	Y	Y.				
b. Relief valves (safety, pressure, & vacuum) are properly labeled [§599.18(d)]? Y/N/X	Υ	Y	Υ	Υ				
49. Secondary Containment [§598.5(c) & §599.9].					70.7			
a. Tank has secondary containment? Y/N	Υ	Υ	Υ	Υ				
b. Spill containment volume is 110%? Y/N	Y	Υ	Y	Y				
c. Construction satisfies permeability of 1x10 ⁻⁶ cm/sec to substance stored? Y/N	Y	Y	Y	Υ		•		
d. Constructed, coated, or lined with materials that are compatible? Y/N	Υ	Υ	Y	Y				
e. Equipped with a sump and a drainage system which is manually-controlled from outside the diked area? Y/N	Υ	Y	Υ	Υ				
f. Is gravity drainage system valve locked closed)? Y/N/X	Y	Υ	Υ	Υ				
50. Valves for filling/emptying a tank are properly labeled for closed/open positions [§598.4(b)(8)]? Y/N	Y	Υ	Y	Υ				
51. AST tank properly labeled [§596.2(h); §599.17(b)(1)(iii)]? Tank ID #; chemical or common name; total cap./working cap.; hazard signs/NYSUFP&BC. Y/N	Ÿ	Υ	Υ	Y				
Aboveground Piping Systems 52. Are aboveground tanks/piping protected from atmospheric corrosion [§598.9(e)] & §599.13(c)(1)? Corrosion resistant eq; non-metallic cladding; paint; equivalent. Y/N (not corrosion protected)	Υ	Υ	Υ	Υ				
53. Does aboveground piping > 2" diameter have welded or flanged connections, or is constructed of plastic-lined metal piping with flared-end connections [§599.13(c)]? Y/N/X	Y	Υ	Y.	Υ				
54. Piping in contact with soil is protected from corrosion [§599.13(b)] Y/N/X/1 (improper design)/2 (not isolated from tank)/3 (not isolated	Х	Х	X	Х				
55. Automatic line leak detector for pressurized underground and on-ground piping [§598.6(c)(2)][§599,15(a)]?								
a. Is piping equipped with automatic line leak detector? Y/N/X	Х	Х	Х	X				
b. Is the leak detection system operable [§598.6(c)(2)? Y/N/X	Х	Х	Х	Х				
56.* Piping installed after Feb. 11, 1995 is properly labeled [§599.13(c)(4)]? Chemical name & placement at valves, pumps, switches, each side of wall, & each end of pipe. Y/N/X	х	х	x	х				
Pumps/valves are protected from leaks [§598.5(e)] using:								
57. Sealless or double seal pumps and values OR Y/N/X	1						1000	

			\ \ \ \			<u>\</u> .
			\angle		\angle	$\overline{}$
58. Pump/valve maintenance program, OR Y/N/X						
59. Pump/valves have secondary containment. Y/N/X / 1(permeable) /2(€ompatible)	- Υ	Y	Y	Y		
Valves/Couplings Used in Transfers [§599.17(b)(2)]:						
60. Valves/couplings are located within transfer station? Y/N/X	Y	Y	Y	Υ		
61. Dry disconnect valve provided on fill line? Y/N/X	Υ	Y	Y	Υ		
62. Check valve provided on fill line? Y/N/X	Y	Υ	Υ	Υ		
63. Control valve provided for each tank connection through which hazards substances flows? Y/N	ous Y	Y	Υ	Υ		

V. UNDERGROUND STORAGE TANKS/PIPING

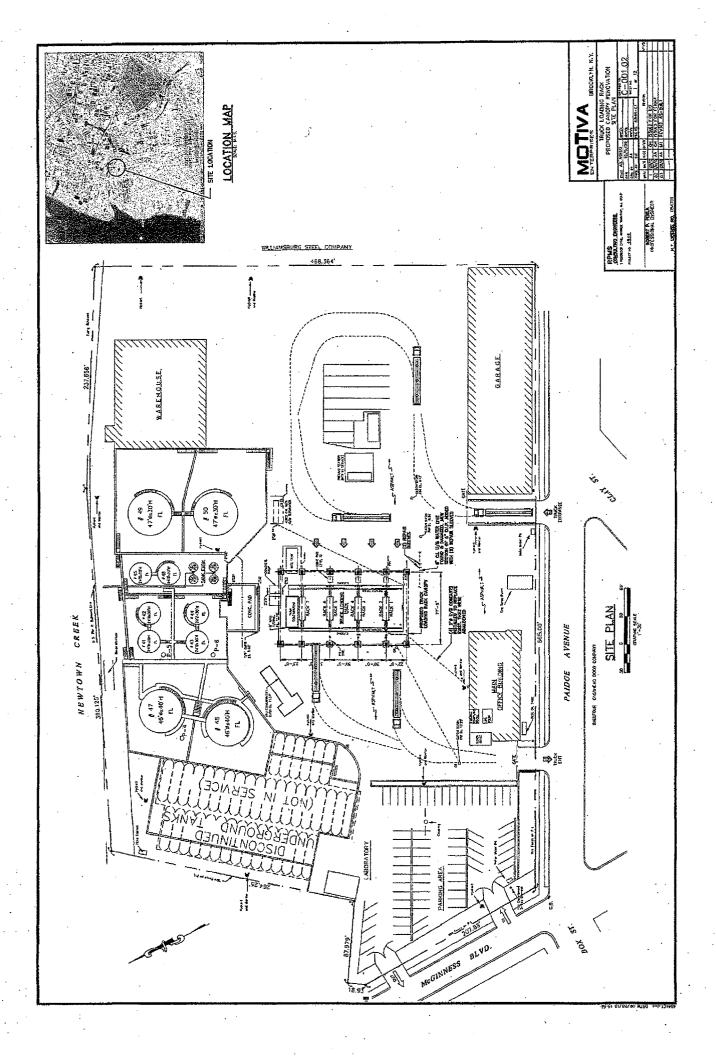
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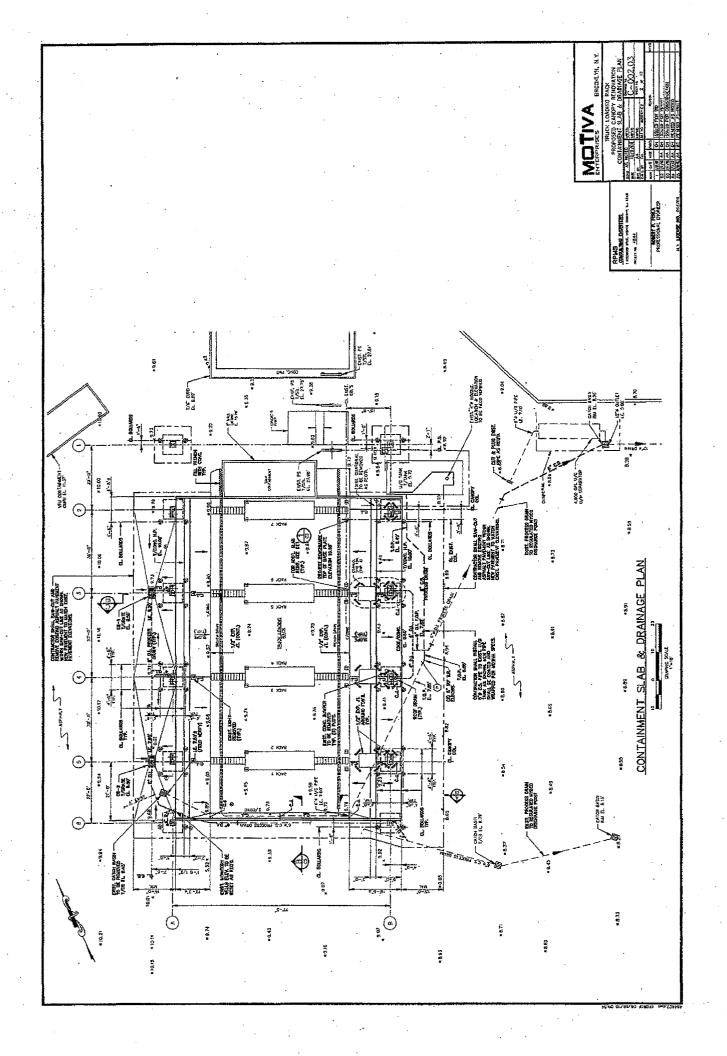
d. Allows for detection & collection of releases or spills until material is removed? Y/N						
e. Constructed of, or lined with, materials compatible with substance stored and having sufficient strength & thickness to prevent failure? Y/N						
f. Foundation suitable to prevent failure due to settlement, compression, & uplift? Y/N						
71. Does tank have leak monitoring §598.6 (b)(2)]?,[§599.5]? Y/N (not installed).	′					111
72. High level alarm, high-level trip, or automatic bypass to overflow tank is installed [§599.17(b)(1)(1)]? Y/N/1 (not visible/audible at remote fill port)/2(operational)			,			,
73. Vacuum and over pressurization [§599.18]? a. Vacuum and over pressurization equipment installed? Y/N						
b. Relief valves (safety, pressure, & vacuum) are properly labeled [§599.18(d)]? Y/N						
74. Valves for filling/emptying a tank are properly labeled for closed/open position [§598.4(b)(8)]? Y/N	ns					

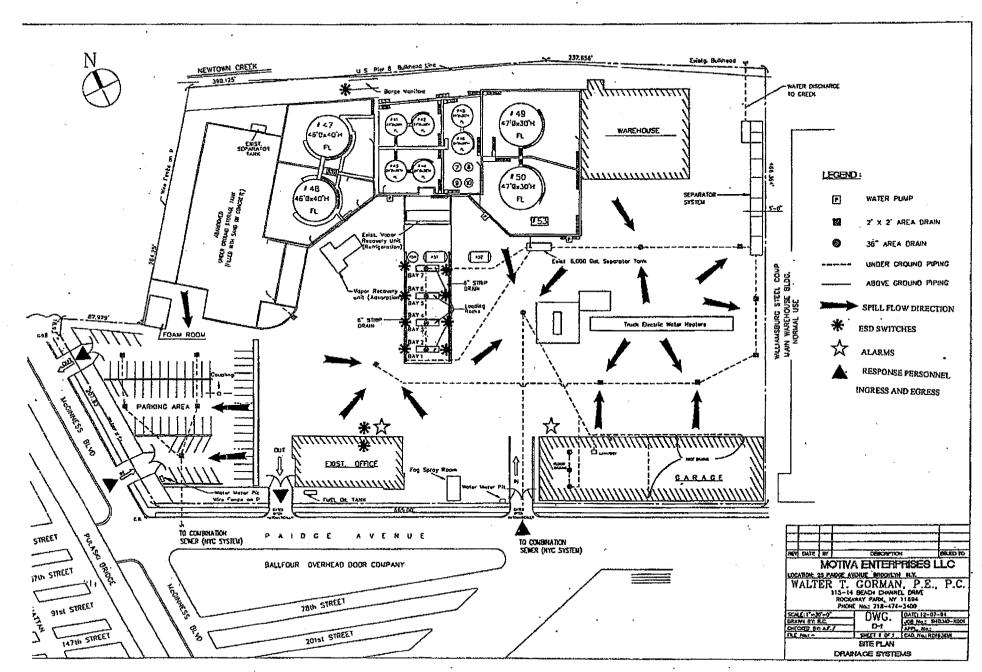
If no on-ground or underground piping, inspection is COMPLETED. On-Ground/Underground Piping:					
75. Secondary Containment [§599.14]					
a. Piping has secondary containment? Double wall, vault, or liner Y/N/X					
b. Construction satisfies permeability of 1x10 ⁻⁶ cm/sec to sub. stored? Y/N					
c. Designed, installed, and operated to prevent release to environment? Y/N					
 d. Allows for detection and collection of releases or spills until material is removed? Y/N 					
e. Constructed of, or lined with, materials compatible with substance stored and having sufficient strength & thickness to prevent failure? Y/N					
f. Foundation suitable to prevent failure due to settlement, compression, and uplift? Y/N					
 g. Sloped and operated to remove liquids resulting from leaks, spills, precipitation? Y/N 					
76. Automatic line leak detector for pressurized underground and on-ground piping [§599.15(a)]? a. Is piping equipped with automatic line leak detector? Y/N/X					
b. Is the leak detection system operable? Y/N/X					
77. Leak detection systems for piping - a. Is piping equipped with a leak detection system [§599.15(b)]? Y/N		·			
b. Is the leak detection system operable [§599.14(a)(2)(vii)]? Y/N					
78. Piping in contact with soil is protected from corrosion [§599.13(b)] Y/N/X/1 (improper design)/2 (not isolated from tank)/3 (not isolated from stray current)					

Y=Yes N=No X=Not Applicable Transfer Stations #29 AST #35 AG PIPING #52 UST #64

NOTES:			·
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DAILY CHECKLIST

MOTIVA ENTERPRISES LLC FACILITY REGISTRATION NUMBER 2-1940 25 PAIDGE AVENUE BROOKLYN, NY 11222

DATE: / / SHIFT:		
PERFORMED BY:		
YARD	TIME	STATUS
CHECK SEPARATOR FOR OIL ACCUMULATION / CREEK FOR SHEEN		
CHECK YARD FOR UNSAFE CONDITIONS	1	1
CHECK PERIMETER FENCING AND LIGHTING	 	
CHECK FOG ROOM / FOAM ROOM HEATERS AND PIPING	1	
DRAIN AIR COMPRESSOR YES INO	†	†
CHECK HAZARDOUS WASTE AREA		
FORKLIFT USED. YES / NO		
COMMENTS:	1	
		- · · · · · · · · · · · · · · · · · · ·
DOCK / TANK FARM 41-42-43-44-45-46-47-48-49-80-81-52-53-54-55 9/10	TIME	STATUS
CHECK ALL VALVES, PUMPS & MOTORS FOR UNSAFE CONDITIONS / LEAKS		
GAUGE TANKS, CHECK TANKS, PIPING, COUPLINGS, FLANGES FOR LEAKS	 	
CHECK STAIRWAYS / CROSSOVERS FOR UNSAFE CONDITIONS		
RECEIVING BARGE OR PIPELINE		
CHECK DOCK LINES FOR PRODUCT SEEPAGE, WASTE & SEWAGE		
CHECK DOCK SYSTEM FOR DISCHARGE AT CREEK	l	
CHECK CONTAINMENT FOR SIGNS OF DEBRIS, EROSION, CRACKS, DISCOLORATION,	 	
SIGNS OF SPILLED OR LEAKING PRODUCT (SIGHT, SOUND, SMELL)	 	
COMMENTS:	L 	<u> </u>
A A 4 M M M M M M M M M M M M M M M M M		
VAPOR RECOVERY	TIME	STATUS
DRAIN VAPOR LINE EACH SHIFT		
USE CHECKLIST ONCE PER WEEK		
CHECK FOR LIQUID AND VAPOR (SIGHT, SOUND, SMELL) LEAKS, PRESSURES, UNSAFE		<u> </u>
CONDITIONS DURING TRUCK LOADING	j	
COMMENTS:		
RACK5	TIME	STATUS
CLOSEOUT		
CHECK ADDITIVE		
CHECK FOR UNSAFE CONDITIONS, LIQUID AND VAOPR LEAKS (SIGHT, SOUND, SMELL) DURING TRUCK LOADING		
SROUND CABLES / AIR HOSE OK / NG SCULLY SYSTEM OK / NG		
OADING ARMS / COUPLER CONDITION OK / NG		
CHECK DRAIN VALVE UNDER RACK 7 (NORMALLY CLOSED) OPEN / CLOSE		
COMMENTS:		/

NOTIFY SUPERVISOR OF ANY POOR CONDITIONS IMMEDIATELY LEAKS DETECTED MUST BE REPORTED TO TERMINAL SUPERINTENDENT PLEASE INSERT G = GOOD P = POOR IN STATUS

Date: Terminal: Brooklyn	inspected	Ву:	·	·	
	51	52	53	54	55
	yes / no	yes / no	yes / no	yes i no	yes / no
I. Foundation	•	:			
A. Is there any discoloration visible?	• •	n/a	n/a	1	n/a
B. Are there any cracks, settling gaps, vegetation roots?	0	ก/a	n/a	1	n/a
C. Is there any puddle containing spilled or leaked material?	S	n/a	n/a	1	n/a
D. Does water drain away from the tank?	0	n/a	n/a	1	n/a
E. Is any erosion evident?	0	n/a	n/a	1	n/a
F. Is bottom angle free of rock and/or other debnis?	8	n/a	n/a	1	n/a
Comments:		!			
II. Shell			,		
A. Visually inspected for paint failures, pitting, drip marks,	0	n/a	1	1	I^{*}
discoloration and corrosion (tank is free of defects)?	0				
B. Any evidence of seam seepage, cracks, bulges or indentations?	s	nia		1	1
Comments:					
III. Shell Appurtenances					
A. Are there any cracks or signs of seepage on weld joints at	0	1	1	1	1
nozzies, man ways and reinforcing plates?					
8. Is there evidence of seepage around bolts at flanges & valves?	0	1	:1	<i>t</i>	1
C. is the visual (automatic) gauge operating properly?	S	1	1	1	1.
Comments:					
1V. Roof		·			
A. Visually inspected for paint failures, pitting & corrosion on roof deck (roof is free of defects)?	0	n/a	.1	1.1	1
B. Is there evidence of seepage around bolts at flanges and fittings?	0	n/a	1	1	1
C. Inspected floating roof through roof hatch for: roof resting properly on	S	n/a	j	1	1
liquid surface, water or product on pan, gaps between roof &					
shell, tears, holes or separation of seal and other roof defects (roof is free of defects)?					
Comments:					

		51	52	53	24	บบ
		yes / no	yes / no	yes I no	yes i no	yes / no
	V. Roof Appurtenances			•		٠
-4	A. Have checked all hatches and vents (working properly)?	0	n/a			
TTOE	B. Have inspected gauge well (free of debris)?	0	n/a:	1	<u> </u>	1 .
- 30	C. Access hatches have been inspected & are free of debris, hazards or corrosion?	S	n/a	1	t .	1 -
	Comments:	······································		· ·	·	
	VI. Containment & Drainage Areas					
	A. Dike or Berm System					
	Checked level of precipitation in dike, is there capacity?	0	n/a	n/a	n/a .	I^{-1}
	Inspected (left closed) drainage valve to insure operation?	0	n/a	n/a	n/a	1
	Checked for debris & verified there was none evident?	5	n/a	n/a	n/a	1
	Any signs of erosion?	0	n/a	n/a	n/a	1
	Inspected dike and basin area for integrity (No breaches)?	S	n/a	n/a	п/a	1
es.	Comments:					
ENTERPRISES	B. Secondary Containment (steal)				•	
93	Inspected for cracks?	n/a	n/a	n/a	n/a	nla
氫	Any signs of corrosion?	r√a	n/a	n/a	n/a	r√a
MOTIVA	Checked for discoloration?	n/a	n/a	n/a	n/a	n/a
O.E.	Is there any standing liquid?	n/a	n/a	n/a	n/a	n/a
200	Inspected drainage valve condition?	n/a	n/a	n/a	n/a	n/a
	Comments:	. ·				
8	C. Retention and Drainage Ponds					
7970	Checked for debris?	n/a	n/a	n/a	n/a	n/a
	Any sign of erosion or stressed vegetation?	n/a	n/a	nya	n/a	n/a
383	Checked available capacity?	п/a	n/a	n/a	n/a	n/a
718	Is there any standing liquid?	ก/ล	, n∕a	R/a	n/a	n/a
FAX	Comments:					
5:37	VII. Double Bottom Installations		•	-		
	A. Opened & checked monitoring valves for liquid detection?	n/a	n/a	n/a_	n/a	n/a
010	Glosed valves after inspections?	n/a	n/a	n/a	n/a_	n/a
2	B. Inspected double bottom shell wall?	n/a	n/a	nla	n/a	n/a
10/21/2010		•				
1						

C	. Where cathodic protection is installed?
	Inspected the test station for damage?
	Is the header wire from the anode to the test station OK?
	For older installations are the anodes (which pass through the tank shell
	welded to the shell?
	·

51	52	53	54	55
yes / no	yes / no	yes / no	yes / no	yes I no
n/a	n/a	n/a	n/a_	n/a
n/a	n/a	n/a	n/a	n/a
n/a	n/a	n/a	n/a	n/a
π⁄a	n/a	n/a	n/a	n/a

Comments:			 	· · · · · · · · · · · · · · · · · · ·		
VIII. Comments		•				
(reference tank ar	nd Item number from abo	ove; if appropriate.)				
			 		•	
		·				·
						4.
	,					

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ANNEX 10

NEW YORK SPILL PREVENTION REPORT (6NYCRR 598.1(k))

TABLE

	Pursuant to <u>598.1</u>	Section
General Information Current Registration Application and Certificate Management Approval and Certification Name & Signature of qualified person who prepared the Report (NYS Professional Engineer or Qualified Person)	(k)(2)i (k)(2)ii (k)2)iv	Annex 10, Attachment 1 Annex 8, Section 8.2.3 Annex 10, Attachment 2
Facility Map Locations and identification of tanks, transfer stations & piping	(k)(2)iii	Annex 1
Summary of Releases During Past Five Years	(k)(2)v	Annex 4, Section 4.2
Identification and Assessment of Causes of Releases	(k)(2)vi	Annex 7, Section 7.1
Compliance Status	(k)(2)vii	Annex 10, Attachment 3
nspections	(K)(2)viii	Inspection Program described in Annex 7, Section 7.5.4, 7.7.1, 7.7.2, 7.7.3
General Daily		Start of Shift Checklist and SPCC Checklist located at the end of Annex 7
Monthly		Monthly inspections are performed, although not required under this section
Annual		 (1) Annual inspections of cathodic protection systems are performed and maintained in a separate report. Reports are maintained on site (2) Tanks, secondary containment systems, and equipment are inspected daily – See Forms in Annex 7
Five-Year		Five-Year inspection records maintained on site
Financial Responsibility (If applicable)	(k)(2)ix	N/A – will be provided to NYSDEC upon request

Annex 10, Page 3

pill Response Plan	(k)(2)x	Core Plan, Annexes 1, 2, 3, 4, 5, 7, 8 & 9
Discussion and Assessment of Equivalent Equipment, Method, or Practice (If applicable)	(k)(3)	N/A
Site Assessment and Findings (If applicable)	(k)(4)	N/A
Spill Reporting Form		Core Plan, Section 1.1.3
Written Procedures for the Prevention of Mixing of Incompatible Substances (if applicable)	598.4(b)(7)	N/A – Storage/handling of petroleum products and fuel additives does not present a compatibility concern under this section (all materials are compatible)

ANNEX 7.... PREVENTION

7.1..... HAZARD EVALUATION

7.1.1..... Potential for Contamination

The potential for contamination offsite is considered very slight. Each aboveground tank is contained in a concrete dike structure with concrete floors. The greatest potential for contamination is at the Dock facility where transfers occur over water.

7.1.2..... Tank Farm

Table 7-1 lists all tanks present at the Brooklyn Terminal including the substance stored. The prefix "A" indicates an aboveground tank and the prefix "B" indicates a below ground tank. The table indicates the tank type, the year originally installed; maximum volume in gallons, the possible types of failure, the prediction of flow rate and the direction of flow for all tanks. Surface impoundments are not used for product storage at this Facility. The words "tank" and "container" can be used interchangeably in the document.

7.1.3...... Estimates of Quantity of Oils Potentially Discharged

The estimates of the quantity of oils potentially discharged are shown in Table 7-1.

The Facility is a bulk storage terminal handling several types of petroleum products. The Facility receives petroleum from Buckeye Pipeline, truck, or incidental barge. The Facility stores it and transfers it to customers through the truck loading rack.

The potential for release of gasoline during a pipeline or barge receipt is dependent upon the rate at which material is pumped from the pipeline or vessel. The Facility receives products from either the pipeline or from a vessel at a maximum delivery rate of 5,400 barrels per hour.

7.1.4..... Possible Spill Pathways

The Facility is located in Brooklyn, New York on the shore of Newtown Creek. Any release from the piping at the Dock has the potential to directly impact Newtown Creek.

Site overflow drainage would most likely gently flow northeast on the Facility's property. Drainage from the employee parking lot and the washbay drain in the garage is to the City Sanitary and Sewer System.

TABLE 7-1 DESCRIPTION OF ABOVEGROUND AND BELOW GROUND STORAGE TANK STORAGE

eficank or						Containment
Source	Substance Stored	Tank Type or Surface Area	Year Installed	Type of Failure	Volume (gallens)	Capacity (gallens)
A41	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	188,184 ¹
A42	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	
A43	Gasoline	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	187,782 ²
A44	Gasoline	int. Floating Roof	1945	Overflow, rupture, leak	90,700	
A45	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	240,859 ³
A46	Ethanol	Int. Floating Roof	1945	Overflow, rupture, leak	90,700	
A47	Gasoline	Int. Floating Roof	1960	Overflow, rupture, leak	442,062	519,886 ⁴
A48	Gasoline	Int. Floating Roof	1960	Overflow, rupture, leak	445,126	490,187 ⁴
A49	Gasoline	Int, Floating Roof	1969	Overflow, rupture, leak	484,042	992,332 ⁴
A50	Gasoline	Int. Floating Roof	1969	Overflow, rupture, leak	483,790	
A51	oos	Horizontal	1987	Overflow, rupture, leak	5,000	15, 625 ⁵
A54	Puradd Gas Additive	Cone Roof	1993	Overflow, rupture, leak	5,000	

Note: Based on Tank inspections both internal and external, and prevention measures in place, the potential for a discharge is remote.

* A = aboveground tank B = belowground tank

** Prediction of rate of flow- pinpoint leak to catastrophic collapse

Direction of Flow - Northeast

Note¹: These tanks are within the same containment.

Note²: These tanks are within the same containment.

Note³: These tanks are within the same containment.

Note⁴: These tanks are contained within their own containment area.

Note⁵: These tanks are contained within their own containment area.

TABLE 7-1 DESCRIPTION OF ABOVEGROUND AND **BELOW GROUND STORAGE TANK STORAGE (Cont'd)**

Tank or Source ID*	Substance Stored	Tank Type or Surface Area	Year Installed	Type of Fallure	Maximum Volume (gallons)	Containment Capacity (gallons)
A53	Slop Tank	Horizontal	1993	Overflow, rupture, leak	6,000	598,000 ⁴
A55	oos	Horizontal	1999	Overflow, rupture, leak	10,000	12,000 ⁶
A7	oos	Horizontal	1945	Overflow, rupture, leak	9,600	228,000 ³
A8	oos	Horizontal	1945	Overflow, rupture, leak	9,600	228,000 ³
A9	Ultrazol Gas Additive	Horizontal	1945	Overflow, rupture, leak	9,600	228,000³
A10	Nemo	Horizontal	1945	Overflow, rupture, leak	9,600	228,000 ³
	O	THER POTEN	ITIAL SPI	LLSOURC	ES	1 2
A Recovery Well Tank	Petroleum Contact Water	Horizontal	1999	Overflow, rupture, leak	275	560
Rack Separators	Petroleum Contact Water	Horizontal	1940s	Overflow, rupture, leak	6,000	N/A
B Final Separator	Petroleum Contact Water	Horizontal	1940s	Overflow, rupture, leak	25,000	N/A
B 52	Rack Water Containment	Horizontal with cement vault	1989	Overflow, rupture, leak	4,000	6,800

Note: Based on Tank inspections both internal and external, and prevention measures in place, the potential for a discharge is remote.

A = aboveground tank B = belowground tank

Prediction of rate of flow-pinpoint leak to catastrophic collapse Direction of Flow - Northeast

Note¹: These tanks are within the same containment.

Note²: These tanks are within the same containment.

Note³: These tanks are within the same containment.

Note⁴: These tanks are contained within their own containment area.

Note⁶: These tanks are contained within their own containment area.

Note⁶: This tank is contained within a vault.

TABLE 7-1 DESCRIPTION OF ABOVEGROUND AND **BELOW GROUND STORAGE TANK STORAGE (Cont'd)**

	OT	HERPOTE	NTIAL SP	ILL SOURC	ES	
Tank or Source ID*	Substance Stored	Tank Type or Surface Area	Year Installed	Type of Fallure	Maximum Volume (gallons)	Containment Capacity (gallons)
Loading Rack(s)/ Transfer Area(s)	Petroleum Products	N/A	Various	Valve Failure; Leak	N/A	Catch Basins
Pipeline/ Pumps	Petroleum Products	N/A	Various	Receiving	N/A	Tank/Catch Basins
Vapor Recovery Unit	Condensate/ Glycol	N/A	Unknown	Maintenance	110	110
Garage/ Used Oil	Used Oil	Horizontal	1988	Overflow, rupture, leak	280	400
Water Collection	Petroleum Contact Water 7@700 gal. tanks	Horizontal	Various	Overflow, rupture, leak	4,900	> 700 gal. (inside dike walls)
Prover	Gasoline/ Distillates	Steel	Unknown	Overflow, rupture, leak	1,000	> 1,000 (use under truck rack)
			DRUMS			
Lessee Storage Areas	Various Petroleum Products	Drums, Pails, Cases		Overflow, rupture, leak	50,000	Inside Building
Drum Storage Area	Glycol/Red Dye	Drums 4@ 55 gals.		Overflow, rupture, leak	220	6,800
Satellite Accumulation Area	Petroleum Debris	Drums 1@ 55 gals.	25,41=-	Overflow, rupture, leak	55	755 gal (inside truck rack)
Garage/ Grease	Grease Oil	Drums 6@ 55		Overflow, rupture, leak	330	> 55 gal (inside warehouse)

A = aboveground tank B = belowground tank

Prediction of rate of flow-pinpoint leak to catastrophic collapse Direction of Flow - Northeast

Note1: These tanks are within the same containment.

Note²: Note³: These tanks are within the same containment. These tanks are within the same containment.

These tanks are contained within their own containment area. Note^{5;}

These tanks are contained within their own containment area.

This tank is contained within a vault.

7.1.5 Diked Areas

All aboveground storage tanks at the Brooklyn Terminal are completely surrounded by containment dikes. Spills from the storage tanks or related product and pipeline will be contained within the diked areas and pumped out over the dike walls in accordance with NYFD requirements. Air pumps equipped with hard pipe suction are used to transfer accumulated precipitation to the oil/water separator system prior to discharge through Outfall 001.

The Facility's truck loading rack, truck pump-off area, and additive unloading is equipped with curbs, roof and strip drains designed to hold the contents of the largest single compartment on a tank truck. The spill containment system drains to a 4,000-gallon underground tank. The tank is emptied as needed and the material is transported off site for disposal. The additive unloading and truck pump-off areas are located adjacent to the truck loading rack.

Discharges from paved yard area catch basins, tank truck parking area, warehouse loading platform, garage drains (excluding wash bay), and pump out from the VRU goes to the final separator prior to discharge through Outfall 001.

The final separator is equipped with a mechanical shut-off valve that prevents flow through until the oil is pumped out of the separator. Treated water from the separator is discharged under the Facility's SPDES permit.

Drawings of the spill control drainage plan for the Facility are shown in the Core Plan, Figure 1.4 and in Annex 1. These drawings indicate the general arrangement of the fixed facilities that will prevent the release of oil and petroleum to the environment.

7.1.6 Undiked Areas

The major portion of the tank farm piping is run in the tank farm containment area or in the protected truck loading rack area. The remaining piping is run aboveground and over the protected truck loading rack area and asphalt yard area. All other drainage of the paved area flows toward catch basin drains located throughout the Facility that ultimately drains to the final separator and processed prior to discharge.

7.1.7 Schematic Drawing of Facility

A schematic drawing of the Brooklyn Terminal with all tanks labeled is provided in the Core Plan, Figure 1.2, and in Annex 1, Figure 1.2.

7.1.8 Procedures for Routine Handling of Products

The Brooklyn Terminal has a number of established procedures in use for truck loading and transfer operations. The Facility receives products from either pipeline or barge at an average delivery rate of 5,400 barrels per hour for gasoline.

7.1.8.1Loading (Receiving) Procedures

To provide a dependable safeguard against tank overfilling, each of the storage tanks receiving product is equipped with a two-stage high-level alarm system. In an overfill situation, both a visual and audible alarm is set off, followed by a third high-high alarm which will automatically close the valve on the receiving line to effectively shut off the transfer of product into the tank and prevent an overfill. The primary alarm is set at 90% fill capacity and with a visual white light, secondary alarm at 95% fill capacity with an amber light and shut down audible alarm, and the tertiary alarm is at 98% fill capacity with a red light and shut down alarm. The Buckeye Pipeline is equipped with an automatic shut down system if a high-high (secondary or tertiary) alarm is received, while the dock operation has manual shut down devices during product receipts.

The Facility has secondary containment around each storage tank that is described in Annex 7.2. This dike has sufficient capacity to contain any expected overflow or tank rupture.

No person is allowed to handle the receipt of products unless he or she has been thoroughly trained and has demonstrated the ability to perform these procedures. Additional details on employee training are contained in Annex 5 of this Plan.

a. Preparation of Tanks Prior to Pipeline or Vessel Receipt

Prior to the receipt of product, the tank(s) are manually gauged and a product storage tank temperature taken. The exact time the gauge was taken, depth of water, (if any), the product depth, and temperature are entered in the Facility gauge worksheet. The person taking this gauge will initial the gauge worksheet. The gauger will calculate the headroom in the storage tank(s) scheduled for receipt to ensure the tank(s) will hold the amount of the receipt.

The designated responsible person for the Facility will arrange to open the manifold receiving valves and the tank receiving valves. Receipt valves and high level alarms are tested.

Other procedures for receipt by pipeline or vessel are specified in the Operations Manual.

b. Procedures During Receipt of Product

The following descriptions are general in nature and for informational purposes only. The Facility's operating procedures and instructions govern the receipt of product. These procedures are maintained in the Terminal Office.

Qualified personnel will be on duty during receipt of product. These personnel receive periodic refresher instructions on the correct procedures to use during product transfer. The person in charge of receipt of the product follows local Facility procedures for receipt of product.

After product has started to flow, the qualified person walks the pipeline to the receiving tank checking for leaks. At the tank, the automatic gauge is checked to assure product is flowing into the proper tank.

During the tank receipt, the person in charge will calculate a rough gauge (final height) for the receiving tank. Thereafter, the person in charge of the receipt will check the tank gauge (product level) at least once an hour.

If the tank is to be filled to near capacity, it will be gauged more often when the tank is nearly full. The qualified person will remain on watch on the platform of the tank (or other suitable observation location) during the last half hour of pumping. After each hourly gauge, the receiving lines will be walked to check for leaks.

If more than one tank is on a delivery line, the tank not receiving product will be gauged prior to start of delivery and at the first hourly gauge to make sure there is no leak in its valve or confusion in quantities received that could possibly cause an overfill of the tank.

c. After pumping procedures

After completion of the receipt, external valves on the delivery line will be closed. The tank will be manually gauged and measured for water and the temperature of the produce will be accurately measured at the midpoint of the product. This information will be recorded in the gauge worksheet along with the time receipt was completed. The qualified person will initial the entries in the gauge worksheet for identification.

d. Communications During Receipt

(1) When product is received by marine transport - On barge receipts, visual and oral communication is maintained between the vessel's hose watch and the Facility's hose watch. Product to be received, pumping rate and batch size are reviewed prior to start-up. Adequate sets of portable, intrinsically safe transceiver radios are available and used, which enables direct communication between pumping station or vessel, hose watch and tank watch.

7.1.8.1 Loading (Receiving) Procedures (Cont'd)

d. Communications During Receipt (Cont'd)

(2) When product is received by pipeline, the person responsible for the receipt maintains the frequent communication with the pipeline company. Meanwhile, another person is constantly gauging the tanks while communicating via intrinsically safe radios with personnel in the office. Any changes (such as type of product, quantity, amount of room in the tank, the need for pipeline wash, and other appropriate information) are exchanged between the pipeline and the Facility.

7.1.8.2.... Tank Truck Procedures

a. Receipt of Product by Tank Truck

Receipt of product by tank truck is scheduled by Facility personnel. The procedures covering the receipt of product by tank truck are specified in the *Terminal Operations Manual*. Those procedures and Facility operating procedures and instructions control the receipt of product. The following description is for the purposes of information only. The procedures and instructions are maintained in the Terminal Office.

Preparation includes assignment of qualified personnel to receive the product. The truck unloading area is maintained free of obstacles. Should any accidental discharge occur, the area is graded to discharge into strip drains that go to a primary separator and then to the final separator prior to discharge.

- A fire extinguisher is maintained at the pump-off spot.
- Only qualified employees are permitted to pump-off transport trucks.
 These individuals are trained in the prescribed loading / unloading procedure for tank trucks according to instructions in the training manual.
- ◆ The transport truck is attended at all times during the unloading process to provide instant shut down in case of an emergency.
- ♦ All pump-off lines are capped, all valves kept closed, and the tank valve locked except when in use.
- No mobile storage tanks are at the Facility.

7.1.8.3.... Tank Truck Loading Procedures Using the Loading Rack

a. Transfer of Product Into Tank Trucks

The Facility uses an automated system for the transfer of product into tank trucks. The system is designed to prevent spills and overfills. As an additional precaution against spills, the drivers are permitted to use the truck rack control system and have received instruction from Motiva on the correct procedures to use in accessing the system, safety precautions, and spill reporting.

7.1.8.3.... Tank Truck Loading Procedures Using the Loading Rack (Cont'd)

a. Transfer of Product Into Tank Trucks (Cont'd)

The general procedures for operation of the truck rack control system are found in the *TMS System User Manual* located in the Terminal Office.

Only authorized truck drivers can gain access to the loading rack by presenting an authorization card and entering a unique driver code number (PIN).

The trucks are bottom loaded at this Facility. The trucks are equipped with a loading bar or brake locks that lock the brakes and prevent the truck from starting.

The drivers are instructed to carefully inspect vehicles to make sure that bottom valves are not leaking. Trucks are occasionally spot inspected. In the event that a vehicle fails inspection the truck will be barred from the Facility until the necessary repairs have been completed.

The automatic loading equipment also verifies that the driver has connected the grounding, overfill protection equipment, and vapor connection. This ensures that the truck is properly grounded to reduce the potential for static electrical discharges and that the truck overfilling protection equipment is properly operating. While loading, drivers must hold a "dead man" button or pumps while shut down and product will not flow to the truck.

When the driver completes loading he or she proceeds to the bill of lading printing area, obtains the bill of lading, opens the automatic gate, and leaves the Facility. Once the truck is loaded, the driver has custody of the shipment and is responsible for safe delivery of the product. Despite the fact that the driver is still inside the Facility gates, the driver is responsible for the shipment, and any spills that occur at that point will be considered transportation related.

b. Specific Procedures in Use for Truck Loading

Specific procedures in use for truck loading at the Facility are described in the *Terminal Operations Manual* and in specific terminal operating procedures. These are kept in the Terminal Office files.

- The Facility has specific safety procedures that include requirements for trucks to park away from the loading rack when awaiting the opportunity to load product.
- Loading will be stopped during severe electrical storms.
- Smoking permitted in designed areas.

7.1.8.3.... Tank Truck Loading Procedures Using the Loading Rack (Cont'd)

b. Specific Procedures in Use for Truck Loading

- Under no circumstances will a truck in the process of loading be left unattended or will it be parked at the rack unattended.
- All truck lights, heaters, accessories, and non-operating electrical equipment will be turned off before entering the loading area, and will only be turned on after leaving.
- Any stalled trucks will be towed away from rack prior to repairs.
 Booster batteries will be connected more than 100 feet away.
- All DOT regulations will be followed.

7.1.8.4.... Facility Tank Truck Loading and Unloading Facilities

a. Description of Drainage and Barrier Systems

The Facility's truck loading rack has a drainage system that is designed to hold the contents of the largest single compartment on a tank truck. The spill containment system has a cement slab with drain inlets and strip drains connected to a 4,000-gallon underground tank. The truck pump-off and additive unloading areas are also located within the loading rack area. The additive unloading area utilizes the same containment system as the loading rack. The holding tank is emptied as needed.

The truck rack is covered by a large canopy to minimize rainwater collecting at the rack. Any liquid (water, melted snow or hydrocarbon) that falls beneath the canopy flows by gravity to a sub surface holding tank where it is manually emptied via a vacuum truck.

b. Disconnect Protection Systems

All trucks that load at the Facility have either a locking bar or other interlocking system to prevent the truck from being moved while the vapor recovery and/or loading hoses are still connected to the truck. All trucks are also equipped with over-fill protection and are grounded to ensure further safety. Truck over-fill protection is tested annually by the carrier for every truck and records are kept in the Terminal Office.

c. Examination of Bottom Drains on Vehicles

The drivers are instructed to carefully inspect vehicles to make sure that bottom valves are not leaking. In the event that a bottom valve is discovered leaking, the truck will be barred from the Facility until the necessary repairs have been completed.

7.1.8.4 Facility Tank Truck Loading and Unloading Facilities (Cont'd)

d. Overfill Protection System

The overfill protection system shall be checked for proper operation prior to loading.

7.2..... SECONDARY CONTAINMENT

7.2.1 Dikes and Dike Capacity

The Facility tanks are surrounded by dikes that have a capacity in excess of the largest of the tanks plus an allowance for rainfall. The total storage capacity of the tank farm containment area is adequate to contain the largest tank (450,000 gallons) and has enough volume for a rainfall allowance.

The volumetric capacity of the containment areas has been prepared by David Martin, Motiva Enterprises, and RPMS Engineers.

7.2.2..... Dike Integrity

Diked areas are sufficiently imperious to contain spilled oil. Containment walls and floors are fully intact and have no permeable voids. The tank farm containment dikes are constructed of concrete. The additive tanks are contained within concrete containments or contained within underground containment areas.

7.2.3 Curbing

The other principal area that could result in a release of petroleum is the truck loading rack. The loading rack has curbs to direct any potential spilled product to flow by gravity to a sub-surface holding tank where it is manually emptied via a vacuum truck. The loading rack containment system is substantially larger than the largest single compartment that could spill on the rack.

7.2.4...... Culverts, Gutters or Other Drainage Systems

The Facility removes tank water bottoms by transferring it into water collection tanks, then the water is pumped to a holding tank and the product is returned to storage. The tank is contained within a concrete containment dike that is adequately sized to contain the entire contents of the tank plus sufficient freeboard.

Dock drainage procedures (booming equipment and drip pans) are covered in the Dock Operations Manual.

7.2.5...... Retention Ponds

This Facility does not have a retention pond.

7.2.6 Sorbent Materials

All sorbents used for spill response will be supplied by contracted OSROs.

7.2,7...... Positive Controls to Prevent Drainage From Diked Areas

The positive controls used to prevent drainage from diked storage areas include procedural controls and equipment to prevent the discharge of oils from all areas of this Facility.

- The preferred method of removal of accumulated stormwater is by natural evaporation provided that the accumulation does not damage the equipment / structures or inhibit operations conducted within the containment area.
- ◆ In the event that drainage of an area becomes necessary due to accumulated stormwater, the containment area air pumps equipped with hard-pipe suction and discharges are pumped to the oil/water separator outside the diked area then to the final separator prior to discharge through Outfall 001. If a visible sheen or other condition indicating the presence of oil or gasoline is present, the valves are not operated.
- In the tank farm area, all tank water withdrawal valves are closed and locked when not in use. All basin drain valves, where installed, are closed and locked when not in use. When the basin drain valves are operated, the water in the basin is inspected by an employee prior to operation of the valve.
- Accumulated water is visually inspected for oil and / or oil product contamination (sample procedures and documentation forms are provided in Annex 7) and discharged only if no contamination is observed.
- The Facility does not have an effluent treatment facility.
- In the event that drainage of contaminated liquids from a containment area is required, the use of a vacuum truck, pump, or other means will be evaluated for the removal.

7.2.8...... Disapproval of Flapper-Type Drain Valves

Flapper-type drain valves are not used in this Facility.

7.2.9...... Drainage from Undiked Areas

This topic is discussed in detail in Annex 7.1.6.

7.3...... BULK STORAGE INSTALLATION

7.3.1 Material Compatibility Standards

The Facility's bulk oil and oil product storage tanks have been designed in accordance with industry standards. The tanks have the following design characteristics:

- ◆ Tanks are constructed of a material that is compatible with the oil and petroleum products stored and the conditions of storage.
- ◆ Tanks are operated within "Safe Fill" levels positioned below the established capacity limits of the tank.
- ♦ A conversion of tanks or construction of a new tank for Ethanol is constructed at regulatory standards. A Management of Change for the standard is completed to cover an Ethanol change.

7.3.2..... Secondary Containment Sufficiency

A discussion of the secondary containment sufficiency for this Facility is presented in Annex 7.2 above.

7.3.3 Drainage Bypass Systems

The Facility does not have a bypass system for Facility drainage.

7.3.4...... Underground Metallic Storage Tanks

There is one underground storage tank at this Facility. The tank is registered, within a cement vault, and provided with cathodic protection.

7.3.5 Partially Buried Metallic Storage Tanks

There are no partially buried metallic storage tanks at this Facility.

7.3.6...... Integrity Testing Standards for Aboveground Storage Tanks

The tank integrity and testing standards are discussed in Section 7.10.

7.3.7 Internal Heating Coils

There are no internal heating coils in any of the Facility tanks.

7.4...... DISCUSSION OF FAIL SAFE ENGINEERING AND DESIGN STANDARDS

As far as practical, the Facility has been engineered to fail-safe engineering standards. The fail-safe provisions include, but are not limited to:

 Automated truck loading rack system that allows the loading of trucks with maximum safety.

- ◆ The use of large loading rack roof to minimize the entry of rainwater into the loading rack.
- ◆ The use of audio high-level alarms on all tanks that receive product from the pipeline or vessel.
- ◆ The use of tank dikes to prevent petroleum from flowing from the Facility property.
- ◆ Tank inventory is maintained by the Alliance Distribution Measurement Policy.
- The policy manual is a separate document located at the Terminal Office.

7.4.1 High Liquid Level Alarms

Motiva Enterprises LLC petroleum storage tanks have high liquid level alarms that have audible signal to detect high levels during filling operations. Upon hearing a high-level alarm, Facility Personnel will check the tank and tank level to verify its contents and integrity. This Facility also has valves with fusible link cut-offs to stop a high-flow event. Alarms are tested on a regular basis.

Tank high-level alarms and gauging devices are tested by pulling alarms and verifying manual versus automatic gauges prior to every receipt by the Terminal Operators. Tank high-level alarms are inspected by a certified electrician annually. Tank high-level calculations are reviewed and verified annually by Terminal Management.

7.4.2..... Emergency Shut-off Devices

The Buckeye Pipeline will shut down flow to the Facility immediately upon receiving a high-high (secondary or tertiary) level alarm. Upon receiving the high-high level alarm, the Buckeye Pipeline will automatically close pipeline valves to the Facility. The pipeline can shut down flow within five minutes in an emergency.

7.4.3...... Direct Communications Between Facility and Pipeline

The Terminal Operator and the Buckeye Pipeline Operator communicate verbally before each receipt. For attended receipts, communication is maintained after flow has started and at the completion of each receipt.

7.4.4..... Fast Response Gauging Systems

The Facility uses quick response manual gauges that enable the Terminal Operator to determine the level in each of the tanks. The tank gauges are float-style gauges.

7.4.5 Visible Oil Leaks

Cleanup of all oil leaks starts on discovery and will be completed in a safe and expedient manner. An oil leak is considered cleaned up when there are no visible traces of oil or petroleum on the ground.

7.4.6 Mobile or Portable Oil Storage Tanks

Mobile or portable oil storage tanks may be brought on-site during various operations. These portable tanks will be positioned or located so as to prevent spilled oil from reaching navigable waters. The largest mobile/portable container will be provided with containment plus sufficient freeboard for precipitation.

7.5..... FACILITY TRANSFER OPERATIONS

7.5.1 Buried Piping

Below ground piping is cathodically protected and coated to reduce corrosion.

The cathodic protection system is monitored monthly and the values for impressed voltages are recorded.

The cathodic protection system is checked annually by technically competent personnel. Copies of the reports are maintained in the Terminal Office for a minimum of five (5) years.

All underground product transfer piping is tested periodically. Copies of the reports are maintained in the Terminal Office.

When a section of buried pipe is exposed, it is carefully examined for deterioration and corrective action taken as necessary.

Buried piping installed or replaced after August 16, 2002 will be provided with a protective wrapping and coating and cathodic protection.

7.5.2..... Aboveground Piping

All aboveground valves and pipelines are regularly examined during operating personnel rounds. During these examinations, operating personnel assess the general condition and necessity for corrective actions of the pipelines.

7.5.3...... Out-of-Service Piping

Out-of-service pipelines will be capped or blind flanged and marked to its origin in the event that a Facility pipeline is removed from service or is placed in standby status for an extended time. Any out-of-service piping has had the product removed and the piping has been blind flanged or capped off.

7.5.4..... Design of Piping Supports to Reduce Abrasion

All piping supports are visually inspected to ensure that any abrasion is quickly detected. The aboveground piping is supported on a transverse horizontal pipe to minimize contact and abrasion. Where appropriate, special wearing shoes are welded on to the underside of pipes to further reduce abrasion potential in areas of high pipeline movement.

7.5.5..... Inspections

The Facility conducts a number of different types of inspections. A discussion of inspections and tests is presented in Annex 7, Section 7.7. Pipeline inspections are part of the Facility's Daily Inspection. Sample Inspection Checklist(s) are included at the end of this Annex.

7.5.6 Warning Signs for Vehicular Traffic

Warning signs for vehicular traffic are prominently placed at strategic locations throughout the Facility. These signs warn all vehicles entering the Facility about the dangers related to the aboveground piping or other oil transfer operations. The signs include instruction for use of the loading rack, spill notification directions, and entrance and exit.

7.6..... NORMAL DAILY THROUGHPUT

The normal daily throughput for the Brooklyn Terminal is 840,000 gallons. When demand and, subsequently, daily throughput increase, the potential release volumes increase. This increase typically occurs in the summer.

7.7...... DISCHARGE DETECTION BY PERSONNEL

A spill or release can be discovered by visual inspection. The initial response actions described in Core Plan, Section 1.1.7.1 will be implemented if any spills are detected.

7.7.1 Visual Inspection

The Terminal Operator examines the tanks and the equipment in the tank farm daily to ensure that there are no visible leaks in the tanks or piping system.

All visible tanks, lines, flanges, pumps, and other equipment are examined on a routine basis for indications of leaks, drips, sweating, etc. Repair of any such item is handled on a priority basis. Inspections include gauge hatch covers, manhole covers, gaskets, and foundations.

The exposed surfaces of the tanks, pipelines, and all equipment are inspected visually for the presence of discoloration or blistering that could indicate that the exterior paint is failing, or that the tank is leaking at a seam or through a pinhole. When any discoloration or blistering is observed, the tank or pipeline is repaired or replaced.

Other records of visual inspections that are made on a periodic basis, such as the internal floating roof seals, are kept in the Terminal Office on a dedicated form.

Motiva Enterprises LLC employs contractors to perform maintenance at the Facility. The maintenance is performed as required.

7.7.2..... Facility Self Inspection

The following is a partial list of the inspections that are made periodically at the Facility. Complete files on the results of these inspections are maintained by the Facility and are retained for a period of five (5) years. The following list is for example only and addresses only those items that are important to the operation and spill control issues at the Facility.

TYPICAL FACILITY INSPECTIONS

	Description of Inspection or Test-Repair
item .	if defective .
The first of the f	ADING RACK
Fire Extinguishers at all locations in the Facility	Check for full charge / recharge where needed .
All loading arms on the loading rack	Visually Check for leaks, counter balance operations,
All loading arms on the loading fact.	dry brake coupler seal, jaws, swing stops, adjust where
	required.
Truck Flush Equipment	Visually Check joints, swivels, couplers, and movement freedom
All Flow Control Valves and Meters	Inspect micro-switch screws and O-rings for leaks
All Turbine Flow Meters	Inspect and Check
All Temperature Probes	Re-calibrate
All Pressure Gauges	Inspect for operation / leaks
All Strainers	Inspect
Grounding Devices at lanes on loading rack	Inspect and Check
Overfill Device	Check Operation and status lights. Check to ensure
	bypass switch is locked in on position.
Vapor Flow Sensors	Physical check of successful operation during loading.
Rack Junction Boxes, Electrical	Check
Intercom	Check
Seals and gaskets	Visually inspect all piping, valves, fitting and
	component connections, seals, gaskets and valve
·	pacing for leakage or looseness
Meter Presets	Check function, ensure seals in place
TRUCK UI	NLOADING SYSTEM
Pump motor	Check for leaks
Air Eliminator	Check for leaks
Temperature Probe	Re-calibrate, Check for leaks
Water Draw Off Valves	Check for leaks, valves closed, splash blocks in-place
Pressure Gauges	Check for operation, leaks
Pump off hoses	Check for leaks
STORAG	E TANK FACILITIES
Tanks	Inspect roof devices, openings, for security and
	labeled. Observe domes and roofs for damage.
Water Draw Off Valves	Ensure valves closed and locked, check for leaks
Tank Level Gauges	Check for free movement, level transmitters
Tank Thermometers	Check for calibration
Tank Hi-Level Alarm	Manually Check audible alarm activation
Tank Level Transmitter	Compare readings and re-calibrate
Tank Motor Operated Valves	Completely check operation
Tank Hand Operated Valves	Check for leaks, operation
Tank Safety Control Valve	Check Operation
Product Pump Motor	Inspect for leaks, check operation
Tank Relief Valves	Check operation
Pressure Gauges	Check
Seals / Gaskets / Vitualic Couplings	Check for leaks
Tank Wall & Drains	Visual Inspection
Oil-Water Separator	Visual Inspection
Manifold Area	Thorough check of all valves, visual inspection,
·	lubricate as required
Pipeline Signal Control Panel	Check for correct operation & pipeline signals

TYPICAL FACILITY INSPECTIONS (Cont'd)

item	Description of Inspection of Test-Repair if defective SECURITY SYSTEMS
Perimeter Fence	Visual Inspection
Perimeter Gates	Check for locks and chains
Signs and Signboards	Check to ensure that warning signs, notices, instructions, and "Stop Here" lines are not obstructed and that they are secure and legible
Facility Area Lighting	Visually check lighting and ensure that lights are operating and are aimed for maximum illumination

The Facility maintains the records described below:

- 1. Records of Pressure Tests on Piping
- Records of Meter Calibrations
- 3. Records of Repairs made to Facility
- 4. Environmental Records, including
 - a. Inspections of all water outfalls and water analyses
 - b. Environmental records of any and all groundwater testing
 - c. Personnel Training Records
 - d. Waste disposal manifests
 - e. Tank Cleaning and inspection records
 - f. Other records required by permits
- 5. Product reconciliation and tank testing records
- 6. Reports on cathodic protection testing and inspections
- 7. Records of key and lock assignments
- 8. Records of safety meetings

7.7.3...... Other Procedures

7.7.3.1.... Pressure Testing of All Pipelines

Motiva Enterprises LLC periodically tests all pipelines in the Facility. The work is performed by an outside contractor and reports of each pressure test are kept in the Terminal Office files for a minimum of five (5) years.

7.7.3.2.... Tank Testing

The Facility conducts periodic tank testing to ensure tank integrity. The tests are indirect, but are indications of the tank soundness.

7.7.3.3 Cathodic Protection Testing

All steel tanks and lines are protected by an impressed current cathodic protection system. In order to protect the tanks and the pipelines, the system is inspected annually by technically qualified personnel.

7.7.3.4 Soundness Testing and Inspection

- ◆ The containers are visually inspected by operating personnel for signs of deterioration, leaks, or the accumulation of liquids inside the containment areas.
- Each storage container is inspected according to Company policy, as required by age, condition, and service. The monthly tank inspection records are maintained in a separate file at the Facility.
- ♦ Motiva Supporting Documentation Refer to Tank and Pressure Vessel Inspection and Maintenance Manual for details.
- ◆ Based on these conditions, the aboveground storage containers are professionally inspected and non-destructive thickness testing is performed.
- ♦ All aboveground storage tanks are included in the scope of this inspection and maintenance document. This includes small tanks, additive tanks, water tanks, horizontal tanks, UL-142 tanks, API 650 tanks, vapor tanks, pressure vessel, etc.
- Inspection/testing records are retained in a separate file at the Facility for a minimum period of five (5) years or longer based on industry standard of Corporate policy. (Industry standard is to retain records for the life of the tank).
- ♦ If a field-constructed aboveground container undergoes a repair, alteration, reconstruction, or change in service that might affect the risk of a discharge or failure due to brittle fracture, the container will be evaluated.
- Drums or totes brought on-site are built or tested to the standard(s) or inprocess inspection and testing procedures established by the drum manufacturer or the drum recycler, as applicable.
- While on-site, the drums or totes will be visually examined at least monthly.

7.7.3.5 Product Justification Record

Several types of records are kept in the Facility. These records are examined on a daily basis.

A daily record is kept of the amount of product in storage in the tanks, products shipped through the truck loading rack, and products received from pipelines and vessels.

A bulk stock loss record is maintained at the Facility and balanced monthly. The bulk stock loss record is used to compare the actual variations, both gross and net, of product to the amount that is reasonably anticipated. Any variances in the records are immediately investigated.

7.7.3.6 Locks and Seal Assignments

The Facility maintains a log of current key assignments, locks, and security seals.

7.7.3.7 Written Procedures for Inspection

Written procedures have been developed for this Facility and a record of the inspections, signed by the appropriate inspector, is kept in the Terminal Office files. Sample forms are also located at the end of Annex 7.

7.7.3.8 Record Retention Policy

Records of inspections must include each container, secondary containment, and item of response equipment at the Facility. The records of inspections must be cross-reference to retention location.

Inspection of response equipment is a requirement under 40 CFR 112.7(e). Facility self-inspection requires two-steps; (1) a checklist of things to inspect; and (2) a method of recording the actual inspection and its findings. Facility Response Plan records must be kept for five (5) years. The SPCC records are retained for three (3) years. Industry standards are that tank inspection records be retained for the life of the tank. Records are maintained in the Terminal Office.

7.8.......APPLICABLE MORE STRINGENT STATE DISCHARGE PREVENTION RULES AND REGULATIONS

♦ 6 New York Code of Rules and Regulations, §610-614.

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Name:				Avjet		·	Premium U Gasoline	nleaded
Relief:	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~			Quantity:		Barrels		Gallons
Assistant:				Height:		Split Tanks	}	
1. Checked High Level	Alarms Ye	s No		3. Cut 0	Off Loading R	ack Meters		
2. Notify Pipeline Comp	oany			4. Gaug	jed Tanks			
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				Yes•	No			
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Sample Only

DAILY CHECKLIST MOTIVA ENTERPRISES LLC		
FACILITY REGISTRATION NUMBER 2-1940		
25 PAIDGE AVE, BROOKLYN, NY 11222		
DATE SHIFT PERFORMED BY:		
TEN ONNES ST.		
YARD	TIME	STATUS
CHECK SEPERATOR FOR OIL ACCUMULATION / CREEK FOR SHEEN		
CHECK YARD FOR UNSAFE CONDITIONS	- ·	
CHECK PERIMETER FENCING AND LIGHTING		
MTY GARBAGE PAILS		
CHECK FOG ROOM / FOAM ROOM HEATERS AND PIPING		
DRAIN AIR COMPRESSOR YES / NO		
COMMENTS		1
COMMENTS		
·		
DOCK: TANK FARM 41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-9-10	TIME	STATUS
	THVIE	ISTATUS
CHECK ALL VALVES, PUMPS, MOTORS, FOR UNSAFE CONDITIONS / LEAKS	_	
GAUGE TANKS, CHECK TANKS, PIPING, COUPLINGS, FLANGES FOR LEAKS		
CHECK STAIRWAYS / CROSSOVERS FOR UNSAFE CONDITIONS		
	l l	
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DIKE DRAINAGE MONTHLY LOG REPORT

DATE	=		
UAL	_		

DAY OF MONTH	TIME START	TIME FINISH	ZONE NUMBER	VISIBLE SHEEN	OPERATOR ON DUTY
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ZONE #1 TANKS 47-48 ZONE #2 TANKS 41-42-43-44 ZONE #3 TANKS 45-46 REAR OF TANKS 40-50 ZONE #4 FRONT OF TANKS 49-50 ZONE #5 OLD UNDERGROUND TANK

MUST INSPECT ZONE BEFORE PUMPING. IF A SHEEN IS PRESENT DO NOT PUMP THAT ZONE.

MOTIVA BROOKLYN TE	RMINAL REVISED DIKE VOLUM	IE CALCULATIONS
By:	David O. Martin, Project Coordina	itor
Tank No (s):	41/42	Comments
Dike volume in gallons (from Walter Gorman Calculations)	188,183.93	
Overflow fill volume of largest tank:	88,978.00	Tank 42
Gallons per foot of smaller tank:	3,360.00	Tank 41
Avg. dike wall height:	6,912	
Displacement of other tank:	23,224.32	=gallons per foot of smaller tank X avg. dike wall height
Misc displacement (pipes, pumps, etc)	3,763.68	Assume 2%
Containment Percentage:	162%	'ОК'

MOTIVA BROOKLYN	TERMINAL REVISED DIKE VOLUM	IE CALCULATIONS
By:	David O. Martin, Project Coordinate	r
Tank No (s):	43/44	Comments
Dike volume in gallons (from Walter Gorman Calculations)	187,781.5765	
Overflow fill volume of largest tank:	88,912.00	Tank 44
Gallons per foot of smaller tank:	3,360.00	Tank 43
Avg. dike wall height:	6,870	
Displacement of other tank:	23,083.20	=gallons per foot of smaller tank X avg, dike wall height
Misc displacement (pipes, pumps, etc)	3,755.63	Assume 2%
Containment Percentage:	162%	'OK'

MOTIVA BROOKLYN	TERMINAL REVISED DIKE VOLUM	E CALCULATIONS
By:	David O. Martin, Project Coordinator	r
Tank No (s):	45/46/7/8/9/10	Comments
Avg. Dike Height:	6.95	
Dike Length:	109.00	
Dike width:	42.00	
Dike Area:	31817.10	
Basin 1 Area	141.67	
Basin 2 Area	125.00	
Basin 3 Area	116.67	
Total Area:	32200.43	
Dike volume in gallons :	240,859.2413	
Overflow fill volume of largest		
tank:	96,061.00	Tank 45
Gallons per foot of Tank 46	3,360.00	Tank 46
Gallons per foot of Tank 9	647.69	
Gallons per foot of Tank 10	647.69	
Avg. dike wall height:	6,950	
Displacement of Tank 46	23,352.00	=gallons per foot of smaller tank X avg. dike wall height
Displacement of Tanks 9/10	2.450.40	Active floor of tanks are 50" above dike floor. Area below floor is open for product to enter. Tanks 7 @ 8 are out-of-service and open and will allow
	2,450.43	product to enter.
Misc displacement (pipes, pumps, etc)	4,817.18	Assume 2%
Containment Percentage:	190%	'ОК'

MOTIVA BROOKLYN TE	RMINAL REVISED DIKE VOLUME C	ALCULATIONS
Ву:	David O. Martin, Project Coordinator	
Tank No (s):	47	Comments
Dike volume in gallons (from Walter Gorman Calculations)	519,885.8233	·
Overflow fill volume of largest tank:	442,064.00	Tank 47
Gallons per foot of smaller tank:		N/A
Avg. dike wall height:	9.260	
Displacement of other tank:	_	=gallons per foot of smaller tank X avg. dike wall height
Misc displacement (pipes, pumps, etc)	10,397.72	Assume 2%
Containment Percentage:	115%	'ОК'

MOTIVA BROOKLYN TI	RMINAL REVISED DIKE VOLUME (CALCULATIONS
By:	David O. Martin, Project Coordinator	r
Tank No (s):	48	Comments
Dike volume in gallons (from Walter Gorman Calculations)	490,186.6977	
Overflow fill volume of largest tank:	445,126.00	Tank 48
Gallons per foot of smaller tank:		N/A
Avg. dike wall height:	6.912	
Displacement of other tank:		=gallons per foot of smaller tank X avg. dike wall height
Misc displacement (pipes, pumps, etc)		Assume None
Containment Percentage:	110%	'ОК'

MOTIVA BROOKLYN TE	RMINAL REVISED DIKE VOLUME O	CALCULATIONS
By:	David O. Martin, Project Coordinato	r [.]
Tank No (s):	49/50	Comments
Tank 49 Dike volume in gallons (from Walter Gorman Calculations)	497,662.4868	
Tank 50 Dike volume in gallons (from Walter Gorman Calculations)	494,669.5702	. "
Tank 49 & 50 combined dike volume (connected by overflow)	992,332.0570	
Overflow fill volume of largest tank:	484,039.00	Tank 42
Gallons per foot of smaller tank:	12,978.00	Tank 41
Avg. dike wall height:	8.080	
Displacement of other tank:	104,862.24	=gallons per foot of smaller tank X avg. dike wall height
Displacement of Tank 53 (horiz. Waste) in gallons:	6,000.00	Max capacity
Misc displacement (pipes, pumps, etc)	9,893.39	Assume 2%
Containment Percentage:	164%	'OK'

By: Da	vid O. Martin, Project Coordinator	
Tank No (s):	51/54	Comments
Dike volume in gallons (from Walter Gorman Calculations)	15,625.22	
Overflow fill volume of largest tank:	6,000.00	Tank 51
Gallons per foot of smaller tank:		N/a
Avg. dike wall height:	5.400	
Displacement of other tank:	6,000.00	=Max cap. In gailons
Misc displacement (pipes, pumps, etc)	312.50	Assume 2%
Containment Percentage:	127%	'OK'

CONTAINMENT VOLUME CALCULATIONS

MOTIVA ENTERPRISES LLC

BROOKLYN TERMINAL BROOKLYN, NEW YORK

TRUCK LOADING RACK AND ADDITIVE TANKS 51 & 54 CONTAINMENT AREAS

CONTAINMENT VOLUME CALCULATIONS

PREPARED BY:



CONSULTING ENGINEERS

1 ROSSMOOR DRIVE MONROE TWP., NEW JERSEY 08831

RPMS PROJECT NO. 4844

AUGUST 2010

ADDITIVE TANKS CONTAINMENT

TANK 54 - 3,000 Gal. Vertical Tank

Dimensions:

 $D_{54} := 8.00$ ft

H := 13.33 ft

Tank Volume:

 $V_{54} := 3000$

TANK 51 - 5,000 Gal. Horizontal Tank

Dimensions:

 $D_{51} := 8.00$ ft

L := 14.50

Tank Volume:

 $V_{51} := 5000$

Gal.

Check Dike Containment For 110% of the Largest Tank Capacity

Containment Dike Dimensions

Dimensions:

 $B_c := 12.00$

 $L_c := 32.67$

 $H_c := 5.33$

Containment Capacity

Gross Area:

 $A_g := B_c \cdot L_c$

 $A_g = 392.04$

Area Displaced by Tank 54:

Net Area:

$$A_{net} := A_g - A_{54}$$

$$A_{net} = 385.76$$

Total Dike Containment:

$$V_c := A_{net} \cdot H_c \cdot 7.48$$

$$V_c = 15379.51$$

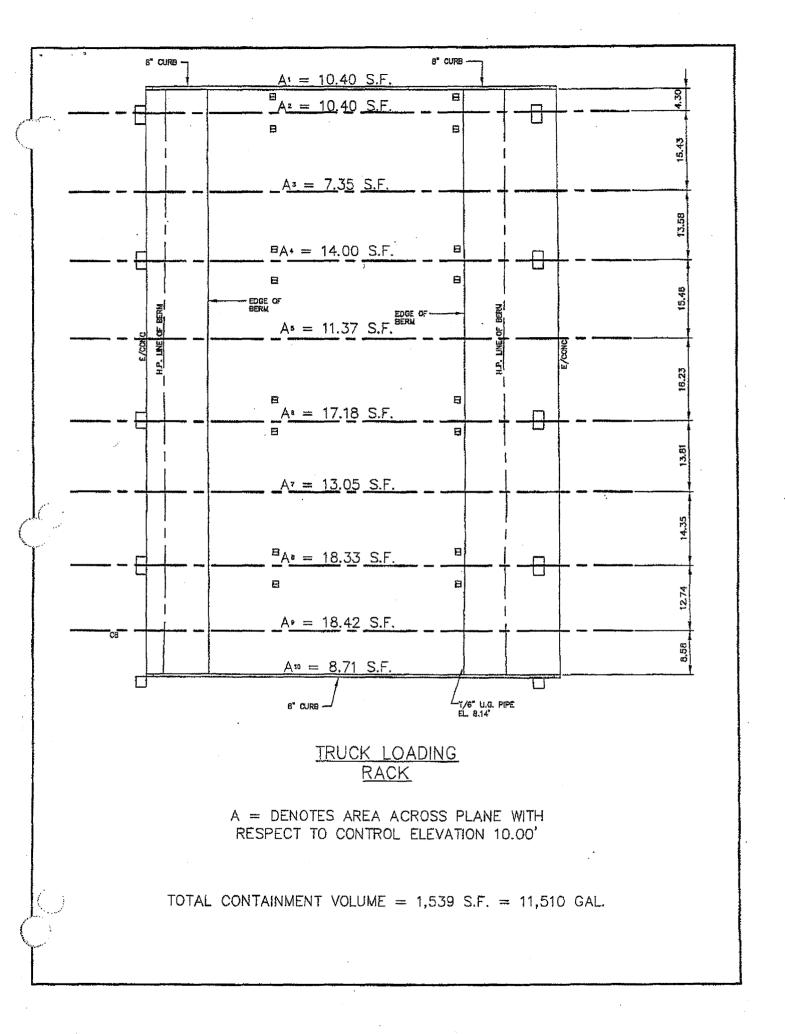
Containment Volume Required

$$V_R := 1.10 \cdot V_{51}$$
 $V_R = 5500.00$

$$V_R = 5500.00$$
 Gal.

$$V_C >> V_R => OK$$

Containment capacity exceeds by far the required capacity



Motiva Enterprises LLC
Brooklyn Terminal
Truck Rack Containment Calculation
RPMS Project No. 4844

Plane	Area (ft²)	Dist. Between Planes (ft)	Volume (ft ³)
A ₁	10.40		
A_2	10.40	4.30	44.72
A_3	7.35	15.43	136.94
		13.58	144.97
A ₄	14.00	15.46	196.11
A ₅	11.37	16.23	231.68
A_6	17,18		
A ₇ ·	13.05	13.81	208.74
A ₈	18.33	14.35	225.15
		12.74	234.10
A ₉	18.42	8.58	116.39
A_{10}	8.71		

Total = 1,539 ft³ 11,510 Gal.

MOTIVA ENTERPRISES LLC. BROOKLYN, NY

TANK NO. 54 INNAGE TABLE

GAUGE HEIGHT 14'-5 3/4" LOCATED 1'-0" IN PROM TANK BHELL TO HIM OPPOSITE HANGE

	IN.	GALLONS	IN.	GALLONE	IN.	GALLONS	سينا
\$	0	2!	F (2,280	112	4,544	₫8A
٥	<u> </u>	50	Π	2,212	11	4,675	╗.
T		83	12	2,349	12	4,607	<u> </u>
ò	الا	112	131	2.374	1 5	4,588	J
M	4	144	4	2,405	4	4,670]
		175	[6]	2.437		4,701	4

FILL

ALPHA TANK COMPANY INC.



Tanks For All Purposes - General Steel Plate Construction

The second section of the second section is the second section of the second section is the second section of

1850 STEINWAY ST. - LONG ISLAND CITY, N. Y. 11105 Phone: 718 274-8700

TANK #5/

NEW YORK CITY

5,000 GALLONS, 96" DIA. X 14'-6" LONG FUEL TANK

<u>GAUGE MEASUREMENT CHART</u>

INCHES	GALLONS	INCHES	GALLONS	INCHES	GALLONS
7	9	33	1,522	65	3,605
2	25	34	1,585	66	3,667
` 3	47	. 35	1,649	. 67	3,727
4	72	36	1,713	68	3,788
5 6	100	37	1,778	69	3,846
	130	38	1.842	70	3,907
7	163	39	1.,907	71	3,966
8	199	40	1,973	72	4,024
9	237	41	2,038	73	4,091
70	277	42	2,104	74	4,137
11 .	31B	43	2,170	7\$	4,192
12	381	44	2,236	76	4,247
73	405	45	2,302	77	4,300
14	451	46	2,368	78	4,352
15	499	47	2,435	79	4,404
16	548 ·	48	2.501	80 / , ,	4.454
17	5 98	49	2,567	81-6-9"	4.502 SAFET
18	649	50	2,633	82	4.550
19	701	51	2,700	83	4,596
20	755	52	2,761	84	4,641
21	810	53	2,832	85	4,684
22	864	54	2,898	86	4,725
23	921	55	2,963	87	4,765
24	978	56	3,029	88	4,802
25	1,035	57	3,094	89	4,838
26	1,094	58	3,160	90	4,871
27	1,153	59	3,224	91	4,902
28	1,213	60	3,288	92	4,930
29	1,274	61	3,352	93	4,955
30	·1,335	62	3,416	94	4.977
31	1,397	63	3,480	95	4,993
32	1,460	64	3,542	96	5,002
					•

MOLITAN CHIERPRISES.

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SAYBOLT INC.

MOTIVA ENTERPRISES LLC. BROOKLYN, NY

TANK NO. 54 INNAGE TABLE

GAUGE HEIGHT 14'-5 3/4" LOCATED 11-8" IN PROM TANK SHELL TO RAIN OPPOSITE HINGE

G	AUGE HE	[G	MT 14'-5	3/	LOCATED	-E" IN FROM	TAN	K SHELL TO	RHW OPPOS	ITE HING	Ε.			
FT.	GALLONS	F.	GALLONS	FT.	GALLONS		``							INCH GALLONS
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2 -	50	1	2.312	12	4,676		ノ゛	~> ~~		_	(i	1/8 75
7 12	81	3	2,343	2 3	4,607 4,638	-								1/4 28 3/8 32
y 4	112	4	2,874 2,408	4	4,570	1								1/2 36
5	175	5 :		I.	4,701	1								5/B 3B
2 6	206	5	2,468	6	4,733	4								3/4 43
7 N B	237 268	7	2,500 2,53;	7	4,764 4,796	4								7/6 46 - 7 50
<u>ء</u> ع	300	9	2,567	3	4,827	-								
10	33!	10	2,693	110	4,859	7								
11	382	7	2,825 2,856	13	4,850	4								1
	394 426	1	2,687	1	4,922 4,083	4								{
-1,-	458	2	2,719											
3	488	3	2,750	4					1					,
<u>4</u>	521 553	4	2,781 2.813	-{									1	ļ
8	685	0	2,844	j						All	1.1			
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	1,154	g	3,410	-										
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3	1,248	3	. 3,504	1									Ī	
4	1.279	5	3,535	4										
8	1,311	C	5,567 1,699	1									i	
	1,373	7	3,630]		•							l	
8	1,436	2	9,567 _3,693	4									1	
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11	1,498	111	2,756]									1	
4	1,530	10	3,780 3,819	-										
2	7,592	2	3,851	j										
2	1,623	3]	3,882	1	•									İ
4 6	1,656	5	3,914	4										ļ
6	1,717	6	3,977	1									İ	
7	1,749	7	4,008]										FRACTIONS
2	1,780	8	4,040	-									l	2/16 2
10	1,811 1,842	10	4,071 4,163	1										3/16 6
	1.874	111	4.134]									i	7/4 8
8	1,905 1,936	11	4,166	4	•									5/16 10
2	1,988	1 2	4,197 4,239	1.									,	7/8 12 7/16 14
3	1,599	3	4,260	1										1/2 16
5	2,030	4 6	4,292	ł										9/16 18
5	2,061 -	6	4,323 _4,355	1	•								ļ	11/76 22
7	2,124	7	4,386											3/4 24
В	2,159	8	4,418	Į			•				•		i	13/16 25
10	2,187 2,218	10	4,449 4,481	4										7/8 27 19/16 29
111		77	4,012	1										1 31
														• •

1. Tank shell height: 13'-4" 2. Diameter: 9'-0"

3. 0°-2° CROWNED UP BOTTOM SIGHTED. 4. LIQUID HEAD STRESS APPLIED AT 25.0 AM 7. TANK EHELL COMPUTED AT 80° F.

E. O'-O" REPRESENTS VOLUME BELOW STRIKE POINT.

7. TABLE COMPUTED AS FER API MPMS CHAPTER 2.2A B. FRACTIONS NOT APPLICABLE BELOW 0'-1"

8. SAFEFILL: 12'-0"

THIS TABLE SUPERSEDES ALL TABLES ISSUED PRIOR TO 05/02

CHART IS CERTIFIED FOR THIS TANK ONLY. COMPUTED BY: JF STRAPFED BY: JPY & SK SAYBOLT LP 08\36\05 09/25/02

(). Endreso

T00/T00 2

MOTIVA ENTERPRISES.

06/24/2010 10:00 FAX 718 383 7970

ANNEX 8.....REGULATORY COMPLIANCE / CROSS REFERENCE

The following pages contain information required by the regulations that act as documentation, authorization, or certification. Additionally, there are matrices with the specific regulatory requirement, and its corresponding section or page number.

8.1 FACILITY RESPONSE PLAN
8.1.1 Response Plan Cover Sheet
8.1.2 Facility Substantial Harm Classification
8.1.3 Determination of Worst-Case Discharge
8.1.4 EPA Expanded Cross-Reference
8.2 SPILL PREVENTION, CONTROL, AND COUNTERMEASURE PLAN
8.2.1 Legal Requirements for Preparation and Implementation Applicability
8.2.2 Professional Engineer's Certification and Approval
8.2.3 Terminal Management Certification
Log of Plan Review and Amendments
8.2.4 Qualified Individuals Authority to Initiate Oil Spill Response
8.2.5 Spill Prevention, Control, and Countermeasure Cross-Reference
8.3 HAZARDOUS WASTE CONTINGENCY PLAN
8.3.1 Distribution Letter to Local Agencies
8.3.2 Regulatory Cross-Reference
8.4 HAZARDOUS WASTE OPERATIONS EMERGENCY RESPONSE PLAN
8.4.1 Regulatory Cross-Reference
8.5 USCG Cross Reference

8.1.1.....Response Plan Cover Sheet

This cover sheet will provide EPA with basic information concerning the facility. It must accompany a submitted facility response plan. Explanations and detailed instructions can be found in Appendix F of 40 CFR 112.20. Please type or write legibly in black or blue ink. Public reporting burden for the collection of this information is estimated to vary from 1 hour to 270 hours per response in the first year, with an average of 5 hours per response. This estimate includes time for reviewing instructions searching existing data sources, gathering the data needed, and completing and reviewing the collection of information. Send comments regarding the burden estimate of this information, including suggestions for reducing this burden to: Chief, Information Policy Branch, PM-223, US Environmental Protection Agency, 401 M St., SW, Washington, DC 20460; and to the office of Information and Regulatory Affairs, Office of Management and Budget, Washington, DC 20503.

GENERAL INFORMATION					
Owner / Operator of Facility:	Motiva Enterprises LLC				
Facility Name:	Brooklyn Terminal				
Facility Address (street address or route):	25 Paidge Avenue				
City, State, US Zip code:	Brooklyn, NY 11222-1281				
Facility Phone Number:	718-383-4066				
Latitude (Degrees: North):	Longitude (Degrees: West)				
40° 44' 15" N	74° 56′ 45″ W				
Degrees, minutes, seconds	Degrees, minutes, seconds				
Dun & Bradstreet Number:	North American Industry Classification System				
#023838670	(NAICS) Code: 424710				
Largest above-ground Fuel Storage Tank Capacity	Maximum Storage Capacity				
(Gallons): 450,000	(Gallons): 2,358,600				
Number of Aboveground Fuel Storage Tanks: <u>18</u>	Worst-case Discharge Amount (Gallons) 450,000				
Facility Distance to Navigable Water. Mar	Facility Distance to Navigable Water. Mark the appropriate line.				
0-1/4 mile X 1/4 - 1/2 mile	1/2 - 1 mile >1 mile				

	Applicability of Substantia	l Harm Criteria					
Does the Facility transfer oil over-water to or from vessels and does the Facility have a total oil storage capacity greater than or equal to 42, 000 gallons?							
YES _	<u>X</u>	NO					
within any storage are	ea, does the Facility lack second of the largest aboveground oil	ater than or equal to 1 million gallons and, lary containment that is sufficiently large to storage tank plus sufficient freeboard to					
YES		NO X					
Does the Facility have a total oil storage capacity greater than or equal to 1 million gallons and is the Facility located at a distance (as calculated using the appropriate formula in Appendix C or a comparable formula) such that a discharge from the Facility could cause injury to fish and wildlife and sensitive environments?							
YES_	X	NO					
is the Facility located or a comparable form	Does the Facility have a total oil storage capacity greater than or equal to 1 million gallons and is the Facility located at a distance (as calculated using the appropriate formula in Appendix C or a comparable formula) such that a discharge from the Facility would shut down a public drinking water intake?						
YES_		NO X					
	ienced a reportable oil spill in a	eater than or equal to 1 million gallons and in amount greater than or equal to 10, 000					
YES_		NO X					
	CERTIFICATI	ON.					
information submitted	in this document, and that I	ally examined and am familiar with the based on my inquiry of those individuals he submitted information is true, accurate,					
Name:	James W. Lintz						
ranne.	Please type or print						
Title:	Metropolitan Complex Manage	Γ					
Date:	4-3-2008						

8.1.2 Facility Substantial Harm Classification

(This page reserved for substantial harm classification from EPA)

8.1.3 Determination of Worst-Case Discharge

INSTRUCTIONS

The calculation of a worst-case discharge is used for emergency planning purposes and is required in 112.20 (h)(5)(A) for facility owners and operators who must prepare a response plan. When planning for the amount of resources and equipment necessary to respond to the worstcase discharge planning volume, adverse weather conditions should be taken into consideration. Owners and operators should determine the facility's worst-case discharge from either Part A for onshore storage facilities or Part B for onshore production facilities. The worksheet integrates a facility's use of secondary containment and its proximity to navigable waters. For production facilities, the presence of exploratory wells, production wells, and storage tanks must be considered in the calculation. Part B takes these additional factors into consideration and provides steps for their inclusion in the total worst-case volume. As defined in this part, onshore oil production facilities may include all wells. flow lines, separation equipment, storage facilities, gathering lines, and auxiliary non-transportation related-equipment and facilities in a single geographical oil or gas field operated by a single operator. Although a potential worst-case volume is dependent on the risk parameter that results in the higher volume.

Marine transportation-related transfer facilities that contain fixed onshore structures used for bulk oil storage are jointly regulated by both EPA and the U.S. Coast Guard (USCG) and are termed "complexes". Because the USCG also requires response plans from transportation-related facilities to address a worst-case discharge of oil, a separate calculation for the worst-case discharge volume for USCG facilities is included in Annex 3.D.3 and done according to 33 CFR §154.1029. All complexes must compare both calculations for worst-case discharge derived by EPA and USCG and plan for whichever volume is greater.

PART A WORST-CASE DISCHARGE CALCULATION FOR ONSHORE STORAGE FACILITIES

Part A of this worksheet is to be completed by owners or operators of SPCC-regulated facilities (excluding oil production facilities) if the facility meets the criteria as presented in Appendix C to this part or if it is determined by the RA that the facility could cause substantial harm to the environment.

If you are an owner or operator of a production facility, please proceed to Part B.

A.1.	SINGLE TANK FACILITIES
	For facilities containing only one aboveground storage, the worst-case volume equals the capacity of the storage tank. - FINAL WORST-CASE VOLUME: N/A GAL - Do not proceed further.
A.2.	SECONDARY CONTAINMENT - MULTIPLE TANK FACILITIES Are all aboveground storage tank or groups of aboveground storage tanks at the facility without adequate secondary containment? N(Y/N)
A.2.1	If the answer is yes, the final worst-case volume equals the total aboveground oil storage capacity at the facility. (1) -FINAL WORST-CASE VOLUME:N(Y/N) (2) -Do not proceed any further.
A.2.2	If the answer is no, calculate the total aboveground capacity of tanks without adequate secondary containment. If all aboveground storage tanks or groups of aboveground storage tanks of the facility have adequate secondary containment, ENTER "0" (zero).
A.2.3	Calculate the capacity of the largest single aboveground oil storage tank within an adequate secondary containment area or the combined capacity of a group of aboveground oil storage tanks permanently manifolded together, whichever is greater, PLUS THE VOLUME FROM QUESTION A2.
	FINAL WORST-CASE VOLUME450,000 GAL

1 "Storage facilities" represent all facilities subject to this part, excluding oil production facilities.

Secondary containment is defined in 112.7(e)(2) of the current rule. Acceptable methods and structures for containment are given in 112.7 (c)(1) of the current rule.

All complexes that are jointly regulated by EPA and the USCG must also calculate the worst-case discharge planning volume for the transportation related portion of the facility and plan for which ever volume is greater.

PART B: WORST-CASE DISCHARGE PLANNING VOLUME CALCULATION FOR ONSHORE PRODUCTION FACILITIES

Part B of this worksheet is to be completed by owners or operators of SPCC-regulated oil production facilities if they meet the criteria presented in Appendix C to this part, or if it is determined by the RA that the facility could cause harm. A production facility consists of all wells (producing and exploratory) and related equipment in a single geographical oil or gas field operated by a single operator.

B.1 SINGLE-TANK FACILITIES

- B.1.1 For facilities containing only one aboveground oil storage tank, the worst-case discharge planning volume equals the capacity of the aboveground oil storage tank plus the production volume of the well with the highest output at the facility. If adequate secondary containment (sufficiently large to contain the capacity of the aboveground oil storage tank plus sufficient freeboard to allow for precipitation) exists for the storage tank, multiply the capacity of the tank by 0.8.
- B.1.2 For facilities with production wells produced by pumping, if the rate of the well with the highest output is known and the number of days the facility is unattended can be predicted, then the production volume is equal to the pumping rate of the well multiplied by the greatest number of days the facility is unattended.
- B.1.3 If the pumping rate of the well with the highest output is estimated or the unattended is estimated then the production volume is determined from the pumping rate of the well multiplied by 1.5 times the greatest number of days that the facility has been or is expected to be unattended.
- B.1.4 Attachment D-1 to this appendix provides methods for calculating the production volume for explanatory wells and production wells producing under pressure.
- (1) FINAL WORST-CASE VOLUME: N/A GAL
- (2) Do not proceed further.

B.2 SECONDARY CONTAINMENT - MULTIPLE TANK FACILITIES

Are all aboveground storage tanks or groups of aboveground storage tanks at the facility without adequate secondary containment? <u>No.</u> The Brooklyn Terminal does provide for secondary containment.

- B.2.1 If the answer is yes, the final worst-case volume equals the total aboveground oil storage capacity without adequate secondary containment plus the volume of the well with the highest output at the facility.
- (1) For facilities with production wells producing by pumping. If the rate of the well with the highest output is known and the number of days the facility is unattended can be predicted, then the production volume is equal to the pumping rate of the well multiplied by the greatest number of days the facility is unattended.

(2)	If the pumping rate of the well with the highest output is estimated or the maximum number of days the facility is unattended is estimated, the production volume is determined from the pumping rate of the well multiplied by 1.5 times the greatest number of days that the facility has been or is expected to be unattended.
(3)	Attachment D-1 to this appendix provides methods for calculating production volumes for exploratory wells and production wells producing under pressure.
	(A) - FINAL WORST-CASE VOLUME: N/A GAL (B) - Do not proceed further.
B.2.2	If the answer is no, calculate the total aboveground capacity of tanks without adequate secondary containment. If all aboveground storage tanks or groups of aboveground storage tanks at the facility have adequate secondary containment, ENTER "0" (zero).
	0
B.2.3	Calculate the capacity of the largest single aboveground oil storage tank with an adequate secondary containment area or the combined capacity of a group of aboveground oil storage tanks permanently manifolded together, whichever is the highest, PLUS THE VOLUME FROM QUESTION B.2.6(b). Attachment D-1 provides methods for calculating the production volumes for exploratory wells and production wells producing under pressure.
	(A) FINAL MODET CASE VOLUME: N/A CAL

Do not proceed further.

TABLE 1 TO APPENDIX E
RESPONSE RESOURCE OPERATING CRITERIA OIL RECOVERY DEVICES

Operating Environment	<u>Sigr</u>	nificant Wave ⊦	leight	Sea State
River		≤1 foot		1
Inland		≤3 feet		2
Great Lakes		≤4 feet		2-3
Ocean		≤6 feet		3-4
		BOOM USE		
Boom Property	River	Inland	Great Lakes	Ocean
Significant Wave Height	<1	<3	<4	≤ 6
Sea State	1	2	2-3	3-4
Boom height - in. (draft) plus freeboard)	10-18	18-42	18-42	≥42
Reserve Buoyancy to Weight Ratio	2:1	2:1	2:1	3:1 to 4:1
Total Tensile Strength - lbs.	4,500	15-20,000	15-20,000	≥20,000
Skirt Fabric Tensile Strength - Ibs.	200	300	300	500
Skirt Fabric Tear Strength - lbs.	100	100	100	125

TABLE 3 EMULSIFICATION FACTORS FOR OIL PRODUCT GROUPS

NON-PERSISTENT OIL	
GROUP 1	1.0
PERSISTENT OIL	
GROUP 2	2.5
GROUP 3	3.0
GROUP 4	1.8

TABLE 4
ON-WATER OIL RECOVERY RESOURCE MOBILIZATION FACTORS

Operating Area	Tier 1	Tier 2	Tier 3
River & Canals	.30	.40	.60
Inland / Nearshore / Great Lakes	.15	.25	40
Offshore	.10	.165	.21

Note: These mobilization factors are for total resources mobilized; not incremental resources.

TABLE 5 RESPONSE CAPABILITY CAPS BY GEOGRAPHIC AREA

February 18, 1993 All except rivers, canals, Great Lakes	<u>Tier 1</u> 10K	<u>Tier 2</u> 20K	<u>Tier 3</u> 40K
Great Lakes	5K	10K	20K
Rivers & Canals	1,500	3,000	6,000
February 18, 1998 All except rivers, canals, & Great Lakes	12.5K	_25K	50K
Great Lakes	6.35	12.3	25
Rivers & Canals	1,875	3,750	7,500

Note:

The caps show cumulative overall effective daily recovery rate, not incremental increases. This table updated to conform to EPA Final Rule 40 CFR 112-July 1, 1994.

TABLE 2
REMOVAL CAPACITY PLANNING TABLE

Spill Location		Nearshore / Inland	1		River	
Sustainability of on-water recovery		4 days			3 days	
Oil Group	% Natural Dissipation	% Recovered Floating Oil	% Oil Onshore	% Natural Dissipation	% Recovered Floating Oil	% Oil Onshore
1 Nonpersistent Oils	80	20	10	80	10	10
2 Light Crudes and Fuels	50	50	30	40	15	45
3 Medium Crudes and Fuels	30	50	50	20	15	65
4* Heavy Crudes, Fuel Residuals	10	50	70	5	20	75

For planning purposes, non-petroleum oil must be considered a Group 4 persistent oil.

Attachment 8.1.3.1

Worksheet for Determining Planning Volume for Response Resources for Worst-case Discharge Brooklyn Terminal

Pai	t 1	Bac	ground Information						
	Step	(A)	Calculate Worst-Cas	se Discharge ir	ո barre	els (Appendix	kD)	10,714	
	Step	(B)	Oil Group** (Table 3	and Section 1	.2 of ti	his Appendi	·	1	
	Step	(C)	Geographic Area (cl	noose one)	x	Nearshore / Great Lake		or F and Can	
<u>%</u>	•		Percentages of Oil (atural Dissipation 80	% Recovere	20	ating Oil	% Oil	Onshore 10	
			(D1)		(D2)			(D3)	 1
	Step	(E1)	On-Water Recovery	Step (D	02) x St 100	tep (A)		2,143	
	Step	(E2)	On-Shore Recovery	Step (D	03) x S 100	tep (A)		1,071	
•	Step	(F)	Emulsification Facto	or (Table 3)		•		1.00	
	Step	(G)	On-Water Oil Recov	ery Resource	Mobiliz	zation Facto	r (Table 4	!)	
			Tier 1	Tier	2			Tier 3	
			0.15	0.25	 5			0.40	
			(G1)	(G2	()			(G3)	

^{**} Facilities storing multiple groups of oil should prepare a separate worksheet for each group that comprises 10% or more of the volume of the facility. All oil volumes or all oils must be totaled for percentage determinations.

Attachment 8.1.3.1 (continued)

Worksheet for Determining Planning Volume for Response Resources for Worst Case Discharge (continued)

Part II On-Water Recovery Capacity (barrels / day)

Tier 1	Tier 2	Tier 3
321	536	857
Step (E1) x (Step (F) x Step (G1)	Step (E1) x (Step (F) x Step (G2)	Step (E1) x (Step(F) x Step (G3)
Part III Shoreline Cleanu	ıp Volume (barrels / day_	1,071
	city By Geographic Area (Table 5) to be contracted for, barrels / day)	Step (E2) x (Step(F)
Tier 1	Tier 2	Tier 3
12,500 (J1)	25,000 (J2)	50,000 (J3)
Part V <u>Amount needed (barrels / day)</u>	to be identified, but not contracted for	or in advance
Tier 1	Tier 2	Tier 3
0	0	0
Part II Tier I - Step (J1)	Part II Tier 2 - Step (J2)	Part II Tier 3 - Step (J3)

8.1.4..... EPA Expanded Cross-Reference (40 CFR 112.20)

BASED ON APPENDIX F FACILITY-SPECIFIC RESPONSE PLAN

	LOCATION
1: Emergency Response Action Plan (ERAP) consisting of #	
Qualified Individual Information	Core Plan
2. Emergency Notification Phone List	Core Plan
Spill Response Notification Form	Core Plan
4. Response Equipment List and Location	Core Plan
Response Equipment Testing & Development	OSRO dependent
Facility Equipment Testing & Deployment	Core Plan
7. Evacuation Plan	Core Plan, Diagram in Annex
8. Immediate Actions	Core Plan
9. Facility Actions	Core Plan
.2 Facility Information including:	
Facility Name and Location	Introduction 1.2
2. Latitude and longitude	Introduction 1.2
Location and drainage to a Wellhead Protection Area	Introduction 1.2
4. Owner / Operator Information	Introduction 1.2
5. Qualified Individual name with authority to implement the Plan	Introduction 1.2, Core Plan 1.1.2
6. Date of oil storage start-up	Introduction 1.2
7. Description of current facility operations	Introduction 1.2
Dates and types of substantial expansions	Introduction 1.2
.3 Emergency Response Information including:	
Notification Phone List & Notification Form	Core Plan 1.1.2, 1.1.3, Annex 2
2. Equipment List	Core Plan, 1.1.4
Equipment Testing / Deployment	OSRO dependent, Annex 1
4. Personnel	Core Plan, Annex 3a
5. Evacuation Plan	Core Plan 1.1.6, Annex 1, Figure 1.3
6. Qualified Individual Duties	Annex 3a, 3b
4 Hazard Evaluation including:	
1.4.1. Hazard Identification	Annex 7.1
List each aboveground tank and below ground tank.	Table 7.1
3.a. Identify each tank or SI that stores oil or hazardous materials.	Table 7.1
3.b&c. Substance, quantity stored.	Table 7.1
3.d. Tank type / surface, area, ;year.	Table 7.1

	V.	LOCATION
3.e. Maximum capacity.		Table 7.1
3.f. Record of tank failures / caus	ses.	Table 7.1
4. Schematic drawing using ab	ove information on tanks.	Annex 1, Figure 1.2
Description of Facility Opera	tions:	Annex 7
vehicles that risk the rele processes. Include all t railroad cars, vessels.	nd unloading of transportation ease of oil during transfer transfer processes for trucks,	Annex 7.1.8
◆ Identify operations that r	nay present a risk of release.	Annex 7.1
tank and transfer point a	volume associated with each at the facility.	Annex 7.2
volumes that a negative throughput may	and effect on potential release or positive change in that	Annex 7.6
2-Vulnerability Analysis: Rotentlal/e property environment of spill	ffects to human health,	
1. Water intakes		Annex 3.d
2. Schools		Annex 3.d
3. Medical facilities		Annex 3.d
4. Residential areas		Annex 3.d
5. Businesses		Annex 3.d
6. Wetlands and environmentally ser	nsitive areas	Annex 3.d
7. Fish and wildlife		Annex 3.d
8. Lakes and streams		Annex 3.d
9. Endangered flora and fauna		Annex 3.d
10. Recreational areas		Annex 3.d
11. Transportation routes (air, land, w	vater)	Annex 3.d
12. Utilities		Annex 3.d
 Economically sensitive areas inclienvironments, aquatic environments 	nts, and unique habitats.	Annex 3.d
3 Analysis of the Potential for a Spill	based on these factors	
◆ Tank age,		Table 7.1, Annex 3d
◆ Spill history,		Annex 4.2; 3d
 Horizontal range of spill, and 		Annex 3.d.4
 Vulnerability to natural disaster. 		Annex 3.d.1

1:4:4 Spill History description including:	LOCATION
1. Date of spill	Annex 4.2
2. Cause,	Annex 4
3. Material spilled,	Annex 4
4. Amount in gailons,	Annex 4
Amount that reached navigable waters,	Annex 4
Effectiveness and capacity of secondary containment,	Annex 4
7. Clean-up actions taken,	Annex 4
8. Steps taken to reduce recurrence,	Annex 4
Total storage capacity of tanks or impoundments from spill occurred.	which Annex 4
10. Enforcement actions,	Annex 4
11, Effectiveness of monitoring equipment, and	Annex 4
12, Description of how each spill was detected.	Annex 4
1,5 Response Scenarios information needed	
1.5.1 Small spill / Medium Spill	Core Plan, Annex 3.d.4
 Response equipment to be used for each scenario 	Core Plan, Annex 3.d.4
 Mitigation and response actions to be used in each 	scenarios. Core Plan, Annex 3.d.4
1.5.2 Worst-case scenario	Core Plan, Annex 3.d.4
1.6 Discharge Detection Systems including text on:	
1.6.1 Procedures and equipment used to detect spills, and spill detection by personnel	types of Annex 7.4-7.7
 1.6.2 Automated spill detection and frequency of inspection systems 	n of all Annex 7.4 - 7.5.5; 7.7.1; 7.7.2
1.7. Plan Implementation covering: #	
1.7.1 Response resources for small, medium, worst-case s	spills. Annex 3.d; 3.d.3.3 - 3.d.5
1.7.1.1 Emergency plans of spill response	Core Plan, Annex 3.c; 3.d; 3.d.3.3 - 3.d.5
1.7.1.2 Additional response training	Core Plan, Annex 3.c; 3.d; 3.d.3.3 - 3.d.5
1.7.1.3 Additional contracted help	Core Plan, Annex 3.c; 3.d; 3.d.3.3 - 3.d.5
1.7.1.4 Access to additional response equipment / exper	ts Core Plan, Annex 3.c
1.7.1.5 Ability to implement the Plan including response training and practice drills	Annex 3.c.2; Annex 5
1.7.2 Disposal plans-description of how and where the fac intends to recover, reuse, decontaminate, or dispose of materials after a spill	

1.7.3 Containment and drainage planning including:	LOCATION Annex 3.c.3; Annex 7.1.5, 7.2
1.7.3.1 Available volume of containment	Annex 7 - Table 7.1; Annex 7.2.1
1.7.3.2 Route of drainage from storage and transfer areas,	Annex 7.1.5; Drainage Diagram in Annex 1
1.7.3.3 Construction materials of drainage troughs	NA
1.7.3.4 Type and number of valves and separators used in the drainage system,	.Annex 7.1.5
1.7.3.5 Sump pump capacities	Annex 7.1.5
1.7.3.6 The containment capacity of weirs and booms, location of all,	NA
1.7.3.7 Other cleanup materials	OSRO dependent
1.8 Self-inspection, Drills/Exercises and Response Training	
1.8.1 Facility self-inspection, including checklists and records of inspection, meeting logs, etc.	Annex 7.7.1
1.8.1.1 Tank Inspection	Annex 7.7
1.8.1.2 Response Equipment Inspection	Annex 7.7
1.8.1.3 Secondary Containment Inspection	Annex 7.7
1.8.2 Facility Drills / Exercises	Annex 5
◆ Internal Exercise	Annex 5
◆ Ql notification drills	Annex 5
Spill Management Team Tabletop Exercise	Annex 5
Equipment Deployment Exercise	Annex 5
◆ Unannounced Drills	Annex 5
External Exercises	Annex 5
◆ Area Exercises	Annex 5
1.8.3 Response Training	Annex 5
1.8.3.1 Personnel Response Training Logs	Annex 5
1.8.8.2 Discharge Prevention Meeting Logs	Annex 5
1.9 Diagrams and Plots Plans of the facility:	
1.9.1 Detailed Plot Plan	Core Plan 1.1.8; Annex 1, Figure 1.2
1.9.2 Site Drainage Plan Diagram	Annex 1
1.9.3 Site Evacuation Diagram	Annex 1
1:10 Security including:	
1.10.1 Emergency cut-off locations	Annex 3.e.2.3 Annex 1, Figure 1.2, Annex 7.4.2
1.10.2 Enclosures (e.g., fencing)	Annex 3.e.2.1

	LOCATION
1.10.3 Guards, their duties, day and night,	Annex 3.e.2.6, Core Plan 1.1.6.3
1.10.4 Lighting,	Annex 3.e.2.5
1.10.5 Valve and pump locks	Annex 3.e.2.2
1.10.6 Pipeline	Annex 3.e.2
2:0 Response Plan Cover Sheet Information Including:	
◆ Facility Name	Annex 8.1.1
◆ Facility Address	Annex 8.1.1
◆ Facility Phone Number	Annex 8.1.1
◆ Latitude and Longitude	Annex 8.1.1
◆ Dun & Bradstreet Number	Annex 8.1.1
Standard Industrial Classification (SIC) Code	Annex 8.1.1
◆ Largest Oil Storage Tank Capacity	Annex 8.1.1
Maximum Oli Storage Capacity	Annex 8.1.1
Number of Oil Storage Tanks	Annex 8.1.1
◆ Worst-Case Discharge Amount	Annex 8.1.1
◆ Facility Distance to Navigable Water	Annex 8.1.1
Applicability of Substantial Harm Criteria	Annex 8.1.1
◆ Certification	Annex 8.1.1

8.2...... SPILL PREVENTION CONTROL AND COUNTERMEASURE (40 CFR 112.7)

8.2.1...... Legal Requirements for Preparation and Implementation Applicability

This is a Spill Prevention, Control, and Countermeasure Plan to be used by the Brooklyn Terminal in responding to and reporting a petroleum discharge or substantial threat of a petroleum discharge into the navigable waters or adjoining shorelines of the United States or the State of New York. The requirement for this Plan is found in the Code of Federal Regulations, Title 40, Part 112.

This Plan has been developed to fully address the regulatory requirements of the Federal Spill Prevention, Control and Countermeasure Regulation; U. S. EPA Final Rule for Oil Pollution Prevention; Non-Transportation Related On-Shore and Off-Shore Facilities (40 CFR 112 – as amended on November 13, 2009). When accompanied by the OPA-90 Plan, this document and the OPA-90 Plan fulfill the requirements of 40 CFR Part 112.

All facilities that have the potential to discharge harmful quantities of oil into or onto the navigable waters of the United States, which have more than 1,320 gallons of aboveground storage, or a total underground storage capacity which exceeds 42,000 gallons are required to have a Spill Prevention, Control, and Countermeasure Plan. This facility meets those criteria. Harmful quantities of oil are defined in 40 CFR 110 as a visible sheen on the surface of the water or shoreline, or which are in excess of permit quantities for those facilities that have a limit in their facility NPDES Permit.

As the owners or operators of this Facility, Motiva Enterprises LLC will maintain a complete copy of this Spill Prevention, Control, and Countermeasure portion of this Plan at the Facility and will make the Plan available to the Regional Administrator or authorized representative of the Environmental Protection Agency for on-site review during normal working hours. A complete copy is maintained at the Facility because the Facility is manned at least four (4) hours per day. A complete copy is maintained at the Facility because the Facility is manned at least four hours a day.

In the event that this facility discharges more than 1,000 gallons of oil into or upon the navigable waters of the United States or adjoining shorelines in a single event, or discharges more than 42 gallons of oil upon the navigable waters of the United States or adjoining shorelines in two reportable spill events within any twelve month period, the owner or operator of this facility will submit the following information to the Regional Administrator of the Environmental Protection Agency within 60 days.

- 1. Name of facility
- 2. Name of owner / operator
- 3. Location of facility
- 4. Maximum storage or handling capacity of the Facility and normal daily throughput
- 5. Corrective action and countermeasures including description of equipment repairs and replacements
- 6. Description and maps of facility
- 7. Cause of such discharge including failure analysis of the system
- 8. Additional prevention measures taken or contemplated
- 9. Other information as required by the RA pertinent to the Plan or discharge

8.2.2 Professional Engineer's Certification and Approval

PROFESSIONAL ENGINEER CERTIFICATION

By means of this Professional Engineer Certification, I hereby attest to the following:

- I am familiar with the requirements of 40 CFR Part 112 and have verified that this Plan has been prepared in accordance with the requirements of this Part.
- I or my agent have visited and examined the Facility(s).
- I have verified that this Plan has been prepared in accordance with good engineering practice, including consideration of applicable industry standards.
- I have verified that the required inspection and testing procedures have been established as described in Annex 7.
- I have verified that the Plan is adequate for the Facility.
- My certification of this Plan in no way relieves the owner/operator of the Facility(s) of their duty to prepare and fully implement the Plan in accordance with the requirements of 40 CFR Part 112. I in no way assume any liability of whatsoever kind of nature by my certification.
- The owner/operator, by "Management Approval" located on the following page, acknowledges this certification and the compliance measures described herein.
- This certification is limited to the sections referenced in the Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.7) cross reference table located in Section 8.2.5.

LICENSON DE NEW PORTE RESSIONAL MENT P. DORA

Date: SEP 23 2010

(Seal)

Registered Professional Engineer

Robert P. Perla, P.E.

RPMS Consulting Engineers
State of New York
Registration No: 054709

8.2.3 Terminal Management Certifications

	WIANAC	SEMENT APPROVAL
	erator responsible for Facility: y Name and Location:	Motiva Enterprises LLC Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222-1281
eleme	ents identified within this Plan ha	rpproves this Plan and acknowledges that the ve been implemented, including a commitment to ditiously control and cleanup oil spills.
	page may be used for the initial M gement and/or change of design	lanagement Approval or for subsequent change of ated person accountable.
• This S	SPCC Plan will be implemented a	s herein described.
Signa	ture: Jours W. Lit	Designated person accountable for oil spill prevention at the Facility:
Name	: James W. Lintz	Name: James W. Lintz
Date:	4-3-2008	Title: Metropolitan Complex Mgr
Title:	Metropolitan Complex Mgr.	
This SignalNameDate:Title:	: JAMES LINTZ	Designated person accountable for oil spill prevention at the Facility: Name: Takes Lint Title: Metropolitan Complex Mar.
	SPCC Plan will be implemented a	·
Oigile	itui 6	spill prevention at the Facility:
Name): 	Name:
Date:		Title:
Title:		

8.2.3 Terminal Management Certifications

	MANAGEMENT APPROVAL				
Owner/Operator responsible for Far Facility Name and Location:	cility: Motiva Enterprises LLC Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222-1281				
elements identified within this	 By signature below, the Manager approves this Plan and acknowledges that the elements identified within this Plan have been implemented, including a commitment to expend money and resources to expeditiously control and cleanup oil spills. 				
	initial Management Approval or for subsequent change of designated person accountable.				
This SPCC Plan will be implem	nented as herein described.				
Signature: Journ W. (Designated person accountable for oil spill prevention at the Facility:				
Name: <u>James W. Lintz</u>	Name: James W. Lintz				
Date: <u>4-3-2008</u>	Title: <u>Metropolitan Complex Mgr</u>				
Title: <u>Metropolitan Comple</u>	ex Mgr.				
This SPCC Plan will be implementation	nented as herein described.				
Signature:	Designated person accountable for oil spill prevention at the Facility:				
Name:	Name:				
Date:	espoist 1				
Title:	· · · · · · · · · · · · · · · · · · ·				
This SPCC Plan will be implent	nented as herein described.				
Signature:	Designated person accountable for oil spill prevention at the Facility:				
Name:	Name:				
Date:	Tido				
Title:					

8.2.3......Terminal Management Certification

	IAIWIAW	GEMENT APPROVAL
Ow	ner/Operator responsible for Facility:	Motiva Enterprises LLC
•	Facility Name and Location:	Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222-1281
•		oproves this Plan and acknowledges that the elements implemented, including a commitment to expend money and cleanup oil spills.
•	This page may be used for the initial management and/or change of designations	al Management Approval or for subsequent change of ated person accountable.
•	This SPCC Plan will be implemented a Signature:	1
	Name: M.A. D'Antonio Date: /c//o/03 Title: Complex Manager	Name: <u>M.A. D'Antonio</u> Title: <u>Complex Manager</u>
•	This SPCC Alan will be implemented a Signature: Name: MARC A. HETEURO Date: 2/3/2008 Title: Cery 160 Mary CL	Designated person accountable for oil spill prevention at the Facility:
•	This SPCC Plan will be implemented a Signature:	
	Name: Date: Title:	Title:

Annex 8, Page 22a

LOG OF PLAN REVIEW AND AMENDMENTS

NON TECHNICAL AMENDMENTS

Non-technical amendments are not certified by a Professional Engineer.

Examples of changes include, but are not limited to, phone numbers, name changes, or any non-technical text change(s).

TECHNICAL AMENDMENTS

- Technical amendments are certified by a Professional Engineer.
- Examples of changes include, but are not limited to, commissioning or decommissioning containers; replacement, reconstruction, or movement of containers; reconstruction, replacements, or installation of piping systems; construction or demolition that might alter secondary containment structures; changes or product or service; or revision of standard operation or maintenance procedures at a Facility.
- An amendment made under this section will be prepared within six (6) months of the change and implemented as soon as possible but not later than six (6) months following preparation of the amendment.

MANAGEMENT REVIEW

Management will review this SPCC Plan at least each five (5) years and document the review on the form below.

Review/ Amend Date,	Signature	Amend Plan (will/will not)	Description of Review Amendment	Affected Page(s)	P.E. Certification (Y/N)
3/1/10.	the to	> 10			N
10-20-10	- Juli-ta	s No	Amended 9/2010	MULTIPLE	4
			,		
	·				
	·				

Annex 8, Page 22a

LOG OF PLAN REVIEW AND AMENDMENTS

NON TECHNICAL AMENDMENTS

Non-technical amendments are not certified by a Professional Engineer.

Examples of changes include, but are not limited to, phone numbers, name changes, or any non-technical text change(s).

TECHNICAL AMENDMENTS

- Technical amendments are certified by a Professional Engineer.
- Examples of changes include, but are not limited to, commissioning or decommissioning containers; replacement, reconstruction, or movement of containers; reconstruction, replacements, or installation of piping systems; construction or demolition that might alter secondary containment structures; changes or product or service; or revision of standard operation or maintenance procedures at a Facility.
- An amendment made under this section will be prepared within six (6) months of the change and implemented as soon as possible but not later than six (6) months following preparation of the amendment.

MANAGEMENT REVIEW

Management will review this SPCC Plan at least each five (5) years and document the review on the form below.

Review/ Amend Date;	Signature	Amend Plan (will/will not)	Description of Review Amendment	Affected Page(s)	P.E. Certification (Y/N)
3/1/10.	Just to	> No			N
		•			
·					
			•		

8.2.4...... Qualified Individuals Authority to Initiate Oil Spill Response - 10/98

Pursuant to the Oil Pollution Act of 1990 (OPA), State Oil Spill Response laws and Federal and State regulations under Federal and State Oil Spill Response statutes, authority to sign Notices of Federal Interest for an Oil Pollution Incident (or their equivalent), Notices of State Interest for an Oil Pollution Incident (or their equivalent), designation of responsible party for an oil spill, authority to approve witness statements, and authority to initiate oil spill response activities is hereby assigned and delegated to persons occupying and acting in the capacity of the positions as specified below in accordance with such facilities' Oil Spill Response Contingency Plans and/or the Company's Regional Response Teams.

- 1. At marketing terminals, Terminal Manager, Complex Manager, Superintendents, or in their absence, Assistance Terminal Managers, Terminal Supervisors, Terminal Operators, Regional Managers, Regional Response Team On-Scene Coordinator.
- 2. For all other locations, Manager, LSDR/HSE and Emergency Management, or any officer of the Company. Any employee of the Company serving on the Regional Response Teams or performing work required by the Regional Response Plans has necessary authority to perform their work in accordance with the objectives established with the Alliance of Shell and Saudi Refining, Inc. Limitations on approval amounts are governed by Motiva's Delegation of Authority.

8.2.5 Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference

40 CFR § 112	BRIEF DESCRIPTION	SECTION
112.3	Requirements for preparation and implementation of Spill Prevention Control and Countermeasure Plan	
(a,b,c)	Owners or operators and could reasonably be expected to have a discharge oil as describedmust prepare and implement a Plan	Sec. III, Annex 8.2.1
(d)	A licensed Professional Engineer must review and and certify a Plan for it to be effective	Sec. III, Annex 8.2.2 (PE Certification)
(e)	Maintain a complete copy of the Plan at the facility if the facility is normally attended at least 4 hours per day, or at the nearest field office	Sec. III Annex 8.2.1
112.5	Amendment of Spill Prevention Control and Countermeasures Plans by owners or operators	***
(a)	Amend the SPCCwhen there is a change in facility design, construction, operation or maintenance which materially affects the facility's potential for the discharge of oil	Sec. III, Annex 8.2.3.a
(b)	complete a review and evaluation of the SPCC at least once every five years amend the SPCC within six months of the reviewimplement within six months of preparation of any amendment.	Sec. Ili, Annex 8.2.3.a
(c)	Have a Professional Engineer certify any technical amendment	Sec. III, Annex 8.2.2
112.7	Guidelines for the preparation and implementation of a Spill Prevention Control and Countermeasures Plan	Pau
4949	must prepare a Planhave full approval of managementin writing,	Sec. 1 Introduction 1.1 Sec. III, Annex 8.2.3
	If the plan calls for additional facilities or procedures, methods, or equipment not yet fully operational, these items should be discussed in separate paragraphs, and the detalls of installation and operational start-up should be explained separately.	
	follow the sequence specified (or cross-reference)	Sec. III, Annex 8.2.5
(a)(2)	Comply with all applicable requirements in this part [or] state reasons for non-conformance and describe alternate methods	Sec. III, Annex 8.2.1
(a)3)	Describe physical layout and include diagram	Sec. I, Intro. 1.2.7; Sec. II, Core Plan, Figure 1.2; Sec. III Annex 1 Fig 1.2
(a)(3)(i)	[address in your Plan] the type of cil in each container and its capacity	Sec. III. Annex 7 Table 7-1
(a)(3)(ii)	discharge prevention measures including routine handling of products	Sec. III. Annex 7.1.8
(a)(3)(iii)	Drainage or discharge controls and procedures for control of a discharge	Sec. III. Annex 7.1.5, 7.1.6, 7.2.7
(a)(3)(iv)	Countermeasures for discharge discovery, response, and cleanup (both facility's and contractor)	Sec. II, Core Plan 1.1.7
(a)(3)(v)	Methods of disposal of recovered materials	Sec. III, Annex 3.d.6
(a)(3)(vi)	Contact list and phone numbers	Sec. II, Core Plan 1.1.2
(a)(4)	Relate information [on a discharge]	Sec. II, Core Plan 1.1.3
(a)(5)	Organize portions of the Plan that will make them readily usable	Core Plan, Section Dividers
(b)	Where experience indicates a reasonable potential for equipment failureinclude a prediction	Sec. III, Annex 7 Table 7-1

8.2.5...... Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference (Cont'd)

40 CFR § 112	BRIEF DESCRIPTION	SECTION
(c)(1)	Onshore facilities.	Sec. III, Annex 7.2.
(c)(1)(i)	Dikes, berms or retaining walls sufficiently impervious to contain spilled oil	Sec. III, Annex 7.2.2
(c)(1)(ii)	Curbing	Sec. III, Annex 7.2.3
(c)(1)(iii)	Culverting, gutters or other drainage systems	Sec. III, Annex 7.2.4
(c)(1)(iv)	Weirs, booms or other barriers	N/A
(c)(1)(v)	Splil diversion ponds	Sec. III, Annex 7.2.5
(c)(1)(vi)	Retention ponds	Sec. III, Annex 7.2.5
(c)(1)(vii)	Sorbent materials	Sec. III, Annex 7,2.6
(c)(2)	Offshore Facilities.	
(c)(2)(l)	Curbing, drip pans	N/A
(c)(2)(ii)	Sumps and collection systems	N/A
(d)	If you determine that the installation of structures or equipment listed in paragraphs (c) and (h)(1) of this sectionis not practicableclearly explain in your Planand provide	
(d)(1)	A strong oil spill contingency plan following40 CFR 109.	Entire Plan
(d)(2)	A written commitment of manpower, equipment and materials required to expeditiously control and remove any harmful quantity of oil discharged.	Sec. III, Annex 8.2.3
(e)	Inspections and records	
	in accordance with written procedures that you or the certifying engineer developwith the SPCC Plan for a period of three years.	Sec. III, Annex 7.7.2, 7.7.3.8
(f)	Personnel, training and spill prevention procedures	
(f)(1)	train your oil-handling personnel in the operation and maintenance of equipment to prevent the discharges	Sec. III, Annex 5.2.2
(f) (2)	Designate a personaccountable for oil spill prevention	Sec. III, Annex 8.2.3
(f)(3)	Schedule and conduct spill prevention briefingshighlight and describe known spill dischargesor failures, malfunctioning components, and recently developed precautionary measures.	Sec. III, Annex 5.2.3
(g)	Security (excluding oil production facilities)	Sec. III, Annex 3.3.2
(h)	Facility tank car and tank truck loading/unloading rack	BEFFF
(h)(1)	Where loading/unloading area drainage does not flow into a catchment basin or treatment facility designed to handle discharges, use a quick drainage system design any containment system to hold at least maximum capacity of any single compartment of a tank car or tank truck loaded or unloaded at the facility.	Sec. III, Annex 7.1.8.4
(h)(2)	Provide an interlocked warning light or physical barrier system, warning signs, wheel chocks, or vehicle break to prevent vehicular departure before complete disconnect of flexible or fixed oil transfer lines.	Sec. III, Annex 7.1.8.4.b
(h)(3)	Prior to filling and departure of any tank car of tank truck, closely inspect for discharges the lowermost drain and all outlets of such vehicles should be closely examined for leakage, and if necessary, that they are tightened, adjusted, or replaced to prevent liquid leakage while in transit.	Sec. III, Annex 7.1.8.4.c
(i)	If a field-constructed aboveground container undergoes a repair, alteration, reconstruction, or change in service that might affect the risk of a discharge or failure due to brittle fractureevaluate the container for risk	Sec. III, Annex 7.7.3.4
(j)	In additioninclude a complete discussion of conformance with applicable requirementsor any more stringent, with State rules, regulations and guidelines.	Sec. III, Annex 7.8

8.2.5...... Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference (Cont'd)

40 CFR § 112	BRIEF DESCRIPTION	SECTION
(k)	Qualified Oil-filled Operation Equipment	
(k)(1)	Qualification Criteria – Reportable Discharge History: The owner or operatorthat has had no discharges as described in § 112.1(b) from any oil-filled operational equipment; and	N/A
(k)(2)	Alternative Requirements to General Secondary Containment. If secondary containment is not provided for qualified oil-filled operational equipment pursuant to paragraph (c) of this section, the owner or operator of a facility with qualified oil-filled operational equipment must:	N/A
(k)(2)(i)	Establish and document the facility procedures for inspections or a monitoring program to detect equipment failure and/or a discharge; and	N/A
(k)(2)(ii)	Unless you have submitted a response plan under § 112.20, provide in your Plan the following:	N/A
(k)(2)(li)(A)	An oil spill contingency plan following the provisions of part 109 of this chapter,	N/A
(k)(2)(ii)(B)	A written commitment of manpower, equipment, and materials required to expeditiously control and remove any quantity of oil discharged that may be harmful.	N/A
112.8	Spill Prevention, Control, and Countermeasure Plan requirements for onshore facilities (excluding production facilities)	
(a)	Meet the general requirements for the Plan listed under § 112.7, and	
(b)(1)	Restrain drainage from diked storage areas by valves or other positive means to prevent a spillInto the drainage system or inplant effluent treatment system, except where plan systems are designed to handle such leakage. You may empty diked areas by pumps or ejectors; however you must be manually activate these pumpsand inspect the condition of the accumulation before starting	Sec. III, Annex 7.2.7, 7.2.8
(b)(2)	Use valves of manual, open-and-closed design If facility drainage drains directly into water courseyou must inspect and drain uncontaminated retained stormwater, as provided inparagraphs (c)(3)(ii)(iii), and (iv).	Sec. III, Annex 7.2.7, 7.2.8
(b)(3)	Design facility drainage systems from undiked areas to flow into ponds, lagoons or catchment basins, designed to retain oil or return it to the facility. You must not locate catchment basins in areas subject to periodic flooding.	Sec. III, Annex 7.1.6
(b)(4)	Ifnot engineered as in paragraphs (b)(3), equip the final discharge of all ditches with a diversion system that wouldretain the oil in the facility.	Sec. III, Annex 7.1.6
(b)(5)	Where drainage waters are treated in more than one treatment unit provide two "lift" pumps and permanently install at least one of the pumps. Whatever techniques are used, facility drainage systems engineer to prevent a discharge as described in § 112.1(b) in case there is an equipment fallure or human error	Sec. III, Annex 7.2.7
(c)	Bulk storage containers (onshore)	
(c)(1)	Not use a container for the storage of oil unless its material and construction are compatible with the material stored and conditions of storage	Sec. III, Annex 7.3.1
(c)(2)	Construct all bulk storage container installations so that you provide a secondary means of containment for the entire contents of the largest single container plus sufficient freeboard to allow for precipitation. You must ensure that diked areas are sufficiently impervious to contain discharged oil.	Sec. III, Annex 7.2.1, 7.2.2
(c)(3)	Not allow drainage of uncontaminated rainwater from the diked area into a storm drain or discharge of an effluent discharge into an open water course, lake, or pond, bypassing the in-plant treatment system unless you:	Annex 7.2.7
(c)(3)(i)	Normally keep the bypass valve sealed closed.	Sec. III, Annex 7.2.7
(c)(3)(ii)	Inspect the retained rainwater to ensure that its presence will not cause a discharge as described in § 112.1(b).	Sec. III, Annex 7.2.7
(c)(3)(lii)	Open the bypass valve and reseal it following drainageunder responsible supervision.	Sec. III, Annex 7.2.7

8.2.5...... Spill Prevention, Control, and Countermeasure Plan (40 CFR 112.3, 5, 7, 8) Cross-Reference (Cont'd)

40 CFR § 112	BRIEF DESCRIPTION	SECTION
(c)(3)(iv)	Keep adequate records of such events.	Sec. III, Annex 7.2.7
(c)(4)	Protect any completely buried metallic storage tank installed on or after January 10, 1974 from corrosion by coatings or cathodic protection	Sec. III, Annex 7.3.4
(c)(5)	Not use partially buried metallic tanks for the storage of oil should be avoided, unless the buried section of the shell is adequately coated	Sec. III, Annex 7.3.5
(c)(6)	Test each aboveground container for integrity testing on a regular Keep comparison records In additionfrequently inspect the outside of the container for signs of deterioration, discharges, or accumulation of oil inside diked areas. Records of inspections and tests kept under usual and customary business practices will suffice for the purposes of this paragraph.	Sec. III, Annex 7.7
(c)(7)	Control leakage through defective internal heating coils by monitoring the steam return and exhaust lines	Sec. III, Annex 7.3.7
(c)(8)	Engineer or update each container installation in accordance with good engineering practice to avoid discharges (and) provide at least one of the following devices:	
(c)(8)(i)	High liquid level alarms with an audible or visual signal at a constantly attended operation or surveillance station. In smaller facilities, an audible air vent may suffice.	Sec. III, Annex 7.4.1
(c)(8)(ii)	High liquid level pump cutoff devices set to stop flow at a predetermined container content level.	Sec. III, Annex 7.4.2
(c)(8)(iii)	Direct audible or code signal communication between the container gauger and the pumping station.	Sec. III, Armex 7.4.3
(c)(8)(iv)	A fast response system for determining the liquid level of each bulk storage container such as digital computers, telepulse, or direct vision gauges.	Sec. III, Annex 7.4.4
(c)(8)(v)	You must regularly test liquid level sensing devices to ensure proper operation.	Sec. III, Annex 7.4.1
(c)(9)	Observe effluent treatment facilities frequently enough to detect possible system upsets that could cause a discharge	Sec. III, Annex 7.4.1
(c)(10)	Promptly correct visible discharges which result in a loss of oil from container includingseam, gaskets, piping, pumps, valves	Sec. III, Annex 7.4.5
(c)(11)	Position or locate mobile or portable oil storage container to prevent a discharge as described in § 112.1(b)furnish a secondary means of containmentfor the largest single compartment or container with sufficient freeboard.	Sec. III, Annex 7.4.6
(d)	Facility transfer operations, pumping, and facility process	
(d)(1)	Provide buried piping installed or replaced on or after August 16, 2002, with a protective wrapping and coatingcathodically protect. If a section of buried line is exposedcarefully inspect it for deterioration. If you find corrosion damage, you must undertake additional examination and corrective action as indicated	Sec. III, Annex 7.5.1
(d)(2)	Cap or blank-flange the terminal connectionand mark it as to origin when piping is not in service, or in standby service for an extended time.	Sec. III, Annex 7.5.3
(d)(3)	Properly design pipe supports to minimize abrasion and corrosion and allow for expansion and contraction.	Sec. III, Annex 7.5.4
(d)(4)	Regularly inspect all aboveground valves, piping, and appurtenancesalso conduct integrity and leak testing on buried piping at the time of installation, modification, construction, relocation, or replacement.	Sec. III, Annex 7.7.1
(d)(5)	Warn all vehicles entering the facility to be sure that no vehicle will endanger above ground piping or other oil transfer operations.	Sec. III, Annex 7.5.6



U.S. ENVIRONMENTAL PROTECTION AGENCY SPCC FIELD INSPECTION AND PLAN REVIEW CHECKLIST

FOR USE AT ONSHORE FACILITIES (EXCLUDING PRODUCTION)

FACILITY INFORMATION	;	:		
FACILITY NAME: MOTIVA Ente	rorises 1	LLC	Brown	lyn Terminal
LAT: LONG:			Section/Townsh	ip/Range:
ADDRESS: 25 Paidge Ave.			•	
CITY: Brooklyn				COUNTY: KINGS
TELEPHONE: 718 383 4440 FACIL	LITY REPRESENTAT	TIVE N	AME: Frank	Signoriello
OWNER NAME: Shell Oil			· ·	J
OWNER ADDRESS: 25 Pardge AV	-			
CITY: BOUNEIUM	•		STATE: NY	ZIP: 11222
OWNER CONTACT PERSON: Jim Ly	ntz			
TELEPHONE: 203 520 0403	FAX: 718 383	379	70 EMAIL:	
FACILITY OPERATOR NAME (IF DIFFERENT FROM C	WNER – IF NOT, PF	RINT "S	SAME"):	ame
OPERATOR ADDRESS:				
CITY:			STATE:	ZIP:
TELEPHONE: 860 749 2839 OPER	RATOR CONTACT P	ERSO	N: Jennifer	Bothevell
FACILITY TYPE: Oil Storage + di	stributio.	;····	•	NAICS CODE:
HOURS PER DAY FACILITY ATTENDED: 24 h	1365 day	TOTAL	FACILITY CAPAC	ITY: 52,000 BBLS
TYPE(S) OF OIL STORED: Reg gas, F	scemium g	~2	+ e Dro-u	(0)
LOCATED IN INDIAN COUNTRY? - YES ANO RE	SERVATION NAME:			_
INSPECTION INFORMATION			·	
INSPECTION DATE: 9/29/10 TIME: 12	2150	INSF	PECTION NUMBER	2:
LEAD INSPECTOR: Margaret Ch	ona	<u> </u>		
OTHER INSPECTOR(S):				
INSPECTOR ACKNOWLEDGMENT				
I performed an SPCC inspection at the facility specified a	above.	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~		
INSPECTOR SIGNATURE: Mafent	Chy			DATE: 9/29/15
FACILITY RESPONSE PLAN (FRP) APPLICABIL				
A non-transportation related onshore facility is required t	o prepare and impler	ment ar	n FRP as outlined in	1 40 CFR 112.20 if:

Onshore Facilities (Excluding Production)

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112.3(g)(1)	The aggregate aboveground storage capacity is 10,000 gallons or less	□ Yes ∠No
	AND	
112.3(g)(2)	The facility has had no single discharge as described in §112.1(b) exceeding 1,000 U.S. gallons, OR the facility has had no two discharges as described in §112.1(b) exceeding 42 U.S. gallons within any twelve-month period in the three years prior to the SPCC Plan self-certification date, or since becoming subject to the rule if the facility has been in operation for less than three years. (Note: Oll discharges that result from natural disasters, acts of war, or terrorism are not included in this qualification determination.)	□ Yes ØÑo
	OTH OF THE ABOVE, THEN THE FACILITY IS CONSIDERED A QUALIFIED FACILITY: Cort and Appendix A.	nplete relevant sections of
REQUIREM	ENTS FOR PREPARATION AND IMPLEMENTATION OF A SPCC PLAN—40 CFF	R 112.3
Date facility b	egan operations: 1945	
Date of initial	SPCC Plan preparation: May 2003 Current Plan version (date/number):	4/3/2008
112.3(a), (c)	For facilities (excluding farms) in operation prior to August 16, 2002, Plan amended to reflect 2002 SPCC requirements and changes implemented by July 1, 2009	
	For facilities (excluding farms) beginning operation between August 17, 2002, and July 1, 2009, Plan prepared and fully implemented by July 1, 2009	□Yes □No ØNA
112.3(b), (c)	For facilities beginning operation after July 1, 2009, Plan prepared and fully implemented before beginning operations	□Yes □No PNA
112.3(d)	[2002 Rule Requirement] [Except for self-certified Plans]	
	Professional Engineer certification includes statement that the PE attests:	
	PE is familiar with the requirements of 40 CFR part 112	pzYes □ No □ NA
	PE or agent has visited and examined the facility	Yes □ No □ NA
	 Plan is prepared in accordance with good engineering practice including consideration of applicable industry standards and the requirements of 40 CFR part 112 	ZaYes □ No □ NA
	Procedures for required inspections and testing have been established	⊠Yes □ No □ NA
	Plan is adequate for the facility	ZYes □ No □ NA
	[Requirement for facilities that began operation on or before August 16, 2002] [Except for sea	f-certified Plans]
	Plans should include evidence that the PE:	
	Has examined the facility	ZYes □ No □ NA
	Is familiar with the provisions of this part	ØYes □ No □ NA
	 Attests that the SPCC that Plan has been prepared in accordance with good engineering practices 	∠Yes □ No □ NA
PE Name: 🙎	Fit G. Politte License No.: 77962 State: NY Date of ce	rtification: 12 -/ \$ -03
112.3(e)	[2002 Rule Requirement]	
	Plan available onsite if facility is attended at least 4 hours per day (If facility is unattended, please note nearest field office contact information in comments section below)	Yes O No O NA
	[Interim requirement for facilities that began operation on or before August 16, 2002]	
,	Plan available onsite if facility is attended at least 8 hours per day (if facility is unattended, please note nearest field office contact information in comments section below)	□Yes □ No ÆNA

The facility transfers oil over water to or fro	om vessels and has a total oil storage o	apacity greater tha	n or equal to 42,000
galtons, OR The facility has a total oil storage capacity of at least 1 n	nilling gallogs, and at least one of the fo	ollowing is true:	
The facility does not have secondary conta tank plus sufficient freeboard for precipitat	ainment sufficiently large to contain the ion.	capacity of the larg	
☐ The facility is located at a distance such the environments.			sensitive
 The facility is located such that a discharge The facility has had a reportable discharge 			rs.
Facility has FRP: Yes No Not Required	FRP Number: 200	128	
Facility has a completed and signed copy of Appendix D), Attachment C-II,		
"Certification of the Applicability of the Substantial Harm	Criteria."		□ Yes □ No
Comments:			
	•		
SPCC GENERAL APPLICABILITY-40 CFR 112	.1	1	
IS THE FACILITY REGULATED UNDER 40 CFR part 1	12?	·	
The completely buried oil storage capacity is over 42,00 capacity is over 1,320 gallons	00 gallons, OR the aggregate abovegro	ound oil storage	Yes □ No
AND			
The facility is a non-transportation-related facility engag refining, transferring, distributing, using, or consuming or reasonably be expected to discharge oil into or upon the 40 CFR 110.1).	il and oil products, which due to its loc	ation could	Yes □ No
AFFECTED WATERWAY(S):		DISTANCE:	
Newton Creek PATH: Direct		200 ft	
PATH:		•	
JA CI			
Note: The following storage capacity is not considered in deter Completely buried tanks subject to all the technical requirer Equipment subject to the authority of the U.S. Department of defined in Memoranda of Understanding dated November 2 Any facility or part thereof used exclusively for wastewater t Containers smaller than 55 gallons. Permanently closed containers. Motive power containers	nents of 40 CFR part 280 or a state program of Transportation, U.S. Department of the In 24, 1971, and November 8, 1993.	terior, or Minerals Ma	nagement Service, as
Does the facility have an SPCC Plan?			_Erres □ No
	A 1. 1		
Comments: Plan 18 being	updured		
Comments: Plan 13 being	v p direa		

Page 3 of 19

Comments:		·
	NT OF SPCC PLAN BY REGIONAL ADMINISTRATOR (RA)—40 CFR 112.4	
112.4(a)	Has the facility discharged more than 1,000 gallons of oil in a single reportable discharge or more than 42 gallons in each of two reportable discharges in any 12-month period (see 40 CFR part 110)? Note: A reportable discharge is a discharge as described in §112.1(b).	□ Yes 🗹 No
	 If yes, was information submitted to the RA as required in §112.4(a)? 	□ Yes □ No NA
·	Date(s) of reportable discharges(s):	
	Were the discharges reported to the NRC?	□ Yes □ No
112.4(d), (e)	Have changes required by the RA been implemented in the Plan and/or facility?	□Yes □No ANA
Comments:	No discharge	
·		
	NT OF SPCC PLAN BY THE OWNER OR OPERATOR—40 CFR 112.5	····
112.5(a)	Has there been a change at the facility that materially affects the potential for a discharge?	☐ Yes
, 	If yes, was the Plan amended within six months of the change?	□ Yes □ No
112.5(b)	Review and evaluation of the Plan completed at least once every 5 years?	∠ZYes □ No □ NA
	Following Plan review, and if amendment was required, was Plan amended within six months to include more effective prevention and control technology, if available?	Yes □ No □ NA
	[2002 Rule Requirement]	
	Amendments implemented within six months of any Plan amendment?	DYes □ No □ NA
	Plan review and evaluation documented in Plan?	DYes □ No □ NA
112.5(c)	Professional Engineer certification of any technical Plan amendments in accordance with §112.3(d) [Except for self-certified Plans]	□ Yes □ No □ NA
Name:	License No.: State: Date of	f certification:
Reason for a	mendment:	
Amendments	implemented within six months of any Plan amendment	□Yes □No □NA
Comments:	Amendant 1s process now. New Bee available	plan will
	Bee available	

ENERAL S	PCC REQUIREMENTS-40 CFR 112.7	PLAN	FIELD
anagement a	approval at a level of authority to commit the necessary resources to fully implement the Plan	z Yes ⊏	No
ame:	anne gt. Wealintz Title: Metro pointen Complex Mas	Date: Z	1-3-0
an follows se	equence of the rule or provides a cross-reference of requirements in the Plan and the rule	Yes D No	
	facilities, procedures, methods, or equipment not yet fully operational, details of their installation and scussed (Note: Relevant for inspection evaluation and testing baselines.)	☐ Yes ☐ No ☐ NA	
12.7(a)(2)	If there are deviations from the requirements of the rule, the Plan states reasons for nonconformance	☐ Yes ☐ No ☐ NA	
	Alternative measures described in detail and provide equivalent environmental protection (Note: Inspector should document if the environmental equivalence is implemented in the field)	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☑ NA
Plai	deviation and reasons for nonconformance n refers to main Contingency Plan for all f	egui	remon
	MON Bula Bookkation	<u> </u>	
2.7(a)(3)	[2002 Rule Requirement] Plan includes diagram with location and contents of all regulated containers (including completely buried tanks otherwise exempt from the SPCC requirements), transfer stations, and connecting pipes (Note in comments any discrepancies between the diagram and what is observed in the field)	□ Yes □ No	□ Yes □ No
2.7(a)(3)	Plan addresses each of the following:		
(i) For e	ach container, type of oil and storage capacity (see Appendix B)	☑ Yes □ No	☐ Yes ☐ No
(ii) Disch	narge prevention measures, including procedures for routine handling of products	✓ Yes	Z Yes □ No
	narge or drainage controls, such as secondary containment around containers, and other structures, ment, and procedures for the control of a discharge	☑ Yes □ No	Ø Yes □ No
(iv) Coun resou	ntermeasures for discharge discovery, response, and cleanup (both facility's and contractor's urces)	☑ Yes □ No	□ Yes
(v) Meth	ods of disposal of recovered materials in accordance with applicable legal requirements	☑ Yes □ No	
contr	act list and phone numbers for the facility response coordinator, National Response Center, cleanup actors contracted to respond to a discharge, and all Federal, State, and local agencies who must be acted in the case of a discharge as described in §112.1(b)	☑ Yes □ No □ NA	
	[2002 Rule Requirement]		
12.7(a)(4)	Plan includes information and procedures that enable a person reporting a discharge as described in §112.1(b) to relate information on the exact address or location and phone number of the facility; the date and time of the discharge; the type of material discharged; estimates of the total quantity discharged; estimates of the quantity discharged as described in §112.1(b); the source of the discharge; a description of all affected media; the cause of the discharge; any damages or injuries caused by the discharge; actions being used to stop, remove, and mitigate the effects of the discharge; whether an evacuation may be needed; and the names of individuals and/or organizations who have also been contacted (Not required if a facility has an FRP)	Ø Yes □ No □ NA	Transportation of the Contract
	[2002 Rule Requirement]	7	1
12.7(a)(5)	Plan organized so that portions describing procedures to be used when a discharge occurs will be readily usable in an emergency (Not required if a facility has an ERP)	☐ Yes ☐ No	

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GENERAL	SPCC REQUIREMENTS—40 CFR 112.7	PLAN	FIELD
112.7(b)	Plan includes a prediction of the direction, rate of flow, and total quantity of oil that could be discharged for each type of major equipment failure where experience indicates a reasonable potential for equipment failure	Yes No	Yes Do No
112.7(c)	Appropriate containment and/or diversionary structures or equipment provided to prevent a discharge as described in §112.1(b), except as provided in 112.7(k) of this section for qualified operational equipment, before cleanup occurs. The entire containment system including walls and floors are capable of containing of land are constructed to prevent escape of a gischarge from the containment system before cleanup occurs (1) For onshore facilities, one of the following or its equivalent: (i) dikes, berms, or retaining walls sufficiently impervious to contain oil, (ii) curbing, (iii) culverting, gutters or other drainage systems, (iv) weirs, booms or other barriers, (v) spill diversion ponds, (vi) retention ponds, or (vii) sorbent materials (See Appendix B)	Yes II No II NA	à Yes □ No □ NA
112.7(d)	Determination(s) of impracticability of secondary containment	☑ Yes □ No	
If YES:	Is the impracticability of secondary containment clearly demonstrated?	☐ Yes ☐ No ☐ NA	Yes D No D NA
	[2002 Rule Requirement] For bulk storage containers, periodic integrity testing of containers and leak testing of the valves and piping associated with the container is conducted	☐ Yes ☐ No ☐ NA	□ Yes □ No □ NA
•	Unless facility has FRP: (1) Contingency Plan following 40 CFR part 109 (see Appendix D checklist) is provided AND	☐ Yes ☐ No ☐ NA	- William Section
	(2) Written commitment of manpower, equipment, and materials required to control and remove any quantity of oil discharged that may be harmful	☐ Yes ☐ No ☐ NA	☑ Yes □ No □ NA
Comments of	concerning impracticability determination(s) for secondary containment: $FRPIan$		
			-
Other comm	nents:		

GENERA	LS	PCC REQUIREMENTS—40 CFR 112.7	PLAN	FIELD
112.7(e)		Inspections and tests conducted in accordance with written procedures	☑ Yes □ No	E Yes □ No
		Record of inspections or tests signed by supervisor or inspector and kept with Plan for at least 3 years (see Appendix C checklist)	∠Z Yes □ No	☑ Yes □ No
112.7(f)		Personnel, training, and oil discharge prevention procedures [1973 Rule: 112.7(e)(10)]		
-	(1)	Training of oil-handling personnel in operation and maintenance of equipment to prevent discharges; discharge procedure protocols; applicable pollution control laws, rules and regulations; general facility operations, and contents of Special 120-11	Yes No NA	Yes No
	(2)	Person designated as accountable for discharge prevention at the facility	☑ Yes □ No □ NA	Æ Yes □ No □ NA
	47: T	[2002 Rule Requirement]	ZIYes □ No	☑ Yes □ No
	(3)	Discharge prevention briefings conducted at least once a year for oil handling personnel	□ NA	□ NA
		[Interim requirement for facilities that began operation on or before August 16, 2002]		•
	(3)	Spill prevention briefings scheduled and conducted at intervals frequent enough to assure adequate understanding of the SPCC Plan for that facility.	Yes No	Yes No
112.7(g)		Security (excluding production facilities) [1973 Rule: 112.7(e)(9)] [Except self-certified Plans]		
	(1)	Facility fully fenced and gates are locked and/or guarded when facility is unattended	✓ Yes □ No □ NA	☐ Yes ☐ No ☐ NA
	(2)	Master flow and drain valves and any other valves permitting direct outward flow of the container's contents to the surface have adequate security measures so that they remain in the closed position when in non-operating or non-standby status	☑ Yes □ No □ NA	Yes No
	(3)	Pump starter controls locked in "off" position and accessible only to authorized personnel when in non-operating/non-standby status	Z Yes □ No □ NA	Yes □ No □ NA
	(4)	Loading/unloading connections of oil pipelines or facility piping securely capped or blank-flanged when not in service or when in standby service for an extended period of time, including piping that is emptied of liquid content either by draining or by inert gas pressure	Yes D No	Yes I No I NA
	(5)	Adequate facility lighting commensurate with the type and location of the facility that assists in the discovery of discharges occurring during hours of darkness and to prevent discharges occurring through acts of vandalism	☑ Yes □ No □ NA	Yes No
Comments	s:	Plan refer to & Master Contrying Plan		
112.7(h)	•	Tank car and tank truck loading/unloading rack [1973 Rule: 112.7(4)] Note that a tank car/truck loading/unloading rack must be present for §112.7(h) to apply		
	(1)	Does loading/unloading area (the location adjacent to the loading or unloading rack) drainage flow to catchment basin or treatment facility? ∠Yes □ No • If NO, quick drainage system used	☑ Yes. □ No □ NA	☐ Yes ☐ No ☐ NA
,		Containment system holds capacity of the largest single compartment of a tank car/truck loaded/unloaded at the facility	El Yes □ No □ NA	☐ Yes ☐ No ☐ NA
	(2)	Physical barriers, warning signs, wheel chocks, or vehicle brake interlock system in loading/unloading areas (the location adjacent to the loading or unloading rack) to prevent vehicles from departing before complete disconnection of flexible or fixed oil transfer lines	☐ Yes ☐ No ☐ NA	Yes No
	(3)	Lower-most drains and all outlets on tank cars/trucks inspected prior to filling/departure, and, if necessary ensure that they are tightened, adjusted, or replaced to prevent liquid discharge while in transit	Yes No NA	☐ Yes☐ No☐ NA

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GENERAL:	SPCC REQUIREMENTS—40 CFR 112.7	PLAN	FIELD
Comments:			
112.7(i)	Brittle fracture evaluation of field-constructed aboveground containers [2002 Rule Requirement]	1	- 10 to 20
of a	le fracture evaluation is conducted after tank repair/alteration/change in service that might affect the risk discharge or after a discharge/failure due to brittle fracture or other catastrophe, and appropriate action n as necessary (for field-constructed aboveground containers)	☐ Yes ☐ No ☐ NA	□ Yes □ No ☑ NA
112.7(j)	State rules, regulations and guidelines and conformance with applicable sections of 40 CFR part 112.7(e)]	t 112 [19	173 Rule:
	cussion of conformance with applicable more stringent State rules, regulations, and guidelines and ar effective discharge prevention and containment procedures listed in 40 CFR part 112	☑ Yes □ No □ NA	
112.7(k)	Qualified oil-filled operational equipment secondary containment option [2006 Rule Amendment]	I	
(1)	Has a single reportable discharge as described in §112.1(b) from any oil-filled operational equipment exceeding 1,000 U.S. gallons occurred within any 12-month period within the three years prior to Plan certification date?	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☐ NA
	Have two reportable discharges as described in §112.1(b) from any oil-filled operational equipment each exceeding 42 U.S. gallons occurred within any 12-month period within the three years prior to Pian certification date?	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☐ NA
	 If YES for either, secondary containment is required. (Note: Oil discharges that result from natural war, or terrorism are not included in this qualification determination.) See 112.7(c). 	disasters,	, acts of
If NO and no secondary containment	(2)(i) Facility procedure for inspections/monitoring program is established and documented	☐ Yes ☐ No ☑ NA	☐ Yes ☐ No ☑ NA
is provided	(2)(ii) Unless facility has FRP: Contingency plan following 40 CFR part 109 (see Appendix D checklist) is provided AND	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☑ NA
	Written commitment of manpower, equipment, and materials required to control and remove any quantity of oil discharged that may be harmful	Yes No	Yes No
Comments:	Rep plan available No spill history		
ONSHORE	FACILITIES (EXCLUDING PRODUCTION)—112.8/112.12	PLAN	FIELD
112.8(b)/112	.12(b) Facility Drainage [1973 Rule: 112.7(e)(1)]		
	brailings from dived solvings already is restrained by views, Or instruding activated parties of ejectors	2 Yes □ No □ NA	Yes No
(2)	/alves from diked storage areas are manual, open-and-closed design (not flapper-type drain valves)	Ó Yes □ No □ NA	Æ Yes □ No □ NA
	f drainage is released directly to a watercourse and not into an onsite wastewater treatment plant, storm water inspected per §112.8(c)(3)(ii), (iii), and (iv) or §112.12(c)(3)(ii), (iii), and (iv)	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☐ NA
(3)	prantage from undired areas with a potential for discrizing designed to how into points, ragionis, or	□ Yes □ No ☑ Na	☐ Yes ☐ No

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(4) If facility drainage not engineered as in (b)(3), the facility is equipped with a diversion system to retain oil in the facility in the event of a discharge.*

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□ No ₽ÑA □ Yes □ No No PNA

☐ Yes

ONSHORE FACILITIES (EXCLUDING PRODUCTION)—112.8/112.12	PLAN	FIELD
(5) Are facility drainage waters continuously treated in more than one treatment unit and pump transfer is n ☐ Yes ☑ No If YES:	eeded?	
Two "lift" pumps available and at least one permanently installed	□ Yes □ No	□ Yes □ No
 Facility drainage systems engineered to prevent a discharge as described in §112.1(b) in the case of equipment failure or human error 	□ Yes □ No	□ Yes □ No
comments: drainage is observed prior to treatment of the served prior to treatment of the served of the served of the served. * These provisions apply only when a facility drainage system is used for containment; otherwise mark NA.	al	20
112.8(c)/112.12(c) Bulk Storage Containers [1973 Rule: 112.7(e)(2)]		
If bulk storage containers are not present, mark this section Non Applicable (NA). If present, complete this section this checklist)		
(1) Containers compatible with material stored and conditions of storage such as pressure and temperature	Yes No	Yes No NA
 (2) Except for mobile refuelers, construct secondary containment to hold capacity of largest container and sufficient freeboard for precipitation 	☑ Yes □ No □ NA	Yes No
Diked areas sufficiently impervious to contain discharged oil	ZiYes □ No □ NA	Yes I No NA
Alternatively, any discharge to a drainage trench system will be safely confined in a facility catchment basin or holding pond	☐ Yes ☐ No NA	☐ Yes ☐ No ☑ NA
(3) Is there drainage of uncontaminated rainwater from diked areas into a storm drain or open watercourse	?	
∠ZYes □ No If YES:	T	
(i) Bypass valve normally sealed closed	Yes No	☐ Yes ☐ No ☐ NA
(ii) Retained rainwater is inspected to ensure that its presence will not cause a discharge as described in §112.1(b)	Yes No	☑ Yes □ No □ ŅA
(iii) Bypass valve opened and resealed under responsible supervision	Æ Yes □ No □ NA	☑ Yes □ No □ NA
(iv) Adequate records of drainage are kept; for example, records required under permits issued in accordance with 40 CFR 122.41(j)(2) and (m)(3)	∠ Yes □ No □ NA	☑ Yes □ No □ NA
(4) For completely buried metallic tanks installed on or after January 10, 1974 (if not exempt from SPCC results subject to all of the technical requirements of 40 CFR part 280 or 281):	_	_,
Corrosion protection with coatings or cathodic protection compatible with local soil conditions	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☐ NA
Regular leak testing conducted	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☑ NA
(5) Partially buried or bunkered metallic tanks protected from corrosion with coatings or cathodic protection compatible with local soil conditions	☐ Yes ☐ No ☑ NA	☐ Yes ☐ No ☐ NA

ONSHOR	SHORE FACILITIES (EXCLUDING PRODUCTION)—112.8/112.12		
Comments:			
		•	
		•	,
(6)	[2002 Rule Requirement]		1 1 1
Except for	Aboveground containers integrity tested by visual inspection and another technique such as	Yes	Yes
self- certified	hydrostatic testing, radiographic testing, ultrasonic testing, acoustic emissions testing, or another system of non-destructive shell testing on a regular schedule and whenever material repairs are made	□ No □ NA	□ No □ NA
Plans]	[Interim requirement for facilities that began operation on or before August 16, 2002]		
	Aboveground tanks integrity tested using such techniques as hydrostatic testing, visual inspection or a system of non-destructive shell thickness testing.	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No Æ-NA
	Container supports and foundations regularly inspected	Ø Yes □ No □ NA	Yes No
,	Outside of containers frequently inspected for signs of deterioration, discharges, or accumulation of oil inside diked areas	☐ Yes☐ No☐ NA	→ Yes □ No □ NA
	Records of inspections and tests maintained	☑ Yes □ No □ NA	PYes □ No □ NA
(7)	Leakage through defective internal heating coils controlled:	☐ Yes ☐ No	☐ Yes ☐ No
	 Steam returns and exhaust lines from internal heating coils that discharge into an open water source are monitored for contamination, OR 	De NA	D-NA
	 Steam returns and exhaust lines pass through a settling tank, skimmer, or other separation or retention system 		
(8)	Each container is equipped with at least one of the following for liquid level sensing (i) high liquid level- alarms with an audible or visual signal at a constantly attended operation or surveillance station, or audible air vent in smaller facilities, (ii) high liquid level pump cutoff devices set to stop flow at a predetermined container content level, (iii) direct audible or code signal communication between container gauger and pumping station, (iv) fast response system (such as digital computers, telepulse,	En Yes □ No □ NA	Ves No NA
	or direct vision gauges) and a person is present to monitor gauges and the overall filling of bulk storage containers. (v) liquid level sensing devices regularly tested to ensure proper operation		
(9)	Effluent treatment facilities observed frequently enough to detect possible system upsets that could cause a discharge as described in §112.1(b)	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No ☐ NA
(10)	Visible discharges which result in a loss of oil from the container, including but not limited to seams, gaskets, piping, pumps, valves, rivets, and bolts are promptly corrected and oil in diked areas is promptly removed	P Yes □ No □ NA	□ Yes □ No □ NA
(11)	Mobile or portable containers positioned to prevent a discharge to prevent a discharge as described in §112.1(b).	☐ Yes ☐ No Æ NA	☐ Yes ☐ No ☐ NA
· ! !	Mobile or portable containers (excluding mobile refuelers) have secondary containment with sufficient capacity to contain the largest single compartment or container and sufficient free beard to contain precipitation	☐ Yes ☐ No ☐ NA	☐ Yes ☐ No Æ NA

ONSHOR	FACILITIES (EXCLUDING PRODUCTION)—112.8/112.12	PLAN	FIELD
Comments:			
		•	. :
112.8(d)/11	2.12(d) Facility transfer operations, pumping, and facility process [1973 Rule: 112.7(e)(3)]		-
(1)	[2002 Rule Requirement]	☐ Yes ☐ No	☐ Yes ☐ No
•	Buried piping installed or replaced on or after August 16, 2002 has protective wrapping or coating	D NA	E NA
	Buried piping installed or replaced on or after August 16, 2002 is cathodically protected or otherwise	□ Yes □ No	□ Yes □ No
	satisfies corrosion protection standards for piping in 40 CFR part 280 or 281	D NA	PZ NA
	[Interim requirement for facilities that began operation on or before August 16, 2002]		
	Buried piping has protective wrapping or coating and is cathodically protected if soil conditions	☐ Yes ☐ No	☐ Yes ☐ No
	warrant.	□ NA	□ NA
	Exposed buried piping is inspected for deterioration and corrosion damage is examined and corrected	☐ Yes ☐ No Ø NA	☐ Yes ☐ No
(2)	Piping terminal connection at the transfer point is marked as to origin and capped or blank-flanged	NA Yes	D NA E Yes
(2)	when not in service or in standby service for an extended time.	□ No □ NA	□ No □ NA
(3)	Pipe supports are properly designed to minimize abrasion and corrosion and allow for expansion and	☐ Yes	□ Yes
	contraction	□ NA	□ NA
(4)	Aboveground valves, piping, and appurtenances such as flange joints, expansion joints, valve glands	Ø Yes □ No	P Yes □ No
i	and bodies, catch pans, pipeline supports, locking of valves, and metal surfaces are inspected regularly	□ NA	□ NA
	[2002 Rule Requirement]		1
	Integrity and leak testing conducted on buried piping at time of installation, modification, construction,	☐ Yes	□ Yes
	relocation, or replacement	□ No □-NA	□ No □ NA
(5)	Vehicles warned so that no vehicle endangers aboveground piping and other of transfer operations	Er Yes □ No	Yes No
		I NA	IT NA

all Broned piping has Been fieled will concrete + and. Not used.

ONSHORE FACILITIES (EXCLUDING PRODUCTION)—112.8/112.12	PLAN	FIELD
Comments:		
		-
	•	
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	ADDITIONAL COMMENTS				
Rule Provision	Comment				
	·				
РНОТО DOCUM	ENTATION LOG				
Photo Number	Description (include date, location, and direction)				
. 					
	·				
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### **Qualified Facilities Checklist**

Appendix A: Qualified Facility Plan Requirements

Complete this Appendix only if the facility is a "qualified facility" as defined in §112.3(g). A qualified facility's Plan, whether certified by a PE or self-certified, must comply with all of the applicable requirements of §112.7 and subparts B and C of 40 CFR Part 1.12 referenced earlier in this checklist.

112.6-Qualified Facility Plan Requirements	Yes	No	NA
(a) Did the owner/operator of the qualified facility self-certify the SPCC Plan?			
If NO, see requirements for 112.3(d) above. If YES, did the owner/operator certify in the Plan that:			
(1) He or she is familiar with the requirements of 40 CFR part 112.			
(2) He or she has visited and examined the facility.			
(3) The Plan has been prepared in accordance with accepted and sound industry practices and standards.			
(4) Procedures for required inspections and testing have been established.			
(5) The Plan is being fully implemented.			
(6) The facility meets the qualification criteria set forth under §112.3 (g).			
(7) The Plan does not deviate from any requirements as allowed by §112.7(a)(2) and 112.7(d), except as described under §112.6(c).			
(8) Management has given full approval of the Plan and necessary resources have been committed for the Plan's full implementation.			
b) Did the owner/operator self-certify any of the Plan's technical amendments?			
f YES: Is the certification of any technical amendments in accordance with the provisions above (§112.6(a))?			
(c)(1) and (d)(1) Environmental Equivalence. For each alternative measure allowed under §112.7(a)(2), the Plan is accompanied by a written statement by a PE that states the reason for nonconformance and describes the alternative method and how it provides equivalent environmental protection in accordance with §112.7(a)(2).			
(c)(2) and (d)(1) Impracticability. For each determination of impracticability of secondary containment pursuant to §112.7(d), the Plan clearly explains why secondary containment measures are not practicable at this facility and provides the alternative measures required in §112.7(d) in lieu of secondary containment.			
(c)(3) Security. The Plan contains one of the following:  (i) The Plan complies with requirements under §112.7(g), OR  (ii) The Plan complies with the requirements under §112.6(c)(3)(ii): Plan describes how the owner/operator secures and and controls access to the oil handling, processing and storage areas; secures master flow and drain valves; prevents unauthorized access to starter controls on oil pumps; secures out-of-service and loading/unloading connections of oil pipelines; addresses the appropriateness of security lighting to both prevent acts of vandalism and assist in the discovery of oil discharges.			
(i) The Plan complies with the requirements under §§112.8(c)(6) or 112.12(c)(6), as applicable; OR  (ii) The Plan complies with the requirements under §112.6(c)(4)(ii):  Aboveground containers, supports and foundations tested for integrity on a regular schedule and whenever repairs are made.			
<ul> <li>Appropriate qualifications for personnel performing tests and inspections have been determined in accordance with industry standards.</li> <li>The frequency and type of testing and inspections have been determined in accordance with industry standards, taking into account container size, configuration and design.</li> <li>Container supports and foundations regularly inspected</li> <li>Outside of containers frequently inspected for signs of deterioration, discharges, or accumulation of oil inside diked areas</li> </ul>			
Records of inspections and tests maintained  d) Did a PE certify a portion of a qualified facility's self-certified Plan?			
If YES, the PE must certify in the Plan that:  d)(2)  (I) He/she is familiar with the requirements of 40 CFR Part 112.  (Ii) He/she or a representative agent has visited and examined the facility.  (iii) The alternative method of environmental equivalence in accordance with §112.7(a)(2) or the determination of impracticability and alternative measures in accordance with §112.7(d) is consistent with good engineering practice, including consideration of applicable industry standards, and with the requirements of 40 CFR Part 112.			

Onshore Facilities (Excluding Production)

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Comments:		did a PE certify any technical ame				
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#### SPCC INSPECTION AND TESTING CHECKLIST

Appendix C: Required Documentation of Tests and Inspections

Records of inspections and tests required by 40 CFR part 112 signed by the appropriate supervisor or inspector must be kept with the SPCC Plan for a period of three years. Records of inspections and tests conducted under usual and customary business practices will

suffice. Documentation of the following inspections and tests should be kept with the SPCC Plan. Documentation Not Inspection or Test Applicable **Not Present** Present 112.7-General SPCC Requirements [2002 Rule Requirement] (d) Integrity testing is conducted for bulk storage containers with no secondary containment system and for which an impracticability determination has been made (d) Integrity and leak testing of valves and piping associated with bulk storage containers with no secondary containment system and for which an impracticability determination has been made Evaluate field-constructed aboveground containers for potential for brittle fracture or other catastrophic failure when the container undergoes a repair, alteration, reconstruction or change in service 112.8/112.12-Onshore facilities (excluding production) (b)(2)Storm water released from facility drainage directly to a watercourse is inspected and records of drainage are kept Rainwater released directly from diked containment areas to a storm drain or open (c)(3)(iv)watercourse is inspected and records of drainage are kept Regular leak testing of completely buried metallic storage tanks (c)(4)Aboveground containers tested for integrity on a regular schedule (c)(6)(c)(6)Aboveground containers, supports and foundations visually inspected on a regular schedule (c)(6)Diked areas inspected for accumulations of oil. Liquid level sensing devices regularly tested to ensure proper operation (c)(8)(v)Effluent treatment facilities are observed frequently enough to detect possible system (c)(9)upsets that could cause a discharge as described in §112.1(b) When buried piping is exposed, it is carefully inspected for deterioration and corrosion (d)(1)Aboveground valves, piping and appurtenances are regularly inspected and the general (d)(4)condition of flange joints, expansion joints, valve glands and bodies, catch pans, pipeline supports, locking of valves, and metal surfaces are assessed [2002 Rule Requirement] (d)(4)Integrity and leak testing of buried piping is conducted at time of installation, modification, construction, relocation or replacement 112.6--Qualified Facilities (Complete this section only if the facility is a "qualified facility" as defined in §112.3(g)) (c)(4)(i)Comply with the requirements under §112.8(c)(6) or §112.12(c)(6) as applicable (see above); OR Aboveground containers inspected and/or tested for integrity on a regular (c)(4)(ii) schedule and whenever repairs are made

Onshore Facilities (Excluding Production)

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Appropriate qualifications for personnel performing tests and inspections have been

The frequency and type of testing and inspections have been determined in accordance with industry standards, taking into account container size, configuration and design

determined in accordance with industry standards

### PRODUCT STORAGE TANK LIST

TANK NO.	PRODUCT IDENTIFICATION		NOMINAL CAPACETY (GAL.)	ACTUAL CAPACITY (GAL.)
41	ETHANOL	A/G	90,700	80,500
42	ETHANOL	A/G	90,700	80,500
43	GASOLINE (REGULAR)	A/G	90,700	80,500
44	GASOLINE (REGULAR)	A/G	90,700	80,700
45	ETHANOL	A/G	90,700	80,700
46	ETHANOL	A/G	88,875	78,373
47	GASOLINE (REGULAR)	A/G	425,000	373,755
48	GASOLINE (REGULAR)	A/G	425,000	373,609
49	GASOLINE (SUPER)	A/G	450,000	419,926
50	GASOLINE (SUPER)	A/G	450,000	422,926
51	ADDITIVE (SHELL)	A/G	5,000	4,500
52	ADDITIVE (EXXON)	U/G	5,000	3,600
53	WATER/GASOLINE	A/G	6,000	5,400
54	ADDITIVE (MOBIL)	A/G	5,000	4,500
55	DIESEL	A/G	10,000	9,300
7	OUT OF SERVICE	A/G	12,000	10,200
8	OUT OF SERVICE	A/G	12,000	10,200
9	ADDITIVE (GENERIC)	A/G	12,000	10,200
10	ADDITIVE (SHELL)	A/G	12,000	10,200
16	OIL/WATER SEP.	U/G	6,000	5,400

A/G : ABOVE GROUND A/U : UNDER GROUND

### SPCC FIELD INSPECTION AND PLAN REVIEW TABLE

Appendix B: Documentation of Field Observations for Containers and Associated Requirements

Inspectors should use this table to document observations of containers as needed.

Containers and Piping

Check containers for leaks, specifically looking for: drip marks, discoloration of tanks, puddles containing spilled or leaked material, corrosion, cracks, and localized dead vegetation, and standards/specifications of construction.

Check foundation for: cracks, discoloration, puddles containing spilled or leaked material, settling, gaps between container and foundation, and damage caused by vegetation roots.

Check piping for: droplets of stored material, discoloration, corrosion, bowing of pipe between supports, evidence of stored material seepage from valves or seals, and localized dead vegetation. (Document in comments section of §112.8(d) / §112.12(d).)

### Secondary Containment (Active and Passive)

Check secondary containment for: containment system (including walls and floor) ability to contain oil such that oil will not escape the containment system before cleanup occurs, proper sizing, cracks, discoloration, presence of spilled or leaked material (standing liquid), erosion, corrosion, and valve conditions.

Check dike or berm systems for: level of precipitation in dike/available capacity, operational status of drainage valves (closed), dike or berm impermeability, debris, erosion, impermeability of the earthen floor/walls of diked area, and location/status of pipes, inlets, drainage around and beneath containers, presence of oil discharges within diked areas.

Check retention and drainage ponds for: erosion, available capacity, and presence of spilled or leaked material, debris, and stressed vegetation.

Check active measures (countermeasures) for: amount indicated in plan is available and appropriate; deployment procedures are realistic; material is located so that they are readily available; efficacy of discharge detection; availability of personnel and training, appropriateness of measures to prevent a discharge as described in §112.1(b).

Container ID/ General Condition	Storage Capacity and Type of Oil	Type of Containment/ Drainage Control	Overfill Protection and Testing & Inspections
	· · · · · · · · · · · · · · · · · · ·		
	-		
· ·			

Onshore Facilities	(Excluding	Production)
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Not applicable

### SPCC CONTINGENCY PLAN REVIEW CHECKLIST

Appendix D: 40 CFR Part 109-Criteria for State, Local and Regional Oil Removal Contingency Plans

If a facility makes an impracticability determination for secondary containment in accordance with §112.7(d), it is required to provide an oil spill contingency plan following 40 CFR part 109. An oil spill contingency plan may also be developed as an alternative to general secondary containment for qualified oil filled operational equipment in accordance with §112.7(k).

109.5-Development and implementation criteria for State, local and regional oil removal contingency plans*	Yes	No
(a) Definition of the authorities, responsibilities and duties of all persons, organizations or agencies which are to be involved in planning or directing oil removal operations.		
(b) Establishment of notification procedures for the purpose of early detection and timely notification of an oil discharge including:		
(1) The identification of critical water use areas to facilitate the reporting of and response to oil discharges.		
(2) A current list of names, telephone numbers and addresses of the responsible persons (with alternates) and organizations to be notified when an oil discharge is discovered.		
(3) Provisions for access to a reliable communications system for timely notification of an oil discharge, and the capability of interconnection with the communications systems established under related oil removal contingency plans, particularly State and National plans (e.g., NCP).		
(4) An established, prearranged procedure for requesting assistance during a major disaster or when the situation exceeds the response capability of the State, local or regional authority.		
(c) Provisions to assure that full resource capability is known and can be committed during an oil discharge situation including:		-
(1) The identification and inventory of applicable equipment, materials and supplies which are available locally and regionally.		
(2) An estimate of the equipment, materials and supplies that would be required to remove the maximum oil discharge to be anticipated.		
(3) Development of agreements and arrangements in advance of an oil discharge for the acquisition of equipment, materials and supplies to be used in responding to such a discharge.		
(d) Provisions for well defined and specific actions to be taken after discovery and notification of an oil discharge including:		
(1) Specification of an oil discharge response operating team consisting of trained, prepared and available operating personnel.		
(2) Predesignation of a properly qualified oil discharge response coordinator who is charged with the responsibility and delegated commensurate authority for directing and coordinating response operations and who knows how to request assistance from Federal authorities operating under existing national and regional contingency plans.		
(3) A preplanned location for an oil discharge response operations center and a reliable communications system for directing the coordinated overall response operations.		
(4) Provisions for varying degrees of response effort depending on the severity of the oil discharge.		
(5) Specification of the order of priority in which the various water uses are to be protected where more than one water use may be adversely affected as a result of an oil discharge and where response operations may not be adequate to protect all uses.		
(e) Specific and well defined procedures to facilitate recovery of damages and enforcement measures as provided for by State and local statutes and ordinances.		
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^{*} The contingency plan should be consistent with all applicable state and local plans, Area Contingency Plans, and the National Contingency Plan (NCP).

8.3 ...........HAZARDOUS WASTE CONTINGENCY PLAN (40 CFR 265 SUBPART D)

8.3.1 ...... Distribution Letter to Local Agencies

September 30, 2001

To: Distribution List

Re: 40 CFR 265 Subpart D Hazardous Waste Contingency Plan

This document is being provided to meet the requirements of 40 CFR 265 Subpart D requiring hazardous waste facilities to provide a contingency plan for responding to fires, explosions, or any unplanned sudden or non-sudden release of hazardous waste or hazardous waste constituents to air, soil, or surface water.

This regulation allows for the amendment of an existing emergency or contingency plan to address the release of a hazardous waste. The document being provided to you is the Hazardous Waste Contingency Plan (HWCP) for the Motiva Enterprises LLC Brooklyn Terminal. This plan represents the pertinent information that would be necessary to respond to an incident at the terminal, or similarly, treat victims of any incident at the terminal. For the Brooklyn Terminal, hazardous materials generated from the facility will be petroleum-based products. Material Safety Data Sheets (MSDS) for products that are stored and handled at the terminal have also been included to aid in the response effort.

The intent of this regulation is to ensure that local responders have an understanding of the facilities with which they are dealing in the event of an emergency. The Oil Spill Response Plan was prepared under the guidelines of the Oil Pollution Act of 1990 (OPA-90) and provides large quantities of information regarding terminal operations. This HWCP represents the initial actions and information that would be needed for a response from any of the local responders or emergency services. By additionally providing MSDS sheets for products handled at the terminal we believe we are meeting the intent of the regulation.

Please maintain this document as a record of the actions that will be taken to minimize hazards to human health or the environment from fires, explosions or any unplanned release of hazardous waste.

Nassau County Emergency Management

Attn: Inspector Tom Skelly

140 15th Street Mineola, NY 11501

Lawrence Fire Department 75 Washington Avenue Lawrence, NY 11559

Nassau County Fire Marshall's Office

899 Jerusalem Avenue Uniondale, NY 11553

Nassau County Medical Center

Emergency Coordinator 2201 Hempstead Turnpike East Meadow, NY 11554

Nassau County Police Dept.

1699 Broadway Hewlett, NY 11557

Malverne Fire Dept. 1 Britton Circle

Malverne, NY 11565

At this time, it is our intentions that this document will be updated when significant changes in chemical storage result in a change in emergency strategy. Please retain this letter as an introduction to this document. If additional information is needed, please contact the Terminal Manager at 516-371-4780.

Sincerely,

George O'Connor Health and Safety Representative

### Attachments

c: Nassau County Emergency Management
Lawrence Fire Department
Malverne Fire Dept.
Nassau County Medical Center
Nassau County Police Department
Nassau County Fire Marshall's Office

### 8.3.2 ...... Regulatory Cross-Reference

# (Hazardous Waste Contingency Plan Cross Reference 40 CFR 265 Subpart D)

HWCP 40 CFR 265 Subpart D	Located In ICP
265.52(a). Implementation Actions.	Core Plan 1.1.7
265.52(c). Arrangements with local agencies.	Core Plan 1.1.6.4
265.52(d). Names, addresses, numbers of Emergency Response Coordinators (Qualified Individuals)	Core Plan 1.1.2
265.52(e). Listing of emergency equipment:	Core Plan
Fire extinguishing systems	1.1.4.5
Spill control equipment, communications	1.1.4.4
Alarms	1.1.4.4, 1.1.6.1
Decontamination equipment	1.1.7.16
265.52(f). Evacuation Plan. 265.16 (d)(2) Job Descriptions	Core Plan 1.1.6 Annex 3.a.5

### 8.4 ......HAZARDOUS WASTE OPERATIONS EMERGENCY RESPONSE PLAN (29 CFR 1920.120)

### 8.4.1 ......Regulatory Cross-Reference

### CROSS REFERENCE FOR HAZARDOUS WASTE OPERATIONS EMERGENCY RESPONSE PLAN AND THE FACILITY RESPONSE PLAN (OPA '90)

	Motiva Enterprises LLG HAZWOPER Plan (29 CFR 1910.120(d)(2)(i-XiII)	Location in Core Plan (ERAP) & Integrated Contingency Plan
1.0	Pre-Emergency Planning and Coordination with Outside Parties (q)(2)(i)	
	1.1 Hazardous Substances Stored At facility*	Core Plan 1.1; Annex 7, Table 7.1
	1.2 Foreseeable types of incidents*	Core Plan 1.1.7.1; Annex 1, Figure 1.2
	1.3 Plot Plan*	Core Plan 1.1.8; Annex 1, Figure 1.2
	1.4 Pre-emergency planning and coordination*	Core Plan 1.1.6.1-1.1.6.4
2.0	Personnel Roles and Training (q)(2)(ii)	Core Plan 1.0 - Introductory Note; Annex 3.a.5; Annex 5; Annex 11.2
3.0	Communications and Notifications (q)(2)(ii)	Core Plan 1.1.1, 1.1.2 - Notification Lists; Core Plan 1.1.4.3; Annex 9.1.2, 9.2
4.0	Emergency Recognition and Prevention (q)(2)(iii)	Core Plan 1.1; 1.1.7.1; Annex 9
5.0	Safe Distances and Places of Refuge (q)(2)(iv)	Core Plan 1.1.6.1; Annex 9.6.7
6.0	Evacuation Routes and Procedures (q)(2)(vi)	Core Plan 1.1.6.1, 1.1.6.2, 1.1.8, Figure 1.3; Annex 1, Figure 1.3
7.0	Site Security and Control (q)(2)(v)	Core Plan 1.1.6.3; Annex 9
8.0	Decontamination (q)(2)(vii)	Core Plan 1.1.7.16
9.0	Emergency Medical Treatment and First Aid (q)(2)(viii)	Core Plan 1.1.7.16
10.0	Emergency Response Notifications (q)(2)(ix)	Core Plan 1.1.1 - 1.1.3, 1.1.4.4, 1.1.6.1,1.1.7.1; Annex 9.2
11.0	Emergency Response Procedure (q)(2)(ix)	1.1.7 - Immediate Actions; Annex 9
12.0	Personal Protective Equipment (q)(2)(xi)	Core Plan 1.0 - Introductory Note, 1.1.4.1
13.0	Review Process (q)(2)(x)	Core Plan 1.1.7.3

### 8.5 .......... U.S. Coast Guard Cross-Reference

33 C	FR §154:1030	LOCATION
(a)	The plan must be written in English.	Entire Plan
(b)	A response plan must be divided into the sections listed in this paragraph and formatted in the order specified herein unless noted otherwise. It must also have some easily found marker identifying each	TOC, Tabs and Annex 8.5
	section listed below. The following are the sections and subsections of a facility response plan:	
	(1) Introduction and plan contents.	Section I, 1.1
	(2) Emergency response action plan:	Section II Core Plan, 1.1
	(i) Notification procedures.	Section II Core Plan, 1.1.2 and 1.1.3
	(ii) Facility's spill mitigation procedures.	Section II Core Plan, 1.1.7
	(iii) Facility's response activities.	Section II Core Plan, 1.1.7.4
	(iv) Fish and wildlife and sensitive environments.	Section III Annex 3
	(v) Disposal plan.	Section III Annex 3.d.6
	(3) Training and Exercises:	Section III Annex 5
	(i) Training procedures.	Section III Annex 5.2
	(ii) Exercise procedures.	Section III Annex 5.1
	(4) Plan review and update procedures.	Section III Annex 6
	(5) Appendices.	
	(i) Facility-specific information.	Section I, 1.2
	(ii) List of contacts.	Section II Core Plan, 1.1.2
	(iii) Equipment lists and records.	Section II Core Plan, 1.1.4
	(iv) Communications plan.	
	(v) Site-specific safety and health plan.	Section II Core Plan, 2.1.1.1 and Section III Annex 3.b.3
	(vi) List of acronyms and definitions.	Section III Annex 12
	(vii) A geographic-specific appendix for each zone in which a mobile facility operates.	N/A
(c)	The required contents for each section and subsection of the plan are contained in §§ 154.1035, 154.1040, and 154.1041, as appropriate.	Section III Annex 8.5
(d)	The sections and subsections of response plans submitted to the COTP must contain at a minimum all the information required in §§154.1035, 154.1040, and 154.1041, as appropriate. It may contain other appropriate sections, subsections, or information that are required by other Federal, State, and local agencies.	Section III Annex 8.5 and Annex 10
(⊕)	For initial and subsequent submission, a plan that does not follow the format specified in paragraph (b) of this section must be supplemented with a detailed cross-reference section to identify the location of the applicable sections required by this subpart.	Section III Annex 8.5
<b>(f)</b>	The information contained in a response plan must be consistent with the National Oil and Hazardous Substances Pollution Contingency Plan (NCP) (40 CFR part 300) and the Area Contingency Plan(s) (ACP) covering the area in which the facility operates. Facility owners or operators shall ensure that their response plans are in accordance with the ACP in effect 6 months prior to initial plan submission or the annual plan review required under § 154.1065(a). Facility owners or operators are not required to, but may at their option, conform to an ACP which is less than 6 months old at the time of plan submission.	Section I, 1.1

### 8.5 .......... USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030 and 33 CFR §154.1035) Final Rules (Cont'd)

CFR	§154.1035	LOCATION		
(a)				
( ,	facility and plan information as follows:			
	(1) The facility's name, street address, city, county, state, ZIP code,	Section I, 1.2.1		
	facility telephone number, and telefacsimile number, if so			
	equipped. Include mailing address if different from street address.			
	(2) The facility's location described in a manner that could aid both a	Section I, 1.2.1, 1.2.2		
	reviewer and a responder in locating the specific facility covered			
	by the plan, such as, river mile or location from a known landmark			
	that would appear on a map or chart.  (3) The name, address, and procedures for contacting the facility's	Section I, 1.2.4 Section II, 1.1.2		
	owner or operator on a 24-hour basis.	3ection, 1.2.4 3ection 1, 1.1.2		
	(4) A table of contents.	TOC		
	(5) During the period that the submitted plan does not have to	Section III Annex 8.5		
	conform to the format contained in this subpart, a cross index, if	Codion in famox c.c		
	appropriate.			
	(6) A record of change(s) to record information on plan updates.	Section III Annex 6.2		
(b)	Emergency Response Action Plan. This section of the plan must be			
	organized in the subsections described in this paragraph:			
	(1) Notification procedures. (i) This subsection must contain a	Section II Core Plan, 1.1.2 and 1.1.3;		
	prioritized list identifying the person(s), including name, telephone	Section III Annex 2.1		
	number, and their role in the plan, to be notified of a discharge or			
	substantial threat of a discharge of oil. The telephone number	·		
	need not be provided if it is listed separately in the list of contacts required in the plan. This Notification Procedures listing must			
	include			
	(A) Facility response personnel, the spill management team, oil	Section III Core Plan, 1.1.2		
	spill removal organizations, and the qualified individual(s) and			
	the designated alternate(s); and	<u>'</u>		
	(B) Federal, State, or local agencies, as required.	Section II Core Plan, 1.1.2		
	(ii) This subsection must include a form,, which contains	Section II Core Plan, 1.1.3		
	information to be provided in the initial and follow-up			
	notifications to Federal, State, and local agencies.			
ı	(2) Facility's spill mitigation procedures. (i) This subsection must describe the volume(s) and oil groups that would be involved in			
	the			
	(A) Average most probable discharge from the MTR facility;	Section II Core Plan, 1.1.7.4		
	(B) Maximum most probable discharge from the MTR facility;	Section II Core Plan, 1.1.7.4		
	(C) Worst case discharge from the MTR facility; and	Section II Core Plan, 1.1.7.4		
	(D) Where applicable, the worst case discharge from the non-	Section II Core Plan, 1.1.7.4		
	transportation-related facility. This must be the same volume	•		
	provided in the response plan for the non-transportation-			
	related facility.			
	(ii) This subsection must contain prioritized procedures for			
	facility personnel to mitigate or prevent any discharge or			
	substantial threat of a discharge of oil resulting from			
	operational activities associated with internal or external			
	facility transfers including specific procedures to shut down affected operations. Facility personnel responsible	,		
	for performing specified procedures to mitigate or			
	prevent any discharge or potential discharge shall be			
	identified by job title. A copy of these procedures shall be			
	maintained at the facility operations center. These			
	procedures must address actions to be taken by facility			
	personnel in the event of a discharge, potential			
	discharge, or emergency involving the following	·		
	equipment and scenarios:			

### 8.5......USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030 and 33 CFR §154.1035) Final Rules (Cont'd)

CFR 3194.1003	(Cont'd)	LOCATION
	<ul> <li>(A) Failure of manifold, mechanical loading arm, other transfer equipment, or hoses, as appropriate;</li> </ul>	Section II Core Plan, 1.1.7.5
	(B) Tank overfill;	Section II Core Plan, 1.1.7.6
	(C) Tank failure;	Section II Core Plan, 1.1.7.7
	(D) Piping rupture;	Section II Core Plan, 1.1.7.8
	(E) Piping leak, both under pressure and not under	Section II Core Plan, 1.1.7.9
	pressure, if applicable;	,
	(F) Explosion or fire; and	Section Il Core Plan, 1.1.7.10
	(G) Equipment failure (e.g. pumping system failure, relief	Section II Core Plan, 1.1.7.5 thru
	valve failure, or other general equipment relevant to	1.1.7.10
•	operational activities associated with internal or	•
	external facility transfers.)	
	(iii) This subsection must contain a listing of equipment and	Section II Core Plan, 1.1.7
	the responsibilities of facility personnel to mitigate an	·
	average most probable discharge.	
(3) Fac	ility's response activities. (i) This subsection must contain a	Section II Core Plan, 1.1.7; Section
des	cription of the facility personnel's responsibilities to initiate a	III Annex 3.a.1 and Annex 3.b.1
resp	onse and supervise response resources pending the arrival of	
	qualified individual.	
(ii)	This subsection must contain a description of the	Section III Annex 3.b.1
	responsibilities and authority of the qualified individual and	
	alternate as required in § 154.1026.	
(iii)	This subsection must describe the organizational structure	Section III Annex 3.a.6
	that will be used to manage the response actions. This	
	structure must include the following functional areas.	
	(A) Command and control;	Section III Annex 3.b.1
	(B) Public information;	Section III Annex 3.b.2
	(C) Safety;	Section III Annex 3.b.3
	(D) Liaison with government agencies;	Section III Annex 3.b.4
	(E) Spill Operations;	Section III Annex 3c
	(F) Planning;	Section III Annex 3d
	(G) Logistics support; and	Section III Annex 3e
	(H) Finance.	Section III Annex 3f
(iv)	This subsection must identify the oil spill removal	M
	organizations and the spill management team to:	
	(A) Be capable of providing the following response	
	resources:	
	(1) Equipment and supplies to meet the requirements of	Section II Core Plan, 1.1.2, 1.1.4.1,
•	§§ 154.1045, 154.1047 or subparts H or I of this	1.1.4.3 and 1.1.7
	part, as appropriate; and	
	(2) Trained personnel necessary to continue operation	Section II Core Plan 1.1.7; Section III
	of the equipment and staff of the oil spill removal	Annex 11.1
	organization and spill management team for the first	
	7 days of the response.	
	(B) This section must include job descriptions for each spill	Section III Annex 3a thru 3f
	management team member within the organizational	
	structure described in paragraph (b)(3)(iii) of this section.	
	These job descriptions should include the responsibilities	·
	and duties of each spill management team member in a	
	response action.	
(v)	For mobile facilities that operate in more than one COTP	N/A
	zone, the plan must identify the oil spill removal organization	· · · · · · · · · · · · · · · · · · ·
• •	and the spill management team in the applicable geographic-	
	specific appendix. The oil spill removal organization(s) and	
	specific appendix. The oil spill removal organization(s) and the spill management team discussed in paragraph	
	specific appendix. The oil spill removal organization(s) and	

# 8.5 ......USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030 and 33 CFR §154.1035) Final Rules (Cont'd)

CFR §154:1035 (Cont:d)	LOCATION
(4) Fish and wildlife and sensitive environments. (i) This section of the plan must identify areas of economic importance and environmental sensitivity, as identified in the ACP, which are	Section III Annex 1, Fig 1.5; Annex 3.d.1 and 3.d.3
potentially impacted by a worst case discharge. ACPs are required under section 311(j)(4) of the FWPCA to identify fish and wildlife and sensitive environments. The applicable ACP shall be	
used to designate fish and wildlife and sensitive environments in the plan. Changes to the ACP regarding fish and wildlife and sensitive environments shall be included in the annual update of	
the response plan, when available.  (ii) For a worst case discharge from the facility, this section of the plan must	
(A) List all fish and wildlife and sensitive environments identified in the ACP which are potentially impacted by a discharge of persistent oils, non-persistent oils, or non-petroleum oils.	Section III Annex 1, Fig 1.5; Annex 3.d.1
(B) Describe all the response actions that the facility anticipates taking to protect these fish and wildlife and sensitive environments.	Section III Annex 3.d.3
(C) Contain a map or chart showing the location of those fish and wildlife and sensitive environments which are potentially impacted. The map or chart shall also depict each response action that the facility anticipates taking to protect these areas. A legend of activities must be included on the map page.	Section fil Annex 1, Fig 1.5
(iii) For a worst case discharge, this section must identify appropriate equipment and required personnel, available by contract or other approved means as described in § 154.1028, to protect fish and wildlife and sensitive environments which fall within the distances calculated using the methods outlined in this paragraph as follows:	
(A) Identify the appropriate equipment and required personnel to protect all fish and wildlife and sensitive.	Section III Annex 3.d.3.3
environments in the ACP for the distances, as calculated in paragraph (b)(4)(iii)(B) of this section, that the persistent oils, non-persistent oils, or non-petroleum oils are likely to travel in the noted geographic area(s) and number of days listed in Table 2 of appendix C of this part;	
(B) Calculate the distances required by paragraph (b)(4)(ii)(A) of this section by selecting one of the methods described in this paragraph;	
(1) Distances may be calculated as follows:	
(i) For persistent oils and non-petroleum oils discharged into non-tidal waters, the distance from the facility reached in 48 hours at maximum current.	N/A
(ii) For persistent and non-petroleum oils discharged into tidal waters, 15 miles from the facility down current during ebb tide and to the point of maximum tidal influence or 15 miles, whichever is less, during flood tide.	N/A
(iii) For non-persistent oils discharged into non-tidal waters, the distance from the facility reached in 24 hours at maximum current.	N/A
(iv) For non-persistent oils discharged into tidal waters, 5 miles from the facility down current during ebb tide and to the point of maximum tidal influence or 5 miles, whichever is less, during flood tide.	Section III Annex 3.d.1

# 8.5 ..........USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030 and 33 CFR §154.1035) Final Rules (Cont'd)

CFR	§154.1035 (Cont'd)	LOCATION
	(2) A spill trajectory or model may be substituted for the distances calculated under paragraph (b)(4)(iii)(B)(I) of this section. The spill trajectory or model must be acceptable to the COTP.	N/A
	(3) The procedures contained in the Environmental Protection's Agency's regulations on oil pollution prevention for non-transportation-related onshore facilities at 40 CFR part 112, appendix C, Attachment C-III may be substituted for the	N/A
	distances listed in non-tidal and tidal waters; and	
	(C) Based on historical information or a spill trajectory or model, the COTP may require the additional fish and wildlife and sensitive environments also be protected.	•
	(5) Disposal Plan. This subsection must describe any actions to be taken or procedures to be used to ensure that all recovered oil and oil contaminated debris produced as a result of any discharge are disposed according to Federal, state, or local requirements.	Section III Annex 3.d.6
(c)	Training and exercises. This section must be divided into the following two subsections:	
	(1) Training procedures. This subsection must describe the training procedures and programs of the facility owner or operator to meet the requirements in § 154.1050.	Section III Annex 5.2
	(2) Exercise procedures. This subsection must describe the exercise program to be carried out by the facility owner or operator to meet the requirements in § 154.1055.	Section III Annex 5.1
(d)	Plan review and update procedures. This section must address the procedures to be followed by the facility owner or operator to meet the requirements of § 154.1065 and the procedures to be followed for any post-discharge review of the plan to evaluate and validate its effectiveness.	Section III Annex 6
(e)	Appendices. This section of the response plan must include the appendices described in this paragraph.	
	<ol> <li>Facility-specific information. This appendix must contain a description of the facility's principal characteristics.</li> </ol>	пана
	(i) There must be a physical description of the facility including a plan of the facility showing the mooring areas, transfer locations, control stations, locations of safety equipment, and the location and capacities of all piping and storage tanks.	Section III Annex 1, Fig 1.2
	(ii) The appendix must identify the sizes, types, and number of vessels that the facility can transfer oil to or from simultaneously.	Section I, 1.2.7
	(iii) The appendix must identify the first valve(s) on facility piping separating the transportation-related portion of the facility from the non-transportation-related portion of the facility, if any. For piping leading to a manifold located on a dock serving tank vessels, this valve is the first valve inside the secondary containment required by 40 CFR part 112.	Section III Annex 1, Fig 1.2
	(iv) The appendix must contain information on the oil(s) and hazardous material handled, stored, or transported at the facility in bulk. A material safety data sheet meeting the requirements of 29 CFR 1910.1200, 33 CFR 154.310(a)(5) or an equivalent will meet this requirement. This information can be maintained separately providing it is readily available and the appendix identifies its location. This information must include	Section III Annex 11.3

# 8.5 ............ USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030 and 33 CFR §154.1035) Final Rules (Cont'd)

CFR §154.1035 (Cont'd)		LOCATION
(A) The generic or chemical name;		Section III Annex 11.3
(B) A description of the appearance a	and odor;	Section III Annex 11.3
(C) The physical and chemical chara	cteristics;	Section III Annex 11.3
(D) The hazards involved in ha hazardous materials. This shall in the coll(s) are come in contact as a result of a d	nclude hazards likely to nd hazardous materials ischarge; and	Section III Annex 11.3
(E) A list of firefighting procedures a effective with fires involving th materials.	e oil(s) and hazardous	Section III Annex 11.3
<ul><li>(v) The appendix may contain any other facility owner or operator determines spill response.</li></ul>	to be pertinent to an oil	Section III Annex 11
(2) List of contacts. This appendix must inc hour contact of key individuals and appropriate, this information may be specific appendix. The list must include	organizations. If more	
(i) The primary and alternate qualifie facility;	. ,	Section II Core Plan, 1.1.2
(ii) The contact(s) identified under para section for activation of the response	resources; and	Section II Core Plan, 1.1.2
(iii) Appropriate Federal, State, and local		Section II Core Plan, 1.1.2
<ul> <li>(3) Equipment list and records. This appering information specified in this paragraph.</li> </ul>	ndix must include the	
(i) The appendix must contain a list of personnel required to respond to an discharge, as defined in § 154.1020. list the location of the equipment.	average most probable	ection II Core Plan, 1.1.4 and 1.1.7
(ii) The appendix must contain a detaile equipment identified in the plan as removal organization(s) that is availa approved means as described in § to a maximum most probable or we defined in § 154.1020. The detail equipment may be located in referenced by the plan. Either the approved in the plan must the major response equipment.	pelonging to an oil spill ole, by contract or other 154.1028(a), to respond orst case discharge, as ed listing of all major a separate document opendix or the separate	N/A
(iii) It is not necessary to list response removal organization(s) when the classified by the Coast Guard and to determined to equal or exceed it needed by the facility. For oil spill classified by the Coast Guard, the noted in this section of the plan. Whe appendix to contain a listing of responding all of the following items the response plan: Skimmers; booms; districtly burning, bioremediation equipment used to apply other NCP Product Schedule (if applications) and beach cleaning equipment; and list must include for each piece of equipment and the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the plan. When the section of the plan when the section of the section of the plan when the section of the plan when the section of the plan when the section of the section of the plan when the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section of the section o	organization has been heir capacity has been he response capability removal organization(s) classification must be n it is necessary for the onse equipment, it shall at are identified in the spersant application, intent and supplies, and chemical agents on the able); communications, ment; boats and motors; heavy equipment. The	ection II Core Plan, 1.1.2; Section II Annex 11.1

## 8.5 ..........USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030 and 33 CFR §154.1035) Final Rules (Cont'd)

CFR §154,1035 (Cont'd)	LOCATION
(A) The type, make, model, and year of manufacture listed on the nameplate of the equipment;	
<ul> <li>(B) For oil recovery devices, the effective daily recovery rate, as determined using section 6 of Appendix C of this part;</li> </ul>	
(C) For containment boom, the overall boom height (draft and freeboard) and type of end connectors;	N/A
<ul> <li>(D) The spill scenario in which the equipment will be used for or which it is contracted;</li> </ul>	N/A
<ul> <li>(E) The total daily capacity for storage and disposal of recovered oil;</li> </ul>	N/A
(F) For communication equipment, the type and amount of equipment intended for use during response activities. Where applicable, the primary and secondary radio frequencies must be specified.	. \
(G) Location of the equipment; and	N/A
<ul> <li>(H) The date of the last inspection by the oil spill removal organization(s).</li> </ul>	N/A
(4) Communications plan. This appendix must describe the primary and alternate method of communication during discharges, including communications at the facility and at remote locations within the areas covered by the response plan. The appendix may refer to additional communications packages provided by the oil spill removal organization. This may reference another existing plan or document.	
(5) Site-specific safety and health plan. This appendix must describe the safety and health plan to be implemented for any response location(s). It must provide as much detailed information as is practicable in advance of an actual discharge. This appendix may reference another existing plan requiring under 29 CFR 1910.120.	
(6) List of acronyms and definitions. This appendix must list all acronyms used in the response plan including any terms or acronyms used by Federal, State, or local governments and any operational terms commonly used at the facility. This appendix must include all definitions that are critical to understanding the response plan.	

# 8.5 .......USCG Cross Reference for OPA 90 Plan (33 CFR §154.1030 and 33 CFR §154.1035, §154.1050, §154.1055) (Cont'd)

§ 154.1050	DESCRIPTION OF GUIDELINE ITEM	SECTION
(a)	must identify the training to be provided to each individual with responsibilities under the plan.	Annex 5
(b)	A facility owner or operator shall ensure the maintenance of records sufficient to document training of facility personnel	Annex 5.2
(c)	Where applicable, a facility owner or operator shall ensure that an oil spill removal organization identified in a response plan to meet the requirements of this subpart maintain records sufficient to document training	Annex 5.1.1
(d)	The facility owner or operator remains responsible for ensuring that all private response personnel are trained to meet the Occupational Safety and Health Administration (OSHA) standards for emergency response operations in 29 CFR 1910.120.	Introduction 1.1
§ 154.1055	DESCRIPTION OF GUIDELINE ITEM	SECTION
(a)(1)	Qualified individual notification exercises	Annex 5
(a)(2)	Spill management team tabletop exercises	Annex 5
(a)(3)(i)	Equipment deployment exercisesfacility owned and operated.	Annex 5
(a)(3)(ii)	Equipment deployment exercisesoil spill removal organization equipment.	Annex 5
(a)(4)	Emergency procedures exercises (optional)	Alexander of the

### ANNEX 9.... COMPANY EMERGENCY PLAN AND REPORTING PROCEDURES

### 9.1..... CORPORATE EMERGENCY REPORTING

#### 9.1.1..... Guidelines

Houston Office personnel and appropriate affiliates are to be promptly notified and be kept informed of unusual events and reportable incidents occurring at our marketing facilities or involving Motiva owned product or property handled or operated by others. This procedure must be carefully followed to ensure that Headquarters personnel receive the required information. Information on how to effectively communicate with the news media during an emergency situation is provided in Annex 3.b.2.

### 9.1.2..... Reporting Incidents Internally

To report incidents internally, take the following actions:

1. If the situation warrants potential use of resources from Emergency Management, Preparedness, and Response (EMP&R), call their 24 hr. hotline immediately at (877) 242-7400 to report incidents. When notification is made to or assistance is requested from Emergency Management, Preparedness, and Response (EMP&R), notification information should be documented on the EMP&R Notification Log.

Collect the information requested on the Spill Response Notification Form (located in the Core Plan) prior to calling the Emergency Management, Preparedness, and Response Team.

- 2. Contact the Regional Manager and the Manager, LSDR/HSE and Emergency Management within 24 hours (7 days a week).
- 3. If the reportable event involves a spill or an impact to the community, a written event investigation report (Investigation Report*) will be provided, within 10 calendar days, to the Regional Manager and the Manager, LSDR/HSE and Emergency Management.

*NOTE: Exceptions to the Investigation Report will be made for sensitive matters which may need to be investigated under the attorney-client work product privilege. Contact Legal immediately where circumstances warrant. Advise the above contacts accordingly. On rare occasions an incident (e.g., certain process safety incidents) may require additional time to complete the investigation. The Manager, LSDR/HSE and Emergency Management is authorized to extend the reporting requirements where appropriate.

The event Investigation Report should address the facts of the matter and specifically discuss what preventative steps will be taken to help prevent a similar occurrence. The report should provide sufficient detail to enable others to learn from the experience.

Other reportable environmental events will not require a written followup report unless specifically requested.

- 4. For environmental incidents that are reportable to the National Response Center (NRC) pursuant to various federal laws, notify NRC at 1-800-424-8802 upon discovery of the environmental incident. If required by law, you must also contact local and State agencies in a timely manner to report certain environmental incidents.
- 5. Fatalities or incidents resulting in the hospitalization of three (3) or more Motiva employees must be initially reported orally by telephone or in person to the nearest OSHA area office within eight hours. Facilities can either call the nearest OSHA area office or call the OSHA 24-hour toll free telephone number at 1-800-321-OSHA (6742). The report must relate the circumstances of the accident, the number of fatalities and hospitalizations, and the extent of any injuries. The OSHA area director may require additional reports, in writing or otherwise, concerning the accident. Although the regulation does not require the employer to confirm in writing the oral or in person report to OSHA, Motiva facilities should work with the Motiva Legal Department to prepare a confirmation letter to send to OSHA.

# 9.1.3..... Incident Investigation

Investigation of incidents qualifying for emergency reporting should be coordinated with the Law Department. Do not delay required regulatory or insurance company reporting.

Subject to the requirement to coordinate incident investigations with the Law Department for environmental incidents, injury accidents, and property damage / product loss, a full Incident Report detailing the known factors, confirmed causes, costs, and actions taken to address the incident must be submitted to the Houston Office within ten (10) working days of the start date of an incident investigation that does not require any testing, sampling, or other activities that require more than 10 working days to complete. For incident investigations that require testing, sampling, or other activities that cannot reasonably be completed in ten (10) working days, the incident report must be submitted within thirty (30) working days of the start of date of the incident.

#### 9.1.3.1 .... Environmental

Environmental incidents should be reported if any one of the following conditions is present:

- 1. Any spill, discharge, or migration that threatens significant ecological damage or poses a threat to employee or public welfare.
- Any incident that may have serious legal repercussions, such as the threat of legal action against the Company or an employee, the imposition of a significant penalty, or cleanup operations being taken over by a governing agency.
- Any significant or potential side effects such as hazardous materials, petroleum products, or chemicals reaching a drinking water source, entering a public sewer system, or entering into basements of buildings or homes.
- 4. Any significant public reaction or news media coverage which has or may reflect on the Company's reputation.

## 9.1.3.2 .... Accidents, Property Damage, Security, and Unfavorable Publicity

The following incidents should be reported:

Injury accidents (employees, contractors, or third parties) requiring hospitalization or a fatality.

Property damage, product loss, or other unusual happening (fires, explosions, power failures) where the losses or costs are expected to exceed \$50,000.

Any act of criminal violence resulting in serious injury or fatality, bomb threats, death threats, group demonstrations, wildcat strikes, or unexpected picketing, whether actual, threatened or potential, that could impact on Company operations, facilities, or personnel.

Any incident or event likely to result in significant unfavorable public reaction or news media coverage that is not covered within other categories.

## 9.1.4 ...... Handling the News Media

Motiva seeks to be a cooperative, forthright, and a responsible corporate citizen. In keeping with this, it is our goal to keep the public informed in the event of an emergency involving the safety of individuals or property.

9.2ENIPAR NOTIFICATION LOG	
Person on the EMP&R staff to whom you rela	ayed this emergency information:
Name: Phone:() Time:: AM or PM (circle or	ne) Time Zone: EST or CST
Document any calls or actions that you ta (including calls where you leave a message)	
Follow-up call:	Time Called:
Follow-up call:	Time Called:
·	
Follow-up call:	Time Called:
	· · · · · · · · · · · · · · · · · · ·
Follow-up call:	Time Called:
1 Onow up can.	Time odilod.

#### 9.3 .....LOCAL EMERGENCY PLAN

#### 9.3.1 ......General Emergencies and Disasters

#### 9.3.1.1 .... Introduction

The objective of this Plan is to prepare for a general emergency and in so doing provide for the safety of Company personnel, protect Company property, and maintain the ability to continue operations.

#### 9.3.1.2 .... Authority to Activate Plan

This Plan may be activated by the designated Qualified Individual or the designated Alternate Qualified Individual. The individual activating the Plan shall assume responsibility for its complete execution until such time as relieved by higher authority.

#### 9.3.1.3. ... Emergency Agencies and Control Center

When deemed necessary, persons listed on the emergency notification phone list (Core Plan 1.1.2) may be summoned.

#### 9.3.2 ..... Natural Disasters

#### 9.3.2.1 .... Floods

Floods may result from an unusually heavy rain following a long period of wet weather or a sudden spring thaw with, or without, rainfall. They may be caused by hurricanes with heavy rainfall and exceptionally high tides in coastal areas. Tidal waves may also flood coastal areas or areas adjacent to large inland lakes. Generally, there is ample advance warning of these conditions and as warranted, the following preparations should be considered:

- 1. Disconnect the main electrical switch, shut the main valve in the gas service line and water line, if any. Determine whether connections on sanitary sewer would be blocked to prevent back up (storm sewer drains should not be blocked).
- Clear the yard of all loose items that could float away. Store empty drums inside a building and secure them against floating. Underground tanks in yard storage should be filled with water or otherwise anchored to prevent floating and sealed to prevent product or other contaminate from escaping.
- 3. Store carton packages above anticipated flood level or remove them to a safe place.
- 4. Remove motors and other electrical equipment and store them above anticipated flood level.

- 5. Remove automotive equipment, including forklift trucks and other motorized portable equipment, to a safe place.
- 6. Make sure that vertical tanks and large pipelines (8" and over) are filled, preferably with product. Safety requires maintaining the product level in the tanks at least 10" above the highest anticipated flood level. If sufficient product is not available, water should be used. However, water should be admitted to the tanks and lines only as a last resort, and only in sufficient quantities to keep ahead of the flood rise. Horizontal tanks that would be below flood-water level should be filled an anchored.
- 7. Close and lock product line valves.
- 8. Consideration should also be given to protection of Company funds and records. If deemed necessary on account of expected high water, valuable papers and funds should be removed from the safe to be stored elsewhere for safekeeping.
- 9. If possible, file cabinets should be elevated to a height above the expected flood level. If this is not possible, the contents of the file drawers that are subject to flood damage should be removed, tied securely in bundles and stored temporarily at a height above the expected high water level. In the same manner, see that correspondence and records in desk drawers are removed if in danger of loss or damage.
- 10. Pump out the oil collection compartment of open-top oil / water separators so flood waters do not impact the compartment causing a release to the lands or waters.

#### 9.3.2.2 .... Hurricanes

in the event of an approaching hurricane, the following precautions should be taken:

- 1. Clear the yard area of all loose items, empty drums, etc., that blow around and cause further damage.
- 2. Close all doors and windows.
- 3. Tape and / or board up windows and brace large windows.
- 4. Brace all large outside doors securely.
- 5. Small diameter (10' to 12') vertical or horizontal tanks should be at least half filled with product. If product is low, water should be added, only as a last resort.

6. Take precautions as listed above for impending flood if hurricane warnings indicate this emergency.

#### 9.3.2.3.... Tornadoes

Generally, there is little warning of tornado conditions, from 15 minutes to an hour and a half. However, insofar as time permits, the same preparation should be made as indicated above for hurricanes, giving preference in the order listed. A tornado may follow a period of intense ground heat. The first indication of its approach may be a combination of thick dark storm clouds and heavy rainfall or hail. When such signs appear in tornado areas, it is important to maintain contact with local weather reporting agencies.

#### 9.3.2.4....Earthquakes

Brooklyn is in Zone 2 - Moderate Damage Area.

#### 9.3.2.5.... Cleanup

After any emergency has passed, facilities should be returned to operating condition as soon as possible. However, in doing so, certain precautions should be observed:

- Do not touch loose wires under any circumstances until they have been checked out by a qualified electrician. They may be electrically charged.
- 2. Do not turn on main electrical switch until the entire system has been checked out (if any part was flooded) by a qualified electrician.
- 3. Do not operate any electrical equipment until thoroughly dried out and checked (if flooded) by a qualified electrician.
- 4. Check thoroughly all product lines and tanks for leaks or any other evidence of damage.
- 5. Check entire Facility for possible damage.
- 6. Prepare accident report, if necessary.

#### 9.3.3..... Media

All contact with the press or other media will be made by the Complex Manager or a Motiva Communications Representative listed in the Core Plan. All contacts should adhere to the Company's public policy statements and follow existing guidelines.

#### 9.3.4..... Emergency Oversight

When this Plan is activated, the Complex Manager will direct all "outside" activities and all "inside" activities. Those handling administrative duties will stand ready to secure and protect the Company funds and records, and stand ready to assist as directed by the Complex Manager. The Terminal Operator on duty will act as telephone coordinator and liaison with Emergency Agencies.

#### 9.3.5..... First Aid

Local Emergency Medical Services will be contacted by calling 911. If required, a First Aid Station will be established in the Terminal Office.

#### 9.3.6..... Special Matters

#### 9.3.6.1.... Criminal Complaints and Arrests

Under long-standing Company policy no employee, on behalf of the Company, may sign a criminal complaint, institute a criminal action or cause the arrest of anyone unless prior approval of the Legal Department has been obtained. Of course, if a Federal or State Law Enforcement officer desires to sign the complaint or file charges in accordance with his statutory authority and duty, he should be encouraged to do so.

#### 9.3.6.2.... Subsequent Investigations

All contacts with investigating authorities during their subsequent investigations of these types of emergencies should be made only through the Company's Security Representatives. Therefore, any inquiries made by public authorities in connection with any post investigations should be referred to them. However, personnel should cooperate in developing for the Security Representatives any information they may deem to be desirable to furnish the investigating authorities.

#### 9.3.6.3.... Conduct of Employees

Emphasis should always be on the side of preventing undesirable publicity; and, except in self-defense:

# NO PHYSICAL FORCE SHOULD BE USED AGAINST OTHER PERSONS AT ANY TIME!!

**QUESTIONS TO ASK** 

Annex 9, Page 9

# 9.3.6.4.... Bomb Threat Checklist

Name Of Person Receivin	g Threat Phone No.	ŝ
		8
Date Threat Received	Time Threat Received Reported To: Phone No.	ā
		å

**EXACT WORDING OF THREAT** 

	ib going to explode? now?			
3. What does it look	k like?			· .
4. What kind of bon				
5. What will cause i	t to explode?			
6. Did you place the	e bomb?			
7. Why?	W			
8. What is your nan	ne?			······
9. What is your add	lress and phone?	, , , , , , , , , , , , , , , , , , ,		
The following r	equite opinions, percep	ions and judgments. Ple	ase give your first impres	sion.
Caller was:	[ ] Male	[] Female	[ ] Adult [ ]	Child
Estimated age:	[3] Pre-teen	[] Teenage	[1] 20-40 - [1]	Other
Caller's Speech:	Accent:	[] Heavy	[ ] Slight   [ ]	Other
	[s] Spanish	ு.[∦].:German,	[3] German (-1)	Other .
	. [ ] Southern	[ ] Northern	[ ] New York [ ]	Other
Caller's Voice:	[a] Fast	[ ] Slow	[引 Excited [ [-]	Angry
	[.] Slurred i	[ ] Quite	[	Slang
	[ ] Impediment	1.] Well Spoken, s	هٔ: [۱] Other	
Background Sound:	[ˈ] Animals 🖺	[ ] Railroad	[] Aircraft []	Street
	[ ] Other (describe			

#### 9.4..... DEMONSTRATIONS

#### 9.4.1..... Introduction

Security procedures to be activated in respect to demonstrations have three objectives:

- 1. Protection of Company employees and property.
- 2. Protection of business visitors and their property.
- 3. Continuity of operations.

In the Company's performance of service to the public, constructive communications are encouraged, but communications which take the form of group demonstrations conducted on Company property not only are not constructive but pose a serious threat to the personal safety of employees and probable harm to Company property.

Since these demonstrations could come at any time, with or without warning, to effectively cope with such an emergency, a threat plan of action for each Company facility must be placed in readiness. Guidelines for the development of a plan to meet this type of emergency, including an outline of the actions to be taken, are set out below.

#### 9.4.2..... Authority to Activate Plan

This Plan may be activated by the designated Qualified Individual or the designated Alternate Qualified Individual.

The individual placing the Plan into effect will remain responsible for all activity until relieved by higher authority. Exercising good judgment and without over-reacting, the individual activating the Plan will take all measures necessary to accomplish the three objectives first mentioned.

The highest local authority present, or the Complex Manager if present, will act as Company spokesperson in the event a meeting with the demonstrators is indicated. He / she shall be familiar with Company's public policy statements and the Emergency Reporting Procedures.

The highest local authority present, the Complex Manager or the Motiva Enterprises LLC Communications Representative, will act as spokesperson with the media.

#### 9.4.3..... Emergency Agencies

When deemed necessary, persons listed on the emergency notification phone list (Core Plan, Section 1.1.2) may be summoned.

#### 9.4.4..... Notification

Any individual observing or receiving notice, verbal or written, of an actual or proposed demonstration shall immediately notify the QI/AQI or the Senior Terminal Operator.

If received or noted after hours, and after consideration of first protecting Company employees and forestalling damage to property, every effort will be made to notify the above by telephone.

All employees in the Facility will be notified in person of what action is being taken and what countermeasures, if any, should be taken. If it becomes necessary to evacuate the Facility, a communications post will be established by the Complex Manager and employees may call there for current instructions.

A Control Center will be established in the Terminal Office, if possible. All activities will be directed by the senior person in charge from the Control Center.

#### 9.4.5..... Action Steps

#### 9.4.5.1.... Entrances

If time allows, all entrances to the Facility, except one, should be locked or blocked so that the demonstrators will be required to enter through only one door. However, predesignated personnel with keys should be posted at all such locked entrances so that all doors may be quickly opened if personnel evacuation becomes necessary.

#### 9.4.5.2... Dangerous Materials

Gates to all fenced areas should be locked and employees positioned where they can warn of points where flammable or other dangerous materials are kept.

#### 9.4.5.3.... Alerting Personnel

All personnel in the Facility should be alerted and kept advised of all developments by the communication means set out in the Plan.

#### 9.4.5.4.... Restricted Areas

Company and other selected personnel will be stationed at every building door, entrance / exit gate, and the truck loading rack (if remote from the office) and advise non-employees that the area is not open to the public. However, no physical force should be used to restrain or resist outsiders.

#### 9.4.5.5.... Files and Desks

If it appears that the protest or demonstration may become unruly or access to restricted areas may be attempted, all desks should be cleared and all desks, files and cabinets locked as directed by the person in charge.

#### 9.4.5.6.... Fire Equipment

Personnel shall be prepared to take up positions where they will be able to readily man hand held fire equipment only. If necessary, the local Fire Department will be summoned by calling 911 by Facility personnel, as directed by the Fire Emergency Plan.

#### 9.4.5.7.... First Aid

Local Emergency Medical Services will be contacted by calling 911. If required, a First Aid Station will be established in the Terminal Office.

#### 9.4.6...... Instructions for Contact with Demonstrators

#### 9.4.6.1.... Clarification

At the outset, the exact reason for and purpose of the groups visit should be requested and such information conveyed immediately to the person in charge.

## 9.4.6.2.... Restrict to Lobby

Efforts should be made to keep demonstrators outside of the Facility or, if they gain entrance, in the lobby or reception area - but by request only. Do not attempt to use force.

#### 9.4.6.3.... Heckling

Do not debate with, taunt, heckle or harass protesters in any manner.

#### 9.4.6.4.... Group Representatives

If possible, the group should be persuaded to designate one (or only a few) person to represent it and it should be suggested that the meeting be held in a separate closed room.

#### 9.4.6.5.... Spokesperson Conduct

The Company spokesperson should always be accompanied by at least two other Company employees (if available), should decline to have his or her conversation recorded, should not pose for pictures, and should not express personal opinions. However, NO attempt to confiscate cameras, film, recorders or any personal articles should be made. The spokesperson should listen courteously, engage in no debate, and answer questions only in terms of authorized Company statements. NO MORE.

#### 9.4.6.6.... Unruly Demonstrations

If the demonstration becomes disruptive or if the group refuses to leave after the Company spokesperson considers the interview at an end, the police should be summoned to the Facility. The Company employee in charge of the emergency should then decide whether the disruptive actions are of such severity as to warrant a request for removal by the police.

#### 9.4.6.7.... Evacuation

If demonstrators begin to intentionally damage or destroy Company property, Company personnel are to be immediately evacuated from the affected area and police action should be immediately requested to protect persons and property.

#### 9.4.6.8.... Criminal Complaints and Arrests

Under a long-standing Company policy, no employee, on behalf of the Company, may sign a criminal complaint, institute a criminal action or cause the arrest of anyone unless prior approval of the Legal Department is obtained. Of course, if a Federal or State Law Enforcement Officer desires to sign the complaint or file charges in accordance with his statutory authority and duty, he should be encouraged to do so.

#### 9.4.6.9.... Restraint by Employees

Emphasis should always be on the side of avoiding provocation or disturbance and preventing undesirable publicity. Except when self-defense becomes necessary, NO PHYSICAL FORCE SHOULD BE USED BY EMPLOYEES AT ANY TIME.

COMMON SENSE, CALMNESS AND DISCRETION SHOULD PREVAIL
AT ALL TIMES!!

#### 9.5..... FIRE EMERGENCY PLAN

#### 9.5.1..... Introduction

The objective of this Plan is to prepare for a fire emergency and in so doing, provide for the safety of Company personnel, protect Company property, and maintain the ability to continue operations.

Facility personnel will take no action or risk to themselves or other to fight a fire, except when the fire is in the incipient stages where hand-held fire extinguishers may be used by Facility personnel.

Facility personnel will not endanger themselves or others in any way.

No employee shall enter a burning building to fight a fire.

#### 9.5.2..... Authority to Activate Plan

This Plan may be activated by the designated Qualified Individual, the designated Alternate Qualified Individual or any other Facility employee. The individual activating the Plan shall assume responsibility for its complete execution until such time as relieved by higher authority.

#### 9.5.3...... Emergency Agencies and Control Center

When deemed necessary, persons listed on the emergency notification phone list (Core Plan, Section 1.1.2) may be summoned.

#### 9.5.4.....In the Event of a Fire

The person observing the fire will sound the nearest alarm and notify the Terminal Office to notify the local Fire Department by calling 911.

All truck loading at the truck loading rack will cease.

Facility personnel will direct the evacuation of all trucks to a safe location outside of the Facility facility. All drivers will remain with their trucks. If starting vehicles will present an ignition hazard, vehicles will not be moved.

If the fire is at the truck loading rack, Facility personnel will stand by the foam system control actuator and initialize the foam system if the automatic system for the loading rack should fail.

If a Facility employee is on duty, providing that it is safe to do so, a Facility employee will close all tank and pipeline valves and shut off all power to the product pumps.

Facility personnel will ensure that all of the entrance / exit gates are open for emergency vehicles.

Facility personnel, as may be available, will be assigned to the entrance / exit gates to deny access to anyone other that emergency vehicles (Police, Fire, and Ambulance). Without placing themselves in danger, Facility employees may assist emergency response vehicles stopping traffic on East Avenue to allow entrance / exit of trucks and emergency vehicles to / from the Facility.

All non-Company personnel will be directed to leave the Facility taking their personal vehicles with them, if safe to do so.

Facility personnel and / or selected individuals arriving at or returning to the Facility will report to the Qualified Individual for instructions. The QI will be the designated liaison with the Fire Department.

If possible, company funds and / or records will be secured or removed from the Facility to a safe location.

If possible, a Facility employee or selected individual will handle all telephone traffic.

#### 9.5.5.....Fire Evacuation Plan

A detailed Facility evacuation plan and Evacuation Diagram is located in the Core Plan and in Annex 1. The diagram depicts the location of the emergency evacuation routes, fire extinguishers, and fire alarm pull stations.

#### 9.5.6.....Fire Safety Equipment

#### 9.5.6.1.....Fire Alarm Switches

See diagrams in Annex 1.

#### 9.5.6.2....Truck Loading Rack Foam System

The truck loading rack is protected by a foam system that is activated automatically by fire sensor equipment located on the under side of the loading rack roof.

The truck loading rack foam system may be activated manually from the Terminal Operator's office or from the foam room.

#### 9.5.6.3.....Tank Farm Foam System

Each tank in the tank farm is protected by a foam system that is activated manually with zone control. To activate, the Operator must open the appropriate foam valve that corresponds to the tank and turn on the foam pump.

#### 9.5.6.4.....Portable Fire Extinguishers

Portable fire extinguishers are located at various locations throughout the Facility. A location listing is found in the Core Plan.

#### 9.5.6.5....Fire Blankets

There are fire blankets located on each lane of the loading rack, one at the pump off station, two in the shop and one in the warehouse.

#### 9.5.7 ...... Predetermined Reassembly Locations

If it becomes necessary to evacuate the Facility due to imminent danger, all Facility employees, contractors, drivers, and visitors will safely and quickly proceed to the "Fire Drill Area" located between the main office and warehouse. All employees and visitors will be accounted for by the designated person in charge. All employees and visitors will remain in this area until directed otherwise by the designated person in charge.

#### **COMMON SENSE SHOULD PREVAIL AT ALL TIMES**

#### BE CALM AT ALL TIMES - DO NOT RUN - DO NOT PANIC

Follow the instruction from the designated person in charge or from such civil authorities that are on the scene

# Environmental Compliance Report Major Petroleum Facility License No. 2-1540

Motiva Enterprises Brooklyn Terminal 25 Paidge Avenue Brooklyn, New York

October 2010

# SECTION A SPCC PLAN IMPLEMENTATION CHECKLIST

# **Environmental Compliance Report**

Regulations 40 CFF	<b>C112.</b>	compliance with certain ceed to Section D, Line 7		rements of F	ederal	
I. STATUS OF	SPCC PLAN (4	CFR 112.3).		Yes	No	
A. Is the Plan up	-to-date with con	tact persons?		X	·	
B. Has the Plan b		thin the past five years?		X, 2010		
Engineer	C. Has the Plan been reviewed and certified by a Professional Engineer, licensed and registered by the New York State Education Department?					
D. Has the Plan been approved and signed by management? X, 2010						
II. SPILL HIST Has there bee within the prinformation	e		Х			
Department Spill Number	Date	Material and Amount Spilled	Cause			
Not Applicable						
જારામાં આવ્યામાં ઓડા કરોક છે રાજ્યા છે. આ આવેલા માટે જે	over electrical conditions of Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 Section 2007 S		S.V.S.S.A.II	-0.00 millioner and on the control		
III. Modification	to the Facility	(40 CFR 112.5)		Yes	No	
A. Has there been a major change in the design, construction, operation or maintenance of the facility during the past five X years?						
licensed a	-	d by a Professional Engin the New York State Educ			X	
Date of major c	hanges: <u>Not Ap</u>	plicable				

		<u> </u>
B. Does the SPCC Plan or the Facility Response Plan contain:	Yes	No
(1) a written commitment by management to provide the	X	
necessary resources to implement the Plan?  (2) a written description of all spills and actions taken to prevent recurrence?	t X	
(3) an assessment of potential spills showing possible location, volume and direction of flow?	X	
<ul><li>(4) a description of the type of secondary containment needed to contain each spill?</li><li>If secondary containment is not provided, explain on a</li></ul>	X	
separate sheet how spills are prevented from reaching waters.		
	Not Applicable	e
IV. Drainage (40/CFR 112.7)		
A. Does the Plan discuss the following issues:		
(1) how drainage from the diked area is contained and released?	X	
(2) the use of drainage valves and how the valves are opened?	X	
(3) undiked system that is used to return a spill to the plant.  If so, does the plan discuss how this is accomplished?	X	·
(4) any diversion system that is used to return a spill to the	X	42.00.00 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.000 A 6.00
plant. If yes, does the plan discuss how this is accomplished?	X	
B. Does the facility have a SPDES Permit to release wastewater from the diked area? (A SPDES Permit is required to discharge wastewater.)	X	
C. Are wastewater discharges from treatment plants monitored to detect system upset?	X	
D. Are there written procedures for draining storm water from the diked area?	X	
(1) Are bypass values normally sealed closed?	X	
(2) When the bypass valve is open, is a supervisor present?	X Terminal Operator	
(3) Are records maintained for each drainage release?	X	

A. Is the petroleum being stored compatible with the material used to construct the tank ,ancillary equipment and secondary containment material?	X	
secondary contaminent material?	<b>A</b>	
he secondary containment system(s)meet the following reqm'ts?	Yes	Nö
International Building Codes	X	
Federal	X	
New York State	X	
County	X	
C. Are aboveground tanks in contact with soil protected from corrosion?	X	
D. Are underground tanks tested or have leak detection to insure that the tanks are not leaking?	X	
E. Are aboveground tanks internally inspected for structural integrity and to insure that they are not leaking?	X	
F. Have plans been implemented to prevent spills during transfers of petroleum products, including the use of:		X
(1) high level alarms and alarm pump shut off devices?	<b>X</b> .	
(2) communications between tank gauger and pumping station?	X	
G. Are leaks from tank seams, gaskets, rivets and bolt immediately repaired?	X	
VI. Transfer Operations, Pumping and In-plant Proces  Does the SPCC Plan address the followin	The control of the second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second second seco	12.7)
A. Are buried pipelines cathodically protected?	X	
B. Are out-of-service pipelines properly closed, capped or blank-flanged and properly labeled?	X	
C. Are aboveground pipe supports properly designed to minimize:	X·	
(1) abrasion and corrosion?		-
(2) expansion and contraction?	X	

D.	Do personnel check the conditions of pipelines, including flange and expansion joints, valves, drip pans, pipeline supports, locking of valves and metal surfaces?	Х	
E.	Are pipelines periodically pressure tested?	X	·
F.	Is vehicular traffic controlled near aboveground pipelines?	X	
	VII. Tank Car and Tank Truck Loading/Unloading R	ack (40 CFR 1	12.7)
	Does the Plan address the following issu	ies:	E
Α.	Do loading/unloading procedures meet Department of Transportation regulations?	Yes X	No
В.	Is the secondary containment for the loading area designed to hold at least the largest single compartment of a tanker truck?	X	·
C.	Are written procedures in place to ensure transfer lines are disconnected prior to vehicular departure?	<b>X</b>	
	VIII. Inspections and Records (40 CFF	R 112.7)	
	Does the Plan include a copy of:		
A.	written inspections procedures to be followed by personnel?	X	
B.	records of inspections for the past three years?	X	
	IX. Security (40 CFR 112.7)		
	Does the Plan discuss:		
A.	the need for security, such as full fencing, locking of entrance gates and/or guards?	X - Annex	
В.	the security for all master flow and drain valves which would permit direct outward flow of a tank's contents?	Х	
C.	how product pump starter controls are locked or limit accessibility when not operating?	X	
C.	the need for capping or installing blank flanges in loading/unloading pipelines when they are not in full service or are in standby service?	X	

D.	the adequacy of facility lighting to facilitate discovery of spills and prevention of vandalism?	X	
x.	Personnel, Training and Spill Prevention Procedures (40	CFR 112.7)	
<u>asmiral</u>		Yes	No
Α.	Does the Plan contain a training program for personnel responsible for:	-	
	(1) operation and maintenance of equipment?	X	
÷	(2) preventing discharges of oil and complying with pollution control laws, rules and regulations?	Х	
	(3) spill response?	X	
В.	Has a person been given responsibility for spill prevention?		
	Name: QI. Frank Signoriello / AQI James Lintz	· .	
	Title: Terminal Superintendent / Complex Manager		
	Telephone No.: 718-383-4066 / 203-520-0403	<del></del>	·
<b>X</b> 1	. Facility Response Plan (40 CFR 112.20)		
	Does the facility have a Facility Response Plan approved by the USCG/USEPA? Date of the latest FRP: Latest update 10/2009, last EPA Inspection 9/29/10	X	
	Date last FRP Drill Performed? 9/9/10		

# **SECTION B**

# FEDERAL UNDERGROUND STORAGE TANK REGULATIONS Environmental Compliance Report

This report address compliance with certain sections of the USEPA Underground Storage Tank Regulations (40 CFR Part 280)

Regulations (40 CFR Part 280)					
I. Tank Number A. What is the tank	Tank#	Tank#	Tanke#	Tank#	Tank#
identification number on the facility information sheet? For additional tanks, use extra copies of this form.	None				
B. Is tank leak detection performed? (Required by 40 CFR Part 280.40) Y/N					
C. Is tank protected from corrosion? (Required by 40 CFR Part 280.21) Y/N					·
D. Does the tank have a spill catchment basin? (Required by 40 CFR Part 280.21[d]) Y/N					
E. Does the tank have an overfill prevention device such as an automatic shutoff device, overfill alarm or float vent valve? (Required by 40 CFR Part 280.21[d]).  Y/N					
F. If the tank has undergone permanent closure since 12/22/88, was a site assessment performed at the time of closure? (Required by 40 CFR Part 280.72)  Y/N					
II. Underground Piping					

A. Do pressurized piping systems have a line leak detector? (Required by 40 CFR Part 280.41[b]) Y/N			
B. Is pipe leak detection being performed? (Required by 40 CFR 280.41(b)) Y/N			
- Do pressurized piping systems have an additional form of leak detection?			
- Do suction systems have a form of leak detection, if exempt from the leak detection requirements. Y/N	,		
C. Is the product piping protected from corrosion? (Required by 40 CFR Part 280.21[c]) Y/N			

# **SECTION C**

# NYS PETROLEUM BULK STORAGE REGULATIONS Environmental Compliance Report

This section of the report addresses compliance with certain sections of the New York State Petroleum Bulk Storage (PBS) Regulations (6 NYCRR Part 613 and 614).

PBS Regulations (6 NYCRR Parts 613 and 614)					
Underground and Aboveground Tanks					
	Yes Yes				
1. Are monitoring wells marked and secured?	X	4 se			
Tank Number	Fank #	Tank #	Tank #	Tank #	Tank #
For additional tanks, use extra copies of this form:	41	42	43	44	45
If tanks are temporarily out-of-service, have they been temporarily closed properly? Y/N/NA	N/A	N/A	N/A	N/A	N/A
Were any unreported spills observed during the inspection?     Y/N     If yes, explain on separate sheet.	N	N	N	N	N
4. For underground tanks: have tank top and dispenser sumps and fill port catch basins been properly maintained?  Y/N (accumulation of product) / 1 (poor condition)	N/A	N/A	N/A	N/A	N/A
5. Are the <b>fill ports color coded</b> to identify the product in the tank? See 613.3(b). Y/N/NA	Y	Y	Y	Y	Y
6. Are the motor fuel tanks with pressurized piping equipped with <b>shear valves</b> .  Y/N/NA/1(Inoperative)	N/A	.N/A	N/A	N/A	N/A

Underground Tanks					
Tank Number For additional tanks, use extra copies of this form.	Tank #	Tank #	Tank #	Tank #	Tank #
<ol> <li>Do the tanks installed after 12/86 comply with the new tank system standards? Y/N/NA         If no, identify the missing item(s)?         (1) corrosion resistant, (2) secondary containment, (3) leak monitoring, (4) overfill prevention (auto shut-off valve, high level alarm or ball float valve) and have (5) corrosion resistant piping with (6) leak monitoring (line leak detector for pressurized piping) or (7) only having one check valve under the pump in suction piping system (8) tank label (9) as built plans or drawings.     </li> </ol>					
8. Is leak monitoring (UST) being performed? Y/N Identify the method(s). 1 (wall tank - interstice is checked) / 2 (inoperative system) / 3 (monitoring records not maintained) / 4 (inappropriate method)	,				
9. Is the cathodic protection for steel UST and piping systems monitored annually? Y/N If no, identify the missing cathodic protection. N (missing both) / 1 (no monitoring on tank) / 2 (no monitoring on line) / 3 (records not maintained) / 4 (system not					
maintained to achieve protection) / 5 (inadequate method)					
10. Are <b>inventory records</b> for metered UST systems being properly maintained and reconciled?					·
Mark (1) for no records, (2) for poor equipment, (3) for no Reconciliation. (4) for reconciliation performed other than 10 days					
11. Do unmetered tanks have annual standpipe, or tank test or other leak detect method? Y/N	e e e e e e e e e e e e e e e e e e e				
12. Has a <b>tightness testing</b> (USTs) been conducted on the tank and piping system? Y/N	·				
Check for both tank and piping. Y/N/1(entire tank not tested) / 2 (no test on line)					

*					
Ahoveground Tanks					
Tank Number	Tank	Tank	Tank	Tank	Tank
For additional tanks use extra copies of this form:	#	#	#	#	#
	41	42	43	44	45
13. For the tanks installed after 12/86, do they meet the new tank system standards? Y/N/NA	N/A	N/A '	N/A	N/A	N/A
If no, identify missing items? <b>ASTs</b> must be (1)welded steel with adequate (2) surface coating (paint), if on soil have (3) cathodic protection and if on grade have an (4) impermeable barrier under the tank with the ability to (5)monitor for leaks.					
14. Are monthly inspections for all ASTs performed? Y/N/1 (records not maintained)	Y	Y	Y	Y	Y
15. Are ten year inspections for ASTs performed? Y/N/X/1 (records not maintained)		Y	Y	Y	Y
16. Secondary containment  Does the secondary containment systems comply with the requirements found in Part 613 and Part 614? Y/N  If no, explain on separate sheet.	Y	Y	Y	Y	Y
17. Are the dike drain valves locked in a closed position Y/N/NA		Y	Y	Y	Y
18. Are the ASTs equipped with a gauge, high level alarm or other equivalent device? Y/N/ 1(inoperative)	Y	. <b>Y</b>	Ÿ	Y	Y
19. Are the ASTs marked with the design/working capacity, and identification number? Y/N		Y	Y	Y	Y
20. Is a solenoid or equivalent valve in place for gravity-fed motor fuel dispensers Y/N/1(inoperative)/X (not applicable)	X	X	X	X	X
21. Is there a check valve in place for pump-filled tanks with remote fills?  Y/N/ 1(inoperative)/ X (not applicable)	Y	Y	Y	Y	Y

# **SECTION C**

# NYS PETROLEUM BULK STORAGE REGULATIONS Environmental Compliance Report

This section of the report addresses compliance with certain sections of the New York State Petroleum Bulk Storage (PBS) Regulations (6 NYCRR Part 613 and 614).

PBS Regulations (6/NYCRR Parts 613 and 614) Underground and Aboveground Tanks							
1. Are monitoring wells marked and secured?	x						
Fank Number	Tank #	Tank #	Tank	Tank #	Tank		
For additional tanks, use extra copies of this form,	· 46	47	48	49	50		
If tanks are temporarily out-of-service, have they been temporarily closed properly? Y/N/NA	N/A	N/A	N/A	N/A	N/A		
3. Were any unreported spills observed during the inspection? Y/N  If yes, explain on separate sheet.		N	N	N	N		
4. For underground tanks: have tank top and dispenser sumps and fill port catch basins been properly maintained? Y/N (accumulation of product) / 1 (poor condition)		N/A	N/A	N/A	N/A		
5. Are the <b>fill ports color coded</b> to identify the product in the tank? See 613.3(b). Y/N/NA	Y	Y	Y	Y	Y		
6. Are the motor fuel tanks with pressurized piping equipped with shear valves. Y/N/NA/1(Inoperative)	N/A	N/A	N/A	N/A	N/A		

Aboveground Tanks			T.		
Tank Number For additional tanks use extra copies of this form.	Tank #	Tank #	Tank #	Tank #	Tank #
	46	47	48	49	50
13. For the tanks installed after 12/86, do they meet the new tank system standards? Y/N/NA	N/A	N/A	N/A	N/A	N/A
If no, identify missing items? <b>ASTs</b> must be (1)welded steel with adequate (2) surface coating (paint), if on soil have (3) cathodic protection and if on grade have an (4) impermeable barrier under the tank with the ability to (5)monitor for leaks.					
14. Are monthly inspections for all ASTs performed? Y/N/1 (records not maintained)	Ý	Y	Y	Y	Y
15. Are ten year inspections for ASTs performed? Y/N/X/1 (records not maintained)	Y	Y	Y	Y	Y
16. Secondary containment  Does the secondary containment systems comply with the requirements found in Part 613 and Part 614? Y/N  If no, explain on separate sheet.	Y	Y	Y	Y	Y
17. Are the dike drain valves locked in a closed position Y/N/NA		Y	Y	Y	Y
18. Are the ASTs equipped with a gauge, high level alarm or other equivalent device? Y/N/ 1(inoperative)	Y	Y	Y	Y	Y
19. Are the ASTs marked with the design/working capacity, and identification number? Y/N	Y	Y	Y	Y	Y
20. Is a <b>solenoid</b> or equivalent valve in place for gravity-fed motor fuel dispensers Y/N/1(inoperative)/X (not applicable)	X	X	X	X	X
21. Is there a <b>check valve</b> in place for pump-filled tanks with remote fills? Y/N/1(inoperative)/ X (not applicable)	Y	Y	Y	Y	Y

# **SECTION C**

# NYS PETROLEUM BULK STORAGE REGULATIONS Environmental Compliance Report

This section of the report addresses compliance with certain sections of the New York State Petroleum Bulk Storage (PBS) Regulations (6 NYCRR Part 613 and 614).

PBS Regulations (6 NYCRR Parts 613 and 614)		u e				
Underground and Aboveground Tanks	•					
	Yes Yes			es		
1. Are monitoring wells marked and secured?	X					
Tank Number	Tank #	Tank #	Tan #	C Tank	Tank #	
For additional tanks, use extra copies of this form.	55					
2. If tanks are temporarily out-of-service, have they been temporarily closed properly? Y/N/NA	Y					
3. Were any unreported spills observed during the inspection? Y/N If yes, explain on separate sheet.	N					
4. For underground tanks: have tank top and dispenser sumps and fill port catch basins been properly maintained?  Y/N (accumulation of product) / 1 (poor condition)	N/A					
5. Are the <b>fill ports color coded</b> to identify the product in the tank? See 613.3(b). Y/N/NA	Y					
6. Are the motor fuel tanks with pressurized piping equipped with shear valves? Y/N/NA/1(Inoperative)	N/A					

Aboveground lanks					
Tank Number For additional tanks use extra copies of this form.	Tank #	Tank #	Tank.	Tank #	Tank
	55				` ,
13. For the tanks installed after 12/86, do they meet the new tank system standards? Y/N/NA	Y				
If no, identify missing items? <b>ASTs</b> must be (1)welded steel with adequate (2) surface coating (paint), if on soil have (3) cathodic protection and if on grade have an (4) impermeable barrier under the tank with the ability to (5)monitor for leaks.					
14. Are monthly inspections for all ASTs performed? Y/N/1 (records not maintained)	Y				
15. Are ten year inspections for ASTs performed? Y/N/X/1 (records not maintained)	Y				
16. Secondary containment  Does the secondary containment systems comply with the requirements found in Part 613 and Part 614? Y/N  If no, explain on separate sheet.	Y				
17. Are the dike drain valves locked in a closed position Y/N/NA	Y				
18. Are the ASTs equipped with a gauge, high level alarm or other equivalent device? Y/N/1(inoperative)	Y				
19. Are the ASTs marked with the design/working capacity, and identification number? Y/N	Y				
20. Is a <b>solenoid</b> or equivalent valve in place for gravity-fed motor fuel dispensers Y/N/1(inoperative)/ X (not applicable)	X				
21. Is there a <b>check valve</b> in place for pump-filled tanks with remote fills? Y/N/1(inoperative)/ X (not applicable)	Y				

#### **SECTION D**

# ONSHORE MAJOR OIL STORAGE FACILITY LICENSING CONDITIONS Environmental Compliance Report

This section of the report addresses licensing conditions applicable to your facility regulated under Article 12 of the New York Navigation Law. N/A A. Closure Plan 1. If the facility is inactive, was a closure plan submitted to the Department? Date: 2. Did the Department approve of the closure plan? N/A 3. Are any of the aboveground tanks considered temporarily or permanently N/A closed? If yes, explain on a separate sheet. Y B. Monitoring Wells and Sampling 1. Has the Department approved the monitoring well system? 2. Has a baseline assessment of groundwater quality been completed? Y 3. Are wells monitored monthly? Y 4. Are wells monitored biannually? 5. Are wells monitored annually? 6. Are sampling results forwarded to the Department's Regional Office? X annually June 30 biannually monthly Y C. Secondary Containment 1. Have secondary containment systems been tested for permeability? Y 2. Has a detailed description of the secondary containment systems been submitted to the Department? 3. Do all secondary containment systems meet the Department's standards Y 613.3(c)(6)? If no, explain on separate sheet.

4. Was a five year in-depth secondary containment system integrity	Y	
inspection performed? Date of last inspection: Sept. 2008 2010 Inspection in progress, report pending.	Y	
Was the inspection approved by the Department?		
If no, explain on a separate sheet: Report Submitted Approval Pending		
5. Does the Plan evaluate groundwater geology, hydrology, contamination and risks?	Y	
6. If secondary containment systems do not meet standards set forth in 613.3(c)(6), have engineering plans been submitted to the Department?	N/A	
7. Has the Department approved the engineering plans?	N/A	
D. Site Map	Y	
Has a site map acceptable to the Department been prepared?		
E. Variance.	Yes	No
Has the Department granted a variance?		X
If yes, is the facility in compliance with the variance?	N/A	
F. Violations  Were any violations to Federal, State and county, local regulations, codes and license conditions cited during the last five years?		X
If yes, explain on a separate sheet.		
G. Additional Licensing Requirements	X	
1. Have accurate monthly reports on the number of barrels transferred at the facility been submitted to the Department each month?	- Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andread - Andr	
2. Have monthly license fees and surcharges been paid to the Department?	x	

# BEST MANAGEMENT PRACTICES & STORMWATER POLLUTION PREVENTION PLAN

# **MOTIVA ENTERPRISES LLC**

# **BROOKLYN TERMINAL**

Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222

Tel. (718) 383-4066

# **FACILITY INFORMATION PAGE**

# Facility Information:

- Facilities Addressed in this Plan:
- · Name & Address of Owner:
- Designated person accountable for the implementation of this Plan at the facility sated above:

Owner/Operator - Motiva Enterprises LLC

Brooklyn Terminal

Motiva Enterprises LLC 910 Louisiana Street Houston, TX 77002

James W. Lintz – Terminal Manager Brooklyn Terminal 25 Paidge Avenue Brooklyn, NY 11222

Tel. (718) 383-4066

# STORMWATER POLLUTION PREVENTION PLAN

# **REVISION RECORD**

**Note:** It is the responsibility of the holder of this plan to insure that all changes and updates are made. The holder should:

- Remove and discard obsolete pages.
- Replace obsolete pages with updated pages.
- · Record each revision on this form.

Change Date	Affected Pages Numbers	Description of Change(s)	Name				
July 2000	Entire Plan	Update per SPDES Permit	D. Bier				
Oct. 26, 2004	Entire Plan	Review of Terminal & Operational changes – None needed at this time.					
July 2009	Cover, ii, v,	Update	D. Bier				
			-				
	·						
			,				
	·						
	EXAMPLE						
01/01/99	1-1 thru 1-4; 5-2	Update					

Motiva Enterprises LLC Brooklyn Terminal

3-1

BMP/SWPPP 2009 Update

#### 2.0 GENERAL INFORMATION

#### 2.1 TYPE OF FACILITY

The facility is an onshore storage terminal that receives and distributes gasoline, ethanol and gasoline additives. Specific facility information is provided in the terminal's Integrated Contingency Plan (ICP).

#### 2.2 POLLUTION PREVENTION TEAM

The Terminal Manager assumes the responsibility for implementation, maintenance and revision of the BMP/SWPP Plan. The Terminal Manager and Terminal Superintendent/Supervisor serve as members of the BMP/Stormwater Pollution Prevention Team. Additional terminal and environmental personnel as designated by the Terminal Manager will assist in the development and implementation of the BMP/SWPP Plan as necessary. Emergency Contacts for the Terminal are provided in the ICP. Roles and responsibilities of the company responders are also detailed in the ICP.

#### 2.3 EXTERNAL CONTACTS

The Facility will ensure that required notifications are made to federal, state and local agencies when appropriate. Internal and External Reporting requirements are outlined in the ICP.

#### 2.4 SURFACE WATER PROXIMITY

The Facility is positioned adjacent to the Newtown Creek. The Newtown Creek empties into the East River. Maps and charts of the surface water bodies are incorporated in to the ICP.

#### 2.5 SURFACE DRAINAGE

The facility is located on a relatively flat area. Drainage from the contained areas is addressed below. The Terminal Spill Prevention Control and Countermeasure (SPCC) Plan (the SPCC Plan is part of the ICP) also addresses the rate and direction of flow from potential spill areas. Rainfall onto the soil surfaces outside of the Terminal's operational area infiltrates into the soil or flows toward the Terminal's operational areas. All operational areas of the Terminal drain to the oil/water separator for treatment prior to discharge from the SPDES Discharge No. 001. Effluent monitoring is conducted for the following parameters:

- Flow
- Oil & Grease
- Hq •
- Benzene, Toluene, Ethylbenzene, Xylene(s) and MTBE

#### **Drainage from Diked Areas**

 The drainage from the diked storage areas is controlled by individual manual valves that are kept closed except when draining stormwater to the oil/water separator. The diked containment basins are isolated from the adjacent basins by dikes and the

Motiva Enterprises LLC Brooklyn Terminal 3-1

BMP/SWPPP 2009 Update

#### 3.0 POTENTIAL POLLUTANT SOURCES

# 3.1 IDENTIFICATION OF POTENTIAL POLLUTANT SOURCES & BEST MANAGEMENT CONTROLS

There is limited potential for the materials stored or processed on site to impact surface waters since most of the materials are contained within closed systems, such as tanks, pipes and other equipment. The significant materials that are handled and/or stored at the Terminal include: gasoline, ethanol and gasoline additives. In addition to these materials, small amounts of maintenance related materials are stored and used. These materials are stored inside buildings to prevent any contact with stormwater. Diesel fuel is not stored at the Terminal, but is contained in fuel tanks of the trucks that load at the Terminal. Figure 3.1 below is a narrative description of the materials, how the materials are handled and the Materials Management Practices (BMPs) empolyed to reduce the potential of these sources to contribute pollutants to stormwater discharges.

#### 3.2 SPILLS & LEAKS

There have been no spills of toxic or hazardous substances by Motiva Enterprises at the Terminal. Spills that occur are reported and are to be documented as prescribed in the ICP. Please see the ICP for a listing of any potential spills or leaks.

#### 3.3 MONITORING PROGRAM

Stormwater is monitored in accordance with the Terminal's SPDES Permit (No. NY0006131). Sampling data is reported in the monthly Discharge Monitoring Reports (DMRs) with copies of the reports and data kept in the Terminal's files. The monitoring parameters are noted in Section 2.5 of this plan.

Motiva Enterprises LLC Brooklyn Terminal

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1 OF 1

JENNIFER BOTHWELL
860-749-2839
MOTIVA ENTERPRISES LLC
35-31 TALCOTTVILLE RD
VERNON CT 06066

SHIP TO:
BUREAU OF TECHNICAL SUPPORT
NYSDEC
11TH FLOOR
625 BROADWAY
ALBANY NY 12207-2942

NY 122 9



NY 122 9-01

UPS NEXT DAY AIR SAVER 1P
TRACKING #: 1Z 71E 42V 13 9039 5114



BILLING: P/P

Reference#1: Brooklyn CBS Renewal

IS 12.5.10. WINTIE70 06.0A 07/2010



Shell/Motiva 0009393

#### Bothwell, Jennifer L MOTIVA-DVM/251

From: Sent: To: UPS Quantum View [auto-notify@ups.com] Monday, October 25, 2010 10:47 AM Bothwell, Jennifer L MOTIVA-DVM/251

Subject:

UPS Delivery Notification, Tracking Number 1Z71E42V1390395114

×

***Do not reply to this e-mail. UPS and Motiva Enterprises LLC will not receive your reply.

At the request of Motiva Enterprises LLC, this notice is to confirm that the following shipment has been delivered.

**Important Delivery Information** 

#### Message from Motiva Enterprises LLC:

The package has been delivered.

**Tracking Number:** 1Z71E42V1390395114

Delivery Date / Time: 25-October-2010 / 10:06 AM

**Delivery Location: RECEIVER** 

Signed by: FULLER

**Shipment Detail** 

Ship To:

Bureau of Technical Support

NYSDEC

625 BROADWAY

ALBANY

NY

12207

US

Number of Packages 1

**UPS Service:** 

**NEXT DAY AIR SAVER** 

Weight:

2.0 LBS

Reference Number 1: Brooklyn CBS Renewal